

SWN Production Company, LLC P O Box 12359 Spring, Texas 77391-2359 www.swn.com

JOHN GOOD JR. PAD

G70-D PERMIT REGISTRATION

0	CHK	-	R13-2982	NA	NA
I	CHK	-	R13-2982A	NA	NA
2	CHK	3/21/2016	R13-2982B	NA	NA
3	CMM	6/22/2017	G70-D	AML	6/23/2017
REV	BY	DATE	DESCRIPTION	FACILITIES REVIEWED	DATE

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INTRODUCTION

SWN Production Company, LLC (SWN), operates the John Good Jr Pad under Permit No. R13-2982B, issued on March 21, 2016. With this application, SWN requests authorization to add two 145-hp Caterpillar G3306 NA compressor engines, two stabilizer heaters, five GPU burners, two condensate tanks, two produced water tanks, and one 30-mmBtu/hr combustor with pilots and to remove two line heaters, one heater treater, and one 20-mmBtu/hr combustor with pilots. Tank throughputs and compositions have also been updated and fugitive emissions have been revised to include seven sand separators. As a result of these changes, truck loading, vapor combustor, fugitive, and haul road emissions have also been updated. SWN also requests to operate under the General Permit G70-D for Oil and Natural Gas Production Facilities. Equipment to be authorized includes the following:

- Two (2) Caterpillar G3306 NA Compressor Engines
- Seven (7) 1.0-mmBtu/hr Gas Production Units
- Two (2) 1.5-mmBtu/hr Stabilizer Heaters
- Eight (8) 400-bbl Condensate Tanks
- Eight (8) 400-bbl Produced Water Tanks
- Condensate Truck Loading
- Produced Water Truck Loading
- One (1) 30.0-mmBtu/hr Vapor Combustor with Pilots
- Fugitive Emissions
- Fugitive Haul Road Emissions

Note that other small storage tanks may be present on site (i.e., methanol, lube oil) but are considered de minimis sources per Table 45-13B and are listed on the application form.

Proposed Emissions

Emissions calculations for the facility are presented in Attachment T. A fuel heating value of 905 Btu/scf was used to calculate emissions from natural gas-fired equipment. Actual heating value may vary (generally 905 - 1,300) but using a lower heating value in the emissions calculations provides a more conservative (higher) estimate of fuel use.

Emissions from the Caterpillar engines were calculated with manufacturer data when available and AP-42/EPA emissions factors for the remaining pollutants.

Condensate and produced water tank emissions were calculated using ProMax process simulation software. Tank emissions are routed to a vapor combustor with 100% capture efficiency and 98% destruction efficiency. Loading emissions were calculated using ProMax process simulation software and AP-42 calculations. Loading emissions are routed to a vapor combustor with 70% capture efficiency and 98% destruction efficiency.

Fugitive emissions were calculated with a component count by equipment type from a similar facility, and representative extended gas and liquids analyses. Fugitive haul road emissions were calculated using EPA/AP-42 methodologies.

Greenhouse gas emissions were calculated with the latest EPA factors and manufacturer data when available. Documents used as references for the emissions calculations, including AP-42 and EPA emission factor references, gas and liquids analyses, and process simulation results are attached.

Regulatory Discussion

STATE

45 CSR 13 - PERMITS FOR CONSTRUCTION, MODIFICATION, RELOCATION AND OPERATION OF STATIONARY SOURCES OF AIR POLLUTANTS, NOTIFICATION REQUIREMENTS, ADMINISTRATIVE UPDATES, TEMPORARY PERMITS, GENERAL PERMITS, AND PROCEDURES FOR EVALUATION:

The facility requests to operate under the General Permit G70-D. Emissions of carbon monoxide and volatile organic compounds are less than 80 tons per year (TPY). Oxides of nitrogen emissions are less than 50 TPY and particulate matter 10/2.5 and sulfur dioxide emissions are each less than 20 TPY. Also, the facility will have less than 8 TPY for each hazardous air pollutant and less than 20 tons for total hazardous air pollutants.

45 CSR 22 - AIR QUALITY MANAGEMENT FEE PROGRAM:

The facility will be required to maintain a valid Certificate to Operate on the premises.

45 CSR 30 - REQUIREMENTS FOR OPERATING PERMITS:

Emissions from the facility do not exceed major source thresholds; therefore, this rule does not apply.

FEDERAL

40 CFR PART 60 SUBPART KB—STANDARDS OF PERFORMANCE FOR VOLATILE ORGANIC LIQUID STORAGE VESSELS (INCLUDING PETROLEUM LIQUID STORAGE VESSELS) FOR WHICH CONSTRUCTION, RECONSTRUCTION, OR MODIFICATION COMMENCED AFTER JULY 23, 1984

The affected facility to which this Subpart applies is each storage vessel with a capacity greater than or equal to 75 cubic meters (m³) that is used to store volatile organic liquids (VOL) for which construction, reconstruction, or modification is commenced after July 23, 1984. The tanks at this facility were constructed after the effective date of this Subpart but are less than 75 m³ (which equals approximately 471 bbl); therefore, this Subpart does not apply.

40 CFR PART 60 SUBPART KKK - STANDARDS OF PERFORMANCE FOR STATIONARY FOR EQUIPMENT LEAKS OF VOC FROM ONSHORE NATURAL GAS PROCESSING PLANTS:

The facility is not considered an affected source (natural gas processing plant) and is therefore not subject to this Subpart.

40 CFR PART 60 SUBPART IIII - STANDARDS OF PERFORMANCE FOR STATIONARY COMPRESSION IGNITION INTERNAL COMBUSTION ENGINES:

The facility does not contain the affected source (diesel-fired engine) and is therefore not subject to this Subpart.

40 CFR PART 60 SUBPART JJJJ - STANDARDS OF PERFORMANCE FOR STATIONARY SPARK IGNITION INTERNAL COMBUSTION ENGINES:

The proposed 145-hp, four-stroke, rich-burn natural gas-fired flash gas compressor engines are assumed to have been constructed after the June 12, 2006 effective date and manufactured after July 1, 2008; therefore, they will be subject to this Subpart. Although final selection of the engines have not yet been made, it is presumed that the engines were manufactured after January 1, 2011 and therefore subject to Stage 2 emission limitations under this Subpart. SWN will comply with all applicable requirements.

40 CFR PART 60 SUBPART OOOO - STANDARDS OF PERFORMANCE FOR CRUDE OIL AND NATURAL GAS PRODUCTION, TRANSMISSION, AND DISTRIBUTION:

The emission sources affected by this Subpart include well completions, pneumatic controllers, equipment leaks from natural gas processing plants, sweetening units at natural gas processing plants, reciprocating compressors, centrifugal compressors and storage vessels which are constructed, modified or reconstructed after August 23, 2011 and before September 18, 2015.

The existing wells at this location were completed during the effective date of this Subpart and are subject to the compliance requirements. There is no centrifugal compressor using wet gas seals at this facility. The pneumatic controllers utilized at the facility are considered low-bleed and are not subject to this Subpart. The storage vessel venting is controlled to less than six (6) TPY VOC and federally enforceable limits are requested; therefore, the storage vessels are not subject to this Subpart.

40 CFR PART 60 SUBPART OOOOA - STANDARDS OF PERFORMANCE FOR CRUDE OIL AND NATURAL GAS FACILITIES FOR WHICH CONSTRUCTION, MODIFICATION, OR RECONSTRUCTION COMMENCED AFTER SEPTEMBER 18, 2015:

The emission sources affected by this Subpart include well completions, centrifugal compressors, reciprocating compressors, pneumatic controllers, storage vessels, fugitive sources at well sites, fugitive sources at compressor stations, pneumatic pumps, equipment leaks from natural gas processing plants and sweetening units at natural gas processing plants which are constructed, modified or reconstructed after September 18, 2015.

The proposed wells at this location will be completed after the effective date of this Subpart and will be subject to the compliance requirements. There is no centrifugal compressor using wet gas seals at this facility. The pneumatic controllers utilized at the facility are considered low-bleed and are not subject to this Subpart. The storage vessels were constructed before the effective date of this Subpart and are not subject to this Subpart.

40 CFR PART 63 SUBPART HH - NATIONAL EMISSION STANDARDS FOR HAZARDOUS AIR POLLUTANTS FOR SOURCE CATEGORIES FROM OIL AND NATURAL GAS PRODUCTION FACILITIES:

The site is a minor (area) source of hazardous air pollutants. This Subpart applies to affected emission points that are located at facilities that are major and area sources of HAP, and either process, upgrade, or store hydrocarbon liquids prior to custody transfer or that process, upgrade, or store natural gas prior to entering the natural gas transmission and storage source category. For purposes of this Subpart natural gas enters the natural gas transmission and storage source category after the natural gas processing plant, if present. The facility is a minor (area) source of HAP; however, there is no triethylene glycol (TEG) dehydration unit present at the facility and therefore this Subpart does not apply.

40 CFR PART 63 SUBPART HHH - NATIONAL EMISSION STANDARDS FOR HAZARDOUS AIR POLLUTANTS FOR SOURCE CATEGORIES FROM NATURAL TRANSMISSION AND STORAGE FACILITIES:

The facility is not a natural gas transmission and storage facility and is therefore not subject to this Subpart.

40 CFR PART 63 SUBPART ZZZZ - NATIONAL EMISSION STANDARDS FOR HAZARDOUS AIR POLLUTANTS FOR SOURCE CATEGORIES FROM STATIONARY RECIPROCATING INTERNAL COMBUSTION ENGINES - AREA SOURCE:

The original rule, published on February 26, 2004, initially affected new (constructed or reconstructed after December 19, 2002) reciprocating internal combustion engines (RICE) with a site-rating greater than 500 brake horsepower (HP) located at a major source of HAP emissions. On January 18, 2008, EPA published an amendment that promulgated standards for RICE constructed or reconstructed after June 12, 2006 with a site rating less than or equal to 500 HP located at major sources, and for engines constructed and reconstructed after June 12, 2006 located at area sources. On August 10, 2010, EPA published another amendment that promulgated standards for existing (constructed or reconstructed before June 12, 2006) RICE at area sources and existing RICE (constructed or reconstructed before June 12, 2006) with a site rating of less than or equal to 500 HP at major sources.

Owners and operators of new or reconstructed engines at area sources must meet the requirements of Subpart ZZZZ by complying with either 40 CFR Part 60 Subpart IIII (for CI engines) or 40 CFR Part 60 Subpart JJJJ (for SI engines). Based on emission calculations, this facility is a minor source of HAP. The 145-hp, four-stroke, rich-burn natural gas-fired flash gas compressor engines are considered new engines manufactured after January 1, 2011 and will meet the requirements of this Subpart by complying with requirements under NSPS Subpart JJJJ.

APPLICATION FOR GENERAL PERMIT REGISTRATION



west virginia department of environmental protection

Division of Air Quality 601 57th Street SE Charleston, WV 25 4 Phone (304) 926-0475 Fax (304) 926-0479 www.dep.wv.gov

G70-D GENERAL PERMIT REGISTRATION APPLICATION

PREVENTION AND CONTROL OF AIR POLLUTION IN REGARD TO THE CONSTRUCTION, MODIFICATION, RELOCATION, ADMINISTRATIVE UPDATE AND OPERATION OF NATURAL GAS PRODUCTION FACILITIES LOCATED AT THE WELL SITE

NATURAL GAS PRO	DUCTION FACII	ITIES LOCATED AT	THE WELL SITE				
⊠CONSTRUCTION □MODIFICATION □RELOCATION	□CLASS I ADMINISTRATIVE UPDATE □CLASS II ADMINISTRATIVE UPDATE						
SI	SECTION 1. GENERAL INFORMATION						
Name of Applicant (as registered with the	WV Secretary of S	tate's Office): SWN I	roduction Company, LLC	2			
Federal Employer ID No. (FEIN): 26-4388	8727						
Applicant's Mailing Address: 10000 Ene	rgy Drive						
City: Spring	State: TX		ZIP Code: 7738	9			
Facility Name: John Good Jr Pad							
Operating Site Physical Address: 1150 Mo If none available, list road, city or town an		d					
City: Wellsburg	Zip Code: 26070)	County: Brooke	;			
Latitude & Longitude Coordinates (NAD83 Latitude: 40.231762 Longitude: -80.582193 SIC Code: 1311	, Decimal Degrees	to 5 digits):					
NAICS Code: 211111		DAQ Facility ID No. (For existing facilities) 009-00105					
	CERTIFICATION (OF INFORMATION	STATE HAVE THE				
This G70-D General Permit Registration Official is a President, Vice President, Sec Directors, or Owner, depending on business authority to bind the Corporation, Pa Proprietorship. Required records of dai compliance certifications and all requi Representative. If a business wishes to cert off and the appropriate names and sign unsigned G70-D Registration Application utilized, the application will here.	cretary, Treasurer, s structure. A busin trenship, Limited ly throughput, hou red notifications m ify an Authorized atures entered. An a will be returned	General Partner, General Partner, General Partner, General Liability Company, As as of operation and mains the signed by a Resperesentative, the officy administratively incomparts to the applicant. Fur	al Manager, a member of the horized Representative who sociation, Joint Venture or S ntenance, general correspon consible Official or an Authorial cial agreement below shall to omplete or improperly sign thermore, if the G70-D for	e Board of shall have Sole dence, orized be checked ned or			
I hereby certify that <u>Carla Suszkowski</u> is the business (e.g., Corporation, Partnership and may obligate and legally bind the busin Official shall notify the Director of the Div I hereby certify that all information contain documents appended hereto is, to the best of have been made to provide the most compression.	, Limited Liability less. If the business ision of Air Qualit led in this G70-D (f my knowledge, to	Company, Association schanges its Authorize y immediately. General Permit Registratue, accurate and comp	Joint Venture or Sole Proprd Representative, a Respons	rietorship) ible pporting			
Responsible Official Signature: Name and Title: Carla Suszkowski Email: Carla_Suszkowski@SWN.com	Phone: 832-7 Date: 6 -	96-1000 21-17	Fax: 405-849-3102				
If applicable: Authorized Representative Signature: Name and Title: Email:	Phone: Date:)	ax:				
If applicable: Environmental Contact Name and Title: Clay Murral Email: Clay_Murral@SWN.com	Pho	ne: 304-884-1715 Date:	Fax:				

OPERATING SITE INFORMATION

Briefly describe the proposed new operation and/or any change(s) to the facility: This application includes two (2) Caterpillar G3306 NA engines (EU-ENG1 – EU-ENG2), seven (7) 1.0-mmBtu/hr natural gas-fired gas production unit (GPU) burners (EU-GPU1 – EU-GPU7), two (2) 1.5-mmBtu/hr natural gas-fired stabilizer heaters (EU-SH1 – EU-SH2), eight (8) 400-bbl condensate tanks (EU-TANKS-COND), eight (8) 400-bbl produced water tanks (EU-TANKS-PW), condensate and produced water truck loading (EU-LOAD-COND and EU-LOAD-PW), one (1) 30.0-mmBtu/hr vapor combustor (APC-COMB) with three (3) 50-SCFH pilots (EU-PILOTS), fugitive emissions (EU-FUG), and fugitive haul road emissions (EU-HR).

Directions to the facility: From I-70 take exit 1A to SR-2 North. Travel SR-2 North for 15.1 miles to SR-67 and turn right on SR-67. Travel 2.5 miles to CR-24, (McAdoo Ridge Rd), and turn left. Turn immediately right and travel 1.1 miles to access road on right.

ATTACHMENTS AND SUPPORTING DOCUMENTS

ATTACHMENTS AND SUPPORTING DOCUMENTS						
I have enclosed the following required document	ts:					
Check payable to WVDEP - Division of Air Quality with the	appropriate application fee (per 45CSR13 and 45CSR22).					
 ☑ Check attached to front of application. ☐ I wish to pay by electronic transfer. Contact for payment (i ☐ I wish to pay by credit card. Contact for payment (incl. na 						
⊠\$500 (Construction, Modification, and Relocation) ⊠\$1,000 NSPS fee for 40 CFR60, Subpart IIII, JJJJ, OOOO a □\$2,500 NESHAP fee for 40 CFR63, Subpart ZZZZ and/or H						
requirements by complying with NSPS, Subparts IIII and/or J.	¹ Only one NSPS fee will apply. ² Only one NESHAP fee will apply. The Subpart ZZZZ NESHAP fee will be waived for new engines that satisfy requirements by complying with NSPS, Subparts IIII and/or JJJJ. NSPS and NESHAP fees apply to new construction or if the source is being modified.					
⊠ Responsible Official or Authorized Representative Signatur	re (if applicable)					
⊠ Single Source Determination Form (must be completed) –	Attachment A					
☐ Siting Criteria Waiver (if applicable) – Attachment B	☐ Current Business Certificate – Attachment C					
□ Process Flow Diagram – Attachment D	□ Process Description – Attachment E					
□ Plot Plan – Attachment F	⊠ Area Map – Attachment G					
□ G70-D Section Applicability Form – Attachment H	⊠ Emission Units/ERD Table – Attachment I					
□ Fugitive Emissions Summary Sheet – Attachment J						
☐ Gas Well Affected Facility Data Sheet (if applicable) – Att	achment K					
 ⊠ Storage Vessel(s) Data Sheet (include gas sample data, USHYSYS, etc.), etc. where applicable) – Attachment L 	EPA Tanks, simulation software (e.g. ProMax, E&P Tanks,					
\boxtimes Natural Gas Fired Fuel Burning Unit(s) Data Sheet (GPUs, M	⊠ Natural Gas Fired Fuel Burning Unit(s) Data Sheet (GPUs, Heater Treaters, In-Line Heaters if applicable) – Attachment M					
\boxtimes Internal Combustion Engine Data Sheet(s) (include manufa N	☑ Internal Combustion Engine Data Sheet(s) (include manufacturer performance data sheet(s) if applicable) – Attachment N					
□ Tanker Truck/Rail Car Loading Data Sheet (if applicable) -	- Attachment O					
☐ Glycol Dehydration Unit Data Sheet(s) (include wet gas analysis, GRI- GLYCalc TM input and output reports and information on reboiler if applicable) – Attachment P						
☑ Pneumatic Controllers Data Sheet – Attachment Q						
⊠ Pneumatic Pump Data Sheet - Attachment R						
 ⊠ Air Pollution Control Device/Emission Reduction Device(sapplicable) – Attachment S) Sheet(s) (include manufacturer performance data sheet(s) if					
⊠ Emission Calculations (please be specific and include all calculations).	alculation methodologies used) - Attachment T					
□ Facility-wide Emission Summary Sheet(s) – Attachment U						
□ Class I Legal Advertisement – Attachment V						
☑ One (1) paper copy and two (2) copies of CD or DVD with pdf copy of application and attachments						

All attachments must be identified by name, divided into sections, and submitted in order.

ATTACHMENT A: SINGLE SOURCE DETERMINATION

ATTACHMENT A - SINGLE SOURCE DETERMINATION FORM

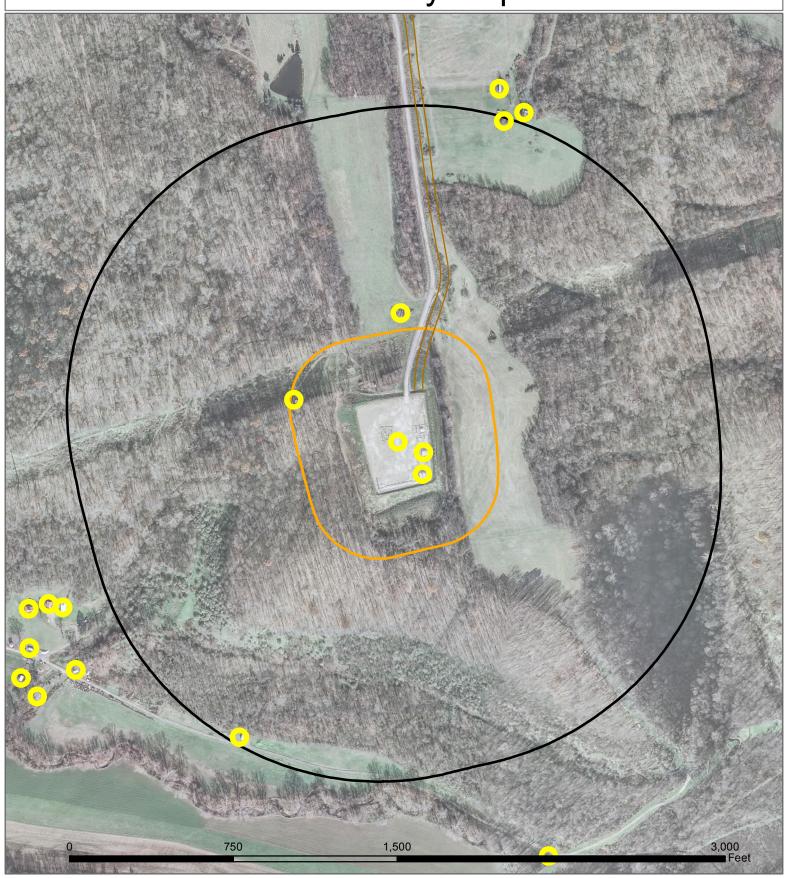
Classifying multiple facilities as one "stationary source" under 45CSR13, 45CSR14, and 45CSR19 is based on the definition of Building, structure, facility, or installation as given in §45-14-2.13 and §45-19-2.12. The definition states:

"Building, Structure, Facility, or Installation" means all of the pollutant-emitting activities which belong to the same industrial grouping, are located on one or more contiguous or adjacent properties, and are under the control of the same person (or persons under common control). Pollutant-emitting activities are a part of the same industrial grouping if they belong to the same "Major Group" (i.e., which have the same two (2)-digit code) as described in the Standard Industrial Classification Manual, 1987 (United States Government Printing Office stock number GPO 1987 0-185-718:QL 3).

The Source Determination Rule for the oil and gas industry was published in the Federal Register on June 3, 2016 and will become effective on August 2, 2016. EPA defined the term "adjacent" and stated that equipment and activities in the oil and gas sector that are under common control will be considered part of the same source if they are located on the same site or on sites that share equipment and are within ½ mile of each other.

Is there equip by SIC code) Yes □ N	
Is there equip person/people Yes □ N	
share equipm	oment and activities located on the same site or on sites that ent and are within $\frac{1}{4}$ mile of each other?

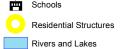
Proximity Map





John Good Jr. Pad

Lease Road: 2,871.10 Feet NAD83 UTM Zone 17N 535.687 4,452.68 Kilometers -80.582193 40.231762 Decimal Degrees





Compressor Stations



ATTACHMENT C: BUSINESS REGISTRATION CERTIFICATE

WEST VIRGINIA STATE TAX DEPARTMENT

BUSINESS REGISTRATION

SSUED TO:

SWN PRODUCTION COMPANY, LLC 5400D BIG TYLER RD

CHARLESTON, WV 25313-1103

GISTRATION ACCOUNT NUMBE

2307-3731

UNE

accordance: With Chapter 11. Article 12, of the West Virginia Code

The person of organization identified on this certificate is registered to conduct business in the State of West-Virginia at the location above.

