

CNX Gas Company LLC

Sims Run Station

Camden, West Virginia

**Permit Determination** 

SLR Ref: 116.00894.00071

October 2017 SLR



## **Sims Run Station Permit Determination**

Prepared for:

**CNX Gas Company LLC** 1000 Consol Energy Drive Canonsburg, PA 15317

This document has been prepared by SLR International Corporation. The material and data in this permit application were prepared under the supervision and direction of the undersigned.

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# SECTION 1. TECHNICAL SUPPORT DOCUMENT

# **Permit Determination**

Sims Run Station Camden, West Virginia

CNX Gas Company LLC 1000 Consol Energy Drive Canonsburg, PA 15317

## 1.1 INTRODUCTION

Sims Run Station is used as a booster station for wells located within the surrounding area. It is currently a non-permitted site planning to operate with (1) 4SRB 145 hp Compressor Engine (Cat 3306 NA) and (1) 50 bbl pipeline liquids tank. There are also (3) wells located within ¼ mile of the site. The nearby wells make it necessary to evaluate the (1) 50 bbl tanks and (5) 100 bbl tanks associated with them. Emission calculations within this determination account for all of the tanks, as well as the reciprocating internal combustion engine (RICE).

The details of this evaluation are provided in section 2.0 with supporting calculations and ProMax Simulations conducted for worst case operating scenarios.

## 1.2 SITE HISTORY

The site is being evaluated to identify any after the fact permitting obligations that may be triggered as a result of applicable engine standards under the Federal NSPS provisions of 40CFR60 Subpart JJJJ.

## **1.3 DESCRIPTION OF FACILITY**

CNX Gas Company LLC is submitting a permit determination to evaluate existing and future equipment at and around Sims Run Station. Emission sources included within the determination include: (1) 4SRB 145 hp Compressor Engine (Cat 3306 NA) manufactured in April, 2008, (2) 50 bbl produced liquids tank, and (5) 100 bbl produced liquids tanks.

## **Description of Emission Calculations**

The tanks were estimated to have a worst case throughput of 5 bbl/day. The tank emissions were estimated using ProMax with representative samples of gas and condensate taken from the Minnie Lee No.1 well pad. The Minnie Lee No.1 condensate composition is viewed as a worst case representation. This estimate predicts approximately 0.97 tpy of VOCs originating from the tanks, these emissions included flashing losses as well as working and breathing losses. The amount of condensate produced at the station is minimal and therefore all produced liquids are sent to the storage vessel (T-1) and hauled from the site via 100 bbl tank truck.

## 1.4 FEDERAL AND STATE REQUIREMENT

## APPLICABLE REGULATIONS

This facility is subject to the following applicable rules and regulations:

## Federal and State:

**40 CFR 61** - This facility is subject to the asbestos inspection and notification requirements. However, there has been no demolition or renovation activity at this site.

**45 CSR 13 -** Permits for Construction, Modification, Relocation, and Operation of Stationary Source of Air Pollutants

The company is applying for a permit determination to assure all permitting thresholds are evaluated with respect to minor source permit requirements, as a result all commonly owned emissions sources are aggregated as one facility if located within ¼ miles from the booster station

## WV Code § 22-5-4 (a) (14)

The Secretary can request any pertinent information such as annual emission inventory reporting. This station is not required to submit an annual air emission inventory.

**45 CSR 17** - Fugitive Particulate Emissions

The site shall minimize fugitive PM so that emissions do not travel offsite.

**40 CFR 60, Subpart JJJJ** – Standards of Performance for Stationary Spark Ignition Internal Combustion Engines

The compressor engine (CE-1) at the station was manufactured on 4-24-2008, which predates the July 1, 2008 applicability date for engines less than 500 hp. Therefore, the compressor engine is not subject to emissions limits according to 40 CFR§60.4230-(a)(4)(iii). Additionally, the compressor will be installed as a booster at the Sims Run location in 2017 and therefore evaluated for applicability to §60.4236 related to requirements for installing previous model year engines. This engine was found to be exempt as a relocated unit according to §60.4236(e).

**40 CFR 63, Subpart ZZZZ** – National Emissions Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines

The natural gas compressor engine (CE-1) is a 4SRB Cat 3306 NA engine manufactured on 4-24-2008; therefore, per 40CFR63.6590(c)(1) the requirements of this regulation are to comply with new SI engines standards in accordance with 40CFR60, Subpart JJJJ.

## NON-APPLICABILITY DETERMINATIONS

The following requirements have been determined "not applicable" due to the following:

45 CSR 2 – Particulate Matter Standards from Combustion of Fuel in Indirect Heat Exchangers

No heat exchangers are in use at Sims Run Station or any of the surrounding wells.

45 CSR 10 - Emission of Sulfur Oxides

No fuel burning units are in use at Sims Run Station or any of the surrounding wells.

**45 CSR 27 -** To Prevent and Control the Emissions of Toxic Air Pollutants

This rule is not applicable because natural gas is included as a petroleum product and contains less than 5% benzene by weight. 45CSR § 27-2.4 exempts equipment "used in the production and distribution of petroleum products providing that such equipment does not produce or contact materials containing more than 5% benzene by weight."

45 CSR 30 – Requirements for Operating Permits – Title V of the Clean Air Act

This facility does not meet the emission thresholds to trigger a 45 CSR 30 Title V Operating Permit nor is it subject to any Federal Standards that require a Title V Permit.

## 40 CFR 60 Subpart K, Ka, Kb - Storage Vessel NSPS

The tanks onsite (T-1 through T-7) is below the size capacity threshold of 75 meters cubed (m^3) [19,813 gallons] defined within the applicability section 60.110b(a) of this Federal standard.

## 40 CFR 60 Subpart OOOO - Storage Vessel NSPS Requirements

The existing storage vessels predate the applicability date of this regulation, Aug 23, 2011.

## 40 CFR 60 Subpart OOOOa - Storage Vessel NSPS Requirements

The existing storage vessels predate the applicability date of this regulation, Sept 18, 2015.

## **40 CFR 60 Subpart OOOOa** – Fugitive Component Leak Monitoring

The site is classified as a compressor facility, which will not be subject to the monitoring requirement of this section since the existing site predates the applicability date of September 18, 2015 as defined under this Federal regulation. However, the site was also evaluated to determine if the installation of the new 3306NA (145 Hp) would trigger a modification. The evaluation compared against the previous 3406NA (215 Hp) which resulted in a decrease in Hp at the facility, thus exempting the site from qualifying as a modification.

**40 CFR 63 Subpart HH** - National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities

There is no dehydration unit at this site.

**40 CFR 63 HHH** - National Emission Standards for Hazardous Air Pollutants from Natural Gas Transmission and Storage Facilities

This subpart is related to Natural Gas Transmission Facilities which are major sources of HAPs. This federal regulation is not applicable since this facility is neither a transmission facility nor is it a major source.

40 CFR 63 Subpart DDDDD - Boilers & Process Heaters Located at Major Sources of HAPs

This subpart is not applicable because the facility is not a major source of HAPs.

## 40 CFR 63 Subpart JJJJJJ - Boilers Located at Area Sources of HAPs

This subpart is not applicable because there are no boilers located at the station or at the surrounding well pads.

## 40 CFR 82 Subpart F - Ozone Depleting Substances

The purpose of this subpart is to reduce emissions of class I and class II refrigerants and their substitutes. The facility does not utilize class I and class II refrigerants nor any substitutes.

## Aggregation Discussion (Facility Determination)

Sims Run Station is operated solely by CNX Gas Company LLC. All sites within a quarter mile of this facility have been evaluated for additional emissions. Sims Run Station is operated solely by CNX Gas Company LLC. All sites within a quarter mile of this facility have been evaluated for additional emissions. Three conventional wells were identified as having shared equipment within ¼ mile from the Sims Run booster station.

# **SECTION 2. APPLICATION FOR PERMIT DETERMINATION**

# **Permit Determination**

Sims Run Station Camden, West Virginia

CNX Gas Company LLC 1000 Consol Energy Drive Canonsburg, PA 15317

WEST VIRGINIA DEPARTMENT OF ENVIRONMENTAL PR DIVISION OF AIR QUALITY		INIA IENTAL PROTECTION QUALITY	PERMIT	T DETERMINATION FORM (PDF)	
6	601 57 <sup>th</sup> Stree Charleston, WV	t, SE / 25304	FOR AGENCY USE O	NLY: PLANT I.D. #	
	Phone: (304) 926-0475 www.dep.wv.gov/daq		PDF #	PERMIT WRITER:	
1.	NAME OF APPLICANT (AS REGISTERE	D WITH THE WV SECR	ETARY OF STATE'S OF	FFICE):	
	CNX Gas Company LLC				
2.	NAME OF FACILITY (IF DIFFERENT FRO	OM ABOVE):		3. NORTH AMERICAN INDUSTRY CLASSIFICATION SYSTEM (NAICS)	
	Sims Run Station			CODE:	
				211111	
4A.	MAILING ADDRESS:		4B. PHYSICAL ADDR	RESS:	
100	0 Consol Energy Drive Canonsburg, PA	15317	Sims Run Rd. Camden	n, WV	
5A.	DIRECTIONS TO FACILITY (PLEASE PR	OVIDE MAP AS ATTAC	CHMENT A):		
F	From Weston, take Route 33-W/119-S (towa located straight ahead.	ards Glenville) for 10.3 n	niles. Turn left on Sims F	Run Rd. and travel 1.7 miles. The station will be	
5B.	NEAREST ROAD:	5C. NEAREST CITY (	OR TOWN:	5D. COUNTY:	
Sim	s Run Rd.	Camden	Lewis		
5E.	UTM NORTHING (KM):	5F. UTM EASTING (K	<m):< td=""><td>5G. UTM ZONE:</td></m):<>	5G. UTM ZONE:	
4,32		534.799	17		
6A. Jerc	INDIVIDUAL TO CONTACT IF MORE INF	ORMATION IS REQUIR	RED:	6B. TITLE: HSE Field – Conventional WV Gas Operations	
6C.	TELEPHONE:	6D. FAX:		6E. E-MAIL:	
304-	-884-2219	<u> </u>		JerodDuelley@consolenergy.com	
7A.	DAQ PLANT I.D. NO. (FOR AN EXISTING	3 FACILITY ONLY):	7B. PLEASE LIST ALL CURRENT 45CSR13, 45CSR14, 45CSR19 AND/OR TITLE V (45CSR30) PERMIT NUMBERS ASSOCIATED WITH <b>THIS</b> PROCESS (FOR AN EXISTING FACILITY ONLY):		
				N/A	
7C.	IS THIS PDF BEING SUBMITTED AS TH	E RESULT OF AN ENFO	ORCEMENT ACTION?	IF YES, PLEASE LIST: No	
8A.	TYPE OF EMISSION SOURCE (CHECK	ONE):	8B. IF ADMINISTRAT APPLICANT'S CC PERMIT WITH TH	IVE UPDATE, DOES DAQ HAVE THE DNSENT TO UPDATE THE EXISTING HE INFORMATION CONTAINED HEREIN?	
	<b>MODIFICATION OTHER</b> (PLEASE EXPLAIN IN 11B)				
9.	IS DEMOLITION OR PHYSICAL RENOV	ATION AT AN EXISTING	3 FACILITY INVOLVED?	?	
10A	DATE OF ANTICIPATED INSTALLATION	OR CHANGE:	10B. DATE OF ANTICIPATED START-UP:		
	2017			2018	
11A. PLEASE PROVIDE A <b>DETAILED PROCESS FLOW DIAGRAM</b> SHOWING EACH PROPOSED OR MODIFIED PROCESS EMISSION POINT AS <b>ATTACHMENT B</b> .					
11B	. PLEASE PROVIDE A DETAILED PROCE	SS DESCRIPTION AS	ATTACHMENT C.		

