

January 30, 2017

West Virginia – Dept. of Environmental Protection Division of Air Quality Beverly McKeone, NSR Manager 601 57th Street, SE Charleston, WV 25304

Reference: G70-D General Permit Registration Application Tonys Bridge wellpad Mt. Claire, Harrison County, West Virginia

Dear Ms. McKeone:

Mountaineer Keystone, LLC is submitting this General Permit G-70D Registration application (1 paper copy and 2 PDF copies on a CD) for their proposed Tonys Bridge wellpad located at 4000 County Route 25, Mt. Claire, Harrison County, West Virginia. It is anticipated that the produced natural gas will be dry; therefore, if any condensate is produced it will be very minimal. Based on these expectations the wellpad will consist of four inline 1mmBTU/hr heaters, four 400 bbl produced liquid tanks, one 210 bbl sand/water tank, and one 700 BTU/Hr thermoelectric generator.

Based upon our understanding, since the wells will be installed after September 18, 2015 and the wellpad will consist of more than a well, the wellpad will be subject to a substantive requirement (i.e. fugitive emission monitoring) and therefore a G70-D permit is required prior to the installation of permanent emission units.

Please note the receipt and affidavit of the required public notice is not included with this application, but will be sent as soon as it is received.

Please feel free to contact me at 724-940-1112, if the WVDEP-DAQ has any questions regarding the information in this General Permit Registration.

Sincerely, Mountaineer Keystone LLC

Meghan M.B. Yingling Environmental Compliance Manager

cc: Stacey Lucas, Mountaineer Keystone LLC William Veigel, Mountaineer Keystone LLC Thomas S. Seguljic, PE, HRP Associates, Inc.

dep	west virginia depart	ection	Division of Air Quality 601 57 th Street SE Charleston, WV 254 Phone (304) 926-0475 Fax (304) 926-0479 www.dep.wv.gov			
G70-D GE	NERAL PERMI	T REGISTRATIO	ON APPL	ICATION		
PREVENTION AND	CONTROL OF AIR POLLU RELOCATION, ADMINIS FURAL GAS PRODUCTIO	TION IN REGARD TO THE C STRATIVE UPDATE AND OP N FACILITIES LOCATED AT	CONSTRUCTIO ERATION OF THE WELL SI	N, MODIFICATION, TE		
X CONSTRUCTION MODIFICATION RELOCATION		□CLASS I ADMINISTRATIV □CLASS II ADMINISTRATIV	E UPDATE /E UPDATE	14		
	SECTION 1	GENERAL INFORMATION				
Name of Applicant (as	egistered with the WV Secre	tary of State's Office):				
Mountaineer Keystor	e LLC					
Federal Employer ID N	o. (FEIN): 47-1919654					
Applicant's Mailing Ad	dress: 65 PROFESSIONAL	PLACE SUITE 200				
City: Bridgeport	State: V	VV	ZIP	Code:26330		
Facility Name: Tonys I	Bridge		>			
Operating Site Physical If none available, list re	Address: oad, city or town and zip of f	acility. 4000 County Route 25				
City: Mt. Claire	Zip Coo	le: 26405	Cour	nty: Harrison		
Latitude & Longitude C Latitude: 39.38585 Longitude: -80.35668	oordinates (NAD83, Decima	Degrees to 5 digits):				
SIC Code: 1311 DAQ Facility ID No. (For existing facilities)						
NAICS Code:	NAICS Code:					
	CERTIFIC	ATION OF INFORMATION				
This G70-DGeneral Official is a President, Directors, or Owner, de authority to bind Proprietorship. Rec compliance certific Representative. If a bus off and the appropr unsigned G70-D Regis utilized, th	Permit Registration Applicat Vice President, Secretary, T pending on business structur the Corporation, Partnership uired records of daily throug ations and all required notifi iness wishes to certify an Au iate names and signatures en tration Application will be application will be return	ion shall be signed below by a R reasurer, General Partner, Gener e. A business may certify an Aut , Limited Liability Company, As hput, hours of operation and man cations must be signed by a Res thorized Representative, the offi tered. Any administratively inc returned to the applicant. Fur ed to the applicant. No substit	tesponsible Offic al Manager, a me horized Represen- sociation, Joint intenance, genera ponsible Official cial agreement b omplete or impu- thermore, if the ution of forms i	tial. A Responsible ember of the Board of ntative who shall have Venture or Sole al correspondence, or an Authorized velow shall be checked roperly signed or G70-D forms are not s allowed.		
I hereby certify that is an Authorized Representative and in that capacity shall represent the interest of the business (e.g., Corporation, Partnership, Limited Liability Company, Association Joint Venture or Sole Proprietor ship) and may obligate and legally bind the business. If the business changes its Authorized Representative, a Responsible Official shall notify the Director of the Division of Air Quality immediately.						
I hereby certify that all information contained in this G70-DGeneral Permit Registration Application and any supporting documents appended hereto is, to the best of my knowledge, true, accurate and complete, and that all reasonable efforts have been made to provide the most comprehensive information possible.						
Responsible Official Si Name and Title: Stace Email slucas@mkeystor	Responsible Official Signature:					
If applicable: Authorized Representat Name and Title: Email:	ive Signature:Pl D	none: F ate:	ax:			
If applicable: Environmental Contact Name and Title: Megha Email:myingling@mkey	M.B. Yingling, Environmen stone.com D	ntal Compliance Manager F	Phone: 724-940-1	112 Fax:		

OPERATING SIT	E INFORMATION				
Briefly describe the proposed new operation and/or any chang Gas including four well heads, four in-line heaters, four (400 sand/produced liquid tank.	Briefly describe the proposed new operation and/or any change(s) to the facility: New operation for production of Natural Gas including four well heads, four in-line heaters, four (400 BBL) produced liquid tanks and one (210 BBL) sand/produced liquid tank.				
Directions to the facility: From 79 South, Take exit 115 for W WV-20 0.1 mi; Turn Left onto Suds Run Rd. 1.4 mi; Turn Rig County Rt 25 1.7 mi; Turn Left onto 2 Licks Rd. Access Rd. i	VV-20 toward Stonewood/Nutterfort 0.3 mi, Turn Right onto ght onto Chub Run Rd/Mt. Clare Rd 2.3 mi; Turn Right onto s at intersection				
ATTACHMENTS AND SU	PPORTING DOCUMENTS				
I have enclosed the following required documen	ts:				
Check payable to WVDEP - Division of Air Quality with the	appropriate application fee (per 45CSR13 and 45CSR22).				
 Check attached to front of application. I wish to pay by electronic transfer. Contact for payment (X I wish to pay by credit card Contact for payment (incl. name tom.seguljic@hrpassociates.com 	incl. name and email address): e and email address): Thomas Seguljic,				
X\$500 (Construction, Modification, and Relocation)□\$300 (□\$1,000 NSPS fee for 40 CFR60, Subpart IIII, JJJJ, OOOO a □\$2,500 NESHAP fee for 40 CFR63, Subpart ZZZZ and/or H	Class II Administrative Update) and/or OOOOa ¹ IH ²				
¹ Only one NSPS fee will apply. ² Only one NESHAP fee will apply. The Subpart ZZZZ NESHAP fee will be waived for new engines that satisfy requirements by complying with NSPS, Subparts IIII and/or JJJJ. NSPS and NESHAP fees apply to new construction or if the source is being modified.					
X Responsible Official or Authorized Representative Signatu	ure (if applicable)				
X Single Source Determination Form (must be completed)-	Attachment A				
□Siting Criteria Waiver (if applicable) – Attachment B	X Current Business Certificate – Attachment C				
X Process Flow Diagram – Attachment D	X Process Description – Attachment E				
X Plot Plan – Attachment F	X Area Map – Attachment G				
X G70-D Section Applicability Form – Attachment H	X Emission Units/ERD Table – Attachment I				
X Fugitive Emissions Summary Sheet – Attachment J					
X Gas Well Affected Facility Data Sheet (if applicable) - Atta	achment K				
X Storage Vessel(s) Data Sheet (include gas sample data, USI HYSYS, etc.), etc. where applicable) – Attachment L	EPA Tanks, simulation software (e.g. ProMax, E&P Tanks,				
X Natural Gas Fired Fuel Burning Unit(s) Data Sheet (GPUs, M	Heater Treaters, In-Line Heaters if applicable) – Attachment				
□Internal Combustion Engine Data Sheet(s) (include manufa N	cturer performance data sheet(s) if applicable) - Attachment				
X Tanker Truck/Rail Car Loading Data Sheet (if applicable) -	- Attachment O				
\Box Glycol Dehydration Unit Data Sheet(s) (include wet gas analysis, GRI- GLYCalc TM input and output reports and information on reboiler if applicable) – Attachment P					
X Pneumatic Controllers Data Sheet – Attachment Q					
X Pneumatic Pump Data Sheet – Attachment R					
□ Air Pollution Control Device/Emission Reduction Device(s) Sheet(s) (include manufacturer performance data sheet(s) if applicable) – Attachment S					
X Emission Calculations (please be specific and include all ca	alculation methodologies used) – Attachment T				
X Facility-wide Emission Summary Sheet(s) – Attachment U					
X Class I Legal Advertisement – Attachment V					
X One (1) paper copy and two (2) copies of CD or DVD with	pdf copy of application and attachments				

All attachments must be identified by name, divided into sections, and submitted in order.

ATTACHMENT A - SINGLE SOURCE DETERMINATION FORM

Classifying multiple facilities as one "stationary source" under 45CSR13, 45CSR14, and 45CSR19 is based on the definition of Building, structure, facility, or installation as given in §45-14-2.13 and §45-19-2.12. The definition states:

"Building, Structure, Facility, or Installation" means all of the pollutant-emitting activities which belong to the same industrial grouping, are located on one or more contiguous or adjacent properties, and are under the control of the same person (or persons under common control). Pollutant-emitting activities are a part of the same industrial grouping if they belong to the same "Major Group" (i.e., which have the same two (2)-digit code) as described in the Standard Industrial Classification Manual, 1987 (United States Government Printing Office stock number GPO 1987 0-185-718:QL 3).

The Source Determination Rule for the oil and gas industry was published in the Federal Register on June 3, 2016 and will become effective on August 2, 2016. EPA defined the term "adjacent" and stated that equipment and activities in the oil and gas sector that are under common control will be considered part of the same source if they are located on the same site or on sites that share equipment and are within ¹/₄ mile of each other.

Is there equipment	and activities	in the	same	industrial	grouping	(defined
by SIC code)?						

Yes 🗆 No X

Is there equipment and activities under the control of the same person/people?

 $Yes \Box No X$

Is there equipment and activities located on the same site or on sites that share equipment and are within ¹/₄ mile of each other?

Yes 🗆 No X

ATTACHMENT C-CURRENT BUSINESS CERTIFICATE

If the applicant is a resident of West Virginia, the applicant should provide a copy of the current Business Registration Certificate issued to them from the West Virginia Secretary of State's Office. If the applicant is not a resident of the State of West Virginia, the registrant should provide a copy of the Certificate of Authority/Authority of LLC/Registration. This information is required for all sources to operate a business in West Virginia regardless of whether it is a construction, modification, or administrative update.

If you are a new business to West Virginia and have applied to the West Virginia Secretary of State's Office for a business license, please include a copy of your application.

Please note: Under the West Virginia Bureau of Employment Programs, 96CSR1, the DAQ may not grant, issue, or renew approval of any permit, general permit registration, or Certificate to Operate to any employing unit whose account is in default with the Bureau of Employment Programs Unemployment Compensation Division.

WEST VIRGINIA STATE TAX DEPARTMENT BUSINESS REGISTRATION CERTIFICATE

ISSUED TO: MOUNTAINEER KEYSTONE LLC 6031 WALLACE ROAD EXT 300 WEXFORD, PA 15090-3430

BUSINESS REGISTRATION ACCOUNT NUMBER:

2247-4512

This certificate is issued on: 01/13/2017

This certificate is issued by the West Virginia State Tax Commissioner in accordance with Chapter 11, Article 12, of the West Virginia Code

The person or organization identified on this certificate is registered to conduct business in the State of West Virginia at the location above.

This certificate is not transferrable and must be displayed at the location for which issued This certificate shall be permanent until cessation of the business for which the certificate of registration was granted or until it is suspended, revoked or cancelled by the Tax Commissioner.

Change in name or change of location shall be considered a cessation of the business and a new certificate shall be required.

TRAVELING/STREET VENDORS: Must carry a copy of this certificate in every vehicle operated by them. CONTRACTORS, DRILLING OPERATORS, TIMBER/LOGGING OPERATIONS: Must have a copy of this certificate displayed at every job site within West Virginia.

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ATTACHMENT D – PROCESS FLOW DIAGRAM

Provide a diagram or schematic that supplements the process description of the operation. The process flow diagram must show all sources, components or facets of the operation in an understandable line sequence of operation. The process flow diagram should include the emission unit ID numbers, the pollution control device ID numbers, and the emission point ID numbers consistent with references in other attachments of the application. For a proposed modification, clearly identify the process areas, emission units, emission points, and/or control devices that will be modified, and specify the nature and extent of the modification.