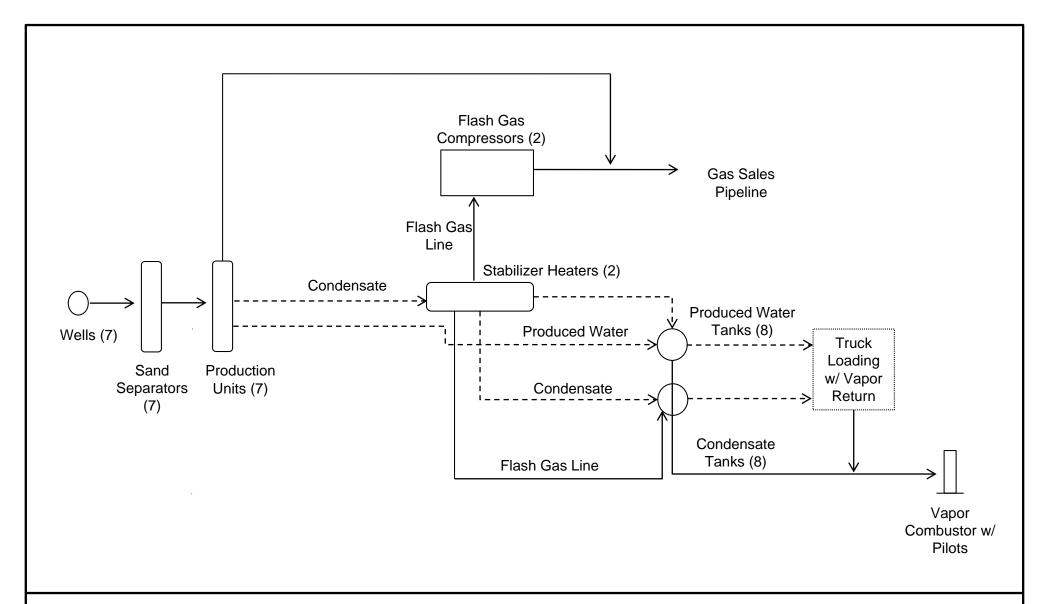
This certificate is not transferrable and must be displayed at the location for which issued This certificate shall be permanent until cessation of the business for which the certificate of registration was granted or until it is suspended, revoked or carricelled by the Tax Commissioner.

Change in name or change of location shall be considered a cessation of the business and a new certificate shall be required.

TRAVELING/STREET-VENDORS: Must-carry a copy of this certificate in every Vehicle operated by them. CONTRACTORS, DRILLING OPERATORS, TIMBER/LOGGING OPERATIONS: Must have a copy of this certificate displayed at every job site within West Virginia?

atL006 v.4 L1180094016

ATTACHMENT D: PROCESS FLOW DIAGRAM



Gas/Vapor
Liquids (Condensate and Produced Water)

Note: Drawing is a depiction of general facility process and is not intended to represent facility and/or equipment layout.

SWN Production Company, LLC John Good Jr Pad

Attachment D: Process Flow Diagram
June 2017

ATTACHMENT E: PROCESS DESCRIPTION

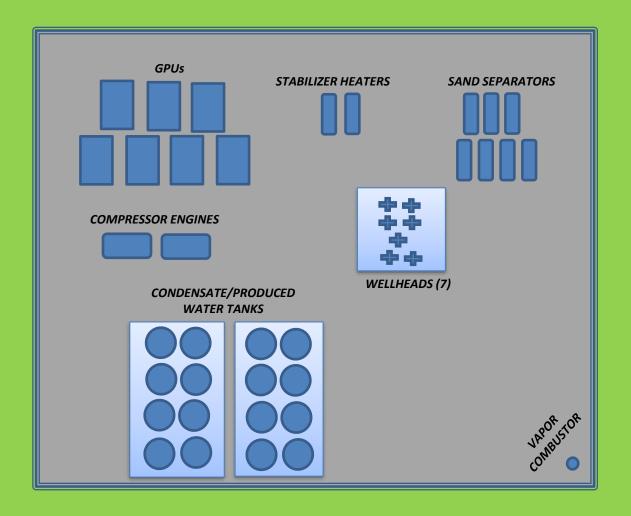
The facility is an oil and natural gas exploration and production facility, responsible for the production of condensate and natural gas. Storage of condensate and produced water also occurs on-site. A description of the facility process is as follows: Condensate, gas and water come from the wellheads through the sand separators then to the production units, where the first stage of separation occurs. Produced water is sent from the production units to the produced water tanks. Condensate and residual water are sent to the stabilizer heaters. The flash from the stabilizer heaters is captured via natural gas-fired engine-driven flash gas compressors. Condensate flows into the condensate storage tanks.

The natural gas stream exits the facility for transmission via pipeline. Condensate and produced water are transported offsite via truck. Loading emissions is controlled with vapor return, which has at least 70% capture efficiency, and is routed to the vapor combustor for at least 98% destruction efficiency. Working, breathing and flashing vapors from the condensate and produced water storage tanks are routed to the vapor combustor with 100% capture efficiency to be burned with at least 98% combustion efficiency. The vapor combustor has three (3) natural gas-fired pilots to ensure a constant flame for combustion.

A process flow diagram reflecting facility operations is shown in Attachment D.

ATTACHMENT F: PLOT PLAN

Please note that the simple plot plan provided is only a representation of production/emissions equipment to be installed. Actual location specifications and equipment placement are not to scale.

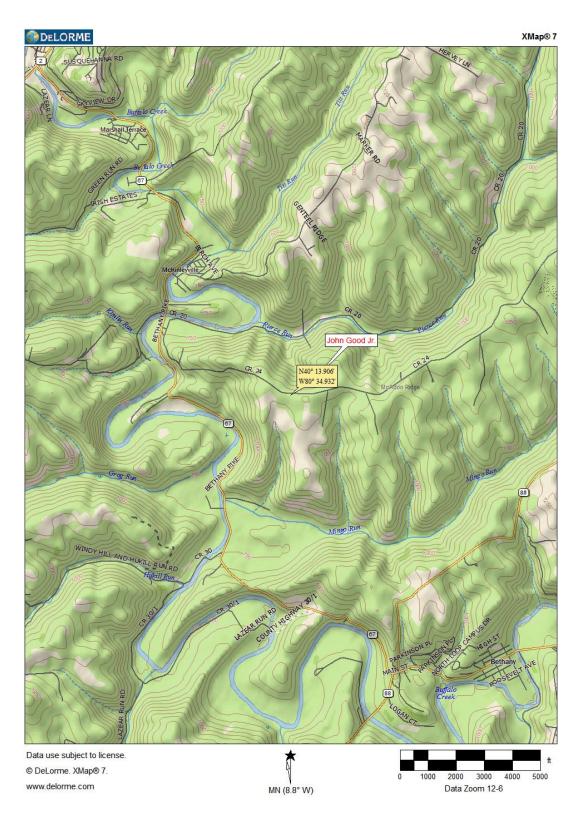


<u>NOTE</u>: Image is only a representation of production/emissions equipment. Actual location specifications and equipment placement are not to scale.

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Attachment F: Simple Plot Plan June 2017

ATTACHMENT G: AREA MAPS



SWN Production Company, LLC John Good Jr Pad Attachment G: Area Map June 2017



SWN Production Company, LLC John Good Jr Pad

Attachment G: Area Map with 300' Radius June 2017

ATTACHMENT H: G70-D SECTION APPLICABILITY FORM

ATTACHMENT H - G70-D SECTION APPLICABILITY FORM

General Permit G70-D Registration Section Applicability Form

General Permit G70-D was developed to allow qualified applicants to seek registration for a variety of sources. These sources include gas well affected facilities, storage vessels, gas production units, in-line heaters, heater treaters, glycol dehydration units and associated reboilers, pneumatic controllers, pneumatic pumps, reciprocating internal combustion engines (RICEs), tank truck/rail car loading, fugitive emissions, completion combustion devices, flares, enclosed combustion devices, and vapor recovery systems. All registered facilities will be subject to Sections 1.0, 2.0, 3.0, and 4.0.

General Permit G70-D allows the registrant to choose which sections of the permit they are seeking registration under. Therefore, please mark which additional sections that you are applying for registration under. If the applicant is seeking registration under multiple sections, please select all that apply. Please keep in mind, that if this registration is approved, the issued registration will state which sections will apply to your affected facility.

GENERAL PER	MIT G70-D APPLICABLE SECTIONS
⊠Section 5.0	Gas and Oil Well Affected Facility (NSPS, Subpart OOOO/OOOa)
⊠Section 6.0	Storage Vessels Containing Condensate and/or Produced Water ¹
□Section 7.0	Storage Vessel Affected Facility (NSPS, Subpart OOOO/OOOa)
⊠Section 8.0	Control Devices and Emission Reduction Devices not subject to NSPS Subpart OOOO/OOOoa and/or NESHAP Subpart HH
⊠Section 9.0	Small Heaters and Reboilers not subject to 40CFR60 Subpart Dc
□Section 10.0	Pneumatic Controllers Affected Facility (NSPS, Subpart OOOO/OOOa)
□Section 11.0	Pneumatic Pump Affected Facility (NSPS, Subpart OOOOa)
□Section 12.0	Fugitive Emissions GHG and VOC Standards (NSPS, Subpart OOOOa)
⊠Section 13.0	Reciprocating Internal Combustion Engines, Generator Engines
⊠Section 14.0	Tanker Truck/Rail Car Loading ²
□Section 15.0	Glycol Dehydration Units ³

¹ Applicants that are subject to Section 6 may also be subject to Section 7 if the applicant is subject to the NSPS, Subparts OOOO or OOOOa control requirements or the applicable control device requirements of Section 8.

² Applicants that are subject to Section 14 may also be subject to control device and emission reduction device requirements of Section 8.

³ Applicants that are subject to Section 15 may also be subject to the requirements of Section 9 (reboilers). Applicants that are subject to Section 15 may also be subject to control device and emission reduction device requirements of Section 8.

ATTACHMENT I: EMISSIONS UNITS/ERD TABLE

ATTACHMENT I - EMISSION UNITS/EMISSION REDUCTION DEVICES (ERD) TABLE

Include ALL emission units and air pollution control devices/ERDs that will be part of this permit application review. Do not include fugitive emission sources in this table. Deminimis storage tanks shall be listed in the Attachment L table. This information is required for all sources regardless of whether it is a construction, modification, or administrative update.

Emission Unit ID ¹	Emission Point ID ²	Emission Unit Description	Year Installed	Manufac. Date ³	Design Capacity	Type ⁴ and Date of Change	Control Device(s) ⁵	ERD(s) ⁶
EU-ENG1	EP-ENG1	145-hp Caterpillar G3306 NA Engine	TBD	after 1/1/2011	145-hp	New	NSCR	NSCR
LO LIVOT	LI LIVOI	THO TIP CULCIPINAL GOODO TWY ETIGING	100	after	140 HP	ITOW	INCOR	INOUN
EU-ENG2	EP-ENG2	145-hp Caterpillar G3306 NA Engine	TBD	1/1/2011	145-hp	New	NSCR	NSCR
EU-GPU1	EP-GPU1	1.0-mmBtu/hr GPU Burner	2013	N/A	1.0-mmBtu/hr	Existing	N/A	N/A
EU-GPU2	EP-GPU2	1.0-mmBtu/hr GPU Burner	2013	N/A	1.0-mmBtu/hr	Existing	N/A	N/A
EU-GPU3	EP-GPU3	1.0-mmBtu/hr GPU Burner	TBD	N/A	1.0-mmBtu/hr	New	N/A	N/A
EU-GPU4	EP-GPU4	1.0-mmBtu/hr GPU Burner	TBD	N/A	1.0-mmBtu/hr	New	N/A	N/A
EU-GPU5	EP-GPU5	1.0-mmBtu/hr GPU Burner	TBD	N/A	1.0-mmBtu/hr	New	N/A	N/A
EU-GPU6	EP-GPU6	1.0-mmBtu/hr GPU Burner	TBD	N/A	1.0-mmBtu/hr	New	N/A	N/A
EU-GPU7	EP-GPU7	1.0-mmBtu/hr GPU Burner	TBD	N/A	1.0-mmBtu/hr	New	N/A	N/A
EU-SH1	EP-SH1	1.5-mmBtu/hr Stabilizer Heater	TBD	N/A	1.5-mmBtu/hr	New	N/A	N/A
EU-SH2	EP-SH2	1.5-mmBtu/hr Stabilizer Heater	TBD	N/A	1.5-mmBtu/hr	New	N/A	N/A
EU-TANKS- COND	APC-COMB	Eight (8) 400-bbl Condensate Tanks Routed to Vapor Combustor	6 - 2013; 2 - TBD	N/A	400-bbl	Modification	APC-COMB	APC-COMB
EU-TANKS- PW	APC-COMB	Eight (8) 400-bbl Produced Water Tanks Routed to Vapor Combustor	6 - 2013; 2 - TBD	N/A	400-bbl	Modification	APC-COMB	APC-COMB
EU-LOAD- COND	APC-COMB	Condensate Truck Loading w/ Vapor Return Routed to Combustor	2013	N/A	33,994,275 gal/yr	Modification	Vapor Return and APC- COMB	Vapor Return and APC- COMB
EU-LOAD- PW	APC-COMB	Produced Water Truck Loading w/ Vapor Return Routed to Combustor	2013	N/A	22,894,129 gal/yr	Modification	Vapor Return and APC- COMB	Vapor Return and APC- COMB
APC-COMB	APC-COMB	30.0-mmBtu/hr Vapor Combustor	TBD	N/A	30.0-mmBtu/hr	New	N/A	N/A
EU-PILOTS	APC-COMB	Vapor Combustor Pilot	TBD	N/A	150-scfh	New	N/A	N/A
EU-FUG	EP-FUG	Fugitive Emissions	2013	N/A	N/A	Modification	N/A	N/A
EU-HR	EP-HR	Fugitive Haul Road Emissions	2013	N/A	N/A	Modification	N/A	N/A

¹ For Emission Units (or Sources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.

² For Emission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.

³ When required by rule

⁴ New, modification, removal, existing

⁵ For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

⁶ For ERDs use the following numbering system: 1D, 2D, 3D,... or other appropriate designation.

ATTACHMENT J: FUGITIVE EMISSIONS SUMMARY SHEET

Fugitive emissions at this site consist of haul road emissions, condensate and produced water loading operations, and equipment leaks.

			ATTACHME	NT J – FUGITIVE EMIS	SIONS SUM	MARY SHE	EET	
	Sources of fugitive emissions may include loading operations, equipment leaks, blowdown emissions, etc. Use extra pages for each associated source or equipment if necessary.							
	Source/Equip	ment: EU-F	FUG					
	Leak Detection Method Used		☐ Audible, visual, and olfactory (AVO) inspections	☐ Infrared (FLIR) cameras	☐ Other (plea	se describe)		⊠ None required
Compone	Closed		Source of	of Leak Factors	Stream type		sions (tpy)	
Туре	Vent System	Count		ther (specify))	(gas, liquid, etc.)	VOC	HAP	GHG (methane, CO ₂ e)
Pumps	☐ Yes ☐ No				☐ Gas ☐ Liquid ☐ Both			
Valves	☐ Yes ⊠ No	119 – ga 166 – LI			☐ Gas ☐ Liquid ☑ Both	1.20 – gas 3.82 – LL	0.01 – gas 0.26 – LL	66.83 – gas 1.02 – LL
Safety Rel Valves	ief ☐ Yes ⊠ No	41	EPA		⊠ Gas □ Liquid □ Both	0.81	0.01	45.02
Open Ende Lines	ed Ses				☐ Gas ☐ Liquid ☐ Both			
Sampling Connection	□ Yes □ No				☐ Gas ☐ Liquid ☐ Both			
Connection (Not sampli	I IXI NO	574	EPA		☐ Gas ☑ Liquid ☐ Both	1.11	0.08	0.30
Compresso	□ Yes ⊠ No	6	EPA		⊠ Gas □ Liquid □ Both	0.12	<0.01	6.59
Flanges	☐ Yes ⊠ No	474 – ga 42 – LL	s EPA		☐ Gas ☐ Liquid ☑ Both	0.41 – gas 0.04 – LL	<0.01 - gas <0.01 - LL	23.07 - gas 0.01 - LL
Other ¹	☐ Yes ☐ No				☐ Gas ☐ Liquid ☐ Both			
¹ Other eq	uipment types	nay include	compressor seals, relief valves,	diaphragms, drains, meters, etc.				
Please pro Equipment		ation of the	sources of fugitive emissions (e.	g. pigging operations, equipment	blowdowns, pneu	matic controller	rs, etc.):	

Please indicate if there are any closed vent bypasses (include component): N/A

Specify all equipment used in the closed vent system (e.g. VRU, ERD, thief hatches, tanker truck/rail car loading, etc.) N/A

TABLE 2-4. OIL AND GAS PRODUCTION OPERATIONS AVERAGE EMISSION FACTORS (kg/hr/source)

Equipment Type	Service ^a	Emission Factor (kg/hr/source)b
Valves	Gas Heavy Oil Light Oil Water/Oil	4.5E-03 8.4E-06 2.5E-03 9.8E-05
Pump seals	Gas Heavy Oil Light Oil Water/Oil	2.4E-03 NA 1.3E-02 2.4E-05
Others ^C	Gas Heavy Oil Light Oil Water/Oil	8.8E-03 3.2E-05 7.5E-03 1.4E-02
Connectors	Gas Heavy Oil Light Oil Water/Oil	2.0E-04 7.5E-06 2.1E-04 1.1E-04
Flanges	Gas Heavy Oil Light Oil Water/Oil	3.9E-04 3.9E-07 1.1E-04 2.9E-06
Open-ended lines	Gas Heavy Oil Light Oil Water/Oil	2.0E-03 1.4E-04 1.4E-03 2.5E-04

^aWater/Oil emission factors apply to water streams in oil service with a water content greater than 50%, from the point of origin to the point where the water content reaches 99%. For water streams with a water content greater than 99%, the emission rate is considered negligible.

bThese factors are for total organic compound emission rates (including non-VOC's such as methane and ethane) and apply to light crude, heavy crude, gas plant, gas production, and off shore facilities. "NA" indicates that not enough data were available to develop the indicated emission factor.

CThe "other" equipment type was derived from compressors, diaphrams, drains, dump arms, hatches, instruments, meters, pressure relief valves, polished rods, relief valves, and vents. This "other" equipment type should be applied for any equipment type other than connectors, flanges, open-ended lines, pumps, or valves.

ATTACHMENT K: GAS WELL AFFECTED FACILITY DATA SHEET

ATTACHMENT K - GAS WELL AFFECTED FACILITY DATA SHEET

Complete this data sheet if you are the owner or operator of a gas well affected facility for which construction, modification or reconstruction commenced after August 23, 2011. This form must be completed for natural gas well affected facilities regardless of when flowback operations occur (or have occurred).

API Number	Date of Flowback	Date of Well Completion	Green Completion and/or Combustion Device	Subject to OOOO or OOOOa?
047-009-001240 (5H)	9/25/2012	8/6/2012	Green Completion	0000
047-009-001130 (5H)	1/12/2013	8/6/2012	Green Completion	0000
PLANNED	TBD	TBD	TBD	TBD
PLANNED	TBD	TBD	TBD	TBD
PLANNED	TBD	TBD	TBD	TBD
PLANNED	TBD	TBD	TBD	TBD
PLANNED	TBD	TBD	TBD	TBD

Note: If future wells are planned and no API number is available please list as PLANNED.

If there are existing wells that commenced construction prior to August 23, 2011, please acknowledge as existing.

This is the same API (American Petroleum Institute) well number(s) provided in the well completion notification and as provided to the WVDEP, Office of Oil and Gas for the well permit. The API number may be provided on the application without the state code (047).

Every oil and gas well permitted in West Virginia since 1929 has been issued an API number. This API is used by agencies to identify and track oil and gas wells.

The API number has the following format: 047-001-00001

Where,

047 = State code. The state code for WV is 047.

001 = County Code. County codes are odd numbers, beginning with 001

(Barbour) and continuing to 109 (Wyoming).

00001= Well number. Each well will have a unique well number.

ATTACHMENT L: STORAGE VESSELS DATA SHEET

REPRESENTATIVE GAS ANALYSES
PROMAX PROCESS SIMULATION RESULTS

ATTACHMENT L - STORAGE VESSEL DATA SHEET

Complete this data sheet if you are the owner or operator of a storage vessel that contains condensate and/or produced water. This form must be completed for *each* new or modified bulk liquid storage vessel(s) that contains condensate and/or produced water. (If you have more than one (1) identical tank (i.e. 4-400 bbl condensate tanks), then you can list all on one (1) data sheet). Include gas sample analysis, flashing emissions, working and breathing losses, USEPA Tanks, simulation software (ProMax, E&P Tanks, HYSYS, etc.), and any other supporting documents where applicable.

The following information is REQUIRED:

- ☑ Composition of the representative sample used for the simulation
- - □ Temperature and pressure (inlet and outlet from separator(s))
 - ⊠ Simulation-predicted composition
- ☑ Resulting flash emission factor or flashing emissions from simulation
- ⊠ Working/breathing loss emissions from tanks and/or loading emissions if simulation is used to quantify those emissions

Additional information may be requested if necessary.

GENERAL INFORMATION (REQUIRED)

1. Bulk Storage Area Name	2. Tank Name			
Condensate Storage	Eight (8) 400-bbl Condensate Storage Tanks			
3. Emission Unit ID number	4. Emission Point ID number			
EU-TANKS-COND	APC-COMB			
5. Date Installed, Modified or Relocated (for existing tanks)	6. Type of change:			
Six – 2013; Two - TBD	\square New construction \square New stored material \boxtimes Other			
Was the tank manufactured after August 23, 2011 and on or	☐ Relocation			
before September 18, 2015?				
⊠ Yes □ No				
Was the tank manufactured after September 18, 2015?				
⊠ Yes □ No				
7A. Description of Tank Modification (if applicable) Update qu	antity of tanks, composition, and throughput.			
7B. Will more than one material be stored in this tank? <i>If so, a separate form must be completed for each material.</i>				
□ Yes ⊠ No				
7C. Was USEPA Tanks simulation software utilized?				
□ Yes ⊠ No				
If Yes, please provide the appropriate documentation and items	8-42 below are not required.			

Bulk Storage Area Name	2. Tank Name		
Produced Water Storage	Eight (8) 400-bbl Produced Water Storage Tanks		
3. Emission Unit ID number	4. Emission Point ID number		
EU-TANKS-PW	APC-COMB		
5. Date Installed, Modified or Relocated (for existing tanks)	6. Type of change:		
Six – 2012; Two - TBD	☐ New construction ☐ New stored material ☒ Other		
Was the tank manufactured after August 23, 2011 and on or	☐ Relocation		
before September 18, 2015?			
⊠ Yes □ No			
Was the tank manufactured after September 18, 2015?			
⊠ Yes □ No			
7A. Description of Tank Modification (if applicable) Update qu	antity of tanks, composition, and throughput.		
7B. Will more than one material be stored in this tank? If so, a s	separate form must be completed for each material.		
☐ Yes ⊠ No			
7C. Was USEPA Tanks simulation software utilized?			
☐ Yes			
If Yes, please provide the appropriate documentation and items	8-42 below are not required.		

STORAGE TANK DATA TABLE

List all deminimis storage tanks (i.e. lube oil, glycol, diesel etc.)

Source	St. 4. 2		W. 1. 4
ID #1	Status ²	Content ³	Volume ⁴
EU-TANKS- LUBEOIL	NEW	Lube Oil	50 gal
EU-TANKS- LUBEOIL	NEW	Lube Oil	50 gal
EU-TANKS- METHANOL	NEW	Methanol	50 gal
EU-TANKS- METHANOL	NEW	Methanol	50 gal
EU-TANKS- METHANOL	EXIST	Methanol	50 gal
EU-TANKS- METHANOL	EXIST	Methanol	50 gal
EU-TANKS- METHANOL	NEW	Methanol	50 gal
EU-TANKS- METHANOL	NEW	Methanol	50 gal
EU-TANKS- METHANOL	NEW	Methanol	50 gal
EU-TANKS- METHANOL	NEW	Methanol	50 gal
EU-TANKS- METHANOL	NEW	Methanol	50 gal

- 1. Enter the appropriate Source Identification Numbers (Source ID #) for each storage tank located at the well site. Tanks should be designated T01, T02, T03, etc.
- 2. Enter storage tank Status using the following:

EXIST Existing Equipment

NEW Installation of New Equipment

REM Equipment Removed

- 3. Enter storage tank content such as condensate, pipeline liquids, glycol (DEG or TEG), lube oil, diesel, mercaptan etc.
- 4. Enter the maximum design storage tank volume in gallons.

