625 Liberty Ave, Suite 1700
Pittsburgh PA 15222
www.eqt.com

TEL: (412) 395-3699
FAX: (412) 395-2156

Alex Bosiljevac
Environmental Coordinator

April 27, 2016

CERTIFIED MAIL # 7015 1660 0000 9399 6062

Mr. William F. Durham, Director
West Virginia Department of Environmental Protection
Division of Air Quality
601 57th Street, SE
Charleston, West Virginia, 25304

RE: G70B Permit Application
EQT Production Company
OXF-157 Natural Gas Production Site
Facility ID No. 017-00139

Dear Mr. Durham,

Enclosed are two electronic copies and one original hard copy of a proposed application for a G70-B General Air Permit for the OXF-157 Natural Gas Production Well Site. The site currently operates under a G70-A General Air Permit (G70-A112A). Please note that this application satisfies a requirement in Consent Order CO-R13-E-2016-04, in which EQT Production Company is required to submit an application with the equipment specified in the consent order. A legal advertisement will be published in the next few days and proof of publication will be forwarded as soon as it is received. Please contact me for payment of the application fee by credit card.

If you have any questions concerning this permit application, please contact me at (412) 395-3699 or by email at abosiljevac@eqt.com.

Sincerely,

Alex Bosiljevac
EQT Corporation

Enclosures

EQT Production Company

G70-B General Permit Registration Application

OXF 157 Natural Gas Production Site

Permit No. G70-A112A

West Union, West Virginia

Prepared By:

ENVIRONMENTAL RESOURCES MANAGEMENT, Inc.
Hurricane, West Virginia

April 2016

INTRODUCTION

EQT Production Company (EQT) is submitting this G70-B General Permit Registration to the WVDEP's Department of Air Quality to receive the authority to operate new units at the OXF-157 facility, currently permitted under G70-A112A. The site is located in Doddridge County, West Virginia. This application addresses the operational activities associated with the production of natural gas and condensates at the OXF-157 pad.

FACILITY DESCRIPTION

The EQT OXF-157 natural gas production site operates in Doddridge County, WV and consists of seven (7) natural gas wells. Natural gas and liquids (including water and condensates) are extracted from underground deposits. The natural gas is transported from the wells to a gas line for compression and additional processing, as necessary. The produced liquids are stored in storage vessels.

The applicant is currently authorized to operate the following:

- Seven (7) natural gas wells;
- Ten (10) 400 barrel (bbl) tanks for storage of condensate and water;
- Two (2) thermoelectric generator (TEG) each rated at 0.013 MMBtu/hr heat input;
- Two (2) enclosed combustion devices each with a capacity of 11.66 MMBtu/hr heat input;
- Two (2) line heaters each rated at 4.50 MMBtu/hr heat input;
- One (1) line heater rated at 1.00 MMBtu/hr heat input; and
- One (1) 140 bbl sand trap blowdown tank for storage of condensate and water.

The applicant seeks to authorize the operation of:

- One (1) 110 HP stationary natural gas compressor engine;
- One (1) line heater rated at 1.15 MMBtu/hr heat input; and
- One (1) line heater rated at 1.54 MMBtu/hr heat input.

The applicant seeks to authorize the removal of:

- One (1) line heater rated at 1.00 MMBtu/hr heat input.

A process flow diagram is included in this application in Attachment D.

STATEMENT OF AGGREGATION

The OXF-157 pad is located in Doddridge County, WV and operated by EQT Production Company. Stationary sources of air pollutants may require aggregation of total emission levels if these sources share the same industrial grouping, are operating under common control, and are classified as contiguous or adjacent properties. EQT operates the OXF-157 with the same industrial grouping as nearby facilities, and some of these facilities are under common control. EQT, however, is not subject to the aggregation of stationary emission sources because these sites do not meet the definition of contiguous or adjacent facilities.

The OXF-157 pad operates under SIC code 1311 (Crude Petroleum and Natural Gas Extraction). There are surrounding wells and compressor stations operated by EQT that share the same two-digit major SIC code of 13 for Crude Petroleum and Natural Gas Extraction. Therefore, the OXF-157 pad does share the same SIC codes as the surrounding wells and compressor stations.

EQT Production Company is the sole operator of the OXF-157 pad. EQT is also the sole operator of other production sites and compressor stations in the area. Therefore, EQT does qualify as having nearby operations under common control.

There are no EQT owned or operated sites within a one (1) mile radius of the OXF-157 pad. EQT's WEU-51 Natural Gas Production site is 1.4 miles north of the OXF-157 pad. Nearby sites do not meet the definition of contiguous or adjacent properties since they are not in contact and do not share a common boundary. Operations conducted at the OXF-157 site do not rely on or interact with other sites. Furthermore, operations separated by this distance do not meet the common sense notion of a "plant."

On August 18, 2015 the EPA Administrator signed the *Source Determination for Certain Emission Units in the Oil and Natural Gas Sector*. This notice is to clarify how properties in the oil and natural gas sector are determined to be adjacent in order to assist permitting authorities and permit applicants in making consistent source determinations. The following proposed regulatory text defines "adjacent" for the oil and gas sector in terms of proximity.

> *Pollutant emitting activities shall be considered adjacent if they are located on the same surface site, or on surface sites that are located within ¼ mile of one another.*

The OXF-157 and WEU-51 pads are located on surface sites located greater than EPA's ¼ mile proposed ruling. Although the applicant notes the proposed status of this adjacency determination, it is the only guidance available on a

finite distance impacting the adjacency determination, and has been noted due to lack of finalized guidance. Based upon the proximity of nearby facilities, EQT does not believe aggregation based upon adjacency is required.

Based on the above reasoning, EQT is not subject to the aggregation of stationary emission sources since the stationary sources are not considered contiguous or adjacent facilities.

REGULATORY DISCUSSION

This section outlines the State air quality regulations that could be reasonably expected to apply to the OXF-157 pad and makes an applicability determination for each regulation based on activities conducted at the site and the emissions of regulated air pollutants. This review is presented to supplement and/or add clarification to the information provided in the WVDEP G70-B permit application forms.

The West Virginia State Regulations address federal regulations, including Prevention of Significant Deterioration permitting, Title V permitting, New Source Performance Standards, and National Emission Standards for Hazardous Air Pollutants. The regulatory requirements in reference to OXF-157 are described in detail in the below section.

WEST VIRGINIA STATE AIR REGULATIONS

45 CSR 02 – To Prevent and Control Particulate Air Pollution from Combustion of Fuel in Indirect Heat Exchangers

The line heaters are indirect heat exchangers that combust natural gas but are exempt since the heat input capacities are less than 10 MMBtu/hr.

45 CSR 04 – To Prevent and Control the Discharge of Air Pollutants into the Air Which Causes or Contributes to an Objectionable Odor

Operations conducted at the OXF-157 wellpad are subject to this requirement. Based on the nature of the process at the wellpad, the presence of objectionable odors is unlikely.

45 CSR 06 – Control of Air Pollution from the Combustion of Refuse

The enclosed combustion device located on the OXF-157 natural gas production site is subject to this regulation. Per 45 CSR 6-4.3, opacity of emissions from the enclosed combustion device shall not exceed 20 percent, except as provided by

4.4. Particulate matter emissions from this unit will not exceed the levels calculated in accordance with 6-4.1.

§45-6-4.1 Determination for Maximum Allowable Particulate Emissions

Emissions (lb/hr) = F x Incinerator Capacity (tons/hr)

Incinerator Capacity = 0.12 tons per hour or 245 lbs/hr

ρNG = 0.042 lb/scf – Density of NG from EPA AP42 – Sections 1.4 and 3.2 (NG combustion)

$$\frac{140{,}000\ scf}{day} * \frac{1\ day}{24\ hours} * \frac{0.042\ lb}{scf} = \frac{245\ lb}{hr} = \frac{1{,}073\ tons}{year}$$

If the Incinerator Capacity is less than 15,000 lbs/hr, then F = 5.43

F = 5.43 * (0.12 tons per hour)

F = 0.67 lbs / hour

The enclosed combustion devices utilize AP-42 Section 1.4 PM emission factors to determine emissions from the combustion of refuse natural gas. Based upon the type of fuel combusted and the emission factors utilized, the PM emissions from the enclosed combustion devices will be well below the maximum allowable particulate emissions mandated by 45 CSR 06.

45 CSR 10 – To Prevent and Control Air Pollution from the Emission of Sulfur Oxides

The line heaters are indirect heat exchangers that combust natural gas but are exempt since the heat input capacities are less than 10 MMBtu/hr.

45 CSR 13 – Permits for Construction, Modification, Relocation, and Operation of Stationary Sources of Air Pollutants

This G70-B permit application is being submitted for the operational activities associated with EQT's production of natural gas.

45 CSR 14 – Permits for Construction and Major Modification of Major Stationary Sources of Air Pollution for the Prevention of Significant Deterioration

Federal construction permitting programs regulate new and modified sources of attainment pollutants under Prevention of Significant Deterioration (PSD). The G70B-applicability criterion excludes facilities that meet the definition of a major source as defined in 45 CSR 19 for being eligible for the general permit.

Operation of equipment at the OXF-157 pad will not exceed emission thresholds established by this permitting program. EQT will monitor future construction and modification activities at the site closely and will compare future increase in emissions with the PSD thresholds to ensure these activities will not trigger this program.

45 CSR 16 - Standards of Performance for New Stationary Sources (NSPS)

45CSR 16 applies to registrants that are subject to NSPS requirements described in more detail in the Federal Regulations section. Applicable requirements of NSPS, Subpart JJJJ and OOOO are included in the G70-B general permit.

This facility is expected to contain gas well affected facilities under Subpart OOOO. This facility will contain a spark ignition internal combustion engine subject to Subpart JJJJ. No additional NSPS are applicable for this facility. Additional discussion is provided in the Federal Regulation Discussion of this permit application.

45 CS R19 – Permits for Construction and Major Modification of Major Stationary Sources of Air Pollution which Cause or Contributed to Non-attainment

Federal construction permitting programs regulate new and modified sources of non-attainment pollutants under Non-Attainment New Source Review (NNSR). The G70-B applicability criterion excludes facilities that meet the definition of a major source as defined in 45 CSR 19 for being eligible for the general permit.

Operation of equipment at the OXF-157 pad will not exceed emission thresholds established by either of these permitting programs. EQT will monitor future construction and modification activities at the site closely and will compare future increase in emissions with the NSR thresholds to ensure these activities will not trigger this program.

45 CSR 25 – Control of Air Pollution from Hazardous Waste Treatment, Storage, and Disposal Facilities

No hazardous waste will be burnt at this well site; therefore, it is not subject to this hazardous waste rule.

45 CSR 30 – Requirements for Operating Permits

45 CSR 30 applies to the requirements of the federal Title V operating permit program (40 CFR 70). The major source thresholds with respect to the West Virginia Title V operating permit program regulations are 10 tons per year (tpy) of a single HAP, 25 tpy of any combination of HAP, and 100 tpy of other regulated pollutants.

The potential emissions of regulated pollutants are below the corresponding threshold(s) at this facility after the proposed project. Therefore, the wellpad is not a major source for Title V purposes.

45 CSR 34 – National Emission Standards for Hazardous Air Pollutants (NESHAP)

45 CSR 34 applies to registrants that are subject to NESHAP requirements. Excluded from G70-B general permit eligibility are sources that are subject to NESHAP Subpart HHH.

The following NESHAP included in the G70-B permit are not subject to the OXF-157 facility:

- 40CFR63 Subpart HH (National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities).

FEDERAL REGULATIONS

40 CFR 60 Subpart JJJJ (Standards of Performance for Stationary Spark Ignition Internal Combustion Engines).

Subpart JJJJ sets forth nitrogen oxides (NOx), carbon monoxide (CO), and volatile organic compound (VOC) emission limits, fuel requirements, installation requirements, and monitoring requirements based on the year of installation of the subject internal combustion engine.

The Ford CSG-637 is a 110 HP EPA Certified 4 stroke rich burn (4SRB) spark ignition (SI) engine manufactured in 2015. Per 40CFR60.4230(a)(4)(iii), an engine manufactured on or after July 1, 2008 with a maximum engine power less than 500 HP must comply with the provisions of 40 CFR 60 Subpart JJJJ.

Emission standards contained in the EPA Certificate of Conformity issued to this engine conform to 40 CFR 60 Subpart JJJJ Table 1 - NOx, CO, VOC Emissions Standards for Stationary Non-Emergency SI Engines greater than 100 HP. Therefore, per 40CFR60.4243(a)(1), EQT must operate and maintain the certified stationary SI internal combustion engine and control device according to the manufacturer's emission-related written instructions to ensure applicable emission standards outlined in Part 60 Subpart JJJJ Table 1 are maintained. Additionally, performance testing is not required.

40 CFR 60 Subpart OOOO (Standards of Performance for Crude oil and Natural Gas Production, Transmission and Distribution)

EPA published the NSPS for the oil and gas sector on August 16, 2012. EPA published final amendments to the subpart on September 23, 2013.

Subpart OOOO establishes emission standards and compliance schedules for the control of volatile organic compounds (VOC) and sulfur dioxide (SO_2) emissions from affected facilities that commence construction, modification or reconstruction after August 23, 2011. The applicable provisions and requirements of Subpart OOOO are included under the G70-B permit.

The only affected facilities expected to be subject to Subpart OOOO located at the OXF-157 production pad are listed below:

- Each gas well affected facility, which is a single natural gas well.

There are several equipment types that will be installed at OXF-157 that do not meet the affected facility definitions as specified by EPA. These include pneumatic controllers and storage vessels.

> Pneumatic Controllers: Pneumatic controllers installed at this facility will be intermittent bleed rate devices. Therefore, there will not pneumatic controller affected facilities located at this site.
>
> Storage vessels: Based on PTE calculations included within this permit, each storage vessel will be manifolded and routed to an enclosed combustion device such that emissions from each of these tanks are expected to be below 6 tons per year (tpy) of VOC. Therefore, these tanks will not be considered group 2 storage vessel affected facilities as specified in §60.5365(e).

No additional NSPS are expected to be applicable to this facility.

40CFR63 Subpart ZZZZ (National Emission Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines)

Subpart ZZZZ establishes national emission limitations and operating limitations for hazardous air pollutants (HAPs) emitted from stationary reciprocating internal combustion engines (RICE) located at major and area sources of HAP emissions. This Subpart also establishes requirements to demonstrate initial and continuous compliance with the emission limitations and operating limitations.

The Ford CSG-637 is a 110 HP EPA Certified 4 stroke rich burn (4SRB) spark ignition (SI) engine manufactured in 2015. The engine meets the requirements of 40 CFR 60 Subpart JJJJ. Per 40CFR63.6590(c)(1), no further requirements apply for a new stationary RICE located at an area source subject to regulation under 40 CFR 60 Subpart JJJJ.

No additional NESHAP are expected to be applicable to this facility.

General Permit G70-B will establish an emission cap on the following regulated and hazardous air pollutants:

Pollutant	Maximum Annual Emission Limit (tons/year)	OXF-157 Potential to Emit (PTE) (tons/year)
Nitrogen Oxides	50	14.51
Carbon Monoxide	80	13.46
Volatile Organic Compounds	80	4.08
Particulate Matter – 10/2.5	20	8.07
Sulfur Dioxide	20	0.08
Any Single Hazardous Air Pollutant	8	0.23 (as C_6H_{14})
Total Hazardous Air Pollutants	20	0.32

The fugitive emissions of a stationary source shall not be considered in determining whether it is a major stationary source for the purposes of 45CSR30-2.26.b or for eligibility of this General Permit.

west virginia department of environmental protection

Division of Air Quality
601 57th Street SE
Charleston, WV 25304
Phone (304) 926-0475
Fax (304) 926-0479
www.dep.wv.gov

G70-B GENERAL PERMIT REGISTRATION APPLICATION

PREVENTION AND CONTROL OF AIR POLLUTION IN REGARD TO THE CONSTRUCTION, MODIFICATION, RELOCATION, ADMINISTRATIVE UPDATE AND OPERATION OF NATURAL GAS PRODUCTION FACILITIES LOCATED AT THE WELL SITE

☐ CONSTRUCTION
☒ MODIFICATION
RELOCATION
CLASS I ADMINISTRATIVE UPDATE
CLASS II ADMINISTRATIVE UPDATE

SECTION 1. GENERAL INFORMATION

Name of Applicant (as registered with the WV Secretary of State's Office): **EQT Production Company**

Federal Employer ID No. (FEIN): **25-0724685**

Applicant's Mailing Address: **625 Liberty Avenue, Suite 1700**

City: **Pittsburgh**	State: **PA**	ZIP Code: **15222**

Facility Name: **OXF-157**

Operating Site Physical Address: **2520 Maxwell Ridge Road, West Union, WV 26456**
If none available, list road, city or town and zip of facility.

City: **West Union, WV**	Zip Code: **26456**	County: **Doddridge**

Latitude & Longitude Coordinates (NAD83, Decimal Degrees to 5 digits):
Latitude: **39.23609**
Longitude: **-80.76635**

SIC Code: **1311** NAICS Code: **211111**	DAQ Facility ID No. (For existing facilities) **017-00139**

CERTIFICATION OF INFORMATION

This G70-B General Permit Registration Application shall be signed below by a Responsible Official. A Responsible Official is a President, Vice President, Secretary, Treasurer, General Partner, General Manager, a member of the Board of Directors, or Owner, depending on business structure. A business may certify an Authorized Representative who shall have authority to bind the Corporation, Partnership, Limited Liability Company, Association, Joint Venture or Sole Proprietorship. Required records of daily throughput, hours of operation and maintenance, general correspondence, compliance certifications and all required notifications must be signed by a Responsible Official or an Authorized Representative. If a business wishes to certify an Authorized Representative, the official agreement below shall be checked off and the appropriate names and signatures entered. **Any administratively incomplete or improperly signed or unsigned G70-B Registration Application will be returned to the applicant. Furthermore, if the G70-B forms are not utilized, the application will be returned to the applicant. No substitution of forms is allowed.**

I hereby certify that is an Authorized Representative and in that capacity shall represent the interest of the business (e.g., Corporation, Partnership, Limited Liability Company, Association Joint Venture or Sole Proprietorship) and may obligate and legally bind the business. If the business changes its Authorized Representative, a Responsible Official shall notify the Director of the Division of Air Quality immediately.

I hereby certify that all information contained in this G70-B General Permit Registration Application and any supporting documents appended hereto is, to the best of my knowledge, true, accurate and complete, and that all reasonable efforts have been made to provide the most comprehensive information possible.

Responsible Official Signature: _____
Name and Title: **Kenneth Kirk - Executive Vice President** Phone: **(412)553-5700** Fax:
Email: **kkirk@eqt.com** Date: 4-27-2016

If applicable:
Authorized Representative Signature: _____
Name and Title: Phone: Fax:
Email: Date:

If applicable:
Environmental Contact **Alex Bosiljevac**
Name and Title: **Environmental Coordinator** Phone: **(412) 395-3699** Fax:
Email: **abosiljevac@eqt.com** Date:

OPERATING SITE INFORMATION
Briefly describe the proposed new operation and/or any change(s) to the facility: **EQT proposes the addition of one (1) 1.15 mmBtu/hr line heater and one (1) low pressure separator to regulate flashing emissions from produced fluids originating from the phase separators. The low pressure separator will be installed between the phase separators and produced fluid tanks. A natural gas compressor engine will be installed to compress the natural gas realized at the low pressure separator and directed to the sales pipeline. EQT also proposes the replacement of a 1.00 mmBtu/hr with a 1.54 mmBtu/hr.**
Directions to the facility: **While traveling Route 50 West at the town of West Union turn left onto WV State Route 18. Travel for about 2 miles and turn left onto Maxwell Ridge (Route 13). Continue for over 2.5 miles, and make a sharp onto Oil Well Rd. Follow Oil Well Road for 0.6 miles and make a left at the fork. Then travel for 0.2 miles and make a sharp left (next left available). After a quarter of a mile make a left. Continue for 0.5 miles and the facility will appear on your right.**

ATTACHMENTS AND SUPPORTING DOCUMENTS	
I have enclosed the following required documents:	
Check payable to WVDEP – Division of Air Quality with the appropriate application fee (per 45CSR13 and 45CSR22). ☐ Check attached to front of application. ☐ I wish to pay by electronic transfer. Contact for payment (incl. name and email address): ☒ I wish to pay by credit card. Contact for payment (incl. name and email address): **Alex Bosiljevac - abosiljevac@eqt.com** ☒$500 (Construction, Modification, and Relocation) ☐$300 (Class II Administrative Update) ☒$1,000 NSPS fee for 40 CFR60, Subpart IIII, JJJJ and/or OOOO [1] ☐$2,500 NESHAP fee for 40 CFR63, Subpart ZZZZ and/or HH [2] [1] Only one NSPS fee will apply. [2] Only one NESHAP fee will apply. The Subpart ZZZZ NESHAP fee will be waived for new engines that satisfy requirements by complying with NSPS, Subparts IIII and/or JJJJ. *NSPS and NESHAP fees apply to new construction or if the source is being modified.*	
☒ Responsible Official or Authorized Representative Signature (if applicable)	
☒ Single Source Determination Form **(must be completed in its entirety)** – Attachment A	
☐ Siting Criteria Waiver (if applicable) – Attachment B	☒ Current Business Certificate – Attachment C
☒ Process Flow Diagram – Attachment D	☒ Process Description – Attachment E
☒ Plot Plan – Attachment F	☒ Area Map – Attachment G
☒ G70-B Section Applicability Form – Attachment H	☒ Emission Units/ERD Table – Attachment I
☒ Fugitive Emissions Summary Sheet – Attachment J	
☒ Gas Well Affected Facility Data Sheet (if applicable) – Attachment K	
☒ Storage Vessel(s) Data Sheet (include gas sample data, USEPA Tanks, simulation software (e.g. ProMax, E&P Tanks, HYSYS, etc.), etc. where applicable) – Attachment L	
☒ Natural Gas Fired Fuel Burning Unit(s) Data Sheet (GPUs, Heater Treaters, In-Line Heaters if applicable) – Attachment M	
☒ Internal Combustion Engine Data Sheet(s) (include manufacturer performance data sheet(s) if applicable) – Attachment N	
☒ Tanker Truck Loading Data Sheet (if applicable) – Attachment O	
☐ Glycol Dehydration Unit Data Sheet(s) (include wet gas analysis, GRI- GLYCalc™ input and output reports and information on reboiler if applicable) – Attachment P	
☒ Pneumatic Controllers Data Sheet – Attachment Q	
☒ Air Pollution Control Device/Emission Reduction Device(s) Sheet(s) (include manufacturer performance data sheet(s) if applicable) – Attachment R	
☒ Emission Calculations (please be specific and include all calculation methodologies used) – Attachment S	
☒ Facility-wide Emission Summary Sheet(s) – Attachment T	
☒ Class I Legal Advertisement – Attachment U	
☒ One (1) paper copy and two (2) copies of CD or DVD with pdf copy of application and attachments	

All attachments must be identified by name, divided into sections, and submitted in order.

Table of Contents

Attachment A

SINGLE SOURCE DETERMINATION FORM

ATTACHMENT A - SINGLE SOURCE DETERMINATION FORM

Classifying multiple facilities as one "stationary source" under 45CSR13, 45CSR14, and 45CSR19 is based on the definition of Building, structure, facility, or installation as given in §45-14-2.13 and §45-19-2.12. The definition states:

"Building, Structure, Facility, or Installation" means all of the pollutant-emitting activities which belong to the same industrial grouping, are located on one or more contiguous or adjacent properties, and are under the control of the same person (or persons under common control). Pollutant-emitting activities are a part of the same industrial grouping if they belong to the same "Major Group" (i.e., which have the same two (2)-digit code) as described in the Standard Industrial Classification Manual, 1987 (United States Government Printing Office stock number GPO 1987 0-185-718:QL 3).

Is there a facility owned by or associated with the natural gas industry located within one (1) mile of the proposed facility? Yes ☐ No **X**

If Yes, please complete the questionnaire on the following page (Attachment A).

Please provide a source aggregation analysis for the proposed facility below:

See Introduction for additional source aggregation analysis.

Attachment B

CITING CRITERIA WAIVER – (NOT APPLICABLE)

Attachment C

BUSINESS CERTIFICATE

WEST VIRGINIA
STATE TAX DEPARTMENT
BUSINESS REGISTRATION CERTIFICATE

ISSUED TO:
EQT PRODUCTION COMPANY
625 LIBERTY AVE 1700
PITTSBURGH, PA 15222-3114

BUSINESS REGISTRATION ACCOUNT NUMBER: **1022-8081**

This certificate is issued on: 08/4/2010

This certificate is issued by
the West Virginia State Tax Commissioner
in accordance with Chapter 11, Article 12, of the West Virginia Code

The person or organization identified on this certificate is registered to conduct business in the State of West Virginia at the location above.

This certificate is not transferrable and must be displayed at the location for which issued.

This certificate shall be permanent until cessation of the business for which the certificate of registration was granted or until it is suspended, revoked or cancelled by the Tax Commissioner.

Change in name or change of location shall be considered a cessation of the business and a new certificate shall be required.