Use the following guidelines to ensure a complete process flow diagram:

- The process flow diagram shall logically follow the entire process from beginning to end.
- Identify each emission source and air pollution control device with proper and consistent emission unit identification numbers, emission point identification numbers, and control device identification numbers.
- The process flow lines may appear different for clarity. For example, dotted lines may be used for vapor flow and solid lines used for liquid flow and arrows for direction of flow.
- The process flow lines may be color coded. For example: new or modified equipment may be red; old or existing equipment may be blue; different stages of preparation such as raw material may be green; and, finished product or refuse, another color.



ATTACHMENT E – PROCESS DESCRIPTION

Provide a detailed written description of the operation for which the applicant is seeking a permit. The process description is used in conjunction with the process flow diagram to provide the reviewing engineer a complete understanding of the activity at the operation. Describe in detail and order the complete process operation.

Use the following guidelines to ensure a complete Process Description:

- The process flow diagram should be prepared first and used as a guide when preparing the process description. The written description shall follow the logical order of the process flow diagram.
- All emission sources, emission points, and air pollution control devices must be included in the process description.
- When modifications are proposed, describe the modifications and the effect the changes will have on the emission sources, emission points, control devices and the potential emissions.
- Proper emission source ID numbers must be used consistently in the process description, the process flow diagram, the emissions calculations, and the emissions summary information provided.
- Include any additional information that may facilitate the reviewers understanding of the process operation.

The process description is required for all sources regardless of whether it is a construction, modification, or administrative update.

Tonys Bridge is a wellpad that will consist of 4 natural gas (dry) production wells and the following equipment:

- 4 1 MMBTU/Hr Heater (HTR-1 [1E], HTR-2 [2E], HTR-3 [3E] and HTR-4 [4E])
- 4 400 BBL Produced Liquid (water) Tanks (TNK-1 [5E], TNK-2 [6E], TNK-3 [7E], TNK-4 [8E]); and
- 1 210 BBL sand/water Tank (TNK-5)
- 1 0.0007 MMBTU/Hr Thermoelectric Generator (TE-1 [9E])

ATTACHMENT F – PLOT PLAN

Provide an accurately scaled and detailed Plot Plan showing the locations of all emission units, emission points, and air pollution control devices. Show all emission units, affected facilities, enclosures, buildings and plant entrances and exits from the nearest public road(s) as appropriate. Note height, width and length of proposed or existing buildings and structures.

A scale between 1"=10' and 1"=200' should be used with the determining factor being the level of detail necessary to show operation or plant areas, affected facilities, emission unit sources, transfer points, etc. An overall small scale plot plan (e.g., 1"=300') should be submitted in addition to larger scale plot plans for process or activity areas (e.g., 1"=50') if the plant is too large to allow adequate detail on a single plot plan. Process or activity areas may be grouped for the enlargements as long as sufficient detail is shown.

Use the following guidelines to ensure a complete Plot Plan:

- Facility name
- Company name
- Company facility ID number (for existing facilities)
- Plot scale, north arrow, date drawn, and submittal date.
- Facility boundary lines
- Base elevation
- Lat/Long reference coordinates from the area map and corresponding reference point elevation
- Location of all point sources labeled with proper and consistent source identification numbers

This information is required for all sources regardless of whether it is a construction, modification, or administrative update.







Emission ID's Located in the site boundary are HTR-1, HTR-2,

ATTACHMENT G – AREA MAP

Provide an Area Map showing the current or proposed location of the operation. On this map, identify plant or operation property lines, access roads and any adjacent dwelling, business, public building, school, church, cemetery, community or institutional building or public park within a 300' boundary circle of the collective emission units.

Please provide a 300' boundary circle on the map surrounding the proposed emission units collectively.

This information is required for all sources regardless of whether it is a construction, modification, or administrative update.



Legend



Well Pad

300 foot Buffer

Approx. Site Boundary



197 SCOTT SWAMP ROAD FARMINGTON, CT 06032 (860) 674-9570 HRPASSOCIATES.COM

North					
0		200	4	00 Fee	et
evisions	o. Date				
Designed By: R	MEW	Drawn By:	BOB	Reviewed By:	22
Issue Date:	01/12/2017	Project No:	MOU7000.AC	Sheet Size:	/ X
Area Map Tonys Bridge Wellpad Mountaineer Keystone LLC County Route 25 Mt. Clare, West Virginia					
	ΤA	TAC	снм G	ENT	Г

ATTACHMENT H-G70-D SECTION APPLICABILITY FORM

General Permit G70-D Registration Section Applicability Form

General Permit G70-D was developed to allow qualified applicants to seek registration for a variety of sources. These sources include gas well affected facilities, storage vessels, gas production units, in-line heaters, heater treaters, glycol dehydration units and associated reboilers, pneumatic controllers, pneumatic pumps, reciprocating internal combustion engines (RICEs), tank truck/rail car loading, fugitive emissions, completion combustion devices, flares, enclosed combustion devices, and vapor recovery systems. All registered facilities will be subject to Sections 1.0, 2.0, 3.0, and 4.0.

General Permit G70-D allows the registrant to choose which sections of the permit they are seeking registration under. Therefore, please mark which additional sections that you are applying for registration under. If the applicant is seeking registration under multiple sections, please select all that apply.Please keep in mind, that if this registration is approved, the issued registration will state which sections will apply to your affected facility.

GENERAL PERM	IIT G70-D APPLICABLE SECTIONS
X Section 5.0	Gas and Oil Well Affected Facility (NSPS, Subpart OOOO/OOOOa)
X Section 6.0	Storage Vessels Containing Condensate and/or Produced Water ¹
□Section 7.0	Storage Vessel Affected Facility (NSPS, Subpart OOOO/OOOOa)
□Section 8.0	Control Devices and Emission Reduction Devices not subject to NSPS Subpart OOOO/OOOOa and/or NESHAP Subpart HH
X Section 9.0	Small Heaters and Reboilers not subject to 40CFR60 Subpart Dc
□Section 10.0	Pneumatic Controllers Affected Facility (NSPS, Subpart OOOO/OOOOa)
□Section 11.0	Pneumatic Pump Affected Facility (NSPS, Subpart OOOOa)
X Section 12.0	Fugitive Emissions GHG and VOC Standards (NSPS, Subpart OOOOa)
□Section 13.0	Reciprocating Internal Combustion Engines, Generator Engines
X Section 14.0	Tanker Truck/Rail Car Loading ²
□Section 15.0	Glycol Dehydration Units ³

1 Applicants that are subject to Section 6 may also be subject to Section 7 if the applicant is subject to the NSPS, Subparts OOOO or OOOOa control requirements or the applicable control device requirements of Section 8.

2 Applicants that are subject to Section 14 may also be subject to control device and emission reduction device requirements of Section 8.

3 Applicants that are subject to Section 15 may also be subject to the requirements of Section 9 (reboilers). Applicants that are subject to Section 15 may also be subject to control device and emission reduction device requirements of Section 8.

ATTACHMENT I - EMISSION UNITS / EMISSION REDUCTION DEVICES (ERD) TABLE

Include ALL emission units and air pollution control devices/ERDs that will be part of this permit application review. Do not include fugitive emission sources in this table. Deminimis storage tanks shall be listed in the Attachment L table. This information is required for all sources regardless of whether it is a construction, modification, or administrative update.

Emission Unit ID ¹	Emission Point ID ²	Emission Unit Description	Year Installed	Manufac. Date ³	Design Capacity	Type ⁴ and Date of Change	Control Device(s) ⁵	ERD(s) ⁶
HTR-1	1E	HEATER-1	2017	2017	1 MMBTU/HR	NEW	NONE	NA
HTR-2	2E	HEATER-2	2017	2017	1 MMBTU/HR	NEW	NONE	NA
HTR-3	3E	HEATER-3	2017	2017	1 MMBTU/HR	NEW	NONE	NA
HTR-4	4E	HEATER-4	2017	2017	1 MMBTU/HR	NEW	NONE	NA
TNK-1	5E	TANK-1	2017	2017	400 BBL	NEW	NONE	NA
TNK-2	6E	TANK-2	2017	2017	400 BBL	NEW	NONE	NA
TNK-3	7E	TANK-3	2017	2017	400 BBL	NEW	NONE	NA
TNK-4	8E	TANK-4	2017	2017	400 BBL	NEW	NONE	NA
TE-1	9E	Thermoelectric Generator	2017	2017	0.0007 MMBTU/HR	NEW	NONE	NA
¹ For Emission Units (or Sources) use the following numbering system:1S, 2S, 3S, or other appropriate designation. ² For Emission Points use the following numbering system:1E, 2E, 3E, or other appropriate designation. ³ When required by rule								

⁴ New, modification, removal, existing

⁵ For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation. ⁶ For ERDs use the following numbering system: 1D, 2D, 3D,... or other appropriate designation.

	ATTACHMENT J – FUGITIVE EMISSIONS SUMMARY SHEET							
	Sources of fugitive emissions may include loading operations, equipment leaks, blowdown emissions, etc. Use extra pages for each associated source or equipment if necessary.							
	Source/Equipm	nent: Fac	ility Wide					
	Leak Detectior Method Used	1	□ Audible, visual, and olfactory (AVO) inspections	□Infrared (FLIR) cameras	XOther (please Subpart OOOC	e describe): Wi Da	ll Comply with	□ None required
Component	Closed		Source of	Leak Factors	Stream type		Estimated Emis	sions (tpy)
Туре	Vent System	Count	(EPA, oth	ner (specify))	(gas, liquid, etc.)	VOC	HAP	GHG (methane, CO ₂ e)
Pumps	□ Yes □ No	0			□ Gas □ Liquid □ Both	0	0	0
Valves	□ Yes X No	249	0.027 scf/hr/component (Subp	0.027 scf/hr/component (Subpart W: Table W-1A)		0.4302	<0.001	27.98
Safety Relief Valves	□ Yes X No	21	0.040 scf/hr/component (Subp	0.040 scf/hr/component (Subpart W: Table W-1A)		0.0537	<0.001	3.50
Open Ended Lines	□ Yes X No	5	0.061 scf/hr/component (Subp	0.061 scf/hr/component (Subpart W: Table W-1A)		0.0.0195	<0.001	1.27
Sampling Connections	□ Yes X No	4	0.003 scf/hr/component (Subp	0.003 scf/hr/component (Subpart W: Table W-1A)		0.0008	<0.001	0.0499
Connections(N sampling)	Not Z Yes	1226	0.003 scf/hr/component (Subp	0.003 scf/hr/component (Subpart W: Table W-1A)		0.2353	<0.001	15.31
Compressors	ssors I Yes 0 I No 0 0 0 I Liquid I Both 0 0							
Flanges	☐ Yes X No	241	0.003 scf/hr/component, Assu emission rate from Subpart W	0.003 scf/hr/component, Assumed to be equal to connection emission rate from Subpart W: Table W-1A		0.0463	<0.001	3.01
Other ¹	□ Yes X No	62	0.003 scf/hr/component, Assu emission rate from Subpart W	0.003 scf/hr/component, Assumed to be equal to connection emission rate from Subpart W: Table W-1A			<0.001	0.7700
¹ Other equip	ment types may	include of	compressor seals, relief valves, dia	aphragms, drains, meters, etc.				

Please provide an explanation of the sources of fugitive emissions (e.g. pigging operations, equipment blowdowns, pneumatic controllers, etc.): Assumed each component is constantly leaking at a specified rate based on Subpart W Please indicate if there are any closed vent bypasses (include component): NA

Specify all equipment used in the closed vent system (e.g. VRU, ERD, thief hatches, tanker truck/rail car loading, etc.) NA

ATTACHMENT K – GAS WELL AFFECTED FACILITY DATA SHEET

Complete this data sheet if you are the owner or operator of a gas well affected facility for which construction, modification or reconstruction commenced after August 23, 2011. This form must be completed for natural gas well affected facilities regardless of when flowback operations occur (or have occurred).

API Number	Date of Flowback	Date of Well Completion	Green Completion and/or Combustion Device	Subject to OOOO or OOOOa?
4703305896	Expected 3/17	Expected 3/17	REC	Yes
4703305870	Expected 3/17	Expected 3/17	REC	Yes
4703305871	Expected 3/17	Expected 3/17	REC	Yes
4703305884	Expected 3/17	Expected 3/17	REC	Yes

Note: If future wells are planned and no API number is available please list as PLANNED. If there are existing wells that commenced construction prior to August 23, 2011, please acknowledge as existing.

This is the same API (American Petroleum Institute) well number(s) provided in the well completion notification and as provided to the WVDEP, Office of Oil and Gas for the well permit. The API number may be provided on the application without the state code (047).

Every oil and gas well permitted in West Virginia since 1929 has been issued an API number. This API is used by agencies to identify and track oil and gas wells.

The API number has the following format: 047-001-00001

Where,

047 =	State code. The state code for WV is 047.
001 =	County Code. County codes are odd numbers, beginning with 001
	(Barbour) and continuing to 109 (Wyoming).
00001=	Well number. Each well will have a unique well number.

ATTACHMENT L – STORAGE VESSEL DATA SHEET

Complete this data sheet if you are the owner or operator of a storage vessel that contains condensate and/or produced water. This form must be completed for *each* new or modified bulk liquid storage vessel(s) that contains condensate and/or produced water. (If you have more than one (1) identical tank (i.e. 4-400 bbl condensate tanks), then you can list all on one (1) data sheet). **Include gas sample analysis, flashing emissions, working and breathing losses, USEPA Tanks, simulation software (ProMax, E&P Tanks, HYSYS, etc.), and any other supporting documents where applicable.**

The following information is **REQUIRED**:

□Composition of the representative sample used for the simulation □For each stream that contributes to flashing emissions:

- □ Temperature and pressure (inlet and outlet from separator(s))
- □ Simulation-predicted composition
- □Molecular weight
- □Flow rate

□Resulting flash emission factor or flashing emissions from simulation □Working/breathing loss emissions from tanks and/or loading emissions if simulation

is used to quantify those emissions

Additional information may be requested if necessary.