TABLE 1-B

COMPOSITIONAL ANALYSIS OF THE SEPARATOR GAS, OIL AND MATHEMATICALLY RECOMBINED WELLSTREAM THROUGH C_{11+}

SEPARATOR GOR.....: 4381 Scf/Sep Bbl

SEPARATOR PRESSURE...... 215 psig SEPARATOR TEMPERATURE.....: 55 °F

	SEPARA	TOR GAS	SEPARA	TOR OIL	WELLS	TREAM
		*		Liquid		*
Component	Mole%	GPM	Mole %	Volume %	Mole %	GPM
Hydrogen Sulfide	0.000	0.000	0.000	0.000	0.000	0.000
Nitrogen	0.496	0.000	0.015	0.004	0.405	0.000
Carbon Dioxide	0.133	0.000	0.010	0.011	0.110	0.000
Methane	70.754	0.000	5.084	0.773	58.285	0.000
Ethane	18.380	4.955	9.419	6.156	16.678	4.496
Propane	7.198	1.999	13.438	9.048	8.383	2.328
Iso-butane	0.590	0.195	2.701	2.160	0.991	0.327
N-butane	1.711	0.544	11.641	8.969	3.596	1.143
2-2 Dimethylpropane	0.000	0.000	0.173	0.162	0.033	0.013
Iso-pentane	0.211	0.078	3.777	3.376	0.888	0.327
N-pentane	0.317	0.116	7.673	6.798	1.714	0.626
2-2 Dimethylbutane	0.003	0.001	0.087	0.088	0.019	0.008
Cyclopentane	0.003	0.001	0.000	0.000	0.002	0.001
2-3 Dimethylbutane	0.005	0.002	0.246	0.246	0.051	0.021
2 Methylpentane	0.039	0.016	2.037	2.067	0.418	0.175
3 Methylpentane	0.022	0.009	1.250	1.248	0.255	0.105
Other Hexanes	0.000	0.000	0.000	0.000	0.000	0.000
n-Hexane	0.067	0.028	4.799	4.823	0.965	0.400
Methylcyclopentane	0.005	0.002	0.578	0.500	0.114	0.041
Benzene	0.001	0.000	0.067	0.046	0.014	0.004
Cyclohexane	0.006	0.002	0.688	0.573	0.136	0.047
2-Methylhexane	0.007	0.003	1.483	1.685	0.287	0.135
3-Methylhexane	0.007	0.003	1.361	1.527	0.264	0.122
2,2,4 Trimethylpentane	0.000	0.000	0.000	0.000	0.000	0.000
Other Heptanes	0.007	0.003	0.628	0.680	0.125	0.056
n-Heptane	0.014	0.007	3.405	3.839	0.658	0.306
Methylcyclohexane	0.006	0.002	1.433	1.408	0.277	0.112
Toluene	0.001	0.000	0.271	0.222	0.052	0.018
Other C-8's	0.008	0.004	4.169	4.862	0.798	0.384
n-Octane	0.003	0.002	2.165	2.710	0.413	0.214
Ethylbenzene	0.000	0.000	0.283	0.267	0.054	0.021
M&P-Xylene	0.001	0.000	0.288	0.273	0.055	0.022
O-Xylene	0.000	0.000	0.123	0.114	0.023	0.009
Other C-9's	0.002	0.001	2.999	3.907	0.571	0.307
n-Nonane	0.001	0.001	1.367	1.880	0.260	0.148
Other C10's	0.000	0.000	2.719	3.893	0.516	0.305
n-Decane	0.000	0.000	0.845	1.268	0.160	0.099
Undecanes Plus	0.002	0.001	12.778	24.418	2.428	1.913
TOTAL	100.000	7.974	100.000	100.000	100.000	14.229

TABLE 1-B

COMPOSITIONAL ANALYSIS OF THE SEPARATOR GAS, OIL AND MATHEMATICALLY RECOMBINED WELLSTREAM THROUGH C_{11+}

SEPARATOR GOR...... 4381 Scf/Sep Bbl

SEPARATOR PRESSURE...... 215 psig SEPARATOR TEMPERATURE.....: 55 °F

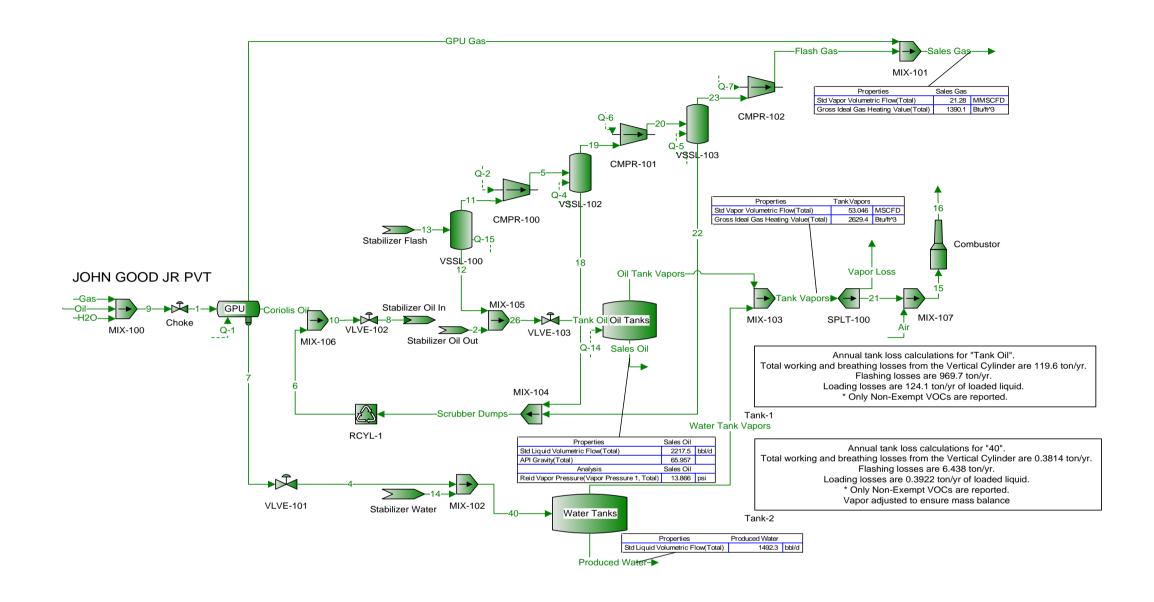
UNDECANES PLUS (C ₁₁₊) FRACTION CHARACTERISTICS					
Molecular Vapor Gross Heating Value Specific Gravity Weight Volume					
COMPONENT	°API	**	lb/lb-mole	Scf/Gal	***
Gas	N/A	0.8250	156.000	16.558	8,400
Oil	41.949	0.8158	201.300	12.689	130,622
Wellstream	N/A	0.8158	201.270	12.691	N/A

TOTAL SAMPLE CHARACTERISTICS						
	Molecular Vapor Gross Heating Value					
	Specific	Specific Gravity		Volume	Dry	Saturated
COMPONENT	°API	**	lb/lb-mole	Scf/Gal	***	***
Gas	N/A	0.7683	22.159	125.402	1,348	1,325
Oil	77.724	0.6763	87.330	24.247	N/A	114,325
Wellstream	N/A	1.1924	34.534	55.616	N/A	N/A

^{*} GPM (gallons per Mscf) determined at 14.85 psia and 60 °F

^{**} Gas specific gravity and wellstream specific gravity determined relative to air (SG=1.000). Oil specific gravity determined relative to water (SG=1.000).

^{***} Gross Heating Value units for gas (real basis) and oil are BTU/Scf and BTU/Gal, respectively.



ProMax AP-42 Emissions Report Condensate Annual Emissions Vertical Cylinder

Components	Working Losses (ton/yr)	Breathing Losses (ton/yr)	Total Losses (ton/yr)
Mixture	57.22	62.35	119.6
C3	23.63	25.75	49.37
iC4	4.353	4.743	9.096
nC4	15.55	16.94	32.48
2,2-Dimethylbutane	0.01517	0.01653	0.0317
iC5	3.368	3.67	7.038
nC5	5.509	6.003	11.51
2,2-Dimethylpropane	0.1346	0.1467	0.2813
Cyclopentane	0.008069	0.008792	0.01686
2,3-Dimethylbutane	0.1168	0.1273	0.2442
2-Methylpentane	0.8779	0.9566	1.834
3-Methylpentane	0.492	0.5361	1.028
C6	1.547	1.685	3.232
Methylcyclopentane	0.1588	0.173	0.3318
Benzene	0.01208	0.01317	0.02525
Cyclohexane	0.1396	0.1521	0.2917
2-Methylhexane	0.07102	0.07738	0.1484
3-Methylhexane	0.2152	0.2345	0.4497
2,2,4-Trimethylpentane	0	0	0.4437
C7	0.4774	0.5202	0.9977
Methylcyclohexane	0.168	0.1831	0.3512
Toluene	0.01814	0.01976	0.0379
C8	0.2617	0.2851	0.5468
Ethylbenzene	0.007528	0.008203	0.01573
m-Xylene	0.007326	0.01017	0.01951
o-Xylene	0.002169	0.002363	0.004532
C9	0.06112	0.0666	0.1277
C10	0.01668	0.01817	0.03485
C11	0.004305	0.004691	0.008997
C12	0.001094	0.001192	0.002287
C13	0.0002937	0.0003201	0.0006138
C14	7.92E-05	8.63E-05	0.0001655
C15	2.20E-05	2.40E-05	4.60E-05
C16	5.11E-06	5.57E-06	1.07E-05
C17	1.26E-06	1.38E-06	2.64E-06
C18	4.20E-07	4.58E-07	8.78E-07
C19	8.85E-08	9.65E-08	1.85E-07
C20	2.44E-08	2.66E-08	5.10E-08
C21	6.13E-09	6.68E-09	1.28E-08
C22	1.80E-09	1.96E-09	3.75E-09
C23	4.26E-10	4.64E-10	8.90E-10
C24	1.02E-10	1.11E-10	2.14E-10
C25	3.31E-11	3.60E-11	6.91E-11
C26	1.69E-11	1.84E-11	3.52E-11
C27	1.76E-12	1.92E-12	3.67E-12
C28	3.03E-13	3.31E-13	6.34E-13
C29	1.20E-13	1.31E-13	2.51E-13
C30	7.61E-14	8.29E-14	1.59E-13
		5.252	

Flashing Emissions Report
Condensate Annual Emissions
Tank flashed at the daily maximum surface temperature (72.3 °F) and the atmospheric pressure of Pittsburgh, Pennsylvania (14.11 psia)

•	
Components	Flashing Losses (ton/yr)
Mixture	969.7
C3	376.9
iC4	74.52
nC4	265.9
2,2-Dimethylbutane	0.2613
iC5	59.85
nC5	99.69
2,2-Dimethylpropane	2.375
Cyclopentane	0.1638
2,3-Dimethylbutane	2.064
2-Methylpentane	15.97
3-Methylpentane	8.998
C6	27.45
Methylcyclopentane	3.3
Benzene	0.3583
Cyclohexane	3.057
2-Methylhexane	4.755
3-Methylhexane	3.998
2,2,4-Trimethylpentane	0
C7	9.117
Methylcyclohexane	3.275
Toluene	0.5254
C8	5.09
Ethylbenzene	0.2004
m-Xylene	0.1908
o-Xylene	0.06977
C9	1.197
C10	0.3481
C11	0.09206
C12	0.02483
C13	0.02403
C14	0.007027
C15	0.002020
C16	0.0003673
C17	4.82E-05
C18	4.82E-05
C19	5.04E-06
C20	1.18E-06
C21	3.15E-07
C22	1.30E-07
C23	3.38E-08
C24	
C25	5.89E-09
	2.05E-09
C26	8.05E-10
C27	6.89E-11
C28	5.06E-11
C29	2.06E-11
C30	5.71E-11

Components	Working Losses (ton/yr)	Breathing Losses (ton/yr)	Total Losses (ton/yr)
Mixture	0.2142	0.1672	0.3814
C3	0.1142	0.08911	0.2033
iC4	0.006918	0.005398	0.01232
nC4	0.03545	0.02766	0.06311
2,2-Dimethylbutane	2.30E-06	1.80E-06	4.10E-06
iC5	0.003427	0.002674	0.006101
nC5	0.0008778	0.0006849	0.001563
2,2-Dimethylpropane	6.98E-05	5.45E-05	0.0001243
Cyclopentane	0.000225	0.0001756	0.0004005
2,3-Dimethylbutane	0.0001195	9.33E-05	0.0002128
2-Methylpentane	0.0002542	0.0001983	0.0004525
3-Methylpentane	0.0008417	0.0006567	0.001498
C6	0.0001074	8.38E-05	0.0001912
Methylcyclopentane	0.0008212	0.0006407	0.001462
Benzene	0.01271	0.009918	0.02263
Cyclohexane	0.003627	0.00283	0.006458
2-Methylhexane	3.77E-05	2.94E-05	6.71E-05
3-Methylhexane	4.56E-05	3.56E-05	8.12E-05
2,2,4-Trimethylpentane	0	0	0
C7	2.01E-05	1.57E-05	3.58E-05
Methylcyclohexane	0.0008208	0.0006404	0.001461
Toluene	0.01828	0.01426	0.03254
C8	2.02E-06	1.58E-06	3.59E-06
Ethylbenzene	0.006672	0.005206	0.01188
m-Xylene	0.006264	0.004887	0.01115
o-Xylene	0.002423	0.00189	0.004313
C9	5.32E-07	4.15E-07	9.47E-07
C10	1.32E-08	1.03E-08	2.35E-08
C11	3.87E-09	3.02E-09	6.89E-09
C12	1.52E-08	1.19E-08	2.71E-08
C13	2.77E-08	2.17E-08	4.94E-08
C14	3.37E-08	2.63E-08	6.00E-08
C15	3.97E-08	3.10E-08	7.07E-08
C16	7.86E-08	6.13E-08	1.40E-07
C17	1.41E-07	1.10E-07	2.52E-07
C18	2.13E-07	1.66E-07	3.79E-07
C19	1.11E-07	8.63E-08	1.97E-07
C20	2.87E-08	2.24E-08	5.12E-08
C21	7.74E-09	6.04E-09	1.38E-08
C22	3.10E-09	2.42E-09	5.51E-09
C23	7.64E-10	5.96E-10	1.36E-09
C24	1.30E-10	1.01E-10	2.31E-10
C25	4.28E-11	3.34E-11	7.62E-11
C26	1.59E-11	1.24E-11	2.83E-11
C27	1.30E-12	1.01E-12	2.31E-12
C28	8.98E-13	7.00E-13	1.60E-12
C29	3.61E-13	2.82E-13	6.42E-13
C30	9.40E-13	7.33E-13	1.67E-12
	332 10		12

Flashing Emissions Report
Water Annual Emissions
Tank flashed at the daily maximum surface temperature (70.83 °F) and the atmospheric pressure of Pittsburgh, Pennsylvania (14.11 psia)

_	
Components	Flashing Losses (ton/yr)
Mixture	6.438
C3	4.13
iC4	0.3477
nC4	1.4
2,2-Dimethylbutane	0.0003134
iC5	0.187
nC5	0.1255
2,2-Dimethylpropane	0.005666
Cyclopentane	0.002164
2,3-Dimethylbutane	0.006133
2-Methylpentane	0.02578
3-Methylpentane	0.03416
C6	0.02218
Methylcyclopentane	0.01988
Benzene	0.01555
Cyclohexane	0.03711
2-Methylhexane	0.005303
•	
3-Methylhexane	0.005321
2,2,4-Trimethylpentane	0
C7	0.005509
Methylcyclohexane	0.01971
Toluene	0.02231
C8	0.001327
Ethylbenzene	0.00831
m-Xylene	0.007621
o-Xylene	0.003006
C9	0.0003183
C10	2.75E-05
C11	7.54E-06
C12	7.59E-06
C13	5.44E-06
C14	3.19E-06
C15	1.81E-06
C16	1.27E-06
C17	7.91E-07
C18	4.75E-07
C19	1.71E-07
C20	4.56E-08
C21	1.25E-08
C22	5.14E-09
C23	1.32E-09
C24	2.29E-10
C25	7.83E-11
C26	3.01E-11
C27	2.55E-12
C28	2.55E-12 1.82E-12
C29	7.40E-13
C30	2.00E-12

ATTACHMENT M: NATURAL GAS FIRED FUEL BURNING UNITS DATA SHEET

AP-42 EMISSION FACTORS

ATTACHMENT M – SMALL HEATERS AND REBOILERS NOT SUBJECT TO 40CFR60 SUBPART DC DATA SHEET

Complete this data sheet for each small heater and reboiler not subject to 40CFR60 Subpart Dc at the facility. The Maximum Design Heat Input (MDHI) must be less than 10 MMBTU/hr.

Emission Unit ID# ¹	Emission Point ID# ²	Emission Unit Description (manufacturer, model #)	Year Installed/ Modified	Type ³ and Date of Change	Maximum Design Heat Input (MMBTU/hr) ⁴	Fuel Heating Value (BTU/scf) ⁵
EU-GPU1	EP-GPU1	Gas Production Unit Burner	2013	EXIST	1.0	905
EU-GPU2	EP-GPU2	Gas Production Unit Burner	2013	EXIST	1.0	905
EU-GPU3	EP-GPU3	Gas Production Unit Burner	TBD	NEW	1.0	905
EU-GPU4	EP-GPU4	Gas Production Unit Burner	TBD	NEW	1.0	905
EU-GPU5	EP-GPU5	Gas Production Unit Burner	TBD	NEW	1.0	905
EU-GPU6	EP-GPU6	Gas Production Unit Burner	TBD	NEW	1.0	905
EU-GPU7	EP-GPU7	Gas Production Unit Burner	TBD	NEW	1.0	905
EU-SH1	EP-SH1	Stabilizer Heater	TBD	NEW	1.5	905
EU-SH2	EP-SH2	Stabilizer Heater	TBD	NEW	1.5	905

- Enter the appropriate Emission Unit (or Source) identification number for each fuel burning unit located at the production pad. Gas Producing Unit Burners should be designated GPU-1, GPU-2, etc. Heater Treaters should be designated HT-1, HT-2, etc. Heaters or Line Heaters should be designated LH-1, LH-2, etc. For sources, use 1S, 2S, 3S...or other appropriate designation. Enter glycol dehydration unit Reboiler Vent data on the Glycol Dehydration Unit Data Sheet.
- Enter the appropriate Emission Point identification numbers for each fuel burning unit located at the production pad. Gas Producing Unit Burners should be designated GPU-1, GPU-2, etc. Heater Treaters should be designated HT-1, HT-2, etc. Heaters or Line Heaters should be designated LH-1, LH-2, etc. For emission points, use 1E, 2E, 3E...or other appropriate designation.
- New, modification, removal
- Enter design heat input capacity in MMBtu/hr.
- ⁵ Enter the fuel heating value in BTU/standard cubic foot.

Table 1.4-1. EMISSION FACTORS FOR NITROGEN OXIDES (NO_x) AND CARBON MONOXIDE (CO) FROM NATURAL GAS COMBUSTION^a

	NO _x ^b			СО
Combustor Type (MMBtu/hr Heat Input) [SCC]	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
Large Wall-Fired Boilers (>100) [1-01-006-01, 1-02-006-01, 1-03-006-01]				
Uncontrolled (Pre-NSPS) ^c	280	A	84	В
Uncontrolled (Post-NSPS) ^c	190	A	84	В
Controlled - Low NO _x burners	140	A	84	В
Controlled - Flue gas recirculation	100	D	84	В
Small Boilers (<100) [1-01-006-02, 1-02-006-02, 1-03-006-02, 1-03-006-03]				
Uncontrolled	100	В	84	В
Controlled - Low NO _x burners	50	D	84	В
Controlled - Low NO _x burners/Flue gas recirculation	32	C	84	В
Tangential-Fired Boilers (All Sizes) [1-01-006-04]				
Uncontrolled	170	A	24	C
Controlled - Flue gas recirculation	76	D	98	D
Residential Furnaces (<0.3) [No SCC]				
Uncontrolled	94	В	40	В

^a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. To convert from lb/10 ⁶ scf to kg/10⁶ m³, multiply by 16. Emission factors are based on an average natural gas higher heating value of 1,020 Btu/scf. To convert from 1b/10 ⁶ scf to lb/MMBtu, divide by 1,020. The emission factors in this table may be converted to other natural gas heating values by multiplying the given emission factor by the ratio of the specified heating value to this average heating value. SCC = Source Classification Code. ND = no data. NA = not applicable.

Expressed as NO₂. For large and small wall fired boilers with SNCR control, apply a 24 percent reduction to the appropriate NO_X emission factor. For

tangential-fired boilers with SNCR control, apply a 13 percent reduction to the appropriate NO x emission factor.

NSPS=New Source Performance Standard as defined in 40 CFR 60 Subparts D and Db. Post-NSPS units are boilers with greater than 250 MMBtu/hr of heat input that commenced construction modification, or reconstruction after August 17, 1971, and units with heat input capacities between 100 and 250 MMBtu/hr that commenced construction modification, or reconstruction after June 19, 1984.

TABLE 1.4-3. EMISSION FACTORS FOR SPECIATED ORGANIC COMPOUNDS FROM NATURAL GAS COMBUSTION $^{\rm a}$

CAS No.	Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
91-57-6	2-Methylnaphthalene ^{b, c}	2.4E-05	D
56-49-5	3-Methylchloranthrene ^{b, c}	<1.8E-06	E
	7,12-Dimethylbenz(a)anthracene ^{b,c}	<1.6E-05	E
83-32-9	Acenaphthene ^{b,c}	<1.8E-06	E
203-96-8	Acenaphthylene ^{b,c}	<1.8E-06	E
120-12-7	Anthracene ^{b,c}	<2.4E-06	E
56-55-3	Benz(a)anthracene ^{b,c}	<1.8E-06	E
71-43-2	Benzene ^b	2.1E-03	В
50-32-8	Benzo(a)pyrene ^{b,c}	<1.2E-06	E
205-99-2	Benzo(b)fluoranthene ^{b,c}	<1.8E-06	E
191-24-2	Benzo(g,h,i)perylene ^{b,c}	<1.2E-06	Е
205-82-3	Benzo(k)fluoranthene ^{b,c}	<1.8E-06	Е
106-97-8	Butane	2.1E+00	Е
218-01-9	Chrysene ^{b,c}	<1.8E-06	Е
53-70-3	Dibenzo(a,h)anthracene ^{b,c}	<1.2E-06	Е
25321-22-6	Dichlorobenzene ^b	1.2E-03	E
74-84-0	Ethane	3.1E+00	Е
206-44-0	Fluoranthene ^{b,c}	3.0E-06	Е
86-73-7	Fluorene ^{b,c}	2.8E-06	Е
50-00-0	Formaldehyde ^b	7.5E-02	В
110-54-3	Hexane ^b	1.8E+00	Е
193-39-5	Indeno(1,2,3-cd)pyrene ^{b,c}	<1.8E-06	Е
91-20-3	Naphthalene ^b	6.1E-04	E
109-66-0	Pentane	2.6E+00	E
85-01-8	Phenanathrene ^{b,c}	1.7E-05	D

TABLE 1.4-3. EMISSION FACTORS FOR SPECIATED ORGANIC COMPOUNDS FROM NATURAL GAS COMBUSTION (Continued)

CAS No.	Pollutant	Emission Factor (lb/10 ⁶ scf)	Emission Factor Rating
74-98-6	Propane	1.6E+00	Е
129-00-0	Pyrene ^{b, c}	5.0E-06	E
108-88-3	Toluene ^b	3.4E-03	С

^a Reference 11. Units are in pounds of pollutant per million standard cubic feet of natural gas fired. Data are for all natural gas combustion sources. To convert from lb/10⁶ scf to kg/10⁶ m³, multiply by 16. To convert from 1b/10⁶ scf to lb/MMBtu, divide by 1,020. Emission Factors preceded with a less-than symbol are based on method detection limits.

