625 Liberty Ave, Suite 1700 Pittsburgh PA 15222 www.eqt.com

TEL: (412) 395-3699 FAX: (412) 395-2156

Alex Bosiljevac Environmental Coordinator



June 28, 2016

CERTIFIED MAIL # 7015 1660 0000 9399 6451

Mr. Joe Kessler, Engineer WVDEP – Division of Air Quality 601 57th Street, SE Charleston, WV 25304

Re: R13 Permit Modification EQT Gathering LLC – Janus Compressor Station Doddridge County, WV

Dear Mr. Kessler:

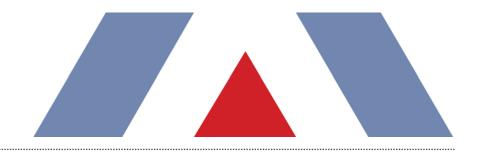
Enclosed are two electronic copies and one original hard copy of a proposed modification to the Janus Station. A legal advertisement will be published in the next few days and proof of publication will be forwarded as soon as it is received. The changes to this application are outlined in the introduction.

If you have any questions concerning this permit application, please contact me at (412) 395-3699 or by email at abosiljevac@eqt.com.

Sincerely,

R. Alex Bosiljevac EQT Corporation

Enclosures



CLASS II ADMINISTRATIVE UPDATE APPLICATION EQT Gathering, LLC > Janus Compressor Station

Doddridge County, West Virginia

Prepared By:

TRINITY CONSULTANTS 4500 Brooktree Rd. Suite 103 Wexford, PA 15090 (724) 935-2611

June 2016



Environmental solutions delivered uncommonly well

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EQT Gathering, LLC (EQT) is submitting this Class II Administrative update application to the West Virginia Department of Environmental Protection (WVDEP) for the natural gas compressor station located in Doddridge County, West Virginia (Janus Compressor Station). Specifically, this application seeks to designate the existing tank enclosed flare (FLARE-003) as an optional control during upset and emergency conditions and updated vented emissions from the facility. The Janus Station is currently permitted under R13 permit number R13-3269

1.1. FACILITY AND PROJECT DESCRIPTION

The Janus Compressor Station is a natural gas gathering facility covered under Standard Industrial Classification (SIC) code 1311. The facility will have the potential to operate 24 hours per day, and 7 days per week.

The station is currently permitted for the following equipment

- > Four (4) lean burn natural gas fired compressor engines (each rated at 5,350 horsepower [hp]) equipped with oxidation catalyst,
- > Two (2) triethylene glycol (TEG) dehydration units (each rated at 125 million standard cubic feet per day [MMscfd])), with associated reboilers (rated at 2.31 MMBtu/hr heat input) and controlled by enclosed flares (each rated at 7.0 MMbtu/hr),
- > Five (5) microturbine generator (each rated 200 kW),
- > Two (2) fuel gas heaters (rated at 1.15 MMbtu/hr and 0.77 MMbtu/hr),
- > Two (2) produced fluid tanks (210 bbl each) controlled by a tank enclosed flare (rated at 41 MMbtu/hr), and
- > Twenty two (22) miscellaneous storage tanks

EQT is submitting this application to in order to address the following:

- > Update the facility wide fugitive emission calculations, station volume venting, and pigging emissions calculations. This includes updating the information included in Condition 4.1.12.c;
- > Revise the description for the enclosed flare (FLARE-003) to "pressure-assisted;" and
- Designate the enclosed flare (FLARE-003) associated with the two (2) produced fluids (T-001 to T-002) as an optional control in the current permit. Specifically, EQT will use the enclosed flare for safety purposes when the produced liquids tanks receive condensate. As a result, EQT is requesting that the Department remove the following conditions from the current permit:
 - Condition 4.1.8.c
 - Conditions 4.1.11 and 4.2.7.

A description of each source category is included below. A process flow diagram is included as Attachment F

1.2. R-13 APPLICATION ORGANIZATION

This R-13 permit application is organized as follows:

- > Section 2: Sample Emission Source Calculations;
- > Section 3: R-13 Application Forms;
- > Attachment A: Business Certificate;
- > Attachment B: Map;
- > Attachment C: Installation and Start Up Schedule;
- > Attachment D: Regulatory Discussion;
- > Attachment E: Plot Plan;
- > Attachment F: Detailed Process Flow Diagram;
- > Attachment G: Process Description;
- > Attachment I: Emission Units Table;
- > Attachment J: Emission Points Data Summary Sheet;
- > Attachment K: Fugitive Emissions Data Summary Sheet;
- > Attachment L: Emissions Unit Data Sheets;
- > Attachment M: Air Pollution Control Device Sheet;
- > Attachment N: Supporting Emission Calculations;
- > Attachment O: Monitoring/Recordkeeping/Reporting/Testing Plans;
- > Attachment P: Public Notice; and
- > Application Fee

The characteristics of air emissions from the Janus Compressor Station, along with the methodology used for calculating emissions from the proposed new sources, are described in narrative form below. Detailed supporting calculations are also provided in Attachment N.

Emissions from the proposed project at Janus Compressor Station will result from the flashing, working, and breathing losses from the storage tanks and fugitive emissions from component leaks will result from the operation of the station. The methodologies employed in calculating emissions from these sources have been summarized below, with specific citations included in Attachment N.

- Storage Tanks: Working, standing, and flash loss emissions of VOC and HAPs from the produced fluids storage tanks are calculated using E&P Tank v2.0. Liquid loading emissions are calculated using EPA AP-42 emission factors.
- Fugitive Emissions: Emissions from fugitive equipment leaks are calculated using published EPA emission factors and 40 CFR Part 98, Subpart W emission factors. Emissions from blowdown events are calculated using engineering estimates of the amount of gas vented during each event. Site specific gas analyses were used to speciate VOC, HAP, and GHG emissions.
- Compressor Engines: Potential emissions of nitrogen oxides (NO_X), CO, VOC, formaldehyde are calculated using factors provided by the engine and catalyst manufacturer. Potential emissions of sulfur dioxide (SO2), particulate matter (PM/PM10/PM2.5), and all other hazardous air pollutants (HAPs) are calculated using U.S. EPA's AP-42 factors for four stroke lean burn engines. Uncontrolled acrolein emission factor is based on San Diego Air Pollution Control District emissions testing factors¹ and assuming 1020 Btu/scf. The controlled emission factors in the reference were taken from units equipped with oxidation catalysts. For conservatism, EQT has calculated emissions assuming uncontrolled emissions (i.e., assuming a 99% control efficiency and back-calculating an uncontrolled emission rate). A sample calculation is included below:

Uncontrolled Emission Factor
$$\left(\frac{lb}{MMBtu}\right) = \frac{Controlled Emission Factor \left(\frac{lb}{MMscf}\right)}{Btu Content \left(\frac{MMBtu}{MMscf}\right) x (1 - Assumed Control Efficiency)}$$
$$= \frac{0.01 \left(\frac{lb}{MMscf}\right)}{1020 \left(\frac{MMBtu}{MMscf}\right) x (1 - 99\%)}$$
$$= 9.80E - 04 \frac{lb}{MMBtu}$$

Potential emissions of greenhouse gas pollutants (GHGs) are calculated using manufacturer's data as available (CO₂ and CH₄ in this case) and U.S. EPA's emission factors from 40 CFR Part 98, Subpart C for all others.

¹ http://www.sdapcd.org/content/dam/sdc/apcd/PDF/Misc/EFT/Gas_Combustion/APCD_Engine_Natural_Gas_Fired_4_Stroke_Lean_Burn_with_Catalytic_Oxidation.pdf EQT Gathering, LLC | Janus Compressor Station

The WVDEP permit application forms contained in this application include all applicable R13 application forms including the required attachments.

WFST VIRGINIA DEPARTMENT OF ENVIRONMENTAL PROTECTION DIVISION OF AIR QUALITY 601 57 th Street, SE Charleston, WV 25304 (304) 926-0475 WWW.dep.wv.gov/dag	APPLICATION FOR NSR PERMIT AND TITLE V PERMIT REVISION (OPTIONAL)
PLEASE CHECK ALL THAT APPLY TO NSR (45CSR13) (IF KNO CONSTRUCTION MODIFICATION RELOCATION CLASS I ADMINISTRATIVE UPDATE TEMPORARY CLASS II ADMINISTRATIVE UPDATE AFTER-THE-FA	
	Revision Guidance" in order to determine your Title V Revision options ability to operate with the changes requested in this Permit Application.
Sect	tion I. General
1. Name of applicant (as registered with the WV Secretary EQT Gathering, LLC	<i>ry of State's Office):</i> 2. Federal Employer ID No. <i>(FEIN):</i> 20-2752042
 Name of facility (if different from above): Janus Station 	4. The applicant is the:
5A. Applicant's mailing address: 625 Liberty Avenue, Suite 1700 Pittsburgh, PA 15222	5B. Facility's present physical address: Off Left Fork Run Road Doddridge County, WV
change amendments or other Business Registration C	ation/Organization/Limited Partnership (one page) including any name Certificate as Attachment A. /Authority of L.L.C./Registration (one page) including any name change
7. If applicant is a subsidiary corporation, please provide the	the name of parent corporation: EQT Corporation
 8. Does the applicant own, lease, have an option to buy or If YES, please explain: Applicant owns site If NO, you are not eligible for a permit for this source. 	
 Type of plant or facility (stationary source) to be const administratively updated or temporarily permitted (crusher, etc.): Natural Gas Compressor Station 	
11A. DAQ Plant ID No. (for existing facilities only): 1 017 – 00158	11B. List all current 45CSR13 and 45CSR30 (Title V) permit numbers associated with this process (for existing facilities only): R13-3269
All of the required forms and additional information can be for	found under the Permitting Section of DAQ's website, or requested by phone.

12A.		
 For Modifications, Administrative Updates or Te present location of the facility from the nearest state 		please provide directions to the
 For Construction or Relocation permits, please provide road. Include a MAP as Attachment B. 	provide directions to the <i>proposed new</i> s	site location from the nearest state
Turn south off of RT 50 at MM 50.5 onto Arnolds C Turn right in 0.9 miles onto station road and procee		
12.B. New site address (if applicable):	12C. Nearest city or town:	12D. County:
Arrnold's Creek Road	West Union	Doddridge
12.E. UTM Northing (KM): 4,345.400	12F. UTM Easting (KM): 516.767	12G. UTM Zone: 17
13. Briefly describe the proposed change(s) at the facilit	iy:	
EQT is proposing to update the current permit limits on t make the current Vapor Destruction Unit (VDU) an option	he storage vessels and vented emissior	ns. Specifically, EQT would like to
 14A. Provide the date of anticipated installation or change If this is an After-The-Fact permit application, providence did happen: 	•	14B. Date of anticipated Start-Up if a permit is granted: ASAP
14C. Provide a Schedule of the planned Installation of/ application as Attachment C (if more than one uni		units proposed in this permit
15. Provide maximum projected Operating Schedule o Hours Per Day 24 Days Per Week 7	f activity/activities outlined in this applica Weeks Per Year 52	ation:
16. Is demolition or physical renovation at an existing fa	cility involved? 🗌 YES 🛛 🛛 NO	
17. Risk Management Plans. If this facility is subject to	112(r) of the 1990 CAAA, or will becom	ne subject due to proposed
changes (for applicability help see www.epa.gov/cepp	oo), submit your Risk Management Pla	n (RMP) to U. S. EPA Region III.
18. Regulatory Discussion. List all Federal and State a	air pollution control regulations that you	believe are applicable to the
proposed process (if known). A list of possible application	able requirements is also included in Att	achment S of this application
(Title V Permit Revision Information). Discuss applica	bility and proposed demonstration(s) of	compliance (if known). Provide this
information as Attachment D.		
Section II. Additional att	achments and supporting d	ocuments.
19. Include a check payable to WVDEP – Division of Air	Quality with the appropriate application	n fee (per 45CSR22 and
45CSR13).		
20. Include a Table of Contents as the first page of you	ur application package.	
 Provide a Plot Plan, e.g. scaled map(s) and/or sket source(s) is or is to be located as Attachment E (Register of the second seco		erty on which the stationary
 Indicate the location of the nearest occupied structure 	e (e.g. church, school, business, residen	ice).
22. Provide a Detailed Process Flow Diagram(s) show device as Attachment F.	ving each proposed or modified emissio	ns unit, emission point and control
23. Provide a Process Description as Attachment G.		
 Also describe and quantify to the extent possible 		
All of the required forms and additional information can be	found under the Permitting Section of DA	AQ's website, or requested by phone.

24. Provide Material Safety Data Shee	ets (MSDS) for all materials proce	essed, used or produced as Attachment H.									
- For chemical processes, provide a M	ISDS for each compound emitted	to the air.									
25. Fill out the Emission Units Table a	and provide it as Attachment I.										
26. Fill out the Emission Points Data	Summary Sheet (Table 1 and Ta	able 2) and provide it as Attachment J.									
27. Fill out the Fugitive Emissions Da	ta Summary Sheet and provide	t as Attachment K.									
28. Check all applicable Emissions Un	it Data Sheets listed below:										
Bulk Liquid Transfer Operations	Haul Road Emissions	Quarry									
Chemical Processes Hot Mix Asphalt Plant Solid Materials Sizing, Handling and Storage											
Concrete Batch Plant	Incinerator	Facilities									
Grey Iron and Steel Foundry	Indirect Heat Exchanger	🛛 Storage Tanks									
General Emission Unit, specify											
Fill out and provide the Emissions Unit	Data Sheet(s) as Attachment L	•									
29. Check all applicable Air Pollution	Control Device Sheets listed bel	ow:									
Absorption Systems	Baghouse	🛛 Flare – Tank Enclosed flare									
Adsorption Systems	Condenser	Mechanical Collector									
	Electrostatic Precipit	ator Uvet Collecting System									
Other Collectors, specify											
Fill out and provide the Air Pollution Co	ontrol Device Sheet(s) as Attac	nment M.									
30. Provide all Supporting Emissions Items 28 through 31.	Calculations as Attachment N,	or attach the calculations directly to the forms listed in									
	e compliance with the proposed	h proposed monitoring, recordkeeping, reporting and emissions limits and operating parameters in this permit									
	nay not be able to accept all meas	ther or not the applicant chooses to propose such sures proposed by the applicant. If none of these plans ude them in the permit.									
32. Public Notice. At the time that the	application is submitted, place a	Class I Legal Advertisement in a newspaper of general									
circulation in the area where the so	urce is or will be located (See 450	CSR§13-8.3 through 45CSR§13-8.5 and <i>Example Legal</i>									
Advertisement for details). Please	e submit the Affidavit of Publicat	ion as Attachment P immediately upon receipt.									
33. Business Confidentiality Claims.	Does this application include con	nfidential information (per 45CSR31)?									
🗌 YES	⊠ NO										
segment claimed confidential, inclu- Notice – Claims of Confidentiality	ding the criteria under 45CSR§31 y" guidance found in the Genera										
S	Section III. Certification	of Information									
34. Authority/Delegation of Authority Check applicable Authority Form		other than the responsible official signs the application.									
Authority of Corporation or Other Bus	siness Entity	Authority of Partnership									
Authority of Governmental Agency	C] Authority of Limited Partnership									
Submit completed and signed Authority	y Form as Attachment R.										
		Permitting Section of DAQ's website, or requested by phone.									