TRAVELING/STREET VENDORS: Must carry a copy of this certificate in every vehicle operated by them. CONTRACTORS, DRILLING OPERATORS, TIMBER/LOGGING OPERATIONS: Must have a copy of this certificate displayed at every job site within West Virginia.

atL006 v.3
L0553297664

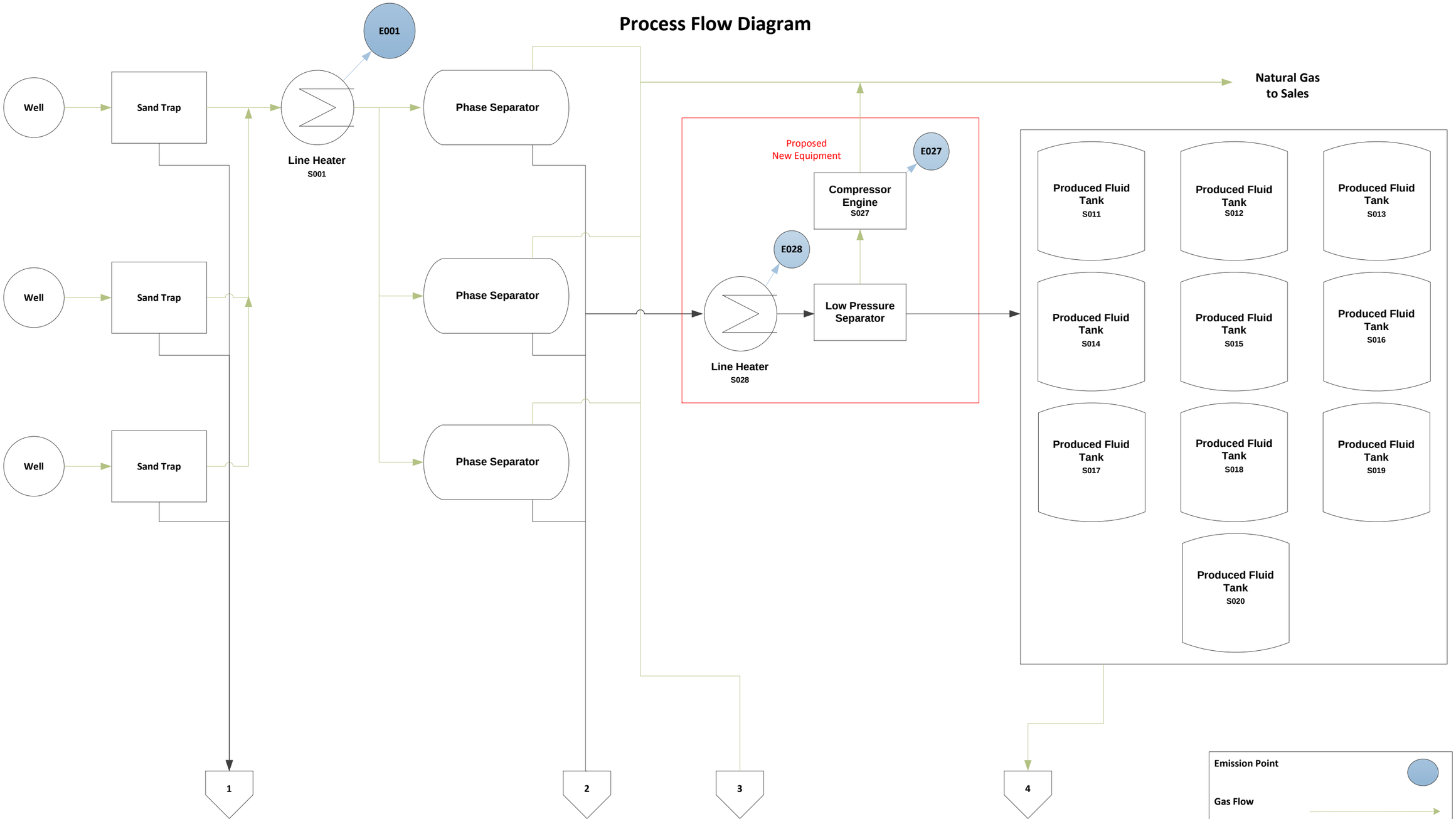
Attachment D

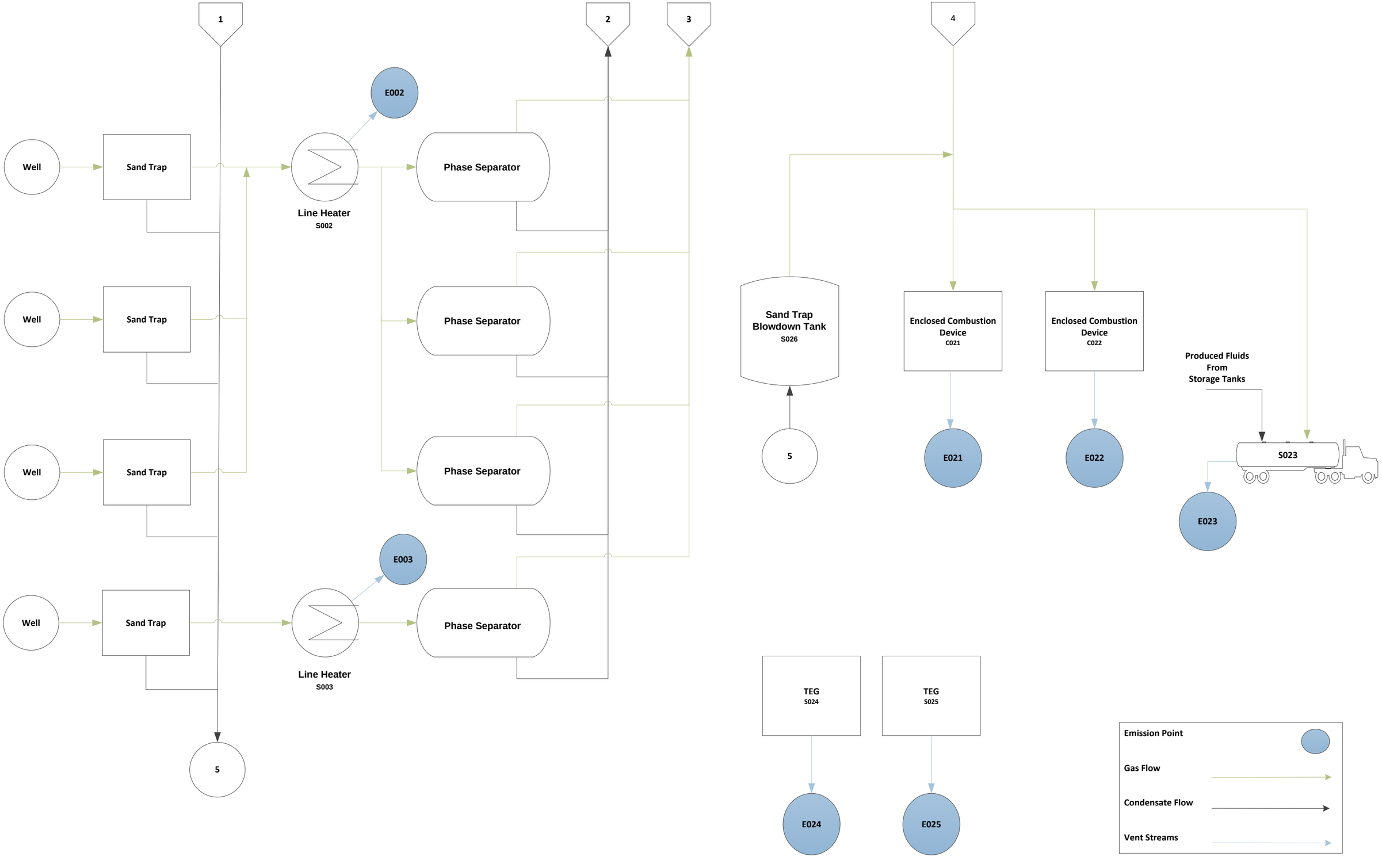
PROCESS FLOW DIAGRAM

Attachment D

OXF 157 Natural Gas Production

Process Flow Diagram




1
2
3
4
5
Well
Sand Trap
Well
Sand Trap
Well
Sand Trap
E002
Line Heater
S002
E003
Line Heater
S003
Phase Separator
Phase Separator
Phase Separator
Sand Trap Blowdown Tank
S026
Enclosed Combustion Device
C021
Enclosed Combustion Device
C022
E021
E022
Produced Fluids From Storage Tanks
S023
E023
TEG
S024
TEG
S025
E024
E025
Emission Point
Gas Flow
Condensate Flow
Vent Streams

Attachment E

PROCESS DESCRIPTION

Attachment E
Process Description

This permit modification application is being filed for EQT Production Company and addresses operational activities associated with the OXF-157 natural gas production site. Incoming raw natural gas from the seven (7) wells enters the site through a pipeline. The raw gas is first routed through the sand traps to remove sediment. Fluids from these sand traps are manually blown down to the sand trap blowdown tank (S026), as needed. From the sand traps, raw gas is routed through line heaters (S001-S003) to assist with the phase separation process in the downstream phase separators. In the high pressure phase separators, produced fluids are removed from the raw gas before being dumped to a second stage of fluid separation. The produced fluids pass through a line heater (S028) to further assist in the separation process. At this low pressure separator, produced fluid pressure is reduced to 30 psig. Vapors realized at the low pressure separator are directed to a 110 bhp compressor engine (S027) and routed to the sales pipeline. Produced fluids from the low pressure separator are routed to the produced fluids storage tanks (S011-S020). Emissions from the produced fluids tanks and sand trap blowdown tank are directed to one of the two enclosed combustion devices (C021, C022) and combusted. Produced fluids are pumped into a tank truck (S023) on an as-needed basis and are disposed of off-site. Vapors during truck loading will be controlled by either of the two enclosed combustion devices.

Two thermoelectric generation units (S024, S025) are operated and provide power to the OXF-157 natural gas production site.

A process flow diagram is included as Attachment D.

Attachment F

PLOT PLAN

Attachment F

Plot Plan

EQT OXF 157 Natural Gas Production Site

Plant ID: 017-00139

N

TRUCK ENTRANCE

PRODUCED FLUIDS TANK S011

PRODUCED FLUIDS TANK S012

PRODUCED FLUIDS TANK S013

PRODUCED FLUIDS TANK S014

PRODUCED FLUIDS TANK S015

PRODUCED FLUIDS TANK S016

PRODUCED FLUIDS TANK S017

PRODUCED FLUIDS TANK S018

PRODUCED FLUIDS TANK S019

PRODUCED FLUIDS TANK S020

SAND TRAP BLOWDOWN TANK S026

ENCLOSED COMBUSTION UNIT C021

ENCLOSED COMBUSTION UNIT C022

TEG S024

TEG S025

WELL

SAND TRAP

FLOWLINE

LINE HEATER S001

LINE HEATER S003

SEPARATOR

LINE HEATER S028

COMPRESSOR ENGINE S027

LOW PRESSURE SEPARATOR

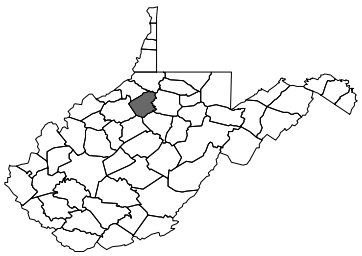
LINE HEATER S002

Coordinates
Latitude: 39.23609
Longitude: -80.76635
Elevation: 960 ft

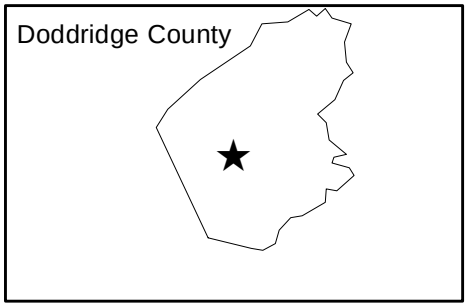
Drawn: 01/26/2016

Attachment G

AREA MAP



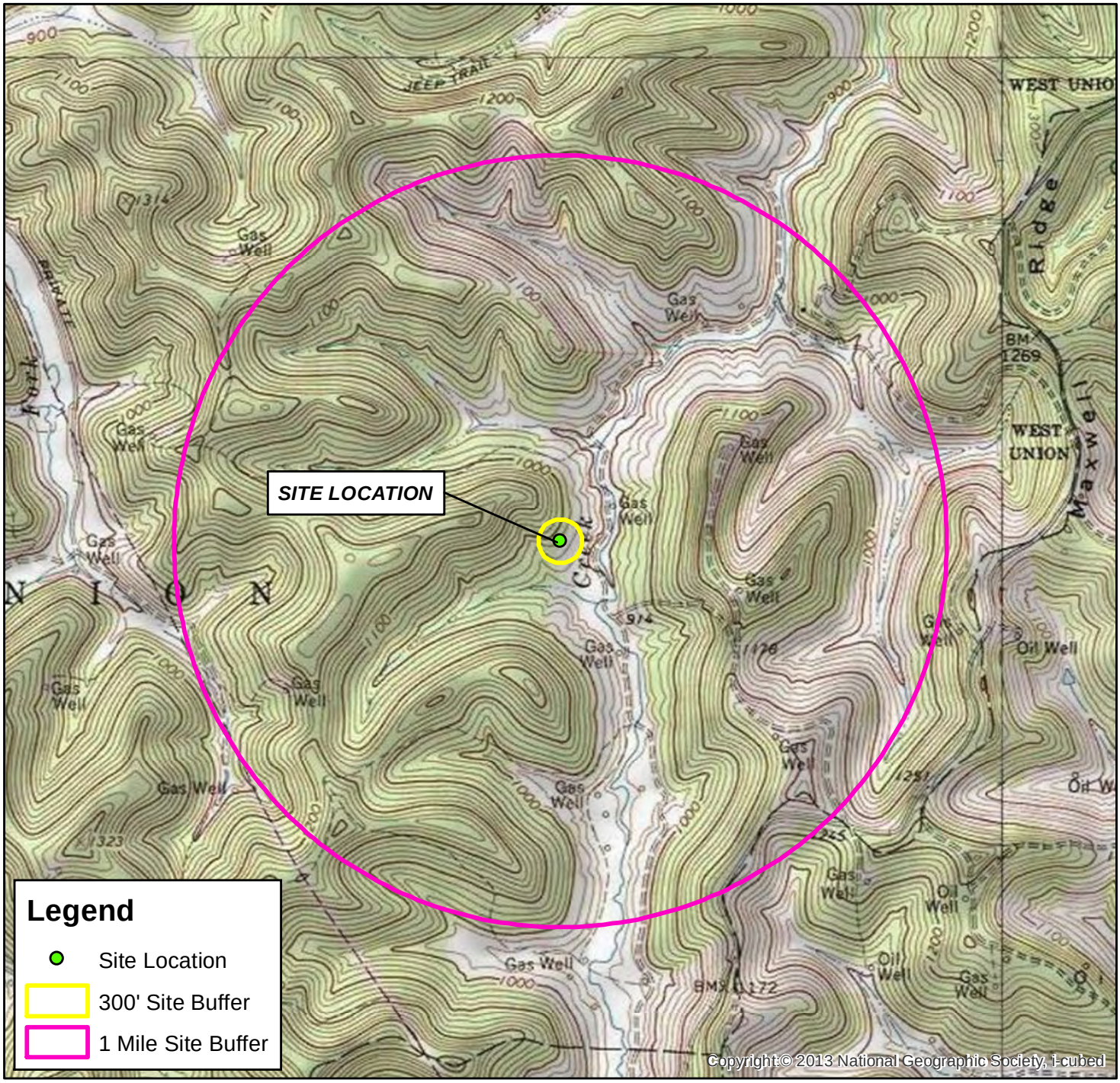
West Virginia



0 1,000 2,000 4,000 Feet

N

LAT. 39.2360 LON. -80.7663
DODDRIDGE COUNTY
WEST VIRGINIA



USGS 1:24K 7.5' Quadrangle:
Oxford, WV

SITE LOCATION MAP

ERM	**EQT PRODUCTION COMPANY** 2520 Mawell Road West Union, West Virginia	GIS Review: JS CHK'D: JS 0250395
Drawn By: SRV-1/21/16	**Environmental Resources Management**	ATTACHMENT G

J:\GIS\Projects\EQT_MXD\2520MawellRd_Site_Location_Map.mxd - 1/21/2016|SRV

Attachment H

APPLICABILITY FORM

ATTACHMENT H – G70-B SECTION APPLICABILITY FORM

General Permit G70-B Registration
Section Applicability Form

General Permit G70-B was developed to allow qualified applicants to seek registration for a variety of sources. These sources include gas well affected facilities, storage vessels, gas production units, in-line heaters, heater treaters, glycol dehydration units and associated reboilers, pneumatic controllers, centrifugal compressors, reciprocating compressors, reciprocating internal combustion engines (RICEs), tank truck loading, fugitive emissions, completion combustion devices, flares, enclosed combustion devices, and vapor recovery systems. All registered facilities will be subject to Sections 1.0, 2.0, 3.0, and 4.0.

General Permit G70-B allows the registrant to choose which sections of the permit they are seeking registration under. Therefore, please mark which additional sections that you are applying for registration under. If the applicant is seeking registration under multiple sections, please select all that apply. Please keep in mind, that if this registration is approved, the issued registration will state which sections will apply to your affected facility.

GENERAL PERMIT G70-B APPLICABLE SECTIONS	
X Section 5.0	Gas Well Affected Facility (NSPS, Subpart OOOO)
X Section 6.0	Storage Vessels Containing Condensate and/or Produced Water[1]
☐Section 7.0	Storage Vessel Affected Facility (NSPS, Subpart OOOO)
X Section 8.0	Control Devices and Emission Reduction Devices not subject to NSPS Subpart OOOO and/or NESHAP Subpart HH
X Section 9.0	Small Heaters and Reboilers not subject to 40CFR60 Subpart Dc
☐Section 10.0	Pneumatic Controllers Affected Facility (NSPS, Subpart OOOO)
☐Section 11.0	Centrifugal Compressor Affected Facility (NSPS, Subpart OOOO)[2]
☐Section 12.0	Reciprocating Compressor Affected Facility (NSPS, Subpart OOOO)[2]
X Section 13.0	Reciprocating Internal Combustion Engines, Generator Engines, Microturbines
X Section 14.0	Tanker Truck Loading[3]
☐Section 15.0	Glycol Dehydration Units[4]

1 *Applicants that are subject to Section 6 may also be subject to Section 7 if the applicant is subject to the NSPS, Subpart OOOO control requirements or the applicable control device requirements of Section 8.*

2 *Applicants that are subject to Section 11 and 12 may also be subject to the applicable RICE requirements of Section 13.*

3 *Applicants that are subject to Section 14 may also be subject to control device and emission reduction device requirements of Section 8.*

4 *Applicants that are subject to Section 15 may also be subject to the requirements of Section 9 (reboilers). Applicants that are subject to Section 15 may also be subject to control device and emission reduction device requirements of Section 8.*

Attachment I

EMISSION UNITS / EMISSION REDUCTION DEVICES (ERD) TABLE

ATTACHMENT I – EMISSION UNITS / EMISSION REDUCTION DEVICES (ERD) TABLE

Include ALL emission units and air pollution control devices/ERDs that will be part of this permit application review. Do not include fugitive emission sources in this table. Deminimis storage tanks shall be listed in the Attachment L table. This information is required for all sources regardless of whether it is a construction, modification, or administrative update.

Emission Unit ID[1]	Emission Point ID[2]	Emission Unit Description	Year Installed	Manufac. Date[3]	Design Capacity	Type[4] and Date of Change	Control Device(s)[5]	ERD(s)[6]
S001	E001	Line Heater	2015	2014	4.5 MMBtu/hr	Modification	NA	NA
S002	E002	Line Heater	2015	2014	4.5 MMBtu/hr	Modification	NA	NA
S003	E003	Line Heater	2015	2014	1.54 MMBtu/hr	Modification	NA	NA
S011	E021 E022	Produced Fluid Tank	2014	2014	400 bbl	Modification	C021 C022	NA
S012	E021 E022	Produced Fluid Tank	2014	2014	400 bbl	Modification	C021 C022	NA
S013	E021 E022	Produced Fluid Tank	2014	2014	400 bbl	Modification	C021 C022	NA
S014	E021 E022	Produced Fluid Tank	2014	2014	400 bbl	Modification	C021 C022	NA
S015	E021 E022	Produced Fluid Tank	2014	2014	400 bbl	Modification	C021 C022	NA
S016	E021 E022	Produced Fluid Tank	2014	2014	400 bbl	Modification	C021 C022	NA
S017	E021 E022	Produced Fluid Tank	2014	2014	400 bbl	Modification	C021 C022	NA
S018	E021 E022	Produced Fluid Tank	2014	2014	400 bbl	Modification	C021 C022	NA
S019	E021 E022	Produced Fluid Tank	2014	2014	400 bbl	Modification	C021 C022	NA
S020	E021 E022	Produced Fluid Tank	2014	2014	400 bbl	Modification	C021 C022	NA
C021	E021	Enclosed Combustion Device	2014	2014	11.66 MMBtu/hr	Modification	NA	NA
C022	E022	Enclosed Combustion Device	2014	2014	11.66 MMBtu/hr	Modification	NA	NA
S023	E021 E022 E023	Tank Truck Loading Rack	2014	2014	30,209 gal/day	Modification	NA	NA
S024	E024	Thermal Electric Generator	2014	2014	0.013 MMBtu/hr	Modification	NA	NA
S025	E025	Thermal Electric Generator	2014	2014	0.013 MMBtu/hr	Modification	NA	NA
S026	E021 E022	Sand Trap Blowdown Tank	2014	2014	140 bbl	Existing	C021 C022	NA

Emission Unit ID[1]	Emission Point ID[2]	Emission Unit Description	Year Installed	Manufac. Date[3]	Design Capacity	Type[4] and Date of Change	Control Device(s)[5]	ERD(s)[6]
S027	E027	Natural Gas Compressor Engine	2016	2015	110 bhp	New	NA	Non-Selective Catalytic Reduction
S028	E028	Line Heater	2016	2015	1.15 MMBtu/hr	New	NA	NA

[1] For Emission Units (or Sources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.
[2] For Emission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.
[3] When required by rule
[4] New, modification, removal, existing
[5] For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.
[6] For ERDs use the following numbering system: 1D, 2D, 3D,... or other appropriate designation.

*OXF-157 is currently permitted to operate under G70-A112A. To provide clarity to Attachment I, units are noted as “New” if they were not included in G70-A112A, “Existing” if there was no change from the permitted conditions, or “Modification” if there is a difference between the G70-A112A issued registration and the requested updates in this G70-B application. Updates are also included that utilize site specific data.

Attachment J

FUGITIVE EMISSIONS SUMMARY SHEET

ATTACHMENT J – FUGITIVE EMISSIONS SUMMARY SHEET

Sources of fugitive emissions may include loading operations, equipment leaks, blowdown emissions, etc.
Use extra pages for each associated source or equipment if necessary.

Source/Equipment: **Facility Wide**

Leak Detection Method Used	☐ Audible, visual, and olfactory (AVO) inspections	☐ Infrared (FLIR) cameras	☒ Other (please describe) **Permittee will follow section 4.1.4 in issued permit.**	☐ None required

Component Type	Closed Vent System	Count	Source of Leak Factors (EPA, other (specify))	Stream type (gas, liquid, etc.)	Estimated Emissions (tpy)		
					VOC	HAP	GHG (CO_2e)
Pumps	☐ Yes ☐ No			☐ Gas ☐ Liquid ☐ Both			
Valves	☐ Yes ☒ No	**152**	**EPA, 40 CFR 98 Subpart W**	☒ Gas ☐ Liquid ☐ Both	**0.12**	**0.02**	**14.58**
Safety Relief Valves	☐ Yes ☒ No	**4**	**EPA, 40 CFR 98 Subpart W**	☒ Gas ☐ Liquid ☐ Both	**<0.01**	**<0.01**	**0.57**
Open Ended Lines	☐ Yes ☒ No	**10**	**EPA, 40 CFR 98 Subpart W**	☒ Gas ☐ Liquid ☐ Both	**0.02**	**<0.01**	**2.17**
Sampling Connections	☐ Yes ☐ No			☐ Gas ☐ Liquid ☐ Both			
Connections (Not sampling)	☐ Yes ☒ No	**661**	**EPA, 40 CFR 98 Subpart W**	☒ Gas ☐ Liquid ☐ Both	**0.06**	**0.01**	**7.04**
Compressors	☐ Yes ☒ No	**1**	**EPA, 40 CFR 98 Subpart W Table W-1B: Default average component counts are used for major equipment. Compressor components (12 valves and 57 connections) are included in valve and connection counts.**	☒ Gas ☐ Liquid ☐ Both			
Flanges	☐ Yes ☐ No			☐ Gas ☐ Liquid ☐ Both			
Other[1]	☐ Yes ☐ No			☐ Gas ☐ Liquid ☐ Both			

[1] Other equipment types may include compressor seals, relief valves, diaphragms, drains, meters, etc.

Please provide an explanation of the sources of fugitive emissions (e.g. pigging operations, equipment blowdowns, pneumatic controllers, etc.):
Fugitive emissions occur from sealed surfaces associated with production equipment, including equipment leaks.

Please indicate if there are any closed vent bypasses (include component): **NA**
Specify all equipment used in the closed vent system (e.g. VRU, ERD, thief hatches, tanker truck loading, etc.) **NA**

Attachment K

GAS WELL AFFECTED FACILITY DATA SHEET

ATTACHMENT K – GAS WELL AFFECTED FACILITY DATA SHEET

Complete this data sheet if you are the owner or operator of a gas well affected facility for which construction, modification or reconstruction commenced after August 23, 2011. This form must be completed for natural gas well affected facilities regardless of when flowback operations occur (or have occurred).

API Number	Date of Flowback	Date of Well Completion	Green Completion and/or Combustion Device
047-017-06458			Green Completion
047-017-06459			Green Completion
047-017-06460			Green Completion
047-017-06461			Green Completion
047-017-06462			Green Completion
047-017-06463			Green Completion
TBD			Green Completion

Note: If future wells are planned and no API number is available please list as PLANNED.
If there are existing wells that commenced construction prior to August 23, 2011, please acknowledge as existing.

This is the same API (American Petroleum Institute) well number(s) provided in the well completion notification and as provided to the WVDEP, Office of Oil and Gas for the well permit. The API number may be provided on the application without the state code (047).

Every oil and gas well permitted in West Virginia since 1929 has been issued an API number. This API is used by agencies to identify and track oil and gas wells.

The API number has the following format: 047-001-00001

Where,

047 = State code. The state code for WV is 047.
001 = County Code. County codes are odd numbers, beginning with 001 (Barbour) and continuing to 109 (Wyoming).
00001= Well number. Each well will have a unique well number.