GENERAL INFORMATION (REQUIRED)

1. Bulk Storage Area Name	2. Tank Name Tank -1				
Tonys Bridge					
3. Emission Unit ID number: TNK-1	4. Emission Point ID number 5E				
5. Date Installed, Modified or Relocated (for existing	6. Type of change:				
tanks)March 2017 (expected)	X New construction \Box New stored material \Box Other				
Was the tank manufactured after August 23, 2011 and on or	□Relocation				
before September 18, 2015?					
□ Yes X No					
Was the tank manufactured after September 18, 2015?					
X Yes 🗆 No					
7A. Description of Tank Modification (if applicable)					
7B. Will more than one material be stored in this tank? If so, a s	separate form must be completed for each material.				
\Box Yes X No					
7C. Was USEPA Tanks simulation software utilized?					
\Box Yes X No					
If Yes, please provide the appropriate documentation and items	8-42 below are not required.				

TANK INFORMATION

8. Design Capacity (*specify barrels or gallons*). Use the internal cross-sectional area multiplied by internal height. 400 BBL

9A. Tank Internal Diameter (ft.) 12	9B. Tank Internal Height (ft.) 20	
10A. Maximum Liquid Height (ft.) 17	10B. Average Liquid Height (ft.) 10	
11A. Maximum Vapor Space Height (ft.) 17	11B. Average Vapor Space Height (ft.) 10	
12. Nominal Capacity (specify barrels or gallons). This is also known as "working volume".		

13A. Maximum annual throughput (gal/yr) 873,600	13B. Maximum daily throughput (gal/day) 2393				
14. Number of tank turnovers per year 52	15. Maximum tank fill rate (gal/min) 60				
16. Tank fill method X Submerged □ Splash	Bottom Loading				
17. Is the tank system a variable vapor space system? \Box Ye	s X No				
If yes, (A) What is the volume expansion capacity of the system	n (gal)?				
(B) What are the number of transfers into the system per	r year?				
18. Type of tank (check all that apply):					
X Fixed Roof \Box vertical \Box horizontal \Box flat roo	f \Box cone roof \Box dome roof \Box other (describe)				
\Box External Floating Roof \Box pontoon roof \Box double	e deck roof				
Domed External (or Covered) Floating Roof					
□ Internal Floating Roof □ vertical column support	□ self-supporting				
□ Variable Vapor Space □ lifter roof □ diaphragm	n				
\Box Pressurized \Box spherical \Box cylindrical					
□ Other (describe)					

PRESSURE/VACUUM CONTROL DATA

X Does Not Apply	19. Check as many as app	ly:								
□ Inert Gas Blanket of □ Carbon Adsorption ¹ □ Vent to Vapor Combustion Device ¹ (vapor combustors, flares, thermal oxidizers, enclosed combustors) □ Conservation Vent (psig) □ Condenser ¹ Vacuum Setting Pressure Setting □ Thief Hatch Weighted □ Yes □ No ¹ Complete appropriate Air Pollution Control Device Sheet 20. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application). Material Name Flashing Loss Breathing Loss Vorking Loss Total Emissions Loss (VOC) Estimation Method ¹ Produced Liquid Image: Im	X Does Not Apply				□ Rupture	e Disc (psi	g)			
	\Box Inert Gas Blanket of		Ca	arbon Ads	orption ¹					
	□Vent to Vapor Combust	ion Devic	e ¹ (vapor	combusto	rs, flares,	thermal ox	dizers, e	nclosed co	mbustors))
Vacuum Setting Pressure Setting Vacuum Setting Pressure Setting Thief Hatch Weighted Vs N 1 Complete appropriate Air Pollution Control Device Sheet \mathbf{V} Notation Setting Total Endevice State State Or Calculations here or elsewhere in the application Score Sheet Material Name Flashing Loss Breathing Loss Vorking Loss Total Endison Score Estimation Method ¹ Produced Liquid Image: State S	□ Conservation Vent (psi	ig)□Con	denser ¹							
$ \begin{array}{ $	Vacuum Setting		Pressure	Setting						
Vacuum Setting Pressure Setting Thief Hatch Weighted Yes No 1 Complete appropriate Air Pollution Control Device Sheet 1 20. Expected Emission Rate (submit Test Data or Calculations her or elsewhere in the application). Total Emissions Loss (VOC) Estimation Method ¹ Material Name Flashing Loss Breathing Loss Working Loss (VOC) Total Emissions Loss (VOC) Estimation Method ¹ Produced Liquid Image: Imag	□ Emergency Relief Valv	ve (psig)								
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	Vacuum Setting		Pressure	Setting						
¹ Complete appropriate Air Pollution Control Device Sheet 20. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application). Material Name Flashing Loss Breathing Loss Working Loss Total Emissions Loss (VOC) Estimation Method ¹ Material Name Ib/hr tpy lb/hr tpy <tdt< td=""><td>\BoxThief Hatch Weighted \Box</td><td>Yes 🗆</td><td>No</td><td></td><td></td><td></td><td></td><td></td><td></td><td></td></tdt<>	\Box Thief Hatch Weighted \Box	Yes 🗆	No							
30. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application). Material Name Flashing Loss Breathing Loss Working Loss Total Emissions Loss (VOC) Estimation Method ¹ Material Name Ib/hr tpy Ib/hr tpy Ib/hr tpy Ib/hr tpy Produced Liquid Image: Color of the test of test	¹ Complete appropriate Air	r Pollutio	n Control	Device Sh	neet					
Output Destination of Calculations here or elsewhere in the application). Material Name Flashing Loss Breathing Loss Working Loss Total Emissions Loss (VOC) Estimation Method ¹ Material Name Ib/hr tpy lb/hr										
Material Name Flashing Loss Breathing Loss Working Loss Total Emissions Loss (VOC) Estimation Method ¹ Ib/hr tpy Ib/hr tpy Ib/hr tpy Ib/hr tpy Produced Liquid Image: Constraint of the set of the se	20. Expected Emission Ra	ate (subm	it Test Da	ta or Calcu	ulations he	ere or elsev	where in the	ne applicat	ion).	1
Image:	Material Name	Flashi	hing Loss Breathing Loss Working Loss Total		_	Estimation Method ¹				
Ib/hr tpy Ib/hr tpy Ib/hr tpy Ib/hr tpy Produced Liquid Image:								Emissio	ns Loss	
Ib/hrtpyIb/hrtpyIb/hrtpyIb/hrtpyProduced Liquid0.29750.0771MB <t< th=""><th></th><th></th><th></th><th></th><th></th><th></th><th></th><th></th><th></th><th></th></t<>										
Produced Liquid Image: Second sec		11.0			1.			(VOC)		-
Image: state of the state	Ducdwood Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr	tpy	MB
Image: state of the state	Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr 0.2975	tpy 0.0771	MB
Image: state of the state	Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr 0.2975	tpy 0.0771	MB
	Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr 0.2975	tpy 0.0771	MB
	Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr 0.2975	tpy 0.0771	MB
	Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) Ib/hr 0.2975	tpy 0.0771	MB
	Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr 0.2975	tpy 0.0771	MB
	Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr 0.2975	tpy 0.0771	MB
	Produced Liquid			lb/hr	tpy	b/hr	tpy	(VOC) Ib/hr 0.2975	tpy 0.0771	MB

¹ EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify) *Remember to attach emissions calculations, including TANKS Summary Sheets and other modeling summary sheets if applicable.*

TANK CONSTRUCTION AND OPERATION	ON INFORMATION	
21. Tank Shell Construction:		
X Riveted \Box Gunite lined \Box Epoxy	\square -coated rivets \square Other (describe)	
21A. Shell Color: Tan	21B. Roof Color: Tan	21C. Year Last Painted:2017

22. Shell Condition (if metal and unlined):						
X No Rust 🗆 Light Rust 🗆 Dense	Rust 🛛 Not application	able				
22A. Is the tank heated? \Box Yes X No	22B. If yes, operating t	emperati	ire:	22C. If yes tank?	s, how is heat provided to	
23. Operating Pressure Range (psig): Ambient						
Must be listed for tanks using VRUs wi	th closed vent system	l.				
24. Is the tank a Vertical Fixed Roof Tank?	24A. If yes, for dome a	roof prov	vide radius (ft):	24B. If yes	s, for cone roof, provide slop (ft/ft):	
X Yes □No	6					
25. Complete item 25 for Floating Roof Tanks	\square Does not apply	Х				
25A. Year Internal Floaters Installed:						
25B. Primary Seal Type (check one):	llic (mechanical) shoe	seal	Liquid mou	nted resilier	nt seal	
\Box Vapor mounted resilient seal \Box O	ther (describe):					
25C. Is the Floating Roof equipped with a seco	ndary seal? 🗌 Yes	□No				
25D. If yes, how is the secondary seal mounted	? (check one) \Box Shoe	□ F	tim 🗆 Other	r (describe)	:	
25E. Is the floating roof equipped with a weath	er shield? 🗌 Yes	ΠN	0			
25F. Describe deck fittings:						
_						
26. Complete the following section for Interna	l Floating Roof Tanks	X Does	not apply			
26A. Deck Type: \Box Bolted \Box W	Velded	26B. I	For bolted decks,	provide dec	k construction:	
26C Deck seam Continuous sheet constructio	n.					
\square 5 ft wide \square 6 ft wide \square 7 ft wide	e. □ 5 v 7 5 ft wide	□ 5 v	12 ft wide	other (de	scribe)	
26D Dook seem length (ft.): $26E$ Area	$rac{1}{2}$ of deals (ft ²):		T2 II. wide L	uted uter	26G. For column supported	
20D. Deck seam length (It.): 20E. Alea	t of deck (It):	20F. f	for columns suppo	oned	tanks diameter of column:	
27. Closed Vent System with VRU? Yes	X No					
28. Closed Vent System with Enclosed Combus	stor? 🗆 Yes X No					
SITE INFORMATION						
29. Provide the city and state on which the data	in this section are based:	Charle	ston, WV			
30. Daily Avg. Ambient Temperature (°F): 54.	75	31. A	nnual Avg. Maxi	mum Tempe	rature (°F):65.5	
32. Annual Avg. Minimum Temperature (°F):	44	33. A	g. Wind Speed	(mph): 6.3		
34. Annual Avg. Solar Insulation Factor (BTU/	(ft ² -day):1123	35. At	mospheric Press	ure (psia):14	.617	
LIQUID INFORMATION						
36. Avg. daily temperature range of bulk	36A. Minimum (°F): 5	52.2		36B. Maxi	imum (°F): 65.5	
liquid (°F): 13.3						
37. Avg. operating pressure range of tank	37A. Minimum (psig):	0.2191		37B. Maxi	mum (psig): 0.9075	
(psig): 0.425						
38A Minimum liquid surface temperature (°F)	.52.2	38B (orresponding v	apor pressure	(nsia):0.2191	
39A. Avg. liquid surface temperature (°F): 56.	3	39B. Corresponding vapor pressure (psia):0.4525				
40A. Maximum liquid surface temperature (°F)	:66.7	40B. Corresponding vapor pressure (psia):0.9075				
41. Provide the following for each liquid or gas	to be stored in the tank.	Add add	itional pages if r	necessary.	4	
41A. Material name and composition:	Produced Liqui	d	10			
41B. CAS number:	-					
41C. Liquid density (lb/gal):	8.33					
41D. Liquid molecular weight (lb/lb-mole):	18.02					
41E. Vapor molecular weight (lb/lb-mole):	18.02					
41F. Maximum true vapor pressure (psia):	1.0					
41G. Maximum Reid vapor pressure (psia):	0.46					
41H. Months Storage per year.	10					
From: To:	12					
42. Final maximum gauge pressure and						
temperature prior to transfer into tank used as	O/Ambient					
inputs into flashing emission calculations.						

ATTACHMENT L – STORAGE VESSEL DATA SHEET

Complete this data sheet if you are the owner or operator of a storage vessel that contains condensate and/or produced water. This form must be completed for *each* new or modified bulk liquid storage vessel(s) that contains condensate and/or produced water. (If you have more than one (1) identical tank (i.e. 4-400 bbl condensate tanks), then you can list all on one (1) data sheet). **Include gas sample analysis, flashing emissions, working and breathing losses, USEPA Tanks, simulation software (ProMax, E&P Tanks, HYSYS, etc.), and any other supporting documents where applicable.**

The following information is **REQUIRED**:

□Composition of the representative sample used for the simulation □For each stream that contributes to flashing emissions:

 \Box Temperature and pressure (inlet and outlet from separator(s))

□ Simulation-predicted composition

□Molecular weight

□Flow rate

□Resulting flash emission factor or flashing emissions from simulation □Working/breathing loss emissions from tanks and/or loading emissions if simulation is used to quantify those emissions

Additional information may be requested if necessary.