^b Hazardous Air Pollutant (HAP) as defined by Section 112(b) of the Clean Air Act.

^c HAP because it is Polycyclic Organic Matter (POM). POM is a HAP as defined by Section 112(b) of the Clean Air Act.

^d The sum of individual organic compounds may exceed the VOC and TOC emission factors due to differences in test methods and the availability of test data for each pollutant.

ATTACHMENT N: INTERNAL COMBUSTION ENGINE DATA SHEETS

ENGINE SPECIFICATION SHEETS
AP-42 AND EPA EMISSION FACTORS

ATTACHMENT N - INTERNAL COMBUSTION ENGINE DATA SHEET

Complete this data sheet for each internal combustion engine at the facility. Include manufacturer performance data sheet(s) or any other supporting document if applicable. Use extra pages if necessary. *Generator(s) and microturbine generator(s) shall also use this form.*

	<i>j</i>						
Emission Unit I	D#1	EU-F	ENG1	EU-ENG2			
Engine Manufac	turer/Model	Caterpillar G3306 NA		Caterpillar G3306 NA			
Manufacturers F	Rated bhp/rpm	145-hp/1	,800-rpm	145-hp/1,800-rpm			
Source Status ²		N	S	N	1S		
Date Installed/ Modified/Remov	ved/Relocated ³	Ti	BD	TI	BD		
Engine Manufac		After 1	/1/2011	After 1	/1/2011		
Check all applicable Federal Rules for the engine (include EPA Certificate of Conformity if applicable) ⁵			ed? ubpart IIII ed? ubpart ZZZZ	□JJJJ Certified? □40CFR60 Subpart IIII □IIII Certified? art ZZZZ □ MESHAP ZZZZ/ NSPS JJJJ Window		□40CFR60 Subpart JJJJ □JJJJ Certified? □40CFR60 Subpart IIII □IIII Certified? □40CFR63 Subpart ZZZZ □ NESHAP ZZZZ/ NSPS JJJJ Window □ NESHAP ZZZZ Remote Sources	
Engine Type ⁶		4S	RB	4S	RB		
APCD Type ⁷		NS	CR	NSCR			
Fuel Type ⁸		P	Q	PQ			
H ₂ S (gr/100 scf)	2S (gr/100 scf) Ne		igible	ble Negligible			
Operating bhp/r	Operating bhp/rpm		,800-rpm	145-hp/1,800-rpm			
BSFC (BTU/bhp	FC (BTU/bhp-hr) 8,625		525	8,625			
Hourly Fuel Thi	oughput	1,382 ft³/hr gal/hr		1,382 ft ³ /hr gal/hr			³/hr l/hr
Annual Fuel The (Must use 8,760 emergency gene	hrs/yr unless	12.11 MMft³/yr gal/yr		12.11 MMft³/yr gal/yr		MMft³/yr gal/yr	
Fuel Usage or H Operation Meter		Yes 🗆	No ⊠	Yes □	No ⊠	Yes □	No 🗆
Calculation Methodology ⁹	Pollutant ¹⁰	Hourly PTE (lb/hr) ¹¹	Annual PTE (tons/year)	Hourly PTE (lb/hr) 11	Annual PTE (tons/year)	Hourly PTE (lb/hr) 11	Annual PTE (tons/year)
MD	NO _x	0.32	1.40	0.32	1.40		
MD	СО	0.64	2.80	0.64	2.80		
MD	VOC	0.31	1.36	0.31	1.36		
AP	SO ₂	< 0.01	< 0.01	< 0.01	< 0.01		
AP	PM ₁₀	0.01	0.05	0.01	0.05		
MD	Formaldehyde	0.09	0.38	0.09	0.38		
AP	Total HAPs	0.10	0.44	0.10	0.44		
MD and EPA	GHG (CO ₂ e)	155.19	679.73	155.19	679.73		

¹ Enter the appropriate Source Identification Number for each natural gas-fueled reciprocating internal combustion engine/generator engine located at the well site. Multiple engines should be designated CE-1, CE-2, CE-3 etc. Generator engines should be designated GE-1, GE-3, etc. Microturbine generator engines should be designated MT-1, MT-2, MT-3 etc. If more than three (3) engines exist, please use additional sheets.

2 Enter the Source Status using the following codes:

NS Construction of New Source (installation) ES Existing Source
MS Modification of Existing Source RS Relocated Source

REM Removal of Source

- 3 Enter the date (or anticipated date) of the engine's installation (construction of source), modification, relocation or removal.
- 4 Enter the date that the engine was manufactured, modified or reconstructed.
- Is the engine a certified stationary spark ignition internal combustion engine according to 40CFR60 Subpart IIII/JJJJ? If so, the engine and control device must be operated and maintained in accordance with the manufacturer's emission-related written instructions. You must keep records of conducted maintenance to demonstrate compliance, but no performance testing is required. If the certified engine is not operated and maintained in accordance with the manufacturer's emission-related written instructions, the engine will be considered a non-certified engine and you must demonstrate compliance as appropriate.

Provide a manufacturer's data sheet for all engines being registered.

6 Enter the Engine Type designation(s) using the following codes:

2SLB Two Stroke Lean Burn 4SRB Four Stroke Rich Burn

4SLB Four Stroke Lean Burn

7 Enter the Air Pollution Control Device (APCD) type designation(s) using the following codes:

A/F Air/Fuel Ratio IR Ignition Retard

HEIS High Energy Ignition System SIPC Screw-in Precombustion Chambers
PSC Prestratified Charge LEC Low Emission Combustion

NSCR Rich Burn & Non-Selective Catalytic Reduction OxCat Oxidation Catalyst

SCR Lean Burn & Selective Catalytic Reduction

8 Enter the Fuel Type using the following codes:

PQ Pipeline Quality Natural Gas RG Raw Natural Gas /Production Gas D Diesel

9 Enter the Potential Emissions Data Reference designation using the following codes. Attach all reference data used.

MD Manufacturer's Data AP AP-42

GR GRI-HAPCalcTM OT Other (please list)

- Enter each engine's Potential to Emit (PTE) for the listed regulated pollutants in pounds per hour and tons per year. PTE shall be calculated at manufacturer's rated brake horsepower and may reflect reduction efficiencies of listed Air Pollution Control Devices. Emergency generator engines may use 500 hours of operation when calculating PTE. PTE data from this data sheet shall be incorporated in the *Emissions Summary Sheet*.
- 11 PTE for engines shall be calculated from manufacturer's data unless unavailable.

Engine Air Pollution Control Device (Emission Unit ID# APC-NSCR-ENG-1, ENG-2 use extra pages as necessary)

(-,
Air Pollution Control Device Mar Yes ⊠	nufacturer's Data Sheet included? No 🏻
⊠ NSCR □ SCR	☐ Oxidation Catalyst
Provide details of process control used for proper mixing/cont	rol of reducing agent with gas stream:
Manufacturer: N/A	Model #: N/A
Design Operating Temperature: 1,101 °F	Design gas volume: 678 scfm
Service life of catalyst:	Provide manufacturer data? ⊠Yes □ No
Volume of gas handled: acfm at °F	Operating temperature range for NSCR/Ox Cat: From 600 °F to 1,250 °F
Reducing agent used, if any:	Ammonia slip (ppm):
Pressure drop against catalyst bed (delta P): inches of	H ₂ O
Provide description of warning/alarm system that protects unit	t when operation is not meeting design conditions:
Is temperature and pressure drop of catalyst required to be mo \square Yes \boxtimes No	nitored per 40CFR63 Subpart ZZZZ?
How often is catalyst recommended or required to be replaced	(hours of operation)?
How often is performance test required? ☐ Initial ☐ Annual ☐ Every 8,760 hours of operation ☐ Field Testing Required ☐ No performance test required. If so, why (please list any numbers)	naintenance required and the applicable sections in

G3306 NA

SET POINT TIMING:

GAS ENGINE SITE SPECIFIC TECHNICAL DATA



ENGINE SPEED (rpm): COMPRESSION RATIO: JACKET WATER OUTLET (°F): COOLING SYSTEM: IGNITION SYSTEM: **EXHAUST MANIFOLD:** COMBUSTION: EXHAUST 02 EMISSION LEVEL %: 1800 10,5:1 210 JW+OC MAG WC

FUEL SYSTEM:

LPG IMPCO WITH CUSTOMER SUPPLIED AIR FUEL RATIO CONTROL

SITE CONDITIONS:

FUEL: FUEL PRESSURE RANGE(psig): FUEL METHANE NUMBER: FUEL LHV (Btu/scf):

Nat Gas 1.5-10.0 84.8

Catalyst 0.5 ALTITUDE(ft): 30.0

905 500

MAXIMUM INLET AIR TEMPERATURE(°F):

77

145 hhp@1800rpm

			MAXIMUM	SITE DATING	G AT MAXIMU	MIND ET ALE
			RATING		EMPERATUR	
RATING	NOTES	LOAD	100%	100%	75%	50%
ENGINE POWER	(1)	bhp	145	145	109	72
INLET AIR TEMPERATURE		°F	77	77	77	77
ENGINE DATA						
FUEL CONSUMPTION (LHV)	(2)	Btu/bhp-hr	7775	7775	8318	9509
FUEL CONSUMPTION (HHV)	(2)	Btu/bhp-hr	8625	8625	9227	10548
AIR FLOW	(3)(4)	lb/hr	922	922	739	556
AIR FLOW WET (77°F, 14.7 psia)	(3)(4)	scfm	208	208	167	125
INLET MANIFOLD PRESSURE	(5)	in Hg(abs)	26.2	26.2	21.8	17.6
EXHAUST STACK TEMPERATURE	(6)	°F	1101	1101	1067	1037
EXHAUST GAS FLOW (@ stack temp, 14.5 psia)	(7)(4)	ft3/min	678	678	532	393
EXHAUST GAS MASS FLOW	(7)(4)	lb/hr	978	978	784	590
EMISSIONS DATA						
EMISSIONS DATA	(0)	a fla la calla a	13.47	40.47	12.15	0.70
NOx (as NO2)	(8)	g/bhp-hr		13.47		9.76
CO	(8)	g/bhp-hr	13.47	13.47	11.44	9.56
THC (mol. wt. of 15.84)	(8)	g/bhp-hr	2.20	2.20	2.49	3.22
NMHC (mol. wt. of 15.84)	(8)	g/bhp-hr	0.33	0.33	0.37	0.48
NMNEHC (VOCs) (mol. wt. of 15.84)	(8)(9)	g/bhp-hr	0.22	0.22	0.25	0.32
HCHO (Formaldehyde)	(8)	g/bhp-hr	0.27	0.27	0.31	0.33
CO2	(8)	g/bhp-hr	485	485	525	601
EXHAUST OXYGEN	(10)	% DRY	0.5	0.5	0.5	0.5
HEAT REJECTION						
HEAT REJ. TO JACKET WATER (JW)	(11)	Btu/min	6049	6049	5237	4455
HEAT REJ. TO ATMOSPHERE	(11)	Btu/min	751	751	602	459
HEAT REJ. TO LUBE OIL (OC)	(11)	Btu/min	990	990	857	729

(12)

Btu/min

7842

CONDITIONS AND DEFINITIONS
Engine rating obtained and presented in accordance with ISO 3046/1, adjusted for fuel, site altitude and site inlet air temperature. 100% rating at maximum inlet air temperature is the maximum engine capability for the specified fuel at site altitude and maximum site inlet air temperature. Max. rating is the maximum capability for the specified fuel at site altitude and reduced inlet air temperature. Lowest load point is the lowest continuous duty operating load allowed. No overload permitted at rating shown.

For notes information consult page three.

PREPARED BY:

Data generated by Gas Engine Rating Pro Version 3.04.00 Ref. Data Set DM5053-07-000, Printed 31Jan2011

HEAT EXCHANGER SIZING CRITERIA

TOTAL JACKET WATER CIRCUIT (JW+OC)





Prepared For:

Jason Stinson
MIDCON COMPRESSION, LP

MANUFACTURED ON OR AFTER 1/1/2011

INFORMATION PROVIDED BY CATERPILLAR

G3306 NA Engine: 145 Horsepower: 1800 RPM: Compression Ratio: 10.5:1 678 CFM **Exhaust Flow Rate:** 1101 °F Exhaust Temperature: Reference: DM5053-07 Natural Gas Fuel: Annual Operating Hours: 8760

Uncontrolled Emissions

 NOx:
 13.47 g/bhp-hr

 CO:
 13.47 g/bhp-hr

 THC:
 2.20 g/bhp-hr

 NMHC:
 0.33 g/bhp-hr

 NMNEHC:
 0.22 g/bhp-hr

 HCHO:
 0.27 g/bhp-hr

 Oxygen:
 0.50 %

POST CATALYST EMISSIONS

NOx: <1.0 g/bhp-hr CO: <2.0 g/bhp-hr VOC: <0.7 g/bhp-hr

CONTROL EQUIPMENT

Catalytic Converter

Model: EAH-1200T-0404F-21CEE
Catalyst Type: NSCR, Precious group metals
Manufacturer: EMIT Technologies, Inc.

Element Size: Round 12 x 3.5

Catalyst Elements: 1

Housing Type: 2 Element Capacity
Catalyst Installation: Accessible Housing
Construction: 10 gauge Carbon Steel

Sample Ports: 6 (0.5" NPT)

Inlet Connections: 4" Flat Face Flange
Outlet Connections: 4" Flat Face Flange
Configuration: End In / End Out

Silencer: Integrated
Silencer Grade: Hospital
Insertion Loss: 35-40 dBA

Air Fuel Ratio Controller

Model: ENG-S-075-T

Manufacturer: EMIT Technologies, Inc.

Description: EDGE NG Air Fuel Ratio Controller

4-Wire Narrowband O2 Sensor

Digital Power Valve
O2 Sensor Weldment

Wiring Harness

(2) 25' Type K Thermocouple

Digital Power Valve Size: 0.75" NPT

Table 3.2-3. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE RICH-BURN ENGINES $^{\rm a}$ (SCC 2-02-002-53)

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
Criteria Pollutants and Greenhous	se Gases	
NO _x c 90 - 105% Load	2.21 E+00	A
NO _x c <90% Load	2.27 E+00	С
CO ^c 90 - 105% Load	3.72 E+00	A
CO ^c <90% Load	3.51 E+00	С
CO_2^{d}	1.10 E+02	A
SO ₂ ^e	5.88 E-04	A
TOC^f	3.58 E-01	С
Methane ^g	2.30 E-01	С
VOCh	2.96 E-02	С
PM10 (filterable) ^{i,j}	9.50 E-03	E
PM2.5 (filterable) ^j	9.50 E-03	E
PM Condensable ^k	9.91 E-03	E
Trace Organic Compounds		
1,1,2,2-Tetrachloroethane ¹	2.53 E-05	C
1,1,2-Trichloroethane ¹	<1.53 E-05	E
1,1-Dichloroethane	<1.13 E-05	E
1,2-Dichloroethane	<1.13 E-05	E
1,2-Dichloropropane	<1.30 E-05	E
1,3-Butadiene ^l	6.63 E-04	D
1,3-Dichloropropene ¹	<1.27 E-05	Е
Acetaldehyde ^{l,m}	2.79 E-03	С
Acrolein ^{1,m}	2.63 E-03	С
Benzene	1.58 E-03	В
Butyr/isobutyraldehyde	4.86 E-05	D
Carbon Tetrachloride ¹	<1.77 E-05	E

Table 3.2-3. UNCONTROLLED EMISSION FACTORS FOR 4-STROKE RICH-BURN ENGINES (Concluded)

Pollutant	Emission Factor (lb/MMBtu) ^b (fuel input)	Emission Factor Rating
Chlorobenzene	<1.29 E-05	Е
Chloroform	<1.37 E-05	Е
Ethane ⁿ	7.04 E-02	С
Ethylbenzene ¹	<2.48 E-05	Е
Ethylene Dibromide ^l	<2.13 E-05	Е
Formaldehyde ^{l,m}	2.05 E-02	A
Methanol ¹	3.06 E-03	D
Methylene Chloride ^l	4.12 E-05	С
Naphthalene	<9.71 E-05	Е
PAH ^l	1.41 E-04	D
Styrene ¹	<1.19 E-05	Е
Toluene	5.58 E-04	A
Vinyl Chloride ^l	<7.18 E-06	Е
Xylene ^l	1.95 E-04	A

Reference 7. Factors represent uncontrolled levels. For NO_x , CO, and PM-10, "uncontrolled" means no combustion or add-on controls; however, the factor may include turbocharged units. For all other pollutants, "uncontrolled" means no oxidation control; the data set may include units with control techniques used for NOx control, such as PCC and SCR for lean burn engines, and PSC for rich burn engines. Factors are based on large population of engines. Factors are for engines at all loads, except as indicated. SCC = Source Classification Code. TOC = Total Organic Compounds. PM10 = Particulate Matter \leq 10 microns (μ m) aerodynamic diameter. A "<" sign in front of a factor means that the corresponding emission factor is based on one-half of the method detection limit.

b Emission factors were calculated in units of (lb/MMBtu) based on procedures in EPA Method 19. To convert from (lb/MMBtu) to (lb/10⁶ scf), multiply by the heat content of the fuel. If the heat content is not available, use 1020 Btu/scf. To convert from (lb/MMBtu) to (lb/hp-hr) use the following equation:

lb/hp-hr = db/MMBtu, heat input, MMBtu/hr, d1/operating HP, 1/hp

^c Emission tests with unreported load conditions were not included in the data set. ^d Based on 99.5% conversion of the fuel carbon to CO_2 . CO_2 [lb/MMBtu] = (3.67)(%CON)(C)(D)(1/h), where %CON = percent conversion of fuel carbon to CO_2 ,

C = carbon content of fuel by weight (0.75), D = density of fuel, $4.1 \text{ E}+04 \text{ lb}/10^6 \text{ scf}$, and h = heating value of natural gas (assume 1020 Btu/scf at 60°F).

^e Based on 100% conversion of fuel sulfur to SO_2 . Assumes sulfur content in natural gas of 2,000 gr/ 10^6 scf.

Emission factor for TOC is based on measured emission levels from 6 source tests.

- ^g Emission factor for methane is determined by subtracting the VOC and ethane emission factors from the TOC emission factor.
- h VOC emission factor is based on the sum of the emission factors for all speciated organic compounds. Methane and ethane emissions were not measured for this engine category.
- No data were available for uncontrolled engines. PM10 emissions are for engines equipped with a PCC.
- ^j Considered $\leq 1 \ \mu \text{m}$ in aerodynamic diameter. Therefore, for filterable PM emissions, PM10(filterable) = PM2.5(filterable).
- ^k No data were available for condensable emissions. The presented emission factor reflects emissions from 4SLB engines.
- ¹ Hazardous Air Pollutant as defined by Section 112(b) of the Clean Air Act.
- ^m For rich-burn engines, no interference is suspected in quantifying aldehyde emissions. The presented emission factors are based on FTIR and CARB 430 emissions data measurements.
- ⁿ Ethane emission factor is determined by subtracting the VOC emission factor from the NMHC emission factor.

ATTACHMENT O: TANKER TRUCK LOADING DATA SHEET

ATTACHMENT O - TANKER TRUCK/RAIL CAR LOADING DATA SHEET

Complete this data sheet for each new or modified bulk liquid transfer area or loading rack at the facility. This is to be used for bulk liquid transfer operations to tanker trucks/rail cars. Use extra pages if necessary.

Truck/Rail Car Loadout Collection Efficiencies

The following applicable capture efficiencies of a truck/rail car loadout are allowed:

- For tanker trucks/rail cars passing the MACT level annual leak test 99.2%
- For tanker trucks/rail cars passing the NSPS level annual leak test 98.7%
- For tanker trucks/rail cars not passing one of the annual leak tests listed above 70%

Compliance with this requirement shall be demonstrated by keeping records of the applicable MACT or NSPS Annual Leak Test certification for *every* truck and railcar loaded/unloaded. This requirement can be satisfied if the trucking/rail car company provided certification that its entire fleet was compliant. This certification must be submitted in writing to the Director of the DAQ. These additional requirements must be noted in the Registration Application.