Attachment L

STORAGE VESSEL DATA SHEET

ATTACHMENT L – STORAGE VESSEL DATA SHEET

GENERAL INFORMATION (REQUIRED)

1. Bulk Storage Area Name **OXF-157 Storage Tank Area**	2. Tank Name **Produced Fluid Tanks (S011-S020)**
3. Emission Unit ID number **S011-S020**	4. Emission Point ID number **E021 or E022**
5. Date Installed , Modified or Relocated *(for existing tanks)* **04/2016 (anticipated)** Was the tank manufactured after August 23, 2011? ☒ Yes ☐ No	6. Type of change: ☐ New construction ☐ New stored material ☒ Other ☐ Relocation
7A. Description of Tank Modification *(if applicable)* **Installation of low pressure separator.**	
7B. Will more than one material be stored in this tank? *If so, a separate form must be completed for each material.* ☐ Yes ☒ No	
7C. Was USEPA Tanks simulation software utilized? ☐ Yes ☒ No ***If Yes, please provide the appropriate documentation and items 8-42 below are not required.***	

TANK INFORMATION

8. Design Capacity *(specify barrels or gallons).* Use the internal cross-sectional area multiplied by internal height. **16,800 gallons**	
9A. Tank Internal Diameter (ft.) **12**	9B. Tank Internal Height (ft.) **20**
10A. Maximum Liquid Height (ft.) **20**	10B. Average Liquid Height (ft.) **10**
11A. Maximum Vapor Space Height (ft.) **20**	11B. Average Vapor Space Height (ft.) **10**
12. Nominal Capacity *(specify barrels or gallons).* This is also known as "working volume". **16,800 gallons**	
13A. Maximum annual throughput (gal/yr) **10,719,656**	13B. Maximum daily throughput (gal/day) **29,369**
14. Number of tank turnovers per year **638**	15. Maximum tank fill rate (gal/min) **20.40**
16. Tank fill method ☐ Submerged ☐ Splash ☒ Bottom Loading	
17. Is the tank system a variable vapor space system? ☐ Yes ☒ No If yes, (A) What is the volume expansion capacity of the system (gal)? (B) What are the number of transfers into the system per year?	
18. Type of tank (check all that apply): ☒ Fixed Roof ☒ vertical ☐ horizontal ☐ flat roof ☐ cone roof ☒ dome roof ☐ other (describe) ☐ External Floating Roof ☐ pontoon roof ☐ double deck roof ☐ Domed External (or Covered) Floating Roof ☐ Internal Floating Roof ☐ vertical column support ☐ self-supporting ☐ Variable Vapor Space ☐ lifter roof ☐ diaphragm ☐ Pressurized ☐ spherical ☐ cylindrical ☐ Other (describe)	

PRESSURE/VACUUM CONTROL DATA

19. Check as many as apply:

☐ Does Not Apply ☐ Rupture Disc (psig)

☐ Inert Gas Blanket of _____ ☐ Carbon Adsorption[1]

☒ Vent to Vapor Combustion Device[1] (vapor combustors, flares, thermal oxidizers, enclosed combustors)

☒ Conservation Vent (psig) ☐ Condenser[1]

-0.5 oz Vacuum Setting **14.0 oz** Pressure Setting

☒ Emergency Relief Valve (psig)

-0.5 oz Vacuum Setting **14.4 oz** Pressure Setting

☐ Thief Hatch Weighted ☐ Yes ☒ **No - A lock down screw hatch will be installed instead of Thief Hatch.**

[1] Complete appropriate Air Pollution Control Device Sheet

20. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application).

Material Name	Flashing Loss		Breathing Loss		Working Loss		Total Emissions Loss		Estimation Method[1]
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	Tpy	
Produced Fluid (Pre-Control)	**25.37**	**111.13**	**0.01**	**0.05**	**0.04**	**0.19**	**25.43**	**111.37**	**O - ProMax**

[1] EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)
Remember to attach emissions calculations, including TANKS Summary Sheets and other modeling summary sheets if applicable.

TANK CONSTRUCTION AND OPERATION INFORMATION

21. Tank Shell Construction:
☐ Riveted ☐ Gunite lined ☐ Epoxy-coated rivets ☒ Other (describe) **Welded**

21A. Shell Color: **Green**	21B. Roof Color: **Green**	21C. Year Last Painted: **NA**

22. Shell Condition (if metal and unlined):
☒ No Rust ☐ Light Rust ☐ Dense Rust ☐ Not applicable

22A. Is the tank heated? ☐ Yes ☒ No	22B. If yes, operating temperature:	22C. If yes, how is heat provided to tank?

23. Operating Pressure Range (psig):
Must be listed for tanks using VRUs with closed vent system.

24. Is the tank a **Vertical Fixed Roof Tank**? ☒ Yes ☐ No	24A. If yes, for dome roof provide radius (ft): **5 ft**	24B. If yes, for cone roof, provide slop (ft/ft):

25. Complete item 25 for **Floating Roof Tanks** ☐ Does not apply ☒

25A. Year Internal Floaters Installed:

25B. Primary Seal Type *(check one):* ☐ Metallic (mechanical) shoe seal ☐ Liquid mounted resilient seal ☐ Vapor mounted resilient seal ☐ Other (describe):

25C. Is the Floating Roof equipped with a secondary seal? ☐ Yes ☐ No

25D. If yes, how is the secondary seal mounted? *(check one)* ☐ Shoe ☐ Rim ☐ Other (describe):

25E. Is the floating roof equipped with a weather shield? ☐ Yes ☐ No

25F. Describe deck fittings:

26. Complete the following section for **Internal Floating Roof Tanks** ☒ Does not apply

26A. Deck Type: ☐ Bolted ☐ Welded	26B. For bolted decks, provide deck construction:

26C. Deck seam. Continuous sheet construction:
☐ 5 ft. wide ☐ 6 ft. wide ☐ 7 ft. wide ☐ 5 x 7.5 ft. wide ☐ 5 x 12 ft. wide ☐ other (describe)

26D. Deck seam length (ft.):	26E. Area of deck (ft^2):	26F. For column supported tanks, # of columns:	26G. For column supported tanks, diameter of column:

27. Closed Vent System with VRU? ☐ Yes ☒ No

28. Closed Vent System with Enclosed Combustor? ☒ Yes ☐ No

SITE INFORMATION

29. Provide the city and state on which the data in this section are based: **Charleston, WV**

30. Daily Avg. Ambient Temperature (°F): **70.0**	31. Annual Avg. Maximum Temperature (°F): **65.5**
32. Annual Avg. Minimum Temperature (°F): **44.0**	33. Avg. Wind Speed (mph): **18 mph**
34. Annual Avg. Solar Insulation Factor (BTU/ft^2-day): **1,123**	35. Atmospheric Pressure (psia): **14.7**

LIQUID INFORMATION

36. Avg. daily temperature range of bulk liquid (°F): **110**	36A. Minimum (°F): **110**	36B. Maximum (°F): **110**
37. Avg. operating pressure range of tank (psig): **0**	37A. Minimum (psig): **0**	37B. Maximum (psig): **0**

38A. Minimum liquid surface temperature (°F): **110**	38B. Corresponding vapor pressure (psia): **0.1**
39A. Avg. liquid surface temperature (°F): **110**	39B. Corresponding vapor pressure (psia): **0.1**
40A. Maximum liquid surface temperature (°F): **110**	40B. Corresponding vapor pressure (psia): **0.1**

41. Provide the following for each liquid or gas to be stored in the tank. Add additional pages if necessary.			
41A. Material name and composition:	**Produced Fluid**		
41B. CAS number:			
41C. Liquid density (lb/gal):	**7.97**		
41D. Liquid molecular weight (lb/lb-mole):	**19.311**		
41E. Vapor molecular weight (lb/lb-mole):			
41F. Maximum true vapor pressure (psia):			
41G. Maximum Reid vapor pressure (psia):			
41H. Months Storage per year.	From: **January** To: **December**		
42. Final maximum gauge pressure and temperature prior to transfer into tank used as inputs into flashing emission calculations.	**30 psig** **110 F**		

STORAGE TANK DATA TABLE

List all deminimis storage tanks (i.e. lube oil, glycol, diesel etc.)

Source ID #[1]	Status[2]	Content[3]	Volume[4]
NA	**NA**	**NA**	**NA**

1. Enter the appropriate Source Identification Numbers (Source ID #) for each storage tank located at the compressor station. Tanks should be designated T01, T02, T03, etc.
2. Enter storage tank Status using the following:
   - EXIST Existing Equipment
   - NEW Installation of New Equipment
   - REM Equipment Removed
3. Enter storage tank content such as condensate, pipeline liquids, glycol (DEG or TEG), lube oil, diesel, mercaptan etc.
4. Enter the maximum design storage tank volume in gallons.

ATTACHMENT L – STORAGE VESSEL DATA SHEET

GENERAL INFORMATION (REQUIRED)

1. Bulk Storage Area Name **OXF-157 Storage Tank Area**	2. Tank Name **Sand Trap Blowdown Tank**
3. Emission Unit ID number **S026**	4. Emission Point ID number **E021 or E022**
5. Date Installed , Modified or Relocated *(for existing tanks)* **Anticipated 04/2016** Was the tank manufactured after August 23, 2011? ☒ Yes ☐ No	6. Type of change: ☐ New construction ☐ New stored material ☒ Other ☐ Relocation
7A. Description of Tank Modification *(if applicable)* **Installation of low pressure separator.**	
7B. Will more than one material be stored in this tank? *If so, a separate form must be completed for each material.* ☐ Yes ☒ No	
7C. Was USEPA Tanks simulation software utilized? ☐ Yes ☒ No ***If Yes, please provide the appropriate documentation and items 8-42 below are not required.***	

TANK INFORMATION

8. Design Capacity *(specify barrels or gallons).* Use the internal cross-sectional area multiplied by internal height. **5,880 gallons**	
9A. Tank Internal Diameter (ft.) **10**	9B. Tank Internal Height (ft.) **10**
10A. Maximum Liquid Height (ft.) **8**	10B. Average Liquid Height (ft.) **5**
11A. Maximum Vapor Space Height (ft.) **8**	11B. Average Vapor Space Height (ft.) **5**
12. Nominal Capacity *(specify barrels or gallons).* This is also known as "working volume". **5,880 gallons**	
13A. Maximum annual throughput (gal/yr) **306,600**	13B. Maximum daily throughput (gal/day) **840**
14. Number of tank turnovers per year **52**	15. Maximum tank fill rate (gal/min) **4.1**
16. Tank fill method ☐ Submerged ☐ Splash ☒ Bottom Loading	
17. Is the tank system a variable vapor space system? ☐ Yes ☒ No If yes, (A) What is the volume expansion capacity of the system (gal)? (B) What are the number of transfers into the system per year?	
18. Type of tank (check all that apply): ☒ Fixed Roof ☐ vertical ☒ horizontal ☐ flat roof ☐ cone roof ☐ dome roof ☐ other (describe) ☐ External Floating Roof ☐ pontoon roof ☐ double deck roof ☐ Domed External (or Covered) Floating Roof ☐ Internal Floating Roof ☐ vertical column support ☐ self-supporting ☐ Variable Vapor Space ☐ lifter roof ☐ diaphragm ☐ Pressurized ☐ spherical ☐ cylindrical ☐ Other (describe)	

PRESSURE/VACUUM CONTROL DATA

19. Check as many as apply:

☐ Does Not Apply ☐ Rupture Disc (psig)

☐ Inert Gas Blanket of _____ ☐ Carbon Adsorption[1]

☒ Vent to Vapor Combustion Device[1] (vapor combustors, flares, thermal oxidizers, enclosed combustors)

☐ Conservation Vent (psig) ☐ Condenser[1]

Vacuum Setting Pressure Setting

☒ Emergency Relief Valve (psig)

-0.5 oz Vacuum Setting **14.4 oz** Pressure Setting

☒ Thief Hatch Weighted ☒ Yes ☐ No - **Two 16 oz. weighted emergency hatches.**

[1] Complete appropriate Air Pollution Control Device Sheet

20. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application).									
Material Name	**Flashing Loss**		**Breathing Loss**		**Working Loss**		**Total Emissions Loss**		**Estimation Method[1]**
	lb/hr	**tpy**	**lb/hr**	**tpy**	**lb/hr**	**tpy**	**lb/hr**	**tpy**	
Produced Fluid (pre-control)	**9.02**	**1.65**	**<0.01**	**<0.01**	**<0.01**	**0.01**	**9.02**	**1.65**	**O - ProMax**
Assumed that all daily blowdowns occur in 1 hour, so the lb/hr emission rate is equivalent to the lb/day emission rate for this tank. Therefore, tpy emission rate is based on 1 blowdown per day x 365 days / 2,000 lbs/ton.									

[1] EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)
Remember to attach emissions calculations, including TANKS Summary Sheets and other modeling summary sheets if applicable.

TANK CONSTRUCTION AND OPERATION INFORMATION		
21. Tank Shell Construction: ☐ Riveted ☐ Gunite lined ☐ Epoxy-coated rivets ☒ Other (describe) **WELDED**		
21A. Shell Color: **Green**	21B. Roof Color: **Green**	21C. Year Last Painted: **NA**
22. Shell Condition (if metal and unlined): ☒ No Rust ☐ Light Rust ☐ Dense Rust ☐ Not applicable		
22A. Is the tank heated? ☐ Yes ☒ No	22B. If yes, operating temperature:	22C. If yes, how is heat provided to tank?
23. Operating Pressure Range (psig): **Must be listed for tanks using VRUs with closed vent system.**		
24. Is the tank a **Vertical Fixed Roof Tank**? ☐ Yes ☒ No	24A. If yes, for dome roof provide radius (ft): **NA**	24B. If yes, for cone roof, provide slop (ft/ft): **NA**
25. Complete item 25 for **Floating Roof Tanks** ☐ Does not apply ☒		
25A. Year Internal Floaters Installed:		
25B. Primary Seal Type *(check one):* ☐ Metallic (mechanical) shoe seal ☐ Liquid mounted resilient seal ☐ Vapor mounted resilient seal ☐ Other (describe):		
25C. Is the Floating Roof equipped with a secondary seal? ☐ Yes ☐ No		
25D. If yes, how is the secondary seal mounted? *(check one)* ☐ Shoe ☐ Rim ☐ Other (describe):		
25E. Is the floating roof equipped with a weather shield? ☐ Yes ☐ No		
25F. Describe deck fittings:		
26. Complete the following section for **Internal Floating Roof Tanks** ☒ Does not apply		
26A. Deck Type: ☐ Bolted ☐ Welded	26B. For bolted decks, provide deck construction:	
26C. Deck seam. Continuous sheet construction: ☐ 5 ft. wide ☐ 6 ft. wide ☐ 7 ft. wide ☐ 5 x 7.5 ft. wide ☐ 5 x 12 ft. wide ☐ other (describe)		
26D. Deck seam length (ft.):	26E. Area of deck (ft^2):	26F. For column supported tanks, # of columns:	26G. For column supported tanks, diameter of column:
27. Closed Vent System with VRU? ☐ Yes ☒ No		
28. Closed Vent System with Enclosed Combustor? ☒ Yes ☐ No		
SITE INFORMATION		
29. Provide the city and state on which the data in this section are based: **Charleston, WV**		
30. Daily Avg. Ambient Temperature (°F): **70 °F**	31. Annual Avg. Maximum Temperature (°F): **65.5 °F**	
32. Annual Avg. Minimum Temperature (°F): **44 °F**	33. Avg. Wind Speed (mph): **18 mph**	
34. Annual Avg. Solar Insulation Factor (BTU/ft^2-day): **1,123**	35. Atmospheric Pressure (psia): **14.70**	
LIQUID INFORMATION		
36. Avg. daily temperature range of bulk liquid (°F): **83.2**	36A. Minimum (°F): **83.2**	36B. Maximum (°F): **83.2**
37. Avg. operating pressure range of tank (psig): **0 psig**	37A. Minimum (psig): **0 psig**	37B. Maximum (psig): **0 psig**

38A. Minimum liquid surface temperature (°F): **83.2**		38B. Corresponding vapor pressure (psia): **0.1**	
39A. Avg. liquid surface temperature (°F): **83.2**		39B. Corresponding vapor pressure (psia): **0.1**	
40A. Maximum liquid surface temperature (°F): **83.2**		40B. Corresponding vapor pressure (psia): **0.1**	
41. Provide the following for each liquid or gas to be stored in the tank. Add additional pages if necessary.			
41A. Material name and composition:	**Produced Fluid**		
41B. CAS number:			
41C. Liquid density (lb/gal):	**8.04**		
41D. Liquid molecular weight (lb/lb-mole):	**19.305**		
41E. Vapor molecular weight (lb/lb-mole):			
41F. Maximum true vapor pressure (psia):			
41G. Maximum Reid vapor pressure (psia):			
41H. Months Storage per year.	**From: January** **To: December**		
42. Final maximum gauge pressure and temperature prior to transfer into tank used as inputs into flashing emission calculations.	**307 psig** **85 F**		

GAS ANALYTICAL SERVICES

C6+ Gas Analysis Report

Gas Analytical

Report Date: Sep 14, 2015 9:23a

Client:	Equitable Production	Date Sampled:	Sep 8, 2015 11:00a
Site:	514394	Analysis Date:	Sep 11, 2015 2:17p
Field No:	9998	Collected By:	J. Brown
Meter:	514394	Date Effective:	Sep 8, 2015 12:00a
Source Laboratory	Clarksburg (Bridgeport), WV	Sample Pressure (PSI):	70.0
Lab File No:	**X_CH1-6024.CHR**	Sample Temp (°F):	
Sample Type:	Spot	Field H2O:	No Test
Reviewed By:		Field H2S:	No Test

Component	Mol %	Gal/MSCF
Methane	78.1311	
Ethane	14.2559	3.79
Propane	4.0036	1.10
I-Butane	0.5947	0.19
N-Butane	1.1890	0.37
I-Pentane	0.3163	0.12
N-Pentane	0.3248	0.12
Nitrogen	0.4544	
Oxygen	<MDL	
Carbon Dioxide	0.1535	
Hexanes+	0.5767	0.24
TOTAL	100.0000	5.93

Analytical Results at Base Conditions (Real)	
BTU/SCF (Dry):	1,262.4954 BTU/ft³
BTU/SCF (Saturated):	1,241.4002 BTU/ft³
PSIA:	14.730 PSI
Temperature (°F):	60.00 °F
Z Factor (Dry):	0.99644
Z Factor (Saturated):	0.99604

Analytical Results at Contract Conditions (Real)	
BTU/SCF (Dry):	1,262.4954 BTU/ft³
BTU/SCF (Saturated):	1,241.4002 BTU/ft³
PSIA:	14.730 PSI
Temperature (°F):	60.00 °F
Z Factor (Dry):	0.99644
Z Factor (Saturated):	0.99604

Calculated Specific Gravities			
Ideal Gravity:	0.7188	Real Gravity:	0.7211
Molecular Wt:	20.8177 lb/lbmol		

Gross Heating Values are Based on:
GPA 2145-09, 2186
Compressibility is Calculated using AGA-8.

Source	Date	Notes
Gas Analytical	Sep 11, 2015	results to Bob Gum

<MDL = Less than Method Detection Limits, NG = Not Given, NT = Not Tested

Certificate of Analysis

Number: 2030-15070269-001A

Carencro Laboratory
4790 NE Evangeline Thruway
Carencro, LA 70520

Gary Vermillion
Gas Analytical Services
PO Box 1028
Bridgeport, WV 26330

Aug. 04, 2015

Field: EQT
Station Name: 513149-OXF 157 Pad
Station Number:
Sample Point: Submeter
Analyzed: 08/03/2015 15:53:03 by GR

Sampled By: RM-GAS
Sample Of: Condensate Spot
Sample Date: 07/13/2015
Sample Conditions: 1052 psig
Method: GPA-2186M/GPA-2103
Cylinder No: 0065

Analytical Data

Components	Mol. %	MW	Wt. %	Sp. Gravity	L.V. %
Nitrogen	NIL	28.013	NIL	0.807	NIL
Methane	26.433	16.043	6.890	0.300	13.674
Carbon Dioxide	0.185	44.010	0.132	0.817	0.096
Ethane	16.284	30.069	7.955	0.356	13.295
Propane	11.163	44.096	7.997	0.507	9.388
Iso-Butane	2.473	58.122	2.335	0.563	2.470
n-Butane	6.130	58.122	5.788	0.584	5.899
Iso-Pentane	2.814	72.149	3.299	0.625	3.142
n-Pentane	3.189	72.149	3.738	0.631	3.529
i-Hexanes	2.494	85.322	3.455	0.666	3.088
n-Hexane	2.130	86.175	2.982	0.664	2.674
2,2,4-Trimethylpentane	0.009	114.231	0.016	0.697	0.014
Benzene	0.058	78.114	0.073	0.885	0.049
Heptanes	6.585	97.989	10.481	0.702	8.895
Toluene	0.418	92.141	0.626	0.872	0.427
Octanes	6.744	109.766	12.031	0.733	9.771
Ethylbenzene	0.064	106.167	0.111	0.872	0.076
Xylenes	0.108	106.167	0.185	0.885	0.125
Nonanes	4.256	124.837	8.632	0.744	6.910
Decanes Plus	8.463	169.272	23.274	0.841	16.478
	100.000		100.000		100.000

Physical Properties	Total	C10+
Specific Gravity at 60°F	0.5954	0.8410
API Gravity at 60°F	106.151	36.752
Molecular Weight	61.552	169.272
Pounds per Gallon (in Vacuum)	4.964	7.011
Pounds per Gallon (in Air)	4.959	7.004
Cu. Ft. Vapor per Gallon @ 14.73 psia	30.534	15.683

Patti L. Perro

Hydrocarbon Laboratory Manager

Quality Assurance: The above analyses are performed in accordance with ASTM, UOP, GPA guidelines for quality assurance, unless otherwise stated.

Attachment M

HEATER AND REBOILERS NOT SUBJECT TO 40CFR60 SUBPART Dc

ATTACHMENT M – SMALL HEATERS AND REBOILERS NOT SUBJECT TO 40CFR60 SUBPART DC
DATA SHEET

Complete this data sheet for each small heater and reboiler not subject to 40CFR60 Subpart Dc at the facility. ***The Maximum Design Heat Input (MDHI) must be less than 10 MMBTU/hr.***

Emission Unit ID#[1]	Emission Point ID#[2]	Emission Unit Description (manufacturer, model #)	Year Installed/ Modified	Type[3] and Date of Change	Maximum Design Heat Input (MMBTU/hr)[4]	Fuel Heating Value (BTU/scf)[5]
S001	E001	Line Heater	2015	Modification	4.50	1,262
S002	E002	Line Heater	2015	Modification	4.50	1,262
S003	E003	Line Heater	2015	Modification	1.54	1,262
S024	E024	TEG	2015	Modification	0.013	1,262
S025	E025	TEG	2015	Modification	0.013	1,262
S028	E028	Line Heater	2016	New	1.15	1,262

***OXF-157 is currently permitted to operate under G70-A146. To provide clarity to Attachment M, units are noted as "New" if they were not included in G70-A146, "Existing" if there was no change from the permitted conditions, or "Modification" if there is a difference between the G70-A146 issued registration and the requested updates in this G70-B application. Updates are also included that utilize site specific data.**

1 Enter the appropriate Emission Unit (or Source) identification number for each fuel burning unit located at the production pad. Gas Producing Unit Burners should be designated GPU-1, GPU-2, etc. Heater Treaters should be designated HT-1, HT-2, etc. Heaters or Line Heaters should be designated LH-1, LH-2, etc. For sources, use 1S, 2S, 3S…or other appropriate designation. Enter glycol dehydration unit Reboiler Vent data on the Glycol Dehydration Unit Data Sheet.

2 Enter the appropriate Emission Point identification numbers for each fuel burning unit located at the production pad. Gas Producing Unit Burners should be designated GPU-1, GPU-2, etc. Heater Treaters should be designated HT-1, HT-2, etc. Heaters or Line Heaters should be designated LH-1, LH-2, etc. For emission points, use 1E, 2E, 3E…or other appropriate designation.

3 New, modification, removal

4 Enter design heat input capacity in MMBtu/hr.

5 Enter the fuel heating value in BTU/standard cubic foot.

Attachment N

INTERNAL COMBUSTION ENGINE DATA SHEET

ATTACHMENT N – INTERNAL COMBUSTION ENGINE DATA SHEET

Emission Unit ID#[1]	**S027**		
Engine Manufacturer/Model	**Ford / CSG-637**		
Manufacturers Rated bhp/rpm	**110 / 3200**		
Source Status[2]	**NS**		
Date Installed/ Modified/Removed/Relocated[3]	**06/01/2016**		
Engine Manufactured /Reconstruction Date[4]	**2015**		
Check all applicable Federal Rules for the engine (include EPA Certificate of Conformity if applicable)[5]	☒40CFR60 Subpart JJJJ ☒JJJJ Certified? ☐40CFR60 Subpart IIII ☐IIII Certified? ☐40CFR63 Subpart ZZZZ ☐ NESHAP ZZZZ/ NSPS JJJJ Window ☐ NESHAP ZZZZ Remote Sources	☐40CFR60 Subpart JJJJ ☐JJJJ Certified? ☐40CFR60 Subpart IIII ☐IIII Certified? ☐40CFR63 Subpart ZZZZ ☐ NESHAP ZZZZ/ NSPS JJJJ Window ☐ NESHAP ZZZZ Remote Sources	☐40CFR60 Subpart JJJJ ☐JJJJ Certified? ☐40CFR60 Subpart IIII ☐IIII Certified? ☐40CFR63 Subpart ZZZZ ☐ NESHAP ZZZZ/ NSPS JJJJ Window ☐ NESHAP ZZZZ Remote Sources
Engine Type[6]	**4SRB**		
APCD Type[7]	**NSCR**		
Fuel Type[8]	**PQ**		
H_2S (gr/100 scf)	**0.25**		
Operating bhp/rpm	**110 / 3,200**		
BSFC (BTU/bhp-hr)	**6,552.9**		
Hourly Fuel Throughput	**686.5** ft^3/hr gal/hr	ft^3/hr gal/hr	ft^3/hr gal/hr
Annual Fuel Throughput (Must use 8,760 hrs/yr unless emergency generator)	**6.01** $MMft^3$/yr gal/yr	$MMft^3$/yr gal/yr	$MMft^3$/yr gal/yr
Fuel Usage or Hours of Operation Metered	Yes ☒ No ☐	Yes ☐ No ☐	Yes ☐ No ☐

Calculation Methodology[9]	**Pollutant[10]**	**Hourly PTE (lb/hr)[11]**	**Annual PTE (tons/year)[11]**	**Hourly PTE (lb/hr)[11]**	**Annual PTE (tons/year)[11]**	**Hourly PTE (lb/hr)[11]**	**Annual PTE (tons/year)[11]**
COC	NO_x	**0.24**	**1.03**				
COC	CO	**0.49**	**2.14**				
COC	VOC	**0.16**	**0.71**				
AP	SO_2	**<0.01**	**<0.01**				
AP	PM (Filterable)	**<0.01**	**0.03**				
AP	PM (Condensable)	**<0.01**	**0.03**				
AP	Formaldehyde	**0.01**	**0.06**				
AP	Total HAPs	**0.02**	**0.07**				
AP	GHG (CO_2e)	**82.58**	**361.69**				

1 Enter the appropriate Source Identification Number for each natural gas-fueled reciprocating internal combustion compressor/generator engine located at the compressor station. Multiple compressor engines should be designated CE-1, CE-2, CE-3 etc. Generator engines should be designated GE-1, GE-2, GE-3 etc. Microturbine generator engines should be designated MT-1, MT-2, MT-3 etc. If more than three (3) engines exist, please use additional sheets.