GENERAL INFORMATION (REQUIRED)

1. Bulk Storage Area Name	2. Tank Name Tank -2
Tonys Bridge	
3. Emission Unit ID number: TNK-2	4. Emission Point ID number 6E
5. Date Installed , Modified or Relocated (for existing tanks)	6. Type of change:
(Expected March 2017)	X New construction \Box New stored material \Box Other
Was the tank manufactured after August 23, 2011 and on or	□Relocation
before September 18, 2015?	
\Box Yes X No	
Was the tank manufactured after September 18, 2015?	
X Yes 🗆 No	
7A. Description of Tank Modification (<i>if applicable</i>)	
7B. Will more than one material be stored in this tank? If so, a	separate form must be completed for each material.
\Box Yes X No	
7C. Was USEPA Tanks simulation software utilized?	
\Box Yes X No	
If Yes, please provide the appropriate documentation and items	8-42 below are not required.

TANK INFORMATION

8. Design Capacity (specify barrels or gallons). Use the internal cross-sectional area multiplied by internal height.					
400 BBL					
9A. Tank Internal Diameter (ft.) 12	9B. Tank Internal Height (ft.) 20				
10A. Maximum Liquid Height (ft.) 17	10B. Average Liquid Height (ft.) 10				
11A. Maximum Vapor Space Height (ft.) 17	11B. Average Vapor Space Height (ft.) 10				

12. Nominal Capacity (specify barrels or gallons). This is also	known as "working volume".				
13A. Maximum annual throughput (gal/yr) 873,600	13B. Maximum daily throughput (gal/day) 2393				
14. Number of tank turnovers per year 52	15. Maximum tank fill rate (gal/min) 60				
16. Tank fill method X Submerged	Bottom Loading				
17. Is the tank system a variable vapor space system? \Box Yes	X No				
If yes, (A) What is the volume expansion capacity of the system	(gal)?				
(B) What are the number of transfers into the system per y	/ear?				
18. Type of tank (check all that apply):					
X Fixed Roof \Box vertical \Box horizontal \Box flat roof	\Box cone roof \Box dome roof \Box other (describe)				
\Box External Floating Roof \Box pontoon roof \Box double	deck roof				
Domed External (or Covered) Floating Roof					
□ Internal Floating Roof □ vertical column support	□ self-supporting				
\Box Variable Vapor Space \Box lifter roof \Box diaphragm					
\Box Pressurized \Box spherical \Box cylindrical					
\Box Other (describe)					

PRESSURE/VACUUM CONTROL DATA

19. Check as many as app	ly:								
X Does Not Apply				☐ Rupture	e Disc (psi	g)			
□ Inert Gas Blanket of		Ca	arbon Ads	orption ¹					
□Vent to Vapor Combust	ion Devic	e ¹ (vapor	combusto	rs, flares, t	thermal ox	dizers, e	nclosed co	mbustors)	
□ Conservation Vent (psi	g) 🗆 Con	denser ¹							
Vacuum Setting		Pressure	Setting						
Emergency Relief Value	ve (psig)								
Vacuum Setting		Pressure	Setting						
□ Thief Hatch Weighted □	Yes 🗆	No							
¹ Complete appropriate Air	Pollutio	n Control	Device Sh	leet					
20. Expected Emission Ra	ite (submi	it Test Da	ta or Calcı	ilations he	ere or elsev	where in the	he applicat	tion).	1
Material Name	Flashi	Flashing Loss Breathing Loss Working Loss Total				-	Estimation Method ¹		
							Emissio	ns Loss	
	lb/br	tow	lb/br	tor	lb/br	tny	(VUC)	tny	
Produced Liquid	10/111	ιру	10/111	ιpy	10/111	ιpy	0.2975	0.0771	MB
Filoadood Elquid							0.25775		

¹ EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify) *Remember to attach emissions calculations, including TANKS Summary Sheets and other modeling summary sheets if applicable.*

TANK CONSTRUCTION AND OPERATION INFORMATION

21. Tank Shell Construction:

X Riveted \Box Gunite lined \Box Epoxy-	-coated rivets 🛛 Oth	ner (des	cribe)			
21A. Shell Color: Tan	21B. Roof Color: Tan			21C. Year	Last Painted:2017	
22. Shell Condition (if metal and unlined):	1					
X No Rust 🗆 Light Rust 🗆 Dense	Rust 🗌 Not applic	able				
22A. Is the tank heated? \Box Yes X No	22B. If yes, operating t	emperati	ire:	22C. If yes	s, how is heat provided to	
				tank?		
23. Operating Pressure Range (psig):Ambient						
Must be listed for tanks using VRUs with	th closed vent system	•				
24. Is the tank a Vertical Fixed Roof Tank ?	24A. If yes, for dome	coof provide radius (ft): 24B. If yes, for cone roof, provide slo				
X Yes UNo	6					
25. Complete item 25 for Floating Roof Tanks	\square Does not apply	Х				
25A. Year Internal Floaters Installed:						
25B. Primary Seal Type (check one):	llic (mechanical) shoe	seal	🗆 Liquid mou	nted resilie	nt seal	
\Box Vapor mounted resilient seal \Box O	ther (describe):					
25C. Is the Floating Roof equipped with a seco	ndary seal? 🗌 Yes	□No				
25D. If yes, how is the secondary seal mounted	? (check one) \Box Shoe	□ F	Rim 🗆 Other	r (describe)	:	
25E. Is the floating roof equipped with a weath	er shield? Ves		Ĩ0	, ,		
25E. Describe deck fittings:			0			
251. Describe deck multzs.						
26. Complete the following section for Interna	l Floating Roof Tanks	X Does	not apply			
26A Deck Type: D Bolted W	/elded	26B. 1	For bolted decks.	provide dec	k construction:	
	ciucu			1		
26C. Deck seam. Continuous sheet construction	n:					
\Box 5 ft. wide \Box 6 ft. wide \Box 7 ft. wide	e \Box 5 x 7.5 ft. wide	□ 5 x	12 ft. wide	other (de	scribe)	
26D. Deck seam length (ft.): 26E. Area	of deck (ft ²):	26F. For column supported 26G. For column supported				
		tanks,	# of columns:		tanks, diameter of column:	
27. Closed Vent System with VRU? \Box Yes 2	X No					
28. Closed Vent System with Enclosed Combus	stor? 🗆 Yes X No					
SITE INFORMATION						
29. Provide the city and state on which the data	in this section are based:	Charle	ston, WV			
30. Daily Avg. Ambient Temperature (°F): 54.	75	31. Ai	nnual Avg. Maxi	mum Tempe	rature (°F):65.5	
32. Annual Avg. Minimum Temperature (°F): 4	44	33. A	vg. Wind Speed	(mph): 6.3		
34. Annual Avg. Solar Insulation Factor (BTU/	ft ² -day):1123	35. At	mospheric Press	ure (psia):14	.617	
LIQUID INFORMATION				1		
36. Avg. daily temperature range of bulk	36A. Minimum (°F): 5	52.2		36B. Max	imum (°F): 65.5	
Inquid (FF): 13.5	27.4 Minimum (naia)	0.0101 27D M : (:) 0.0075			imum (nois): 0 0075	
(psig): 0.425	57A. Willingin (psig):	0.2191		J/D. Max	mum (psig): 0.9073	
(psig). 0.425						
38A. Minimum liquid surface temperature (°F)	:52.2	38B. (Corresponding va	apor pressure	e (psia):0.2191	
39A. Avg. liquid surface temperature (°F): 56.	3	39B. Corresponding vapor pressure (psia):0.4525				
40A. Maximum liquid surface temperature (°F)	:66.7	40B. Corresponding vapor pressure (psia):0.9075				
41. Provide the following for each liquid or gas	to be stored in the tank.	Add add	litional pages if 1	necessary.		
41A. Material name and composition:	Produced Liqui	d				
41B. CAS number:	-					
41C. Liquid density (lb/gal):	8.33					
41D. Liquid molecular weight (lb/lb-mole):	18.02					
41E. Vapor molecular weight (lb/lb-mole):	18.02					
41F. Maximum true vapor pressure (psia):	1.0					
410. Maximum Kelu vapor pressure (psia): 41H. Months Storage per year	0.46					
From: To:	12					
42. Final maximum gauge pressure and						
temperature prior to transfer into tank used as	O/Ambient					
inputs into flashing emission calculations.						

ATTACHMENT L – STORAGE VESSEL DATA SHEET

Complete this data sheet if you are the owner or operator of a storage vessel that contains condensate and/or produced water. This form must be completed for *each* new or modified bulk liquid storage vessel(s) that contains condensate and/or produced water. (If you have more than one (1) identical tank (i.e. 4-400 bbl condensate tanks), then you can list all on one (1) data sheet). **Include gas sample analysis, flashing emissions, working and breathing losses, USEPA Tanks, simulation software (ProMax, E&P Tanks, HYSYS, etc.), and any other supporting documents where applicable.**

The following information is **REQUIRED**:

□Composition of the representative sample used for the simulation □For each stream that contributes to flashing emissions:

- \Box Temperature and pressure (inlet and outlet from separator(s))
- □ Simulation-predicted composition
- □Molecular weight
- □Flow rate
- □Resulting flash emission factor or flashing emissions from simulation

 \Box Working/breathing loss emissions from tanks and/or loading emissions if simulation is used to quantify those emissions

Additional information may be requested if necessary.

GENERAL INFORMATION (REQUIRED)

1. Bulk Storage Area Name	2. Tank Name Tank -3
Tonys Bridge	
3. Emission Unit ID number: TNK-3	4. Emission Point ID number 7E
5. Date Installed , Modified or Relocated (for existing tanks)	6. Type of change:
(Expected March 2017)	X New construction \Box New stored material \Box Other
Was the tank manufactured after August 23, 2011 and on or	
before September 18, 2015?	
□ Yes X No	
Was the tank manufactured after September 18, 2015?	
X Yes 🗆 No	
7A. Description of Tank Modification (<i>if applicable</i>)	
7B. Will more than one material be stored in this tank? If so, a s	eparate form must be completed for each material.
\Box Yes X No	
7C. Was USEPA Tanks simulation software utilized?	
\Box Yes X No	
If Yes, please provide the appropriate documentation and items	8-42 below are not required.

TANK INFORMATION

8. Design Capacity (specify barrels or gallons). Use the internal	l cross-sectional area multiplied by internal height.
400 BBL	
9A. Tank Internal Diameter (ft.) 12	9B. Tank Internal Height (ft.) 20
10A. Maximum Liquid Height (ft.) 17	10B. Average Liquid Height (ft.) 10
11A. Maximum Vapor Space Height (ft.) 17	11B. Average Vapor Space Height (ft.) 10
12. Nominal Capacity (specify barrels or gallons). This is also I	known as "working volume".

13A. Maximum annual throughput (gal/yr) 873,600	13B. Maximum daily throughput (gal/day) 2393
14. Number of tank turnovers per year 52	15. Maximum tank fill rate (gal/min) 60
16. Tank fill method X Submerged \Box Splash	□ Bottom Loading
17. Is the tank system a variable vapor space system? \Box Ye	s X No
If yes, (A) What is the volume expansion capacity of the system	m (gal)?
(B) What are the number of transfers into the system pe	r year?
18. Type of tank (check all that apply):	
X Fixed Roof \Box vertical \Box horizontal \Box flat roo	f \Box cone roof \Box dome roof \Box other (describe)
\Box External Floating Roof \Box pontoon roof \Box doub	le deck roof
□ Domed External (or Covered) Floating Roof	
\Box Internal Floating Roof \Box vertical column support	□ self-supporting
□ Variable Vapor Space □ lifter roof □ diaphrag	n
\Box Pressurized \Box spherical \Box cylindrical	
\Box Other (describe)	

PRESSURE/VACUUM CONTROL DATA

19. Check as many as app	ly:								
X Does Not Apply				□ Rupture	e Disc (psi	g)			
\Box Inert Gas Blanket of		Ca	arbon Ads	orption ¹					
□Vent to Vapor Combust	ion Devic	e ¹ (vapor	combusto	rs, flares,	thermal ox	dizers, e	nclosed co	mbustors)	
□ Conservation Vent (psi	g)□Con	denser ¹							
Vacuum Setting		Pressure	Setting						
□ Emergency Relief Valv	ve (psig)								
Vacuum Setting		Pressure	Setting						
□ Thief Hatch Weighted □	Yes 🗆	No							
¹ Complete appropriate Air	Pollutio	n Control	Device Sh	neet					
20. Expected Emission Ra	te (subm	it Test Da	ta or Calcı	ulations he	ere or elsev	where in t	ne applicat	tion).	
Material Name	Flashi	ng Loss	Loss Breathing Loss Working Loss Total		-	Estimation Method ¹			
							Emissio	ns Loss	
							(\mathbf{VOC})		
	lb/br	tny	lh/hn	tny	lb/br	tny	(VOC)	tny	-
Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr	tpy	MB
Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr 0.2975	tpy 0.0771	МВ
Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr 0.2975	tpy 0.0771	МВ
Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr 0.2975	tpy 0.0771	MB
Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr 0.2975	tpy 0.0771	MB
Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) lb/hr 0.2975	tpy 0.0771	MB
Produced Liquid	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	(VOC) Ib/hr 0.2975	tpy 0.0771	MB
Produced Liquid	lb/hr		lb/hr		lb/hr	tpy	(VOC) Ib/hr 0.2975	tpy 0.0771	MB
Produced Liquid	lb/hr				b/hr	tpy	(VOC) Ib/hr 0.2975	tpy 0.0771	MB
Produced Liquid	lb/hr		b/hr		b/hr	tpy	(VOC) Ib/hr 0.2975	tpy 0.0771	MB