35A. Certification of Information. To certify this permit application, a Responsible Official (per 45CSR§13-2.22 and 45CSR§30-2.28) or Authorized Representative shall check the appropriate box and sign below.

Certification of Truth, Accuracy, and Completeness

I, the undersigned Responsible Official / Authorized Representative, hereby certify that all information contained in this application and any supporting documents appended hereto, is true, accurate, and complete based on information and belief after reasonable inquiry I further agree to assume responsibility for the construction, modification and/or relocation and operation of the stationary source described herein in accordance with this application and any amendments thereto, as well as the Department of Environmental Protection, Division of Air Quality permit issued in accordance with this application, along with all applicable rules and regulations of the West Virginia Division of Air Quality and W.Va. Code § 22-5-1 et seq. (State Air Pollution Control Act). If the business or agency changes its Responsible Official or Authorized Representative, the Director of the Division of Air Quality will be notified in writing within 30 days of the official change.

Compliance Certification

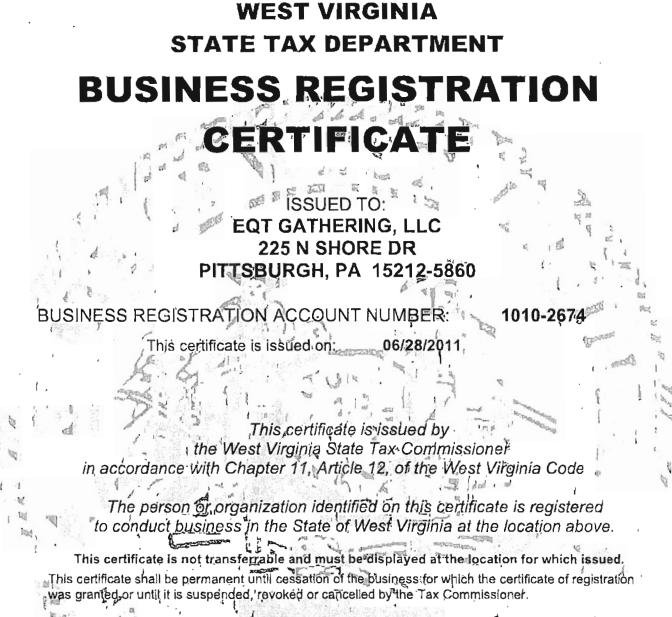
Except for requirements identified in the Title V Application for which compliance is not achieved, I, the undersigned hereby certify that, based on information and belief formed after reasonable inquiry, all air contaminant sources identified in this application are in compliance with all applicable requirements.

SIGNATURE	use blue ink)	DATE: <u>627/16</u> (Please use blue ink) 35C. Title: Sr. Vice President
35D. E-mail: <u>dcharletta@eqt.com</u>	36E. Phone:	36F. FAX:
36A. Printed name of contact person (if differe	nt from above): Alex Bosiljevac	36B Title: Environmental Coordinator
36C. E-mail: <u>abosiljevac@eqt.com</u>	36D. Phone: 412-395-3699	36E. FAX: 412-395-7027

PLEASE CHECK ALL APPLICABLE ATTACHMENTS INCLUDE	D WITH THIS PERMIT APPLICATION:
 Attachment A: Business Certificate Attachment B: Map(s) Attachment C: Installation and Start Up Schedule Attachment D: Regulatory Discussion Attachment E: Plot Plan Attachment F: Detailed Process Flow Diagram(s) Attachment G: Process Description Attachment H: Material Safety Data Sheets (MSDS) Attachment I: Emission Units Table Attachment J: Emission Points Data Summary Sheet 	 Attachment K: Fugitive Emissions Data Summary Sheet Attachment L: Emissions Unit Data Sheet(s) Attachment M: Air Pollution Control Device Sheet(s) Attachment N: Supporting Emissions Calculations Attachment O: Monitoring/Recordkeeping/Reporting/Testing Plans Attachment P: Public Notice Attachment Q: Business Confidential Claims Attachment R: Authority Forms Attachment S: Title V Permit Revision Information Application Fee
	permit application with the signature(s) to the DAQ, Permitting Section, at the s application. Please DO NOT fax permit applications.
FOR AGENCY USE ONLY – IF THIS IS A TITLE V SOURCE:	
Forward 1 copy of the application to the Title V Permitting	g Group and:
For Title V Administrative Amendments:	
NSR permit writer should notify Title V permit writ	er of aran permit,
For Title V Minor Modifications:	
	ication to EPA and affected states within 5 days of receipt,
NSR permit writer should notify Title V permit write	-
□ For Title V Significant Modifications processed in parallel	
NSR permit writer should notify a Title V permit wr	•
Public notice should reference both 45CSR13 and	Title V permits,
EPA has 45 day review period of a draft permit.	
All of the required forms and additional information can be for	ound under the Permitting Section of DAQ's website, or requested by phone.

ATTACHMENT A

Current Business Certificate



Change in name or change of location shall be considered a cessation of the business and a new certificate shall be required.

all wit

TRAVELING/STREET VENDORS: Must carry a copy of this certificate in every vehicle operated by them. CONTRACTORS, DRILLING OPERATORS, TIMBER/LOGGING OPERATIONS: Must have a copy of this certificate displayed at every job site within West Virginia.

atL006 v.4 L2077129856

ATTACHMENT B

Мар

Figure 1 - Map of Janus Station



UTM Northing (KM): 4,345.000 UTM Easting (KM): 516.767 Elevation: 900 ft

ATTACHMENT C

Startup and Installation Schedule

ATTACHMENT C

Schedule of Planned Installation and Start-Up

The proposed changes will be implemented upon issuance of the revised permit. No installation is required by the proposed changes.

ATTACHMENT D

Regulatory Discussion

ATTACHMENT D - REGULATORY APPLICABILITY

This section documents the applicability determinations made for Federal and State air quality regulations. The monitoring, recordkeeping, reporting, and testing plan is presented in Attachment O. In this section, applicability or non-applicability of the following regulatory programs is addressed:

- > Prevention of Significant Deterioration (PSD) permitting;
- > Title V of the 1990 Clean Air Act Amendments;
- > New Source Performance Standards (NSPS);
- > National Emission Standards for Hazardous Air Pollutants (NESHAP); and
- > West Virginia State Implementation Plan (SIP) regulations.

This review is presented to supplement and/or add clarification to the information provided in the WVDEP R13 permit application forms. In addition to providing a summary of applicable requirements, this section of the application also provides non-applicability determinations for certain regulations, allowing the WVDEP to confirm that identified regulations are not applicable to the Janus Compressor Station. Note that explanations of non-applicability are limited to those regulations for which there may be some question of applicability specific to the operations at the Janus Compressor Station. Regulations that are categorically non-applicable are not discussed (e.g., NSPS Subpart J, Standards of Performance for Petroleum Refineries).

Prevention of Significant Deterioration (PSD) Source Classification

Federal construction permitting programs regulate new and modified sources of attainment pollutants under Prevention of Significant Deterioration (PSD) and new and modified sources of non-attainment pollutants under Non-Attainment New Source Review (NNSR). PSD and NNSR regulations apply when a major source makes a change, such as installing new equipment or modifying existing equipment, and a significant increase in emissions results from the change. The Janus Compressor Station will remain a minor source with respect to the NSR program after the project since its potential emissions are below all the NNSR/PSD thresholds. As such, NNSR/PSD permitting is not triggered by this construction activity. EQT will monitor future construction activities at the site closely and will compare any future increase in emissions with the NSR/PSD thresholds to ensure these activities will not trigger this program.

Title V Operating Permit Program

Title 40 of the Code of Federal Regulations Part 70 (40 CFR 70) establishes the federal Title V operating permit program. West Virginia has incorporated the provisions of this federal program in its Title V operating permit program in West Virginia Code of State Regulations (CSR) 45-30. The major source thresholds with respect to the West Virginia Title V operating permit program regulations are 10 tons per year (tpy) of a single HAP, 25 tpy of any combination of HAP, and 100 tpy of all other regulated pollutants. Potential emissions of NO_X exceed 100 tpy. Therefore, the Janus Compressor Station will be continue to be a major source with respect to the Title V permit program and as such is required to submit a Title V operating permit application. EQT will submit the Title V operating permit application within one year of start-up of the facility.

New Source Performance Standards

New Source Performance Standards (NSPS), located in 40 CFR 60, require new, modified, or reconstructed sources to control emissions to the level achievable by the best demonstrated technology as specified in the applicable provisions. Moreover, any source subject to an NSPS is also subject to the general provisions of NSPS Subpart A, except where expressly noted. The following is a summary of applicability and non-applicability determinations for NSPS regulations of relevance to the proposed project at the Janus Compressor Station.

NSPS Subparts K, Ka, and Kb

These subparts apply to storage tanks of certain sizes constructed, reconstructed, or modified during various time periods. Subpart K applies to storage tanks constructed, reconstructed, or modified prior to 1978, and Subpart Ka applies to those constructed, reconstructed, or modified prior to 1984. Both Subparts K and Ka apply to storage tanks with a capacity greater than 40,000 gallons. Subpart Kb applies to volatile organic liquid (VOL) storage tanks constructed, reconstructed, or modified after July 23, 1984 with a capacity equal to or greater than 75 m3 (~19,813 gallons). The storage tanks at the Janus Compressor Station have a capacity of 19,000 gallons or less. As such, Subparts K, Ka, and Kb do not apply to the storage tanks at the Janus Compressor Station.

NSPS Subpart OOOO—Crude Oil and Natural Gas Production, Transmission, and Distribution

Subpart 0000, Standards of Performance for Crude Oil and Natural Gas Production, Transmission, and Distribution, applies to affected facilities that commenced construction, reconstruction, or modification after August 23, 2011 (see clarification below regarding dates). This NSPS was published in the Federal Register on August 16, 2012, and subsequently amended. Although there are sources proposed to be installed that could potentially be subject to this regulation, due to the anticipated installation dates, some will not be subject to the rule. This is due to the most recent proposed developments related to the rule, which are the inclusion of an end date for applicability to Subpart 00000 (September 18, 2015) and the promulgation of 40 CFR 60 Subpart 0000a.

For this project, EQT is proposing to remove the enclosed combustor as the primary control for the two (2) produced storage tanks at the Janus Station. However, since VOC emissions are less than 6 tpy, these tanks will not be storage vessel affected facilities under this rule.

NSPS Subpart OOOOa-Crude Oil and Natural Gas Facilities

Subpart OOOOa, Standards of Standards of Performance for Crude Oil and Natural Gas Facilities, will apply to affected facilities that commenced construction, reconstruction, or modification after September 18, 2015. This regulation has yet to be finalized. The currently proposed version of the rule includes provisions for the following facilities:

- > Hydraulically fractured wells;
- Centrifugal compressors located between the wellhead and the point of custody transfer to the natural gas distribution segment;
- > Reciprocating compressors located between the wellhead and the point of custody transfer to the natural gas distribution segment;
- Continuous bleed natural gas-driven pneumatic controllers with a bleed rate of > 6 scfh located in the production, gathering, processing, or transmission and storage segments (excluding natural gas processing plants);
- > Continuous bleed natural gas-driven pneumatic controllers located at natural gas processing plants;
- > Pneumatic pumps located in the production, gathering, processing, or transmission and storage segments;
- > Storage vessels located in the production, gathering, processing, or transmission and storage segments;
- > The collection of fugitive emissions components at a well site;
- > The collection of fugitive emissions components at a compressor station; and
- > Sweetening units located onshore that process natural gas produced from either onshore or offshore wells.

Based on the current version of the proposed rule, the following paragraphs describe the potential applicability related to the proposed changes at the facility.

There are two (2) produced fluid storage vessels at the Janus Station. The storage tanks will be installed after the applicability date of Subpart 0000a, and could therefore be potentially subject to the rule. The storage vessels at the facility each have potential VOC emissions less than 6 tpy based on the permit application materials and as such, per 60.5365a(e), the tanks will not be storage vessel affected facilities under the rule.

Non-Applicability of All Other NSPS

NSPS are developed for particular industrial source categories. Other than NSPS developed for natural gas operations (Subpart 0000/0000a), and associated equipment (Subparts D-Dc, KKKK, and K-Kb), the applicability of a particular NSPS to the Janus Compressor Station can be readily ascertained based on the industrial source category covered. All other NSPS are categorically not applicable to natural gas compressor stations.

National Emission Standards for Hazardous Air Pollutants (NESHAP)

Part 63 NESHAP allowable emission limits are established on the basis of a maximum achievable control technology (MACT) determination for a particular major source. A HAP major source is defined as having potential emissions in excess of 25 tpy for total HAP and/or potential emissions in excess of 10 tpy for any individual HAP. Note that Subpart HH has specific major source applicability criteria (i.e., excluding engine emissions from the major source determination). The Janus Compressor Station will be an Area (minor) source of HAP since its potential emissions of HAP are less than the 10/25 major source thresholds. The proposed project does not include any emission unit that is subject to NESHAP regulations. Therefore this part does not apply.