Emission Unit ID#: EU-LOAD-COND			n Point ID# AD-COND/A	ID#: D/APC-COMB		Year Installed/Modified: 2013			
Emission Unit Description: Condensate Truck Loading Emissions									
			Loading A	Area Data					
Number of Pumps: 1		Number	of Liquids	Loaded: 1		Max nur at one (1		trucks/rail cars loading	
Are tanker trucks/rail ca If Yes, Please describe:	ars pressure teste	d for leak	s at this or a	any other loc	ation?	□ Yes	⊠ No	□ Not Required	
Provide description of closed vent system and any bypasses. Vapors are collected and routed to a vapor combustor.									
Are any of the following truck/rail car loadout systems utilized? Closed System to tanker truck/rail car passing a MACT level annual leak test? Closed System to tanker truck/rail car passing a NSPS level annual leak test? Closed System to tanker truck/rail car not passing an annual leak test and has vapor return? Projected Maximum Operating Schedule (for rack or transfer point as a whole)									
Time	Jan – Ma		Apr -	<u> </u>		ul – Sept	15 a who	Oct - Dec	
Hours/day	24			4	,	24		24	
Days/week	5				5			5	
,	Bul	k Liquid 1	Data (use e	xtra pages a	s necess:	ary)			
Liquid Name	Condens	ate	<u> </u>						
Max. Daily Throughput (1000 gal/day)	93.14								
Max. Annual Throughpu (1000 gal/yr)	33,994.2	8							
Loading Method ¹	SUB								
Max. Fill Rate (gal/min)) 125								
Average Fill Time (min/loading)	Approx.	60							
Max. Bulk Liquid Temperature (°F)	77.98	77.98							
True Vapor Pressure ²	13.5172	13.5172							
Cargo Vessel Condition	3 U	U							
Control Equipment or Method ⁴		or Return/ ion Contro							
Max. Collection Efficient(%)	70%								

Max. Control (%)	Efficiency	98%	
Max.VOC Emission	Loading (lb/hr)	16.16	
Rate	Annual (ton/yr)	36.62	
Max.HAP	Loading (lb/hr)	1.04	
Emission Rate Annual (ton/yr)		2.37	
Estimation Method ⁵		EPA/O = ProMax process simulation	

Emission Unit ID#: EU-LOAD-PW		Emission Point ID#: EP-LOAD-PW/APC-COMB			Year Installed/Modified: 2013					
Emission Unit Description: Produced Water Truck Loading Emissions										
					Loading A	Area Data				
Number of Pu	mps: 1			Numbe	r of Liquids	Loaded: 1		Max num at one (1)		trucks/rail cars loading 1
Are tanker tru If Yes, Please		rs pre	ssure tested	l for lea	ks at this or a	any other loca	ition?	□ Yes	⊠ No	o □ Not Required
Provide descri	ption of c	losed	vent system	and an	y bypasses.	Vapors are co	llected a	and routed	to a va	por combustor.
Are any of the following truck/rail car loadout systems utilized? □ Closed System to tanker truck/rail car passing a MACT level annual leak test? □ Closed System to tanker truck/rail car passing a NSPS level annual leak test? □ Closed System to tanker truck/rail car not passing an annual leak test and has vapor return?										
	Pro	jected	Maximum	Operat	ing Schedul	e (for rack o	r transf	er point as	s a who	ole)
Time			Jan – Mar	•	Apr	- Jun	J	ul – Sept		Oct - Dec
Hours/day			24		2	4		24		24
Days/week			5		4	5		5		5
			Bulk	Liquid	Data (use e	xtra pages as	necessa	ary)		
Liquid Name			Produced	Water						
Max. Daily Th			62.72							
Max. Annual (1000 gal/yr)	Γhroughpu	t	t 22,894.13							
Loading Meth										
Max. Fill Rate	(gal/min)		125							
Average Fill T (min/loading)	Time		Approx. 6	50						
Max. Bulk Lic Temperature (75.36							
True Vapor Pr	essure ²		13.4746							
Cargo Vessel	Condition	3	U							
Control Equip Method ⁴	ment or		O = Vapo Combusti							
Max. Collection (%)	on Efficie	псу	70%							
Max. Control (%)	Efficiency		98%							
Max.VOC Emission	Loading (lb/hr)									
Rate	Annual (ton/yr)		1.81							
Max.HAP Loading (lb/hr) 0.08										
Emission Rate	Annual (ton/yr)		0.12							
Estimation Method ⁵ EPA/O =		EPA/O = simulatio		process						

1	BF	Bottom Fill	SP	Splash Fill			SUB	Submerged Fill
2	At maxi	mum bulk liquid temperature						
3	В	Ballasted Vessel	C	Cleaned			U	Uncleaned (dedicated service)
	O	Other (describe)						
4	List as	many as apply (complete and	submit ap	propriate A	Air Polluti	ion Cont	rol Device	Sheets)
	CA	Carbon Adsorption		VB	Dedicate	ed Vapor	Balance (closed system)
	ECD	Enclosed Combustion Dev	ice	F	Flare	_		
	TO	Thermal Oxidization or Incineration						
5	EPA	EPA Emission Factor in A	P-42			MB	Materia	l Balance
	TM	Test Measurement based upon test data submittal			al	O	Other (de	escribe)

ATTACHMENT Q: PNEUMATIC CONTROLLERS DATA SHEET

ATTACHMENT Q – PNEUMATIC CONTROLLERS **DATA SHEET** Are there any continuous bleed natural gas driven pneumatic controllers at this facility that commenced construction, modification or reconstruction after August 23, 2011, and on or before September 18, 2015? ☐ Yes ☐ No Please list approximate number. Are there any continuous bleed natural gas driven pneumatic controllers at this facility that commenced construction, modification or reconstruction after **September 18, 2015?** ☐ Yes ⊠ No Please list approximate number. Are there any continuous bleed natural gas driven pneumatic controllers at this facility with a bleed rate greater than 6 standard cubic feet per hour that are required based on functional needs, including but not limited to response time, safety and positive actuation that commenced construction, modification or reconstruction after August 23, 2011, and on or before September 18, 2015? ☐ Yes ☐ No Please list approximate number. Are there any continuous bleed natural gas driven pneumatic controllers at this facility with a bleed rate greater than 6 standard cubic feet per hour that are required based on functional needs, including but not limited to response time, safety and positive actuation that commenced construction, modification or reconstruction after September 18, 2015? ☐ Yes ⊠ No

Please list approximate number.

ATTACHMENT R: PNEUMATIC PUMP DATA SHEET

ATTACHMENT R – PNEUMATIC PUMP DATA SHEET

Are there any natural gas-driven diaphragm pumps located at a well site that commenced construction, modification or reconstruction after September 18, 2015?

☐ Yes ⊠ No

Please list.

Source ID#	Date	Pump Make/Model	Pump Size

ATTACHMENT S: AIR POLLUTION CONTROL DEVICE/EMISSION REDUCTION DEVICES SHEETS

VAPOR COMBUSTION

AP-42 EMISSION FACTORS

ATTACHMENT S – AIR POLLUTION CONTROL DEVICE / EMISSION REDUCTION DEVICE SHEETS

Complete the applicable air pollution control device sheets for each flare, vapor combustor, thermal oxidizer, condenser, adsorption system, vapor recovery unit, BTEX Eliminator, Reboiler with and without Glow Plug, etc. at the facility. Use extra pages if necessary.

Emissions calculations must be performed using the most conservative control device efficiency.

The following five (5) rows are only to be completed if registering an alternative air pollution control device.					
Emission Unit ID:	Make/Model:				
Primary Control Device ID:	Make/Model:				
Control Efficiency (%):	APCD/ERD Data Sheet Completed: ☐ Yes ☐ No				
Secondary Control Device ID:	Make/Model:				
Control Efficiency (%):	APCD/ERD Data Sheet Completed: ☐ Yes ☐ No				

VAPOR COMBUSTION								
(Including Enclosed Combustors)								
General Information								
Control Device ID#: APC-COMB				Installation Date: TBD ☑ New ☐ Modified ☐ Relocated				
Maximum Rated Total Flow Capacity 11,187.5 scfh 268,500 scfd			Maximum Design Heat Input (from mfg. spec sheet) 30 MMBTU/hr		Design Heat Content 2,682 BTU/scf			
Control Device Information								
Type of Vapor Combustion Control? Enclosed Combustion Device								
Manufacturer: MRW Technologies Model: TBF-6.5-34-268500				Hours of operation per year? 8,760				
List the emission units whose emissions are controlled by this vapor control device (Emission Point ID# APC-COMB)								
Emission Unit ID#	Emission Source Description		Emission Unit ID#	Emissio	ion Source Description			
EU-TANKS-COND	Condensate Tanks		EU-LOAD- COND	Conden	ensate Truck Loading			
EU-TANKS-PW	Produced Water Ta		Tanks	EU-LOAD- PW	Produced Water Truck Loading		ruck Loading	
If this vapor combustor controls emissions from more than six (6) emission units, please attach additional pages.								
Assist Type (Flares only) Flare Hei			lare Height	Tip Diameter			Was the design per §60.18?	
Steam Pressure	= =		34 feet	6.5 feet			☐ Yes ⊠ No Provide determination.	
Waste Gas Information								
Maximum Waste Gas Flow Rate 187 (scfm)		Rate		of Waste Gas Stream 682 BTU/ft ³		Exit Velocity of the Emissions Stream (ft/s)		
Provide an attachment with the characteristics of the waste gas stream to be burned.								
Pilot Gas Information								
Number of Pilot Lights 3		Flam	w Rate to Pilot te per Pilot 50 scfh	Heat Input per Pilo 45,250 BTU/hr		ot	Will automatic re-ignition be used? ⊠ Yes □ No	
If automatic re-ignition is used, please describe the method. If the pilot flame is lost, the control system will automatically attempt to relight the pilot. If the re-ignition attempt fails, the pilot solenoid valve will automatically close and a local remote alarm signal will be generated to indicate loss of pilot flame.								
Is pilot flame equipped with a monitor to detect the presence of the flame? \boxtimes Yes \square No				If Yes, what type? □ Thermocouple □ Infrared □ Ultraviolet □ Camera ☑ Other: flame rod				
Describe all operating ranges and maintenance procedures required by the manufacturer to maintain the warranty. (If unavailable, please indicate).								
Additional information attached? Yes No Please attach copies of manufacturer's data sheets, drawings, flame demonstration per §60.18 or §63.11(b) and performance testing.								



Tank Battery Combustor Specification Sheet MRW Technologies, Inc. Combustor Model Number: TBF-6.5-34-268500

Expected Destruction Removal Efficiency (DRE): 98% or Greater of

Non-Methane Hydrocarbons

Unit Size: 6.5-foot Diameter

34-Foot Overall Height

Design Heat Input: 30 MMBTU/HR

Design Flow Rates: 268,500 SCFD

Design Heat Content: 2682 BTU/SCF

Waste Gas Flame Arrestor: Enardo

Pilot Type: MRW Electric Ignition

Pilot Operation (Continuous/Intermittent): Three (3) Continuous

Pilot Fuel Consumption: 150 SCFH or Less Total

(50 SCFH per Pilot)

Pilot Monitoring Device: Flame Rod

Automatic Re-Ignition: Included

Remote Alarm Indication: Included

Description of Control Scheme:

The Combustor pilots are monitored via flame rod. If one of the pilot flames are lost, the control system will automatically attempt to relight the pilot. If the re-ignition attempt fails, the pilot solenoid valve will automatically close and a local & remote alarm signal will be generated to indicate loss of pilot flame.

Since flares do not lend themselves to conventional emission testing techniques, only a few attempts have been made to characterize flare emissions. Recent EPA tests using propylene as flare gas indicated that efficiencies of 98 percent can be achieved when burning an offgas with at least 11,200 kJ/m³ (300 Btu/ft³). The tests conducted on steam-assisted flares at velocities as low as 39.6 meters per minute (m/min) (130 ft/min) to 1140 m/min (3750 ft/min), and on air-assisted flares at velocities of 180 m/min (617 ft/min) to 3960 m/min (13,087 ft/min) indicated that variations in incoming gas flow rates have no effect on the combustion efficiency. Flare gases with less than 16,770 kJ/m³ (450 Btu/ft³) do not smoke.

Table 13.5-1 presents flare emission factors, and Table 13.5-2 presents emission composition data obtained from the EPA tests. ¹ Crude propylene was used as flare gas during the tests. Methane was a major fraction of hydrocarbons in the flare emissions, and acetylene was the dominant intermediate hydrocarbon species. Many other reports on flares indicate that acetylene is always formed as a stable intermediate product. The acetylene formed in the combustion reactions may react further with hydrocarbon radicals to form polyacetylenes followed by polycyclic hydrocarbons.²

In flaring waste gases containing no nitrogen compounds, NO is formed either by the fixation of atmospheric nitrogen (N) with oxygen (O) or by the reaction between the hydrocarbon radicals present in the combustion products and atmospheric nitrogen, by way of the intermediate stages, HCN, CN, and OCN. Sulfur compounds contained in a flare gas stream are converted to SO_2 when burned. The amount of SO_2 emitted depends directly on the quantity of sulfur in the flared gases.

Table 13.5-1 (English Units). EMISSION FACTORS FOR FLARE OPERATIONS^a

EMISSION FACTOR RATING: B

Component	Emission Factor (lb/10 ⁶ Btu)
Total hydrocarbons ^b	0.14
Carbon monoxide	0.37
Nitrogen oxides	0.068
Soot ^c	0 - 274

^a Reference 1. Based on tests using crude propylene containing 80% propylene and 20% propane.

^b Measured as methane equivalent.

^c Soot in concentration values: nonsmoking flares, 0 micrograms per liter (μg/L); lightly smoking flares, 40 μg/L; average smoking flares, 177 μg/L; and heavily smoking flares, 274 μg/L.

ATTACHMENT T: EMISSIONS CALCULATIONS

SWN Production Company, LLC John Good Jr Pad Summary of Criteria Air Pollutant Emissions

Equipment	Unit ID	Emission Point	N	Ox	C	0	Tota	I VOC ¹	S	O ₂	PM	Total
Equipment	Onit ib	ID	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
145-hp Caterpillar G3306 NA Engine	EU-ENG1	EP-ENG1	0.32	1.40	0.64	2.80	0.31	1.36	<0.01	<0.01	0.02	0.11
145-hp Caterpillar G3306 NA Engine	EU-ENG2	EP-ENG2	0.32	1.40	0.64	2.80	0.31	1.36	<0.01	<0.01	0.02	0.11
1.0-mmBtu/hr GPU Burner	EU-GPU1	EP-GPU1	0.11	0.48	0.09	0.41	0.01	0.03	<0.01	<0.01	0.01	0.04
1.0-mmBtu/hr GPU Burner	EU-GPU2	EP-GPU2	0.11	0.48	0.09	0.41	0.01	0.03	<0.01	<0.01	0.01	0.04
1.0-mmBtu/hr GPU Burner	EU-GPU3	EP-GPU3	0.11	0.48	0.09	0.41	0.01	0.03	<0.01	<0.01	0.01	0.04
1.0-mmBtu/hr GPU Burner	EU-GPU4	EP-GPU4	0.11	0.48	0.09	0.41	0.01	0.03	<0.01	<0.01	0.01	0.04
1.0-mmBtu/hr GPU Burner	EU-GPU5	EP-GPU5	0.11	0.48	0.09	0.41	0.01	0.03	<0.01	<0.01	0.01	0.04
1.0-mmBtu/hr GPU Burner	EU-GPU6	EP-GPU6	0.11	0.48	0.09	0.41	0.01	0.03	<0.01	<0.01	0.01	0.04
1.0-mmBtu/hr GPU Burner	EU-GPU7	EP-GPU7	0.11	0.48	0.09	0.41	0.01	0.03	<0.01	<0.01	0.01	0.04
1.5-mmBtu/hr Stabilizer Heater	EU-SH1	EP-SH1	0.17	0.73	0.14	0.61	0.01	0.04	<0.01	<0.01	0.01	0.06
1.5-mmBtu/hr Stabilizer Heater	EU-SH2	EP-SH2	0.17	0.73	0.14	0.61	0.01	0.04	<0.01	<0.01	0.01	0.06
Eight (8) 400-bbl Condensate Tanks Routed to Vapor Combustor	EU-TANKS- COND	APC-COMB	-	-	-	-	-	-	-	-	-	-
Eight (8) 400-bbl Produced Water Tanks Routed to Vapor Combustor	EU-TANKS-PW	APC-COMB	-	-	-	-	-	-	-	-	-	-
Condensate Truck Loading w/ Vapor Return Routed to Combustor	EU-LOAD- COND	APC-COMB	-	-	-	-	8.36	36.62	-	-	-	-
Produced Water Truck Loading w/ Vapor Return Routed to Combustor	EU-LOAD-PW	APC-COMB	-	-	-	-	0.41	1.81	-	-	-	-
30.0-mmBtu/hr Vapor Combustor	APC-COMB	APC-COMB	4.14	18.13	8.27	36.20	5.41	23.72	-	-	0.09	0.37
Vapor Combustor Pilot	EU-PILOTS	APC-COMB	0.02	0.07	0.01	0.06	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
Fugitive Emissions	EU-FUG	EP-FUG	-	-	-	-	1.83	8.00	-	-	-	-
Fugitive Haul Road Emissions	EU-HR	EP-HR	-	-	-	-	-	-	-	-	5.71	18.77
		Total =	5.90	25.84	10.48	45.92	16.70	73.13	0.01	0.04	5.93	19.73

¹ Total VOC includes all constituents heavier than Propane (C3+), including hazardous air pollutants (HAP). Speciated HAP presented in following table.

SWN Production Company, LLC John Good Jr Pad Summary of Hazardous Air Pollutants

						Estimated Em	nissions (lb/hr)				
Equipment	Unit ID	Acetalde- hyde	Acrolein	Benzene	Ethyl- benzene	Formalde- hyde	Methanol	n-Hexane	Toluene	Xylenes	Total HAP
145-hp Caterpillar G3306 NA Engine	EU-ENG1	<0.01	<0.01	<0.01	<0.01	0.09	<0.01	-	<0.01	<0.01	0.10
145-hp Caterpillar G3306 NA Engine	EU-ENG2	<0.01	<0.01	<0.01	<0.01	0.09	<0.01	-	<0.01	<0.01	0.10
1.0-mmBtu/hr GPU Burner	EU-GPU1	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.0-mmBtu/hr GPU Burner	EU-GPU2	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.0-mmBtu/hr GPU Burner	EU-GPU3	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.0-mmBtu/hr GPU Burner	EU-GPU4	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.0-mmBtu/hr GPU Burner	EU-GPU5	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.0-mmBtu/hr GPU Burner	EU-GPU6	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.0-mmBtu/hr GPU Burner	EU-GPU7	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.5-mmBtu/hr Stabilizer Heater	EU-SH1	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.5-mmBtu/hr Stabilizer Heater	EU-SH2	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
Eight (8) 400-bbl Condensate Tanks Routed to Vapor Combustor	EU-TANKS- COND	-	-	-	-	-	-	-	-	-	-
Eight (8) 400-bbl Produced Water Tanks Routed to Vapor Combustor	EU-TANKS-PW	-	-	-	-	-	-	-	-	-	-
Condensate Truck Loading w/ Vapor Return Routed to Combustor	EU-LOAD- COND	-	-	0.01	0.03	-	-	0.43	0.03	0.05	0.54
Produced Water Truck Loading w/ Vapor Return Routed to Combustor	EU-LOAD-PW	-	-	<0.01	<0.01	-	-	0.02	<0.01	<0.01	0.03
30.0-mmBtu/hr Vapor Combustor	APC-COMB	-	-	<0.01	0.02	-	-	0.28	0.02	0.03	0.35
Vapor Combustor Pilot	EU-PILOTS	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
Fugitive Emissions	EU-FUG	-	-	<0.01	<0.01	-	-	0.07	<0.01	0.01	0.09
Fugitive Haul Road Emissions	EU-HR	-	-	-	-	-	-	-	-	-	-
	Total =	0.01	0.01	0.01	0.06	0.17	0.01	0.83	0.05	0.09	1.23

Continued on Next Page

SWN Production Company, LLC John Good Jr Pad Summary of Hazardous Air Pollutants (Continued)

		Estimated Emissions (TPY)										
Equipment	Unit ID	Acetalde- hyde	Acrolein	Benzene	Ethyl- benzene	Formalde- hyde	Methanol	n-Hexane	Toluene	Xylenes	Total HAP	
145-hp Caterpillar G3306 NA Engine	EU-ENG1	0.02	0.01	0.01	<0.01	0.38	0.02	-	<0.01	<0.01	0.44	
145-hp Caterpillar G3306 NA Engine	EU-ENG2	0.02	0.01	0.01	<0.01	0.38	0.02	-	<0.01	<0.01	0.44	
1.0-mmBtu/hr GPU Burner	EU-GPU1	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01	
1.0-mmBtu/hr GPU Burner	EU-GPU2	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01	
1.0-mmBtu/hr GPU Burner	EU-GPU3	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01	
1.0-mmBtu/hr GPU Burner	EU-GPU4	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01	
1.0-mmBtu/hr GPU Burner	EU-GPU5	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01	
1.0-mmBtu/hr GPU Burner	EU-GPU6	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01	
1.0-mmBtu/hr GPU Burner	EU-GPU7	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01	
1.5-mmBtu/hr Stabilizer Heater	EU-SH1	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01	
1.5-mmBtu/hr Stabilizer Heater	EU-SH2	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01	
Eight (8) 400-bbl Condensate Tanks Routed to Vapor Combustor	EU-TANKS- COND	-	-	-	-	-	-	-	-	-	-	
Eight (8) 400-bbl Produced Water Tanks Routed to Vapor Combustor	EU-TANKS-PW	-	-	-	-	-	-	-	-	-	-	
Condensate Truck Loading w/ Vapor Return Routed to Combustor	EU-LOAD- COND	-	-	0.02	0.14	-	-	1.89	0.11	0.20	2.37	
Produced Water Truck Loading w/ Vapor Return Routed to Combustor	EU-LOAD-PW	-	-	<0.01	0.01	-	-	0.09	0.01	0.01	0.12	
30.0-mmBtu/hr Vapor Combustor	APC-COMB	-	-	0.02	0.09	-	-	1.22	0.07	0.13	1.53	
Vapor Combustor Pilot	EU-PILOTS	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01	
Fugitive Emissions	EU-FUG	-	-	<0.01	0.02	-	-	0.32	0.02	0.03	0.40	
Fugitive Haul Road Emissions	EU-HR	-	-	-	-	-	-	-	-	-	-	
	Total =	0.03	0.03	0.06	0.25	0.76	0.03	3.62	0.22	0.37	5.38	

SWN Production Company, LLC John Good Jr Pad Summary of Greenhouse Gas Emissions - Metric Tons per Year (Tonnes)

Equipment	Unit ID	Carbon Die	oxide (CO ₂)	Methar	ne (CH ₄)	Methane (0	CH ₄) as CO _{2 Eq.}	Nitrous C	xide (N ₂ O)	Nitrous Oxide	(N ₂ O) as CO _{2 Eq.}	Total CO	2 + CO _{2 Eq.} 1
Equipment	Official	lb/hr	tonnes/yr	lb/hr	tonnes/yr	lb/hr	tonnes/yr	lb/hr	tonnes/yr	lb/hr	tonnes/yr	lb/hr	tonnes/yr
145-hp Caterpillar G3306 NA Engine	EU-ENG1	155.04	616.04	<0.01	0.01	0.07	0.27	<0.01	<0.01	0.08	0.33	155.19	616.64
145-hp Caterpillar G3306 NA Engine	EU-ENG2	155.04	616.04	<0.01	0.01	0.07	0.27	<0.01	<0.01	0.08	0.33	155.19	616.64
1.0-mmBtu/hr GPU Burner	EU-GPU1	116.98	464.80	<0.01	0.01	0.06	0.22	<0.01	<0.01	0.07	0.26	117.10	465.28
1.0-mmBtu/hr GPU Burner	EU-GPU2	116.98	464.80	<0.01	0.01	0.06	0.22	<0.01	<0.01	0.07	0.26	117.10	465.28
1.0-mmBtu/hr GPU Burner	EU-GPU3	116.98	464.80	<0.01	0.01	0.06	0.22	<0.01	<0.01	0.07	0.26	117.10	465.28
1.0-mmBtu/hr GPU Burner	EU-GPU4	116.98	464.80	<0.01	0.01	0.06	0.22	<0.01	<0.01	0.07	0.26	117.10	465.28
1.0-mmBtu/hr GPU Burner	EU-GPU5	116.98	464.80	<0.01	0.01	0.06	0.22	<0.01	<0.01	0.07	0.26	117.10	465.28
1.0-mmBtu/hr GPU Burner	EU-GPU6	116.98	464.80	<0.01	0.01	0.06	0.22	<0.01	<0.01	0.07	0.26	117.10	465.28
1.0-mmBtu/hr GPU Burner	EU-GPU7	116.98	464.80	<0.01	0.01	0.06	0.22	<0.01	<0.01	0.07	0.26	117.10	465.28
1.5-mmBtu/hr Stabilizer Heater	EU-SH1	175.47	697.21	<0.01	0.01	0.08	0.33	<0.01	<0.01	0.10	0.39	175.65	697.93
1.5-mmBtu/hr Stabilizer Heater	EU-SH2	175.47	697.21	<0.01	0.01	0.08	0.33	<0.01	<0.01	0.10	0.39	175.65	697.93
Eight (8) 400-bbl Condensate Tanks Routed to Vapor Combustor	EU-TANKS- COND	-	-	-	-	-	-	-	-	-	-	-	-
Eight (8) 400-bbl Produced Water Tanks Routed to Vapor Combustor	EU-TANKS-PW	-	-	-	-	-	-	-	-	-	-	-	-
Condensate Truck Loading w/ Vapor Return Routed to Combustor	EU-LOAD-COND	0.01	0.02	1.20	4.75	29.91	118.84	-	-	-	-	29.92	118.87
Produced Water Truck Loading w/ Vapor Return Routed to Combustor	EU-LOAD-PW	<0.01	0.02	0.81	3.20	20.14	80.04	-	-	-	-	20.15	80.05
30.0-mmBtu/hr Vapor Combustor	APC-COMB	3,509.31	13,944.14	0.07	0.26	1.65	6.57	0.01	0.03	1.97	7.83	3,512.94	13,958.54
Vapor Combustor Pilot	EU-PILOTS	15.88	63.10	<0.01	<0.01	0.01	0.03	<0.01	<0.01	0.01	0.04	15.90	63.16
Fugitive Emissions	EU-FUG	0.01	0.03	1.31	5.19	32.63	129.67	-	-	-	-	32.64	129.69
Fugitive Haul Road Emissions	EU-HR	-	-	-	-	-	-	-	-	-	-	-	-
	Total =	5,005.06	19,887.42	3.40	13.52	85.04	337.88	0.01	0.04	2.80	11.13	5,092.89	20,236.44

¹CO₂ Equivalent = Pollutant times GWP multiplier. 40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier (100-Year Time Horizon): CO₂ = 1, CH₄ = 25, N₂O = 298

² Per API Compendium (2009) Chapter 5: Because most of the CH₄ and CO₂ emissions from storage tanks occur as a result of flashing (which is controlled by the vapor combustor in this case), working and breathing loss emissions of these gases are very small in production and virtually non-existent in the downstream segments. Vapors from the tanks are routed to the vapor combustor at this site. Therefore, GHG emissions from the condensate and produced water tanks are assumed to be negligible.