2 Enter the Source Status using the following codes:

NS	Construction of New Source (installation)	ES	Existing Source
MS	Modification of Existing Source	RS	Relocated Source
REM	Removal of Source		

3 Enter the date (or anticipated date) of the engine's installation (construction of source), modification, relocation or removal.

4 Enter the date that the engine was manufactured, modified or reconstructed.

5 Is the engine a certified stationary spark ignition internal combustion engine according to 40CFR60 Subpart IIII/JJJJ? If so, the engine and control device must be operated and maintained in accordance with the manufacturer's emission-related written instructions. You must keep records of conducted maintenance to demonstrate compliance, but no performance testing is required. If the certified engine is not operated and maintained in accordance with the manufacturer's emission-related written instructions, the engine will be considered a non-certified engine and you must demonstrate compliance as appropriate.

Provide a manufacturer's data sheet for all engines being registered.

6 Enter the Engine Type designation(s) using the following codes:

2SLB	Two Stroke Lean Burn	4SRB	Four Stroke Rich Burn
4SLB	Four Stroke Lean Burn		

7 Enter the Air Pollution Control Device (APCD) type designation(s) using the following codes:

A/F	Air/Fuel Ratio	IR	Ignition Retard
HEIS	High Energy Ignition System	SIPC	Screw-in Precombustion Chambers
PSC	Prestratified Charge	LEC	Low Emission Combustion
NSCR	Rich Burn & Non-Selective Catalytic Reduction	OxCat	Oxidation Catalyst
SCR	Lean Burn & Selective Catalytic Reduction		

8 Enter the Fuel Type using the following codes:

PQ	Pipeline Quality Natural Gas	RG	Raw Natural Gas /Production Gas	D	Diesel

9 Enter the Potential Emissions Data Reference designation using the following codes. Attach all reference data used.

MD	Manufacturer's Data	AP	AP-42	
GR	GRI-HAPCalc™	OT	Other	(please list)

10 Enter each engine's Potential to Emit (PTE) for the listed regulated pollutants in pounds per hour and tons per year. PTE shall be calculated at manufacturer's rated brake horsepower and may reflect reduction efficiencies of listed Air Pollution Control Devices. Emergency generator engines may use 500 hours of operation when calculating PTE. PTE data from this data sheet shall be incorporated in the *Emissions Summary Sheet*.

11 PTE for engines shall be calculated from manufacturer's data unless unavailable.

Engine Air Pollution Control Device
(Emission Unit ID# E027, use extra pages as necessary)

Air Pollution Control Device Manufacturer's Data Sheet included?
Yes ☒ No ☐

☒ NSCR ☐ SCR ☐ Oxidation Catalyst

Provide details of process control used for proper mixing/control of reducing agent with gas stream:

Manufacturer: **Ford**	Model #: **CSG-637**
Design Operating Temperature: **1,600 °F**	Design gas volume: scfm
Service life of catalyst: **5000 hrs**	Provide manufacturer data? ☒Yes ☐ No
Volume of gas handled: **444.9** cfm at **1,600** °F	Operating temperature range for NSCR/Ox Cat: From °F to °F
Reducing agent used, if any:	Ammonia slip (ppm):

Pressure drop against catalyst bed (delta P): **6"** inches of H_2O

Provide description of warning/alarm system that protects unit when operation is not meeting design conditions:

Is temperature and pressure drop of catalyst required to be monitored per 40CFR63 Subpart ZZZZ?
☐ Yes ☒ No

How often is catalyst recommended or required to be replaced (hours of operation)?
5000 hrs

How often is performance test required?
☐ Initial
☐ Annual
☐ Every 8,760 hours of operation
☐ Field Testing Required
☒ No performance test required. If so, why (please list any maintenance required and the applicable sections in NSPS/GACT, **40CFR60.4243(a)(1) – EQT must operate and maintain the certified stationary SI internal combustion engine and control device according to the manufacturer's emission-related written instructions, keep records of conducted maintenance to demonstrate compliance, but no performance testing is required.**

EDI Ford Industrial LSI Fuel and Power Figures

CSG637

	Gasoline				LPG				NG				
RPM	Power Cont. [HP]	Power Int. [HP]	BSFC [lb/hp-hr]	Fuel Consumption [gal/hr]	Power Cont. [HP]	Power Int. [HP]	BSFC [lb/hp-hr]	Fuel Consumption [gal/hr]	Power Cont. [HP]	Power Int. [HP]	BSFC [ft^3/hp-hr]	Fuel Consumption [ft^3/hr]	Fuel Consumption [btu/hr]
1500	42.3	47.0	0.48	3.7	52.1	57.9	0.34	4.1	47.8	53.1	6.81	361.8	379,914
1600	47.7	53.0	0.45	3.9	56.8	63.2	0.33	4.3	52.4	58.2	6.54	380.9	399,966
1700	52.2	58.0	0.43	4.1	60.0	66.7	0.33	4.6	54.7	60.8	6.58	400.0	420,019
1800	55.0	61.1	0.43	4.2	63.1	70.2	0.33	4.8	57.0	63.3	6.62	419.1	440,071
1900	58.5	65.0	0.42	4.4	66.3	73.7	0.33	5.0	60.1	66.7	6.57	438.2	460,124
2000	61.2	68.0	0.41	4.6	69.5	77.2	0.33	5.2	63.1	70.2	6.52	457.3	480,176
2100	65.7	73.0	0.40	4.7	73.1	81.2	0.33	5.5	66.0	73.4	6.49	476.4	500,229
2200	70.2	78.0	0.39	4.9	76.7	85.2	0.33	5.7	68.9	76.6	6.47	495.5	520,281
2300	74.7	83.0	0.37	5.0	81.1	90.1	0.32	5.9	73.0	81.1	6.34	514.6	540,334
2400	79.2	88.0	0.36	5.2	85.4	94.9	0.32	6.2	77.1	85.6	6.23	533.7	560,386
2500	82.8	92.0	0.35	5.3	89.4	99.3	0.31	6.4	80.7	89.6	6.17	552.8	580,439
2600	85.5	95.0	0.35	5.4	93.3	103.7	0.31	6.6	84.3	93.6	6.11	571.9	600,491
2700	87.3	97.0	0.35	5.5	95.9	106.6	0.31	6.9	87.0	96.6	6.12	591.0	620,544
2800	88.2	98.0	0.35	5.7	98.6	109.5	0.31	7.1	89.7	99.6	6.12	610.1	640,596
2900	89.1	99.0	0.36	5.8	101.0	112.3	0.32	7.3	92.6	102.9	6.11	629.2	660,649
3000	90.9	101.0	0.36	5.9	103.5	115.0	0.32	7.5	95.5	106.1	6.11	648.3	680,701
3100	93.6	104.0	0.35	6.0	104.8	116.5	0.32	7.8	97.3	108.1	6.17	667.4	700,754
3200	96.3	107.0	0.35	6.1	106.1	117.9	0.33	8.0	99.0	110.0	6.24	686.5	720,806

*Fuel Consumption and BSFC listed is 100% Intermittent Load

*Figures are Gross; Fan losses not accounted for.

Attachment O

TANKER TRUCK LOADING DATA SHEET

ATTACHMENT O – TANKER TRUCK LOADING DATA SHEET

Emission Unit ID#: **S023**	Emission Point ID#: **E021, E022, E023**	Year Installed/Modified:**2014/2016**
Emission Unit Description: **Tank Truck Loading Rack**		
Loading Area Data		
Number of Pumps: **1**	Number of Liquids Loaded: **1**	Max number of trucks loading at one (1) time: **1**
Are tanker trucks pressure tested for leaks at this or any other location? ☐ Yes ☒ No ☐ Not Required If Yes, Please describe:		
Provide description of closed vent system and any bypasses. **Emissions collected and controlled by enclosed combustion device. Bypass is not available.**		
Are any of the following truck loadout systems utilized? ☐ Closed System to tanker truck passing a MACT level annual leak test? ☐ Closed System to tanker truck passing a NSPS level annual leak test? ☒ Closed System to tanker truck not passing an annual leak test and has vapor return?		

Projected Maximum Operating Schedule (for rack or transfer point as a whole)

Time	Jan – Mar	Apr - Jun	Jul – Sept	Oct - Dec
Hours/day	**As needed**	**As needed**	**As needed**	**As needed**
Days/week	**As needed**	**As needed**	**As needed**	**As needed**

Bulk Liquid Data (use extra pages as necessary)

Liquid Name		**Produced Fluids**		
Max. Daily Throughput (1000 gal/day)		**30.21**		
Max. Annual Throughput (1000 gal/yr)		**11,026.56**		
Loading Method[1]		**BF**		
Max. Fill Rate (gal/min)		**42**		
Average Fill Time (min/loading)		**100 min**		
Max. Bulk Liquid Temperature (°F)		**70 °F**		
True Vapor Pressure[2]		**NA**		
Cargo Vessel Condition[3]		**U**		
Control Equipment or Method[4]		**Enclosed Combustion Device (C021 or C022)**		
Max. Collection Efficiency (%)		**70 %**		
Max. Control Efficiency (%)		**98 %**		
Max.VOC Emission Rate	Loading (lb/hr)	**0.15**		
	Annual (ton/yr)	**0.66**		
Max.HAP Emission Rate	Loading (lb/hr)	**<0.01**		
	Annual (ton/yr)	**0.02**		
Estimation Method[5]		**EPA AP-42, ProMax**		

1 BF Bottom Fill SP Splash Fill SUB Submerged Fill
2 At maximum bulk liquid temperature
3 B Ballasted Vessel C Cleaned U Uncleaned (dedicated service)
O Other (describe)
4 List as many as apply (complete and submit appropriate Air Pollution Control Device Sheets)
CA Carbon Adsorption VB Dedicated Vapor Balance (closed system)
ECD Enclosed Combustion Device F Flare
TO Thermal Oxidization or Incineration
5 EPA EPA Emission Factor in AP-42 MB Material Balance
TM Test Measurement based upon test data submittal O Other (describe)

Attachment P

GLYCOL DEHYDRATION UNIT DATA SHEET

(NOT APPLICABLE)

Attachment Q

PNEUMATIC CONTROLLERS DATA SHEET

ATTACHMENT Q – PNEUMATIC CONTROLLERS DATA SHEET

Are there any continuous bleed natural gas driven pneumatic controllers at this facility that commenced construction, modification or reconstruction after August 23, 2011?

☐ Yes ☒ No

Please list approximate number.

Are there any continuous bleed natural gas driven pneumatic controllers at this facility with a bleed rate greater than 6 standard cubic feet per hour that are required based on functional needs, including but not limited to response time, safety and positive actuation that commenced construction, modification or reconstruction after August 23, 2011?

☐ Yes ☒ No

Please list approximate number.

Attachment R

AIR POLLUTION CONTROL DEVICE / EMISSION REDUCTION DEVICE (ERD) SHEET

ATTACHMENT R – AIR POLLUTION CONTROL DEVICE / EMISSION REDUCTION DEVICE SHEETS

VAPOR COMBUSTION (Including Enclosed Combustors)

General Information

Control Device ID#: **C021**	Installation Date: **2014** ☐ New ☒ Modified ☐ Relocated	
Maximum Rated Total Flow Capacity **~7,800** scfh **188,000** scfd	Maximum Design Heat Input (from mfg. spec sheet) **11.66** MMBTU/hr	Design Heat Content **1,262** BTU/scf

Control Device Information

Type of Vapor Combustion Control?

☒ Enclosed Combustion Device ☐ Elevated Flare ☐ Ground Flare
☐ Thermal Oxidizer

Manufacturer: **LEED Fabrication** Model: **Enclosed Combustor 48"**	Hours of operation per year? **8,760**

List the emission units whose emissions are controlled by this vapor control device (Emission Point ID# **S011-S020, S023, S026**))

Emission Unit ID#	Emission Source Description	Emission Unit ID#	Emission Source Description
S011-S020	**Produced Fluid Tanks**		
S023	**Tank Truck Loading Rack**		
S026	**Sand Trap Blowdown Tank**		

If this vapor combustor controls emissions from more than six (6) emission units, please attach additional pages.

Assist Type (Flares only)	Flare Height	Tip Diameter	Was the design per §60.18?
☐ Steam ☐ Air ☐ Pressure ☒ Non	**~25** feet	**4** feet	☐ Yes ☐ No Provide determination.

Waste Gas Information

Maximum Waste Gas Flow Rate	Heat Value of Waste Gas Stream	Exit Velocity of the Emissions Stream
102.93 (lb/hr)	**Variable** BTU/ft^3	(ft/s)

Provide an attachment with the characteristics of the waste gas stream to be burned.

Pilot Gas Information

Number of Pilot Lights	Fuel Flow Rate to Pilot Flame per Pilot	Heat Input per Pilot	Will automatic re-ignition be used?
1	**~30** scfh	**0.03** BTU/hr	☐ Yes ☒ No

If automatic re-ignition is used, please describe the method.

Is pilot flame equipped with a monitor to detect the presence of the flame? ☒ Yes ☐ No	If Yes, what type? ☒ Thermocouple ☐ Infrared ☐ Ultraviolet ☐ Camera ☐ Other:

Describe all operating ranges and maintenance procedures required by the manufacturer to maintain the warranty. *(If unavailable, please indicate).* **See attached manufacture specification sheet.**

Additional information attached? ☒ Yes ☐ No
Please attach copies of manufacturer's data sheets, drawings, flame demonstration per §60.18 or §63.11(b) and performance testing.

VAPOR COMBUSTION
(Including Enclosed Combustors)

General Information

Control Device ID#: **C022**	Installation Date: **2014** ☐ New ☒ Modified ☐ Relocated	
Maximum Rated Total Flow Capacity **~7,800** scfh **188,000** scfd	Maximum Design Heat Input (from mfg. spec sheet) **11.66** MMBTU/hr	Design Heat Content **1,262** BTU/scf

Control Device Information

Type of Vapor Combustion Control?

☒ Enclosed Combustion Device ☐ Elevated Flare ☐ Ground Flare
☐ Thermal Oxidizer

Manufacturer: **LEED Fabrication** Model: **Enclosed Combustor 48"**	Hours of operation per year? **8,760**

List the emission units whose emissions are controlled by this vapor control device (Emission Point ID# **S011-S020, S023, S026**))

Emission Unit ID#	Emission Source Description	Emission Unit ID#	Emission Source Description
S011-S020	**Produced Fluid Tanks**		
S023	**Tank Truck Loading Rack**		
S026	**Sand Trap Blowdown Tank**		

If this vapor combustor controls emissions from more than six (6) emission units, please attach additional pages.

Assist Type (Flares only)	Flare Height	Tip Diameter	Was the design per §60.18?
☐ Steam ☐ Air ☐ Pressure ☒ Non	**~25** feet	**4** feet	☐ Yes ☐ No Provide determination.

Waste Gas Information

Maximum Waste Gas Flow Rate	Heat Value of Waste Gas Stream	Exit Velocity of the Emissions Stream
102.93 (lb/hr)	**Variable** BTU/ft^3	(ft/s)

Provide an attachment with the characteristics of the waste gas stream to be burned.

Pilot Gas Information

Number of Pilot Lights	Fuel Flow Rate to Pilot Flame per Pilot	Heat Input per Pilot	Will automatic re-ignition be used?
1	**~30** scfh	**0.03** BTU/hr	☐ Yes ☒ No

If automatic re-ignition is used, please describe the method.

Is pilot flame equipped with a monitor to detect the presence of the flame? ☒ Yes ☐ No	If Yes, what type? ☒ Thermocouple ☐ Infrared ☐ Ultraviolet ☐ Camera ☐ Other:

Describe all operating ranges and maintenance procedures required by the manufacturer to maintain the warranty. *(If unavailable, please indicate).* **See attached manufacture specification sheet.**

Additional information attached? ☒ Yes ☐ No
Please attach copies of manufacturer's data sheets, drawings, flame demonstration per §60.18 or §63.11(b) and performance testing.

		Item/Tag No.:		Page	1	of	2
		Project No.:		Revision:	B		
		Project:		Date:	27 February 2014		
	Enviromental Control Equipment Data Sheet			By:	JS		
		P.O. No.:	-	Checked:	SG		
		RFQ No.:	-	Approved:	MS		
	Client:	Ref. P&ID:	-				
	Site:			Supplier:	LEED FABRICATION		
	Unit/Lease:	Remarks:	-	Model No.:	L30-0011-00		

GENERAL

1	Design Code:		NDE:	LEED Fabrication Standards
2	Service:		Customer Specs:	☐ Yes
3	Description:	Standard Dual Stage 48 High Efficiency Combustor		☑ No

PROCESS DATA

	Gas Composition:	mol %	Process Conditions: Variable	Value	Units
4	Methane		Flow Rate	Up to 140	Mscfd
5	Ethane		Pressure	Up to 12	oz/in2
6	Propane		Temperature		°F
7	I-Butane		Molecular Weight		
8	n-Butane		Process/Waste Stream	☑ Gas	☐ Liquid
9	I-Pentane		Detailed Process Description / Process Notes:		
10	n-Pentane		1. Turndown 10:1. Based on an expected normal operating rate indicated above.		
11	n-Hexane		2. DRE: 98 % operating at design conditions		
12	CO2		3. Burner Pressure Drop: Min. 0.10 oz/in2		
13	N2				
14	Helium				
15	H_2O				
16	C7				
17	C8				
18	C9				
19	C10				
20	C11+				
21	TOTAL				

	Other Components:	PPMV	Available Utilities:	
22	H2S		Fuel / Pilot Gas	Min. 30psig Natural Gas /Propane 40-50 SCFH
23	Benzene		Instrument Air	NA
24	Toluene		Power	120 V / 60 Hz or Solar Power
25	E-Benzene		Steam	NA
26	Xylene		Purge Gas	

DESIGN DATA

27	Ambient Temperatures:		Noise Performance Requirements:	Under 85 dBA
28	Low, °F	-20	Structural Design Code:	
29	High, °F	120	Wind Design Code:	ASCE
30	Design Conditions: Pressure/Temperature			
31	Max. Relative Humidity, %	90	Pressure/Speed	100 mph
32	Elevation (ASL), ft		Category	
33	Area Classification:	Class I Div 2	Seismic Design Code:	
34	Electrical Design Code:	NEC	Location	

EQUIPMENT SPECIFICATION

35	Type:	☐ Elevated	☑ Enclosed		Equipment Design:		
36		☐ Above Ground			Component	Material / Size / Rating / Other	
37		☑ Stack	☐ Multiple Stack		Burner		
38		☐ Portable / Trailer			Burner Tip / Assist Gas Burner	304 SS	
39					Burner Body	Carbon Steel	
40	Smokeless By:	☐ Steam	☐ Assist Air		Pilot		
41		☐ Gas Assist	☑ Staging		Pilot Tip	304 SS	
42					Pilot Line(s)	Carbon Steel	
43	Stack:	☑ Self Supporting			Firebox / Stack		
44	Flare Burner:	☐ Non-Smokeless	☑ Smokeless	☐ Gas Assist	Shell	Carbon Steel	
45	Pilot:	☑ Intermittent	☐ Continuous		Piping	Carbon Steel	
46	Pilot Air Inspirator:	☑ Local	☐ Remote		Nozzles	Carbon Steel	
47	Pilot Flame Control:	☐ No	☑ Yes (Thermocouple)		Flanges	Carbon Steel	
48					Insulation	Blanket	
49	Pilot Ignition:	☐ Flamefront Generator	☑ Inspirating Ignitor		Insulation Pins	304 SS	
50		☐ Electronic	☑ Automatic	☐ Manual	Refractory	NA	
51		☐ With Pilot Flame Control			Refractory Anchors	NA	
52		☐ With Auto Pilot Re-Ignition			Ladders and Platforms	NA	
53					Stack Sample Connections	Per EPA requirements	
54	Pilot Ignition Backup:	☐ Manual	Specify: i.e Piezo-Electric		Sight Glass	2	
55		☐ Battery Pack			Other		

		Item/Tag No.:		Page	2	of	3
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		Project:		Date:	27 February 2014		
				By:	JS		
	Environmental Control Equipment	P.O. No.:	-	Checked:	SG		
	Data Sheet	RFQ No.:	-	Approved:	MS		
	Client:	Ref. P&ID:	-				
	Site:			Supplier:	LEED FABRICATION		
	Unit/Lease:	Remarks:	-	Model No.:	L30-0011-00		

EQUIPMENT SPECIFICATION

56	**Flame Detection:**	☐ Thermocouple ☑ Ionization Rod	**Auxiliary Equipment**		
57		☐ UV Scanner	Valves	NA	
58	**General Configuration:**		Blowers	NA	
59			Dampers	NA	
60			Inlet KO / Liquid Seal	NA	
61			Flame / Detonation Arrestor	Yes	
62			**Instrumentation & Controls**		
63			Solenoids / Shut-Off Valves	Check with Sales for available config.	
64			Flow Meters	NA	
65			Calorimeter	NA	
66			Pressure Switches/Transmitters	NA	
67			Thermocouples	Check with Sales for available config.	
68			Temperature Switches/Transmitters	NA	
69			BMS	Check with Sales for available config.	
70			CEMS	NA	
71			Other	NA	
72					
73					
74					
75					

FABRICATION AND INSPECTION

76	**Special requirements**	☐ Skid Mounted ☑ Concrete Pad	**Equipment Info**	
77		☐ Other	**Component**	**Weight / Dimensions**
78			**Burner**	
79	**Inspection**	☑ Vendor Standard	Burner Assembly	
80		☐ Other. Specify:	**Stack**	
81	**Material Certification**	☑ Vendor Standard	Stack Assembly	48 " OD x 25 ' H
82		☐ MTR	Pilot Tip	
83		☐ Certificate of Compliance	Pilot Line(s)	
84		☐ Other (Specify):	Stack Assembly	
85	**NDE**	☑ Vendor Standard	**Auxiliary Equipment**	
86		☐ Radiography. Specify:	Blowers	
87		☐ Ultrasonic. Specify:	Inlet KO / Liquid Seal	
88		☐ Liquid Penetrant.	Flame / Detonation Arrestor	
89		☐ Magnetic Particles.	Skid	
90		☐ PMI. Specify:	**Instrumentation & Controls**	
91		☐ Other. Specify:	BMS	
92	**Surface Preparation**	☑ Vendor Standard	Control Panel	
93		☐ Other. Specify:		
94	**Paint System**	☑ Vendor Standard		
95		☐ Other. Specify:		
96	**Finished Color**	☑ Vendor Standard		
97		☐ Other. Specify:		
98				
99				

Additional Notes:

		Item/Tag No.:		Page	3	of	3
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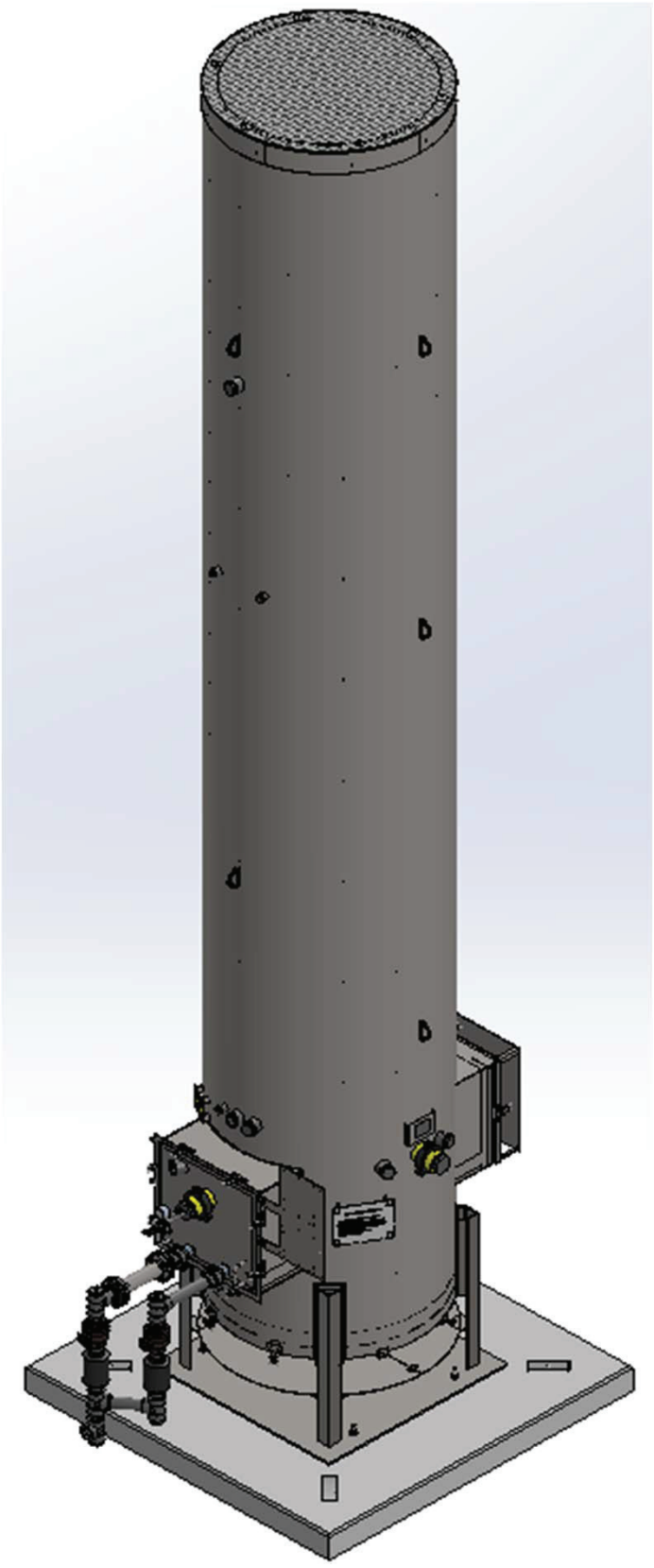
				By:	JS		
Environmental Control Equipment Data Sheet		P.O. No.:	-	Checked:	SG		
		RFQ No.:	-	Approved:	MS		
Client:		Ref. P&ID:	-				
Site:				Supplier:	LEED FABRICATION		
Unit/Lease:		Remarks:	-	Model No.:	L30-0011-00		