West Virginia SIP Regulations

The Janus Compressor Station is potentially subject to regulations contained in the West Virginia Code of State Regulations, Chapter 45 (Code of State Regulations). The Code of State Regulations fall under two main categories, those regulations that are generally applicable (e.g., permitting requirements), and those that have specific applicability (e.g., PM standards for manufacturing equipment).

45 CSR 4: To Prevent and Control the Discharge of Air Pollutants into the Air Which Causes or Contributes to an Objectionable Odor

According to 45 CSR 4-3:

No person shall cause, suffer, allow or permit the discharge of air pollutants which cause or contribute to an objectionable odor at any location occupied by the public.

The Janus Compressor Station is generally subject to this requirement. However, due to the nature of the process at the station, production of objectionable odor from the compressor station during normal operation is unlikely.

45 CSR 6: Control of Air Pollution from the Combustion of Refuse

45 CSR 6 applies to activities involving incineration of refuse, defined as "the destruction of combustible refuse by burning in a furnace designed for that purpose. For the purposes of this rule, the destruction of any combustible liquid or gaseous material by burning in a flare or flare stack, thermal oxidizer or thermal catalytic oxidizer stack shall be considered incineration." The tank enclosed flare is an incinerators and therefore must comply with this regulation. Per 45 CSR 6-4.3, opacity of emissions from this unit shall not exceed 20 percent, except as provided by 4.4. PM emissions from this unit will not exceed the levels calculated in accordance with 6-4.1

45 CSR 16: Standards of Performance for New Stationary Sources

45 CSR 16-1 incorporates the federal Clean Air Act (CAA) standards of performance for new stationary sources set forth in 40 CPR Part 60 by reference. As such, by complying with all applicable requirements of 40 CFR Part 60 at the Janus Compressor Station (discussed earlier in this attachment), EQT will be complying with 45 CSR 16.

45 CSR 17: To Prevent and Control Particulate Matter Air Pollution from Materials Handling, Preparation, Storage and Other Sources of Fugitive Particulate Matter

According to 45 CSR 17-3.1:

No person shall cause, suffer, allow or permit fugitive particulate matter to be discharged beyond the boundary lines of the property lines of the property on which the discharge originates or at any public or residential location, which causes or contributes to statutory air pollution.

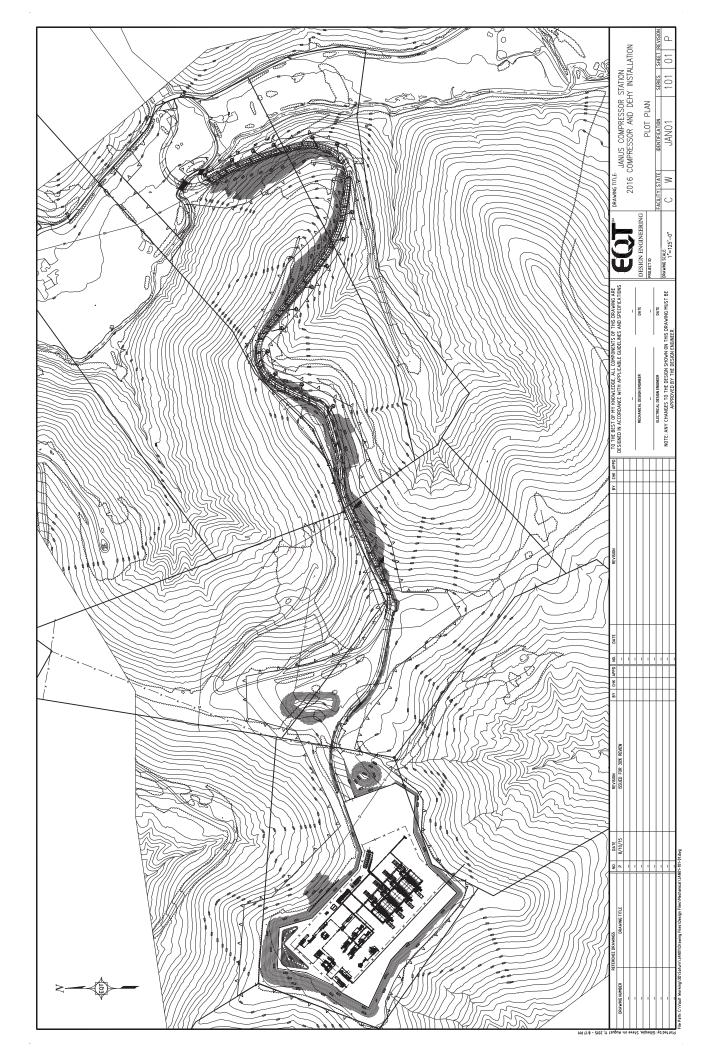
Due to the nature of the activities at the Janus Station it is unlikely that fugitive particulate matter emissions will be emitted under normal operating conditions. However, EQT will take measures to ensure any fugitive particulate matter emissions will not cross the property boundary should any such emissions occur.

45 CSR 21-28: Petroleum Liquid Storage in Fixed Roof Tanks

45 CSR 21-28 applies to any fixed roof petroleum liquid storage tank with a capacity greater than 40,000 gallons. The capacity of each storage tank proposed for the Janus Compressor Station is less than 40,000 gallons; therefore, 45 CSR 21-28 will not apply.

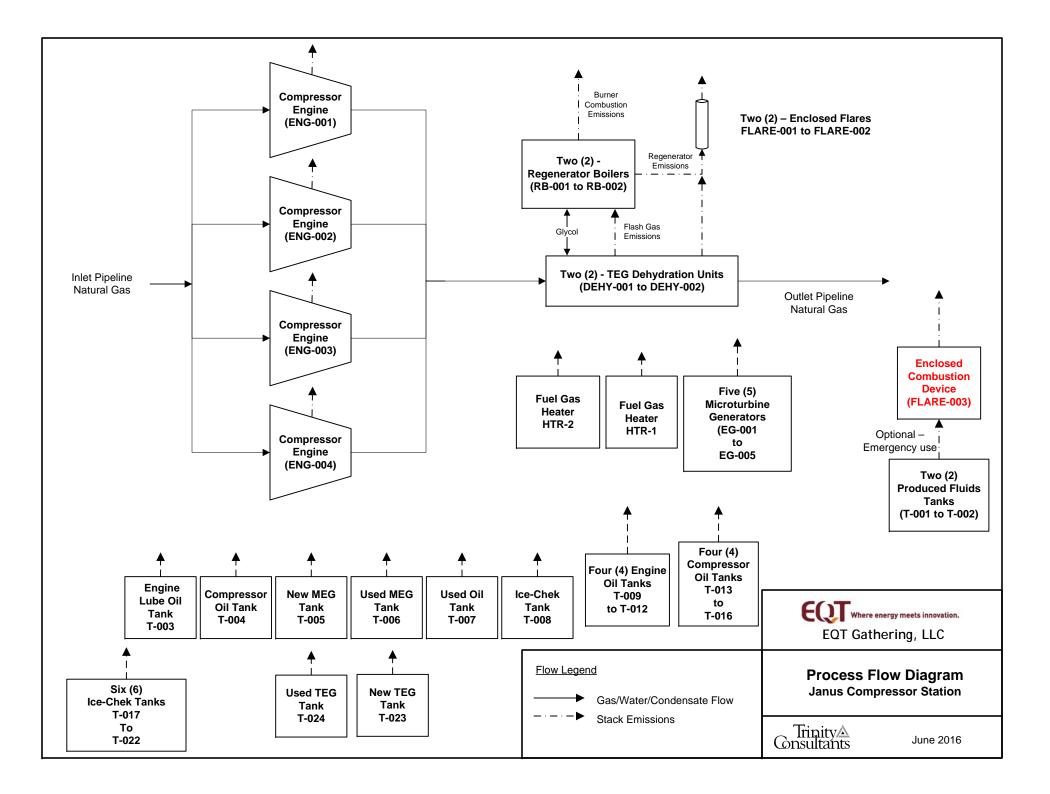
ATTACHMENT E

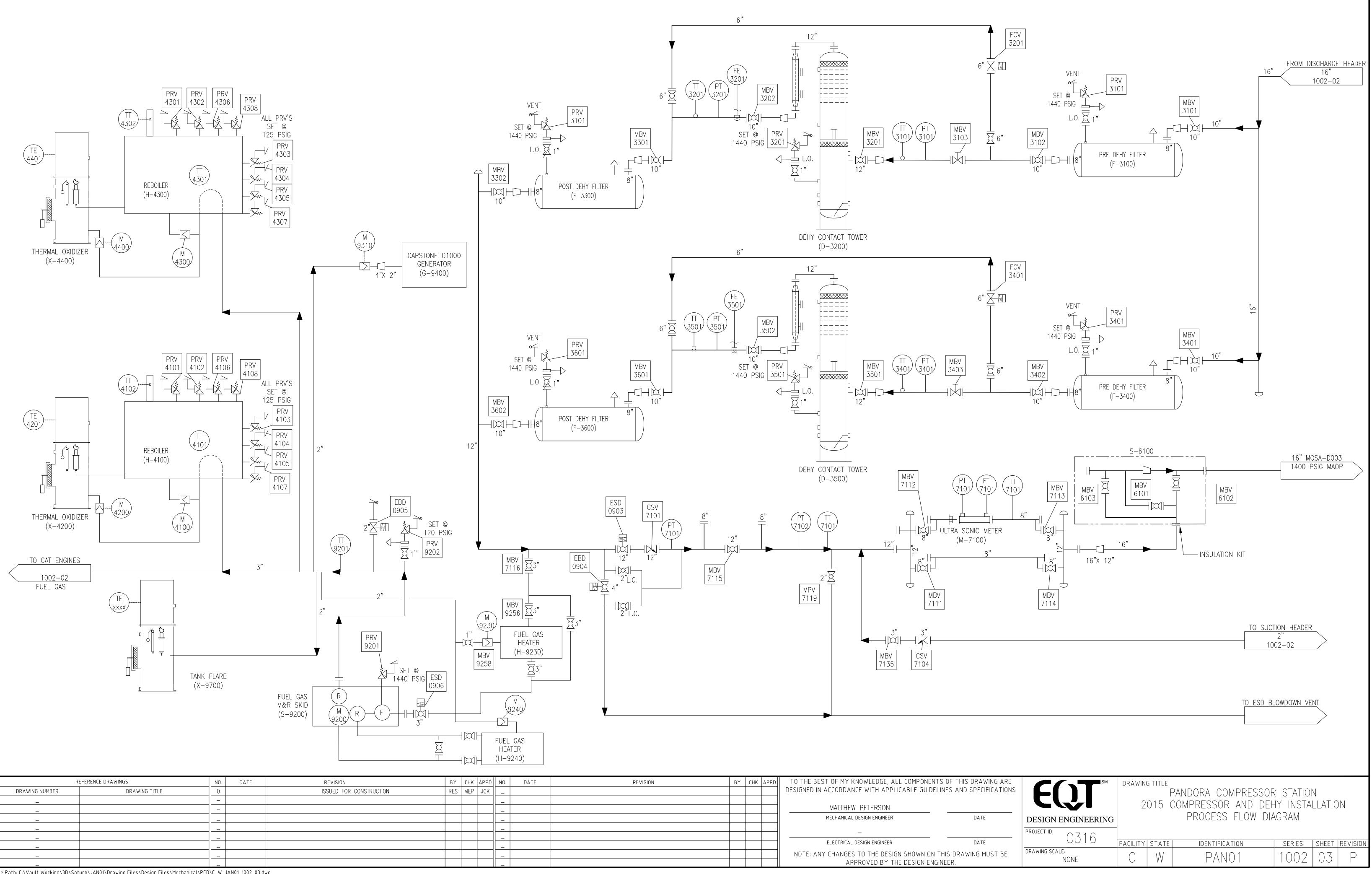
Plot Plan



ATTACHMENT F

Detailed Process Flow Diagram





File Path: C:\Vault Working\3D\Saturn\JAN01\Drawing Files\Design Files\Mechanical\PFD\C-W-JAN01-1002-03.dwg

ATTACHMENT G

Process Description

ATTACHMENT G - PROCESS DESCRIPTION

EQT is submitting this Class II application to update the permit for the Janus Station. Specifically, EQT seeks to designate the existing enclosed flare (FLARE-003) associated with the produced water tanks as an optional control for emergency use. Additionally, this application involves the update of blowdown and station venting emission calculations as well.

Natural gas enters the station via the gathering pipeline system and is compressed using one of the four (4) natural gas-fired compressor engines (identified as ENG-1 to ENG-4, each rated at 5,350 hp). The compressed natural gas stream is then processed through the triethylene glycol (TEG) dehydration units (with associated reboilers). The dehydration units will introduce TEG to the gas stream in a contact tower to absorb water vapor from the gas to a level not exceeding 7 pounds per million standard cubic feet (lb/MMscf). The TEG is then sent to the natural gas-fired reboilers, each rated at 2.3 MMBtu/hr heat input. The water is evaporated from the TEG in the reboiler and discharged, and the glycol is then sent back to the contact tower for reuse. Each dehydration unit is equipped with an enclosed flare which will control emissions from the dehydration still vent and emissions from the flash tank. The natural gas stream from the contact tower flows into the pipeline to be transported further along the pipeline system.

The station is also equipped with two (2) fuel gas heaters, two (2) produced fluids storage tanks, and twenty two (22) miscellaneous storage tanks. Once the tanks are filled, the contents are loaded into trucks for transport. Electricity at the station will be provided by the five (5) Capstone microturbine generators.

A process flow diagram is included as Attachment F.