12. PLEASE PROVIDE **MATERIAL SAFETY DATA SHEETS (MSDS)** FOR ALL MATERIALS PROCESSED, USED OR PRODUCED AS **ATTACHMENT D**. FOR CHEMICAL PROCESSE, PLEASE PROVIDE A MSDS FOR EACH COMPOUND EMITTED TO AIR.

#### 13A. REGULATED AIR POLLUTANT EMISSIONS:

Sec. State

 $\Rightarrow$  FOR A NEW FACILITY, PLEASE PROVIDE PLANT WIDE EMISSIONS BASED ON THE POTENTIAL TO EMIT (PTE) FOR THE FOLLOWING AIR POLLUTANTS INCLUDING ALL PROCESSES.

 $\Rightarrow$  FOR AN EXISTING FACILITY, PLEASE PROVIDE THE PROPOSED CHANGE IN EMISSIONS BASED ON THE PTE OF ALL PROCESS CHANGES FOR THE FOLLOWING AIR POLLUTANTS.

PTE FOR A GIVEN POLLUTANT IS TYPICALLY <u>BEFORE AIR POLLUTION CONTROL DEVICES</u> AND IS COLLECTED BASED ON THE MAXIMUM DESIGN CAPACITY OF PROCESS EQUIPMENT.

POLLUTANT	HOURLY PTE (LB/HR)	YEARLY PTE (TON/YR) (HOURLY PTE MULTIPLIED BY 8760 HR/YR) DIVIDED BY 2000 LB/TON			
РМ	0.03	0.12			
PM <sub>10</sub>	0.03	0.12			
VOCs	0.79	3.44			
со	4.86	21.28			
NO <sub>x</sub>	4.66	20.38			
SO <sub>2</sub>	0.01	0.01			
Pb	<0.01	<0.01			
HAPs (AGGREGATE AMOUNT)	0.11	0.45			
TAPs (INDIVIDUALLY)* Formaldehyde Benzene	0.09 0.01	0.38 0.01			
OTHER (INDIVIDUALLY)*					
* ATTACH ADDITIONAL PAGES AS	NEEDED				
13B. PLEASE PROVIDE ALL <b>SUPPORTING CALCULATIONS</b> AS <b>ATTACHMENT E</b> . CALCULATE AN HOURLY AND YEARLY PTE OF EACH PROCESS EMISSION POINT (SHOWN IN YOUR DETAILED PROCESS FLOW DIAGRAM) FOR ALL AIR POLLUTANTS LISTED ABOVE INCLUDING INDIVIDUAL HAP'S (LISTED IN SECTION 112[b] OF THE 1990 CAAA), TAP'S (LISTED IN 45CSR27), AND OTHER AIR POLLUTANTS (E.G. POLLUTANTS LISTED IN TABLE 45-13A OF 45CSR13, MINERAL ACIDS PER 45CSR7, ETC.).					
14. CERTIFICATION OF DATA  I, <u>CRAIG NEAL</u> ( <i>TYPE NAME</i> ) ATTEST THAT ALL THE REPRESENTATIONS CONTAINED IN THIS APPLICATION, OR APPENDED HERETO, ARE TRUE, ACCURATE, AND COMPLETE TO THE BEST OF MY KNOWLEDGE BASED ON INFORMATION AND BELIEF AFTER REASONABLE INQUIRY, AND THAT I AM A RESPONSIBLE OFFICIAL** ( <i>PRESIDENT, Vice President, Secretary or Treasurer, General Partner or Sole Proprietor</i> ) of the Applicant.  SIGNATURE OF RESPONSIBLE OFFICIAL:  TITLE: <u>VICE PRESIDENT GAS OPERATIONS</u> DATE:					
NOTE: PLEASE CHECK ENCLOSED ATTACHMENTS: ATTACHMENT A ATTACHMENT B ATTACHMENT C ATTACHMENT D ATTACHMENT E Records on all changes are required to be kept and maintained on-site for two (2) years. THE PERMIT DETERMINATION FORM WITH THE INSTRUCTIONS CAN BE FOUND ON DAQ'S PERMITTING SECTION WEB SITE: www.dep.wv.gov/daq					

## ATTACHMENT A

## **AREA MAP**

# **Permit Determination**

Sims Run Station Camden, West Virginia

CNX Gas Company LLC 1000 Consol Energy Drive Canonsburg, PA 15317



# ATTACHMENT B

# **PROCESS FLOW DIAGRAM**

# **Permit Determination**

Sims Run Station Camden, West Virginia

CNX Gas Company LLC 1000 Consol Energy Drive Canonsburg, PA 15317





# ATTACHMENT C

## **PROCESS DESCRIPTION**

## **Permit Determination**

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The compressor site will consist of (1) 4SRB Cat 3306 NA compressor and (2) 50 bbl produced liquids tanks. The site also has De Minimis tanks for new/used lube oil. There are (3) conventional wells within a quarter of a mile of a facility, as well as a master metering run. The (3) well sites add an additional (1) 50 bbl produced liquid tanks and (5) 100 bbl produced liquid tanks.

Sims Run Station collects gas from unconventional wells and provides compression services. Any liquid removed in the inlet separator will be sent to the produced liquids tank prior to compression. All tank and engine emissions will be uncontrolled.

The source's potential to emit was modeled using ProMax equation of state (EOS) software based on gas sampling taken from the Minnie Lee No.1 well pad. In accordance with DAQ guidance, emission potentials were evaluated and reported for truck loading, fugitive equipment leaks, and compressor blowdowns. The emission calculations summarized within this application show the facility's potential to emit to be no more than 20.38 tpy NOx, 21.28 tpy CO, and 3.44 tpy VOC.

# ATTACHMENT D

# SAFETY DATA SHEETS

## **Permit Determination**

Sims Run Station Camden, West Virginia

CNX Gas Company LLC 1000 Consol Energy Drive Canonsburg, PA 15317



## Safety Data Sheet (SDS)

### **Section 1 – Identification**

1(a) Product Identifier used on Label: Condensate

1(b) Other Means of Identification: Natural Gas Condensate, Produced Hydrocarbons, Drip Gas, Natural Gasoline, Petroleum Crude Oil Condensates

1(c) Recommended Use of the Chemical and Restrictions on Use: Used as a petrochemical feedstock, home heating fuel and refinery blending.

1(d) Name, Address, and Telephone Number:

CONSOL Energy Inc. 1000 CONSOL Energy Drive Canonsburg, PA 15317 General information: (724) 485-4000

1(e) Emergency Phone Number: Chemtrec (800) 424-9300

## Section 2 – Hazard(s) Identification

**2(a) Classification of the Chemical: Condensate** is considered a hazardous material according to the criteria specified in REACH [REGULATION (EC) No 1907/2006] and CLP [REGULATION (EC) No 1272/2008] and OSHA 29 CFR 1910.1200 Hazard Communication Standard. The categories of Health Hazards as defined in <u>"GLOBALLY HARMONIZED SYSTEM OF CLASSIFICATION AND LABELLING OF CHEMICALS (GHS), Third revised edition ST/SG/AC.10/30/Rev. 3" United Nations, New York and Geneva, 2009 have been evaluated. Refer to Section 3, 8 and 11 for additional information.</u>

2(b) Signal Word, Hazard Statement(s), Symbol(s) and Precautionary Statement(s):

Hazard Symbol	Hazard Classification	Signal Word	Hazard Statement(s)
	Flammable Liquid - 2		
	Germ Cell Mutagenicity - 1B Carcinogenicity - 1A Toxic Reproduction - 1B Specific Target Organ Toxicity (STOT) Following Single Exposure - 2 STOT following Repeated Exposure - 1 Aspiration - 1	Danger	Highly Flammable liquid and vapor Toxic if inhaled Causes skin irritation and serious eye irritation May cause genetic defects, cancer and damage fertility or the unborn child May cause damage to central and peripheral nervous system, lungs, liver and red blood cells
	Acute Toxicity Hazard - 3		Causes damage to the blood, spleen, and liver through prolonged or repeat exposures May be fatal if swallowed and enters airways
	Skin Corrosion/Irritation - 2 Eye Damage/ Irritation - 2A		
Precautionary	Statement(s)		
Keep away from heat/sparks/open flames/hot surfaces. No smoking. Keep container tightly closed.			If on skin: Wash with plenty of water If skin irritation occurs: Get medical advice/attention. Take off contaminated clothing and wash it before reuse.
Use explos	ion-proof electrical/ventilating/lighting/	equipment.	If swallowed: Immediately call a poison center/doctor/ Do NOT induce
Take p	Use only non-sparking tools. recautionary measures against static disc	charge.	vomiting. Obtain special instructions before use.
Wear protective gloves/protective clothing/eye protection/face			Do not handle until all safety precautions have been read and understood. Wash thoroughly after handling.
Do not breathe dust/fume/gas/mist/ vapors/spray.			Do not eat, drink or smoke when using this product.
If exposed, concerned or feel unwell: Get medical advice/attention.			If exposed or concerned: Call a poison center or doctor. Get medical attention if you feel unwell.
In maleu: Kemove person to fresh air and keep comfortable for breathing. Call a poison center/doctor.			Store in well-ventilated place. Keep cool. Use only outdoors or in a well- ventilated area. Store locked up.
contact lenses, if present and easy to do. Continue rinsing. If eye irritation persists: Get medical advice/attention.			Dispose of contents in accordance with federal, state and local regulations.



## Section 2 – Hazard(s) Identification (continued)

2(c) Hazards not Otherwise Classified: None Known or Found

2(d) Unknown Acute Toxicity Statement (mixture): None Known or Found

## Section 3 – Composition/Information on Ingredients

#### 3(a-c) Chemical Name, Common Name (synonyms), CAS Number and Other Identifiers, and Concentration:

J(a-c) Chemical Name, Common Name (synonyms), CAS Number and Other Tuentmers, and Concentration.						
Chemical Name	CAS Number	EC Number	% weight			
Natural Gas Condensate	64741-47-5	64741-47-5 265-047-3				
Natural Gas Condensate is a petroleum substance comprised of a complex mixture of hydrocarbons. Major classes of hydrocarbons contained in the substance are listed below:						
Hydrocarbons Aromatic	Mixture	Mixture	~ 5			
Hydrocarbons Naphthalenes	Mixture	Mixture	~ 8			
Hydrocarbons (total Paraffin and isoparaffin)	Mixture	Mixture	~ 65			
Benzene	71-43-2	200-753-7	~ 0.1			

EC - European Community

CAS - Chemical Abstract Service

## Section 4 – First-aid Measures

#### 4(a) Description of Necessary Measures: If exposed, concerned or feel unwell: Get medical advice/attention.

- Inhalation: If inhaled: Remove person to fresh air and keep comfortable for breathing. Call a poison center/doctor.
- Eye Contact: If in eyes: Rinse cautiously with water for several minutes. Remove contact lenses, if present and easy to do. Continue rinsing. If eye irritation persists: Get medical advice/attention.
- Skin Contact: If on skin: Wash with plenty of water. If skin irritation occurs: Get medical advice/attention. Take off contaminated clothing and wash it before reuse.
- Ingestion: If swallowed: Immediately call a poison center/doctor/ DO NOT induce vomiting.

#### 4(b) Most Important Symptoms/Effects, Acute and Delayed (chronic):

#### Acute Effects:

- Inhalation: Aspiration hazard, May be fatal if enters airways. May cause CNS and peripheral depression and damage to liver lungs and red blood cells.
- Eye: Causes irritation to eyes and mucous membranes.
- Skin: Causes irritation to skin.
- Ingestion: Aspiration hazard. May be fatal if swallowed.

#### Delayed (chronic) Effects:

• May cause genetic defects or cancer. May damage fertility or cause damage to the unborn child. Causes damage to the hematopoietic (blood) system, spleen, and liver through prolonged or repeat exposures.