GENERAL ARRANGEMENT



§ MMBTU/hr values are calculated based on 1500 BTU/scf gas

Flare Size	# of Orifices (N)	Pressure (OZ/in^2)	m^3/s	mSCFD	MMBTU/hr
18	2	1	0.0021	6.34	0.39
18	2	2	0.0029	8.97	0.56
18	2	3	0.0036	10.99	0.68
18	2	4	0.0042	12.69	0.78
18	2	5	0.0046	14.18	0.88
18	2	6	0.0051	15.54	0.96
18	2	7	0.0055	16.78	1.04
18	2	8	0.0059	17.94	1.11
18	2	9	0.0062	19.03	1.18
18	2	10	0.0066	20.06	1.24
18	2	11	0.0069	21.04	1.30
18	2	12	0.0072	21.97	1.36
18	2	13	0.0075	22.87	1.42
18	2	14	0.0078	23.73	1.47
18	2	15	0.0081	24.57	1.52
18	2	16	0.0083	25.37	1.57
18	2	17	0.0086	26.15	1.62
18	2	18	0.0088	26.91	1.67
24	4	1	0.0042	12.69	0.78
24	4	2	0.0059	17.94	1.11
24	4	3	0.0072	21.97	1.36
24	4	4	0.0083	25.37	1.57
24	4	5	0.0093	28.37	1.76
24	4	6	0.0102	31.08	1.92
24	4	7	0.0110	33.56	2.08
24	4	8	0.0118	35.88	2.22
24	4	9	0.0125	38.06	2.35
24	4	10	0.0131	40.12	2.48
24	4	11	0.0138	42.08	2.60
24	4	12	0.0144	43.95	2.72
24	4	13	0.0150	45.74	2.83
24	4	14	0.0156	47.47	2.94
24	4	15	0.0161	49.13	3.04
24	4	16	0.0166	50.75	3.14
24	4	17	0.0171	52.31	3.24
24	4	18	0.0176	53.82	3.33
36	10	1	0.0104	31.72	1.96
36	10	2	0.0147	44.85	2.78
36	10	3	0.0180	54.93	3.40

36	10	4	0.0208	63.43	3.92
36	10	5	0.0232	70.92	4.39
36	10	6	0.0255	77.69	4.81
36	10	7	0.0275	83.91	5.19
36	10	8	0.0294	89.71	5.55
36	10	9	0.0312	95.15	5.89
36	10	10	0.0329	100.29	6.21
36	10	11	0.0345	105.19	6.51
36	10	12	0.0360	109.87	6.80
36	10	13	0.0375	114.35	7.08
36	10	14	0.0389	118.67	7.34
36	10	15	0.0403	122.83	7.60
36	10	16	0.0416	126.86	7.85
36	10	17	0.0429	130.77	8.09
36	10	18	0.0441	134.56	8.33
48	14	1	0.0146	44.40	2.75
48	14	2	0.0206	62.79	3.89
48	14	3	0.0252	76.91	4.76
48	14	4	0.0291	88.80	5.49
48	14	5	0.0325	99.29	6.14
48	14	6	0.0356	108.76	6.73
48	14	7	0.0385	117.48	7.27
48	14	8	0.0412	125.59	7.77
48	14	9	0.0437	133.21	8.24
48	14	10	0.0460	140.41	8.69
48	14	11	0.0483	147.27	9.11
48	14	12	0.0504	153.81	9.52
48	14	13	0.0525	160.09	9.91
48	14	14	0.0545	166.14	10.28
48	14	15	0.0564	171.97	10.64
48	14	16	0.0582	177.61	10.99
48	14	17	0.0600	183.07	11.33
48	14	18	0.0617	188.38	11.66

Attachment S

EMISSION CALCULATIONS

Line Heaters S001 - S002

Pollutant	Emission Factor	Emission Factor Units	Emission Factor Basis / Source	Boiler Rating (MMBtu/hr)	Heat Value of Natural Gas (Btu/scf)	Annual Operating Hours	Max. Hourly Emissions. (lb/hr)	Max. Annual Emissions. (tpy)
VOC's	5.5	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	0.020	0.09
Hexane	1.8	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	<0.01	0.03
Formaldehyde	0.075	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	<0.01	<0.01
Benzene	0.0021	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	<0.01	<0.01
Toluene	0.0034	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	<0.01	<0.01
Pb	0.0005	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	<0.01	<0.01
CO	84	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	0.30	1.31
NO_x	100	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	0.36	1.56
$PM_{Filterable}$	1.9	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	<0.01	0.03
$PM_{Condensable}$	5.7	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	0.02	0.09
PM_{Total}	7.6	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	0.03	0.12
SO_2	0.6	lb/10^6 scf	AP-42 Chapter 1.4	4.50	1,262	8,760	<0.01	<0.01
CO_2	53.06	kg CO_2 / MMBtu	40CFR98 Subpart C	4.50	1,262	8,760	526.40	2305.62
CH_4	0.001	kg CH_4 / MMBtu	40CFR98 Subpart C	4.50	1,262	8,760	<0.01	0.043
N_2O	0.0001	kg N_2O / MMBtu	40CFR98 Subpart C	4.50	1,262	8,760	<0.01	<0.01
Total HAPs							<0.01	0.03
Total CO_2e							526.94	2308.00

Notes:

- Emission rates displayed above represent the max. hourly and max. annual emissions for one line heater. Cumulative emission rates for both line heaters are diplayed in the Total Site Emissions Table.
- Greenhouse Gas Emissions are calculated using 40 CFR 98 Subpart C Table C-1 and C-2 emission factors.
- AP-42, Chapter 1.4 references are from the July 1998 revision.
- Max. Annual Emissions based upon Max. Hourly Emissions @ 8760 hr/yr.
- CO_2 equivalency solved for using Global Warming Potentials found in 40CFR98 Table A-1 (Updated January 2014). GWP CO_2=1, GWP CH_4=25, GWP N_2O=298

Example Equations:

Max. Hourly Emission Rate **(lb/hr) =** Emission Factor **(lb/10^6 scf)** ÷ Heating Value of Natural Gas **(Btu/scf)** x Boiler Rating (**MMBtu/hr)**

Line Heaters S003

Pollutant	Emission Factor	Emission Factor Units	Emission Factor Basis / Source	Boiler Rating (MMBtu/hr)	Heat Value of Natural Gas (Btu/scf)	Annual Operating Hours	Max. Hourly Emissions. (lb/hr)	Max. Annual Emissions. (tpy)
VOC's	5.5	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	<0.01	0.03
Hexane	1.8	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	<0.01	<0.01
Formaldehyde	0.075	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	<0.01	<0.01
Benzene	0.0021	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	<0.01	<0.01
Toluene	0.0034	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	<0.01	<0.01
Pb	0.0005	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	<0.01	<0.01
CO	84	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	0.10	0.45
NO_x	100	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	0.12	0.53
$PM_{Filterable}$	1.9	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	<0.01	0.01
$PM_{Condensable}$	5.7	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	<0.01	0.03
PM_{Total}	7.6	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	<0.01	0.04
SO_2	0.6	lb/10^6 scf	AP-42 Chapter 1.4	1.54	1,262	8,760	<0.01	<0.01
CO_2	53.06	kg CO_2 / MMBtu	40CFR98 Subpart C	1.54	1,262	8,760	180.14	789.03
CH_4	0.001	kg CH_4 / MMBtu	40CFR98 Subpart C	1.54	1,262	8,760	<0.01	0.015
N_2O	0.0001	kg N_2O / MMBtu	40CFR98 Subpart C	1.54	1,262	8,760	<0.01	<0.01
Total HAPs							<0.01	0.01
Total CO_2e							180.33	789.85

Notes:

- Emission rates displayed above represent the max. hourly and max. annual emissions for one line heater. Cumulative emission rates for this line heater is diplayed in the Total Site Emissions Table.
- Greenhouse Gas Emissions are calculated using 40 CFR 98 Subpart C Table C-1 and C-2 emission factors.
- AP-42, Chapter 1.4 references are from the July 1998 revision.
- Max. Annual Emissions based upon Max. Hourly Emissions @ 8760 hr/yr.
- CO_2 equivalency solved for using Global Warming Potentials found in 40CFR98 Table A-1 (Updated January 2014). GWP CO_2=1, GWP CH_4=25, GWP N_2O=298

Example Equations:

Max. Hourly Emission Rate **(lb/hr) =** Emission Factor **(lb/10^6 scf)** ÷ Heating Value of Natural Gas **(Btu/scf)** x Boiler Rating (**MMBtu/hr)**

Line Heaters S028

Pollutant	Emission Factor	Emission Factor Units	Emission Factor Basis / Source	Boiler Rating (MMBtu/hr)	Heat Value of Natural Gas (Btu/scf)	Annual Operating Hours	Max. Hourly Emissions. (lb/hr)	Max. Annual Emissions. (tpy)
VOC's	5.5	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	<0.01	0.02
Hexane	1.8	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	<0.01	<0.01
Formaldehyde	0.075	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	<0.01	<0.01
Benzene	0.0021	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	<0.01	<0.01
Toluene	0.0034	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	<0.01	<0.01
Pb	0.0005	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	<0.01	<0.01
CO	84	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	0.08	0.34
NO_x	100	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	0.09	0.40
$PM_{Filterable}$	1.9	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	<0.01	<0.01
$PM_{Condensable}$	5.7	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	<0.01	0.02
PM_{Total}	7.6	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	<0.01	0.03
SO_2	0.6	lb/10^6 scf	AP-42 Chapter 1.4	1.15	1,262	8,760	<0.01	<0.01
CO_2	53.06	kg CO_2 / MMBtu	40CFR98 Subpart C	1.15	1,262	8,760	134.52	589.21
CH_4	0.001	kg CH_4 / MMBtu	40CFR98 Subpart C	1.15	1,262	8,760	<0.01	0.011
N_2O	0.0001	kg N_2O / MMBtu	40CFR98 Subpart C	1.15	1,262	8,760	<0.01	<0.01
Total HAPs							<0.01	<0.01
Total CO_2e							134.66	589.82

Notes:

- Emission rates displayed above represent the max. hourly and max. annual emissions for one line heater. Cumulative emission rates for this line heater is diplayed in the Total Site Emissions Table.
- Greenhouse Gas Emissions are calculated using 40 CFR 98 Subpart C Table C-1 and C-2 emission factors.
- AP-42, Chapter 1.4 references are from the July 1998 revision.
- Max. Annual Emissions based upon Max. Hourly Emissions @ 8760 hr/yr.
- CO_2 equivalency solved for using Global Warming Potentials found in 40CFR98 Table A-1 (Updated January 2014). GWP CO_2=1, GWP CH_4=25, GWP N_2O=298

Example Equations:

Max. Hourly Emission Rate **(lb/hr) =** Emission Factor **(lb/10^6 scf)** ÷ Heating Value of Natural Gas **(Btu/scf)** x Boiler Rating (**MMBtu/hr)**

Thermoelectric Generators S024 & S025

Pollutant	Emission Factor	Emission Factor Units	Emission Factor Basis / Source	Boiler Rating (MMBtu/hr)	Heat Value of Natural Gas (Btu/scf)	Annual Operating Hours	Max. Hourly Emissions. (lb/hr)	Max. Annual Emissions. (tpy)
VOC's	5.5	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
Hexane	1.8	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
Formaldehyde	0.075	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
Benzene	0.0021	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
Toluene	0.0034	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
Pb	0.0005	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
CO	84	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
NO_x	100	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
$PM_{Filterable}$	1.9	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
$PM_{Condensable}$	5.7	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
PM_{Total}	7.6	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
SO_2	0.6	lb/10^6 scf	AP-42 Chapter 1.4	0.013	1,262	8,760	<0.01	<0.01
CO_2	53.06	kg CO_2 / MMBtu	40CFR98 Subpart C	0.013	1,262	8,760	1.52	6.66
CH_4	0.001	kg CH_4 / MMBtu	40CFR98 Subpart C	0.013	1,262	8,760	<0.01	<0.01
N_2O	0.0001	kg N_2O / MMBtu	40CFR98 Subpart C	0.013	1,262	8,760	<0.01	<0.01
Total HAPs							<0.01	<0.01
Total CO_2e							1.52	6.67

Notes:

- Emission rates displayed above represent the max. hourly and max. annual emissions for one TEG. Cumulative emission rates for both TEGs are diplayed in the Total Site Emissions Table.
- Greenhouse Gas Emissions are calculated using 40 CFR 98 Subpart C Table C-1 and C-2 emission factors.
- AP-42, Chapter 1.4 references are from the July 1998 revision.
- Max. Annual Emissions based upon Max. Hourly Emissions @ 8760 hr/yr.
- CO_2 equivalency solved for using Global Warming Potentials found in 40CFR98 Table A-1 (Updated January 2014). GWP CO_2=1, GWP CH_4=25, GWP N_2O=298

Example Equations:

Max. Hourly Emission Rate **(lb/hr) =** Emission Factor **(lb/10^6 scf)** ÷ Heating Value of Natural Gas **(Btu/scf)** x Boiler Rating (**MMBtu/hr)**

Natural Gas Compressor Engine S027

Pollutant	Emission Factor	Emission Factor Units	Emission Factor Basis / Source	Engine Rating (bhp)	Engine Rating (kW)	Fuel Consumption (Btu/bhp-hr)	Heat Value of Natural Gas (Btu/scf)	Annual Operating Hours	Hourly Emissions (lb/hr)	Annual Emissions (tpy)
VOC's	0.90	g/kW-hr	Vendor Guarantee	110.0	82.0	6,553	1,262	8,760	0.16	0.71
Formaldehyde	2.05E-02	lb/MMBtu	AP-42 Chapter 3.2	110.0	82.0	6,553	1,262	8,760	0.01	0.06
Benzene	1.58E-03	lb/MMBtu	AP-42 Chapter 3.2	110.0	82.0	6,553	1,262	8,760	<0.01	<0.01
Toluene	5.58E-04	lb/MMBtu	AP-42 Chapter 3.2	110.0	82.0	6,553	1,262	8,760	<0.01	<0.01
Ethylbenzene	2.48E-05	lb/MMBtu	AP-42 Chapter 3.2	110.0	82.0	6,553	1,262	8,760	<0.01	<0.01
Xylene	1.95E-04	lb/MMBtu	AP-42 Chapter 3.2	110.0	82.0	6,553	1,262	8,760	<0.01	<0.01
CO	2.70	g/kW-hr	Vendor Guarantee	110.0	82.0	6,553	1,262	8,760	0.49	2.14
NO_x	1.30	g/kW-hr	Vendor Guarantee	110.0	82.0	6,553	1,262	8,760	0.24	1.03
$PM_{Filterable}$	9.50E-03	lb/MMBtu	AP-42 Chapter 3.2	110.0	82.0	6,553	1,262	8,760	<0.01	0.03
$PM_{Condensable}$	9.91E-03	lb/MMBtu	AP-42 Chapter 3.2	110.0	82.0	6,553	1,262	8,760	<0.01	0.03
PM_{Total}	1.94E-02	lb/MMBtu	AP-42 Chapter 3.2	110.0	82.0	6,553	1,262	8,760	0.01	0.06
SO_2	5.88E-04	lb/MMBtu	AP-42 Chapter 3.2	110.0	82.0	6,553	1,262	8,760	<0.01	<0.01
CO_2	53.06	kg CO_2 / MMBtu	40 CFR Subpart C	110.0	82.0	6,553	1,262	8,760	82.49	361.32
CH_4	0.001	kg CH_4 / MMBtu	40 CFR Subpart C	110.0	82.0	6,553	1,262	8,760	<0.01	<0.01
N_2O	0.0001	kg N_2O / MMBtu	40 CFR Subpart C	110.0	82.0	6,553	1,262	8,760	<0.01	<0.01
Total HAPs									0.02	0.07
Total CO_2e									82.58	361.69

Notes:

- Emission rates displayed above represent the max. hourly and max. annual emissions for one NG compressor.
- Greenhouse Gas Emissions are calculated using 40 CFR 98 Subpart C Table C-1 and C-2 emission factors.
- AP-42, Chapter 3.2, Table 3.2-3 - Uncontrolled Emission Factors for 4-Stroke Rich Burn Engines
- Max. Annual Emissions based upon Max. Hourly Emissions @ 8760 hr/yr.
- CO_2 equivalency solved for using Global Warming Potentials found in 40 CFR 98 Table A-1 (Updated January 2014). GWP CO_2=1, GWP CH_4=25, GWP N_2O=298
- Vendor Guarantee Emissions are listed in Attachment S
- Vendor Guarantee Emissions are converted from g/kW-hr to g/bhp-hr. 1 kW = 1.34 bhp

Example Equations:

Max. Hourly Emission Rate **(lb/hr) =** Emission Factor **(lb/10^6 scf)** ÷ Heating Value of Natural Gas **(Btu/scf)** x Boiler Rating (**MMBtu/hr)**

Produced Fluids Tanks S011 - S020

Pollutant	Max. Hourly Emissions using ProMax (lb/hr)	Max. Yearly Emissions using ProMax (tons/yr)
VOCs	25.43	111.37
HAPs	1.21	5.28
Hexane	1.08	4.74
Benzene	0.03	0.11
Toluene	0.08	0.37
Ethylbenzene	<0.01	0.02
Xylene	<0.01	0.03
CO_2	0.07	0.30
CH_4	0.85	3.73
Total CO_2e	21.38	93.64

Notes:

- Emission rates for Produced Fluid Tanks S011 - S020 were calculated using ProMax software. ProMax output sheets for the OXF 157 Pad are attached.
- The emission rates displayed above are pre-control device emissions.
- CO_2 equivalency solved for using Global Warming Potentials found in 40CFR98 Table A-1 (Updated January 2014). GWP CO_2=1, GWP CH_4=25, GWP N_2O=298
- For emission calculation purposes, the total throughput for tanks S011 - S020 is modeled as being received through a single tank. The throughput value represents the total throughput for all ten (10) 400-barrel tanks. Therefore, emission rates represent a total from all produced fluids tanks located on the well pad. Actual throughput for each tank will vary based on operations.

Sand Trap Blow Tank S026

Pollutant	Max. Hourly Emissions using ProMax (lb/hr)	Max. Yearly Emissions using ProMax (tons/yr)
VOCs	9.02	1.65
HAPs	0.40	0.07
Hexane	0.36	0.07
Benzene	<0.01	<0.01
Toluene	0.03	<0.01
Ethylbenzene	<0.01	<0.01
Xylene	<0.01	<0.01
CO_2	0.05	<0.01
CH_4	2.63	0.48
Total CO_2e	65.74	12.00

Notes:

- Blowdown operations are conducted on the OXF 157 pad daily to allow for the removal of fluids from the sand traps. Based on available operational information, blowdowns are assummed to occur for one hour per day.
- Emissions from the Sand Trap Blowdown Tank are routed to an enclosed combustion device. The values displayed above a pre-control emission rates.
- Emission rates for the Sand Trap Blowdown Tank were calculated using ProMax software. ProMax output sheets for the OXF 157 Pad are attached.
- CO_2 equivalency solved for using Global Warming Potentials found in 40CFR98 Table A-1. GWP CO_2=1, GWP CH_4=25, GWP N_2O=298

Tank Unloading Operations S023

Total Emissions from Tank Unloading Operations

Pollutant	Max. Hourly Emissions (lb/hr)	Max. Yearly Emissions (tons/yr)	Loading Rack Collection Efficiency	Enclosed Combustion Device Combusion Efficiency	Post-Control Max. Yearly Emissions (lb/hr)	Post-Control Max. Yearly Emissions (tons/yr)	Max. Hourly Emissions Not Collected by Loading Rack (lb/hr)	Max. Hourly Emissions Not Collected by Loading Rack (tons/yr)
VOCs	0.50	2.19	70%	98%	<0.01	0.03	0.15	0.66
HAPs	0.02	0.07	70%	98%	<0.01	<0.01	<0.01	0.02
CO_2	<0.01	0.02	70%	98%	2.29	10.05	<0.01	<0.01
CH_4	0.01	0.05	70%	98%	<0.01	<0.01	<0.01	0.01
Total CO_2e	0.29	1.26	--	--	2.30	10.07	0.09	0.38

Notes:

- Emission rates for liquid unloading operations were calculated using ProMax software. ProMax summary sheets are attached.
- Vapors from tank unloading operations are vapor-balanced to the produced fluid tanks and realized at one of the two enclosed combustion devices. AP-42 calculation methods were used to estimate the collection efficiency from tank unloading operations. Emissions that are not collected during the unloading events are realized at the Loading Rack Emission Point, E020.

Enclosed Ground Flares C021 - C022

Emissions from Tanks

Input to Enclosed Combustion Device	Pollutant	Amount of Gas Sent to Enclosed Combustion Device (lbs/hr)	Amount of Gas Sent to Enclosed Combustion Device (tons/year)	Enclosed Combustion Device Combustion Efficiency	Max. Hourly Emissions (lb/hr)	Max. Yearly Emissions (tons/yr)
Produced Fluids Tanks S008 - S015	VOCs	12.71	55.68	98%	0.25	1.11
	HAPs	0.60	2.64	98%	0.01	0.05
	Hexane	0.54	2.37	98%	0.01	0.05
	Benzene	0.01	0.06	98%	<0.01	<0.01
	Toluene	0.04	0.18	98%	<0.01	<0.01
	Ethylbenzene	<0.01	0.01	98%	<0.01	<0.01
	Xylene	<0.01	0.02	98%	<0.01	<0.01
	CO_2	0.03	0.15	98%	262.98	1,151.87
	CH_4	0.43	1.87	98%	<0.01	0.04
Sand Trap Blowdown Tank - S016	VOCs	4.51	0.82	98%	0.09	0.02
	HAPs	0.20	0.04	98%	<0.01	<0.01
	Hexane	0.18	0.03	98%	<0.01	<0.01
	Benzene	<0.01	<0.01	98%	<0.01	<0.01
	Toluene	0.01	<0.01	98%	<0.01	<0.01
	Ethylbenzene	<0.01	<0.01	98%	<0.01	<0.01
	Xylene	<0.01	<0.01	98%	<0.01	<0.01
	CO_2	0.02	<0.01	98%	5.21	22.83
	CH_4	1.31	0.24	98%	0.03	<0.01
Truck Loading - S017	VOCs	0.25	1.09	98%	<0.01	0.02
	HAPs	<0.01	0.03	98%	<0.01	<0.01
	CO_2	<0.01	0.01	98%	1.15	5.02
	CH_4	<0.01	0.02	98%	<0.01	<0.01
Totals	VOCs	17.47	57.60	--	0.35	1.15
	HAPs	0.81	2.71	--	0.02	0.05
	Hexane	0.72	2.40	--	0.01	0.05
	Benzene	0.02	0.06	--	<0.01	<0.01
	Toluene	0.06	0.19	--	<0.01	<0.01
	Ethylbenzene	<0.01	0.01	--	<0.01	<0.01
	Xylene	<0.01	0.02	--	<0.01	<0.01
	CO_2	0.06	0.17	--	269.34	1,179.72
	CH_4	1.75	2.13	--	0.03	0.04
	CO2e	43.70	53.45	--	270.21	1,180.78

Gas Composition of Vent Gas

Gas Stream	Mole Fraction
Methane	0.12
Ethane	0.25
Propane	0.25
Butane	0.16
Pentanes	0.06
Carbon Dioxide	0.007

Vent Gas Properties

Vent Gas Properties	Mass Flow Rate (lb/hr)	Density (lb/ft^3)
Produced Fluids Tank	101.30	0.10
Blowdown Tank	1.63	0.08

Emissions from Pilot Operations

Pollutant	Emission Factor ($lb/10^6$ scf)	Emission Factors (kg XX/MMBtu)	Heat Value of Natural Gas (Btu/scf)	Enclosed Ground Flare Pilot Rating (Btu/hr)	Enclosed Ground Flare Burner Rating (Btu/hr)	Pilot Max. Hourly Emissions (lb/yr)	Pilot Max. Hourly Emissions (tons/yr)	Burner Max.Hourly Emissions (lb/hr)	Burner Max.Hourly Emissions (tons/hr)	Max. Hourly Emissions (lb/hr)	Max. Yearly Emissions (tons/yr)
VOCs	5.50	--	1,262	30,000	11,660,000	<0.01	<0.01	--	--	<0.01	<0.01
Hexane	1.80	--	1,262	30,000	11,660,000	<0.01	<0.01	--	--	<0.01	<0.01
Formaldehyde	0.075	--	1,262	30,000	11,660,000	<0.01	<0.01	--	--	<0.01	<0.01
CO	84	--	1,262	30,000	11,660,000	<0.01	0.01	0.90	3.94	0.90	3.95
NO_x	100	--	1,262	30,000	11,660,000	<0.01	0.01	1.07	4.69	1.07	4.71
$PM_{Condensable}$	5.70	--	1,262	30,000	11,660,000	<0.01	<0.01	0.06	0.27	0.06	0.27
$PM_{Filterable}$	1.90	--	1,262	30,000	11,660,000	<0.01	<0.01	0.02	0.09	0.02	0.09
PM_{Total}	7.60	--	1,262	30,000	11,660,000	<0.01	<0.01	0.08	0.36	0.08	0.36
SO_2	0.60	--	1,262	30,000	11,660,000	<0.01	<0.01	<0.01	0.03	<0.01	0.03
CO_2	120,000	53.06	1,262	30,000	11,660,000	3.51	15.37	1,363.95	5,974.12	1,367.46	5,989.49
CH_4	2.3	0.001	1,262	30,000	11,660,000	<0.01	<0.01	0.03	0.11	0.03	0.11
N_2O	2.2	<0.001	1,262	30,000	11,660,000	<0.01	<0.01	<0.01	0.01	<0.01	0.01
Total HAPs										<0.01	<0.01
CO_2e										1,368.88	5,995.67

Total Enclosed Combustion Device Emissions

Pollutant	Max. Hourly Emissions (lb/hr)	Max. Yearly Emissions (tons/yr)
VOCs	0.35	1.15
HAPs	0.02	0.05
CO	0.90	3.95
NO_x	1.07	4.71
$PM_{Condensable}$	0.06	0.27
$PM_{Filterable}$	0.02	0.09
PM_{Total}	0.08	0.36
SO_2	<0.01	0.03
CO_2	1,636.81	7,169.21
CH_4	0.06	0.16
N_2O	<0.01	0.01
CO_2e	1,639.09	7,176.46

Notes:

- Emissions from Enclosed Combustion Device Operations from AP-42, Chapter 1.4 references are from the July 1998 revision.
- Greenhouse Gas Emissions from the Enclosed Combustion Device Pilot and Burner calculated using 40 CFR 98 Subpart C Table C-1 and C-2 emission factors.
- Max. Annual Emissions based upon Max. Hourly Emissions @ 8760 hr/yr.
- CO_2 equivalency solved for using Global Warming Potentials found in 40CFR98 Table A-1 (Updated January 2014). GWP CO_2=1, GWP CH_4=25, GWP N_2O=298

Example Calculations:

- Emissions from Tanks VOCs (lb/hr) = Amount of Gas sent to Enclosed Combustion Device (lb/hr) x 0.02 = Max. Hourly Emissions (lb/hr)
- Emissions from Enclosed Combustion Device Operations (lb/hr) = Emission factor (lb/106 Btu) x Heat Value of Natural Gas (Btu/scf) ÷ 1,000,000 x Enclosed Combustion Device Pilot Gas Usage (mcfd) x 1,000 ÷ 24
- Emissions from Enclosed Combustion Device Vapor Destruction CO2 Methodologies shown below sample equation
- Emissions from Enclosed Combustion Device Operations CO2 (tons/yr) = ((Enclosed Combustion Device Pilot Gas Usage (mcfd) x 1,000 x 365 x Fraction of Gas Combusted by Enclosed Combustion Device x Mole Fraction of Methane x Number of Carbon Atoms in Methane) + … + (Enclosed Combustion Device Pilot Gas Usage (mcfd) x 1,000 x 365 x Fraction of Gas Combusted by Enclosed Combustion Device x Mole Fraction of Pentanes-plus x Number of Carbon Atoms in Pentanes-plus)) x .0526 (kg/ft3) CO2 x .001 x 1.102 tons/tonnes

$$E_{a,CH4}(un-combusted) = V_a * (1-\eta) * X_{CH4} \qquad \text{(Eq. W-19)}$$

$$E_{a,CO2}(un-combusted) = V_a * X_{CO2} \qquad \text{(Eq. W-20)}$$

$$E_{a,CO2}(combusted) = \sum_{J=1}^{5} (\eta * V_a * Y_j * R_j) \qquad \text{(Eq. W-21)}$$

Where:

Ea,CH_4(un-combusted) = Contribution of annual un-combusted CH4 emissions from Enclosed Combustion Device stack in cubic feet, under actual conditions.