¹ EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify) *Remember to attach emissions calculations, including TANKS Summary Sheets and other modeling summary sheets if applicable.*

TANK CONSTRUCTION AND OPERATION INFORMATION							
21. Tank Shell Construction:							
X Riveted \Box Gunite lined \Box Epoxy-coated rivets \Box Other (describe)							
21A. Shell Color: Tan	21B. Roof Color: Tan	21C. Year Last Painted:2017					

22. Shell Condition (if metal and unlined):								
X No Rust 🗆 Light Rust 🗆 Dense	Rust 🗌 Not application	able						
22A. Is the tank heated? \Box Yes X No 22B. If yes, operating temperature: 22C. If yes, how is heat provided to								
23 Operating Pressure Pange (psig): Ambient								
23. Operating ressure Range (psig). Amorent	th closed vent system							
24 Is the tank a Vortical Fixed Doof Tank?	24A If yes, for dome	roof prov	ride radius (ft):	24B If you	s for cone roof provide slop (ft/ft);			
X Yes \square No	6		ide fadius (it).	24 D . II ye	s, for cone foor, provide slop (1717).			
25. Complete item 25 for Floating Roof Tanks	$s \square$ Does not apply	Х						
25A. Year Internal Floaters Installed:								
25B. Primary Seal Type (check one):	llic (mechanical) shoe	seal	🗆 Liquid mou	nted resilie	nt seal			
\Box Vapor mounted resilient seal \Box O	ther (describe):		1					
25C. Is the Floating Roof equipped with a seco	ndary seal? 🛛 Yes	□No						
25D. If yes, how is the secondary seal mounted	? (check one) \Box Shoe	□ F	Rim 🗌 Other	r (describe)	:			
25E. Is the floating roof equipped with a weath	er shield? 🗌 Yes	ΠN	о					
25F. Describe deck fittings:								
2011 Deserve deen mangs								
26. Complete the following section for Interna	l Floating Roof Tanks	X Does	not apply					
26A. Deck Type: D Bolted W	Velded	26B. 1	For bolted decks,	provide dec	k construction:			
				•				
26C. Deck seam. Continuous sheet construction	n:							
\Box 5 ft. wide \Box 6 ft. wide \Box 7 ft. wide	e \Box 5 x 7.5 ft. wide	□ 5 x	12 ft. wide \Box	other (de	scribe)			
26D. Deck seam length (ft.): 26E. Area	u of deck (ft ²):	26F. I	For column suppo	orted	26G. For column supported			
		tanks, # of columns: tanks, diameter			tanks, diameter of column:			
	N							
27. Closed Vent System with VRU? \Box Yes 2	X No							
28. Closed Vent System with Enclosed Combus	stor? 🗆 Yes X No							
SITE INFORMATION								
29. Provide the city and state on which the data	in this section are based:	Charle	ston, WV					
30. Daily Avg. Ambient Temperature (°F): 54.	75	31. Ai	nnual Avg. Maxi	mum Tempe	rature (°F):65.5			
32. Annual Avg. Minimum Temperature (°F): 4	44	33. A	vg. Wind Speed ((mph): 6.3				
34. Annual Avg. Solar Insulation Factor (BTU/	(ft ² -day):1123	35. At	mospheric Press	ure (psia):14	.617			
LIQUID INFORMATION								
36. Avg. daily temperature range of bulk liquid (°F): 13.3	36A. Minimum (°F): 5	52.2		36B. Max	imum (°F): 65.5			
37. Avg. operating pressure range of tank	37A. Minimum (psig):	0.2191		37B. Max	imum (psig): 0.9075			
(psig): 0.425								
	50.0	2010			(
38A. Minimum liquid surface temperature (°F)	:52.2	38B. 0	Corresponding va	apor pressure	e (psia):0.2191			
39A. Avg. inquid surface temperature (°F): 56.	3	39B. Corresponding vapor pressure (psia):0.4525						
40A. Maximum inquid surface temperature (F)	1:00. /	40B. C	Corresponding va	apor pressure	e (psia):0.9075			
41. Provide the following for each liquid of gas	Dredered Lizzi	Auu auu	intional pages if I	lecessaly.				
41A. Material hame and composition.	Produced Liqui	a						
41C Liquid density (lb/gal):	-							
41D Liquid molecular weight (lb/lb-mole):	18.02							
41E. Vapor molecular weight (lb/lb-mole):	41E Vanor molecular weight (lb/lb-mole): 10.02							
41F Maximum true vapor pressure (psia): 1.0								
41G. Maximum Reid vapor pressure (psia).	0.46							
41H. Months Storage per year.	0.40							
From: To:	12							
42. Final maximum gauge pressure and								
temperature prior to transfer into tank used as	O/Ambient							
inputs into flashing emission calculations.								

ATTACHMENT L – STORAGE VESSEL DATA SHEET

Complete this data sheet if you are the owner or operator of a storage vessel that contains condensate and/or produced water. This form must be completed for *each* new or modified bulk liquid storage vessel(s) that contains condensate and/or produced water. (If you have more than one (1) identical tank (i.e. 4-400 bbl condensate tanks), then you can list all on one (1) data sheet). **Include gas sample analysis, flashing emissions, working and breathing losses, USEPA Tanks, simulation software (ProMax, E&P Tanks, HYSYS, etc.), and any other supporting documents where applicable.**

The following information is **REQUIRED**:

□Composition of the representative sample used for the simulation □For each stream that contributes to flashing emissions:

- \Box Temperature and pressure (inlet and outlet from separator(s))
- □ Simulation-predicted composition

□Molecular weight

□Flow rate

□Resulting flash emission factor or flashing emissions from simulation

 \Box Working/breathing loss emissions from tanks and/or loading emissions if simulation is used to quantify those emissions

Additional information may be requested if necessary.

GENERAL INFORMATION (REQUIRED)

1. Bulk Storage Area Name	2. Tank Name Tank -4				
Tonys Bridge					
3. Emission Unit ID number: TNK-4	4. Emission Point ID number 8E				
5. Date Installed, Modified or Relocated (for existing tanks)	6. Type of change:				
(Expected March 2017)	X New construction \Box New stored material \Box Other				
Was the tank manufactured after August 23, 2011 and on or	□Relocation				
before September 18, 2015?					
\Box Yes X No					
Was the tank manufactured after September 18, 2015?					
X Yes 🗆 No					
7A. Description of Tank Modification (<i>if applicable</i>)					
7B. Will more than one material be stored in this tank? If so, a	separate form must be completed for each material.				
\Box Yes X No					
7C. Was USEPA Tanks simulation software utilized?					
\Box Yes X No					
If Yes, please provide the appropriate documentation and items 8-42 below are not required.					

TANK INFORMATION

 Design Capacity (<i>specify barrels or gallons</i>). Use the internal cross-sectional area multiplied by internal height. 400 BBL 			
9A. Tank Internal Diameter (ft.) 12	9B. Tank Internal Height (ft.) 20		
10A. Maximum Liquid Height (ft.) 17	10B. Average Liquid Height (ft.) 10		

12. Nominal Capacity (specify barrels or gallons). This is also known as "working volume".					
13A. Maximum annual throughput (gal/yr) 873,600	13B. Maximum daily throughput (gal/day) 2393				
14. Number of tank turnovers per year 52	15. Maximum tank fill rate (gal/min) 60				
16. Tank fill method X Submerged \Box Splash	□ Bottom Loading				
17. Is the tank system a variable vapor space system? \Box Yes	X No				
If yes, (A) What is the volume expansion capacity of the system	(gal)?				
(B) What are the number of transfers into the system per	year?				
18. Type of tank (check all that apply):					
X Fixed Roof \Box vertical \Box horizontal \Box flat roof	\Box cone roof \Box dome roof \Box other (describe)				
\Box External Floating Roof \Box pontoon roof \Box double	e deck roof				
Domed External (or Covered) Floating Roof					
□ Internal Floating Roof □ vertical column support	□ self-supporting				
\Box Variable Vapor Space \Box lifter roof \Box diaphragm					
\Box Pressurized \Box spherical \Box cylindrical					
\Box Other (describe)					

PRESSURE/VACUUM CONTROL DATA

19. Check as many as app	ly:								
X Does Not Apply									
□ Inert Gas Blanket of	\Box Inert Gas Blanket of \Box Carbon Adsorption ¹								
□Vent to Vapor Combusti	ion Devic	e ¹ (vapor	combusto	rs, flares, t	thermal ox	idizers, e	nclosed co	mbustors)	
□ Conservation Vent (psi	g) 🗆 Con	denser ¹							
Vacuum Setting		Pressure	Setting						
Emergency Relief Value	ve (psig)								
Vacuum Setting		Pressure	Setting						
□ Thief Hatch Weighted □	Yes 🗆	No							
¹ Complete appropriate Air	Pollutio	n Control	Device Sh	leet					
20. Expected Emission Ra	ite (subm	it Test Da	ta or Calcı	ulations he	ere or elsev	where in the	he applicat	tion).	1
Material Name	Flashi	ng Loss	Breathi	ng Loss	Workin	g Loss	Total	-	Estimation Method ¹
						Emissions Loss			
	lb/br	tow	lb/br	tor	lb/bn	tny	(VUC)	tny	
Produced Liquid	10/111	ιру	10/111	ιpy	10/111	ιpy	0.2975	0.0771	MB
Filoadeed Elquid							0.237.0	010771	MD
								-	

¹ EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify) *Remember to attach emissions calculations, including TANKS Summary Sheets and other modeling summary sheets if applicable.*

TANK CONSTRUCTION AND OPERATION INFORMATION

21. Tank Shell Construction:

X Riveted \Box Gunite lined \Box Epoxy-coated rivets \Box Other (describe)									
21A. Shell Color: Tan	21A. Shell Color: Tan 21B. Roof Color: Tan 21C. Year Last Painted:2017								
22. Shell Condition (if metal and unlined):									
X No Rust 🗆 Light Rust 🗆 Dense Rust 🗆 Not applicable									
22A. Is the tank heated? \Box Yes X No	22B. If yes, operating t	emperati	ire:	22C. If yes	s, how is heat provided to				
				tank?					
23. Operating Pressure Range (psig):Ambient									
Must be listed for tanks using VRUs with closed vent system.									
24. Is the tank a Vertical Fixed Roof Tank? 24A. If yes, for dome roof provide radius (ft): 24B. If yes, for cone roof, provide slop (ft									
λ Yes ⊔No 0									
25. Complete item 25 for Floating Roof Tanks	\square Does not apply	Х							
25A. Year Internal Floaters Installed:									
25B. Primary Seal Type (check one):	llic (mechanical) shoe	seal	🗆 Liquid mou	nted resilie	nt seal				
\Box Vapor mounted resilient seal \Box O	ther (describe):								
25C. Is the Floating Roof equipped with a second	ndary seal? 🛛 Yes	□No							
25D. If yes, how is the secondary seal mounted	? (check one) \Box Shoe	□ F	Rim 🗆 Other	r (describe)	:				
25E Is the floating roof equipped with a weath	er shield? \Box Ves		 0	(======================================	·				
25E. Describe deck fittings:			0						
251. Describe deck muligs.									
26 Complete the following section for Interna	l Floating Roof Tanks	X Does	not apply						
26A Deck Type: Bolted W	/elded	26B. 1	For bolted decks.	provide dec	k construction:				
	elded		,	·					
26C. Deck seam. Continuous sheet construction	n:								
\Box 5 ft. wide \Box 6 ft. wide \Box 7 ft. wide	e \Box 5 x 7.5 ft. wide	□ 5 x	12 ft. wide	dia ther (de	scribe)				
26D. Deck seam length (ft.): 26E. Area	of deck (ft ²):	26F. I	For column suppo	orted	26G. For column supported				
		tanks, # of columns:			tanks, diameter of column:				
27. Closed Vent System with VRU? \Box Yes λ	X No								
28. Closed Vent System with Enclosed Combus	stor? 🗆 Yes X No								
SITE INFORMATION									
29. Provide the city and state on which the data	in this section are based:	Charle	ston, WV						
30. Daily Avg. Ambient Temperature (°F): 54.	75	31. Ai	nnual Avg. Maxi	mum Tempe	rature (°F):65.5				
32. Annual Avg. Minimum Temperature (°F): 4	44	33. Av	vg. Wind Speed	(mph): 6.3					
34. Annual Avg. Solar Insulation Factor (BTU/	ft ² -day):1123	35. At	mospheric Press	ure (psia):14	.617				
LIQUID INFORMATION									
36. Avg. daily temperature range of bulk	36A. Minimum (°F): 5	36B. Maximum (°F): 65.5			imum (°F): 65.5				
37 Avg operating pressure range of tank	374 Minimum (nsig)	0.2101 27D Marin			imum (psig): 0 9075				
(psig): 0.425	57A. Willindin (psig).	0.2171		57D. Max	inium (psig). 0.9075				
(1-2),									
38A. Minimum liquid surface temperature (°F)	:52.2	38B. (Corresponding va	apor pressure	e (psia):0.2191				
39A. Avg. liquid surface temperature (°F): 56.	3	39B. (Corresponding va	apor pressure	e (psia):0.4525				
40A. Maximum liquid surface temperature (°F)	:66.7	40B. (Corresponding va	apor pressure	e (psia):0.9075				
41. Provide the following for each liquid or gas	to be stored in the tank.	Add add	litional pages if 1	necessary.					
41A. Material name and composition:	Produced Liqui	d							
41B. CAS number:	-								
41C. Liquid density (Ib/gal):	8.33								
41D. Liquiu nioiccutai Weight (10/10-inioie): 18.02									
41F. Maximum true vanor pressure (psia): 1.0									
41G. Maximum Reid vapor pressure (psia):	0.46								
41H. Months Storage per year.									
From: To:	12								
42. Final maximum gauge pressure and									
temperature prior to transfer into tank used as	O/Ambient								
inputs into flashing emission calculations.									