SWN Production Company, LLC John Good Jr Pad Summary of Greenhouse Gas Emissions - Short Tons per Year (Tons)

Equipment	Unit ID	Carbon Did	oxide (CO ₂)	Methar	ne (CH ₄)	Methane (C	H ₄) as CO _{2 Eq.}	Nitrous O	xide (N ₂ O)	Nitrous Oxide	(N ₂ O) as CO _{2 Eq.}	Total CO ₂	+ CO _{2 Eq.}
Equipment	Official	lb/hr	tons/yr²	lb/hr	tons/yr ²	lb/hr	tons/yr	lb/hr	tons/yr ²	lb/hr	tons/yr	lb/hr	tons/yr
145-hp Caterpillar G3306 NA Engine	EU-ENG1	155.04	679.06	<0.01	0.01	0.07	0.30	<0.01	<0.01	0.08	0.36	155.19	679.73
145-hp Caterpillar G3306 NA Engine	EU-ENG2	155.04	679.06	<0.01	0.01	0.07	0.30	<0.01	<0.01	0.08	0.36	155.19	679.73
1.0-mmBtu/hr GPU Burner	EU-GPU1	116.98	512.36	<0.01	0.01	0.06	0.24	<0.01	<0.01	0.07	0.29	117.10	512.89
1.0-mmBtu/hr GPU Burner	EU-GPU2	116.98	512.36	<0.01	0.01	0.06	0.24	<0.01	<0.01	0.07	0.29	117.10	512.89
1.0-mmBtu/hr GPU Burner	EU-GPU3	116.98	512.36	<0.01	0.01	0.06	0.24	<0.01	<0.01	0.07	0.29	117.10	512.89
1.0-mmBtu/hr GPU Burner	EU-GPU4	116.98	512.36	<0.01	0.01	0.06	0.24	<0.01	<0.01	0.07	0.29	117.10	512.89
1.0-mmBtu/hr GPU Burner	EU-GPU5	116.98	512.36	<0.01	0.01	0.06	0.24	<0.01	<0.01	0.07	0.29	117.10	512.89
1.0-mmBtu/hr GPU Burner	EU-GPU6	116.98	512.36	<0.01	0.01	0.06	0.24	<0.01	<0.01	0.07	0.29	117.10	512.89
1.0-mmBtu/hr GPU Burner	EU-GPU7	116.98	512.36	<0.01	0.01	0.06	0.24	<0.01	<0.01	0.07	0.29	117.10	512.89
1.5-mmBtu/hr Stabilizer Heater	EU-SH1	175.47	768.54	<0.01	0.01	0.08	0.36	<0.01	<0.01	0.10	0.43	175.65	769.33
1.5-mmBtu/hr Stabilizer Heater	EU-SH2	175.47	768.54	<0.01	0.01	0.08	0.36	<0.01	<0.01	0.10	0.43	175.65	769.33
Eight (8) 400-bbl Condensate Tanks Routed to Vapor Combustor	EU-TANKS- COND	-	-	-	-	-	-	-	-	-	-	-	-
Eight (8) 400-bbl Produced Water Tanks Routed to Vapor Combustor	EU-TANKS-PW	-	-	-	-	-	-	-	-	-	-	-	-
Condensate Truck Loading w/ Vapor Return Routed to Combustor	EU-LOAD-COND	0.01	0.03	1.20	5.24	29.91	131.00	-	-	-	-	29.92	131.03
Produced Water Truck Loading w/ Vapor Return Routed to Combustor	EU-LOAD-PW	<0.01	0.02	0.81	3.53	20.14	88.23	-	-	-	-	20.15	88.24
30.0-mmBtu/hr Vapor Combustor	APC-COMB	3,509.31	15,370.78	0.07	0.29	1.65	7.24	0.01	0.03	1.97	8.63	3,512.94	15,386.66
Vapor Combustor Pilot	EU-PILOTS	15.88	69.55	<0.01	<0.01	0.01	0.03	<0.01	<0.01	0.01	0.04	15.90	69.62
Fugitive Emissions	EU-FUG	0.01	0.03	1.31	5.72	32.63	142.93	-	-	-	-	32.64	142.96
Fugitive Haul Road Emissions	EU-HR	-	-	-	-	-	-	-	-	-	-	-	-
	Total =	5,005.06	21,922.13	3.40	14.90	85.04	372.45	0.01	0.04	2.80	12.27	5,092.89	22,306.86

¹CO₂ Equivalent = Pollutant times GWP multiplier. 40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier (100-Year Time Horizon): CO₂ = 1, CH₄ = 25, N₂O = 298

² EPA and API GHG calculation methodologies calculate emissions in metric tons (tonnes). These values have been converted to short tons for consistency with permitting threshold units.

³ Per API Compendium (2009) Chapter 5: Because most of the CH₄ and CO₂ emissions from storage tanks occur as a result of flashing (which is controlled by the vapor combustor in this case), working and breathing loss emissions of these gases are very small in production and virtually non-existent in the downstream segments. Vapors from the tanks are routed to the vapor combustor at this site. Therefore, GHG emissions from the condensate and produced water tanks are assumed to be negligible.

SWN Production Company, LLC John Good Jr Pad Engine Emissions Calculations - Criteria Air Pollutants

Equipment Information

Unit ID:	EU-ENG1	EU-ENG2
Emission Point ID:	EP-ENG1	EP-ENG2
Make:	Caterpillar	Caterpillar
Model:	G3306 NA	G3306 NA
Design Class:	4S-RB	4S-RB
Controls:	NSCR	NSCR
Horsepower (hp):	145	145
Fuel Use (Btu/hp-hr):	8,625	8,625
Fuel Use (scfh):	1,382	1,382
Annual Fuel Use (mmscf):	12.11	12.11
Fuel Use (mmBtu/hr):	1.25	1.25
Exhaust Flow (acfm):	678	678
Exhaust Temp (°F):	1,101	1,101
Manufacture Date:	after 1/1/2011	after 1/1/2011
Operating Hours:	8,760	8,760
Fuel Heating Value (Btu/scf):	905	905
Uncontrolled Manufacturer Emission Factors	<u>1</u>	
NOx (g/hp-hr):	13.47	13.47
CO (g/hp-hr):	13.47	13.47
NMNEHC/VOC (g/hp-hr):	0.22	0.22
Total VOC = NMNEHC + HCHO (g/hp-hr):	0.49	0.22
Post-Catalyst Emission Factors		
NOx Control Eff. %	92.58%	92.58%
CO Control Eff. %	85.15%	85.15%
CO Control Ell. 76	03.1370	03.1370
NOx (g/hp-hr):	1.00	1.00
CO (g/hp-hr):	2.00	2.00
NMNEHC/VOC (g/hp-hr):	0.70	0.70
Total VOC = NMNEHC + HCHO (g/hp-hr):	0.97	0.97

Uncontrolled Criteria Air Pollutant Emissions

Unit ID: <u>EU-ENG1</u> <u>EU-ENG2</u>

Pollutant	lb/hr	TPY	lb/hr	TPY
NOx	4.31	18.86	4.31	18.86
СО	4.31	18.86	4.31	18.86
NMNEHC/VOC (does not include HCHO)	0.07	0.31	0.07	0.31
Total VOC (includes HCHO)	0.16	0.69	0.07	0.31
SO ₂	<0.01	<0.01	<0.01	<0.01
PM _{10/2.5}	0.01	0.05	0.01	0.05
PM_{COND}	0.01	0.05	0.01	0.05
PM _{TOT}	0.02	0.11	0.02	0.11

SWN Production Company, LLC John Good Jr Pad Engine Emissions Calculations - Criteria Air Pollutants (Continued)

Proposed Criteria Air Pollutant Emissions²

Pollutant	lb/hr	TPY	lb/hr	TPY
NOx	0.32	1.40	0.32	1.40
CO	0.64	2.80	0.64	2.80
NMNEHC/VOC (does not include HCHO)	0.22	0.98	0.22	0.98
Total VOC (includes HCHO)	0.31	1.36	0.31	1.36
SO ₂	<0.01	<0.01	<0.01	<0.01
PM _{10/2.5}	0.01	0.05	0.01	0.05
PM _{COND}	0.01	0.05	0.01	0.05
PM _{TOT}	0.02	0.11	0.02	0.11

AP-42 Emission Factors (lb/mmBtu)³

4S-RB

Pollutant	3.2-3 (7/00)
SO ₂	5.88E-04
PM _{10/2.5}	9.50E-03
PM _{COND}	9.91E-03
PM _{TOT}	1.94E-02

¹ Uncontrolled emission factors based on engine manufacturer data. Per Caterpillar, NMNEHC emission factor does not include formaldehyde (HCHO); therefore, NMNEHC and HCHO factors have been added to demonstrate total uncontrolled VOC. All other pollutants calculated using AP-42.

² Post-catalyst emission factors for the Caterpillar engine are based on catalyst manufacturer data and/or NSPS Subpart JJJJ limits, if applicable. Per NSPS Subpart JJJJ, VOC limit does not include HCHO; therefore, HCHO emissions have been added to the NSPS JJJJ VOC emission rates for demonstration purposes only.

³ Per AP-42, all particulate matter (PM) from combustion of natural gas (total, condensable and filterable PM) is presumed <1 micrometer in diameter.

SWN Production Company, LLC John Good Jr Pad Engine Emissions Calculations - Hazardous Air Pollutants

Equipment Information

Unit ID:	<u>EU-ENG1</u>	<u>EU-ENG2</u>
Emission Point ID:	EP-ENG1	EP-ENG2
Make:	Caterpillar	Caterpillar
Model:	G3306 NA	G3306 NA
Design Class:	4S-RB	4S-RB
Controls:	NSCR	NSCR
Horsepower (hp):	145	145.0
Fuel Use (Btu/hp-hr):	8,625	8,625
Fuel Use (scfh):	1,382	1,382
Annual Fuel Use (mmscf):	12.11	12.11
Fuel Use (mmBtu/hr):	1.25	1.25
Exhaust Flow (acfm):	678	678
Exhaust Temp (°F):	1,101	1,101
Operating Hours:	8,760	8,760

Proposed HAP Emissions^{1,2}

Unit ID: <u>EU-ENG1</u> <u>EU-ENG2</u>

Pollutant	lb/hr	TPY	lb/hr	TPY
Acetaldehyde	<0.01	0.02	<0.01	0.02
Acrolein	<0.01	0.01	<0.01	0.01
Benzene	<0.01	0.01	<0.01	0.01
Ethylbenzene	<0.01	<0.01	<0.01	<0.01
Formaldehyde	0.09	0.38	0.09	0.38
Methanol	<0.01	0.02	<0.01	0.02
Toluene	<0.01	<0.01	<0.01	<0.01
Xylenes	<0.01	<0.01	<0.01	<0.01
Total HAP =	0.10	0.44	0.10	0.44

AP-42 Emission Factors (lb/mmBtu)

4S-RB

Pollutant	3.2-3 (7/00)		
Acetaldehyde	2.79E-03		
Acrolein	2.63E-03		
Benzene	1.58E-03		
Ethylbenzene	2.18E-05		
Methanol	3.06E-03		
Toluene	5.58E-04		
Xylenes	1.95E-04		

Notes:

0.27

¹ Manuf. data for uncontrolled Caterpillar G3306 HCHO emissions (g/hp-hr):

 $^{^{2}\,\}mbox{For conservative}$ estimate, no reduction taken for any HAP .

SWN Production Company, LLC John Good Jr Pad Engine Emissions Calculations - Greenhouse Gases

Equipment Information

Unit ID:	EU-ENG1	EU-ENG2
Emission Point ID:	EP-ENG1	EP-ENG2
Make:	Caterpillar	Caterpillar
Model:	G3306 NA	G3306 NA
Design Class:	4S-RB	4S-RB
Horsepower (hp):	145	145.0
Capacity (kW):	NA	NA
Fuel Use (Btu/hp-hr):	8,625	8,625
Fuel Use (Btu/kW-hr):	NA	NA
Fuel Use (scfh):	1,382	1,382
Fuel Use (mmBtu/hr):	1.25	1.25
Exhaust Flow (acfm):	678	678
Exhaust Temp (°F):	1,101	1,101
Operating Hours:	8,760	8,760

Manufacturer Emission Factors (g/hp-hr)¹

 $CO_2 = 485$ 485

Greenhouse Gas (GHG) Emissions¹

Pollutant	lb/hr	tonnes/yr	lb/hr	tonnes/yr
CO ₂	155.04	616.04	155.04	616.04
CH₄	<0.01	0.01	<0.01	0.01
N_2O	<0.01	<0.01	<0.01	<0.01
CH₄ as CO₂e	0.07	0.27	0.07	0.27
N₂O as CO₂e	0.08	0.33	0.08	0.33
Total CO ₂ + CO ₂ e =	155.19	616.64	155.19	616.64

40 CFR 98 Tables ENG-1 Emission Factors (kg/mmBtu)²

Carbon Dioxide (CO ₂)	53.06
Methane (CH ₄)	1.00E-03
Nitrous Oxide (N ₂ O)	1.00E-04

¹ Caterpillar ^manufacturer data used to estimate CO₂ emissions for the Caterpillar engine. All other emissions estimated using EPA data. Conversion to short tons (tons) found in site-wide Summary of Greenhouse Gases - Short Tons per Year (tons) table.

 ²CO₂e = CO₂ equivalent (Pollutant times GWP multiplier):
 40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier: CO₂ = 1, CH₄ = 25, N₂O = 298

SWN Production Company, LLC John Good Jr Pad Gas Production Unit Burner Emissions Calculations - Criteria Air Pollutants

Equipment Information

Unit ID: <u>EU-GPU1 - EU-GPU7 (EACH)</u>

Emission Point ID: EP-GPU1 - EP-GPU7

Description: Gas Production Unit Burner

Number of Units: 7

Burner Design (mmBtu/hr): 1.0
Fuel HHV (Btu/scf): 905
Annual Fuel Use (mmscf): 9.68

Annual Operating Hours: 8,760

Criteria Air Pollutant Emissions

Unit ID: <u>EU-GPU1 - EU-GPU7 (EACH)</u>

Pollutant	lb/hr	TPY
NOx	0.11	0.48
CO	0.09	0.41
VOC	0.01	0.03
SO ₂	<0.01	<0.01
PM _{10/2.5}	0.01	0.03
PM_{COND}	<0.01	0.01
PM _{TOT}	0.01	0.04

AP-42 Emission Factors for Units <100 mmBtu/hr (lb/mmscf)¹

Pollutant	1.4-1, -2 (7/98)
NOx	100.0
CO	84.0
VOC	5.5
SO ₂	0.6
PM _{10/2.5}	5.7
PM _{COND}	1.9
PM _{TOT}	7.6

¹ All PM (total, condensable and filterable) is assumed to be <1 micrometer in diameter. Total PM is the sum of filterable PM and condensable PM.

SWN Production Company, LLC John Good Jr Pad Gas Production Unit Burner Emissions Calculations - Hazardous Air Pollutants

Equipment Information

Unit ID: <u>EU-GPU1 - EU-GPU7 (EACH)</u>

Emission Point ID: EP-GPU1 - EP-GPU7

Description: Gas Production Unit Burner

Number of Units: 7

Burner Design (mmBtu/hr): 1.0

Fuel HHV (Btu/scf): 905
Annual Fuel Use (mmscf): 9.68
Annual Operating Hours: 8,760

Hazardous Air Pollutant Emissions

Unit ID: <u>EU-GPU1 - EU-GPU7 (EACH)</u>

Pollutant	lb/hr	TPY
n-Hexane	<0.01	0.01
Formaldehyde	<0.01	<0.01
Benzene	<0.01	<0.01
Toluene	<0.01	<0.01
Total HAP =	<0.01	0.01

AP-42 Emission Factors (lb/mmscf)

Pollutant	1.4-3 (7/98)	
n-Hexane	1.80E+00	
Formaldehyde	7.50E-02	
Benzene	2.10E-03	
Toluene	3.40E-03	

SWN Production Company, LLC John Good Jr Pad Gas Production Unit Burner Emissions Calculations - Greenhouse Gases

Equipment Information

Unit ID: <u>EU-GPU1 - EU-GPU7 (EACH)</u>

Emission Point ID: EP-GPU1 - EP-GPU7

Description: Gas Production Unit Burner

Number of Units: 7

Burner Design (mmBtu/hr): 1.0 Fuel HHV (Btu/scf): 905

Annual Fuel Use (mmscf): 9.68
Annual Operating Hours: 8,760

Greenhouse Gas (GHG) Emissions¹

Unit ID: <u>EU-GPU1 - EU-GPU7 (EACH)</u>

Pollutant	lb/hr	tonnes/yr
CO_2	116.98	464.80
CH ₄	<0.01	0.01
N₂O	<0.01	<0.01
CH₄ as CO₂e	0.06	0.22
N ₂ O as CO ₂ e	0.07	0.26
Total CO ₂ + CO ₂ e =	117.10	465.28

40 CFR 98 Tables C-1 and C-2 Emission Factors (kg/mmBtu)²

Carbon Dioxide (CO ₂)	53.06
Methane (CH ₄)	1.00E-03
Nitrous Oxide (N ₂ O)	1.00E-04

Notes:

40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier: CO₂ = 1, CH₄ = 25, N₂O = 298

¹ Conversion to short tons (tons) found in site-wide Summary of Greenhouse Gases - Short Tons per Year (tons) table.

²CO₂e = CO₂ equivalent (Pollutant times GWP multiplier):

SWN Production Company, LLC John Good Jr Pad Stabilizer Heater Emissions Calculations - Criteria Air Pollutants

Equipment Information

Unit ID: <u>EU-SH1 - EU-SH2 (EACH)</u>

Emission Point ID: EP-SH1 - EP-SH2

Description: Stabilizer Heater

Number of Units: 2

Burner Design (mmBtu/hr): 1.5

Fuel HHV (Btu/scf): 905

Annual Fuel Use (mmscf): 14.52

Annual Operating Hours: 8,760

Criteria Air Pollutant Emissions

Unit ID: <u>EU-SH1 - EU-SH2 (EACH)</u>

Pollutant	lb/hr	TPY
NOx	0.17	0.73
CO	0.14	0.61
VOC	0.01	0.04
SO ₂	<0.01	<0.01
PM _{10/2.5}	0.01	0.04
PM_{COND}	<0.01	0.01
PM _{TOT}	0.01	0.06

AP-42 Emission Factors for Units <100 mmBtu/hr (lb/mmscf)¹

Pollutant	1.4-1, -2 (7/98)
NOx	100.0
CO	84.0
VOC	5.5
SO_2	0.6
PM _{10/2.5}	5.7
PM_COND	1.9
PM _{TOT}	7.6

¹ All PM (total, condensable and filterable) is assumed to be <1 micrometer in diameter. Total PM is the sum of filterable PM and condensable PM.

SWN Production Company, LLC John Good Jr Pad Stabilizer Heater Emissions Calculations - Hazardous Air Pollutants

Equipment Information

Unit ID: <u>EU-SH1 - EU-SH2 (EACH)</u>

Emission Point ID: EP-SH1 - EP-SH2

Description: Stabilizer Heater

Number of Units: 2
Burner Design (mmBtu/hr): 1.5

Fuel HHV (Btu/scf): 905

Annual Fuel Use (mmscf): 14.52

Annual Operating Hours: 8,760

Hazardous Air Pollutant Emissions

Unit ID: <u>EU-SH1 - EU-SH2 (EACH)</u>

Pollutant	lb/hr	TPY
n-Hexane	<0.01	0.01
Formaldehyde	<0.01	<0.01
Benzene	<0.01	<0.01
Toluene	<0.01	<0.01
Total HAP =	<0.01	0.01

AP-42 Emission Factors (lb/mmscf)

Pollutant	1.4-3 (7/98)
n-Hexane	1.80E+00
Formaldehyde	7.50E-02
Benzene	2.10E-03
Toluene	3.40E-03

SWN Production Company, LLC John Good Jr Pad Stabilizer Heater Emissions Calculations - Greenhouse Gases

Equipment Information

Unit ID: <u>EU-SH1 - EU-SH2 (EACH)</u>

Emission Point ID: EP-SH1 - EP-SH2

Description: Stabilizer Heater

Number of Units: 2

Burner Design (mmBtu/hr): 1.5

Fuel HHV (Btu/scf): 905
Annual Fuel Use (mmscf): 14.52
Annual Operating Hours: 8,760

Greenhouse Gas (GHG) Emissions¹

Unit ID: <u>EU-SH1 - EU-SH2 (EACH)</u>

Pollutant	lb/hr	tonnes/yr
CO_2	175.47	697.21
CH ₄	<0.01	0.01
N₂O	<0.01	<0.01
CH ₄ as CO ₂ e	0.08	0.33
N ₂ O as CO ₂ e	0.10	0.39
Total CO ₂ + CO ₂ e =	175.65	697.93

40 CFR 98 Tables C-1 and C-2 Emission Factors (kg/mmBtu)²

Carbon Dioxide (CO ₂)	53.06
Methane (CH ₄)	1.00E-03
Nitrous Oxide (N ₂ O)	1.00E-04

Notes:

40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier: $CO_2 = 1$, $CH_4 = 25$, $N_2O = 298$

¹ Conversion to short tons (tons) found in site-wide Summary of Greenhouse Gases - Short Tons per Year (tons) table.

²CO₂e = CO₂ equivalent (Pollutant times GWP multiplier):

SWN Production Company, LLC John Good Jr Pad Storage Tank Emissions - Criteria Air Pollutants

Tank Information

Unit ID:	EU-TANKS-COND	EU-TANKS-PW
Emission Point ID:	APC-COMB	APC-COMB
Contents: 1,3	Condensate	Produced Water
Number of Tanks:	8	8
Capacity (bbl) - Per Tank:	400	400
Capacity (gal) - Per Tank:	16,800	16,800
Total:		
Total Throughput (bbl/yr):	809,388	545,098
Total Throughput (gal/yr):	33,994,275	22,894,129
Total Throughput (bbl/d):	2,218	1,493
Per Tank:		
Throughput (bbl/yr):	101,173	68,137
Throughput (gal/yr):	4,249,284	2,861,766
Throughput (bbl/d):	277	187
Turnovers:	2,023.47	1,362.75
Tank Vapor Capture Efficiency:	100%	100%
Captured Vapors Routed to:	Vapor Combustor	Vapor Combustor

Uncontrolled Storage Tank Emissions

Unit ID: <u>EU-TANKS-COND</u> <u>EU-TANKS-PW</u>

Emissions	lb/hr	TPY	lb/hr	TPY
Working Losses	13.06	57.22	0.05	0.21
Breathing Losses	14.24	62.35	0.04	0.17
Flashing Losses ²	221.39	969.70	1.47	6.44
Total VOC =	248.69	1,089.27	1.56	6.82

Controlled Storage Tank Emissions³

Unit ID: <u>EU-TANKS-COND</u> <u>EU-TANKS-PW</u>

Emissions	lb/hr	TPY	lb/hr	TPY
Working Losses	0.26	1.14	<0.01	<0.01
Breathing Losses	0.28	1.25	<0.01	<0.01
Flashing Losses	4.43	19.39	0.03	0.13
Total VOC =	4.97	21.79	0.03	0.14
Per Tank =	0.62	2.72	<0.01	0.02

¹ Produced water tanks assumed to contain 99% produced water and 1% condensate.