4(c) Immediate Medical Attention and Special Treatment: If exposed, concerned or feel unwell: Get medical advice/attention.

#### **Additional Information:**

Primary Entry Routes: Inhalation, Ingestion, skin and eye contact.

**Target Organs:** Central nervous system, blood, eyes, skin lungs, and liver. Causes damage to the hematopoietic (blood) system, spleen, and liver. **Carcinogenicity:** IARC, NTP, ACGIH and OSHA list benzene as a carcinogen.

## **Section 5 – Fire-fighting Measures**

5(a) Suitable (and unsuitable) Extinguishing Media: In case of fire: Use foam, dry powder or carbon dioxide for extinction. Do not use a solid stream of water as it may scatter and spread the fire.

5(b) Specific Hazards Arising from the Chemical: Vapors are heavier than air and may accumulate in low areas. Fire will produce irritating, corrosive and toxic gasses.

**5(c) Special Protective Equipment and Precautions for Fire-Fighters:** Self-contained NIOSH approved respiratory protection and full protective clothing should be worn when fumes and/or smoke from fire are present. Heat and flames cause formation of acrid smoke and fumes. Do not release runoff from fire control methods to sewers or waterways. Firefighters should wear full face-piece self-contained breathing apparatus and chemical protective clothing with thermal protection. Direct water stream will scatter and spread flames and, therefore, should not be used. Evacuate area. Remove pressurized gas cylinders from the immediate vicinity. Cool containers exposed to flames with water until well after the fire is out. Close the valve if no risk is involved. Fight fire from a protected location. Prevent buildup of vapors or gases to explosive concentrations.



### **Section 6 - Accidental Release Measures**

**6(a) Personal Precautions, Protective Equipment and Emergency Procedures:** Spills of condensate will create a fire hazard and may form an explosive atmosphere. Stay up wind and away from the spill. Clean-up personnel should be protected against contact with eyes and skin. Collect material in appropriate, labeled containers for recovery or disposal in accordance with federal, state, and local regulations.

**6(b)** Methods and Materials for Containment and Clean Up: Collect with sand or oil absorbing materials. Collect material in appropriate, labeled containers for recovery or disposal in accordance with federal, state, and local regulations. Follow applicable OSHA regulations (29 CFR 1910.120) and all other pertinent state and federal requirements.

## **Section 7 - Handling and Storage**

7(a) Precautions for Safe Handling: Keep away from heat/sparks/open flames/hot surfaces. No smoking. Ground/Bond container and receiving equipment. Use explosion-proof electrical/ventilating/lighting/equipment. Use only non-sparking tools. Take precautionary measures against static discharge.

7(b) Conditions for Safe Storage, Including Any Incompatibilities: Store in well-ventilated place. Keep cool. Take precautions to avoid static discharges around stored condensate. Ground storage tanks and transfer piping. Use only outdoors or in a well-ventilated area. If feasible, store locked up.

## **Section 8 - Exposure Controls / Personal Protection**

**8(a) Occupational Exposure Limits (OELs):** The following exposure limits are offered as reference, for an experience industrial hygienist to review.

Ingredients	OSHA PEL <sup>1</sup>	ACGIH TLV <sup>2</sup>	NIOSH REL <sup>3</sup>	IDLH <sup>4</sup>
Benzene	1.0 ppm	0.5 ppm (1.6 mg/m <sup>3</sup> ), skin	0.1 ppm (0.32 mg/m <sup>3</sup> )	500 ppm
	"STEL" 5.0 ppm	"STEL" 2.5 ppm (8 mg/m <sup>3</sup> )	"STEL" 1.0 ppm (3.2 mg/m <sup>3</sup> )	

1. OSHA PEL are 8-hour TWA concentrations unless otherwise noted. A Short Term Exposure Limit (STEL) is defined in the benzene standard as: The employer shall assure that no employee is exposed to an airborne concentration of benzene in excess of five (5) ppm as averaged over any 15 minute period.

2. TLVs established by the ACGIH are 8-hour TWA concentrations unless otherwise noted. ACGIH TLVs are for guideline purposes only and as such are not legal, regulatory limits for compliance purposes. A Short Term Exposure Limit (STEL) is defined as the maximum concentration to which workers can be exposed for a short period of time (15 minutes) for only four times throughout the day with at least one hour between exposures.

- 3. The NIOSH-REL- Compendium of Policy and Statements. NIOSH, Cincinnati, OH (1992). NIOSH is the federal agency designated to conduct research relative to occupational safety and health. As is the case with ACGIH TLVs, NIOSH RELs are for guideline purposes only and as such are not legal, regulatory limits for compliance purposes.
- 4. The IDLHs are used by NIOSH as part of the respirator selection criteria and were first developed in the mid 1970's by NIOSH. The Documentation for IDLHs is a compilation of the rationale and sources of information used by NIOSH during the original determination of 387 IDLHs and their subsequent review and revision in 1994.

**8(b)** Appropriate Engineering Controls: Local exhaust ventilation should be used to control the emission of air contaminants. General dilution ventilation may assist with the reduction of air contaminant concentrations. Emergency eye wash stations and deluge safety showers should be available in the work area.

#### 8(c) Individual Protection Measures:

• **Respiratory Protection:** Seek professional advice prior to respirator selection and use. Follow OSHA respirator regulations (29 CFR 1910.134) and, if necessary, use only a NIOSH-approved respirator. Select respirator based on its suitability to provide adequate worker protection for given working conditions, level of airborne contamination, and presence of sufficient oxygen. Concentration in air of the various contaminants determines the extent of respiratory protection needed. Half-mask negative-pressure, air-purifying respirator equipped with organic vapor cartridge is acceptable for concentrations up to 10 times the exposure limit. Full-face negative-pressure air purifying respirator equipped with organic vapor cartridges is acceptable for concentrations up to 50 times the exposure limit. Protection by air purifying both negative-pressure and powered air respirators is limited. Use a positive-pressure-demand, full-face, supplied air respirator or self contained breathing apparatus (SCBA) for concentrations above 50 times the exposure limit. If exposure is above the IDLH (Immediately dangerous to life or health) for any of the constituents, or there is a possibility of an uncontrolled release or exposure levels are unknown, then use a positive-demand, full-face, supplied air respirator with escape bottle or SCBA.

Warning! Air-purifying respirators both negative-pressure, and powered-air do not protect workers in oxygen-deficient atmospheres.

- Eyes: Employees should be required to wear chemical safety glasses to prevent eye contact. A face shield should be used when appropriate to prevent contact with splashed materials. Chemical goggles, face shields or glasses should be worn to prevent eye contact. Contact lenses should not be worn where industrial exposure to this material is likely.
- Skin: Persons handling this product should wear appropriate clothing to prevent skin contact. Contaminated work clothing should not be allowed out of the workplace. Wash contaminated clothing before reuse. Wear protective gloves. Chemical goggles, face shields or glasses should be worn to prevent eye contact. Contact lenses should not be worn where industrial exposure to this material is likely. Wash skin that has been exposed with soap and water.
- Other Protective Equipment: An eyewash fountain and deluge shower should be readily available in the work area.

#### **Section 9 - Physical and Chemical Properties**

9(a) Appearance (physical state, color, etc.): Colorless to amber	9(j) Upper/lower Flammability or Explosive Limits: 10% / 1%
liquid	
9(b) Odor: gasoline - like	9(k) Vapor Pressure: 200-500 mmHg@68°F



## Section 9 - Physical and Chemical Properties (continued)

9(c) Odor Threshold: NA	9(1) Vapor Density (Air = 1): ND
9(d) pH: NA	9(m) Relative Density: 6.25 lbs/gal (Bulk Density)
9(e) Melting Point/Freezing Point: NA	9(n) Solubility(ies): ND
<b>9(f) Initial Boiling Point and Boiling Range:</b> 96.8 - 258 °F (36-125.6 °C)	9(o) Partition Coefficient n-octanol/water: ND
<b>9(g) Flash Point:</b> <-50°F (<-45.6 °C)	9(p) Auto-ignition Temperature: ND
9(h) Evaporation Rate: NA	9(q) Decomposition Temperature: ND
9(i) Flammability (liquid): Highly Flammable	9(r) Viscosity: ND
NA - Not Applicable	
<b>ND</b> - Not Determined for product as a whole	

## Section 10 - Stability and Reactivity

10(a) Reactivity: Not Determined (ND) for product as a whole.

10(b) Chemical Stability: Stable under normal storage and handling conditions.

10(c) Possibility of Hazardous Reaction: No Data Found

10(d) Conditions to Avoid: Storage with incompatible materials. Avoid heat, flame, or ignition sources.

10(e) Incompatible Materials: Strong acids and oxidizing agents.

10(f) Hazardous Decomposition Products: Can produce carbon dioxide and carbon monoxide.

## **Section 11 - Toxicological Information**

**11(a-e)** Information on Toxicological Effects: The following toxicity data have been determined using the information available for its components applied to the guidance on the preparation of an SDS under the GHS requirements of OSHA and the EU CPL:

Hazard Classification	Hazard EU*	Category OSHA	Hazard Symbols	Signal Word	Hazard Statement
Acute Toxicity Hazard (covers Categories 1-5)	NA**	3ª		Danger	Toxic if inhaled
Skin Corrosion/Irritation (covers Categories 1A, 1B, 1C and 2)	2	2 <sup>b</sup>		Warning	Causes skin irritation
<b>Eye Damage/ Irritation</b> (covers Categories 1, 2A and 2B)	NA**	2A <sup>c</sup>		Warning	Causes serious eye irritation
Skin/Dermal Sensitization (covers Category 1)	NA**	NA**	NA**	NA**	NA**
Germ Cell Mutagenicity (covers Categories 1A, 1B and 2)	1B	$1B^d$		Danger	May cause genetic defects
<b>Carcinogenicity</b> (covers Categories 1A, 1B and 2)	1B	1A <sup>e</sup>		Danger	May cause cancer
<b>Toxic Reproduction</b> (covers Categories 1A, 1B and 2)	NA**	$1B^{f}$		Danger	May damage fertility or the unborn child
Specific Target Organ Toxicity (STOT) Following Single Exposure (covers Categories 1-3)	NA**	2 <sup>g</sup>		Warning	May cause CNS and Peripheral depression, and damage lung liver (vacuoled hepatocytes) and red blood cells
<b>STOT following Repeated</b> <b>Exposure</b> (covers Categories 1 and 2)	NA**	1 <sup>h</sup>		Warning	May cause damage to the Hematopoietic system, spleen, liver through prolonged or repeat exposures
Aspiration (covers category 1)	1	1		Danger	May be fatal if swallowed and enters the airway

\*Natural Gas Condensate has been harmonized as - Base classification: High Benzene Naphtha, flashpoint  $< 23^{\circ}$ C and initial boiling point  $\ge 35^{\circ}$ C, benzene or 1,3-butadiene  $\ge 0.1\%$ , naphthalene < 25%.

\*\* Not Applicable - Many categories have conclusive but not sufficient for classification information.