STORAGE TANK DATA TABLE

List all deminimis storage tanks (i.e. lube oil, glycol, diesel etc.)

Source ID # ¹	Status ²	Content ³	Volume ⁴
TNK-5	New	Water w/ Sand	8820 (gal)

1. Enter the appropriate Source Identification Numbers (Source ID #) for each storage tank located at the well site. Tanks should be designated T01, T02, T03, etc. 2.

Enter storage tank Status using the following: EXIST Existing Equipment

NEW Installation of New Equipment

REM Equipment Removed

Enter storage tank content such as condensate, pipeline liquids, glycol (DEG or TEG), lube oil, diesel, mercaptan etc. 3.

Enter the maximum design storage tank volume in gallons. 4.

ATTACHMENT M – SMALL HEATERS AND REBOILERS NOT SUBJECT TO 40CFR60 SUBPART DC DATA SHEET

Complete this data sheet for each small heater and reboiler not subject to 40CFR60 Subpart Dc at the facility. *The Maximum Design Heat Input (MDHI)must be less than 10 MMBTU/hr.*

Emission Unit ID# ¹	Emission Point ID# ²	Emission Unit Description (manufacturer, model #)	Year Installed/ Modified	Type ³ and Date of Change	Maximum Design Heat Input (MMBTU/hr) ⁴	Fuel Heating Value (BTU/scf) ⁵
HTR-1	1E	River Bend Industries	3/17	New	1	1030
HTR-2	2E	River Bend Industries	3/17	New	1	1030
HTR-3	3E	River Bend Industries	3/17	New	1	1030
HTR-4	4E	River Bend Industries	3/17	New	1	1030
TE-1	9E	Gentherm Global Power Technologies (Model 5220)	3/17	NEW	0.0007	1030

- ¹ Enter the appropriate Emission Unit (or Source) identification number for each fuel burning unit located at the production pad. Gas Producing Unit Burners should be designated GPU-1, GPU-2, etc. Heater Treaters should be designated HT-1, HT-2, etc. Heaters or Line Heaters should be designated LH-1, LH-2, etc. For sources, use 1S, 2S, 3S...or other appropriate designation. Enter glycol dehydration unit Reboiler Vent data on the Glycol Dehydration Unit Data Sheet.
- ² Enter the appropriate Emission Point identification numbers for each fuel burning unit located at the production pad. Gas Producing Unit Burners should be designated GPU-1, GPU-2, etc. Heater Treaters should be designated HT-1, HT-2, etc. Heaters or Line Heaters should be designated LH-1, LH-2, etc. For emission points, use 1E, 2E, 3E...or other appropriate designation.
- ³ New, modification, removal
- ⁴ Enter design heat input capacity in MMBtu/hr.
- ⁵ Enter the fuel heating value in BTU/standard cubic foot.

ATTACHMENT O – TANKER TRUCK/RAIL CAR LOADING DATA SHEET

Complete this data sheet for each new or modified bulk liquid transfer area or loading rack at the facility. This is to be used for bulk liquid transfer operations to tanker trucks/rail cars. Use extra pages if necessary.

Truck/Rail Car Loadout Collection Efficiencies

The following applicable capture efficiencies of a truck/rail car loadout are allowed:

- For tanker trucks/rail cars passing the MACT level annual leak test 99.2%
- For tanker trucks/rail cars passing the NSPS level annual leak test 98.7%
- For tanker trucks/rail cars not passing one of the annual leak tests listed above 70%

Compliance with this requirement shall be demonstrated by keeping records of the applicable MACT or NSPS Annual Leak Test certification for *every* truck and railcar loaded/unloaded. This requirement can be satisfied if the trucking/rail car company provided certification that its entire fleet was compliant. This certification must be submitted in writing to the Director of the DAQ. These additional requirements must be noted in the Registration Application.

Emission Unit ID#: LO-	on Unit ID#: LO-1 Emission Point ID#: NA				Year Installed/Modified: 2017			
Emission Unit Description: TNK-1, TNK-2, TNK-3, TNK-4								
			Loading A	Area Data				
Number of Pumps: NA		Numbe	r of Liquids	Loaded:		Max number at one (1) t	er of t ime:	trucks/rail cars loading 1
Are tanker trucks/rail ca If Yes, Please describe:	ars pressure teste	ed for lea	ks at this or	any other loc	ation?	□ Yes □	No	X Not Required
Provide description of c	Provide description of closed vent system and any bypasses. NA							
 Are any of the following truck/rail car loadout systems utilized? Closed System to tanker truck/rail car passing a MACT level annual leak test? Closed System to tanker truck/rail car passing a NSPS level annual leak test? Closed System to tanker truck/rail car not passing an annual leak test and has vapor return? 								
Pro	jected Maximu	n Operat	ing Schedul	e (for rack o	r transf	er point as a	n who	ole)
Time	Jan – Ma	ır	Apr	- Jun	J	ul – Sept		Oct - Dec
Hours/day	2			2		2		2
Days/week	1			1	1			1
	Bulk Liquid Data (use extra pages as necessary)							
Liquid Name	Producti	on Liquio	1					
Max. Daily Throughput (1000 gal/day)	21.4							
Max. Annual Throughpu (1000 gal/yr)	ut 151.2							
Loading Method ¹	BF							
Max. Fill Rate (gal/min) 60							
Average Fill Time (min/loading)	30							
Max. Bulk Liquid Temperature (°F)	80	80						
True Vapor Pressure ²	10.2							
Cargo Vessel Condition	³ C							
Control Equipment or Method ⁴	NA							
Max. Collection Efficie (%)	ncy NA							

Max. Control Efficiency (%)		NA	
Max.VOC Emission Rate Loading (lb/hr) Annual (ton/yr)	Loading (lb/hr)	<0.5929	
	Annual (ton/yr)	<0.0617	
Max.HAP Emission Rate	Loading (lb/hr)	De minimis	
	Annual (ton/yr)	De minimis	
Estimation Method ⁵		МВ	

1	BF	Bottom Fill	SP	Splash Fill			SUB	Submerged Fill
2	At maxim	um bulk liquid temperature						
3	В	Ballasted Vessel	С	Cleaned			U	Uncleaned (dedicated service)
	0	Other (describe)						
4	List as m	any as apply (complete and su	ıbmit appı	ropriate A	ir Pollutio	on Contro	l Device S	heets)
	CA	Carbon Adsorption		VB	Dedicate	d Vapor B	alance (cl	osed system)
	ECD	Enclosed Combustion Device	•	F	Flare	-		-
	ТО	Thermal Oxidization or Incin	eration					
5	EPA	EPA Emission Factor in AP-4	42			MB	Material	Balance
	TM Test Measurement based upon test data submittal			1	0	Other (des	cribe)	

ATTACHMENT Q – PNEUMATIC CONTROLLERS DATA SHEET				
Are there any continuous bleed natural gas driven pneumatic controllers at this facility that commenced construction, modification or reconstruction after August 23, 2011, and on or before September 18, 2015?				
\Box Yes \boxtimes No				
Please list approximate number.				
Are there any continuous bleed natural gas driven pneumatic controllers at this facility that commenced construction, modification or reconstruction after September 18, 2015?				
\Box Yes \boxtimes No				
Please list approximate number.				
Are there any continuous bleed natural gas driven pneumatic controllers at this facility with a bleed rate greater than 6 standard cubic feet per hour that are required based on functional needs, including but not limited to response time, safety and positive actuation that commenced construction, modification or reconstruction after August 23, 2011, and on or before September 18, 2015?				
\Box Yes \boxtimes No				
Please list approximate number.				
Are there any continuous bleed natural gas driven pneumatic controllers at this facility with a bleed rate greater than 6 standard cubic feet per hour that are required based on functional needs, including but not limited to response time, safety and positive actuation that commenced construction, modification or reconstruction after September 18, 2015?				
\Box Yes \boxtimes No				
Please list approximate number.				

ATTACHMENT R – PNEUMATIC PUMP DATA SHEET

Are there any natural gas-driven diaphragm pumpslocated at a well site that commenced construction, modification or reconstruction after September 18, 2015?

Yes No

Please list.

Source ID #	rce Date Pump Make/M		Model Pump Size		

ATTACHMENT T-EMISSIONS CALCULATIONS

Provide detailed potential to emit (PTE) emission calculations for criteria and hazardous air pollutants (HAPs) for each emission point identified in the application. For hazardous air pollutants and volatile organic compounds (VOCs), the speciated emission calculations must be included.

Use the following guidelines to ensure complete emission calculations:

- All emission sources and fugitive emissions are included in the emission calculations, as well as all methods used to calculate the emissions.
- Proper emission point identification numbers and APCD and ERD identification numbers are used consistently in the emission calculations that are used throughout the application.
- A printout of the emission summary sheets is attached to the registration application.
- Printouts of any modeling must be included with the emission calculations. The modeling printout must show all inputs/outputs or assumptions that the modeled emissions are based upon.
- If emissions are provided from the manufacturer, the manufacturer's documentation and/or certified emissions must also be included.
- The emission calculations results must match the emissions provided on the emissions summary sheet.
- If calculations are based on a compositional analysis of the gas, attach the laboratory analysis. Include the following information: the location that the sample was taken (and whether the sample was taken from the actual site or a representative site); the date the sample was taken; and, if the sample is considered representative, the reasons that it is considered representative (same gas field, same formation and depth, distance from actual site, etc.).
- Provide any additional clarification as necessary. Additional clarification or information is especially helpful when reviewing modeling calculations to assist the engineer in understanding the basis of assumptions and/or inputs.

Please follow specific guidance provided on the emissions summary sheet when providing the calculations.

Fugitive Emission Calculations

Mountaineer Keystone - Tonys Bridge Fugitive Emission Calculations (See Attachment J)

Density					
Pollutant	Density (kg/m ³)	Density (lb/scf)			
VOC	3.35	0.2087			
CH4	0.656	0.0409			

Emission Factors ¹					
Component Type	Count	(scf /hr/ component)			
Pumps	0	13.30			
Valves	249	0.027			
Safety Relief Valves	21	0.04			
Open Ended Lines	5	0.061			
Sampling Connections	4	0.003			
Connections	1226	0.003			
Compressors	0	7.00			
Flanges	241	0.003			
Other⁵	62	0.003			

Emissions						
Componenty Type	VOC Emissions (tons/yr) ^{2,3}	Methane (tons/yr) ⁴	CO2 eq (tons/yr)			
Pumps	0	0	0			
Valves	0.4302	1.1192	27.98			
Safety Relief Valves	0.0537	0.1398	3.50			
Open Ended Lines	0.0195	0.0508	1.27			
Sampling Connections	0.0008	0.0020	0.0499			
Connections	0.2353	0.6123	15.31			
Compressors	0	0	0			
Flanges	0.0463	0.1204	3.01			
Other	0.0119	0.0310	0.77			
Total	0.80	2.08	51.88			

Emissions are calculated as follows:

Emissions = Emission Factor (scf/hr/component) * Component Count * Density (lb/scf) * 8,760 (hrs/yr) * Constituent CO2e Emissions = Methane Emissions (tons/yr) * 25 (GWP)

¹ Emission Factors for Pumps, Valves. Safety Relief Valves, and Open Ended Lines taken from 40 CFR 98 Table W-1A. Flanges emission factor assumed to be equal to Connections emission factor

Notes:

² VOC calculated using gas analysis average of VOCs

³ VOC weight % approximated to be 7% of fugitive emissions based on gas analysis

⁴ Methane weight % assumed to be about 93% of fugitive emissions

⁵ Other components include meters, regulators and Diaphragms

Tank Emission Calculations

Mountaineer Keystone - Tony's Bridge Wellpad TK-1, TK-2, TK-3, TK-4 Combined Emission Calculation (See Attachment L)

			l oapaoi	- J	
Appual Throughput ²	bbl/yr	gal/yr	L/yr		
Annual mroughput	416,000	17,472,000	66,131,520		
Compound	Concentration ¹ (ug/L)	Emissions (g/yr)	Emissions (lbs/yr)	Emissions (lbs/hr)	Emissions (tons/yr)
Methane	24000	1,587,156	3,499	6.73	1.75
Ethane	2100	138,876	306.17	0.5888	0.1531
Propane	5	330.66	0.7290	0.0014	0.0004
iso-Butane	1.6	105.81	0.2333	0.0004	0.0001
n-Butane	7.9	522.44	1.15	0.0022	0.0006
Methane Total ³	-	3,174,313	6,998	13.46	3.50
CO2e Total ³	-	158,715,648	349,908	672.90	174.95
VOC Total ³	-	279,670	616.57	1.19	0.3083

TK-1, TK-2, TK-3, TK-4 - 400 bbl Capacity

Emissions are calculated as follows:

Emissions (lb/yr) = Throughput (L/yr) * Concentration (ug/L) * (lb/ 4.54E8 ug)

Emissions (lb/hr) = Emissions (lb/yr) * (yr/ 1040 unloads) * (Unload /1 hr)

CO2e Emissions = Methane Emissions (tons/yr) * 25 (GWP)

¹ Concentrations of Produced Liquid is based on analytical results dated November 11, 2016

² Each tank is fully unloaded 5 times per week (52 weeks/yr * 400 bbl/tank * 4 tanks * 5 unloads = 416,000 bbl/yr)

Assumptions:

- All VOC and GHG present in the Produced Liquid is emitted

- Produced liquid is mostly water with minimal amounts of VOC and GHG

³ VOC and GHG totals from the above calculation is doubled for each tank in the facility total to overestimate any other potential VOCs not detected in the analytical results

- Each tank unloading takes one half hour and each tank is unloaded 5 times per week



Pace Analytical Energy Services LLC 220 William Pitt Way Pittsburgh, PA 15238

> Phone: (412) 826-5245 Fax: (412) 826-3433

November 11, 2016

Michael Michalski Ryan Environmental 5793 W Memorial Veteran's Hwy Bridgeport, WV 26330

RE: 161028_MKM_COMET&GOLFF

Pace Workorder: 20814

Dear Michael Michalski:

Enclosed are the analytical results for sample(s) received by the laboratory on Monday, October 31, 2016. Results reported herein conform to the most current NELAC standards, where applicable, unless otherwise narrated in the body of the report.