Ea,CO_2(un-combusted) = Contribution of annual un-combusted CO2 emissions from Enclosed Combustion Device stack in cubic feet, under actual conditions.

Ea,CO_2(combusted) = Contribution of annual combusted CO2 emissions from Enclosed Combustion Device stack in cubic feet, under actual conditions.

Va = Volume of gas sent to Enclosed Combustion Device in cubic feet, during the year.

η = Fraction of gas combusted by a burning Enclosed Combustion Device (default is 0.98). For gas sent to an unlit Enclosed Combustion Device, η is zero.

XCH4 = Mole fraction of CH4 in gas to the Enclosed Combustion Device.

XCO2 = Mole fraction of CO2 in gas to the Enclosed Combustion Device.

Y_j = Mole fraction of gas hydrocarbon constituents j (such as methane, ethane, propane, butane, and pentanes-plus).

R_j = Number of carbon atoms in the gas hydrocarbon constituent j: 1 for methane, 2 for ethane, 3 for propane, 4 for butane, and 5 for pentanes plus).

Fugitive Emissions from Unpaved Haul Roads

Constant	Industrial Roads		
	PM	PM-10	PM-2.5
k (lb/VMT)	4.9	1.5	0.15
a	0.7	0.9	0.9
b	0.45	0.45	0.45

where

k		Particle size multiplier [1]
s	4.8	Silt content of road surface material (%) [2]
p	150	Number of days per year with precipitation >0.01 in. [3]

Item Number	Description	Number of Wheels	W Mean Vehicle Weight (tons)	Mean Vehicle Speed (mph)	Miles per Trip	Maximum Trips per Hour	Maximum Trips per Year	Control Device ID Number	Control Efficiency (%)	PM Emissions (lbs/hr)	PM Emissions (tons/yr)	PM-10 Emissions (lbs/hr)	PM-10 Emissions (tons/yr)	PM-2.5 Emissions (lbs/hr)	PM-2.5 Emissions (tons/yr)
1	Liquids Hauling	14	30	10	1.72	1	1,826	NA	NA	7.37	6.73	1.88	1.71	0.19	0.171
2	Employee Vehicles	4	3	10	1.72	1	200	NA	NA	2.61	0.26	0.67	0.07	0.07	<0.01
									Totals:	**9.98**	**6.99**	**2.54**	**1.78**	**0.25**	**0.178**

Notes:

[1] - Particle Size Multiplier used from AP-42 13.2.2 - Final Version 11/2006

[2] - Silt Content of Road Surface uses Sand and Gravel Processing Plant Road from AP-42 13.2.2 - Final Version 11/2006

[3] - Number of days per year with precipitation >0.01 in[3] found using AP-42 13.2.2 Figure 13.2.2-1 - Final Version 11/2006

Example Calculations:

Emissions (lb/Vehicle Mile Traveled) - $E = k \times (s/12)^a \times (W/3)^b$ Equation 1a from AP-42 13.2.2 - Final Version 11/2006

Size Specific Emissions (lb/VMT) - $E_{ext} = E[(365-p)/365]$ Equation 2 from AP-42 13.2.2 - Final Version 11/2006

Fugitive Leaks

Default Average Component Counts for Major Onshore Natural Gas Production Equipment[1]				
Facility Equipment Type	Valves	Connectors	Open-ended Lines	Pressure Relief Valves
Wellheads	8	38	0.5	0
Separators	1	6	0	0
Meters/Piping	12	45	0	0
Compressors	12	57	0	0
In-line Heaters	14	65	2	1
Dehydrators	24	90	2	2

[1]- Table W-1B to 40CFR98 Subpart W

Well Specific Equipment Counts	
Facility Equipment Type	Count on Site
Wellheads	7
Separators	3
Meters/Piping	4
Compressors	1
In-line Heaters	3
Dehydrators	0

Gas Composition						
Emissions from Flaring Operations	Propane	Butane	Pentanes	Hexanes +	CO_2	CH_4
Mole %	4.0036	0.5947	0.6411	0.5767	0.15	78.13
MW	44	58	72	86.00	44.00	16.00

Fugitive Emissions															
Facility Equipment Type	Total Count	Emission Rate (scf/hr/component)[2]	Hours of Operation	VOCs (lbs/hr)	VOCs (tons/yr)	Hexane (lbs/hr)	Hexane (tons/yr)	HAPs (lbs/hr)	HAPs (tons/yr)	CO_2 (lbs/hr)	CO_2 (tons/yr)	CH_4 (lbs/hr)	CH_4 (tons/yr)	Total CO_2e (lbs/hr)	Total CO_2e (tons/yr)
Valves	152	0.027	8760	0.03	0.12	<0.01	0.02	<0.01	0.02	<0.01	<0.01	0.13	0.58	3.33	14.58
Connectors	661	0.003	8760	0.01	0.06	<0.01	0.01	<0.01	0.01	<0.01	<0.01	0.06	0.28	1.61	7.04
Open-ended Lines	10	0.061	8760	<0.01	0.02	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	0.02	0.09	0.49	2.17
Pressure Relief Valves	4	0.040	8760	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	0.02	0.13	0.57
			Total Emissions:	**0.05**	**0.20**	**<0.01**	0.04	**<0.01**	**0.04**	**<0.01**	**<0.01**	**0.22**	**0.97**	**5.56**	**24.35**

[2]- Table W-1A to 40CFR98 Subpart W

Notes:
-A gas sample from the OXF-157 Site is included with this submittal

Example Equations:
Fugitive Emissions (lb/hr) = Count x Emission Rate x Hours of Operation ÷ 385.5 scf/lbmol x mol VOC's

Total OXF 157 Site Emission Levels

	VOCs		HAPs		CO		NO_x		PM_{Total}		$PM_{Filterable}$		$PM_{Condensable}$		SO_2		CO_2		CH_4		N_2O		CO_2e	
Emission Sources	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**
Line Heater (E001)	0.02	0.09	<0.01	0.03	0.30	1.31	0.36	1.56	0.03	0.12	<0.01	0.03	0.02	0.09	<0.01	<0.01	526.40	2,305.62	<0.01	0.04	<0.01	<0.01	526.94	2,308.00
Line Heater (E002)	0.02	0.09	<0.01	0.03	0.30	1.31	0.36	1.56	0.03	0.12	<0.01	0.03	0.02	0.09	<0.01	<0.01	526.40	2,305.62	<0.01	0.04	<0.01	<0.01	526.94	2,308.00
Line Heater (E003)	<0.01	0.03	<0.01	0.01	0.10	0.45	0.12	0.53	<0.01	0.04	<0.01	0.01	<0.01	0.03	<0.01	<0.01	180.14	789.03	<0.01	0.01	<0.01	<0.01	180.33	789.85
Enclosed Combustion Unit (E021)	0.35	1.15	0.02	0.05	0.90	3.95	1.07	4.71	0.08	0.36	0.02	0.09	0.06	0.27	<0.01	0.03	1,636.81	7,169.21	0.06	0.16	<0.01	0.01	1,639.09	7,176.46
Enclosed Combustion Unit (E022)	0.35	1.15	0.02	0.05	0.90	3.95	1.07	4.71	0.08	0.36	0.02	0.09	0.06	0.27	<0.01	0.03	1,636.81	7,169.21	0.06	0.16	<0.01	0.01	1,639.09	7,176.46
*Tank Truck Loading Operations (E023)	0.15	0.66	<0.01	0.02	<0.01	<0.01	<0.01	<0.01	--	--	--	--	--	--	<0.01	<0.01	<0.01	<0.01	<0.01	0.01	<0.01	<0.01	0.09	0.38
TEG (E024)	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	1.52	6.66	<0.01	<0.01	<0.01	<0.01	1.52	6.67
TEG (E025)	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	1.52	6.66	<0.01	<0.01	<0.01	<0.01	1.52	6.67
Compressor Engine (E027)	0.14	0.63	0.02	0.07	3.72	16.31	0.14	0.63	0.014	0.06	<0.01	0.03	<0.01	0.03	<0.01	<0.01	82.49	361.32	<0.01	<0.01	<0.01	<0.01	82.58	361.69
Line Heater (S028)	<0.01	0.02	<0.01	<0.01	0.08	0.34	0.09	0.40	<0.01	0.03	<0.01	<0.01	<0.01	0.02	<0.01	<0.01	134.52	589.21	<0.01	0.011	<0.01	<0.01	134.66	589.82
Haul Roads	--	--	--	--	--	--	--	--	9.98	6.99	9.98	6.99	<0.01	<0.01	--	--	--	--	--	--	--	--	--	--
Fugitives Leaks	0.05	0.20	<0.01	0.04	--	--	--	--	--	--	--	--	--	--	--	--	<0.01	<0.01	0.22	0.97	--	--	5.56	24.35
Totals	**1.09**	**4.01**	**0.08**	**0.32**	**6.31**	**27.63**	**3.22**	**14.11**	**10.23**	**8.07**	**10.05**	**7.27**	**0.18**	**0.80**	**0.02**	**0.08**	**4,726.61**	**20,702.56**	**0.37**	**1.42**	**0.01**	**0.03**	**4,738.32**	**20,748.35**

-Two enclosed combustion devices are being included in this application. Emissions from the produced fluids tanks, sand trap blowdown tanks, and truck loading are routed to either C021 or C022. For the permitting of these sources, it is assumed that vapors are being evenly distributed between the two enclosed combustion devices. For this reason, the emissions from the combustion of vent gases between C021 and C022 are additive.

*Emissions from Tank Truck Loading Operations are routed to the enclosed combustion devices. The collection efficiency of the vapors has been calculated using AP-42 methodologies. Emissions that are not collected and routed the enclosed combustion devices are realized at the Tank Truck Loading Operations Emission Point.

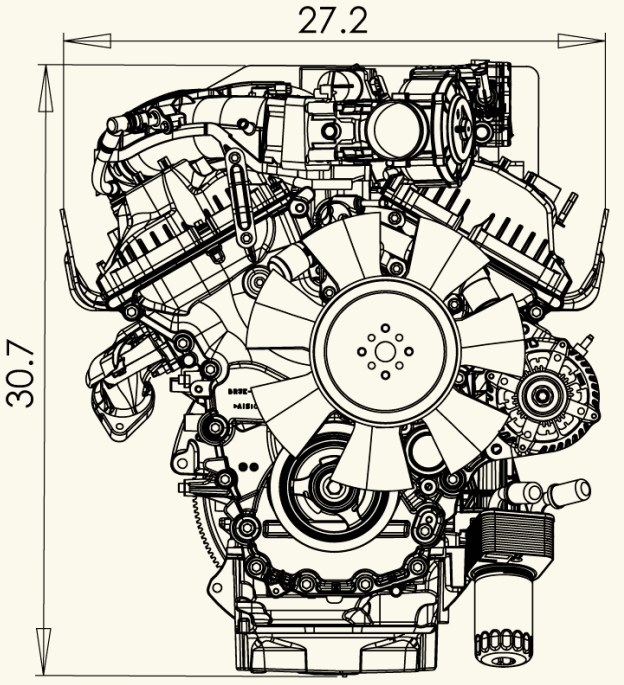
Total OXF 157 Site Emission Levels - HAP Speciation

	Total HAPs		Formaldehyde		Hexane		Benzene		Toluene		Ethylbenzene		Xylene	
Emission Sources	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**	**lb/hr**	**tons/yr**
Line Heater (E001)	<0.01	0.03	<0.01	<0.01	<0.01	0.03	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
Line Heater (E002)	<0.01	0.03	<0.01	<0.01	<0.01	0.03	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
Line Heater (E003)	<0.01	0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
Enclosed Combustion Unit (E021)	0.02	0.05	<0.01	<0.01	0.01	0.05	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
Enclosed Combustion Unit (E022)	0.02	0.05	<0.01	<0.01	0.01	0.05	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
Tank Truck Loading Activities (E023)	<0.01	0.02	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
TEG (E024)	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
TEG (E025)	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
Compressor Engine (E027)	0.02	0.07	0.01	0.06	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
Line Heater (E028)	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
Haul Roads	--	--	--	--	--	--	--	--	--	--	--	--	--	--
Fugitives Leaks	<0.01	0.04	<0.01	<0.01	0.01	0.04	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
Totals	**0.08**	**0.32**	**0.02**	**0.07**	**0.06**	**0.23**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**

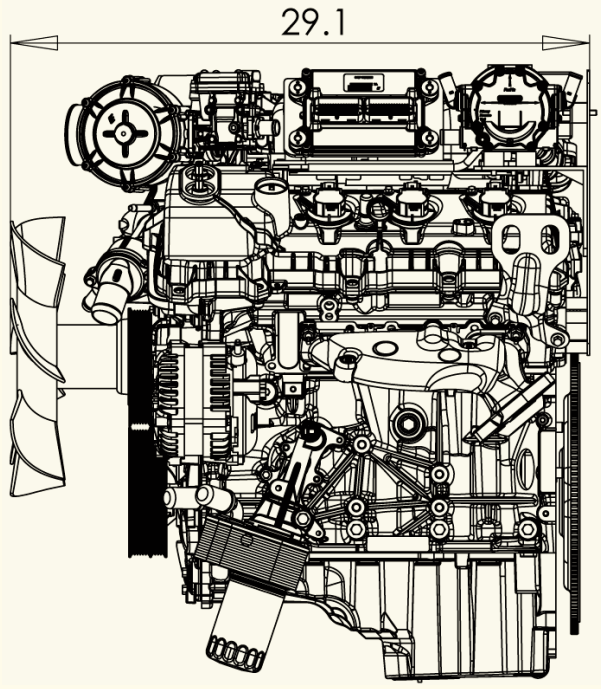
-Two enclosed combustion devices are being included in this application. Emissions from the produced fluids tanks, sand trap blowdown tanks, and truck loading are routed to either C021 or C022. For the permitting of these sources, it is assumed that vapors are being evenly distributed between the two enclosed combustion devices. For this reason, the emissions from the combustion of vent gases between C021 and C022 are additive.

Installation Drawings

Front End View

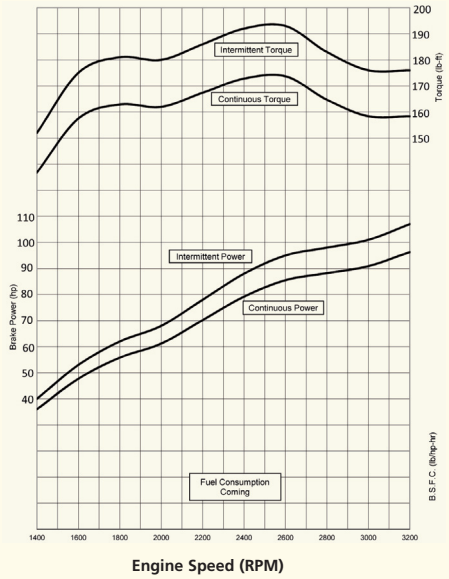


Left Side View

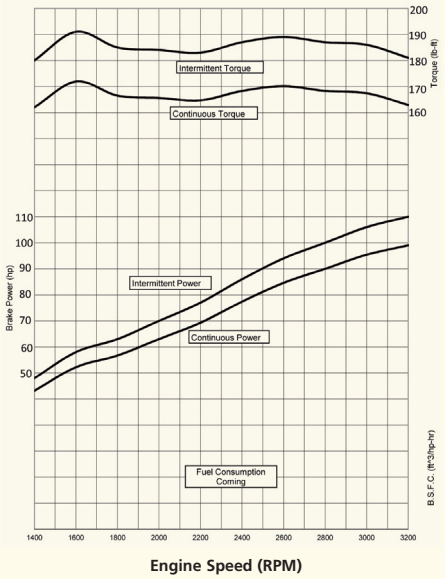


Power Curves (corrected per SAE J1349)

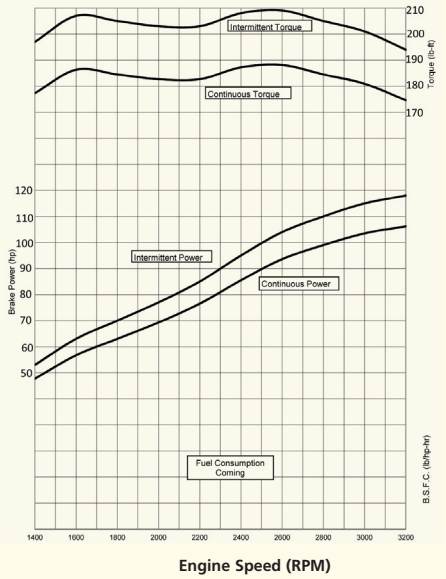
Gasoline



Natural Gas



Liquefied Petroleum Gas



Ford Power Products

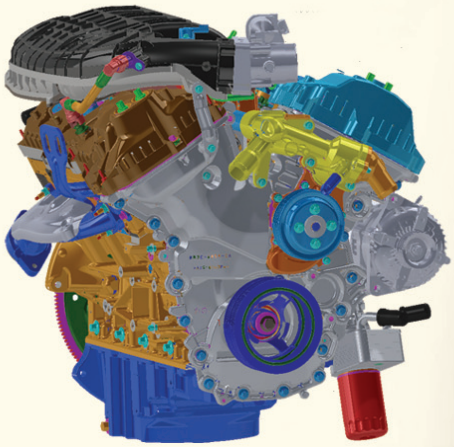
Powertrain Assemblies & Components Provided By Ford Component Sales

For additional information Contact:

ENGINE DISTRIBUTORS INC.
400 University Ct • Blackwood NJ 08012
856/228-7298 • Fax:856/228-5531
www.edi-dist.com

CSG-637 EFI

3.7 Liter
6-Cylinder



Options

Engine Cooling Fans
- 14" (355mm) diameter suction
- 14" (355mm) diameter pusher

Flywheels
- 11.5" (292mm) SAE over-center clutch
- flat face flywheel

Flywheel Housings
- SAE #3

Exhaust Manifold
- rear dump down

Power Steering Pump
Air Conditioning
Wiring Harnesses
Discrete Speed Switch
Variable Speed Hand Throttle
Variable Speed Foot Pedal
Engine Mounts
- Automotive with insulators
- Open power unit

Electronic Instrument Panel, Gauges
Three Way Catalyst / Muffler Standard

Transmissions

6R80 electronic shift

Emissions Information

California Air Resources Board (CARB)
Environmental Protection Agency (EPA)
Emission Certified Packages

Warranty

Contact Engine Distributors, Inc
for warranty details.

Power Products

Powertrain Assemblies
& Components
Provided By Ford
Component Sales

Specifications

Engine Type	V-6
Bore and Stroke	3.7"x 3.4" (94mm x 86mm)
Displacement	3.7L Liter (225.7 CID)
Compression Ratio	10.5:1
Oil Capacity	6 qts. including filter
Net Weight	355 Lbs. with accessories (161 Kgs.)
Dimensions	L 25.4" x W 29.5" x H 29.4" (646 mm x 751 mm x 748 mm)

Gasoline (corrected per SAE J1349)

Unleaded 87 or 89 octane

Intermittent Power	107 [HP] @ 3200rpm	(80 [kW] @ 3200rpm)
Continuous Power	96 [HP] @ 3200rpm	(72 [kW] @ 3200rpm)
Intermittent Torque	193 [ft-lbs] @ 2600rpm	(261 [N-m] @ 2600rpm)
Continuous Torque	173 [ft-lbs] @ 2600rpm	(235 [N-m] @ 3200rpm)

Natural Gas (corrected per SAE J1349)

Fuel Specification	1050 BTU/FT3	
Intermittent Power	110 [HP] @ 3200rpm	(82 [kW] @ 3200rpm)
Continuous Power	99 [HP] @ 3200rpm	(74 [kW] @ 3200rpm)
Intermittent Torque	191 [ft-lbs] @1600rpm	(259 [N-m] @ 1600rpm)
Continuous Torque	172 [ft-lbs] @1600rpm	(233 [N-m] @ 1600rpm)

Liquefied Petroleum Gas (corrected per SAE J1349)

Fuel Specification	HD-5	
Intermittent Power	118 [HP] @ 3200rpm	(88 [kW] @ 3200rpm)
Continuous Power	106 [HP] @ 3200rpm	(79 [kW] @ 3200rpm)
Intermittent Torque	209 [ft-lbs] @ 2600rpm	(284 [N-m] @ 2600rpm)
Continuous Torque	188 [ft-lbs] @ 2600rpm	(255 [N-m] @ 2600rpm)

Standard Features / Benefits

Set-for-life valvetrain

Deep skirted, ribbed cylinder block casting for rigidity

150 AMP Alternator

Aluminum cylinder block and heads.

Chain driven dual camshafts with automatic tensioning system

Structural front cover and deep sump oil pan

Alternate fuel ready valvetrain components

Individual coil on plug electronic ignition

Four main bolts with side bolts through block for strength and durability

Gasoline Sequential Port Fuel Injection

Closed loop fuel control for all fuels

Electronic engine management system with built-in engine protection against detonation, high coolant temperature, low oil pressure, over speed shutdown and starter lockout

Next generation governing – discrete speeds, variable speeds, drive by wire – using the highest quality components.

Variable CAM Timing for intake camshafts - advances or retards timing to maximize engine power and fuel efficiency

Forged steel crankshaft

UNITED STATES ENVIRONMENTAL PROTECTION AGENCY
2015 MODEL YEAR
CERTIFICATE OF CONFORMITY
WITH THE CLEAN AIR ACT

OFFICE OF TRANSPORTATION AND AIR QUALITY
ANN ARBOR, MICHIGAN 48105

Certificate Issued To: **Engine Distributors, Inc.**
(U.S. Manufacturer or Importer)

Certificate Number: FEDIB03.7CSG-006

Effective Date: 06/08/2015

Expiration Date: 12/31/2015

Byron J. Bunker, Division Director
Compliance Division

Issue Date: 06/08/2015

Revision Date: N/A

Manufacturer: Engine Distributors, Inc.
Engine Family: FEDIB03.7CSG
Mobile/Stationary Certification Type: Mobile and Stationary
Fuel : LPG/Propane
Gasoline (up to and including 10% Ethanol)
Natural Gas (CNG/LNG)
Emission Standards :
Mobile Part 1048
HC + NOx (g/kW-hr) : 0.8
NMHC + NOx (g/kW-hr) : 0.8
CO (g/kW-hr) : 20.6
Part 60 Subpart JJJ Table 1
NOx (g/kW-hr) : 1.3
HC + NOx (g/kW-hr) : 0.8
CO (g/kW-hr) : 2.7
CO (g/kW-hr) : 20.6
VOC (g/kW-hr) : 0.9
Emergency Use Only : N

Pursuant to Section 213 of the Clean Air Act (42 U.S.C. section 7547) and 40 CFR Part 60, 40 CFR Part 1048, 1065, 1068, and 60 (stationary only and combined stationary and mobile) and subject to the terms and conditions prescribed in those provisions, this certificate of conformity is hereby issued with respect to the test engines which have been found to conform to applicable requirements and which represent the following nonroad engines, by engine family, more fully described in the documentation required by 40 CFR Part 60, 40 CFR Part 1048 and produced in the stated model year.

This certificate of conformity covers only those new nonroad spark-ignition engines which conform in all material respects to the design specifications that applied to those engines described in the documentation required by 40 CFR Part 60, 40 CFR Part 1048 and which are produced during the model year stated on this certificate of the said manufacturer, as defined in 40 CFR Part 60, 40 CFR Part 1048. This certificate of conformity does not cover nonroad engines imported prior to the effective date of the certificate.

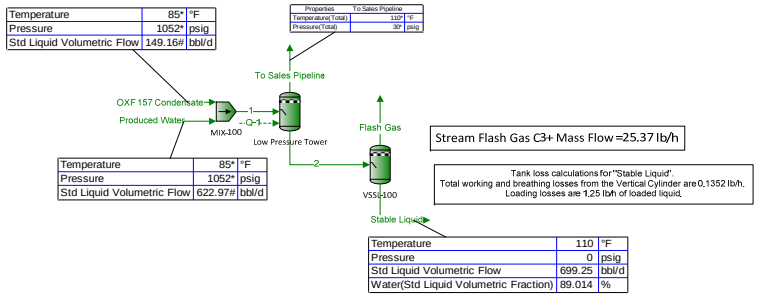
It is a term of this certificate that the manufacturer shall consent to all inspections described in 40 CFR 1068.20 and authorized in a warrant or court order. Failure to comply with the requirements of such a warrant or court order may lead to revocation or suspension of this certificate for reasons specified in 40 CFR Part 60, 40 CFR Part 1048. It is also a term of this certificate that this certificate may be revoked or suspended or rendered void *ab initio* for other reasons specified in 40 CFR Part 60, 40 CFR Part 1048.