ATTACHMENT I

Emission Units Table

		Attach	ment I								
Emission Units Table (includes all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status)											
Emission Unit ID ¹	Emission Point ID ²	Emission Unit Description	Year Installed/ Modified	Design Capacity	Type ³ and Date of Change	Control Device ⁴					
ENG-001	ENG-001	Caterpillar G3616 Compressor Engine #1	2016	5,350 HP	Existing	Ox. Cat. (C1)					
ENG-002	ENG-002	Caterpillar G3616 Compressor Engine #2	2016	5,350 HP	Existing	Ox. Cat. (C2)					
ENG-003	ENG-003	Caterpillar G3616 Compressor Engine #3	2016	5,350 HP	Existing	Ox. Cat. (C3)					
ENG-004	ENG-004	Caterpillar G3616 Compressor Engine #4	2016	5,350 HP	Existing	Ox. Cat. (C4)					
DEHY-001	FLARE-001	Dehydration Unit #1	2016	125 MMscfd	Existing	Enclosed Flare (FLARE-001)					
DEHY-002	FLARE-002	Dehydration Unit #2	2016	125 MMscfd	Existing	Enclosed Flare (FLARE-002)					
RB-001	RB-001	Dehydration Unit Reboiler #1	2016	2.31 MMBtu/hr	Existing	N/A					
RB-002	RB-002	Dehydration Unit Reboiler #2	2016	2.31 MMBtu/hr	Existing	N/A					
EG-001	EG-001	Microturbine Generator	2016	200 KW	Existing	N/A					
EG-002	EG-002	Microturbine Generator	2016	200 KW	Existing	N/A					
EG-003	EG-003	Microturbine Generator	2016	200 KW	Existing	N/A					
EG-004	EG-004	Microturbine Generator	2016	200 KW	Existing	N/A					
EG-005	EG-005	Microturbine Generator	2016	200 KW	200 KW Existing						
HTR-1	HTR-1	Fuel Gas Heater	2016	1.15 MMBtu/hr	Existing	N/A					
HTR-2	HTR-2	Fuel Gas Heater	2016	0.77 MMBtu/hr	Existing	N/A					
T-001	Enclosed Flare (FLARE- 003) – Optional	Produced Fluids Tank	2016	8,820 gallons	Modified	Enclosed Flare (FLARE-003) – Optional					
T-002	Enclosed Flare (FLARE- 003) – Optional	Produced Fluids Tank	2016	8,820 gallons	Modified	Enclosed Flare (FLARE-003) – Optional					
T-003	T-003	Engine Lube Oil Tank	2016	2,000 gallons	Existing	N/A					
T-004	T-004	Compressor Oil Tank	2016	2,000 gallons	Existing	N/A					
T-005	T-005	New MEG Tank	2016	2,000 gallons	Existing	N//A					
T-006	T-006	Used MEG Tank	2016	2,000 gallons	Existing	N/A					
T-007	T-007	Used Oil Tank	2016	4,200 gallons	Existing	N/A					
T-008	T-008	Ice-chek Tank	2016	4,000 gallons	Existing	N/A					
T-009	T-009	Engine Oil Tank	2016	300 gallons	Existing	N/A					

T-010	T-010	Engine Oil Tank	2016	300 gallons	Existing	N/A
T-011	T-011	Engine Oil Tank	2016	300 gallons	Existing	N/A
T-012	T-012	Engine Oil Tank	2016	300 gallons	Existing	N/A
T-013	T-013	Compressor Oil Tank	2016	300 gallons	Existing	N/A
T-014	T-014	Compressor Oil Tank	2016	300 gallons	Existing	N/A
T-015	T-015	Compressor Oil Tank	2016	300 gallons	Existing	N/A
T-016	T-016	Compressor Oil Tank	2016	300 gallons	Existing	N/A
T-017	T-017	Ice-chek Tank	2016	550 gallons	Existing	N/A
T-018	T-018	Ice-chek Tank	2016	550 gallons	Existing	N/A
T-019	T-019	Ice-chek Tank	2016	550 gallons	Existing	N/A
T-020	T-020	Ice-chek Tank	2016	550 gallons	Existing	N/A
T-021	T-021	Ice-chek Tank	2016	550 gallons	Existing	N/A
T-022	T-022	Ice-chek Tank	2016	550 gallons	Existing	N/A
T-023	T-023	New TEG Tank	2016	2,000 gallons	Existing	N//A
T-024	T-024	Used TEG Tank	2016	2,000 gallons	Existing	N/A
FLARE-001	FLARE-001	Dehy Enclosed Flare #1	2016	7 MMBtu/hr	Existing	N/A
FLARE-002	FLARE-002	Dehy Enclosed Flare #2	2016	7 MMBtu/hr	Existing	N/A
FLARE-003	FLARE-003	Tank Enclosed Flare #3	2016	41 MMBtu/hr	Existing	N/A
L1	L1	Liquid Loading	2016	210,000 gal/yr	Existing	N/A

¹ For Emission Units (or Sources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.
 ² For Emission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.
 ³ New, modification, removal
 ⁴ For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

ATTACHMENT J

Emission Points Data Summary Sheet

Attachment J EMISSION POINTS DATA SUMMARY SHEET

						Т	able 1:	Emissions Da	ta						
Emission Point ID No. (Must match Emission Units Table	Emission Point Type ¹	t Through This Point		Air Pollution Control Device (Must match Emission Units Table & Plot Plan)		Vent Time for Emission Unit (chemical processes only)		Unit Pollutants - chemical		Pollutants - Potential Chemical Uncontrolled		Maximum Potential Controlled Emissions ⁵		Est. Method Used ⁶	Emission Concentration ⁷ (ppmv or mg/m ⁴)
& Plot Plan)		ID No.	Source	ID No.	Device Type	Short Term ²	Max (hr/yr)	(Speciate VOCs & HAPS)	lb/hr	ton/yr	lb/hr	ton/yr	conditions, Solid, Liquid or Gas/Vapor)		
ENG-001 to ENG-004 (Each unit)	Upward Vertical stack	ENG-001 to ENG-004	Compressor Engine (Each unit)	C-1	Oxidation Catalyst	NA	NA	NOx CO VOC SO2 PM/PM10/PM2.5 HAPs CO2e	5.90 29.13 8.85 0.02 0.003 2.96 5,741	25.83 127.60 38.75 0.10 0.01 12.96 25,144	5.90 2.04 3.93 0.02 0.003 0.84 5,741	25.83 8.93 17.23 0.10 0.01 3.66 25,144	Gas/Vapor	$\begin{array}{c} O^A \\ O^A \\ O^A \\ O^B \\ O^B \\ O^{A,B} \\ O^{A,C} \end{array}$	
FLARE-001 & FLARE-002 (Each unit)	Upward Vertical Stack	DEHY- 001 & DEHY- 002	Dehydration Unit (Each Unit)	FLARE- 001 to FLARE - 002	Enclosed Flares	NA	NA	VOC HAP Benzene	77.61 33.76 4.11	339.92 147.88 18.02	1.55 0.68 0.08	6.80 2.96 0.36	Gas/Vapor	O ^D	
RB-001 & RB-002 (Each unit)	Upward Vertical Stack	RB-001 & RB-002	Reboiler	NA	NA	NA	NA	NOx CO PM/PM10/PM2.5 SO2 VOC CO2e	$\begin{array}{c} 0.19 \\ 0.16 \\ 0.01 \\ < 0.01 \\ 0.01 \\ 271 \end{array}$	$\begin{array}{c} 0.83 \\ 0.69 \\ 0.06 \\ < 0.01 \\ 0.05 \\ 1.185 \end{array}$	0.19 0.16 0.01 <0.01 0.01 271	$\begin{array}{c} 0.83 \\ 0.69 \\ 0.06 \\ < 0.01 \\ 0.05 \\ 1.185 \end{array}$	Gas/Vapor	O^{F} O^{F} O^{F} O^{F} O^{C}	
FLARE-001 & FLARE-002 (Each unit)	Upward Vertical Stack	FLARE- 001 & FLARE- 002	Dehy Enclosed Flares (Each unit)	NA	NA	NA	NA	NOx CO PM/PM10/PM2.5 SO2 CO2e	0.58 0.49 0.04 <0.01 830	2.53 2.13 0.19 0.02 3,637	0.58 0.49 0.04 <0.01 830	2.53 2.13 0.19 0.02 3,637	Gas/Vapor	O^{F} O^{F} O^{F} O^{C}	
FLARE-003 (Optional) Or T-001 & T-002	Upward Vertical Stack	T-001 & T-002 (Each unit)	Produced Fluids Storage Tank	FLARE- 003 (Option)	Enclosed Flares	NA	NA	VOC HAP	0.96 0.02	4.19 0.10	0.96 0.02	4.19 0.10	Gas/Vapor	O ^E	
FLARE-003	Upward Vertical Stack	FLARE- 003	Tank Enclosed Flare	NA	NA	NA	NA	NOx CO PM/PM10 SO2 CO2e	3.35 2.82 0.25 0.02 4,816	14.69 12.34 1.12 0.09 21,095	3.35 2.82 0.25 0.02 4,816	14.69 12.34 1.12 0.09 21,095	Gas/Vapor	O^{F} O^{F} O^{F} O^{C}	
L1	Fugitive	L1	Liquid Loading	NA	NA	NA	NA	VOC	NA	0.09	NA	0.09	Gas/Vapor	O^{H}	

HTR-1	Upward Vertical stack	HTR-1	Fuel Gas Heater	NA	NA	NA	NA	NOx CO VOC SO2 PM/PM10/PM2.5 CO2e	0.09 0.08 0.01 <0.01 0.01 135	0.41 0.35 0.02 <0.01 0.02 590	0.09 0.08 0.01 <0.01 0.01 135	$\begin{array}{c} 0.41 \\ 0.35 \\ 0.02 \\ < 0.01 \\ 0.02 \\ 590 \end{array}$	Gas/Vapor	$O^{\rm F}$ $O^{\rm F}$ $O^{\rm F}$ $O^{\rm C}$	
HTR-2	Upward Vertical stack	HTR-2	Fuel Gas Heater	NA	NA	NA	NA	NOx CO VOC SO2 PM/PM10/PM2.5 CO2e	$\begin{array}{c} 0.06 \\ 0.05 \\ < 0.01 \\ < 0.01 \\ < 0.01 \\ 90 \end{array}$	0.28 0.23 <0.01 <0.01 <0.01 395	0.06 0.05 <0.01 <0.01 <0.01 90	0.28 0.23 <0.01 <0.01 <0.01 395	Gas/Vapor	$O^{\rm F}$ $O^{\rm F}$ $O^{\rm F}$ $O^{\rm C}$	
EG-001 to EG-005 (Combined)	Upward Vertical stack	EG-001 to EG- 005	Microturbine	NA	NA	NA	NA	NOx CO VOC SO2 PM/PM10/PM2.5 HAPs CO2e	$\begin{array}{c} 0.40 \\ 1.10 \\ 0.10 \\ 0.04 \\ 0.08 \\ 0.01 \\ 1,331 \end{array}$	1.75 4.82 0.44 0.17 0.33 0.05 5,831	$\begin{array}{c} 0.40 \\ 1.10 \\ 0.10 \\ 0.04 \\ 0.08 \\ 0.01 \\ 1,331 \end{array}$	1.75 4.82 0.44 0.17 0.33 0.05 5,831	Gas/Vapor	$\begin{array}{c} O^A \\ O^A \\ O^A \\ O^G \\ O^G \\ O^G \\ O^{A,C} \end{array}$	

A- Manufacturer's specific pollutant emission Factor

B- AP-42 Section 3.2, Table 3.2-2 "Uncontrolled Emission Factors for 4-Stroke Lean-Burn Engines" Supplement F, August 2000, except for Formaldehyde which is manufacturer's spec.

C- 40 CFR 98, Subpart C for natural gas fired combustion.

D- GRI-GLYCalc

E- API E&PTanks

F- AP-42 Section 1.4 Tables 1.4-1, 1.4-2 and 1.4-3, July 1998.

G- AP-42 Section 3.1 Table 3.1-2a

H- AP-42 Section 5.2 Table 5.2-1

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit emissions are not typically considered to be fugitive and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugitive emission activities.

¹ Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.

² Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (ie., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).

³ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. **LIST** Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. **DO NOT LIST** H₂, H₂O, N₂, O₂, and Noble Gases.

⁴ Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁵ Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁶ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

⁷ Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmv) are used. If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m³) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO₂, use units of ppmv (See 45CSR10).

Attachment J **EMISSION POINTS DATA SUMMARY SHEET**

	Table 2: Release Parameter Data												
	Inner		Exit Gas		Emission Point El	evation (ft)	UTM Coordinates (km)						
Point ID No. (Must match Emission Units Table)	Diameter (ft.)	Temp. (°F)	Volumetric Flow ¹ Velocity (acfm) <i>at operating conditions</i> (fps)		Ground Level (Height above mean sea level) Stack Height ² (Release height of emissions above ground level)		Northing	Easting					

¹ Give at operating conditions. Include inerts. ² Release height of emissions above ground level.

ATTACHMENT K

Fugitive Emissions Data Summary Sheet

Attachment K

FUGITIVE EMISSIONS DATA SUMMARY SHEET

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not typically considered to be fugitive, and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET.

Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

	APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS
1.)	Will there be haul road activities?
	Yes No (Not associated with this project)
	If YES, then complete the HAUL ROAD EMISSIONS UNIT DATA SHEET.
2.)	Will there be Storage Piles?
	□ Yes
	☐ If YES, complete Table 1 of the NONMETALLIC MINERALS PROCESSING EMISSIONS UNIT DATA SHEET.
3.)	Will there be Liquid Loading/Unloading Operations?
	Yes No (Not associated with this project)
	If YES, complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET.
4.)	Will there be emissions of air pollutants from Wastewater Treatment Evaporation?
	□ Yes
	If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
5.)	Will there be Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, open-ended valves, sampling connections, flanges, agitators, cooling towers, etc.)?
	Yes No
	☑ If YES, complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS UNIT DATA SHEET.
6.)	Will there be General Clean-up VOC Operations?
	□ Yes
	If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
7.)	Will there be any other activities that generate fugitive emissions?
	□ Yes
	If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form.
	bu answered "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions nmary."

FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants ⁻ Chemical Name/CAS ¹	Maximum Potential Uncontrolled Emissions ²		Maximum P Controlled Em	Est. Method	
	Ib/hr		ton/yr	lb/hr	ton/yr	Used ⁴
Haul Road/Road Dust Emissions Paved Haul Roads	NA					
Unpaved Haul Roads	NA					
Storage Pile Emissions	NA					
Loading/Unloading Operations	NA					
Wastewater Treatment Evaporation & Operations	NA					
Equipment Leaks (includes blowdowns and maintenance)	VOC HAP	N/A	30.80 1.69	N/A	30.80 1.69	O ^A
General Clean-up VOC Emissions	NA					
Other	NA					

A – Oil and Gas Production Operations Average Emission Factors, Protocol for Equipment Leak Emission Estimates, EPA 453/R-95-017, Table 2-4, November 1995, 40 CFR 98 Subpart W, and mass balance.