Section 11 - Toxicological Information (continued)				
11(a-e) Information on toxicological effects (continued):				
a. The following $LC_{50}$ or $LD_{50}$ has been established for <b>Condensate</b> as a mixture:				
• Rat (4 hr) $LC_{50} > 5.2 \text{ mg/L}$				
• Rat (4 hr) $LC_{50} > 5.81 \text{ mg/L}$				
• Rat (4 hr) LC <sub>50</sub> >5.2 mg/L				
b. The following Skin Corrosion/Irritation information was found for Condensate as a mixture:				
• Rabbit – Slightly irritating.				
Rabbit - Irritating but not corrosive.				
<ul> <li>c. The following Eye Damage/Irritation information was found for Condensate as a mixture:</li> <li>Rabbit – Slightly irritating.</li> </ul>				
d. No Germ Cell Mutagenicity data available for Condensate as a mixture. The following Germ Cell Mutagenicity information was found for the components:				
Benzene - Positive with activation. Positive In vitro Clastogenicity.				
e. No Carcinogenicity data available for Condensate as a mixture. The following Carcinogenicity information was found for the components:				
Benzene - Listed as class 1 carcinogen by the NTP, IARC, EPA and ACGIH.				
f. No <b>Reproductive Toxicity</b> data available for <b>Condensate</b> as a mixture. The following <b>Reproductive Toxicity</b> information was found for the components:				
<ul> <li>Benzene - NOAEC for both adult and offspring toxicity and female fertility. 300ppm (960 mg/m<sup>3</sup>). NOAEC for maternal toxicity as teratogenicity was 100 ppm (320 mg/m<sup>3</sup>). The NOAEC for slight fetotoxicity was 40 ppm (128 mg/m<sup>3</sup>).</li> </ul>				
g. No <b>Specific Target Organ Toxicity (STOT) following Single Exposure</b> data available for <b>Condensate</b> as a mixture. The following STC following Single Exposure information was found for the components:				
• Benzene - CNS and peripheral Depression, lung liver (vacuoled hepatocytes) and red blood cells may be effected.				
h. No Specific Target Organ Toxicity (STOT) following Repeated Exposure data available for Condensate as a mixture. The following STOT following Repeated Exposure data is available for the components:				
<ul> <li>Benzene - Spleen hematopoiesis, Liver, lung kidney effects are specific to male Rat. Early signs and symptoms of chronic overexposure inclue effects on CNS &amp; the GI tract (headache, loss of appetite, drowsiness, nervousness, &amp; pallor) but the major manifestation of toxicity is aplass anemia. Bone marrow depression may occur resulting in leucopoenia, anemia, or thrombocytopenia (leukemogenic action). With continue exposure the disease states may progress to pancytopenia resulting from bone marrow aplasia. Evidence has linked benzene in the etiology leukemia.</li> </ul>				
The above toxicity information was determined from available scientific sources to illustrate the prevailing posture of the scientific community. The scientific resources includes: The American Conference of Governmental Industrial Hygienist (ACGIH) Documentation of the Threshold Limit Values (TLVs) and Biological Exposure indices (BEIs) with Other Worldwide Occupational Exposure Values 2009, The International Agency for Research on Cancer (IARC), The National Toxicology Program (NTP) updated documentation, the World Health Organization (WHO) and other available resources, the International Uniform Chemical Information Database (IUCLID), European Union Risk Assessment Report (EU-RAR), Concise International Chemical Assessment Documents (CICAD), European Union Scientific Committee for Occupational Exposure Limits (EU-SCOEL), Agency for Toxic Substances and Disease Registry (ATSDR), Hazardous Substance Data Bank (HSDB), and International Programme on Chemical Safety (IPCS).				
Section 12 - Ecological Information				
12(a) Ecotoxicity (aquatic & terrestrial): No Data Found				
12(b) Persistence & Degradability: Loss due to volatility. Not readily biodegradable but is inherently biodegradable by microorganisms.				
12(c) Bioaccumulative Potential: No Data Found				
12(d) Mobility (in soil): Will float on water and will volatilize in air.				
12(e) Other adverse effects: No Data Found				
Additional Information:				
Hazard Category: Not Reported Signal Word: No Signal Word				
Hazard Symbol:				
Hazard Statement: No Statement				
Section 13 - Disposal Considerations				
Disposal: Waste code D001: Waste Flammable material with a flash point <140°F. This material and its container must be disposed of				
hazardous waste. Under RCRA, it is the responsibility of the user of the product to determine, at the time of disposal, whether the product mee RCRA criteria for hazardous waste. <b>European Waste Catalogue (EWC):</b> 05-01-99 (waste from petroleum refining).				

**Container Cleaning and Disposal:** Containers should be completely empty prior to discarding. Dispose of contents in accordance with federal, state and local regulations. Observe safe handling precautions.

Please note this information is for Condensate in its original form. Any alterations can void this information.



## **Section 14 - Transportation Information**

#### 14(a-g) Transportation Information:

US DOT under 49 CFR 172.101 regulates Condensate as a hazardous material. All federal, state, and local laws and regulations that apply to the transport of this type of material must be adhered to. Shipping Name: RQ, UN3295, Hydrocarbon, Liquid, N.O.S. **Packaging Authorizations Ouantity Limitations** a) Exceptions: 150 PGIII (Benzene) a) Passenger, Aircraft, or Railcar: 60L Shipping Symbols: Flammable Liquid b) Non-Bulk: 203 b) Cargo Aircraft Only: 220L Hazard Class: 3 c) Bulk: 242 **Vessel Stowage Requirements** UN No.: UN3295 a) Vessel Stowage: A Packing Group: III b) Other: NA DOT/ IMO Label: 3 DOT Reportable Quantities: 10 lbs. Special Provisions (172.102): 144, B1, IB3, T4, TP1, TP29 IMDG and RID classification, packaging and shipping requirements follow the US DOT Hazardous Materials Regulation. ADR regulates Condensate as a hazardous material. Shipping Name: Hydrocarbons, Liquid, N.O.S. Portable Tanks & Bulk Containers Packaging **Classification Code: 3** a) Packing Instructions: P001, LP01 a) Instructions: T4 UN No.: 3295 b) Special Packing Provisions: NA b) Special Provisions: TP1, TP29 Packing Group: III c) Mixed Packing Provisions: NA ADR Label: Flammable Liquid Special Provisions: 223 Limited Quantities: 5L Excepted Quantities (EQ): E1 IATA regulates Condensate as a hazardous material. Shipping Name: Hydrocarbons, Liquid, N.O.S. Cargo Aircraft Only **Special Provisions:** Passenger & Cargo Aircraft A3 Class/Division: 3 Limited Quantity (EQ) Pkg Inst: 303 ERG Code: 3H Hazard Label (s): Flammable Liquid Pkg Inst: Pkg Inst: 302 Max Net Qty/Pkg: 30 Forbidden Max Net Qty/Pkg: L UN No.: 3295 Max Net Otv/Pkg: 1L Packing Group: 1 Forbidden Excepted Quantities (EQ): E3 Pkg Inst - Packing Instructions Max Net Qty/Pkg - Maximum Net Quantity per Package ERG - Emergency Response Drill Code TDG Classification: Condensate does have a TDG classification. **Section 15 - Regulatory Information** Regulatory Information: The following listing of regulations relating to a CONSOL Energy Inc. product may not be complete and should not be solely relied upon for all regulatory compliance responsibilities. This product and/or its constituents are subject to the following regulations: OSHA Regulations: Air Contaminant (29 CFR 1910.1000, Table Z-1, Z-2, Z-3): The product, Condensate as a whole is not listed. However, individual components of the product are listed: Refer to Section 8, Exposure Controls and Personal Protection EPA Regulations: Condensate is not listed as a whole. However, individual components of the product are listed: Components Regulations SARA 313, CERCLA, RCRA, SDWA, CWA, CAA Benzene SARA Potential Hazard Categories: Immediate Acute Health Hazard, Delayed Chronic Health Hazard, Fire Hazard **Regulations Key:** CAA Clean Air Act (42 USC Sec. 7412; 40 CFR Part 61 [As of: 8/18/06]) CERCLA Comprehensive Environmental Response, Compensation and Liability Act (42 USC Secs. 9601(14), 9603(a); 40 CFR Sec. 302.4, Table 302.4, Table 302.4 and App. A) CWA Clean Water Act (33 USC Secs. 1311; 1314(b), (c), (e), (g); 136(b), (c); 137(b), (c) [as of 8/2/06]) RCRA Resource Conservation Recovery Act (42 USC Sec. 6921; 40 CFR Part 261 App VIII) SARA Superfund Amendments and Reauthorization Act of 1986 Title III Section 302 Extremely Hazardous Substances (42 USC Secs. 11023, 13106; 40 CFR Sec. 372.65) and Section 313 Toxic Chemicals (42 USC Secs. 11023, 13106; 40 CFR Sec. 372.65 [as of 6/30/05]) TSCA Toxic Substance Control Act (15 U.S.C. s/s 2601 et seq. [1976]) SDWA Safe Drinking Water Act (42 U.S.C. s/s 300f et seq. [1974])

Section 313 Supplier Notification: This product, Condensate contains the following toxic chemicals subject to the reporting requirements of section 313 of Title III of the Superfund Amendments and Reauthorization Act of 1986 and 40 CFR part 372:

CAS #	Chemical Name	Percent by Weight
71-43-2	Benzene	0.1



	Section 15 - Regulatory Information (continued)					
Regulato	ry Information (continued):					
State Reg listed in v	<b>State Regulations:</b> The product, <b>Condensate</b> as a whole is not listed in any state regulations. However, individual components of the product are listed in various state regulations:					
Pennsylva	ania Right to Know: Contains regulated material in the follo	owing categor	ries:			
• Env	vironmental Hazards: Benzene	00				
• Spe	cial Hazardous Substance: Benzene					
California	a Prop. 65: This product contains materials known to the Sta	te of Califorr	ia to cause cancer. Benzene			
New Jerse	ey: Contains regulated material in the following categories:	Hazardous Su	ubstance: Benzene			
Minnesot	a: Benzene					
Massachu	isetts: Benzene					
Other Re WHMIS	gulations: Classification (Canadian): Condensate is not listed as a v	vhole. Howev	er individual components are listed.			
Ing	redients WHMIS Classification					
Ber	nzene D-2A, D-2B, B-2					
This product	t has been classified in accordance with the hazard criteria of the Controlled	Products Regulat	tions and the SDS contains all the information required by the Controlled Products			
Regulations.		_				
	Section 16 -	Other Inf	ormation			
Prepared	By: CONSOL Energy Inc.	Issue	<b>a Date:</b> 8/12/2013			
Addition	al Information:					
HMIS CI	assification	NFP	A			
Health H	Hazard 2		3			
Fire Haz	zard 3	2	1			
Physica	l Hazard 1					
	2 Tomporary or minor injury may occur	HEAT	$\mathbf{T}$ $\mathbf{T}$ $\mathbf{T}$ $\mathbf{T}$ $\mathbf{T}$ $\mathbf{T}$ $\mathbf{T}$ $\mathbf{T}$ $\mathbf{T}$			
FIRE = 3,	A materials capable of ignition under almost all normal temperature cond	litions. possib	le residual injury unless prompt medical attention is given.			
Includes flat	mmable liquids with flash points below 73 °F and boiling points above 100	°F, as FIRE	= 3, Liquids and solids that can be ignited under almost all ambient conditions.			
well as liqui	ds with flash points between 73 °F and 100 °F. (Classes IB & IC). HAZARD = 1 Materials that are normally stable but can become unstable	INSTA	ABILITY = 1, Normally stable, but can become unstable at elevated temperatures			
react) at hig	the temperatures and pressures. Materials may react non-violently with we	ater or	essures of may feact with water with some felease of energy, but not violently.			
undergo haz	ardous polymerization in the absence of inhibitors.					
ABBREV	/IATIONS/ACRONYMS:		1			
ACGIH	American Conference of Governmental Industrial Hygienists	mg/m <sup>3</sup>	milligram per cubic meter of air			
ADR	Regulations Concerning the International Carriage of	NFPA	National Fire Protection Association			
CAS	Chemical Abstracts Service	NIOSH	National Institute for Occupational Safety and Health			
CERCLA	Comprehensive Environmental Response, Compensation, and	NOAEC	No Observed Adverse Effect Concentration			
	Liability Act					
CFR	Code of Federal Regulations	NTP	National Toxicology Program			
CNS	Central Nervous System	OSHA	Occupational Safety and Health Administration			
CPL DOT	Classification, Labeling and Packaging PEL Permissible Exposure Limit					
DOI FC	Department of Transportation     ppm     parts per million					
EU	European Union	REACH	Registration Evaluation Authorization and Restriction of Chemical			
Le		REATON	substances.			
EWC	European Waste Catalogue	RID	Regulations Concerning the International Carriage of Dangerous			
CLOT	Castro Intestinal Castro Intestinal Tract	DEI	Goods by Rail  Pagemended Exposure Limits			
CHS	Globally Harmonized System	SDS	Safety Data Sheet			
HMIS	Hazardous Materials Identification System	SARA	Superfund Amendment and Reauthorization Act			
IARC	International Agency for Research on Cancer	SCBA	Self-contained Breathing Apparatus			
IATA	International Air Transport Association	STEL	Short Term Exposure Limit			
IDLH	Immediately Dangerous to Life or Health	TDG	Transport Dangerous Goods			
IMDG	International Maritime Dangerous Goods	TLV	Threshold Limit Value			
LC50	Median Lethal Concentration	TWA	Time-weighted Average			
	1	1 1				