If you have any questions concerning this report, please feel free to contact me.

Sincerely,

Ruth Weiss

Ruth Welsh 11/11/2016 Ruth.Welsh@pacelabs.com

Customer Service Representative

Enclosures

As a valued client we would appreciate your comments on our service. Please email PAESfeedback@pacelabs.com.

Total Number of Pages 18

Report ID: 20814 - 861768

Page 1 of 15



CERTIFICATE OF ANALYSIS

This report shall not be reproduced, except in full, without the written consent of Pace Analytical Energy Services LLC.



Pace Analytical Energy Services LLC 220 William Pitt Way Pittsburgh, PA 15238

> Phone: (412) 826-5245 Fax: (412) 826-3433

ANALYTICAL RESULTS

Workorder: 20814 161028_MKM_COMET&GOLFF

Lab ID:	208140001		Date R	eceived:	10/31/2016 0	8:30 Matrix	x: Water
Sample ID: 161028_MKM_COMET_TANKS386&387				Date Collected: 10/28/2016 10:45			
Parameters	Results	Units PQ	L MDL	DF Ar	nalyzed	Ву	Qualifiers
RISK - PAES							
Analysis Desc	EPA RSK175	Analytical Method	: EPA RSK17	5			
Methane	24000	uq/l 5	0 1.9	100 11	/4/2016 11:07	AK	d,B
Ethane	2100	ug/l 2	0 0.50	100 11	/4/2016 11:07	AK	d
Ethene	0.20 U	ug/l 0.2	0 0.0070	1 11	/3/2016 10:43	AK	
Propane	58	ug/l 0.2	0.0080	1 11	/3/2016 10:43	AK	
iso-Butane	1.6	ug/l 0.4	0 0.018	1 11	/3/2016 10:43	AK	
n-Butane	7.9	ug/l 0.4	0 0.017	1 11	/3/2016 10:43	AK	
Subcontracte	ed Work - SCPG						G
Analysis Desc	:: SW-846 8260B	Analytical Method	: SW-846 826	60B			
Benzene	620 U	ug/kg 62	0 170	1 11	/9/2016 19:13	PAS	S
Toluene	620 U	ug/kg 62	0 190	1 11	/9/2016 19:13	PAS	s
Ethylbenzene	620 U	ug/kg 62	0 130	1 11	/9/2016 19:13	PAS	s
m,p-Xylene	1200 U	ug/kg 120	0 230	1 11	/9/2016 19:13	PAS	S
o-Xylene	620 U	ug/kg 62	0 120	1 11	/9/2016 19:13	PAS	S

Report ID: 20814 - 861768

nelaci

CERTIFICATE OF ANALYSIS

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Page 5 of 15

Heater Emission Calculations

Mountaineer Keystone - Tony's Bridge Wellpad Heater Emission Summary (HTR-1, HTR-2, HTR-3, HTR-4 Combined) Criteria Pollutants (See Attachment M)

Fuel Usage					
Fuel Units Total					
Natural Gas	ft ³	34,019,417			

Emission Factors ¹			
Heaters			
Pollutant	Natural Gas (lbs/ 10 ⁶ ft ³)		
Particulates	7.60		
Sulfur Dioxide	0.6000		
Oxides of Nitrogen	100.00		
PM-10	7.60		
VOC	5.50		
Carbon Monoxide	84.00		
Lead	0.0005		
CO2 Equiv	120,000		

Emissions						
		Heaters ²				
Pollutant	Natural Gas (lbs/yr)	Natural Gas (lbs/hr)	Natural Gas (tons/yr)			
Particulates	258.55	0.0295	0.1293			
Sulfur Dioxide	20.41	0.0023	0.0102			
Oxides of Nitrogen	3,402	0.3883	1.70			
PM-10	258.55	0.0295	0.1293			
VOC	187.11	0.0214	0.0936			
Carbon Monoxide	2,858	0.3262	1.43			
Lead	0.0170	1.94E-06	8.50E-06			
CO2 Equiv	4,082,330	466.02	2,041			

Emissions are calculated as follows:

Natural Gas Usage (ft^3) = (1 MMBtu/hr * 4 * 8760 hrs/yr * 10⁶ Btu/MMBtu)/ (1030 Btu/ft³) Emissions (Ibs/yr) = Volume of Gas (ft^3) * Emission Factor (Ibs/10⁶ ft³)

¹ Natural Gas Emission Factors were taken from AP-42 Tables 1.4-1 and 1.4-2

Notes:

 2 The wellpad operates 4 GPUs, which each have a heater with a rating of 1 MMBtu/hr. The emissions shown in the table are the sum of the four Heaters - Heating value of Natural Gas assumed to be 1,030 Btu/ft³

Mountaineer Keystone - Tony's Bridge Wellpad Heater Emission Summary (HTR-1, HTR-2, HTR-3, HTR-4 Combined) HAPS (See Attachment M)

Emissions are calculated as follows:

Emissions = Volume of Gas (ft^3) * Emission Factor ($lbs/10^6 ft^3$)

¹ Emission Factors from AP-42 Tables 1.4-3 and 1.4-4

Natural Gas
Heaters
НАР
ft ³
34,019,417

HAP Emissions			Natural Gas			
				Heaters		
			(lbs/yr)	(lbs/hr)	(tons/yr)	
НАР	CAS No.	Natural Gas ¹ (lb/10 ⁶ ft ³)				
2-Methylnaphthalene	91-57-6	2.40E-05	0.0008	9.32E-08	4.08E-07	
3-Methylchloranthrene	56-49-5	1.80E-06	6.12E-05	6.99E-09	3.06E-08	
7,12-Dimethylbenz(a)anthracene	-	1.60E-05	0.0005	6.21E-08	2.72E-07	
Acenaphthene	83-32-9	1.80E-06	6.12E-05	6.99E-09	3.06E-08	
Acenaphthylene	203-96-8	1.80E-06	6.12E-05	6.99E-09	3.06E-08	
Anthracene	120-12-7	2.40E-06	8.16E-05	9.32E-09	4.08E-08	
Benz(a)anthracene	56-55-3	1.80E-06	6.12E-05	6.99E-09	3.06E-08	
Benzene	71-43-2	2.10E-03	0.0714	8.16E-06	3.57E-05	
Benzo(a)pyrene	50-32-8	1.20E-06	4.08E-05	4.66E-09	2.04E-08	
Benzo(b)fluoranthene	205-99-2	1.80E-06	6.12E-05	6.99E-09	3.06E-08	
Benzo(g,h,i)perylene	191-24-2	1.20E-06	4.08E-05	4.66E-09	2.04E-08	
Benzo(k)fluoranthene	207-08-9	1.80E-06	6.12E-05	6.99E-09	3.06E-08	
Chrysene	218-01-9	1.80E-06	6.12E-05	6.99E-09	3.06E-08	
Dibenzo(a,h)anthracene	53-70-3	1.20E-06	4.08E-05	4.66E-09	2.04E-08	
Dichlorobenzene	25321-22-6	1.20E-03	0.0408	4.66E-06	2.04E-05	
Fluoranthene	206-44-0	3.00E-06	0.0001	1.17E-08	5.10E-08	
Fluorene	86-73-7	2.80E-06	9.53E-05	1.09E-08	4.76E-08	
Formaldehyde	50-00-0	7.50E-02	2.55	0.0003	0.0013	
Hexane	110-54-3	1.80E+00	61.23	0.0070	0.0306	
Indeno(1,2,3-cd)pyrene	193-39-5	1.80E-06	6.12E-05	6.99E-09	3.06E-08	
Naphthalene	91-20-3	6.10E-04	0.0208	2.37E-06	1.04E-05	
Phenanathrene	85-01-8	1.70E-05	0.0006	6.60E-08	2.89E-07	
Pyrene	129-00-0	5.00E-06	0.0002	1.94E-08	8.50E-08	
Toluene	108-88-3	3.40E-03	0.1157	1.32E-05	5.78E-05	
Arsenic	7440-38-2	2.00E-04	0.0068	7.77E-07	3.40E-06	
Beryllium	7440-41-7	1.20E-05	0.0004	4.66E-08	2.04E-07	
Cadmium	7440-43-9	1.10E-03	0.0374	4.27E-06	1.87E-05	
Chromium	7440-47-3	1.40E-03	0.0476	5.44E-06	2.38E-05	
Cobalt	7440-48-4	8.40E-05	0.0029	3.26E-07	1.43E-06	
Manganese	7439-96-5	3.80E-04	0.0129	1.48E-06	6.46E-06	
Mercury	7439-97-6	2.60E-04	0.0088	1.01E-06	4.42E-06	
Nickel	7440-02-0	2.10E-03	0.0714	8.16E-06	3.57E-05	
Selenium	7782-49-2	2.40E-05	0.0008	9.32E-08	4.08E-07	
		Total:	64.23	0.0073	0.0321	

Mountaineer Keystone - Tony's Bridge Wellpad Heater Emission Summary (TE-1) Criteria Pollutants (See Attachment M)

Fuel Usage										
Fuel	Units	Total								
Natural Gas	ft ³	255,500								

Emission Factors ¹								
	Thermoelectric Generator ²							
Pollutant	Natural Gas (lbs/ 10 ⁶ ft ³)							
Particulates	7.60							
Sulfur Dioxide	0.6000							
Oxides of Nitrogen	100.00							
PM-10	7.60							
VOC	5.50							
Carbon Monoxide	84.00							
Lead	0.0005							
CO2 Equiv	120,000							

Emissions										
	Thermoelectric Generator ²									
Pollutant	Natural Gas (Ibs/yr)	Natural Gas (lbs/hr)	Natural Gas (tons/yr)							
Particulates	1.94	0.0002	0.0010							
Sulfur Dioxide	0.1533	1.75E-05	7.67E-05							
Oxides of Nitrogen	25.55	0.0029	0.0128							
PM-10	1.94	0.0002	0.0010							
VOC	1.41	0.0002	0.0007							
Carbon Monoxide	21.46	0.0025	0.0107							
Lead	0.0001	1.46E-08	6.39E-08							
CO2 Equiv	30,660	3.50	15.33							

Emissions are calculated as follows:

Natural Gas Usage (ft³) = 700 (scfd) * 365 (days/yr) Emissions (lbs/yr) = Volume of Gas (ft³) * Emission Factor (lbs/10⁶ ft³)

¹ Natural Gas Emission Factors were taken from AP-42 Tables 1.4-1 and 1.4-2

Notes:

 2 The wellpad operates 1 thermoelectric generator, which has a maximum natural gas throughput of 700 scfd. It is assumed boiler emission factors accurately estimate emissions

Mountaineer Keystone - Tony's Bridge Wellpad Heater Emission Summary (TE-1) HAPS (See Attachment M)

Emissions are calculated as follows:

Emissions = Volume of Gas (ft^3) * Emission Factor ($lbs/10^6 ft^3$) ¹ Emission Factors from AP-42 Tables 1.4-3 and 1.4-4