¹ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. DO NOT LIST H₂, H₂O, N₂, O₂, and Noble Gases.

² Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

³ Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁴ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

LEAK-SOURCE DATA SHEET

Source Category	Pollutant	Number of Source Components ¹	Number of Components Monitored by Frequency ²	Average Time to Repair (days) ³	Estimated Annual Emission Rate (Ib/yr) ⁴
Pumps⁵	light liquid VOC ^{6,7}				
	heavy liquid VOC ⁸				
	Non-VOC ⁹				
Valves ¹⁰	Gas VOC	700	0		11,292
	Light Liquid VOC				
	Heavy Liquid VOC				
	Non-VOC				
Safety Relief Valves ¹¹	Gas VOC				
	Non VOC				
Open-ended Lines ¹²	VOC	12	0		86
	Non-VOC				
Sampling Connections ¹³	VOC	650	0		466
	Non-VOC				
Compressors	VOC				
	Non-VOC				
Flanges	VOC	250	0		350
	Non-VOC				
Other	VOC				
	Non-VOC				

¹⁻¹³ See notes on the following page.

Notes for Leak Source Data Sheet

- 1. For VOC sources include components on streams and equipment that contain greater than 10% w/w VOC, including feed streams, reaction/separation facilities, and product/by-product delivery lines. Do not include certain leakless equipment as defined below by category.
- 2. By monitoring frequency, give the number of sources routinely monitored for leaks, using a portable detection device that measures concentration in ppm. Do not include monitoring by visual or soap-bubble leak detection methods. "M/Q(M)/Q/SA/A/O" means the time period between inspections as follows:

Monthly/Quarterly, with Monthly follow-up of repaired leakers/Quarterly/Semi-annual/Annually/Other (specify time period)

If source category is not monitored, a single zero in the space will suffice. For example, if 50 gas-service valves are monitored quarterly, with monthly follow-up of those repaired, 75 are monitored semi-annually, and 50 are checked bimonthly (alternate months), with non checked at any other frequency, you would put in the category "valves, gas service:" 0/50/0/75/0/50 (bimonthly).

- 3. Give the average number of days, after a leak is discovered, that an attempt will be made to repair the leak.
- 4. Note the method used: MB material balance; EE engineering estimate; EPA emission factors established by EPA (cite document used); O other method, such as in-house emission factor (specify).
- 5. Do not include in the equipment count sealless pumps (canned motor or diaphragm) or those with enclosed venting to a control device. (Emissions from vented equipment should be included in the estimates given in the Emission Points Data Sheet.)
- 6. Volatile organic compounds (VOC) means the term as defined in 40 CFR 51.100 (s).
- 7. A light liquid is defined as a fluid with vapor pressure equal to or greater than 0.04 psi (0.3 Kpa) at 20°C. For mixtures, if 20% w/w or more of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20 °C, then the fluid is defined as a light liquid.
- 8. A heavy liquid is defined as a fluid with a vapor pressure less than 0.04 psi (0.3 Kpa) at 20°C. For mixtures, if less than 20% w/w of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20 °C, then the fluid is defined as a heavy liquid.
- 9. LIST CO, H₂S, mineral acids, NO, NO₂, SO₃, etc. DO NOT LIST CO₂, H₂, H₂O, N₂, O₂, and Noble Gases.
- 10. Include all process valves whether in-line or on an open-ended line such as sample, drain and purge valves. Do not include safety-relief valves, or leakless valves such as check, diaphragm, and bellows seal valves.
- 11. Do not include a safety-relief valve if there is a rupture disk in place upstream of the valve, or if the valve vents to a control device.
- 12 Open-ended lines include purge, drain and vent lines. Do not include sampling connections, or lines sealed by plugs, caps, blinds or second valves.
- 13. Do not include closed-purge sampling connections.

ATTACHMENT L

Emission Unit Data Sheet

Attachment L EMISSIONS UNIT DATA SHEET STORAGE TANKS

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <u>www.epa.gov/tnn/tanks.html</u>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<u>http://www.epa.gov/tnn/chief/</u>).

I. GENERAL INFORMATION (required)

1. Bulk Storage Area Name	2. Tank Name			
Janus Compressor Station	Produced Fluids Storage Tanks			
 Tank Equipment Identification No. (as assigned on Equipment List Form) T-001 & T-002 	 Emission Point Identification No. (as assigned on Equipment List Form) FLARE-003 (Optional) 			
5. Date of Commencement of Construction (for existing tanks)				
Type of change 🛛 New Construction 🗌 New Stored Material 🗌 Other Tank Modification				
 Description of Tank Modification (if applicable) Not Applicable 				
7A. Does the tank have more than one mode of operation (e.g. Is there more than one product stored in the tan				
7B. If YES, explain and identify which mode is covered by this application (Note: A separate form must be completed for each mode).				
7C. Provide any limitations on source operation affecting emissions, any work practice standards (e.g. production variation, etc.):				
None				
II. TANK INFORMATION (required)				
 Design Capacity (specify barrels or gallons). Use the internal cross-sectional area multiplied by internal height. 				
T-001 & T-002: 210 bbl (each)				
9A. Tank Internal Diameter (ft)	9B. Tank Internal Height (or Length) (ft)			
~10	~15			
10A. Maximum Liquid Height (ft)	10B. Average Liquid Height (ft)			
~15	~ 10			
11A. Maximum Vapor Space Height (ft)	11B. Average Vapor Space Height (ft)			
~15	~5			
12. Nominal Capacity (specify barrels or gallons). This is also known as "working volume" and considers design liquid levels and overflow valve heights. 210 bbl (each)				

13A. Maximum annual throughput (gal/yr)	13B. Maximum daily throughput (gal/day)			
210,000 (Total)	575 (Total)			
14. Number of Turnovers per year (annual net throughput	t/maximum tank liquid volume)			
24 (Total)				
15. Maximum tank fill rate (gal/min) TBD				
16. Tank fill method Submerged	🛛 Splash 🛛 Bottom Loading			
17. Complete 17A and 17B for Variable Vapor Space Tail	nk Systems Does Not Apply			
17A. Volume Expansion Capacity of System (gal) TBD	17B. Number of transfers into system per year TBD			
	IBD			
 18. Type of tank (check all that apply): □ Fixed Roof <u>x</u> vertical <u>horizontal</u> other (describe) 	flat roofdome roofdome roof			
External Floating Roof pontoon roof	double deck roof			
Domed External (or Covered) Floating Roof				
Internal Floating Roof vertical column su	pport self-supporting			
Variable Vapor Space lifter roof	diaphragm			
Pressurizedsphericalcylindrical				
Underground				
Other (describe)				
III. TANK CONSTRUCTION & OPERATION INFORM	ATION (optional if providing TANKS Summary Sheets)			
19. Tank Shell Construction:				
Riveted Gunite lined Epoxy-coated	d rivets 🛛 Other (describe) Welded			
20A. Shell Color Gray 20B. Roof Colo	r Gray 20C. Year Last Painted			
21. Shell Condition (if metal and unlined):				
🗌 No Rust 🔤 Light Rust 🔤 Dense R	ust 🗌 Not applicable			
22A. Is the tank heated?				
22B. If YES, provide the operating temperature (°F)				
22C. If YES, please describe how heat is provided to t	ank.			
23. Operating Pressure Range (psig): -0.30 to 0.75 psi	g			
24. Complete the following section for Vertical Fixed Ro	of Tanks Does Not Apply			
24A. For dome roof, provide roof radius (ft)				
24B. For cone roof, provide slope (ft/ft) 0.0625				
25. Complete the following section for Floating Roof Tai	nks 🛛 Does Not Apply			
25A. Year Internal Floaters Installed:				
25B. Primary Seal Type: Metallic (Mechanical) (check one) Vapor Mounted Resil	•			
25C. Is the Floating Roof equipped with a Secondary S	Seal? YES NO			
25D. If YES, how is the secondary seal mounted? (che	eck one) Shoe Rim Other (describe):			
25E. Is the Floating Roof equipped with a weather shie	eld? YES NO			

25F. Describe deck fittings; indicate the number of each type of fitting:						
	ACCESS	S НАТСН				
BOLT COVER, GASKETED:	UNBOLTED COVI	ER, GASKETED:	UNBOLTED COVER, UNGASKETED:			
		JGE FLOAT WELL				
BOLT COVER, GASKETED:	UNBOLTED COVI	ER, GASKETED:	UNBOLTED COVER, UNGASKETED:			
	COLUM	N WELL	1			
BUILT-UP COLUMN - SLIDING			PIPE COLUMN – FLEXIBLE			
COVER, GASKETED:	COVER, UNGASH		FABRIC SLEEVE SEAL:			
	•					
PIP COLUMN – SLIDING COVER, G			SLIDING COVER, UNGASKETED:			
FIF COLUMIN – SLIDING COVER, G	ASKETED.		SLIDING COVER, UNGASKETED.			
	GAUGE-HATCH	SAMPLE PORT				
SLIDING COVER, GASKETED:		SLIDING COVER,	UNGASKETED:			
		HANGER WELL				
			SAMPLE WELL-SLIT FABRIC SEAL			
ACTUATION, GASKETED:	ACTUATION, UNC	JASKETED.	(10% OPEN AREA)			
	- - 					
	VACUUM	BREAKER				
WEIGHTED MECHANICAL ACTUAT	ION, GASKETED:	WEIGHTED MECHA	ANICAL ACTUATION, UNGASKETED:			
		·				
		VENT				
WEIGHTED MECHANICAL ACTUAT	ION GASKETED:	WEIGHTED MECHA	ANICAL ACTUATION, UNGASKETED:			
	DECK DRAIN (3-I	INCH DIAMETER)				
OPEN:	22010010101010	90% CLOSED:				
	STUB	DRAIN				
1-INCH DIAMETER:						
UTHER (DESCH	NDE, ATTACH ADL	DITIONAL PAGES I	F NECESSARI)			

26. Complete the following section for Internal	Floating Roof Tanks	🛛 Does Not Apply	ý		
26A. Deck Type: 🗌 Bolted 🗌 We	26A. Deck Type: Bolted Welded				
26B. For Bolted decks, provide deck constru	6B. For Bolted decks, provide deck construction:				
26C. Deck seam:	ida				
 Continuous sheet construction 5 feet with Continuous sheet construction 6 feet with Continuous sheet continuous sheet construction 6 feet with Continuous sheet construction 6 feet with Continuous sheet continuous sheet construction 6 feet with Continuous sheet continuous shee					
Continuous sheet construction 7 feet w	ide				
 Continuous sheet construction 5 x 7.5 f Continuous sheet construction 5 x 12 fe 					
Other (describe)					
26D. Deck seam length (ft)	26E. Ar	ea of deck (ft ²)			
For column supported tanks:		ameter of each column	:		
26F. Number of columns:					
IV. SITE INFORMANTION	(optional if providing	TANKS Summary Shee	ts)		
27. Provide the city and state on which the dat	a in this section are ba	ased.			
Huntington, WV					
28. Daily Average Ambient Temperature (°F)					
29. Annual Average Maximum Temperature (°	F) 65.3				
30. Annual Average Minimum Temperature (°F	-) 45				
31. Average Wind Speed (miles/hr)	6.6				
32. Annual Average Solar Insulation Factor (B	TU/(ft²·day)) 1,1	76			
33. Atmospheric Pressure (psia)	14.	33			
V. LIQUID INFORMATION	(optional if providing	TANKS Summary Shee	ets)		
34. Average daily temperature range of bulk lice	quid: 56.74				
34A. Minimum (°F)	34B. Ma	aximum (°F) 61.79			
35. Average operating pressure range of tank:					
35A. Minimum (psig)	35B. Ma	aximum (psig)			
36A. Minimum Liquid Surface Temperature	(°F) 36B. Co	prresponding Vapor Pre	essure (psia)		
37A. Average Liquid Surface Temperature (°F) 37B. Co	prresponding Vapor Pre	essure (psia)		
56.74					
38A. Maximum Liquid Surface Temperature 61.79	 38A. Maximum Liquid Surface Temperature (°F) 61.79 38B. Corresponding Vapor Pressure (psia) 				
39. Provide the following for each liquid or gas	39. Provide the following for each liquid or gas to be stored in tank. Add additional pages if necessary.				
39A. Material Name or Composition	Produced Fluids				
39B. CAS Number	TBD				
39C. Liquid Density (lb/gal)	TBD				
39D. Liquid Molecular Weight (lb/lb-mole)	TBD				
39E. Vapor Molecular Weight (lb/lb-mole)	36.25				

Maximum Vapor Press 39F. True (psia) 39G. Reid (psia)		TB TB			
Months Storage per Y 39H. From	ear				
391. To					
	VI. EMISSIONS A			E DATA (required)	
40. Emission Control	40. Emission Control Devices (check as many as apply): Does Not Apply				
Carbon Adsorption ¹					
Condenser ¹					
Conservation \	/ent (psig) – Enardo Val	ve			
Vacuum S	Setting 0.30	F	Pressure Se	etting 0.75	
	lief Valve (psig)				
Inert Gas Blan					
Insulation of Ta					
Liquid Absorpt					
Refrigeration o					
Rupture Disc (
Vent to Inciner					
Other ¹ (describ	oriate Air Pollution Conti	ral Davica Sk	aaat		
					P (2)
41. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application).					
-	I		1		dication).
Material Name &	Breathing Loss	Working	J Loss	Annual Loss	Estimation Method ¹
Material Name & CAS No.	I		1		
Material Name & CAS No. See attached	Breathing Loss	Working	J Loss	Annual Loss	
Material Name & CAS No.	Breathing Loss	Working	J Loss	Annual Loss	
Material Name & CAS No. See attached Emissions	Breathing Loss	Working	J Loss	Annual Loss	
Material Name & CAS No. See attached Emissions	Breathing Loss	Working	J Loss	Annual Loss	
Material Name & CAS No. See attached Emissions	Breathing Loss	Working	J Loss	Annual Loss	
Material Name & CAS No. See attached Emissions	Breathing Loss	Working	J Loss	Annual Loss	
Material Name & CAS No. See attached Emissions	Breathing Loss	Working	J Loss	Annual Loss	
Material Name & CAS No. See attached Emissions	Breathing Loss	Working	J Loss	Annual Loss	
Material Name & CAS No. See attached Emissions	Breathing Loss	Working	J Loss	Annual Loss	
Material Name & CAS No. See attached Emissions	Breathing Loss	Working	J Loss	Annual Loss	
Material Name & CAS No. See attached Emissions	Breathing Loss	Working	J Loss	Annual Loss	

 1 EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)

Page 5 of 5

Remember to attach emissions calculations, including TANKS Summary Sheets if applicable.