## **Section 16 - Other Information (continued)**

#### ABBREVIATIONS/ACRONYMS (continued):

MSHA	Mine Safety and Health Administration
mg/L	milligram per liter
-	

WHMIS Workplace Hazardous Materials Information System

**Disclaimer:** This information is taken from sources or based upon data believed to be reliable. Our objective in sending this information is to help you protect the health and safety of your personnel and to comply with the OSHA Hazard Communication Standard and Title III of the Superfund Amendment and Reauthorization Act of 1986. CONSOL Energy Inc. makes no warranty as to the absolute correctness, completeness, or sufficiency of any of the foregoing, or any additional, or other measures that may be required under particular conditions. CONSOL Energy Inc. MAKES NO WARRANTIES, EXPRESS OR IMPLIED, INCLUDING THE IMPLIED WARRANTY OF MERCHANTABILITY, OR ANY IMPLIED WARRANTY OF FITNESS FOR A PARTICULAR PURPOSE, AND ANY IMPLIED WARRANTIES OTHERWISE ARISING FROM COURSE OF DEALING OR TRADE.

Product Name:Processed Natural GasProduct Code:NonePage 1 of 8

## 1. CHEMICAL PRODUCT AND COMPANY IDENTIFICATION

Product Name: Processed Natural Gas Product Code: None Synonyms: Dry Gas Generic Name: Natural Gas Chemical Family: Paraffin hydrocarbon

Responsible Party: Unocal Corporation Union Oil Company of California 14141 Southwest Freeway Sugar Land, Texas 77478

For further information contact MSDS Coordinator 8am - 4pm Central Time, Mon - Fri: 281-287-5310

#### EMERGENCY OVERVIEW

#### 24 Hour Emergency Telephone Numbers:

For Chemical Emergencies: Spill, Leak, Fire or Accident Call CHEMTREC North America: (800)424-9300 Others: (703)527-3887(collect)

For Health Emergencies: California Poison Control System (800)356-3129

Health Hazards: Use with adequate ventilation.

Physical Hazards: Flammable gas. Can cause flash fire. Gas displaces oxygen available for breathing. Keep away from heat, sparks, flames, or other sources of ignition (e.g., static electricity, pilot lights, mechanical/electrical equipment). Do not enter storage areas or confined space unless adequately ventilated.

- < Physical Form: Gas
- < Appearance: Colorless
- < Odor: Odorless in the absence of H2S or mercaptans

NFPA HAZARD CLASS: Health: 1 (Slight) Flammability: 4 (Extreme) Reactivity: 0 (Least)

Issue Date: 03/18/03 Revised Sections: 1, 3

Status: Final Revised

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Product Name:	Processed Natural Gas	
Product Code:	None	Page 2 of 8

## 2. COMPOSITION/INFORMATION ON INGREDIENTS

HAZARDOUS COMPONENTS	% Weight	EXPO	SURE GUIDE	LINE
		Limits	Agency	Туре
Methane CAS# 74-82-8	98	1000 ppm	MSHA	TWA
Carbon Dioxide CAS# 124-38-9	0-5	5000 ppm 30000 ppm 5000 ppm 5000 ppm 5000 ppm 30000 ppm	ACGIH ACGIH OSHA MSHA Cal.OSHA Cal.OSHA	TWA STEL TWA TWA STEL
Nitrogen CAS# 7727-37-9	0-5	1000 ppm	MSHA	TWA
Ethane CAS# 74-84-0	1	1000 ppm	MSHA	TWA

Note: State, local or other agencies or advisory groups may have established more stringent limits. Consult an industrial hygienist or similar professional, or your local agencies, for further information.

### 3. HAZARDS IDENTIFICATION

POTENTIAL HEALTH EFFECTS:

Eye: Not expected to be an eye irritant.

Skin: Skin contact is unlikely. Skin absorption is unlikely.

- Inhalation (Breathing): Asphyxiant. High concentrations in confined spaces may limit oxygen available for breathing.
- Ingestion (Swallowing): This material is a gas under normal
   atmospheric conditions and ingestion is unlikely.
- Signs and Symptoms: Light hydrocarbon gases are simple asphyxiants which, at high enough concentrations, can reduce the amount of oxygen available for breathing. Symptoms of overexposure can include shortness of breath, drowsiness, headaches, confusion,

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Revised Sect	ions:	1,	3		-	novibou

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decreased coordination, visual disturbances and vomiting, and are reversible if exposure is stopped. Continued exposure can lead to hypoxia (inadequate oxygen), cyanosis (bluish discoloration of the skin), numbness of the extremities, unconsciousness and death. High concentrations of carbon dioxide can increase heart rate and blood pressure.

Cancer: No data available.

Target Organs: No data available.

Developmental: Limited data - See Other Comments, below.

Other Comments: High concentrations may reduce the amount of oxygen available for breathing, especially in confined spaces. Hypoxia (inadequate oxygen) and respiratory acidosis (increased carbon dioxide in blood), during pregnancy may have adverse effects on the developing fetus. Exposure during pregnancy to high concentrations of carbon monoxide, which is produced during the combustion of hydrocarbon gases, can also cause harm to the developing fetus.

Pre-Existing Medical Conditions: None known.

#### 4. FIRST AID MEASURES

Eye: If irritation or redness develops, move victim away from exposure and into fresh air. Flush eyes with clean water. If symptoms persist, seek medical attention.

**Skin:** First aid is not normally required. However, it is good practice to wash any chemical from the skin.

Inhalation (Breathing): If respiratory symptoms develop, move victim away from source of exposure and into fresh air. If symptoms persist, seek medical attention. If victim is not breathing, immediately begin artificial respiration. If breathing difficulties develop, oxygen should be administered by qualified personnel. Seek immediate medical attention.

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Product	Name:	Processed	Natural	Gas
Product	Code:	None		

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## 5. FIRE FIGHTING MEASURES

Flammable Properties: Flash Point: Not applicable (gas) OSHA Flammability Class: Flammable gas LEL / UEL: No data Autoignition Temperature: 800-1000°F

- Unusual Fire & Explosion Hazards: This material is flammable and may be ignited by heat, sparks, flames, or other sources of ignition (e.g., static electricity, pilot lights, or mechanical/electrical equipment). Vapors may travel considerable distances to a source of ignition where they can ignite, flashback, or explode. May create vapor/air explosion hazard indoors, outdoors, or in sewers. If container is not properly cooled, it can rupture in the heat of a fire. Closed containers exposed t extreme heat can rupture due to pressure buildup.
- **Extinguishing Media:** Dry chemical or carbon dioxide is recommended. Carbon dioxide can displace oxygen. Use caution when applying carbon dioxide in confined spaces.
- Fire Fighting Instructions: For fires beyond the incipient stage, emergency responders in the immediate hazard area should wear When the potential chemical hazard is unknown, in bunker gear. enclosed or confined spaces, or when explicitly required by DOT, a self-contained breathing apparatus should be worn. In addition, wear other appropriate protective equipment as conditions warrant (see Section 8). Isolate immediate hazard area, keep unauthorized personnel out. Stop spill/release if it can be done with minimal risk. If this cannot be done, allow fire to burn. Move undamaged containers from immediate hazard area if it can be done with minimal risk. Stay away from ends of container. Water spray may be useful in minimizing or dispersing vapors. Cool equipment exposed to fire with water, if it can be done with minimal risk.

#### 6. ACCIDENTAL RELEASE MEASURES

Flammable. Keep all sources of ignition and hot metal surfaces away from spill/release. The use of explosion-proof equipment is recommended. Stay upwind and away from spill/release. Notify persons down wind of spill/release, isolate immediate hazard area and keep unauthorized personnel out. Stop spill/release if it can be done with

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Product	Name:	Processed Natural Gas				
Product	Code:	None	Page	5	of	8
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minimal risk. Wear appropriate protective equipment including respiratory protection as conditions warrant (see Section 8). Notify fire authorities and appropriate federal, state, and local agencies. Water spray may be useful in minimizing or dispersing vapors (see Section 5).

## 7. HANDLING AND STORAGE

- Handling: The use of explosion-proof equipment is recommended and may be required (see appropriate fire codes). Do not enter confined spaces such as tanks or pits without following proper entry procedures such as ASTM D-4276 and 29CFR 1910.146. The use of appropriate respiratory protection is advised when concentrations exceed any established exposure limits (see Section 2 and 8). Use good personal hygiene practice.
- Storage: Keep container(s) tightly closed. Use and store this
  material in cool, dry, well-ventilated areas away from heat,
  direct sunlight, hot metal surfaces, and all sources of ignition.
  Post area "No Smoking or Open Flame." Store only in approved
  containers. Keep away from any incompatible material (see
  Section 10). Protect container(s) against physical damage.
  Outdoor or detached storage is preferred.

## 8. EXPOSURE CONTROLS/PERSONAL PROTECTION

Engineering controls: If current ventilation practices are not adequate to maintain airborne concentrations below the established exposure limits (see Section 2), additional ventilation or exhaust systems may be required. Where explosive mixtures may be present, electrical systems safe for such locations must be used (see appropriate electrical codes).

Personal Protective Equipment (PPE):

- Respiratory: Wear a positive pressure air supplied respirator in oxygen deficient environments (oxygen content <19.5%). A respiratory protection program that meets OSHA's 29 CFR 1910.134 and ANSI Z88.2 requirements must be followed whenever workplace conditions warrant a respirator's use.
- Skin: Not required based on the hazards of the material. However, it is considered good practice to wear gloves when handling chemicals.

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**Eye/Face:** While contact with this material is not expected to cause irritation, the use of approved eye protection to safeguard against potential eye contact is considered good practice.

Other Protective Equipment: A source of clean water should be available in the work area for flushing eyes and skin. Impervious clothing should be worn as needed. Self-contained respirators should be available for non-routine and emergency situations.

## 9. PHYSICAL AND CHEMICAL PROPERTIES

Note: Unless otherwise stated, values are determined at 20°C (68°F) and 760 mm Hg (1 atm).

Flash Point: Not applicable (gas)
Flammable/Explosive Limits (%): No data
Autoignition Temperature: 800-1000°F
Appearance: Colorless
Physical State: Gas
Odor: Odorless in the absence of H2S or mercaptans
Vapor Pressure (mm Hg): No data
Vapor Density (air=1): <1
Boiling Point: -259°F
Freezing/Melting Point: No data
Solubility in Water: Slight
Specific Gravity: 0.30+ (Air=1)
Percent Volatile: 100 vol.%
Evaporation Rate (nBuAc=1): N/A (Gas)</pre>

### **10. STABILITY AND REACTIVITY**

Chemical Stability: Stable under normal conditions of storage and handling.
<b>Conditions To Avoid:</b> Avoid all possible sources of ignition (see Sections 5 & 7).
Incompatible Materials: Avoid contact with strong oxidizing agents.
Hazardous Decomposition Products: Combustion can yield carbon dioxide and carbon monoxide.
Issue Date: 03/18/03 Status: Final Revised

UNOCAL
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Product	Name:	Processed	Natural	Gas
Product	Code:	None		

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## Hazardous Polymerization: Will not occur.