Natural Gas
Heaters
HAP
ft ³
255,500

		Natural Gas						
	HAP Emissions	Heaters						
			(lbs/yr)	(lbs/hr)	(tons/yr)			
НАР	CAS No.	Natural Gas ¹ (lb/10 ⁶ ft ³)						
2-Methylnaphthalene	91-57-6	2.40E-05	6.13E-06	7.00E-10	3.07E-09			
3-Methylchloranthrene	56-49-5	1.80E-06	4.60E-07	5.25E-11	2.30E-10			
7,12-Dimethylbenz(a)anthracene	-	1.60E-05	4.09E-06	4.67E-10	2.04E-09			
Acenaphthene	83-32-9	1.80E-06	4.60E-07	5.25E-11	2.30E-10			
Acenaphthylene	203-96-8	1.80E-06	4.60E-07	5.25E-11	2.30E-10			
Anthracene	120-12-7	2.40E-06	6.13E-07	7.00E-11	3.07E-10			
Benz(a)anthracene	56-55-3	1.80E-06	4.60E-07	5.25E-11	2.30E-10			
Benzene	71-43-2	2.10E-03	0.0005	6.13E-08	2.68E-07			
Benzo(a)pyrene	50-32-8	1.20E-06	3.07E-07	3.50E-11	1.53E-10			
Benzo(b)fluoranthene	205-99-2	1.80E-06	4.60E-07	5.25E-11	2.30E-10			
Benzo(g,h,i)perylene	191-24-2	1.20E-06	3.07E-07	3.50E-11	1.53E-10			
Benzo(k)fluoranthene	207-08-9	1.80E-06	4.60E-07	5.25E-11	2.30E-10			
Chrysene	218-01-9	1.80E-06	4.60E-07	5.25E-11	2.30E-10			
Dibenzo(a,h)anthracene	53-70-3	1.20E-06	3.07E-07	3.50E-11	1.53E-10			
Dichlorobenzene	25321-22-6	1.20E-03	0.0003	3.50E-08	1.53E-07			
Fluoranthene	206-44-0	3.00E-06	7.67E-07	8.75E-11	3.83E-10			
Fluorene	86-73-7	2.80E-06	7.15E-07	8.17E-11	3.58E-10			
Formaldehyde	50-00-0	7.50E-02	0.0192	2.19E-06	9.58E-06			
Hexane	110-54-3	1.80E+00	0.4599	5.25E-05	0.0002			
Indeno(1,2,3-cd)pyrene	193-39-5	1.80E-06	4.60E-07	5.25E-11	2.30E-10			
Naphthalene	91-20-3	6.10E-04	0.0002	1.78E-08	7.79E-08			
Phenanathrene	85-01-8	1.70E-05	4.34E-06	4.96E-10	2.17E-09			
Pyrene	129-00-0	5.00E-06	1.28E-06	1.46E-10	6.39E-10			
Toluene	108-88-3	3.40E-03	0.0009	9.92E-08	4.34E-07			
Arsenic	7440-38-2	2.00E-04	5.11E-05	5.83E-09	2.56E-08			
Beryllium	7440-41-7	1.20E-05	3.07E-06	3.50E-10	1.53E-09			
Cadmium	7440-43-9	1.10E-03	0.0003	3.21E-08	1.41E-07			
Chromium	7440-47-3	1.40E-03	0.0004	4.08E-08	1.79E-07			
Cobalt	7440-48-4	8.40E-05	2.15E-05	2.45E-09	1.07E-08			
Manganese	7439-96-5	3.80E-04	9.71E-05	1.11E-08	4.85E-08			
Mercury	7439-97-6	2.60E-04	6.64E-05	7.58E-09	3.32E-08			
Nickel	7440-02-0	2.10E-03	0.0005	6.13E-08	2.68E-07			
Selenium	7782-49-2	2.40E-05	6.13E-06	7.00E-10	3.07E-09			
		Total:	0.4824	5.51E-05	0.0002			



Standard Features

- Automatic Spark Ignition (SI)
- Automatic Fuel Shut-off (SO)
- Fuel Filter
- Low Voltage Alarm Contacts (VSR)
- Volt & Amp Meter

Optional Features

- Cathodic Protection Interface
- Pole Mount or bench stand
- Corrosive Environmental Fuel System
- Marine Service
- Certification to CSA Std. T.I.L. R-10

Note: Specifications shown are for standard configurations. Gentherm Global Power Technologies' * (GPT) Integrated Systems Engineering Department is available to design custom voltages, fuel supply systems and non-standard operating temperatures.

Specification data stated in this document is subject to change without notice. To verify these specifications are current, contact your Gentherm Global Power Technologies (GPT) sales representative.

* Formerly Global Thermoelectric



ISO 9001 Registered

Model 5220 Thermoelectric Generators

Gentherm Global Power Technologies' * (GPT) 5220 Thermoelectric Generator contains no moving parts. It is a reliable, low maintenance source of DC electrical power for any application where regular utilities are unavailable or unreliable.

Power Specifications

Power Rating at 20°C 195 Watts at 12 Volts 178 Watts at 24 Volts

Electrical

Adjustment: 12 V 12 -18 Volts 24 V 24 - 30 Volts

Reverse current protection included.

Output: Terminal block which accepts up to 8 AWG wire. Opening for 3/4" conduit in the base of the cabinet.

Fuel

Natural Gas:

19.7 m³/day (700 Sft³/day) 1000 BTU/Sft³ (37.7 MJ/SM³) gas max 115 mg/Sm³ (~170 ppm) H₂S max 120 mg/Sm³ H₂Omax 1% free O2 28.0 l/day (7.4 US gal/day) 345 kPa (50 psi)

Propane:

Max. Supply Pressure: Min. Supply Pressure: Fuel Connection:

165 kPa (24 psi) 1/4" MNPT

Environmental

Ambient Operation Temperature: Max. +45°C (115°F) Min. -40°C (-40°F). Operating Conditions: Unsheltered operation Please contact GPT for operating conditions below -40°C or above +45°C.

Materials of Construction

Cabinet: Cooling Type: Fuel System:

304 SS Natural Convection Brass, Aluminum & SS



Power where you need it.®

Tanker Truck Loading Calculations

Mountaineer Keystone – Tonys Bridge Tanker Truck Loading Emissions, LO-1 (See Attachment O)

Assumptions:

- All VOC, Methane, and GHG that enter the tank are emitted during loading
- Lbs/tons of VOC, Methane, and GHG emissions are used from the tank emission calculations

$$0.5929 \frac{lbs VOC}{hr}$$

$$0.0617 \frac{tons VOC}{yr}$$

$$6.73 \frac{lbs Methane}{hr}$$

$$0.6998 \frac{tons Methane}{yr}$$

$$336.45 \frac{lbs GHG}{hr}$$

$$34.99 \frac{tons GHG}{yr}$$

ATTACHMENT U – FACILITY-WIDE CONTROLLED EMISSIONS SUMMARY SHEET																
List all sources	s of emi	ssions i	in this t	able. U	Jse extra	ı pages i	if neces	sary.								
Emission Drint ID#	NO) _x	С	0	VOC		SO_2		PM_{10}		PM _{2.5}		CH_4		GHG (CO ₂ e)	
Emission Point ID#	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
1E (HTR-1)	0.0971	0.0323	0.0816	0.3575	0.0054	0.0234	0.0006	0.0026	0.0073	0.0323	0.0073	0.0323	0	0	116.51	510.25
2E (HTR-2)	0.0971	0.0323	0.0816	0.3575	0.0054	0.0234	0.0006	0.0026	0.0073	0.0323	0.0073	0.0323	0	0	116.51	510.25
3E (HTR-3)	0.0971	0.0323	0.0816	0.3575	0.0054	0.0234	0.0006	0.0026	0.0073	0.0323	0.0073	0.0323	0	0	116.51	510.25
4E (HTR-4)	0.0971	0.0323	0.0816	0.3575	0.0054	0.0234	0.0006	0.0026	0.0073	0.0323	0.0073	0.0323	0	0	116.51	510.25
5E (TNK-1)	NA	NA	NA	NA	0.2975	0.0771	NA	NA	NA	NA	NA	NA	3.37	0.8750	168.23	43.74
6E (TNK-2)	NA	NA	NA	NA	0.2975	0.0771	NA	NA	NA	NA	NA	NA	3.37	0.8750	168.23	43.74
7E (TNK-3)	NA	NA	NA	NA	0.2975	0.0771	NA	NA	NA	NA	NA	NA	3.37	0.8750	168.23	43.74
8E (TNK-4)	NA	NA	NA	NA	0.2975	0.0771	NA	NA	NA	NA	NA	NA	3.37	0.8750	168.23	43.74
LO-1	NA	NA	NA	NA	<0.5929	<0.0617	NA	NA	NA	NA	NA	NA	<6.73	<0.6998	<336.45	<34.99
9E (TE-1)	0.0029	0.0128	0.0025	0.0107	0.0002	0.0007	1.75E-5	7.67E-5	0.0002	0.0010	0.0002	0.0010	0	0	3.50	15.33
TOTAL	0.3913	0.1420	0.3289	1.44	1.80	0.4644	0.0024	0.0105	0.0294	0.1302	0.0294	0.1302	20.21	4.20	1,479	2,266

Annual emissions shall be based on 8,760 hours per year of operation for all emission units except emergency generators. According to 45CSR14 Section 2.43.e, fugitive emissions are not included in the major source determination because it is not listed as one of the source categories in Table 1. Therefore, fugitive emissions shall not be included in the PTE above.

ATTACHMENT U – FACILITY-WIDE HAP CONTROLLED EMISSIONS SUMMARY SHEET														
List all sources of e	emissions	in this t	able. U	se extra	pages if	necessar	у.							
E	Formaldehyde		Benzene		Toluene		Ethylbenzene		Xylenes		Hexane		Total HAPs	
Emission Point ID#	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
1E (HTR-1)	7.50E-05	0.00038	2.04E-06	8.93E-06	3.30E-06	1.45E-05	NA	NA	NA	NA	0.0017	0.0077	0.0018	0.008
2E (HTR-2)	7.50E-05	0.00038	2.04E-06	8.93E-06	3.30E-06	1.45E-05	NA	NA	NA	NA	0.0017	0.0077	0.0018	0.008
3E (HTR-3)	7.50E-05	0.00038	2.04E-06	8.93E-06	3.30E-06	1.45E-05	NA	NA	NA	NA	0.0017	0.0077	0.0018	0.008
4E (HTR-4)	7.50E-05	0.00038	2.04E-06	8.93E-06	3.30E-06	1.45E-05	NA	NA	NA	NA	0.0017	0.0077	0.0018	0.008
5E (TNK-1)	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
6E (TNK-2)	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
7E (TNK-3)	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
8E (TNK-4)	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA
LO-1	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	De minimis	De minimis
9E (TE-1)	2.19E-6	9.58E-6	6.13E-8	2.68E-7	9.92E-8	4.34E-7	NA	NA	NA	NA	5.25E-5	0.0002	5.51E-5	0.0002
TOTAL	3.02E-4	1.53E-3	8.22E-6	3.60E-5	1.33E-5	5.84E-5	NA	NA	NA	NA	6.85E-3	0.0310	7.26E-3	0.0322

Annual emissions shall be based on 8,760 hours per year of operation for all emission units except emergency generators. According to 45CSR14 Section 2.43.e, fugitive emissions are not included in the major source determination because it is not listed as one of the source categories in Table 1. Therefore, fugitive emissions shall not be included in the PTE above.

ATTACHMENT V – CLASS I LEGAL ADVERTISEMENT

Publication of a proper Class I legal advertisement is a requirement of the G70-D registration process. In the event the applicant's legal advertisement fails to follow the requirements of 45CSR13, Section 8 or the requirements of Chapter 59, Article 3, of the West Virginia Code, the application will be considered incomplete and no further review of the application will occur until this is corrected.

The applicant, utilizing the format for the Class I legal advertisement example provided on the following page, shall have the legal advertisement appear a minimum of one (1) day in the newspaper most commonly read in the area where the facility exists or will be constructed. The notice must be published no earlier than five (5) working days of receipt by this office of your application. The original affidavit of publication must be received by this office no later than the last day of the public comment period.

The advertisement shall contain, at a minimum, the name of the applicant, the type and location of the source, the type and amount of air pollutants that will be discharged (excluding fugitive emissions), the nature of the permit being sought, the proposed start-up date for the source, and a contact telephone number for more information.

The location of the source should be as specific as possible starting with: 1.) the street address of the source; 2.) the nearest street or road; 3.) the nearest town or unincorporated area, 4.) the county, and 5.) latitude and longitude coordinates in decimal format.

Types and amounts of pollutants discharged **must include** all regulated pollutants (Nitrogen Oxides, Carbon Monoxide, Particulate Matter-2.5, Particulate Matter-10, Volatile Organic Compounds, Sulfur Dioxide, Carbon Dioxide Equivalents, Methane, Formaldehyde, Benzene, Toluene, Ethylbenzene, Xylenes, Hexane, Total Hazardous Air Pollutants and their potential to emit or the permit level being sought in units of tons per year.

In the event the 30th day is a Saturday, Sunday, or legal holiday, the comment period will be extended until 5:00 p.m. on the following regularly scheduled business day.

A list of qualified newspapers that are eligible to publish legal ads may be found:

http://www.sos.wv.gov/elections/resource/Documents/Qualified%20Newspapers.pdf

RECOMMENDED PUBLIC NOTICE TEMPLATE

AIR QUALITY PERMIT NOTICE Notice of Application

Notice is given that Mountaineer Keystone LLC has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a G70-D (General Permit Registration Application) for a natural gas production facility located on 4000 County Route 25, Mount Claire in Harrison County, West Virginia. The latitude and longitude coordinates are: 39.38585 and -80.35668

The applicant estimates the potential to discharge the following Regulated Air Pollutants will be:

- 0.1420 tons per year NOx;
- 1.44 tons per year CO;
- 0.4644 tons per year VOCs;
- 0.0105 tons per year SO2;
- 0.1302 tons per year PM-10; and
- 0.0322 tons per HAPs.

Startup of operation is planned to begin on or about March 1, 2017. Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1250, during normal business hours. Dated this 30<u>th</u> day of January, 2017.

By: Mountaineer Keystone LLC Meghan M.B. Yingling Environmental Compliance Manager 65 Professional Place, Suite 200 Bridgeport, WV 26330