This certificate does not cover large nonroad engines sold, offered for sale, or introduced, or delivered for introduction, into commerce in the U.S. prior to the effective date of the certificate.

Flowsheet1
Plant Schematic

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	
Flowsheet:	Flowsheet1	

EQT OFX 157 Well Pad
50% Contingency
Low Pressure Tower



Note
Working, Breathing and Loading losses include non-VOC components

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	
Flowsheet:	Flowsheet1	

Connections

	Flash Gas	OXF 157 Condensate	Produced Water	Stable Liquid	To Sales Pipeline
From Block	VSSL-100	--	--	VSSL-100	Low Pressure Tower
To Block	--	MIX-100	MIX-100	--	--

Stream Composition

Mole Fraction	Flash Gas %	OXF 157 Condensate %	Produced Water %	Stable Liquid %	To Sales Pipeline %
Nitrogen	0	0 *	0 *	0	0
Methane	8.32097	26.433 *	0 *	0.000707399	40.5321
Carbon Dioxide	0.240258	0.185 *	0 *	0.000121767	0.270608
Ethane	17.5442	16.284 *	0 *	0.00641273	24.1538
Propane	22.9327	11.163 *	0 *	0.0259113	15.2231
i-Butane	6.20486	2.473 *	0 *	0.0161198	2.92461
n-Butane	15.4698	6.13 *	0 *	0.0552111	6.6654
i-Pentane	5.84189	2.814 *	0 *	0.0504969	2.16345
n-Pentane	5.91275	3.189 *	0 *	0.0664904	2.13318
Isohexane	2.85278	2.494 *	0 *	0.072354	0.978584
n-Hexane	1.96482	2.13 *	0 *	0.066791	0.668178
2,2,4-Trimethylpentane	0.00369484	0.009 *	0 *	0.000329426	0.00124721
Benzene	0.0506547	0.058 *	0 *	0.00184704	0.0172533
Heptane	2.58139	6.585 *	0 *	0.242254	0.871805
Toluene	0.141744	0.418 *	0 *	0.015607	0.0476736
Octane	0.990468	6.744 *	0 *	0.264811	0.336183
Ethylbenzene	0.00802174	0.064 *	0 *	0.00252717	0.00271836
o-Xylene	0.0105591	0.108 *	0 *	0.00429471	0.0035838
Nonane	0.230475	4.256 *	0 *	0.171123	0.078586
Decane	0.166734	8.463 *	0 *	0.343228	0.0578905
Water	8.53125	0 *	100 *	98.5934	2.87004

Molar Flow	Flash Gas lbmol/h	OXF 157 Condensate lbmol/h	Produced Water lbmol/h	Stable Liquid lbmol/h	To Sales Pipeline lbmol/h
Nitrogen	0	0 *	0 *	0	0
Methane	0.0530635	5.50868 *	0 *	0.00361679	5.452
Carbon Dioxide	0.00153214	0.0385543 *	0 *	0.00062257	0.0363996
Ethane	0.111881	3.39361 *	0 *	0.032787	3.24895
Propane	0.146243	2.32639 *	0 *	0.132479	2.04767
i-Butane	0.0395689	0.515378 *	0 *	0.0824175	0.393391
n-Butane	0.0986519	1.2775 *	0 *	0.282283	0.896568
i-Pentane	0.0372542	0.586443 *	0 *	0.258181	0.291008
n-Pentane	0.037706	0.664593 *	0 *	0.339952	0.286935
Isohexane	0.0181924	0.519754 *	0 *	0.369932	0.13163
n-Hexane	0.0125298	0.443896 *	0 *	0.341489	0.0898771
2,2,4-Trimethylpentane	2.35623E-05	0.00187562 *	0 *	0.00168429	0.000167763
Benzene	0.000323029	0.0120873 *	0 *	0.00944352	0.00232075
Heptane	0.0164617	1.37233 *	0 *	1.2386	0.117267
Toluene	0.000903913	0.087112 *	0 *	0.0797954	0.00641261
Octane	0.00631629	1.40546 *	0 *	1.35393	0.0452202
Ethylbenzene	5.11553E-05	0.0133377 *	0 *	0.0129209	0.000365649
o-Xylene	6.73363E-05	0.0225074 *	0 *	0.021958	0.00048206
Nonane	0.00146976	0.886958 *	0 *	0.874918	0.0105707
Decane	0.00106327	1.7637 *	0 *	1.75485	0.00778689
Water	0.0544044	0 *	504.529 *	504.088	0.386052

Mass Fraction	Flash Gas %	OXF 157 Condensate %	Produced Water %	Stable Liquid %	To Sales Pipeline %
Nitrogen	0	0 *	0 *	0	0

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	
Flowsheet:	Flowsheet1	

Mass Fraction	Flash Gas %	OXF 157 Condensate %	Produced Water %	Stable Liquid %	To Sales Pipeline %
Methane	2.77868	7.08145 *	0 *	0.000588072	19.8768
Carbon Dioxide	0.220099	0.135964 *	0 *	0.000277697	0.364051
Ethane	10.9811	8.17683 *	0 *	0.00999212	22.2015
Propane	21.0496	8.22017 *	0 *	0.0592079	20.5198
i-Butane	7.50702	2.40033 *	0 *	0.048551	5.1962
n-Butane	18.7163	5.94986 *	0 *	0.166289	11.8425
i-Pentane	8.77356	3.39045 *	0 *	0.188795	4.77147
n-Pentane	8.87998	3.84227 *	0 *	0.24859	4.7047
Isohexane	5.11735	3.58909 *	0 *	0.323103	2.57785
n-Hexane	3.52452	3.06526 *	0 *	0.298261	1.76016
2,2,4-Trimethylpentane	0.00878544	0.0171681 *	0 *	0.00194997	0.00435502
Benzene	0.0823626	0.0756571 *	0 *	0.00747631	0.0411969
Heptane	5.38423	11.0189 *	0 *	1.25789	2.67037
Toluene	0.271856	0.643164 *	0 *	0.074517	0.134275
Octane	2.3551	12.8646 *	0 *	1.56749	1.17389
Ethylbenzene	0.0177273	0.113466 *	0 *	0.0139031	0.00882196
o-Xylene	0.0233347	0.191474 *	0 *	0.0236271	0.0116306
Nonane	0.615308	9.11551 *	0 *	1.13731	0.308103
Decane	0.493818	20.1084 *	0 *	2.53062	0.251786
Water	3.19924	0 *	100 *	92.0416	1.58054

Mass Flow	Flash Gas lb/h	OXF 157 Condensate lb/h	Produced Water lb/h	Stable Liquid lb/h	To Sales Pipeline lb/h
Nitrogen	0	0 *	0 *	0	0
Methane	0.851268	88.3729 *	0 *	0.0580222	87.4636
Carbon Dioxide	0.0674288	1.69676 *	0 *	0.027399	1.60193
Ethane	3.36415	102.043 *	0 *	0.985873	97.6927
Propane	6.4487	102.584 *	0 *	5.84176	90.2931
i-Butane	2.29983	29.9549 *	0 *	4.79029	22.8648
n-Butane	5.73387	74.2513 *	0 *	16.4069	52.1105
i-Pentane	2.68784	42.3111 *	0 *	18.6274	20.9959
n-Pentane	2.72044	47.9496 *	0 *	24.5271	20.702
Isohexane	1.56773	44.79 *	0 *	31.879	11.3433
n-Hexane	1.07976	38.2529 *	0 *	29.4279	7.74519
2,2,4-Trimethylpentane	0.00269148	0.214249 *	0 *	0.192394	0.0191633
Benzene	0.0252324	0.944162 *	0 *	0.737651	0.181278
Heptane	1.6495	137.51 *	0 *	124.11	11.7504
Toluene	0.0832851	8.02636 *	0 *	7.35223	0.590847
Octane	0.7215	160.544 *	0 *	154.657	5.16544
Ethylbenzene	0.0054309	1.416 *	0 *	1.37175	0.0388191
o-Xylene	0.00714876	2.3895 *	0 *	2.33117	0.0511779
Nonane	0.188504	113.757 *	0 *	112.213	1.35574
Decane	0.151285	250.943 *	0 *	249.684	1.10793
Water	0.980111	0 *	9089.23 *	9081.29	6.95483

Stream Properties

Property	Units	Flash Gas	OXF 157 Condensate	Produced Water	Stable Liquid	To Sales Pipeline
Temperature	°F	109.505	85 *	85 *	109.505	110 *
Pressure	psia	14.6959 *	1066.7 *	1066.7 *	14.6959	44.6959 *
Mole Fraction Vapor	%	100	0	0	0	100
Mole Fraction Light Liquid	%	0	100	100	1.40621	0
Mole Fraction Heavy Liquid	%	0	0	0	98.5938	0
Molecular Weight	lb/lbmol	48.0404	59.8819	18.0153	19.2977	32.7133
Mass Density	lb/ft^3	0.117487	36.5724	62.1827	59.6665	0.244859
Molar Flow	lbmol/h	0.637707	20.8402	504.529	511.28	13.4511
Mass Flow	lb/h	30.6357	1247.95	9089.23	9866.51	440.029
Vapor Volumetric Flow	ft^3/h	260.757	34.1227	146.17	165.361	1797.07

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	
Flowsheet:	Flowsheet1	

Stream Properties

Property	Units	Flash Gas	OXF 157 Condensate	Produced Water	Stable Liquid	To Sales Pipeline
Liquid Volumetric Flow	gpm	32.51	4.25426	18.2238	20.6164	224.05
Std Vapor Volumetric Flow	MMSCFD	0.005808	0.189805	4.59506	4.65655	0.122507
Std Liquid Volumetric Flow	sgpm	0.113164	4.35041 *	18.17 *	20.3947	2.01255
Compressibility		0.983791	0.298803	0.0528707	0.000778148	0.976761
Specific Gravity		1.6587	0.586387	0.997012	0.956668	1.1295
API Gravity			103.133	9.88462	14.8213	
Enthalpy	Btu/h	-34706	-1.35147E+06	-6.19047E+07	-6.2377E+07	-565355
Mass Enthalpy	Btu/lb	-1132.86	-1082.95	-6810.78	-6322.1	-1284.81
Mass Cp	Btu/(lb*°F)	0.425934	0.568968	0.980315	0.945576	0.452621
Ideal Gas CpCv Ratio		1.10826	1.08825	1.32512	1.29881	1.15747
Dynamic Viscosity	cP	0.00872559	0.176	0.840918	0.606498	0.00995828
Kinematic Viscosity	cSt	4.63642	0.300426	0.844235	0.632397	2.53891
Thermal Conductivity	Btu/(h*ft*°F)	0.0113867	0.0642775	0.353848	0.330872	0.014946
Surface Tension	lbf/ft		0.000441128 ?	0.00492858	0.00435669 ?	
Net Ideal Gas Heating Value	Btu/ft^3	2414.76	3087.49	0	77.8937	1708.29
Net Liquid Heating Value	Btu/lb	18892.4	19419.4	-1059.76	543.734	19677.1
Gross Ideal Gas Heating Value	Btu/ft^3	2624.31	3343.77	50.31	133.568	1866.3
Gross Liquid Heating Value	Btu/lb	20547.7	21043.5	0	1638.55	21510

Remarks

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	
Flowsheet:	Flowsheet1	

Connections

	1	2			
From Block	MIX-100	Low Pressure Tower			
To Block	Low Pressure Tower	VSSL-100			

Stream Composition

Mole Fraction	1 %	2 %			
Nitrogen	0	0			
Methane	1.04854	0.0110721			
Carbon Dioxide	0.00733853	0.00042091			
Ethane	0.645949	0.0282599			
Propane	0.442811	0.0544468			
i-Butane	0.0980983	0.0238293			
n-Butane	0.243163	0.0744133			
i-Pentane	0.111625	0.0577114			
n-Pentane	0.1265	0.0737732			
Isohexane	0.0989313	0.0758176			
n-Hexane	0.0844922	0.0691554			
2,2,4-Trimethylpentane	0.000357009	0.000333619			
Benzene	0.00230073	0.00190784			
Heptane	0.261212	0.245168			
Toluene	0.0165811	0.0157641			
Octane	0.267519	0.265715			
Ethylbenzene	0.00253873	0.00253401			
o-Xylene	0.00428411	0.00430251			
Nonane	0.168826	0.171197			
Decane	0.335708	0.343008			
Water	96.0332	98.4812			

Molar Flow	1 lbmol/h	2 lbmol/h			
Nitrogen	0	0			
Methane	5.50868	0.0566803			
Carbon Dioxide	0.0385543	0.00215471			
Ethane	3.39361	0.144668			
Propane	2.32639	0.278723			
i-Butane	0.515378	0.121986			
n-Butane	1.2775	0.380935			
i-Pentane	0.586443	0.295435			
n-Pentane	0.664593	0.377658			
Isohexane	0.519754	0.388124			
n-Hexane	0.443896	0.354019			
2,2,4-Trimethylpentane	0.00187562	0.00170785			
Benzene	0.0120873	0.00976655			
Heptane	1.37233	1.25506			
Toluene	0.087112	0.0806993			
Octane	1.40546	1.36024			
Ethylbenzene	0.0133377	0.0129721			
o-Xylene	0.0225074	0.0220253			
Nonane	0.886958	0.876387			
Decane	1.7637	1.75592			
Water	504.529	504.143			

Mass Fraction	1 %	2 %			
Nitrogen	0	0			
Methane	0.854903	0.0091874			
Carbon Dioxide	0.0164141	0.000958133			

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	
Flowsheet:	Flowsheet1	

Mass Fraction	1 %	2 %			
Ethane	0.987143	0.0439523			
Propane	0.992375	0.124182			
i-Butane	0.289778	0.071638			
n-Butane	0.718294	0.223709			
i-Pentane	0.40931	0.215368			
n-Pentane	0.463856	0.275307			
Isohexane	0.433291	0.337943			
n-Hexane	0.370052	0.308247			
2,2,4-Trimethylpentane	0.00207261	0.00197113			
Benzene	0.00913365	0.00770811			
Heptane	1.33024	1.27066			
Toluene	0.0776456	0.0751278			
Octane	1.55307	1.56993			
Ethylbenzene	0.0136981	0.0139149			
o-Xylene	0.0231156	0.0236262			
Nonane	1.10046	1.13569			
Decane	2.42758	2.52431			
Water	87.9276	91.7666			

Mass Flow	1 lb/h	2 lb/h			
Nitrogen	0	0			
Methane	88.3729	0.909291			
Carbon Dioxide	1.69676	0.0948278			
Ethane	102.043	4.35002			
Propane	102.584	12.2905			
i-Butane	29.9549	7.09012			
n-Butane	74.2513	22.1408			
i-Pentane	42.3111	21.3153			
n-Pentane	47.9496	27.2476			
Isohexane	44.79	33.4467			
n-Hexane	38.2529	30.5077			
2,2,4-Trimethylpentane	0.214249	0.195086			
Benzene	0.944162	0.762883			
Heptane	137.51	125.759			
Toluene	8.02636	7.43551			
Octane	160.544	155.378			
Ethylbenzene	1.416	1.37718			
o-Xylene	2.3895	2.33832			
Nonane	113.757	112.401			
Decane	250.943	249.835			
Water	9089.23	9082.27			

Stream Properties

Property	Units	1	2			
Temperature	°F	85.0825	110			
Pressure	psia	1066.7	44.6959			
Mole Fraction Vapor	%	0	0			
Mole Fraction Light Liquid	%	3.8523	1.51441			
Mole Fraction Heavy Liquid	%	96.1477	98.4856			
Molecular Weight	lb/lbmol	19.676	19.3335			
Mass Density	lb/ft^3	57.4083	59.534			
Molar Flow	lbmol/h	525.369	511.918			
Mass Flow	lb/h	10337.2	9897.15			
Vapor Volumetric Flow	ft^3/h	180.064	166.244			
Liquid Volumetric Flow	gpm	22.4496	20.7265			
Std Vapor Volumetric Flow	MMSCFD	4.78486	4.66236			
Std Liquid Volumetric Flow	sgpm	22.5204	20.5079			
Compressibility		0.0625375	0.00237424			
Specific Gravity		0.920462	0.954544			

* User Specified Values
? Extrapolated or Approximate Values

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	
Flowsheet:	Flowsheet1	

Stream Properties

Property	Units	1	2			
API Gravity		21.2003	15.1057			
Enthalpy	Btu/h	-6.32562E+07	-6.24117E+07			
Mass Enthalpy	Btu/lb	-6119.29	-6306.03			
Mass Cp	Btu/(lb*°F)	0.931469	0.944547			
Ideal Gas CpCv Ratio		1.29383	1.29811			
Dynamic Viscosity	cP	0.711141	0.59957			
Kinematic Viscosity	cSt	0.73824	0.625357			
Thermal Conductivity	Btu/(h*ft*°F)	0.298587	0.32957			
Surface Tension	lbf/ft	0.00408697 ?	0.0043327 ?			
Net Ideal Gas Heating Value	Btu/ft^3	122.474	80.8048			
Net Liquid Heating Value	Btu/lb	1412.57	600.53			
Gross Ideal Gas Heating Value	Btu/ft^3	180.954	136.67			
Gross Liquid Heating Value	Btu/lb	2540.47	1697.08			

Remarks

Energy Stream Report

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	
Flowsheet:	Flowsheet1	

Energy Streams

Energy Stream	Energy Rate	Power	From Block	To Block
Q-1	279086 Btu/h	109.685 hp	--	Low Pressure Tower

Remarks

Blocks
Low Pressure Tower
Separator Report

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	Modified: 10:53 AM, 1/21/2016
Flowsheet:	Flowsheet1	Status: Solved 9:11 AM, 2/4/2016

Connections

Stream	Connection Type	Other Block	Stream	Connection Type	Other Block
1	Inlet	MIX-100	To Sales Pipeline	Vapor Outlet	
2	Light Liquid Outlet	VSSL-100	Q-1	Energy	

Block Parameters

Pressure Drop	1022	psi	Main Liquid Phase	Light Liquid	
Mole Fraction Vapor	2.56031	%	Heat Duty	279086	Btu/h
Mole Fraction Light Liquid	1.47563	%	Heat Release Curve Type	Plug Flow	
Mole Fraction Heavy Liquid	95.9641	%	Heat Release Curve Increments	5	

Remarks

Blocks
MIX-100
Mixer/Splitter Report

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	Modified: 8:44 AM, 1/18/2016
Flowsheet:	Flowsheet1	Status: Solved 9:11 AM, 2/4/2016

Connections

Stream	Connection Type	Other Block	Stream	Connection Type	Other Block
Produced Water	Inlet		OXF 157 Condensate	Inlet	
1	Outlet	Low Pressure Tower			

Block Parameters

Pressure Drop	0 psi	Fraction to PStream 1	100 %

Remarks

Blocks
VSSL-100
Separator Report

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	Modified: 8:45 AM, 1/18/2016
Flowsheet:	Flowsheet1	Status: Solved 9:11 AM, 2/4/2016

Connections

Stream	Connection Type	Other Block	Stream	Connection Type	Other Block
2	Inlet	Low Pressure Tower	Flash Gas	Vapor Outlet	
Stable Liquid	Light Liquid Outlet				

Block Parameters

Pressure Drop	30	psi	Main Liquid Phase	Light Liquid	
Mole Fraction Vapor	0.124572	%	Heat Duty	0	Btu/h
Mole Fraction Light Liquid	1.40446	%	Heat Release Curve Type	Plug Flow	
Mole Fraction Heavy Liquid	98.471	%	Heat Release Curve Increments	5	

Remarks

Flowsheet Environment
Environment1

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	
Flowsheet:	Flowsheet1	

Environment Settings

Number of Poynting Intervals	0	Freeze Out Temperature Threshold Difference	10 °F
Gibbs Excess Model Evaluation Temperature	77 °F	Phase Tolerance	1 %

Components

Component Name	Henry`s Law Component	Phase Initiator	Component Name	Henry`s Law Component	Phase Initiator
Nitrogen	False	False	2,2,4-Trimethylpentane	False	False
Methane	False	False	Benzene	False	False
Carbon Dioxide	False	False	Heptane	False	False
Ethane	False	False	Toluene	False	False
Propane	False	False	Octane	False	False
i-Butane	False	False	Ethylbenzene	False	False
n-Butane	False	False	o-Xylene	False	False
i-Pentane	False	False	Nonane	False	False
n-Pentane	False	False	Decane	False	False
Isohexane	False	False	Water	False	True
n-Hexane	False	False			

Physical Property Method Sets

Liquid Molar Volume	COSTALD	Overall Package	Peng-Robinson
Stability Calculation	Peng-Robinson	Vapor Package	Peng-Robinson
Light Liquid Package	Peng-Robinson	Heavy Liquid Package	Peng-Robinson

Remarks

Calculator Report

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	

Simple Solver 1

Source Code

Residual Error (for CV1) = TP / 255225 - 1

Calculated Variable [CV1]

SourceMoniker	ProMax:ProMax!Project!Flowsheets!Flowsheet1!PStreams!OXF 157 Condensate!Phases!Total!Properties!Std Liquid Volumetric Flow
Value	149.157
Unit	bbl/d

Measured Variable [TP]

SourceMoniker	ProMax:ProMax!Project!Flowsheets!Flowsheet1!PStreams!Stable Liquid!Phases!Total!Properties!Std Liquid Volumetric Flow
Value	255225
Unit	bbl/yr

Solver Properties

Status: Solved

Error	9.3486E-07		Iterations	5
Calculated Value	4.35041	sgpm	Max Iterations	20
Lower Bound		sgpm	Weighting	1
Upper Bound		sgpm	Priority	0
Step Size		sgpm	Solver Active	Active
Is Minimizer	False		Group	
Algorithm	Default		Skip Dependency Check	False

Remarks

Simple Solver 2

Source Code

Residual Error (for CV1) = LF / 89 - 1

Calculated Variable [CV1]

SourceMoniker	ProMax:ProMax!Project!Flowsheets!Flowsheet1!PStreams!Produced Water!Phases!Total!Properties!Std Liquid Volumetric Flow
Value	622.972
Unit	bbl/d

Measured Variable [LF]

SourceMoniker	ProMax:ProMax!Project!Flowsheets!Flowsheet1!PStreams!Stable Liquid!Phases!Total!Composition!Std. Liquid Volumetric Fraction!Water
Value	89.014
Unit	%

Solver Properties

Status: Solved

Error	0.000157812		Iterations	5
Calculated Value	18.17	sgpm	Max Iterations	20
Lower Bound		sgpm	Weighting	1
Upper Bound		sgpm	Priority	0
Step Size		sgpm	Solver Active	Active
Is Minimizer	False		Group	
Algorithm	Default		Skip Dependency Check	False

Remarks

User Value Sets Report

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	

Cn+ Flow/Frac.