#### 11. TOXICOLOGICAL INFORMATION

No definitive information available on carcinogenicity, mutagenicity, target organs or developmental toxicity.

#### 12. DISPOSAL CONSIDERATIONS

This material, if discarded as produced, would be a RCRA "characteristic" hazardous waste due to the characteristic(s) of ignitability (D001). If the material is spilled to soil or water, characteristic testing of the contaminated materials is recommended. Further, this material is subject to the land disposal restriction in 40 CFR 268.40 and may require treatment prior to disposal to meet specific standards. Consult state and local regulations to determine whether they are more stringent than the federal requirements.

Container contents should be completely used and containers should be emptied prior to discard. Container rinsate could be considered a RCRA hazardous waste and must be disposed of with care and in full compliance with federal, state and local regulations. Larger empty containers, such as drums, should be returned to the distributor or to a drum reconditioner. To assure proper disposal of smaller empty containers, consult with state and local regulations and disposal authorities.

### 13. TRANSPORT INFORMATION

DOT Proper Shipping Name / Technical Name: Hydrocarbon Gas, Liquified N.O.S. (Methane) Hazard Class or Division: 2.1 ID #: UN1965

#### 14. REGULATORY INFORMATION

This material contains the following chemicals subject to the reporting requirements of **SARA 313** and 40 CFR 372:

--None--Warning: This material contains the following chemicals which are known to the State of California to cause cancer, birth defects or

Issue Da	ate:	03/1	8/03		
Revised	Sect	ions:	1,	3	

Status: Final Revised

UNOCAL	CAL
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Product Name:	Processed Natural Gas	
Product Code:	None	Page 8 of 8

other reproductive harm, and are subject to the requirements of **California Proposition 65** (CA Health & Safety Code Section 25249.5):

--None Known--

This material has not been identified as a carcinogen by NTP, IARC, or OSHA.

EPA (CERCLA) Reportable Quantity: -- None--

#### 15. DOCUMENTARY INFORMATION

Issue Date: 03/18/03 Previous Issue Date: 11/29/99 Product Code: None Previous Product Code: None

## 16. DISCLAIMER OF EXPRESSED AND IMPLIED WARRANTIES

The information in this document is believed to be correct as of the date issued. HOWEVER, NO WARRANTY OF MERCHANTABILITY, FITNESS FOR ANY PARTICULAR PURPOSE, OR ANY OTHER WARRANTY IS EXPRESSED OR IS TO BE IMPLIED REGARDING THE ACCURACY OR COMPLETENESS OF THIS INFORMATION, THE RESULTS TO BE OBTAINED FROM THE USE OF THIS INFORMATION OR THE PRODUCT, THE SAFETY OF THIS PRODUCT, OR THE HAZARDS RELATED TO ITS USE. This information and product are furnished on the condition that the person receiving them shall make his own determination as to the suitability of the product for his particular purpose and on the condition that he assume the risk of his use thereof.

Issue Date: 03/18/03 Revised Sections: 1, 3

Status: Final Revised

# ATTACHMENT E

# **EMISSION CALCULATIONS**

# **Permit Determination**

Sims Run Station Camden, West Virginia

CNX Gas Company LLC 1000 Consol Energy Drive Canonsburg, PA 15317

#### Table 1. Annual Potential To Emit (PTE) Summary CNX Gas Company - Sims Run Station

#### Criteria Pollutants

Proposed Facility Wide PTE - Criteria	Pollutants		ententa	, endance				
Source	РМ	PM10	PM2.5	SO2	NOx	со	VOC	CO2e
Engines (ton/yr)	0.111	0.111	0.111	0.004	20.372	21.273	0.700	662.285
Tanks (ton/yr)	-	-	-	-	-	-	0.966	-
Truck Loading (ton/yr)	-	-	-	-	-	-	0.290	-
Compressor Blowdowns (ton/yr)	-	-	-	-	-	-	0.231	-
Fugitives (ton/yr)	-	-	-	-	-	-	1.246	28.978
Total Emissions (ton/yr)	0.111	0.111	0.111	0.004	20.372	21.273	3.434	691.263
Total Emissions (lb/hr)	0.025	0.025	0.025	0.001	4.651	4.857	0.784	157.823

#### Proposed Facility Wide PTE - HAPs

#### Hazardous Air Pollutants (HAPs)

Source	Acetaldehyde	Benzene	Toluene	Ethylbenzene	Xylene	n-Hexane	Formaldehyde	Total HAPs
Engines (ton/yr)	0.0160	0.0090	0.0032	0.0001	0.0011	-	0.378	0.446
Tanks (ton/yr)	-	-	-	-	-	-	-	-
Truck Loading (ton/yr)	-	-	-	-	-	-	-	-
Compressor Blowdowns (ton/yr)	-	-	-	-	-	-	-	-
Fugitives (ton/yr)	-	-	-	-	-	-	-	-
Total Emissions (ton/yr)	0.016	0.009	0.003	0.000	0.001	0.000	0.378	0.446
Total Emissions (lb/hr)	0.004	0.002	0.001	0.000	0.000	0.000	0.086	0.102

	Maximum Hour	ly Em	issions		Annual Emi	ssior	ns	
Pollutant	Emission Factor	<u>,</u>	PTE p Engin (Ib/h	per ne r)	Emission Factor		PTE per E (tons/y	ingine /r)
Criteria Pollutants								
PM/PM10/PM2.5**	1.94E-02 lb/MMBtu	(1)	0.025	(a)	1.94E-02 lb/MMBtu	(1)	0.111	(c)
SO <sub>2</sub>	0.25 grains S / 100 ft <sup>3</sup>	(2)	0.001	(e)	0.25 grains S / 100 ft <sup>3</sup>	(2)	0.004	(f)
NOx	1.46E+01 a/hp-hr	(3)	4.651	(b)	1.46E+01 a/hp-hr	(3)	20.372	(d)
со	3.72E+00 lb/MMBtu	(1)	4.857	(a)	3.72E+00 lb/MMBtu	(1)	21.273	(c)
VOC*	5.00E-01 g/hp-hr	(3)	0.160	(b)	5.00E-01 g/hp-hr	(3)	0.700	(d)
VOCs do not include formaldehyde								
lazardous Air Pollutants								
1,1,2,2-Tetrachloroethane	2.53E-05 lb/MMBtu	(1)	0.000	(a)	2.53E-05 lb/MMBtu	(1)	0.000	(c)
1,1,2-Trichloroethane	1.53E-05 lb/MMBtu	(1)	0.000	(a)	1.53E-05 lb/MMBtu	(1)	0.000	(c)
1,3-Butadiene	6.63E-04 lb/MMBtu	(1)	0.001	(a)	6.63E-04 lb/MMBtu	(1)	0.004	(c)
1,3-Dichloropropene	1.27E-05 lb/MMBtu	(1)	0.000	(a)	1.27E-05 lb/MMBtu	(1)	0.000	(c)
Acetaldehyde	2.79E-03 lb/MMBtu	(1)	0.004	(a)	2.79E-03 lb/MMBtu	(1)	0.016	(c)
Acrolein	2.63E-03 lb/MMBtu	(1)	0.003	(a)	2.63E-03 lb/MMBtu	(1)	0.015	(c)
Benzene	1.58E-03 lb/MMBtu	(1)	0.002	(a)	1.58E-03 lb/MMBtu	(1)	0.009	(c)
Carbon Tetrachloride	1.77E-05 lb/MMBtu	(1)	0.000	(a)	1.77E-05 lb/MMBtu	(1)	0.000	(c)
Chlorobenzene	1.29E-05 lb/MMBtu	(1)	0.000	(a)	1.29E-05 lb/MMBtu	(1)	0.000	(c)
Chloroform	1.37E-05 lb/MMBtu	(1)	0.000	(a)	1.37E-05 lb/MMBtu	(1)	0.000	(c)
Ethylona Dibramida	2.48E-05 ID/MIMBtu	(1)	0.000	(a)	2.48E-05 ID/MMBtu	(1)	0.000	(C)
Ethylene Dibromide	2.13E-05 ID/MIMBIU	(1)	0.000	(a) (b)	2.13E-05 ID/IVIVIBIU	(1)	0.000	(C) (d)
Methanol	2.70E-01 g/np-nr	(3)	0.086	(D)	2.70E-01 g/np-nr	(3)	0.378	(a)
Methylopo Chlorido	4.12E-05 lb/MMBtu	(1)	0.004	(a)	4 12E-05 lb/MMBtu	(1)	0.017	(c)
Nanhthalene	9.71E-05 lb/MMBtu	(1)	0.000	(a)	9.71E-05 lb/MMBtu	(1)	0.000	(c) (c)
PAH (POM)	1 41E-04 lb/MMBtu	(1)	0.000	(a)	1 41E-04 lb/MMBtu	(1)	0.001	(c)
Styrene	1 19E-05 lb/MMBtu	(1)	0.000	(a)	1 19E-05 lb/MMBtu	(1)	0.000	(c)
Toluene	5.58E-04 lb/MMBtu	(1)	0.001	(a)	5.58E-04 lb/MMBtu	(1)	0.003	(c)
Vinvl Chloride	7.16E-06 lb/MMBtu	(1)	0.000	(a)	7.16E-06 lb/MMBtu	(1)	0.000	(c)
Xylenes	1.95E-04 lb/MMBtu	(1)	0.000	(a)	1.95E-04 lb/MMBtu	(1)	0.001	(c)
Fotal HAP			0.102				0.446	
Greenhouse Gas Emissions								
CO <sub>2</sub>	110.00 lb/MMBtu	(1)	143.61	(a)	110.00 lb/MMBtu	(1)	629.03	(c)
CH <sub>4</sub>	2.3E-01 lb/MMBtu	(1)	0.30	(a)	2.3E-01 lb/MMBtu	(1)	1.32	(c)
N <sub>2</sub> O	2.2E-04 lb/MMBtu	(4)	0.00	(a)	2.2E-04 lb/MMBtu	(4)	0.00	(c)
			151 21				662 29	

PM emission factor includes condensables and filterables

#### Calculations:

Maximum Hourly Emissions - If emission factor note 1 or 4 is used, use calculation (a). If emission factor note 3 is used, use calculation (b).

(a) Maximum Hourly Emissions (lb/hr) = Emission factor (lb/MMBtu) \* (1MMBtu/1000000 Btu) \* Engine Power Output (hp) \* Average BSFC (Btu/hp-hr)

(b) Maximum Hourly Emissions (lb/hr) = Emission factor (g/hp-hr) \* Engine Power Output (hp) \* (1 lb/453.6 g)

Annual Emissions - If emission factor note 1 or 4 is used, use calculation (c). If emission factor note 3 is used, use calculation (d).

(c) Annual emissions (tons/yr) = Emission factor (lb/MMBtu) \* (1MMBtu/1000000Btu) \* Engine Power Output (hp) \* Average BSFC (Btu/hp-hr) \* Annual Hours of operation (hr/yr) \* (1ton/2000lbs)

(d) Annual emissions (tons/yr) = Emission factor (g/hp-hr) \* Engine Power Output (hp) \* (1 lb/453.6 g) \* Annual Hours of operation (hr/yr) \* (1 ton/2000lbs)

SO2 Emissions - If emission factor note 2 is used, use calculations (e) and (f) for hourly and annual emissions, respectively.