ATTACHMENT M

Air Pollution Control Device Sheet

Attachment M Air Pollution Control Device Sheet (FLARE SYSTEM)

Control Device ID No. (must match Emission Units Table): FLARE-003

	Equipment	Information
1. Mo	Manufacturer: Envirotherm (or similar) del No. EF-96-30 (or similar)	 Method: Elevated flare Ground flare Other Describe Tank Enclosed Flare
3.	Provide diagram(s) of unit describing capture syste capacity, horsepower of movers. If applicable, state	em with duct arrangement and size of duct, air volume, hood face velocity and hood collection efficiency.
4.	Method of system used:	Pressure-assisted Non-assisted
5.	Maximum capacity of flare: scf/min scf/hr	 Dimensions of stack: Diameter 8 ft. Height 30 ft.
7.	Estimated combustion efficiency: (Waste gas destruction efficiency) Estimated: >95 % Minimum guaranteed: >95 %	 8. Fuel used in burners: Natural Gas Fuel Oil, Number Other, Specify:
9.	Number of burners: One (1) Rating: 41 MMBTU/hr	11. Describe method of controlling flame:
10.	Will preheat be used? Yes No	
12.	Flare height: 30 ft	14. Natural gas flow rate to flare pilot flame per pilot light: scf/min
13.	Flare tip inside diameter: 8 ft	100 scf/hr
15.	Number of pilot lights: One (1) Total 0.12 MMBTU/hr	16. Will automatic re-ignition be used? ⊠ Yes □ No
17.	If automatic re-ignition will be used, describe the met The pilot flare will re-ignite upon pilot failure	hod:
	Ultra Violet Cam	☐ No -Red lera with monitoring control room
19.	Hours of unit operation per year: 8760 (optional)	

Steam Injection				
20. Will steam injection be used? Yes	🛛 No	21. Steam pressure Minimum Expected: Design Maximum:	PSIG	
22. Total Steam flow rate:	LB/hr	23. Temperature:	°F	
24. Velocity	ft/sec	25. Number of jet streams		
26. Diameter of steam jets:	in	27. Design basis for steam injected: LB steam/LB hydrod	carbon	
28. How will steam flow be controlled if steam injection is used?				

Characteristics of the Waste Gas Stream to be Burned

29.	Name	Quantity Grains of H ₂ S/100 ft ³	Quantity (LB/hr, ft ³ /hr, etc)		Source of Material	
	See attached emissions calculations					
30.	Estimate total combustible t		LB/I	hr		
	(Maximum mass flow rate o	of waste gas) 33	38 scfr	n (20,2	280 scfh)	
31.	Estimated total flow rate to	flare including materials to	be burned, carrier gases, a	uxiliary	y fuel, etc.:	
32.	2. Give composition of carrier gases:					
22	Temperature of emission st	room:	34. Identify and describe al	l auxili	ary fuels to be burned.	
55.	>70	°F			BTU/scf	
	Heating value of emission s				BTU/scf	
	1,951				BTU/scf	
	Mean molecular weight of e MW = Ib/Ib-mole	emission stream:			BTU/scf	
					BTU/scf	
35.	Temperature of flare gas:	1800 °F	36. Flare gas flow rate:	625	scf/min (37,500 scfh)	
37.	Flare gas heat content: 1,9	951 BTU/ft ³	38. Flare gas exit velocity:	125	ft/sec	
39.	Maximum rate during emerg	gency for one major piece	of equipment or process un	it:	scf/min	
	Maximum rate during emerg				BTU/min	
41.	Describe any air pollution or reheating, gas humidification	control device inlet and on n):	utlet gas conditioning proce	esses (e.g., gas cooling, gas	
42.	Describe the collection mate	erial disposal system:				
43.	Have you included <i>Flare Control Device</i> in the Emissions Points Data Summary Sheet?					

44. Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.				
MONITORING:		RECORDKEEPING:		
Presence of pil	ot (temperature)	Maintain records of the times and duration of all		
		periods where the pilot flame was absent		
		Maintain records of visible emission opacity tests		
REPORTING:		TESTING:		
None		Conduct a Method 22 opacity test as required		
MONITORING:		ocess parameters and ranges that are proposed to be e compliance with the operation of this process equipment		
RECORDKEEPING: REPORTING:	Please describe the proposed re	cordkeeping that will accompany the monitoring. nissions testing for this process equipment on air pollution		
TESTING:		nissions testing for this process equipment on air pollution		
VOC – 100% HAP – 100%	aranteed Capture Efficiency for ea			
46. Manufacturer's Gua VOC – 95%	aranteed Control Efficiency for eac	ch air pollutant.		
HAP – 95%				
47. Describe all operat	ing ranges and maintenance proce	edures required by Manufacturer to maintain warranty.		



Technical Summary

Design Condition

Process inlet stream:

Bullet Tank Flash GasStream #1

Pipe Size:	4" Sch 40
Inlet Pressure:	0-90 PSIG
Volume Max:	20,280 SCFH
BTU Value	1,951 Btu/Scf
Total Heat input MAX	39.6 MMBTU/HR
Total BTU Load Max	41 MMBTU/hr
Combustion Chamber Temp: High	1800 °F
Limit	
Residence Time:	≥ 1.0 Sec.
Exit Velocity:	29.64 FT/sec.
Destruction Efficiency:	≥ 95%
Turn Down	10 : 1

Utility Flare Sizing:

Pipe Size:
Inlet Pressure:
Volume
BTU Value
Total Heat input
Exit Velocity:
Destruction Efficiency:
Δ P tip
Design Radiation

Site Conditions:

Wind Speed Seismic Zone Elevation Humidity

Utilities:

Gas Service Required for Pilot

Gas Service Required for Assist Fuel Electrical Service Required Compressed Gas for Valves

90 MPH 1 1000 ft. High

≥ 95% .15 PSIG

6" Sch 40 8-12 osi

37,500 SCFH 1600 Btu/Scf 60.0 MMBTU/HR 125 FT/sec.

497 BTU/hr-sq.ft.

100 SCFH – Natural Gas @ 20 PSIG Min. / 150 PSIG Max 8,000 SCFH – Natural Gas @ 20 PSIG Min. (Intermittent Usage) 480 VAC, 3ph, 60Hz, 20 amp 80 PSIG – Intermittent

ATTACHMENT N

Supporting Emission Calculations

EQT Gathering - Janus Station Facility-Wide Emissions Summary

							Janus Station																			
	CAT G3616 Compressor Engines	Capstone Microturbine	Fuel Gas	Heaters	Dehydrator Enclosed Flares	Dehydration Units	Reboilers	Tank Enclosed Flare	Haul Roads	Miscellaneous Storage Tanks	Produced Fluids Storage Tanks	Liquid Loading Operations	Station Fugitives Blowdowns & Component Leaks													
Emission Unit ID	ENG-001 to ENG- 004	EG-001 to EG- 005	HTR-1	HTR-2	DEHY-001 to DEHY-002	DEHY-001 to DEHY-002	RB-001 to RB-002	FLARE-003	NA	T003 to T024	T-001 to T002	L1	NA	Janus	Station											
Emission Point ID	ENG-001 to ENG- 004	EG-001 to EG- 005	HTR-1	HTR-2	FLARE-001 to FLARE-002	FLARE-001 to FLARE-002	RB-001 to RB-002	FLARE-003	NA	NA	FLARE-003	LI	NA	TO												
Equipment Count	4	5	1	1	2	2	2	1	NA	22	2	NA	NA													
Equipment Status	Existing	Existing	Existing	Existing	Existing	Existing	Existing	Existing	Existing	Existing	Existing	Existing	Existing													
Fuel Type	Natural Gas	Natural Gas	Natural Gas	Natural Gas	Natural Gas		Natural Gas	Natural Gas	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA	NA		
Capacity	5,350	1.0	1.15	0.77	7	125	2.31	41	NA	4,200 or less	210	INA	ina.													
Unit Hours per Year	bhp 8,760	MW 8,760	MMBtu/hr 8,760	MMBtu/hr 8,760	MMBtu/hr 8,760	MMSCFD 8,760	MMBtu/hr 8,760	MMBtu/hr 8,760	8,760	gallon 8,760	bbl 8,760	8,760	8,760													
Pollutant	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	tpy	lb/hr	tpy											
PM_{10}	6.90	0.33	0.03	0.02	0.38		0.13	1.12	0.20					2.08	9.11											
PM _{2.5}	6.90	0.33	0.03	0.02	0.38		0.13	1.12	0.01					2.04	8.91											
SO _x	0.41	0.17	< 0.01	< 0.01	0.03		0.01	0.09						0.16	0.71											
СО	35.73	4.82	0.35	0.23	4.25		1.39	12.34						13.49	59.10											
NO _X	103.32	1.75	0.41	0.28	5.07		1.65	14.69						29.03	127.16											
VOC (incl. HCHO)	68.91	0.44	0.02	0.02		13.60	0.09			0.00	8.37	0.09	30.80	27.93	122.34											
CO_2	89,682	5,825	589	395	7,267	7,295	2,368	21073					0.47	30706.42	134494.11											
CH_4	433.94	0.11	0.01	0.01	0.14	6.32	0.04	0.40					72.91	117.33	513.88											
N_2O	0.15	0.01	< 0.01	< 0.01	0.01		0.00	0.04						0.05	0.22											
CO ₂ e	100,576	5,831	590	395	7,274	7,453	2,370	21095					1,823	33654.72	147407.68											
Formaldehyde	4.13	0.04	< 0.01	< 0.01			< 0.01							0.95	4.17											
Total HAPs (including HCHO)	14.66	0.05	0.01	0.01		5.92	0.03				0.20		1.69	5.15	22.56											

1. VOC and HAP emissions are included in the storage tank emissions

Compressor Engines (Per Engine)

Manufacturer:	Caterpillar
Model No.:	3616
Stroke Cycle:	4-stroke
Type of Burn:	Lean Burn
Year Installed/Date Manufactured	TBD
Fuel Used:	Natural Gas
Fuel High Heating Value (HHV) (Btu/scf):	1,226
Rated Horsepower (bhp):	5,350
Specific Fuel Consumption (Btu/bhp-hr)	7,338
Maximum Fuel Consumption at 100% Load (scf/hr):	32,160
Heat Input (MMBtu/hr)	39.43
Control Device:	Oxidation Catalyst
Operational Details:	
Potential Annual Hours of Operation (hr/yr):	8,760
Potential Fuel Consumption (MMscf/yr):	281.7

Criteria and Manufacturer Specific Pollutant Emission Factors:

Pollutant	Emission Factors ¹	Units	Estimation Basis / Emission Factor Source
NOx	0.50	g/bhp-hr	CAT GERP Vendor Spec Sheet
СО	0.17	g/bhp-hr	Catalyst Vendor Spec Sheet
SO ₂	5.88E-04	lb/MMBtu	AP-42, Table 3.2-2 (Jul-2000)
PM ₁₀ (Filterable)	7.71E-05	lb/MMBtu	AP-42, Table 3.2-2 (Jul-2000)
PM _{2.5} (Filterable)	7.71E-05	lb/MMBtu	AP-42, Table 3.2-2 (Jul-2000)
PM Condensable	9.91E-03	lb/MMBtu	AP-42, Table 3.2-2 (Jul-2000)
PM Total	9.99E-03	lb/MMBtu	AP-42, Table 3.2-2 (Jul-2000)
NMNEHC	0.31	g/bhp-hr	Catalyst Vendor Spec Sheet
VOC (Includes HCHO)	0.33	g/bhp-hr	Catalyst Vendor Spec Sheet
Formaldehyde (HCHO)	0.02	g/bhp-hr	Catalyst Vendor Spec Sheet
CO ₂	434.0	g/bhp-hr	CAT GERP Vendor Spec Sheet
CH ₄	2.10	g/bhp-hr	Vendor Spec Sheet (=THC-NMHC)
N ₂ O	1.00E-04	kg/MMBtu	40 CFR 98, Table C-2

Criteria and Manufacturer Specific Pollutant Emission Rates:

	Potential Emissions						
Pollutant	$(lb/hr)^2$	(tons/yr) ³					
NO _x	5.90	25.83					
СО	2.04	8.93					
SO ₂	0.02	0.10					
PM ₁₀ (Filterable)	0.003	0.01					
PM _{2.5} (Filterable)	0.003	0.01					
PM Condensable	0.39	1.71					
PM Total	0.39	1.73					
NMNEHC	3.70	16.20					
VOC (incl HCHO)	3.93	17.23					
Formaldehyde (HCHO)	0.24	1.03					
CO_2	5,119	22,420					
CH ₄	24.77	108.49					
N ₂ O	0.01	0.04					

Compressor Engines (Per Engine)

Hazardous Air Pollutant (HAP) Potential Emissions:

	Emission Factor	Potential	Emissions
Pollutant	(lb/MMBtu) ¹	(lb/hr) ²	(tons/yr) ³
HAPs:			
Acenaphthene	1.25E-06	4.93E-05	2.16E-04
Acenaphthylene	5.53E-06	2.18E-04	9.55E-04
Acetaldehyde	8.36E-03	3.30E-01	1.44E+00
Acrolein	9.80E-04	3.87E-02	1.69E-01
Benzene	4.40E-04	1.74E-02	7.60E-02
Benzo(b)fluoranthene	1.66E-07	6.55E-06	2.87E-05
Benzo(e)pyrene	4.15E-07	1.64E-05	7.17E-05
Benzo(g,h,i)perlyene	4.14E-07	1.63E-05	7.15E-05
Biphenyl	2.12E-04	8.36E-03	3.66E-02
1,3-Butadiene	2.67E-04	1.05E-02	4.61E-02
Carbon Tetrachloride	3.67E-05	1.45E-03	6.34E-03
Chlorobenzene	3.04E-05	1.20E-03	5.25E-03
Chloroform	2.85E-05	1.12E-03	4.92E-03
Chrysene	6.93E-07	2.73E-05	1.20E-04
1,3-Dichloropropene	2.64E-05	1.04E-03	4.56E-03
Ethylbenzene	3.97E-05	1.57E-03	6.86E-03
Ethylene Dibromide	4.43E-05	1.75E-03	7.65E-03
Fluoranthene	1.11E-06	4.38E-05	1.92E-04
Fluorene	5.67E-06	2.24E-04	9.79E-04
Methanol	2.50E-03	9.86E-02	4.32E-01
Methylene Chloride	2.00E-05	7.89E-04	3.45E-03
n-Hexane	1.11E-03	4.38E-02	1.92E-01
Phenanthrene	1.04E-05	4.10E-04	1.80E-03
Phenol	2.40E-05	9.46E-04	4.15E-03
Pyrene	1.36E-06	5.36E-05	2.35E-04
Styrene	2.36E-05	9.31E-04	4.08E-03
Toluene	4.08E-04	1.61E-02	7.05E-02
1,1,2,2-Tetrachloroethane	4.00E-05	1.58E-03	6.91E-03
Tetrachloroethane	2.48E-06	9.78E-05	4.28E-04
1,1,2-Trichloroethane	3.18E-05	1.25E-03	5.49E-03
2,2,4-Trimethylpentane	2.50E-04	9.86E-03	4.32E-02
Vinyl Chloride	1.49E-05	5.88E-04	2.57E-03
Xylene	1.84E-04	7.26E-03	3.18E-02
Polycyclic Organic Matter:			
Naphthalene	7.44E-05	2.93E-03	1.29E-02
2-Methylnaphthalene	3.32E-05	1.31E-03	5.73E-03
РАН	2.69E-05	1.06E-03	4.65E-03
Total HAP		0.84	3.66

Notes:
1. SO₂, PM, and HAP emission factors from AP-42 Section 3.2, Table 3.2-2 "Uncontrolled Emission Factors for 4-Stroke Lean-Burn Engines," Supplement F, August 2000. Uncontrolled acrolein emission factor is based on SDAPCD emissions testing factors (assuming controlled values as tested are reduced by 99%) and assuming 1020 Btu/scf $(http://www.sdapcd.org/content/dam/sdc/apcd/PDF/Misc/EFT/Gas_Combustion/APCD_Engine_Natural_Gas_Fired_4_Stroke_Lean_Burn_with_Catalytic_Oxidation.pdf). \ NO_X, and an analytic_Oxidation.pdf$ VOC, CO, CO₂, and CH₄ (=THC-NMHC) and formaldehyde emission factors are based on manufacturer's data. Greenhouse gas emission factors (N₂O) are based on 40 CFR Part 98, Subpart C, Table C-2 for natural gas combustion.

2. Emission Rate (lb/hr) = Rated Capacity (MMBtu/hr or bhp) \times Emission Factor (lb/MMBtu or gr/bhp-hr).

3. Annual Emissions $(tons/yr)_{Potential} = (lb/hr)_{Emissions} \times (Maximum Allowable Operating Hours, 8,760 hr/yr) \times (1 ton/2000 lb).$

Storage Tank Emissions												
Tank Description	Tank Contents	Tank ID Number	Number of Tanks	Tank Capacity (gal)	Tank Diameter (ft)	Tank Length (ft)	Turnovers Per Year	Annual Throughput (gal)	VOC Emissions Per Tank (lb/yr)	Total VOC Emissions (tpy)	HAP Emissions Per Tank (lb/yr)	Total HAP Emissions (tpy)
Produced Fluids Tank	Produced Water	T-001	1	8,820	10	15.0	12	105,000	8,374.56	4.186	201.48	0.10
Produced Fluids Tank	Produced Water	T-002	1	8,820	10	15.0	12	105,000	8,374.56	4.186	201.48	0.10
Engine Lube Oil Tank	Engine Lube Oil	T-003	1	2,000	5.33	12.0	2	4,200	0.65	0.000	< 0.01	< 0.01
Compressor Lube Oil Tank	Compressor Oil	T-004	1	2,000	5.33	12.0	4	7,266	0.70	3.50E-04	< 0.01	< 0.01
New MEG Tank	New MEG	T-005	1	2,000	5.33	12.0	1	1,050	0.04	2.00E-05	< 0.01	< 0.01
Used MEG Tank	Used MEG	T-006	1	2,000	5.33	12.0	1	1,050	0.04	2.00E-05	< 0.01	< 0.01
Used Oil Tank	Used Oil	T-007	1	4,200	5.33	25.1	1	4,200	1.27	6.35E-04	< 0.01	< 0.01
Ice-chek Tank	Ice-chek	T-008	1	3,998	5.33	23.9	5	21.000	0.11	5.50E-05	< 0.01	< 0.01
Engine Lube Oil Tank	Engine Oil	T-009	1	302	3.2	5.1	3	1.050	0.11	5.50E-05	< 0.01	< 0.01
Engine Lube Oil Tank	Engine Oil	T-010	1	302	3.2	5.1	3	1.050	0.11	5.50E-05	< 0.01	< 0.01
Engine Lube Oil Tank	Engine Oil	T-011	1	302	3.2	5.1	3	1.050	0.11	5.50E-05	< 0.01	< 0.01
Engine Lube Oil Tank	Engine Oil	T-012	1	302	3.2	5.1	3	1.050	0.11	5.50E-05	< 0.01	< 0.01
Compressor Lube Oil Tank	Compressor Oil	T-013	1	302	3.2	5.1	6	1,806	0.11	5.50E-05	< 0.01	< 0.01
Compressor Lube Oil Tank	Compressor Oil	T-014	1	302	3.2	5.1	6	1.806	0.11	5.50E-05	< 0.01	< 0.01
Compressor Lube Oil Tank	Compressor Oil	T-015	1	302	3.2	5.1	6	1.806	0.11	5.50E-05	< 0.01	< 0.01
Compressor Lube Oil Tank	Compressor Oil	T-016	1	302	3.2	5.1	6	1.806	0.11	5.50E-05	< 0.01	< 0.01
Ice-chek Tank	Ice-chek	T-017	1	550	4.2	5.4	6	3,486	0.02	1.00E-05	< 0.01	< 0.01
Ice-chek Tank	Ice-chek	T-018	1	550	4.2	5.4	6	3,486	0.02	1.00E-05	< 0.01	< 0.01
Ice-chek Tank	Ice-chek	T-019	1	550	4.2	5.4	6	3,486	0.20	1.0E-04	< 0.01	< 0.01
Ice-chek Tank	Ice-chek	T-020	1	550	4.2	5.4	6	3,486	0.06	3.0E-05	< 0.01	< 0.01
Ice-chek Tank	Ice-chek	T-021	1	550	4.2	5.4	6	3.486	0.06	3.0E-05	< 0.01	< 0.01
Ice-chek Tank	Ice-chek	T-022	1	550	4.2	5.4	6	3.486	0.06	3.0E-05	< 0.01	< 0.01
New TEG Tank	New TEG	T-023	1	2.000	5.3	12.0	2	4.200	0.05	2.5E-05	< 0.01	< 0.01
Used TEG Tank	Used TEG	T-024	1	2,000	5.3	12.0	2	4,200	0.05	2.5E-05	< 0.01	<0.01
Total Potential Emissions (excludi	stal Potential Emissions (excluding pipeline fluids tanks) 4.21 0.00 0.000											0.00

1. Ice-Chek contains ethylene glycol

 Produced Fluids Tank (210 bbl) - T001 & T002

 Operational Hours
 8,760 hrs/yr

 Control Efficiency
 0% No crec

 Annual Fluid Throughput (per tank)
 105,000 gal/yr
 0% No credit is assumed for control using the combustor. 105,000 gal/yr

Description	Potential Throughput ¹ (gal/yr)
Produced Water	105,000

¹ Based on engineering estimate of produced water for the station. Produced water comprises of 90% water and 10% condensate

Storage Tank (210 bbl, each) - Emissions (Each Tank)

	Uncon	trolled	Cont	rolled
	Total En	issions 1	Total Er	nissions ¹
Constituent	lb/hr	tpy	lb/hr	tpy
Carbon Dioxide	0.002	0.007	0.002	0.007
Methane	0.158	0.692	0.158	0.692
Ethane	0.149	0.651	0.149	0.651
Propane	0.273	1.194	0.273	1.194
Isobutane	0.192	0.841	0.192	0.841
n-Butane	0.181	0.791	0.181	0.791
Isopentane	0.149	0.653	0.149	0.653
n-Pentane	0.063	0.276	0.063	0.276
n-Hexane	0.019	0.085	0.019	0.085
Other Hexanes	0.047	0.204	0.047	0.204
Heptanes	0.022	0.095	0.022	0.095
Benzene	0.001	0.005	0.001	0.005
Toluene	0.001	0.005	0.001	0.005
Ethylbenzene	< 0.001	< 0.001	< 0.001	< 0.001
Xylenes	0.000	0.002	0.000	0.002
2,2,4-Trimethylpentane	< 0.001	< 0.001	< 0.001	< 0.001
C8+ Heavies	0.008	0.036	0.008	0.036
Total Emissions:	1.262	5.529	1.262	5.529
Total VOC Emissions:	0.956	4.186	0.956	4.186
Total HAP Emissions:	0.023	0.100	0.023	0.100

¹ E&P TANK v2.0 calculates working, breathing and flashing losses and reports the sum as one total.

Fugitive Emissions

Fugitive Component Information:

	Estimated Component	Gas Leak	Emission Factor	Average Gas Leak Rate	Max Gas Leak Rate	Potential VOC Emissions	Potential HAP Emissions
Component Type	Count	(lb/hr/component)	Factor Source	(lb/hr)	(tpy)	(tpy)	(tpy)
Connectors	650	0.0004	EPA Protocol, Table 2-4	0.29	1.51	0.23	0.01
Flanges	250	0.001	EPA Protocol, Table 2-4	0.21	1.13	0.17	0.01
Open-Ended Lines	12	0.004	EPA Protocol, Table 2-4	0.05	0.28	0.04	0.00
Valves	700	0.010	EPA Protocol, Table 2-4	6.94	36.50	5.65	0.31
		Total		7.50	39.41	6.10	0.33

Notes:
1. The component type "Other" includes any equipment type other than connectors, flanges, open-ended lines, pumps and valves that have fugitive emissions.

2. The component count is a preliminary estimate based on the proposed design of the station

3. Table 2-4 : Oil & Gas Production Operations Average Emission Factors, Protocol for Equipment Leak Emission Estimates, EPA 453/R-95-017, November 1995.

4. Assumes maximum leak rate 20% greater than measured average leak rate.

GHG Fugitive Emissions from Component Leaks:

	Estimated Component	GHG E	mission Factor	CH ₄ Emissions	CO ₂ Emissions	CO ₂ e Emissions
Component Type	Count	(scf/hr/component)	Factor Source	(tpy)	(tpy)	(tpy)
Connectors	650	0.003	40 CFR 98, Table W-1A	0.29	1.9E-03	7.29
Flanges	250	0.003	40 CFR 98, Table W-1A	0.11	7.2E-04	2.80
Open-Ended Lines	12	0.061	40 CFR 98, Table W-1A	0.11	7.1E-04	2.74
Valves	700	0.027	40 CFR 98, Table W-1A	2.83	1.8E-02	70.66
	Total			3.34	0.02	83.49

Notes:

The component count is a preliminary estimate based on the proposed design of the station
 Table W-1 of Subpart W - Default Whole Gas Emission Factors for Onshore Production , 40 CFR 98, Subpart W.

3. Calculated in accordance with Equations W-32a, W-35, and W-36 in Subpart W of 40 CFR 98.

4. GHG (CO_2e) is carbon dioxide equivalent, which is the summation of CO2 (GWP = 1) + CH4 (GWP = 25) + N2O (GWP = 298).

Rod Packing Emissions

Number of Compressors	Number of Rods Per Compressor	Leak Rate (scf/hr/rod)	Total Volume NG Emitted (scf/yr)	Potential VOC Emissions (tpy)	Potential HAP Emissions (tpy)	Potential CO ₂ Emissions (tpy)	Potential CH ₄ Emissions (tpy)	Potential CO ₂ e Emissions (tpy)
4	6	11	2,312,640	8.94	0.49	0.25	39.47	987.03
Total				8.94	0.49	0.25	39.47	987.03

Notes:

 1. Assumes a density of natural gas of
 0.05

 2. Leak rate from https://www3.epa.gov/gasstar/documents/ll_rodpack.pdf

VOC/GHG Fugitive Emissions from Blowdowns:

Blowdown Type	Number of Events	Gas Volume (scf/event)	VOC Emissions (tpy)	HAP Emissions (tpy)	CH ₄ Emissions (tpy)	CO ₂ Emissions (tpy)	CO ₂ e Emissions (tpy)
Station ESD	5	358,000	6.92	0.38	30.55	0.20	763.97
Pigging Operations	250	2,000	1.93	0.11	8.53	0.06	213.40
Filter Maintenance	15	13,500	0.78	0.04	3.46	0.02	86.43
Compressor	36	44,000	6.13	0.34	27.03	0.17	676.05
Total			15.76	0.86	69.58	0.45	1,739.84

Notes:

1. CH₄ and CO₂ emissions are based on fractions of these pollutants in the site-specific gas analysis.

GHG Emissions are calculated in accordance with Equations W-35 and W-36 in Subpart W of 40 CFR 98.
 GHG (CO₂e) is carbon dioxide equivalent, which is the summation of CO₂ (GWP = 1) + CH₄ (GWP = 25) + N₂O (GWP = 298).