User Value [CnPlusSum]

* Parameter	25.3727	lb/h	Upper Bound	
Lower Bound		lb/h	* Enforce Bounds	False

Remarks
This User Value Set was programmatically generated. GUID={E867C485-3D3C-49CB-BC24-EA16096DB2B1}

Tank Losses.12

User Value [ShellLength]

* Parameter	20	ft	Upper Bound	
* Lower Bound	0	ft	* Enforce Bounds	False

User Value [ShellDiam]

* Parameter	12	ft	Upper Bound	
* Lower Bound	0	ft	* Enforce Bounds	False

User Value [BreatherVP]

* Parameter	0.03	psig	Upper Bound	
Lower Bound			* Enforce Bounds	False

User Value [BreatherVacP]

* Parameter	-0.03	psig	Upper Bound	
Lower Bound			* Enforce Bounds	False

User Value [DomeRadius]

Parameter		ft	Upper Bound	ft
Lower Bound		ft	* Enforce Bounds	False

User Value [OpPress]

* Parameter	0	psig	Upper Bound	
Lower Bound			* Enforce Bounds	False

User Value [AvgPercentLiq]

* Parameter	50	%	Upper Bound	
Lower Bound		%	* Enforce Bounds	False

User Value [MaxPercentLiq]

* Parameter	90	%	Upper Bound	
Lower Bound		%	* Enforce Bounds	False

User Value [AnnNetTP]

* Parameter	698.457	bbl/day	Upper Bound	
* Lower Bound	0	bbl/day	* Enforce Bounds	False

User Value [OREff]

* Parameter	0	%	Upper Bound	
Lower Bound		%	* Enforce Bounds	False

User Value [AtmPressure]

* Parameter	97274.7	Pa	Upper Bound	
Lower Bound			* Enforce Bounds	False

User Value Sets Report

Client Name:	EQT	Job: Low Pressure Tower
Location:	OXF 157 50% Contingency	

User Value [MaxLiqSurfaceT]

* Parameter	66.3119	°F	Upper Bound	
Lower Bound			* Enforce Bounds	False

User Value [TotalLosses]

* Parameter	0.135232	lb/h	Upper Bound	
Lower Bound		lb/h	* Enforce Bounds	False

User Value [WorkingLosses]

* Parameter	0.0178363	lb/h	Upper Bound	
Lower Bound		lb/h	* Enforce Bounds	False

User Value [StandingLosses]

* Parameter	0.00470245	lb/h	Upper Bound	
Lower Bound		lb/h	* Enforce Bounds	False

User Value [RimSealLosses]

* Parameter	0	lb/h	Upper Bound	
Lower Bound		lb/h	* Enforce Bounds	False

User Value [WithdrawalLoss]

* Parameter	0	lb/h	Upper Bound	
Lower Bound		lb/h	* Enforce Bounds	False

User Value [LoadingLosses]

* Parameter	1.24999	lb/h	Upper Bound	
Lower Bound		lb/h	* Enforce Bounds	False

User Value [DeckFittingLosses]

* Parameter	0	lb/h	Upper Bound	
Lower Bound		lb/h	* Enforce Bounds	False

User Value [DeckSeamLosses]

* Parameter	0	lb/h	Upper Bound	
Lower Bound		lb/h	* Enforce Bounds	False

User Value [FlashingLosses]

* Parameter	0	lb/h	Upper Bound	
Lower Bound		lb/h	* Enforce Bounds	False

User Value [GasMoleWeight]

* Parameter	0.0263203	kg/mol	Upper Bound	
Lower Bound			* Enforce Bounds	False

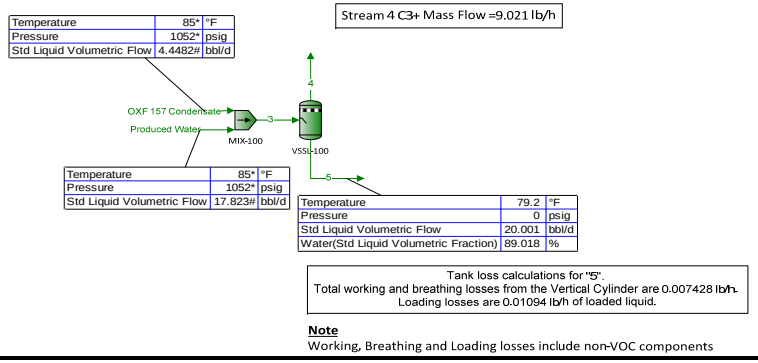
Remarks

This User Value Set was programmatically generated. GUID={797159D1-E12F-494E-9828-D6559CC49710}

Flowsheet1
Plant Schematic

Client Name:	EQT	Job:
Location:	OXF 157 Blowdown Tank	
Flowsheet:	Flowsheet1	

EQT OFX 157 Well Pad
Sand Trap Blowdown Tank



Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	EQT	Job:	
Location:	OXF 157 Blowdown Tank		
Flowsheet:	Flowsheet1		

Connections

	OXF 157 Condensate	Produced Water	3	4	5
From Block	--	--	MIX-100	VSSL-100	VSSL-100
To Block	MIX-100	MIX-100	VSSL-100	--	--

Stream Composition

Mole Fraction	OXF 157 Condensate %	Produced Water %	3 %	4 %	5 %
Nitrogen	0 *	0 *	0	0	0
Methane	26.433 *	0 *	1.09117	37.832	0.00354491
Carbon Dioxide	0.185 *	0 *	0.00763689	0.259872	0.000170097
Ethane	16.284 *	0 *	0.672212	23.0256	0.0104959
Propane	11.163 *	0 *	0.460814	15.2174	0.0239815
i-Butane	2.473 *	0 *	0.102087	3.13756	0.012229
n-Butane	6.13 *	0 *	0.253049	7.41968	0.0408991
i-Pentane	2.814 *	0 *	0.116163	2.71278	0.0392969
n-Pentane	3.189 *	0 *	0.131644	2.76432	0.0537096
Isohexane	2.494 *	0 *	0.102954	1.38207	0.0650886
n-Hexane	2.13 *	0 *	0.0879275	0.954826	0.0622651
2,2,4-Trimethylpentane	0.009 *	0 *	0.000371524	0.00179851	0.000329282
Benzene	0.058 *	0 *	0.00239427	0.0249651	0.00172612
Heptane	6.585 *	0 *	0.271832	1.22751	0.243542
Toluene	0.418 *	0 *	0.0172552	0.0682089	0.0157469
Octane	6.744 *	0 *	0.278396	0.437628	0.273682
Ethylbenzene	0.064 *	0 *	0.00264195	0.00355774	0.00261484
o-Xylene	0.108 *	0 *	0.00445829	0.00457818	0.00445475
Nonane	4.256 *	0 *	0.17569	0.0930973	0.178135
Decane	8.463 *	0 *	0.349357	0.0610687	0.357891
Water	0 *	100 *	95.872	3.37145	98.6102

Molar Flow	OXF 157 Condensate lbmol/h	Produced Water lbmol/h	3 lbmol/h	4 lbmol/h	5 lbmol/h
Nitrogen	0 *	0 *	0	0	0
Methane	0.16428 *	0 *	0.16428	0.163762	0.000518358
Carbon Dioxide	0.00114977 *	0 *	0.00114977	0.0011249	2.48727E-05
Ethane	0.101205 *	0 *	0.101205	0.0996699	0.00153478
Propane	0.0693778 *	0 *	0.0693778	0.0658711	0.00350672
i-Butane	0.0153696 *	0 *	0.0153696	0.0135814	0.0017882
n-Butane	0.0380978 *	0 *	0.0380978	0.0321173	0.00598052
i-Pentane	0.0174889 *	0 *	0.0174889	0.0117427	0.00574624
n-Pentane	0.0198196 *	0 *	0.0198196	0.0119658	0.00785375
Isohexane	0.0155002 *	0 *	0.0155002	0.00598249	0.00951766
n-Hexane	0.0132379 *	0 *	0.0132379	0.00413312	0.00910478
2,2,4-Trimethylpentane	5.59348E-05 *	0 *	5.59348E-05	7.78515E-06	4.81496E-05
Benzene	0.000360469 *	0 *	0.000360469	0.000108065	0.000252403
Heptane	0.0409256 *	0 *	0.0409256	0.00531347	0.0356121
Toluene	0.00259786 *	0 *	0.00259786	0.000295253	0.00230261
Octane	0.0419138 *	0 *	0.0419138	0.00189435	0.0400195
Ethylbenzene	0.000397759 *	0 *	0.000397759	1.54003E-05	0.000382358
o-Xylene	0.000671217 *	0 *	0.000671217	1.98174E-05	0.0006514
Nonane	0.0264509 *	0 *	0.0264509	0.000402987	0.026048
Decane	0.0525973 *	0 *	0.0525973	0.000264346	0.052333
Water	0 *	14.434 *	14.434	0.0145939	14.4194

Mass Fraction	OXF 157 Condensate %	Produced Water %	3 %	4 %	5 %
Nitrogen	0 *	0 *	0	0	0
Methane	7.08145 *	0 *	0.886619	17.5636	0.00294581

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	EQT	Job:
Location:	OXF 157 Blowdown Tank	
Flowsheet:	Flowsheet1	

Mass Fraction	OXF 157 Condensate %	Produced Water %	3 %	4 %	5 %
Carbon Dioxide	0.135964 *	0 *	0.0170231	0.33097	0.000387768
Ethane	8.17683 *	0 *	1.02376	20.0361	0.0163481
Propane	8.22017 *	0 *	1.02919	19.4186	0.0547773
i-Butane	2.40033 *	0 *	0.300529	5.27736	0.036818
n-Butane	5.94986 *	0 *	0.744941	12.4799	0.123136
i-Pentane	3.39045 *	0 *	0.424495	5.66404	0.146864
n-Pentane	3.84227 *	0 *	0.481064	5.77165	0.200729
Isohexane	3.58909 *	0 *	0.449365	3.44663	0.290547
n-Hexane	3.06526 *	0 *	0.38378	2.38117	0.277943
2,2,4-Trimethylpentane	0.0171681 *	0 *	0.0021495	0.00594526	0.00194837
Benzene	0.0756571 *	0 *	0.0094725	0.0564329	0.00698417
Heptane	11.0189 *	0 *	1.37959	3.55945	1.26409
Toluene	0.643164 *	0 *	0.0805261	0.181871	0.0751561
Octane	12.8646 *	0 *	1.61069	1.44665	1.61938
Ethylbenzene	0.113466 *	0 *	0.0142063	0.0109305	0.0143799
o-Xylene	0.191474 *	0 *	0.0239731	0.0140656	0.0244981
Nonane	9.11551 *	0 *	1.14129	0.345537	1.18345
Decane	20.1084 *	0 *	2.51764	0.251449	2.63772
Water	0 *	100 *	87.4797	1.75768	92.0219

Mass Flow	OXF 157 Condensate lb/h	Produced Water lb/h	3 lb/h	4 lb/h	5 lb/h
Nitrogen	0 *	0 *	0	0	0
Methane	2.63546 *	0 *	2.63546	2.62715	0.00831574
Carbon Dioxide	0.0506008 *	0 *	0.0506008	0.0495062	0.00109463
Ethane	3.04313 *	0 *	3.04313	2.99698	0.0461492
Propane	3.05926 *	0 *	3.05926	2.90463	0.154631
i-Butane	0.893317 *	0 *	0.893317	0.789383	0.103934
n-Butane	2.21433 *	0 *	2.21433	1.86673	0.347601
i-Pentane	1.26181 *	0 *	1.26181	0.847222	0.414584
n-Pentane	1.42996 *	0 *	1.42996	0.863319	0.566638
Isohexane	1.33573 *	0 *	1.33573	0.515543	0.820188
n-Hexane	1.14078 *	0 *	1.14078	0.356173	0.784608
2,2,4-Trimethylpentane	0.00638935 *	0 *	0.00638935	0.000889287	0.00550006
Benzene	0.0281569 *	0 *	0.0281569	0.00844119	0.0197157
Heptane	4.10083 *	0 *	4.10083	0.53242	3.56841
Toluene	0.239363 *	0 *	0.239363	0.0272042	0.212159
Octane	4.78775 *	0 *	4.78775	0.216388	4.57136
Ethylbenzene	0.042228 *	0 *	0.042228	0.00163497	0.0405931
o-Xylene	0.0712598 *	0 *	0.0712598	0.00210391	0.0691559
Nonane	3.39247 *	0 *	3.39247	0.0516851	3.34078
Decane	7.48364 *	0 *	7.48364	0.0376115	7.44603
Water	0 *	260.032 *	260.032	0.262913	259.769

Stream Properties

Property	Units	OXF 157 Condensate	Produced Water	3	4	5
Temperature	°F	85 *	85 *	85.0818	79.2466	79.2466
Pressure	psia	1066.7 *	1066.7 *	1066.7	14.6959 *	14.6959
Mole Fraction Vapor	%	0	0	0	100	0
Mole Fraction Light Liquid	%	100	100	4.01359	0	1.38784
Mole Fraction Heavy Liquid	%	0	0	95.9864	0	98.6122
Molecular Weight	lb/lbmol	59.8819	18.0153	19.7436	34.5555	19.3051
Mass Density	lb/ft^3	36.5724	62.1827	57.2424	0.088686	60.1363
Molar Flow	lbmol/h	0.621498	14.434	15.0555	0.432866	14.6226
Mass Flow	lb/h	37.2165	260.032	297.249	14.9579	282.291
Vapor Volumetric Flow	ft^3/h	1.01761	4.18175	5.19281	168.661	4.69418
Liquid Volumetric Flow	gpm	0.126871	0.521361	0.647415	21.0279	0.585249

* User Specified Values
? Extrapolated or Approximate Values

Process Streams Report
All Streams
Tabulated by Total Phase

Client Name:	EQT	Job:	
Location:	OXF 157 Blowdown Tank		
Flowsheet:	Flowsheet1		

Stream Properties

Property	Units	OXF 157 Condensate	Produced Water	3	4	5
Std Vapor Volumetric Flow	MMSCFD	0.00566037	0.131459	0.13712	0.00394238	0.133177
Std Liquid Volumetric Flow	sgpm	0.129738 *	0.519823 *	0.649561	0.0661977	0.583364
Compressibility		0.298803	0.0528707	0.062934	0.990089	0.000815731
Specific Gravity		0.586387	0.997012	0.917802	1.19311	0.964201
API Gravity		103.133	9.88462	21.6261		14.7165
Enthalpy	Btu/h	-40303.7	-1.77102E+06	-1.81133E+06	-18976.2	-1.79235E+06
Mass Enthalpy	Btu/lb	-1082.95	-6810.78	-6093.64	-1268.64	-6349.3
Mass Cp	Btu/(lb*°F)	0.568968	0.980315	0.929624	0.4289	0.944341
Ideal Gas CpCv Ratio		1.08825	1.32512	1.29268	1.15573	1.30113
Dynamic Viscosity	cP	0.176	0.840918	0.706872	0.00925778	0.843531
Kinematic Viscosity	cSt	0.300426	0.844235	0.734747	6.51674	0.869676
Thermal Conductivity	Btu/(h*ft*°F)	0.0642775	0.353848	0.296717	0.013293	0.320594
Surface Tension	lbf/ft	0.000441128 ?	0.00492858	0.00405793 ?		0.00457848 ?
Net Ideal Gas Heating Value	Btu/ft^3	3087.49	0	127.453	1794.98	78.0899
Net Liquid Heating Value	Btu/lb	19419.4	-1059.76	1504.29	19567.2	547.183
Gross Ideal Gas Heating Value	Btu/ft^3	3343.77	50.31	186.266	1959.28	133.78
Gross Liquid Heating Value	Btu/lb	21043.5	0	2634.71	21371.5	1641.9

Remarks

Blocks
MIX-100
Mixer/Splitter Report

Client Name:	EQT	Job:	
Location:	OXF 157 Blowdown Tank	Modified: 2:14 PM, 7/24/2014	
Flowsheet:	Flowsheet1	Status: Solved 9:23 AM, 2/4/2016	

Connections

Stream	Connection Type	Other Block	Stream	Connection Type	Other Block
Produced Water	Inlet		OXF 157 Condensate	Inlet	
3	Outlet	VSSL-100			

Block Parameters

Pressure Drop	0 psi	Fraction to PStream 3	100 %

Remarks

Blocks
VSSL-100
Separator Report

Client Name:	EQT	Job:	
Location:	OXF 157 Blowdown Tank	Modified:	1:11 PM, 7/17/2014
Flowsheet:	Flowsheet1	Status:	Solved 9:23 AM, 2/4/2016

Connections

Stream	Connection Type	Other Block	Stream	Connection Type	Other Block
3	Inlet	MIX-100	4	Vapor Outlet	
5	Light Liquid Outlet				

Block Parameters

Pressure Drop	1052	psi	Main Liquid Phase	Light Liquid	
Mole Fraction Vapor	2.87514	%	Heat Duty	0	Btu/h
Mole Fraction Light Liquid	1.34793	%	Heat Release Curve Type	Plug Flow	
Mole Fraction Heavy Liquid	95.7769	%	Heat Release Curve Increments	5	

Remarks

Flowsheet Environment
Environment1

Client Name:	EQT	Job:	
Location:	OXF 157 Blowdown Tank		
Flowsheet:	Flowsheet1		

Environment Settings

Number of Poynting Intervals	0	Freeze Out Temperature Threshold Difference	10 °F
Gibbs Excess Model Evaluation Temperature	77 °F	Phase Tolerance	1 %

Components

Component Name	Henry`s Law Component	Phase Initiator	Component Name	Henry`s Law Component	Phase Initiator
Nitrogen	False	False	2,2,4-Trimethylpentane	False	False
Methane	False	False	Benzene	False	False
Carbon Dioxide	False	False	Heptane	False	False
Ethane	False	False	Toluene	False	False
Propane	False	False	Octane	False	False
i-Butane	False	False	Ethylbenzene	False	False
n-Butane	False	False	o-Xylene	False	False
i-Pentane	False	False	Nonane	False	False
n-Pentane	False	False	Decane	False	False
Isohexane	False	False	Water	False	True
n-Hexane	False	False			

Physical Property Method Sets

Liquid Molar Volume	COSTALD	Overall Package	Peng-Robinson
Stability Calculation	Peng-Robinson	Vapor Package	Peng-Robinson
Light Liquid Package	Peng-Robinson	Heavy Liquid Package	Peng-Robinson

Remarks

Calculator Report

Client Name:	EQT	Job:
Location:	OXF 157 Blowdown Tank	

Simple Solver 1

Source Code

Residual Error (for CV1) = TP / 20 - 1

Calculated Variable [CV1]

SourceMoniker	ProMax:ProMax!Project!Flowsheets!Flowsheet1!PStreams!OXF 157 Condensate!Phases!Total!Properties!Std Liquid Volumetric Flow
Value	4.44817
Unit	bbl/d

Measured Variable [TP]

SourceMoniker	ProMax:ProMax!Project!Flowsheets!Flowsheet1!PStreams!5!Phases!Total!Properties!Std Liquid Volumetric Flow
Value	20.001
Unit	bbl/d

Solver Properties

Status: Solved

Error	5.20455E-05		Iterations	5
Calculated Value	0.129738	sgpm	Max Iterations	20
Lower Bound		sgpm	Weighting	1
Upper Bound		sgpm	Priority	0
Step Size		sgpm	Solver Active	Active
Is Minimizer	False		Group	
Algorithm	Default		Skip Dependency Check	False

Remarks

Simple Solver 2

Source Code

Residual Error (for CV1) = LF / 89 - 1

Calculated Variable [CV1]

SourceMoniker	ProMax:ProMax!Project!Flowsheets!Flowsheet1!PStreams!Produced Water!Phases!Total!Properties!Std Liquid Volumetric Flow
Value	17.8225
Unit	bbl/d

Measured Variable [LF]

SourceMoniker	ProMax:ProMax!Project!Flowsheets!Flowsheet1!PStreams!5!Phases!Total!Composition!Std. Liquid Volumetric Fraction!Water
Value	89.0178
Unit	%

Solver Properties

Status: Solved

Error	0.000200191		Iterations	5
Calculated Value	0.519823	sgpm	Max Iterations	20
Lower Bound		sgpm	Weighting	1
Upper Bound		sgpm	Priority	0
Step Size		sgpm	Solver Active	Active
Is Minimizer	False		Group	
Algorithm	Default		Skip Dependency Check	False

Remarks

User Value Sets Report

Client Name:	EQT	Job:
Location:	OXF 157 Blowdown Tank	

Cn+ Flow/Frac.

User Value [CnPlusSum]

* Parameter	9.02137	lb/h	Upper Bound	
Lower Bound		lb/h	* Enforce Bounds	False

Remarks
This User Value Set was programmatically generated. GUID={E867C485-3D3C-49CB-BC24-EA16096DB2B1}

Tank Losses

User Value [ShellLength]

* Parameter	10	ft	Upper Bound	
* Lower Bound	0	ft	* Enforce Bounds	False

User Value [ShellDiam]

* Parameter	10	ft	Upper Bound	
* Lower Bound	0	ft	* Enforce Bounds	False

User Value [BreatherVP]

* Parameter	0.03	psig	Upper Bound	
Lower Bound			* Enforce Bounds	False

User Value [BreatherVacP]

* Parameter	-0.03	psig	Upper Bound	
Lower Bound			* Enforce Bounds	False

User Value [DomeRadius]

Parameter		ft	Upper Bound	ft
Lower Bound		ft	* Enforce Bounds	False

User Value [OpPress]

* Parameter	0	psig	Upper Bound	
Lower Bound			* Enforce Bounds	False

User Value [AvgPercentLiq]

* Parameter	50	%	Upper Bound	
Lower Bound		%	* Enforce Bounds	False

User Value [MaxPercentLiq]

* Parameter	90	%	Upper Bound	
Lower Bound		%	* Enforce Bounds	False

User Value [AnnNetTP]

* Parameter	19.9767	bbl/day	Upper Bound	
* Lower Bound	0	bbl/day	* Enforce Bounds	False

User Value [OREff]

* Parameter	0	%	Upper Bound	
Lower Bound		%	* Enforce Bounds	False

User Value [AtmPressure]

* Parameter	14.1085	psia	Upper Bound	
Lower Bound			* Enforce Bounds	False

User Value Sets Report

Client Name:	EQT	Job:
Location:	OXF 157 Blowdown Tank	

User Value [TVP]

* Parameter	0.359146 psia	Upper Bound	
Lower Bound		* Enforce Bounds	False

User Value [AvgLiqSurfaceT]

* Parameter	57.7675 °F	Upper Bound	
Lower Bound		* Enforce Bounds	False

User Value [MaxLiqSurfaceT]

* Parameter	66.3119 °F	Upper Bound	
Lower Bound		* Enforce Bounds	False

User Value [TotalLosses]

* Parameter	0.00742768 lb/h	Upper Bound	
Lower Bound	lb/h	* Enforce Bounds	False

User Value [WorkingLosses]

* Parameter	0.0223799 ton/yr	Upper Bound	
Lower Bound	ton/yr	* Enforce Bounds	False

User Value [StandingLosses]

* Parameter	0.0101534 ton/yr	Upper Bound	
Lower Bound	ton/yr	* Enforce Bounds	False

User Value [RimSealLosses]

* Parameter	0 ton/yr	Upper Bound	
Lower Bound		* Enforce Bounds	False

User Value [WithdrawalLoss]

* Parameter	0 ton/yr	Upper Bound	
Lower Bound		* Enforce Bounds	False

User Value [LoadingLosses]

* Parameter	0.0109435 lb/h	Upper Bound	
Lower Bound	lb/h	* Enforce Bounds	False

User Value [DeckFittingLosses]

* Parameter	0 ton/yr	Upper Bound	
Lower Bound		* Enforce Bounds	False

User Value [DeckSeamLosses]

* Parameter	0 ton/yr	Upper Bound	
Lower Bound		* Enforce Bounds	False

User Value [FlashingLosses]

* Parameter	0 ton/yr	Upper Bound	
Lower Bound		* Enforce Bounds	False

User Value [GasMoleWeight]

* Parameter	0.0249629 kg/mol	Upper Bound	
Lower Bound		* Enforce Bounds	False

Remarks

This User Value Set was programmatically generated. GUID={B57AFC7E-AAE8-4873-921B-7B4031991004}

Attachment T

FACILITY-WIDE CONTROLLED EMISSIONS SUMMARY SHEET

ATTACHMENT T – FACILITY-WIDE CONTROLLED EMISSIONS SUMMARY SHEET

List all sources of emissions in this table. Use extra pages if necessary.

Emission Point ID#	NO_x		CO		VOC		SO_2		PM_{10}		$PM_{2.5}$		GHG (CO_2e)	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Line Heater (S001)	**0.36**	**1.56**	**0.30**	**1.31**	**0.02**	**0.09**	**<0.01**	**<0.01**	**<0.01**	**0.03**	**<0.01**	**0.03**	**526.94**	**2,308.00**
Line Heater (S002)	**0.36**	**1.56**	**0.30**	**1.31**	**0.02**	**0.09**	**<0.01**	**<0.01**	**<0.01**	**0.03**	**<0.01**	**0.03**	**526.94**	**2,308.00**
Line Heater (S003)	**0.12**	**0.53**	**0.10**	**0.45**	**<0.01**	**0.03**	**<0.01**	**<0.01**	**<0.01**	**0.01**	**<0.01**	**0.01**	**180.33**	**789.85**
Enclosed Combustion Unit (C021)	**1.07**	**4.71**	**0.90**	**3.95**	**0.35**	**1.15**	**<0.01**	**0.03**	**0.02**	**0.09**	**0.02**	**0.09**	**1,639.09**	**7,176.46**
Enclosed Combustion Unit (C022)	**1.07**	**4.71**	**0.90**	**3.95**	**0.35**	**1.15**	**<0.01**	**0.03**	**0.02**	**0.09**	**0.02**	**0.09**	**1,639.09**	**7,176.46**
Tank Truck Loading Activities (S023)	**--**	**--**	**<0.01**	**<0.01**	**0.15**	**0.66**	**<0.01**	**<0.01**	**--**	**--**	**--**	**--**	**0.09**	**0.38**
TEG (S024)	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**1.52**	**6.67**
TEG (S025)	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**1.52**	**6.67**
Compressor Engine (S027)	**0.24**	**1.03**	**0.49**	**2.14**	**0.16**	**0.71**	**<0.01**	**<0.01**	**<0.01**	**0.03**	**<0.01**	**0.03**	**82.58**	**361.69**
Line Heater (S028)	**0.09**	**0.40**	**0.08**	**0.34**	**<0.01**	**0.02**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**134.66**	**589.82**
TOTAL	**3.31**	**14.51**	**3.07**	**13.46**	**1.06**	**3.88**	**0.02**	**0.08**	**0.07**	**0.29**	**0.07**	**0.29**	**4,732.76**	**20,723.99**

Annual emissions shall be based on 8,760 hours per year of operation for all emission units except emergency generators.
According to 45CSR14 Section 2.43.e, fugitive emissions are not included in the major source determination because it is not listed as one of the source categories in Table 1. Therefore, fugitive emissions shall not be included in the PTE above.

ATTACHMENT T – FACILITY-WIDE HAP CONTROLLED EMISSIONS SUMMARY SHEET

List all sources of emissions in this table. Use extra pages if necessary.

Emission Point ID#	Formaldehyde		Benzene		Toluene		Ethylbenzene		Xylenes		Hexane		Total HAPs	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
Line Heater (S001)	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**0.03**	**<0.01**	**0.03**
Line Heater (S002)	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**0.03**	**<0.01**	**0.03**
Line Heater (S003)	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**
Enclosed Combustion Unit (C021)	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**0.01**	**0.05**	**0.02**	**0.05**
Enclosed Combustion Unit (C022)	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**0.01**	**0.05**	**0.02**	**0.05**
Tank Truck Loading Activities (S023)	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**0.02**
TEG (S024)	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**
TEG (S025)	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**
Compressor Engine (S027)	**0.01**	**0.06**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**0.02**	**0.07**
Line Heater (S028)	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**
TOTAL	**0.02**	**0.07**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**<0.01**	**0.05**	**0.19**	**0.08**	**0.28**

Annual emissions shall be based on 8,760 hours per year of operation for all emission units except emergency generators.
According to 45CSR14 Section 2.43.e, fugitive emissions are not included in the major source determination because it is not listed as one of the source categories in Table 1. Therefore, fugitive emissions shall not be included in the PTE above.

Attachment U

CLASS I LEGAL ADVERTISEMENT

AIR QUALITY PERMIT NOTICE
Notice of Application

Notice is given that EQT Production Company has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a G70-B General Permit for the OXF-157 natural gas production facility located in West Union, Doddridge County, West Virginia. The latitude and longitude coordinates are: 39.23609 and -80.76635.

The applicant estimates the potential to discharge the following regulated air pollutants on a facility-wide basis will be:

Carbon Monoxide (CO) = 27.63 tpy
Nitrogen Oxides (NO_x) = 14.11 tpy
Particulate Matter (Total) = 8.07 tpy
Sulfur Dioxide (SO_2) = 0.08 tpy
Volatile Organic Compounds (VOC) = 4.01 tpy
Formaldehyde = 0.07 tpy
Hexane = 0.23 tpy
Hazardous Air Pollutants (HAPs) = 0.32 tpy
Carbon Dioxide Equivalents (CO_2e) = 20,748.35 tpy

Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1250, during normal business hours.

Dated this the XXth day of April, 2016.

By: EQT Production Company
Kenneth Kirk
Executive Vice President
625 Liberty Avenue, Suite 1700
Pittsburgh, PA 15222