(e) Maximum Hourly Emissions SO2 Caclulation (lb/hr) = (0.25 grain S/100ft3) \* Fuel throughput (ft3/hr) \* (1lb/7000 grains) \* (lbmol S/32.06 lb S) \* (lbmol SO2/ lbmol S) \* (64.07 lb SO2/lbmol SO2)

(f) Annual Emissions SO2 Caclulation (ton/yr) = (0.25 grain S/100ft3) \* Fuel throughput (ft3/hr) \* (1b/7000 grains) \* (lbmol S/32.06 lb S) \* (lbmol SO2/ lbmol S) \*(64.07 lb SO2/lbmol SO2) \* Annual hours of operation (hr/yr) \* (1ton/2000lbs)

#### MAXIMUM HOURLY EMISSION INPUTS

108	Engine Power Output (kW) =
145	Engine Power Output (hp) =
1	Number of Engines =
9,004	Average BSFC (BTU/HP-hr) =
1,116.0	Heat Content Natural Gas(Btu/scf) =
1,169.9	Fuel Throughput (ft3/hr) =
8,760	PTE Hours of Operation =

 $(g) \ CO_2 \ equivalent = [(CO_2 \ emissions)^*(GWP_{CO2})] + [(CH_4 \ emissions)^*(GWP_{CH4})] + [(N_2O \ emissions)^*(GWP_{N2O})] + [($ Global Warming Potential (GWP)

CO <sub>2</sub>	1	(8)
$CH_4$	25	(8)
N <sub>2</sub> O	298	(8)

Notes:

(1) AP-42, Chapter 3.2, Table 3.2-3. Natural Gas-fired Reciprocating Engines (7/00). Uncontrolled Emission Factors for 4-Stroke Rich-Burn Engines.

(2) AP-42, Chapter 5.3, Section 5.3.1

(3) Emission Limits from manufacture specification sheet (4) Emission factors are from 40 CFR 98, Subpart C, Table C-1 and C-2,

(5) Fuel consumption from manufacturer's specification sheet.

(6) Value supplied from client based on gas composition in area field (7) Fuel throughput = BSFC (BTU/HP-hr) x Power (HP) / Heat Content (BTU/scf)

(8) Global Warming Potentials obtained from 40 CFR 98, Subpart A, Table A-1

#### Table 3. Tank Emissions CNX Gas Company - Sims Run Station

Emission Unit ID	Tank Capacity (gal)	Tank Contents	Control Devices	Tank Throughput (bbls/day)	VOC Emis Factor (lbs/	sion ′bbls)	VOC Emissions (lbs/yr) <sup>(a)</sup>	VOC Emissions (lb/hr) <sup>(b)</sup>	VOC Emissions (tons/yr) <sup>(c)</sup>
T-1	2100	Produced Liquids	None	5.00	1.36E-01	(1)	247.78	0.028	0.124
T-2	2100	Produced Liquids	None	5.00	1.36E-01	(1)	247.78	0.028	0.124
T-3	4200	Produced Liquids	None	5.00	1.57E-01	(1)	287.41	0.033	0.144
T-4	4200	Produced Liquids	None	5.00	1.57E-01	(1)	287.41	0.033	0.144
T-5	4200	Produced Liquids	None	5.00	1.57E-01	(1)	287.41	0.033	0.144
T-6	4200	Produced Liquids	None	5.00	1.57E-01	(1)	287.41	0.033	0.144
T-7	4200	Produced Liquids	None	5.00	1.57E-01	(1)	287.41	0.033	0.144
Totals							1932.59	0.22	0.97

#### Calculations:

(a) VOC Emissions (lb/yr) = Tank Throughput (bbls/day) \* VOC Emission Factor (lbs/bbls) \* (365days/yr)

(b) VOC Emissions (lb/hr) = VOC Emissions (lbs/yr) \* (yr/8760hr)

(c) VOC Emissions (ton/yr) = VOC Emissions (lbs/yr) \* (1ton/2000lbs)

#### Notes:

(1) VOC emission factor includes Flashing/Working/Breathing losses as calculated from the Promax Model Simulation report

Contents	Volume Transferred	PTE VOC Emissions (lb/hr)	PTE VOC Emissions (ton/yr) <sup>(a)</sup>
Pipeline Liquids	536,550 gal/yr	0.066	0.290
Total		0.066	0.290
(a) PTE VOC Emissions (tor	/yr) given as calculated in th	e Promax Model simu <u>Pipeline liquids</u>	lation report
(a) PTE VOC Emissions (tor	/yr) given as calculated in th Saturation factor	e Promax Model simu Pipeline liquids 0.60	Note <sup>(1)</sup>
(a) PTE VOC Emissions (tor	<b>/yr) given as calculated in th</b> Saturation factor Pvap (psia)	e Promax Model simu Pipeline liquids 0.60 6.77	Note <sup>(1)</sup> Note <sup>(2)</sup>
(a) PTE VOC Emissions (tor	/yr) given as calculated in th Saturation factor Pvap (psia) blecular Weight Vap (lb/lbmol)	e Promax Model simu <u>Pipeline liquids</u> 0.60 6.77 25.35	Note <sup>(1)</sup> Note <sup>(2)</sup> Note <sup>(2)</sup>
(a) PTE VOC Emissions (tor	<b>/yr) given as calculated in th</b> Saturation factor Pvap (psia) blecular Weight Vap (lb/lbmol) Bulk Liquid Tempurature (F)	<b>Pipeline liquids</b> 0.60 6.77 25.35 49.08	Note <sup>(1)</sup> Note <sup>(2)</sup> Note <sup>(2)</sup> Note <sup>(2)</sup>
(a) PTE VOC Emissions (tor Ma	<b>/yr) given as calculated in th</b> Saturation factor Pvap (psia) blecular Weight Vap (lb/lbmol) Bulk Liquid Tempurature (F)	e Promax Model simu <u>Pipeline liquids</u> 0.60 6.77 25.35 49.08	Note <sup>(1)</sup> Note <sup>(2)</sup> Note <sup>(2)</sup> Note <sup>(2)</sup>
(a) PTE VOC Emissions (tor Mo Notes: (1) AP-42 Section 5.2, Table Submerged loading - dedicate	Jyr) given as calculated in th Saturation factor Pvap (psia) blecular Weight Vap (lb/lbmol) Bulk Liquid Tempurature (F) 5.2-1 Saturation Factors for C- d normal service	e Promax Model simu <u>Pipeline liquids</u> 0.60 6.77 25.35 49.08 alculating Petroleum Liq	lation report Note <sup>(1)</sup> Note <sup>(2)</sup> Note <sup>(2)</sup> Note <sup>(2)</sup>

# Table 5. Fugitive Leak EmissionsCNX Gas Company - Sims Run Station

Pollutant	Emissio	n Factor	PTE <sup>(a) Gas</sup> <sub>Service</sub> (tons/yr)
Valves	9.9E-03 lb/hr/s	source (1)	4.30
Connectors	8.6E-04 lb/hr/s	source (1)	1.60
Open-Ended Lines	4.4E-03 lb/hr/s	source (1)	0.03
Pressure Relief Valves	1.9E-02 lb/hr/s	source (1)	0.00
Compressors	1.9E-02 lb/hr/s	source (1)	0.08
Total Gas Released	-	-	5.94
Total VOC Released (gas service)		(b)	1.25
Calculations:		CO2e	28.98

(a) Annual emissions (tons/yr) = [Emission Factor (lb/hr/source)] x [Number of Sources] x [Hours of Operation per Year] x [0.0005 tons/ lb]

(b) Gas sample from station's gas analysis assumed to be worst case at **21** wt % VOC from 2012 fractional gas analysis measurements

Number of Components in Gas Service

	Valves=	99	(2)
	Pressure Relief Valves=	0	(2)
	Connectors=	426	(2)
	Open-Ended Lines=	2	(2)
	Compressors=	1.000	(2)
Global Warming Potential (GWP)	Maximum Hour of Operation =	8,760	
5	CO <sub>2</sub>	1	(3)
	CH <sub>4</sub>	25	(3)
	N <sub>2</sub> O	298	(3)

(1) Emission factors from 1995 EPA Protocol for Equipment Leak Emission Estimates, Table 2-4 Oil and Gas Production

(2) Default Average Component Counts for Major Onshore Natural Gas Production Equipment from 40 CFR 98, Subpart W, Table W-1B

(3) Global Warming Potentials obtained from 40 CFR 98, Subpart A, Table A-1

#### Table 8. Reciprocating Engine / Integral Compressor Emissions (CE-1) Blowdown Venting Caterpillar 3306 NA CNX Gas Company - Sims Run Station

	Maximum Hourly Em	issions	Annual Emissions						
Pollutant	Emission Factor	PTE per Engine Event (Ib/hr)	Emission Factor	Annual PTE (tons/yr)					
Criteria Pollutants									
VOC	7.70E+00 lb/Event (1)	7.70 (a)	7.70E+00 lb/Event (1)	0.23 (a)					
(1) - 7.7 lbs VOC/ Engine blowdown event; based on 717 scf/event of 20.45 MW gas with 20.2 wt % VOC									
(a) - Worst case blowdowns per year equal normal	rate 6 times 10 = 60 Events/yr								

Date of Manufacture April 28, 2008 Driver Rated HP Number of Cylinders Displacement, in <sup>3</sup> Raw Engine Emissions Fuel Consumption 8180 LHV B Altitude 1200 ft Maximum Air Inlet Temp 90 F Nitrogen Oxides (NOx)	En <u>145</u> Ra <u>6</u> Co <u>640</u> Fur <i>TU/bhp-hr or</i>	gine Serial Number ted Speed in RPM mpression Ratio el Delivery Method 9004 HHV	G6X04525 1800 10.5:1 Carburetor	Date Modified/ Combustion Ty Combustion Se Combustion Air	Reconstructed pe tting Treatment	N// Spark Ignited 4 Strok Rich Bur Naturally Aspirated
Driver Rated HP Number of Cylinders Displacement, in <sup>3</sup> Raw Engine Emissions Fuel Consumption Altitude 1200 ft Maximum Air Inlet Temp 90 F Nitrogen Oxides (NOx)	145         Ration           6         Co           640         Function           TU/bhp-hr         or	ted Speed in RPM mpression Ratio el Delivery Method 9004 HHV	1800 10.5:1 Carburetor	Combustion Ty Combustion Se Combustion Air	pe tting <sup>.</sup> Treatment	Spark Ignited 4 Strok Rich Bur Naturally Aspirated
Number of Cylinders Displacement, in <sup>3</sup> Raw Engine Emissions Fuel Consumption 8180 LHV B Altitude 1200 ft Maximum Air Inlet Temp 90 F Nitrogen Oxides (NOx)	<u>6</u> Co <u>640</u> Fue TU/bhp-hr or	mpression Ratio el Delivery Method 9004 HHV	10.5:1 Carburetor	Combustion Se Combustion Air	tting Treatment	Rich Bur Naturally Aspirate
Displacement, in <sup>3</sup> Raw Engine Emissions Fuel Consumption 8180 LHV B Altitude 1200 ft Maximum Air Inlet Temp 90 F Nitrogen Oxides (NOx)	640 Fue	el Delivery Method 9004 HHV	Carburetor / BTU/bhp-hr	Combustion Air	Treatment	Naturally Aspirate
Raw Engine Emissions         Fuel Consumption       8180       LHV B         Altitude       1200       ft         Maximum Air Inlet Temp       90       F         Nitrogen Oxides (NOx)       States (NOx)       States (NOx)	TU/bhp-hr or	9004 HHV	/ BTU/bhp-hr			
Fuel Consumption 8180 LHV B Altitude 1200 ft Maximum Air Inlet Temp 90 F Nitrogen Oxides (NOx)	TU/bhp-hr or	9004 HHV	/ BTU/bhp-hr			
Nitrogen Oxides (NOx)						
Nitrogen Oxides (NOx)		g/bhp-hr <sup>1</sup>	lb/MMBTU <sup>2</sup>	lb/hr	ТРҮ	
introgen exides (itex)		14.55		4.651	20.372	
Carbon Monoxide (CO)		14.55		4.651	20.372	
Volatile Organic Compounds (VOC or NMNEHC)		0.5		0.160	0.700	
Formaldehyde (CH2O)		0.27		0.086	0.378	
Particulate Matter (PM)			1.94E-02	0.025	0.111	
Sulfur Dioxide (SO2)			5.88E-04	0.001	0.003	
		g/bhp-hr <sup>1</sup>	Ib/MMBTU <sup>2</sup>	lb/hr	Metric Tonne/yr	
Carbon Dioxide (CO2)		552	110.0	144	571	
Methane (CH4)		0.9	0.23	0.300	1.193	
It is recommended to add a safety margin to em <sup>2</sup> Emission Factor obtained from EPA's AP-42, Fif Gas-Fired Reciprocating Engines, Table 3.2-3).	issions to allow fo	r operational flexibility e I, Chapter 3: Stationar	r and fuel gas compositio ry Internal Combution Sc	n variability. ources (Section 3.2 1	Natural	

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	Simulation Report
Proje	ect: Sims Run Tank Run.pmx
Licensed to SLR Client Name: CNX Gas Location: Sims Run Station	International Corporation and Affiliates
ProMax Filename: N:\West Virginia\CNX ProMax Version: 4.0.16071.0 Simulation Initiated: 9/22/2017 4:14:12 PM	( Gas\Projects\2017\Engine Determinations\Sims Run\ProMax\Sims Run Tank Run.pm
Bry	an Research & Engineering, Inc. Chemical Engineering Consultants P.O. Box 4747 Bryan, Texas 77805 Office: (979) 776-5220 FAX: (979) 776-4818 <u>mailto:sales@bre.com</u> <u>http://www.bre.com/</u>

An asterisk (\*), throughout the report, denotes a user specified value. A question mark (?) after a value, throughout the report, denotes an extrapolated or approximate value.