0.05 lb/ft3 @ STP and wt% are used for VOC and HAP emission calculations. 4. Density of natural gas:

lb/scf

Fugitive Component Emissions Data:

Pollutant	Atmosp	heric Emissions	Emissions Estimation Method			
ronutant	lbs/hr	tpy	Emissions Estimation Method			
VOC	7.03	30.80	EPA Protocol, Table 2-4 and Site-Specific Gas Analysis			
HAPs	0.39	1.69	EPA Protocol, Table 2-4 and Site-Specific Gas Analysis			
GHG (CO ₂ e)	642	2810	40 CFR 98, Table W-1A and Site-Specific Gas Analysis			

E17 - ENGINES, NATURAL GAS FIRED, 4 STROKE, LEAN BURN, WITH CATALYTIC OXIDATION

CALCULATION METHODS

Ea = Ua x EF (lbs/mmft3)

Eh = Uh (scfm) x (60/1000000) x EF (lbs/mmft3)

NOTES:

- Catalytic oxidation can achieve efficiencies of approximately 90% in reducing of CO, ROG, TOG, and AB2588 toxic organic compounds.

- The trace organic factors listed below are based on detected AB 2588 compounds listed in AP-42 Table 3.2-2 (7/00).

- The AP-42 (7/00) emission factors have been converted into lbs/mmscf by assuming a natural gas BTU content of 1020 BTU/scf.

- PM10 and TSP emission factors include filterable and condensable PM in accordance with the District's definition of particulate matter.

- The listed AP-42 emission factors for 1,1,2-trichloroethane, 1,1-dichloroethane, 1,2-dichloroethane, 1,2-dichloropropane, 1,3-dichloropropane, carbon tetrachloride, chloroform, ethylene dibromide, styrene, and vinyl chloride are NOT included since these values are based on nondetectable test results.

- The listed AP-42 emission factors for 1,1,2,2-tetrachloroethane, 1,2,4-trimethylbenzene, 2,2,4-trimethylpentane, 2-methylnaphthalene, acenaphthalene, acenaphthylene, anthracene, benz(a)anthracene, benzo(a)pyrene, benzo(b)fluoranthene, benzo(g,h,i)perylene, benzo(k)fluoranthene, biphenyl, chlorobenzene, chrysene, cyclohexane, fluoranthene, indeno(1,2,3-c,d)pyrene, perylene, phenanthrene, and pyrene are NOT included since these values were based on insignificant and/or nondetectable test results.

- Trace metal emission factors were not reported in AP-42 and are NOT included since natural gas fired engines are not expected to emit metals.

- The AP-42 emission factors for 1,2,3-trimethylbenzene, 1,3,5-trimethylpentane, butyr/isobutyraldehyde, cyclopentane, ethane, isobutane, methylcyclohexane, n-nonane, n-octane, n-pentane, and propane are not included since these are not listed toxic air contaminants.

- The AP-42 acrolein emission factor is NOT included since this value is based on test data and detection limits from incorrect sampling methods. A District factor based on local test results and adjusted for equipment VOC controls is considered more accurate than the AP-42 value.

Pollutant	District Emission Factor (lbs/million ft3 fuel burned)	EPA Reference Document	EPA Factor	Units	Comments
NOx		AP-42, Sect 3.2, 7/00, Table 3.2-2	4.08E+00	lbs/MMBTU	
со		AP-42, Sect 3.2, 7/00, Table 3.2-2 3.17E-01 lbs/MMBTU Catalytic oxida in Table 3.2-2		Catalytic oxidation 90% control of value shown in Table 3.2-2	
SOx		AP-42, Sect 3.2, 7/00, Table 3.2-2	5.88E-04	lbs/MMBTU	Assume a sulfur content of 0.05% and a fuel density of 7 lbs/gal
TOG	149.94	AP-42, Sect 3.2, 7/00, Table 3.2-2	1.47E+00	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
ROG		AP-42, Sect 3.2, 7/00, Table 3.2-2	1.18E-01	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
TSP		AP-42, Sect 3.2, 7/00, Table 3.2-2	9.99E-03	lbs/MMBTU	TSP includes filterable (7.71 E-05) and condensable (9.91 E-03) PM.
PM10		AP-42, Sect 3.2, 7/00, Table 3.2-2	9.99E-03	lbs/MMBTU	PM10 includes filterable (7.71 E-05) and condensable (9.91 E-03) PM.
1,3-Butadiene		AP-42, Sect 3.2, 7/00, Table 3.2-2	2.67E-04	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
Acetaldehyde		AP-42, Sect 3.2, 7/00, Table 3.2-2	8.36E-03	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
Acrolein		AP-42, Sect 3.2, 7/00, Table 3.2-2	5.14E-03	lbs/MMBTU	District emission factor based on SDAPCD source test results.

Benzene	0.04	AP-42, Sect 3.2, 7/00, Table 3.2-2	4.40E-04	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
Ethylbenzene	0.004	AP-42, Sect 3.2, 7/00, Table 3.2-2	3.97E-05	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
Formaldehyde	5.39	AP-42, Sect 3.2, 7/00, Table 3.2-2	5.28E-02	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
Hexane	0.11	AP-42, Sect 3.2, 7/00, Table 3.2-2	1.11E-03	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
Methanol	0.26	AP-42, Sect 3.2, 7/00, Table 3.2-2	2.50E-03	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
Methylene Chloride	0.002	AP-42, Sect 3.2, 7/00, Table 3.2-2	2.00E-05	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
Naphthalene	0.01	AP-42, Sect 3.2, 7/00, Table 3.2-2	7.44E-05	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
РАН	0.003	AP-42, Sect 3.2, 7/00, Table 3.2-2	2.69E-05	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
Phenol	0.002	AP-42, Sect 3.2, 7/00, Table 3.2-2	2.40E-05	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
Toluene	0.04	AP-42, Sect 3.2, 7/00, Table 3.2-2	4.08E-04	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2
Xylenes	0.02	AP-42, Sect 3.2, 7/00, Table 3.2-2	1.84E-04	lbs/MMBTU	Catalytic oxidation 90% control of value shown in Table 3.2-2

Last Updated on 7/20/01 (E06) By D. Byrnes / A. Mar

* * Project Setup Information : Z:\Client\EQT Corporation\West Virginia\Janus\153901.0106 R13 Application\04 Draft\2015-Project File 0708 Janus R13 Application\Attach N - Emission Calculations\E&P Tank\20150715_EQT_Janus_PWT.ept Flowsheet Selection : Oil Tank with Separator : **RVP** Distillation Calculation Method Control Efficiency : 95.0% Known Separator Stream : Geographical Region Geographical Region : All Regions in US Entering Air Composition : No Filed Name : Janus Produced Water Tank Well Name : 210 bbl PWT Date : 2015.07.15 * * Data Input : 300.00[psig] Separator Pressure Separator Temperature : 80.00[F] Ambient Pressure : 14.70[psia] Ambient Temperature : 80.00[F] C10+ SG : 0.8820 : 296.00 C10+ MW -- Low Pressure Oil ------No. Component mol % 1 H₂S 0.0000 2 02 0.0000 3 CO₂ 0.0300 4 N2 0.0900 5 C1 8.4300 6 C2 4.2300 7 C3 5.9100 8 i-C4 5.1700 9 n-C4 6.2200 10 i-C5 8.9100 11 n-C5 4.9700 12 C6 9.1100 13 C7 11.3400 C8 14 10.3900 15 C9 5.9600 C10+ 16 11.7500 17 Benzene 0.3700 18 Toluene 0.9800 19 E-Benzene 0.1500 20 1.1900 Xylenes 21 n-C6 4.8000 22 0.0000 224Trimethylp

Production R Days of Ann	ual Operatio	n : 365 [day	/s/year]			
API Gravity						
Reid Vapor I	Pressure	: 10.60[ps1a]				
		********	********	**********	**************************************	:
	ion Results ********	*******	*******	**********	***************************************	:
Item				trolled Con b/hr]	E&P TANK	
Page 1					E&P TANK	
Total HAPs	0.100	0.023	0.005	0.001		
Total HC	5.529	1.262	0.276	0.063		
VOCs, C2+	4.836	1.104	0.242	0.055		
VOCs, C3+	4.186	0.956	0.209	0.048		
Uncontrolled Vapor	Recovery In 287.1100		TEDI			
-	or 285.830	-	-			
-	287.11	-	-			
		-	-			
-				Controlled	Controlled	
	[ton/yr] [•			
1 H2S	0.000		0.000			
2 O2						
3 CO2 4 N2	0.007	0.002	0.007	0.002		
5 C1			0.035	0.008		
6 C2	0.651	0.149	0.033	0.007		
7 C3	1.194	0.273	0.060	0.014		
8 i-C4	0.841	0.192	0.042	0.010		
9 n-C4	0.791	0.181	0.040	0.009		
10 i-C5	0.653	0.149	0.033	0.007		
11 n-C5 12 C6	0.276 0.204	0.063 0.047	0.014 0.010	0.003 0.002		
12 C0 13 C7	0.204	0.047	0.005	0.002		
13 C7 14 C8	0.030	0.022	0.003	0.001		
14 C8 15 C9	0.006	0.007	0.002	0.000		
16 C10+	0.000	0.001	0.000	0.000		
17 Benzene	0.000	0.000	0.000	0.000		
18 Toluene	0.005	0.001	0.000	0.000		
19 E-Benzei			0.000	0.000		
20 Xylenes	0.002	0.000	0.000	0.000		
20 nJnenes 21 n-C6	0.085	0.019	0.004	0.001		
22 224Trime						
Total	5.550	1.267	0.277	0.063		
Stream Da	to					

-- Stream Data -----

No. Component	MW LP Oil Flash Oil Sale Oil Flash Gas W&S Gas Total Emissions
	mol % mol % mol % mol % mol %
1 H2S	34.80 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
2 O2	32.00 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
3 CO2	44.01 0.0300 0.0021 0.0000 0.1194 0.0496 0.1111
4 N2	28.01 0.0900 0.0006 0.0000 0.3763 0.0145 0.3332
5 C1	16.04 8.4300 0.2054 0.0000 34.7691 4.8646 31.2062
6 C2	30.07 4.2300 0.5879 0.0039 15.8939 13.8313 15.6481
7 C3	44.10 5.9100 2.4063 0.8494 17.1306 37.7108 19.5826
8 i-C4	58.12 5.1700 3.7204 3.2119 9.8124 15.2521 10.4605
9 n-C4	58.12 6.2200 5.2238 4.8805 9.4102 13.0089 9.8389
10 i-C5	72.15 8.9100 9.7007 9.7854 6.3777 7.7795 6.5447
11 n-C5	72.15 4.9700 5.6802 5.7866 2.6955 3.2686 2.7638
12 C6	86.16 9.1100 11.4207 11.8324 1.7100 2.0852 1.7547
13 C7	100.20 11.3400 14.6665 15.2753 0.6869 0.8605 0.7075
14 C8	114.23 10.3900 13.5756 14.1635 0.1882 0.2442 0.1949
15 C9	128.28 5.9600 7.8101 8.1523 0.0352 0.0503 0.0370
16 C10+	175.93 11.7500 15.4190 16.0990 0.0000 0.0000 0.0000
17 Benzene	78.11 0.3700 0.4701 0.4881 0.0496 0.0610 0.0509
18 Toluene	92.13 0.9800 1.2750 1.3293 0.0351 0.0448 0.0363
	106.17 0.1500 0.1963 0.2049 0.0017 0.0022 0.0017
•	106.17 1.1900 1.5580 1.6260 0.0114 0.0152 0.0119
	86.18 4.8000 6.0812 6.3116 0.6969 0.8566 0.7160
22 224Trimethy	lp 114.24 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
MW	100.95 120.35 123.46 38.83 49.76 40.13
Stream Mole	
Heating Value	
Gas Gravity	e [BTU/SCF] 2218.43 2811.04 2289.04 [Gas/Air] 1.34 1.72 1.39
Bubble Pt @	100F [nsia] 322 24 24 57 11 47
Page 2	100F [psia] 322.24 24.57 11.47 E&P TANK
RVP @ 100F	
Spee. Gravity	

ATTACHMENT O

Monitoring/Recordkeeping/Reporting/Testing Plans

Plan Type	Emission unit	Pollutant	Requirements	Frequency	Method of	Regulatory
					Measurement	Reference
Monitoring,	Storage Tanks	VOC	Monitor throughput of Tanks		N/A	(Condition
Recordkeeping						4.1.8.b of
						Permit)
Monitoring	Blowdowns,	VOC	Monitor station blowdown,	Annual	12 Month Rolling	(Condition
	Station		shutdown, pigging venting events		Total	4.1.12.c of
	Fugitives,					Permit)
	Pigging					
Monitoring,	Liquid	VOC	Monitor throughput of loading		Records	(Condition
Recordkeeping	Loading					4.1.9.b of
	C					Permit)

ATTACHMENT O - MONITORING, RECORDING, REPORTING, AND TESTING PLANS

See Attachment D for additional information.

ATTACHMENT P

Public Notice

AIR QUALITY PERMIT NOTICE Notice of Application

Notice is given that EGT Gathering, LLC has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a Class II Administrative Update to permit number R13-3269 for an existing natural gas compressor station (the Janus Station) located off Left Fork Run Road in Doddridge County, West Virginia. The site latitude and longitude coordinates are: 39.25777 N, -80.80566 W.

The applicant estimates the potential increase in the following Regulated Air Pollutants associated with the project will be:

Particulate Matter (PM) = <0.01 tpy Sulfur Dioxide (SO2) = <0.01 tpy Volatile Organic Compounds (VOC) = 7.95 tpy Carbon Monoxide (CO) = <0.01 tpy Nitrogen Oxides (NOx) = <0.01 tpy Hazardous Air Pollutants (HAPs) = <0.01 tpy Carbon Dioxide Equivalents (CO₂e) = 988.85 tpy

Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1250, during normal business hours.

Dated on June 9, 2016.

By: EQT Gathering, LLC Diana Charletta, Senior Vice President – Midstream Operations 625 Liberty Avenue Suite 1700 Pittsburgh, PA 15222