² Tank working, breathing, and flashing emissions were calculated using Promax process simulation. Reports located in Attachment L. Uncontrolled tank working/breathing/flashing emissions will be routed to a vapor combustor with 100% capture efficiency.

³ Controlled tank emissions are shown for reference only.

SWN Production Company, LLC John Good Jr Pad Storage Tank Emissions - Hazardous Air Pollutants

Uncontrolled Storage Tank Emissions

Unit ID: <u>EU-TANKS-COND</u> <u>EU-TANKS-PW</u>

Pollutant	lb/hr	TPY	lb/hr	TPY
Total VOC = 1,2	248.69	1,089.27	1.56	6.82
n-Hexane	12.84	56.24	0.08	0.35
Benzene	0.16	0.71	<0.01	<0.01
Toluene	0.78	3.40	<0.01	0.02
Ethylbenzene	0.93	4.09	0.01	0.03
Xylenes	1.35	5.93	0.01	0.04
Total HAP =	16.07	70.37	0.10	0.44

Controlled Storage Tank Emissions 3

Unit ID: <u>EU-TANKS-COND</u> <u>EU-TANKS-PW</u>

Pollutant	lb/hr	TPY	lb/hr	TPY
Total VOC = 1	4.97	21.79	0.03	0.14
n-Hexane	0.26	1.12	<0.01	0.01
Benzene	<0.01	0.01	<0.01	<0.01
Toluene	0.02	0.07	<0.01	<0.01
Ethylbenzene	0.02	0.08	<0.01	<0.01
Xylenes	0.03	0.12	<0.01	<0.01
Total HAP =	0.32	1.41	<0.01	0.01

Estimated HAP Composition (% by Weight)⁴

Pollutant	Wt%
n-Hexane	5.163%
Benzene	0.065%
Toluene	0.312%
Ethylbenzene	0.375%
Xylenes	0.545%
Total HAP =	6.460%

¹ VOC emissions calculated in Criteria Air Pollutant calculations.

² Uncontrolled tank working/breathing/flashing emissions are controlled by a vapor combustor with 100% capture efficiency.

³ Controlled tank emissions are shown for reference only.

⁴ Speciated liquids analysis located in Fugitive Emissions Calculations. HAP weight % calculated as % of total hydrocarbons in the sample. All HAP assumed to volatilize from liquids for most conservative emissions estimate.

SWN Production Company, LLC John Good Jr Pad Condensate Truck Loading Emissions - Criteria and Hazardous Air Pollutants

Loading Information

Unit ID: <u>EU-LOAD-COND</u>

Emission Point ID: APC-COMB
Fill Method: Submerged
Type of Service: Dedicated
Mode of Operation: Normal

Saturation Factor: 0.6 Em. Factor (lb/1000 gal): 1 8.83 Throughput (1000 gal): 33,994.28

Control Type: Vapor Return/Combustion

Vapor Capture Efficiency: ¹ 70% Average Fill Rate (gal/hr): 7,500 Captured Vapors Routed to: Vapor Combustor

VOC Weight %: 81.37%

13.5172	= P, True vapor pressure of liquid loaded (max. psia)		
46.99	= M, Molecular weight of vapor (lb/lb-mol)		
77.98	= T, Temperature of bulk liquid loaded (average °F)		
537.9796	= T, Temperature of bulk liquid loaded (°F + 460 = °R)		

Uncontrolled Loading Emissions²

Pollutant	Max. lb/hr	Avg. lb/hr	TPY
VOC =	53.87	27.87	122.08
n-Hexane	2.78	1.44	6.30
Benzene	0.04	0.02	0.08
Toluene	0.17	0.09	0.38
Ethylbenzene	0.20	0.10	0.46
Xylenes	0.29	0.15	0.67
Total HAP =	3.48	1.80	7.89

Uncaptured Loading Emissions²

Pollutant	Max. lb/hr	Avg. lb/hr	TPY
VOC =	16.16	8.36	36.62
n-Hexane	0.83	0.43	1.89
Benzene	0.01	0.01	0.02
Toluene	0.05	0.03	0.11
Ethylbenzene	0.06	0.03	0.14
Xylenes	0.09	0.05	0.20
Total HAP =	1.04	0.54	2.37

SWN Production Company, LLC John Good Jr Pad

Condensate Truck Loading Emissions - Criteria and Hazardous Air Pollutants (Continued)

Estimated HAP Composition (% by Weight)³

Pollutant	Wt%
n-Hexane	5.163%
Benzene	0.065%
Toluene	0.312%
Ethylbenzene	0.375%
Xylenes	0.545%
Total HAP =	6.460%

¹ Uncontrolled emissions that are captured by the collection system are routed to a vapor combustor. Per AP-42 5.2-6, 70% capture efficiency can be assumed for trucks not subject to NSPS. Uncaptured emissions shown represent those not captured by the collection system or controlled by the vapor combustor.

² Maximum lb/hr based on average hourly truck loading rate. Average lb/hr based on TPY conversion assuming continuous operation.

³ Speciated liquids analysis located in Fugitive Emissions Calculations. HAP weight % calculated as % of total hydrocarbons in the sample. All HAP assumed to volatilize from liquids for most conservative emissions estimate.

SWN Production Company, LLC John Good Jr Pad Condensate Truck Loading Emissions - Greenhouse Gases

Loading Information

Unit ID: <u>EU-LOAD-COND</u>

Emission Point ID: APC-COMB
Fill Method: Submerged
Type of Service: Dedicated
Mode of Operation: Normal

TOC Em. Factor (tonne/10⁶ gal): 1 0.91

Throughput (10⁶ gal): 33.994

Control Type: Vapor Return/Combustion

Vapor Capture Efficiency: ² 70.00% Average Fill Rate (gal/hr): 7,500 Captured Vapors Routed to: Vapor Combustor

> Analysis CH_4 wt% = 51.22273% Analysis CO_2 wt% = 0.26415%

Uncontrolled Loading Emissions^{3, 4}

Pollutant	Max. lb/hr	Avg. lb/hr	tonnes/yr	tons/yr
CH₄	7.71	3.99	15.85	17.47
CH ₄ as CO ₂ e	192.68	99.70	396.14	436.67
CO_2	0.04	0.02	0.08	0.09
Total CO ₂ + CO ₂ e =	192.72	99.72	396.22	436.76

Uncaptured Loading Emissions^{3, 4}

Pollutant	Max. lb/hr	Avg. lb/hr	tonnes/yr	tons/yr
CH₄	2.31	1.20	4.75	5.24
CH₄ as CO₂e	57.80	29.91	118.84	131.00
CO_2	0.01	0.01	0.02	0.03
Total CO ₂ + CO ₂ e =	57.82	29.92	118.87	131.03

SWN Production Company, LLC John Good Jr Pad Condensate Truck Loading Emissions - Greenhouse Gases (Continued)

API Compendium Table 5-12

Loading Type	Emission Factor (tonne TOC/10 ⁶ gal)
Rail/Truck - Submerged Loading - Dedicated Normal Service	0.91
Rail/Truck - Submerged Loading - Vapor Balance Service	1.51
Rail/Truck - Splash Loading - Dedicated Normal Service	/ / ()
Rail/Truck - Splash Loading - Vapor Balance Service	1.51
Marine Loading - Ships/Ocean Barges	0.28
Marine Loading - Barges	0.45

¹ API Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Gas Industry, Table 5-12.

² Uncontrolled emissions that are captured by the collection system are routed to a vapor combustor. Per AP-42 5.2-6, 70% capture efficiency can be assumed for trucks not subject to NSPS. Uncaptured emissions shown represent those not captured by the collection system or controlled by the vapor combustor.

³ Maximum lb/hr based on average hourly truck loading rate. Average lb/hr based on TPY conversion assuming continuous operation.

 ⁴ CO₂e = CO₂ equivalent (Pollutant times GWP multiplier):
 40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier: CO₂ = 1, CH₄ = 25

SWN Production Company, LLC John Good Jr Pad Produced Water Truck Loading Emissions - Criteria and Hazardous Air Pollutants

Loading Information

Unit ID: <u>EU-LOAD-PW</u>

Emission Point ID: APC-COMB
Fill Method: Submerged
Type of Service: Dedicated
Mode of Operation: Normal

Saturation Factor: 0.6 Em. Factor (lb/1000 gal): 4.26 Throughput (1000 gal): 22,894.13

Control Type: Vapor Return/Combustion

Vapor Capture Efficiency: ¹ 70% Average Fill Rate (gal/hr): 7,500 Captured Vapors Routed to: Vapor Combustor

VOC Weight %: 12.37%

13.4746	= P, True vapor pressure of liquid loaded (max. psia)
22.63	= M, Molecular weight of vapor (lb/lb-mol)
75.36	= T, Temperature of bulk liquid loaded (average °F)
535.3557	= T, Temperature of bulk liquid loaded (°F + 460 = °R)

Uncontrolled Loading Emissions²

Pollutant	Max. lb/hr	Avg. lb/hr	TPY
VOC =	3.95	1.38	6.03
n-Hexane	0.20	0.07	0.31
Benzene	<0.01	<0.01	<0.01
Toluene	0.01	<0.01	0.02
Ethylbenzene	0.01	0.01	0.02
Xylenes	0.02	0.01	0.03
Total HAP =	0.26	0.09	0.39

Uncaptured Loading Emissions²

Pollutant	Max. lb/hr	Avg. lb/hr	TPY
VOC =	1.19	0.41	1.81
n-Hexane	0.06	0.02	0.09
Benzene	<0.01	<0.01	<0.01
Toluene	<0.01	<0.01	0.01
Ethylbenzene	<0.01	<0.01	0.01
Xylenes	0.01	<0.01	0.01
Total HAP =	80.0	0.03	0.12

SWN Production Company, LLC John Good Jr Pad

Produced Water Truck Loading Emissions - Criteria and Hazardous Air Pollutants (Continued)

Estimated HAP Composition (% by Weight)³

Pollutant	Wt%
n-Hexane	5.163%
Benzene	0.065%
Toluene	0.312%
Ethylbenzene	0.375%
Xylenes	0.545%
Total HAP =	6.460%

¹ Uncontrolled emissions that are captured by the collection system are routed to a vapor combustor. Per AP-42 5.2-6, 70% capture efficiency can be assumed for trucks not subject to NSPS. Uncaptured emissions shown represent those not captured by the collection system or controlled by the vapor combustor.

² Maximum lb/hr based on average hourly truck loading rate. Average lb/hr based on TPY conversion assuming continuous operation.

³ Speciated liquids analysis located in Fugitive Emissions Calculations. HAP weight % calculated as % of total hydrocarbons in the sample. All HAP assumed to volatilize from liquids for most conservative emissions estimate.

SWN Production Company, LLC John Good Jr Pad Produced Water Truck Loading Emissions - Greenhouse Gases

Loading Information

Unit ID: <u>EU-LOAD-PW</u>

Emission Point ID: APC-COMB
Fill Method: Submerged
Type of Service: Dedicated
Mode of Operation: Normal

TOC Em. Factor (tonne/10⁶ gal): 1 0.91

Throughput (10⁶ gal): 22.8941

Control Type: Vapor Return/Combustion

Vapor Capture Efficiency: ² 70.00% Average Fill Rate (gal/hr): 7,500 Captured Vapors Routed to: Vapor Combustor

> Analysis CH_4 wt% = 51.22273% Analysis CO_2 wt% = 0.26415%

Uncontrolled Loading Emissions^{3, 4}

Pollutant	Max. lb/hr	Avg. lb/hr	tonnes/yr	tons/yr
CH₄	7.71	2.69	10.67	11.76
CH ₄ as CO ₂ e	192.68	67.14	266.79	294.08
CO_2	0.04	0.01	0.06	0.06
Total CO ₂ + CO ₂ e =	192.72	67.16	266.84	294.15

Uncaptured Loading Emissions^{3, 4}

Pollutant	Max. lb/hr	Avg. lb/hr	tonnes/yr	tons/yr
CH₄	2.31	0.81	3.20	3.53
CH₄ as CO₂e	57.80	20.14	80.04	88.23
CO_2	0.01	<0.01	0.02	0.02
Total CO ₂ + CO ₂ e =	57.82	20.15	80.05	88.24

SWN Production Company, LLC John Good Jr Pad Produced Water Truck Loading Emissions - Greenhouse Gases (Continued)

API Compendium Table 5-12

Loading Type	Emission Factor (tonne TOC/10 ⁶ gal)
Rail/Truck - Submerged Loading - Dedicated Normal Service	0.91
Rail/Truck - Submerged Loading - Vapor Balance Service	1.51
Rail/Truck - Splash Loading - Dedicated Normal Service	/ / ()
Rail/Truck - Splash Loading - Vapor Balance Service	1.51
Marine Loading - Ships/Ocean Barges	0.28
Marine Loading - Barges	0.45

¹ API Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Gas Industry, Table 5-12.

² Uncontrolled emissions that are captured by the collection system are routed to a vapor combustor. Per AP-42 5.2-6, 70% capture efficiency can be assumed for trucks not subject to NSPS. Uncaptured emissions shown represent those not captured by the collection system or controlled by the vapor combustor.

³ Maximum lb/hr based on average hourly truck loading rate. Average lb/hr based on TPY conversion assuming continuous operation.

 ⁴ CO₂e = CO₂ equivalent (Pollutant times GWP multiplier):
 40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier: CO₂ = 1, CH₄ = 25

SWN Production Company, LLC John Good Jr Pad Vapor Combustor Emissions Calculations - Criteria and Hazardous Air Pollutants

Criteria and Hazardous Air Pollutant Emissions

		Emission	Total Captured Emissions ²		Combustor Destruction Efficiency		Emissions (Post- Combustion)
Unit ID	Pollutant	Factors ¹	lb/hr	TPY	%	lb/hr	TPY
	NOx	0.138	-	-	-	4.14	18.13
APC-COMB	co	0.2755	-		-	8.27	36.20
	PM	7.6	1		-	0.09	0.37
	VOC	Mass Balance	270.72	1,185.77	98.00%	5.41	23.72
	n-Hexane	Mass Balance	13.98	61.23	98.00%	0.28	1.22
	Benzene	Mass Balance	0.18	0.77	98.00%	<0.01	0.02
	Toluene	Mass Balance	0.84	3.70	98.00%	0.02	0.07
	Ethylbenzene	Mass Balance	1.02	4.45	98.00%	0.02	0.09
	Xylenes	Mass Balance	1.47	6.46	98.00%	0.03	0.13

Notes:

Hours per Year: 8,760 Number of Combustors: 1

NOx and CO emission factors (lb/mmBtu): *TCEQ Air Permit Technical Guidance for Chemical Sources: Flares and Vapor Oxidizers:* High Btu waste streams (>1,000 Btu/scf) based on heat input to each combustor =

30.0 mmBtu/hr per Combustor

30.0 mmBtu/hr Total Heat Input

¹ Although a vapor combustor is not considered a flare by design, the function is consistent in that it combusts a waste stream for the purpose of reducing emissions; therefore, flare emission factors for NOx and CO were used to provide the most accurate emissions estimates. Although the combustor is designed to be smokeless, PM emissions have been estimated using AP-42 Table 1.4-1 factor (lb/mmscf) for a conservative estimate.

² Total captured emissions are based on 100% capture efficiency from storage tanks and 70% capture efficiency from truck loading with 98% destruction efficiency from the vapor combustor based on 8,760 hours of operation per year. Captured emissions from sources controlled by VOC combustor shown in following tables.

SWN Production Company, LLC John Good Jr Pad Vapor Combustor Emissions Calculations - Criteria and Hazardous Air Pollutants (Continued)

	Captured VOC Emissions		
Source	lb/hr	TPY	
Condensate Storage Tanks	248.69	1,089.27	
Produced Water Storage Tanks	1.56	6.82	
Condensate Truck Loading	19.51	85.45	
Produced Water Truck Loading	0.96	4.22	
Total VOC =	270.72	1,185.77	

	Captured HAP Emissions (lb/hr)				
Source	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylenes
Condensate Storage Tanks	12.84	0.16	0.78	0.93	1.35
Produced Water Storage Tanks	0.08	<0.01	<0.01	0.01	0.01
Condensate Truck Loading	1.01	0.01	0.06	0.07	0.11
Produced Water Truck Loading	0.05	<0.01	<0.01	<0.01	0.01
Total HAP =	13.98	0.18	0.84	1.02	1.47

	Captured HAP Emissions (TPY)				
Source	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylenes
Condensate Storage Tanks	56.24	0.71	3.40	4.09	5.93
Produced Water Storage Tanks	0.35	<0.01	0.02	0.03	0.04
Condensate Truck Loading	4.41	0.06	0.27	0.32	0.47
Produced Water Truck Loading	0.22	<0.01	0.01	0.02	0.02
Total HAP =	61.23	0.77	3.70	4.45	6.46

SWN Production Company, LLC John Good Jr Pad Vapor Combustor Emissions Calculations - Greenhouse Gases

Equipment Information

Unit ID: APC-COMB

Description: Vapor Combustor

Number of Combustors: 1

Burner Design Capacity (mmBtu/hr): 30.0

Stream HHV (Btu/scf): 2,682

Annual Throughput (mmscf): 97.99
Annual Operating Hours: 8,760

Greenhouse Gas (GHG) Emissions

Pollutant	lb/hr	tonnes/yr	tons/yr
CO ₂	3,509.31	13,944.14	15,370.78
CH ₄	0.07	0.26	0.29
N_2O	0.01	0.03	0.03
CH ₄ as CO ₂ e	1.65	6.57	7.24
N ₂ O as CO ₂ e	1.97	7.83	8.63
Total CO ₂ + CO ₂ e =	3,512.94	13,958.54	15,386.66

40 CFR 98 Tables C-1 and C-2 Emission Factors (kg/mmBtu)¹

Carbon Dioxide (CO ₂)	53.06
Methane (CH ₄)	1.00E-03
Nitrous Oxide (N ₂ O)	1.00E-04

Notes:

40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier: $CO_2 = 1$, $CH_4 = 25$, $N_2O = 298$

¹CO₂e = CO₂ equivalent (Pollutant times GWP multiplier):

SWN Production Company, LLC John Good Jr Pad Vapor Combustor Pilot Emissions Calculations - Criteria Air Pollutants

Criteria Air Pollutant Emissions

		Emission		
		Factors 1	Emissio	ns
Unit ID	Pollutant	(lb/mmscf)	lb/hr	TPY
EU-PILOTS	NOx	100	0.02	0.07
APC-COMB	CO	84	0.01	0.06
	VOC	5.5	<0.01	<0.01
	SO ₂	0.6	<0.01	<0.01
	PM	7.6	<0.01	<0.01

905	Pilot Stream Heat Content (Btu/SCF)
8,760	Pilot Hours/Yr
150	Total Pilot Gas Flow Rate (SCFH) ²
135,750	Total Pilot Gas Fuel Use (Btu/hr)
1.31	Total Annual Fuel Use (MMSCF)

¹ AP-42 Table 1.4-1, -2 (7/98)

² Vapor Combustor is equipped with three (3) pilots with a pilot fuel consumption of 50 SCFH per pilot.

SWN Production Company, LLC John Good Jr Pad Vapor Combustor Pilot Emissions Calculations - Hazardous Air Pollutants

Hazardous Air Pollutant Emissions

		Emission Factors ¹	Emis	sions
Unit ID	Pollutant	(lb/mmscf)	lb/hr	TPY
EU-PILOTS	n-Hexane	1.8	<0.01	<0.01
APC-COMB	Formaldehyde	0.075	<0.01	<0.01
	Benzene	0.0021	<0.01	<0.01
	Toluene	0.0034	<0.01	<0.01
		Total HAP =	<0.01	<0.01

905	Pilot Stream Heat Content (Btu/SCF)
8,760	Pilot Hours/Yr
150	Total Pilot Gas Flow Rate (SCFH) ²
135,750	Total Pilot Gas Fuel Use (Btu/hr)
1.31	Total Annual Fuel Use (MMSCF)

¹ AP-42 Table 1.4-3 (7/98)

² Vapor Combustor is equipped with three (3) pilots with a pilot fuel consumption of 50 SCFH per pilot.

SWN Production Company, LLC John Good Jr Pad Vapor Combustor Pilot Emissions Calculations - Greenhouse Gases

Greenhouse Gas (GHG) Emissions

			Emissions	
Unit ID	Pollutant	lb/hr	tonnes/yr	tons/yr
EU-PILOTS	CO_2	15.88	63.10	69.55
APC-COMB	CH₄	<0.01	<0.01	<0.01
	N ₂ O	<0.01	<0.01	<0.01
	CH ₄ as CO ₂ e	0.01	0.03	0.03
	N ₂ O as CO ₂ e	0.01	0.04	0.04
	Total CO ₂ + CO ₂ e =	15.90	63.16	69.62

905	Pilot Stream Heat Content (Btu/SCF)
8,760	Pilot Hours/Yr
150	Total Pilot Gas Flow Rate (SCFH) ²
135,750	Total Pilot Gas Fuel Use (Btu/hr)
1.31	Total Annual Fuel Use (MMSCF)

40 CFR 98 Tables C-1 and C-2 Emission Factors (kg/mmBtu)¹

Carbon Dioxide (CO ₂)	53.06
Methane (CH ₄)	1.00E-03
Nitrous Oxide (N ₂ O)	1.00E-04

¹CO₂e = CO₂ equivalent (Pollutant times GWP multiplier):

⁴⁰ CFR 98 Table A-1, Global Warming Potential (GWP) multiplier: CO₂ = 1, CH₄ = 25, N₂O = 298

² Vapor Combustor is equipped with three (3) pilots with a pilot fuel consumption of 50 SCFH per pilot.

SWN Production Company, LLC John Good Jr Pad Fugitive Emissions Calculations - Criteria and Hazardous Air Pollutants and Greenhouse Gases

Equipment Information

Source Type/Service	Number of Sources ¹	Em. Factor (lb/hr/source) ²	Control Efficiency	TOC lb/hr	TOC TPY	VOC Wt %
Valves - Gas	119	9.92E-03	0.00%	1.18	5.17	23.15%
Flanges - Gas	474	8.60E-04	0.00%	0.41	1.79	23.15%
Compressor Seals - Gas	6	1.94E-02	0.00%	0.12	0.51	23.15%
Relief Valves - Gas	41	1.94E-02	0.00%	0.80	3.48	23.15%
		Total TOC (Gas	Components) =	2.50	10.95	-
Valves - Light Oil	166	5.51E-03	0.00%	0.91	4.01	95.45%
Flanges - Light Oil	42	2.43E-04	0.00%	0.01	0.04	95.45%
Connectors - Light Oil	574	4.63E-04	0.00%	0.27	1.16	95.45%
Other - Light Oil	7	1.65E-02	0.00%	0.12	0.51	95.45%
	T	otal TOC (Liquid	Components) =	1.31	5.72	-

VOC and Greenhouse Gas Emissions

Source Type/Service	V	C	C	H ₄	С	O ₂
Source Type/Service	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
Valves - Gas	0.27	1.20	0.61	2.67	<0.01	0.01
Flanges - Gas	0.09	0.41	0.21	0.92	<0.01	<0.01
Compressor Seals - Gas	0.03	0.12	0.06	0.26	<0.01	<0.01
Relief Valves - Gas	0.18	0.81	0.41	1.80	<0.01	0.01
Components in Gas Service =	0.58	2.53	1.29	5.66	0.01	0.03
Valves - Light Oil	0.87	3.82	0.01	0.04	<0.01	<0.01
Flanges - Light Oil	0.01	0.04	<0.01	<0.01	<0.01	<0.01
Connectors - Light Oil	0.25	1.11	<0.01	0.01	<0.01	<0.01
Other - Light Oil	0.11	0.48	<0.01	0.01	<0.01	<0.01
Components in Liquid Service =	1.25	5.46	0.01	0.06	<0.01	<0.01
Total (Gas + Liquid Components) =	1.83	8.00	1.31	5.72	0.01	0.03

Hazardous Air Pollutant (HAP) Emissions (lb/hr)

Source Type/Service	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylenes	2,2,4-Tri.	Total
Valves - Gas	<0.01	<0.01	<0.01	0.00	<0.01	0.00	<0.01
Flanges - Gas	<0.01	<0.01	<0.01	0.00	<0.01	0.00	<0.01
Compressor Seals - Gas	<0.01	<0.01	<0.01	0.00	<0.01	0.00	<0.01
Relief Valves - Gas	<0.01	<0.01	<0.01	0.00	<0.01	0.00	<0.01
Components in Gas Service =	0.01	<0.01	<0.01	0.00	<0.01	0.00	0.01
Valves - Light Oil	0.05	<0.01	<0.01	<0.01	<0.01	0.00	0.06
Flanges - Light Oil	<0.01	<0.01	<0.01	<0.01	<0.01	0.00	<0.01
Connectors - Light Oil	0.01	<0.01	<0.01	<0.01	<0.01	0.00	0.02
Other - Light Oil	0.01	<0.01	<0.01	<0.01	<0.01	0.00	0.01
Components in Liquid Service =	0.07	<0.01	<0.01	<0.01	0.01	0.00	0.08
Total (Gas + Liquid Components) =	0.07	<0.01	<0.01	<0.01	0.01	0.00	0.09

Hazardous Air Pollutant (HAP) Emissions (TPY)

Source Type/Service	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylenes	2,2,4-Tri.	Total
Valves - Gas	0.01	<0.01	<0.01	0.00	<0.01	0.00	0.01
Flanges - Gas	<0.01	<0.01	<0.01	0.00	<0.01	0.00	<0.01
Compressor Seals - Gas	<0.01	<0.01	<0.01	0.00	<0.01	0.00	<0.01
Relief Valves - Gas	0.01	<0.01	<0.01	0.00	<0.01	0.00	0.01
Components in Gas Service =	0.03	<0.01	<0.01	0.00	<0.01	0.00	0.03
Valves - Light Oil	0.21	<0.01	0.01	0.02	0.02	0.00	0.26
Flanges - Light Oil	<0.01	<0.01	<0.01	<0.01	<0.01	0.00	<0.01
Connectors - Light Oil	0.06	<0.01	<0.01	<0.01	0.01	0.00	0.08
Other - Light Oil	0.03	<0.01	<0.01	<0.01	<0.01	0.00	0.03
Components in Liquid Service =	0.30	<0.01	0.02	0.02	0.03	0.00	0.37
Total (Gas + Liquid Components) =	0.32	<0.01	0.02	0.02	0.03	0.00	0.40

Typical Component Count per Equipment Type based on Representative Facility³

Source Type/Service	WH	GPU	HT	LPT	FGC	OT	TT-O	SP
Valves - Gas	12	3	2	5	5	0	0	0
Flanges - Gas	37	15	9	24	33	3	2	0
Compressor Seals - Gas	0	0	0	0	3	0	0	0
Relief Valves - Gas	1	3	1	1	1	1	1	0
Open-Ended Lines - Gas	0	0	0	0	0	0	0	0
Valves - Light Oil	0	5	6	12	3	6	9	8
Flanges - Light Oil	0	0	0	0	0	0	0	6
Connectors - Light Oil	0	20	24	48	12	24	30	20
Pump Seals - Light Oil	0	0	0	0	0	0	0	0
Other - Light Oil	0	0	0	0	0	0	0	1

Equipment Type	WH	GPU	HT	LPT	FGC	ОТ	TT-O	SP
Number of Each Type On Pad =	7	7	2	0	2	8	1	7

Speciated Gas Analysis⁴

Component	Molecular Weight	Mole %	Equiv. Wt. Basis	Weight %	HC Weight %	lb/hr	TPY
Hydrogen Sulfide	34.082	0.000%	0.000	0.000%	-	0.00	0.00
Carbon Dioxide	44.010	0.133%	0.059	0.264%	-	0.01	0.03
Nitrogen	28.013	0.496%	0.139	0.627%	-	0.02	0.07
Methane	16.042	70.754%	11.350	51.223%	51.683%	1.29	5.66
Ethane	30.069	18.380%	5.527	24.941%	25.165%	0.63	2.76
Propane	44.096	7.198%	3.174	14.324%	14.453%	0.36	1.58
i-Butane	58.122	0.590%	0.343	1.548%	1.561%	0.04	0.17
n-Butane	58.122	1.711%	0.994	4.488%	4.528%	0.11	0.50
i-Pentane	72.149	0.214%	0.154	0.697%	0.703%	0.02	0.08
n-Pentane	72.149	0.317%	0.229	1.032%	1.041%	0.03	0.11
n-Hexane	86.175	0.067%	0.058	0.261%	0.263%	0.01	0.03
Other Hexanes	86.175	0.080%	0.069	0.311%	0.314%	0.01	0.03
Heptanes (as n-Heptane)	100.202	0.041%	0.041	0.185%	0.187%	<0.01	0.02
Benzene	78.114	0.001%	0.001	0.004%	0.004%	<0.01	<0.01
Toluene	92.141	0.001%	0.001	0.004%	0.004%	<0.01	<0.01
Ethylbenzene	106.167	0.000%	0.000	0.000%	0.000%	0.00	0.00
Xylenes	106.167	0.001%	0.001	0.005%	0.005%	<0.01	<0.01
2,2,4-Trimethylpentane	114.230	0.000%	0.000	0.000%	0.000%	0.00	0.00
Octanes (as n-Octane)	114.229	0.011%	0.013	0.057%	0.057%	<0.01	0.01
Nonanes (as n-Nonane)	128.255	0.003%	0.004	0.017%	0.018%	<0.01	<0.01
Decanes (as n-Decane)	142.282	0.002%	0.003	0.013%	0.013%	<0.01	<0.01
	TOTAL =	100.00%	22.16	100.00%	100.00%	2.52	11.05
		TOTAL HC =	21.96	TOTAL VOC =	23.15%	0.58	2.53
				TOTAL HAP =	0.28%	0.01	0.03

Speciated Liquids Analysis⁴

Component	Molecular Weight	Mole %	Equiv. Wt. Basis	Weight %	HC Weight %	lb/hr	TPY
Hydrogen Sulfide	34.082	0.000%	0.000	0.000%	-	0.00	0.00
Carbon Dioxide	44.010	0.010%	0.004	0.005%	-	<0.01	<0.01
Nitrogen	28.013	0.015%	0.004	0.005%	-	<0.01	<0.01
Methane	16.042	5.084%	0.816	1.018%	1.018%	0.01	0.06
Ethane	30.069	9.419%	2.832	3.536%	3.536%	0.05	0.20
Propane	44.096	13.438%	5.926	7.398%	7.398%	0.10	0.42
i-Butane	58.122	2.701%	1.570	1.960%	1.960%	0.03	0.11
n-Butane	58.122	11.641%	6.766	8.447%	8.448%	0.11	0.48
i-Pentane	72.149	3.950%	2.850	3.558%	3.558%	0.05	0.20
n-Pentane	72.149	7.673%	5.536	6.911%	6.912%	0.09	0.40
n-Hexane	86.175	4.799%	4.136	5.163%	5.163%	0.07	0.30
Other Hexanes	86.175	4.886%	4.211	5.256%	5.257%	0.07	0.30
Heptanes (as n-Heptane)	100.202	8.310%	8.327	10.395%	10.396%	0.14	0.59
Benzene	78.114	0.067%	0.052	0.065%	0.065%	<0.01	<0.01
Toluene	92.141	0.271%	0.250	0.312%	0.312%	<0.01	0.02
Ethylbenzene	106.167	0.283%	0.300	0.375%	0.375%	<0.01	0.02
Xylenes	106.167	0.411%	0.436	0.545%	0.545%	0.01	0.03
2,2,4-Trimethylpentane	114.230	0.000%	0.000	0.000%	0.000%	0.00	0.00
Octanes (as n-Octane)	114.229	6.334%	7.235	9.033%	9.034%	0.12	0.52
Nonanes (as n-Nonane)	128.255	4.366%	5.600	6.991%	6.991%	0.09	0.40
Decanes (as n-Decane)	142.282	16.342%	23.252	29.028%	29.031%	0.38	1.66
	TOTAL =	100.00%	80.10	100.00%	100.00%	1.31	5.72
		TOTAL HC =	80.09	TOTAL VOC =	95.45%	1.25	5.46
				TOTAL HAP =	6.46%	0.08	0.37

¹Component counts taken by equipment type at representative facility and made site-specific according to the number of each equipment type at this site.

² Emission Factor Source: EPA-453/R-95-017. TOC multiplied by pollutant content of streams (weight %) to obtain pollutant emissions.

³ Equipment Type Key: WH = Well Head, GPU = Gas Production Unit, HT = Heater, LPT = Low-Pressure Tower, FGC = Flash Gas Compressor, OT = Oil Tank, TT-O = Tank Truck - Oil SP = Separator

⁴Gas and liquids analyses located in Attachment L.

SWN Production Company, LLC John Good Jr Pad Fugitive Haul Road Emissions

Facility Data 1

Vehicle Type	Light Vehicles (Pick-ups and Cars)	Medium Trucks (Service Trucks)	Heavy Trucks (Tanker Trucks) ²
Average vehicle weight ((empty + full)/2) (tons)	2	15	23.5
Number of wheels per vehicle type (w)	4	10	18
Average number of round trips/day/vehicle type	5	3	20
Distance per round trip (miles/trip)	1.25	1.25	1.25
Vehicle miles travelled (miles/day)	6.24	3.75	24.39
Number of days operational (days/yr)	365	365	365
Vehicle miles travelled VMT (miles/yr)	2,279	1,367	8,901
Average vehicle speed S (mph)	10	10	10
Average number of round trips/hour/vehicle type	0.28	0.17	1.09
Average number of round trips/year/vehicle type	1,825	1,095	7,129
Estimated maximum number of round trips/hour/vehicle type	3	3	2
Estimated maximum number of round trips/day/vehicle type	6	4	22
Estimated maximum number of round trips/year/vehicle type	2,300	1,533	8,252

Formula & Calculation Inputs

E=k(s/12) ^a * (W/3) ^b * ((365-P) / 365)	Reference : A	P-42, Section	13.2.2 (11/06), Equation 1a and 2	
where:	Rate	Units	Comment	
Days per year	365	_		
Annual average hours per day of road operations	18	_		
k = PM Particle Size Multiplier	4.90	lb/VMT	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2 (PM)	
k = PM10 Particle Size Multiplier	1.50	lb/VMT	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2 (PM ₁₀)	
k = PM2.5 Particle Size Multiplier	0.15	lb/VMT	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2 (PM _{2.5})	
s = Surface Material Silt Content	3.9	%	State Default Data from AP-42 Data (1999 NEI Data)	
P = Number of days > 0.01 inch of rain	150	days/year	AP-42 Section 13.2.2 (11/06), Figure 13.2.2-1	
a = PM Constant	0.70	unitless	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2 (PM)	
a = PM10 & PM2.5 Constant	0.90	unitless	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2 (PM ₁₀ & PM _{2.5})	
b = PM, PM10, & PM2.5 Constant	0.45	unitless	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2	
Total hourly fleet vehicle miles travelled (miles/hr)	1.91	VMT/hr		
Total annual fleet vehicle miles travelled (miles/yr) ³	12,546.25	VMT/yr		
Average wheels ⁴	15	_		
Average vehicle weight of the fleet (W) ⁵	18.7	tons		
Moisture Ratio	1.00	_	Estimated based on 0.2% uncontrolled surface water content assuming no watering	EPA - BID Document 13.2.2 - 1998
Control Efficiency (CF)	0.00	%	Based on Moisture Ratio and Figure 13.2.2-2 Control	

190 Average Tanker Volume (bbl)
7,980 Gallons Tanker Volume
1,493 bwpd
2,218 bopd
19.53 Tanker Trucks per Day
2,871 Length Leased Access Road (ft)
425 Longest Pad Side (ft)
6,592 Total Round Trip Feet

SWN Production Company, LLC John Good Jr Pad Fugitive Haul Road Emissions (Continued)

	Emission	Factors		Control	Control Total Vehicle Miles			Emission Rates	;	Emission Rates		
	PM	PM ₁₀	PM _{2.5}	Efficiency			Total PM	Total PM ₁₀	PM _{2.5}	Total PM	Total PM ₁₀	PM _{2.5}
Vehicle Type	(lbs/VMT)	(lbs/VMT)	(lbs/VMT)	(%)	(VMT/hr)	(VMT/yr)	(lb/hr)	(lb/hr)	(lb/hr)	(tons/yr)	(tons/yr)	(tons/yr)
Light Vehicles	2.99	0.73	0.07	0.00	0.35	2,278.55	1.04	0.25	0.03	3.41	0.83	0.08
Medium Trucks	2.99	0.73	0.07	0.00	0.21	1,367.13	0.62	0.15	0.02	2.05	0.50	0.05
Heavy Trucks	2.99	0.73	0.07	0.00	1.35	8,900.56	4.05	0.99	0.10	13.32	3.26	0.33
Total =				0.00	1.91	12,546.25	5.71	1.40	0.14	18.77	4.59	0.46

Notes:

- 1) Facility vehicle data based on estimates, GP5.1 and AP-42 13.2.2-2 defaults for industrial unpaved roads
- 2) Tank trucker average vehicle weight as $(W_{(emoty)}+W_{(full)})/2 = (7 + 40)/2 = 23.7$ tons
- 3) Average vehicle miles travelled (VMT/yr) as (No. of round trip/vehicle * No. of vehicles/type * Roundtrip miles/trip)* 365 days/yr * No. of vehicle type)
- 4) Average wheels calculated as average of (No. of wheels per vehicle type * No. of vehicle/type)
- 5) Average vehicle fleet calculated as (Average weight of vehicle type * Percentage of each vehicle type on unpaved surface). Percentage of each vehicle type= VMT_{vehicle type}/VMT
- 6) Minimum one-per-day average pick-up trucks and service trucks even if tanker not required every day.
- 7) Per EPA BID calculations, all emissions based on average trips. Estimated maximum hourly, daily and yearly trips provided for information only.

Calculation of Emission Factors (AP-42, 13.2.2)

Equation 1a: $EF = k(s/12)^a (W/3)^b$ where k, a, and b are empirical constants and EF = size-specific emission factor (Ib/VMT) s = surface material silt content % W = mean vehicle weight (tons)

Equation 2: $EF_{ext} = EF^*((365-P)/365)$ where:

 $EF_{\rm ext}$ = annual size-specific emission factor extrapolated for natural mitigation, lb/VMT

EF = emission factor from Equation 1a

P = number of days in a year with at least 0.01 inches of precipitation

Calculation of Emissions

 $E = EF_{ext} * VMT/yr * ((1-CF)/100) * 1 ton/2000 lbs where:$

E = annual emissions (tons/yr)

 EF_{ext} = annual size-specific emission factor extrapolated for natural mitigation, lb/VMT

CF = control efficiency (%)

ATTACHMENT U: FACILITY-WIDE EMISSION SUMMARY SHEETS

ATTACHMENT U - FACILITY-WIDE CONTROLLED EMISSIONS SUMMARY SHEET

List all sources of emissions in this table. Use extra pages if necessary.

Emission Point ID #	N	O_X	C	O	V	OC	S	O_2	PN	I_{10}	PN	12.5		CH4	GHG	(CO ₂ e)
Ellission Folia ID#	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
EP-ENG1	0.32	1.40	0.64	2.80	0.31	1.36	< 0.01	< 0.01	0.02	0.11	0.02	0.11	< 0.01	0.01	155.19	679.73
EP-ENG2	0.32	1.40	0.64	2.80	0.31	1.36	< 0.01	< 0.01	0.02	0.11	0.02	0.11	< 0.01	0.01	155.19	679.73
EP-GPU1	0.11	0.48	0.09	0.41	0.01	0.03	< 0.01	< 0.01	0.01	0.04	0.01	0.04	< 0.01	0.01	117.10	512.89
EP-GPU2	0.11	0.48	0.09	0.41	0.01	0.03	< 0.01	< 0.01	0.01	0.04	0.01	0.04	< 0.01	0.01	117.10	512.89
EP-GPU3	0.11	0.48	0.09	0.41	0.01	0.03	< 0.01	< 0.01	0.01	0.04	0.01	0.04	< 0.01	0.01	117.10	512.89
EP-GPU4	0.11	0.48	0.09	0.41	0.01	0.03	< 0.01	< 0.01	0.01	0.04	0.01	0.04	< 0.01	0.01	117.10	512.89
EP-GPU5	0.11	0.48	0.09	0.41	0.01	0.03	< 0.01	< 0.01	0.01	0.04	0.01	0.04	< 0.01	0.01	117.10	512.89
EP-GPU6	0.11	0.48	0.09	0.41	0.01	0.03	< 0.01	< 0.01	0.01	0.04	0.01	0.04	< 0.01	0.01	117.10	512.89
EP-GPU7	0.11	0.48	0.09	0.41	0.01	0.03	< 0.01	< 0.01	0.01	0.04	0.01	0.04	< 0.01	0.01	117.10	512.89
EP-SH1	0.17	0.73	0.14	0.61	0.01	0.04	< 0.01	< 0.01	0.01	0.06	0.01	0.06	< 0.01	0.01	175.65	769.33
EP-SH2	0.17	0.73	0.14	0.61	0.01	0.04	< 0.01	< 0.01	0.01	0.06	0.01	0.06	< 0.01	0.01	175.65	769.33
EP-LOAD-COND	-	-	-	-	8.36	36.62	-	-	-	-	-	-	1.20	5.24	29.92	131.03
EP-LOAD-PW	-	-	-	-	0.41	1.81	-	-	-	-	-	-	0.81	3.53	20.15	88.24
APC-COMB	4.16	18.20	8.28	36.26	5.42	23.72	< 0.01	< 0.01	0.09	0.38	0.09	0.38	0.07	0.29	3,528.83	15,456.28
TOTAL	5.90	25.84	10.48	45.92	14.87	65.13	0.01	0.04	0.22	0.96	0.22	0.96	2.10	9.18	5,060.25	22,163.89

Annual emissions shall be based on 8,760 hours per year of operation for all emission units except emergency generators.

According to 45CSR14 Section 2.43.e, fugitive emissions are not included in the major source determination because it is not listed as one of the source categories in Table 1. Therefore, fugitive emissions shall not be included in the PTE above.

Note that the emissions from the APC-COMB includes uncombusted emissions from the uncombusted emissions from the tanks and loading operations, as well as combustor pilot emissions.

ATTACHMENT U – FACILITY-WIDE HAP CONTROLLED EMISSIONS SUMMARY SHEET														
List all sources of emissions in this table. Use extra pages if necessary.														
Emission Point ID #	Formaldehyde		Benzene		Toluene		Ethylbenzene		Xylenes		Hexane		Total HAPs	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
EP-ENG1	0.09	0.38	< 0.01	0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	-	-	0.10	0.44
EP-ENG2	0.09	0.38	< 0.01	0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	-	-	0.10	0.44
EP-GPU1	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	-	-	-	-	< 0.01	0.01	< 0.01	0.01
EP-GPU2	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	-	-	-	-	< 0.01	0.01	< 0.01	0.01
EP-GPU3	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	-	-	-	-	< 0.01	0.01	< 0.01	0.01
EP-GPU4	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	-	-	-	-	< 0.01	0.01	< 0.01	0.01
EP-GPU5	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	-	-	-	-	< 0.01	0.01	< 0.01	0.01
EP-GPU6	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	-	-	-	-	< 0.01	0.01	< 0.01	0.01
EP-GPU7	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	-	-	-	-	< 0.01	0.01	< 0.01	0.01
EP-SH1	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	-	-	-	-	< 0.01	0.01	< 0.01	0.01
EP-SH2	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	< 0.01	-	-	-	-	< 0.01	0.01	< 0.01	0.01
EP-LOAD-COND	-	-	0.01	0.02	0.03	0.11	0.03	0.14	0.05	0.20	0.43	1.89	0.54	2.37
EP-LOAD-PW	-	-	< 0.01	< 0.01	< 0.01	0.01	< 0.01	0.01	< 0.01	0.01	0.02	0.09	0.03	0.12
APC-COMB	< 0.01	< 0.01	0.01	0.04	0.04	0.19	0.05	0.23	0.08	0.34	0.73	3.21	0.92	4.02
TOTAL	0.17	0.76	0.01	0.06	0.05	0.20	0.05	0.23	0.08	0.34	0.75	3.30	1.14	4.98

Annual emissions shall be based on 8,760 hours per year of operation for all emission units except emergency generators.

According to 45CSR14 Section 2.43.e, fugitive emissions are not included in the major source determination because it is not listed as one of the source categories in Table 1. Therefore, fugitive emissions shall not be included in the PTE above.

Note that the emissions from the APC-COMB includes uncombusted emissions from the uncombusted emissions from the tanks and loading operations, as well as combustor pilot emissions.

ATTACHMENT V: LEGAL ADVERTISEMENT

Note: Affidavit of Publication will be submitted upon receipt by SWN from the publisher.

AIR QUALITY PERMIT NOTICE Notice of Application

Notice is given that SWN Production Company, LLC has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a G70-D General Permit Registration for a natural gas production facility (John Good Jr Pad) located in Brooke County, West Virginia. From I-70 take exit 1A to SR-2 North. Travel SR-2 North for 15.1 miles to SR-67 and turn right on SR-67. Travel 2.5 miles to CR-24, (McAdoo Ridge Rd), and turn left. Turn immediately right and travel 1.1 miles to access road on right. Latitude and longitude coordinates are 40.231762, -80.582193.

The applicant estimates the potential to discharge the following Regulated Air Pollutants will be:

Nitrogen Oxides (NOx)	25.84 tons/yr				
Carbon Monoxide (CO)	45.92 tons/yr				
Volatile Organic Compounds (VOC)	73.13 tons/yr				
Sulfur Dioxide (SO ₂)	0.04 tons/yr				
Particulate Matter (PM)	19.73 tons/yr				
Acetaldehyde	0.03 tons/yr				
Acrolein	0.03 tons/yr				
Benzene	0.06 tons/yr				
Ethylbenzene	0.25 tons/yr				
Formaldehyde	0.76 tons/yr				
Methanol	0.03 tons/yr				
n-Hexane	3.62 tons/yr				
Toluene	0.22 tons/yr				
Xylenes	0.37 tons/yr				
Carbon Dioxide	21,922.13 tons/yr				
Methane	14.90 tons/yr				
Nitrous Oxide	0.04 tons/yr				
CO ₂ Equivalent	22,306.86 tons/yr				

Operations is planned to begin on or about August 1, 2017. Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice. Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1250, during normal business hours.

Dated this the XXth of June 2017

SWN Production Company, LLC John Good Jr Pad June 2017

By: SWN Production Company, LLC

Carla Suszkowski, P.E.

Regulatory Manager – West Virginia Division

10000 Energy Drive Spring, TX 77389