Process Streams	Emission Point	Emission Point 2	Pipeline Liquids	Pipeline Liquids 2	Pressurized Liquid	Pressurized Liquid 2
Composition Status:	Solved	Solved	Solved	Solved	Solved	Solved
Phase:   Otal From Block: To Block:	2-50 bbl Tanks	5- 100 bbl Tanks 	2-50 bbl Tanks 	5- 100 bbl Tanks 	 2-50 bbl Tanks	 5- 100 bbl Tanks
Mole Fraction	%	%	%	%	%	%
Carbon Dioxide	0	0	0	0	0*	0*
Nitrogen	1.15424	1.21079	0.00213663	0.00239359	0.0160002*	0.0160002*
Ethane	24.6112	23.8920	0.747858	0.326135	1.03501*	1.03501*
Propane	9.51729	9.01908	1.13616	1.14839	1.23701*	1.23701*
Isobutane	1.40471	1.32220	0.469754	0.471425	0.481005*	0.481005*
n-Butane	2.34122	2.20101	1.13550	1.13804	1.15001*	1.15001*
Isopentane	0.703333	0.660219	0.992489	0.992754	0.989010*	0.989010*
Benzene	0.0100047	0.00938549	0.0768046	0.0767594	0.0760008*	0.0760008*
Toluene	0.0163253	0.0153197	0.489701	0.489342	0.484005*	0.484005*
Ethylbenzene	0.00415519	0.00390107	0.426081	0.425754	0.421004*	0.421004*
p-Xylene	0.0124147	0.0116558	1.36529	1.36424	1.34901*	1.34901*
n-Hexane 2.2.4-Trimethylpentane	0.203179	0.190654	1.49860	1.49773	1.48301*	1.48301- 0*
Other C6's	0.311067	0.291886	1.73313	1.73224	1.71602*	1.71602*
Heptanes	0.261420	0.245361	5.60030	5.59631	5.53606*	5.53606*
Octanes	0.119034	0.111762	8.14263	8.13644	8.04608*	8.04608*
Nonanes	0.0223659	0.0210084	5.07384	5.06990	5.01305*	5.01305*
Molar Flow	3.96089E-07	3.74018E-07	69.7247	lbmol/h	lbmol/h	lbmol/h
Carbon Dioxide	0	0	0	0	0*	0*
Nitrogen	7.42091E-05	0.000182077	1.12785E-05	3.16067E-05	8.54876E-05*	0.000213684*
Methane	0.00377648	0.00906179	0.00157183	0.00430678	0.00534832*	0.0133686*
Etnane Propane	0.00158232	0.00359284	0.00394766	0.0102298	0.00552998*	0.0138227*
Isobutane	9.03122E-05	0.00135628	0.00599737	0.0151641	0.00000920	0.0165204
n-Butane	0.000150523	0.000330985	0.00599390	0.0150275	0.00614442*	0.0153585*
Isopentane	4.52191E-05	9.92828E-05	0.00523898	0.0131090	0.00528420*	0.0132083*
n-Pentane	3.65817E-05	8.02998E-05	0.00573917	0.0143567	0.00577575*	0.0144370*
Benzene	6.43227E-07	1.41138E-06	0.000405423	0.00101359	0.000406066*	0.00101500*
Ethylbenzene	2.67148E-07	5.86637E-07	0.00224912	0.00562196	0.00238000	0.00562255*
p-Xylene	7.98172E-07	1.75278E-06	0.00720687	0.0180144	0.00720767*	0.0180162*
n-Hexane	1.30629E-05	2.86703E-05	0.00791057	0.0197771	0.00792363*	0.0198058*
2,2,4-Trimethylpentane	0	0	0	0	0*	°0 • • • • • • • • • • • • • • • • • • •
Uther Co's Hentanes	1.99993E-05 1.68073E-05	4.38934E-05 3.68970E-05	0.00914854	0.0228737	0.00916854*	0.0229176
Octanes	7.65299E-06	1.68067E-05	0.0429819	0.107439	0.0429896*	0.107456*
Nonanes	1.43796E-06	3.15922E-06	0.0267829	0.0669466	0.0267843*	0.0669497*
Decanes +	2.54656E-11	5.62444E-11	0.368051	0.919974	0.368051*	0.919974*
Mass Fraction	%	%	%	<u>%</u>	<u>%</u>	<u>%</u>
Nitrogen	1 27576	1 36069	0 000262596	0 000294376	0 00198772*	0 00198772*
Methane	37.1797	38.7813	0.0209580	0.0229711	0.0712154*	0.0712154*
Ethane	29.1984	28.8201	0.0986582	0.102269	0.138016*	0.138016*
Propane	16.5583	15.9544	0.219801	0.222316	0.241899*	0.241899*
Isobutane	3.22133	3.08293	0.119786	0.120293	0.123981*	0.123981*
Isopentane	2.00215	1.91091	0.314159	0.314455	0.316442*	0.316442*
n-Pentane	1.61972	1.54554	0.344153	0.344383	0.345878*	0.345878*
Benzene	0.0308338	0.0294102	0.0263208	0.0263230	0.0263269*	0.0263269*
Toluene	0.0593483	0.0566260	0.197955	0.197943	0.197767*	0.197767*
n-Xvlene	0.0174052	0.0496417	0.196456	0.196439	0.196213	0.196213
n-Hexane	0.690828	0.659104	0.566584	0.566637	0.566752*	0.566752*
2,2,4-Trimethylpentane	0	0	0	0	0*	0*
Other C6's	1.04323	0.995304	0.646315	0.646418	0.646852*	0.646852*
neptaries Octanes	1.03361	0.9863/1 0.511122	2.46216	2.46207 4 07219	2.46023* 4.06774*	2.46023* 4.06774*
Nonanes	0.112955	0.107877	2.84932	2.84903	2.84562*	2.84562*
Decanes +	4.44145E-06	4.26423E-06	86.9371	86.9277	86.8195*	86.8195*
Mass Flow	lb/h	lb/h	lb/h	lb/h	lb/h	lb/h
Carbon Dioxide	0 00207895	0	0 000315048	0 000885410	0*	0*
Methane	0.0605841	0 145373	0.000313948	0.000803410	0.00239400	0.00398000
Ethane	0.0475787	0.108033	0.118702	0.307601	0.166281*	0.415634*
Propane	0.0269817	0.0598059	0.264458	0.668672	0.291439*	0.728478*
Isobutane	0.00524914	0.0115565	0.144123	0.361812	0.149372*	0.373369*
n-outarie Isonentane	0.00874874	0.0192376	U.3483/8 0 377986	U.8/3432 0 945801	0.35/127* 0.3812/0*	0.892670*
n-Pentane	0.00263933	0.00579353	0.414074	1.03582	0.416714*	1.04161*
Benzene	5.02436E-05	0.000110245	0.0316683	0.0791730	0.0317186*	0.0792833*
Toluene	9.67077E-05	0.000212265	0.238173	0.595364	0.238270*	0.595576*
Ethylbenzene	2.83618E-05	6.22803E-05	0.238778	0.596855	0.238807*	0.596918*
p-Aylene n-Hexane	8.4/3/9E-05 0.00112570	0.000186084	0.765118	1.91250	0.765202*	1.91269*
2,2,4-Trimethylpentane	0.00112070	0.00247008	0.001090	0	0*	0*
Other C6's	0.00169994	0.00373094	0.777626	1.94426	0.779326*	1.94799*
Heptanes	0.00168426	0.00369745	2.96240	7.40528	2.96408*	7.40898*
Uctanes Nonanes	0.000872441	0.00191596	4.89994	12.2481	4.90081*	12.2500*
110110100	0.000104039	0.000404360	5.42021	0.00910	5.42039	0.00900
Decanes +	7.23732E-09	1.59846E-08	104.600	261.457	104.600*	261.457*

Process Streams		<b>Emission Point</b>	Emission Point 2	<b>Pipeline Liquids</b>	<b>Pipeline Liquids 2</b>	Pressurized Liquid	Pressurized Liquid 2
Properties	Status:	Solved	Solved	Solved	Solved	Solved	Solved
Phase: Total	From Block:	2-50 bbl Tanks	5- 100 bbl Tanks	2-50 bbl Tanks	5- 100 bbl Tanks	-	/
	To Block:	-	-	-	-	2-50 bbl Tanks	5- 100 bbl Tanks
Property	Units						
Temperature	°F	57.7653	57.7930	57.7653	57.7930	58*	58*
Pressure	psig	0	1	0	1	. 21*	21*
Molecular Weight	lb/lbmol	25.3450	24.9274	227.932	. 227.778	225.494	. 225.494
Mass Density	lb/ft^3	0.0674859	0.0709004	51.4304	51.4275	, 49.7590	49.7590
Molar Flow	lbmol/h	0.00642925	0.0150379	0.527863	, 1.32047	0.534292	1.33551
Mass Flow	lb/h	0.162950	0.374854	120.317	300.775	, 120.480	301.150
Vapor Volumetric Flow	ft^3/h	2.41457	5.28705	2.33941	5.84852	2.42127	6.05217
Liquid Volumetric Flow	gpm	0.301037	0.659165	0.291667	0.729167	0.301872	0.754556
API Gravity	0.			40.2833	40.2909	j	
Net Ideal Gas Heating Value	Btu/ft^3	1358.11	1336.39	11167.2	. 11159.7	11049.1	11049.1
Net Liquid Heating Value	Btu/lb	20239.2	20251.8	18439.8	, 18439.9	18442.2	18442.2

			Envi	ronments Repo	rt				
Client Name:	Tank Emission Estimat	e		Job:	N:\West Virginia\CNX G	as\Projects\2017\Engine Determinations\Sims Run\ProMax\Sims Run Ta	ank Run.pmx		
Location:	0								
Flowsheet:	tanks								
Project-Wide Constants									
Atmospheric Pressure	14.6959	) psia	Ideal Gas Reference Volum	e 379.	484 ft^3/lbmol				
Ideal Gas Reference Pressure	14.6959	) psia	Liquid Reference Temperate	ure	60 °F				
Ideal Gas Reference Temperature	60	)°F							
	Environment1								
			Env	vironment Settings					
Number of Poynting Intervals	(	)	Phase Tolerance		1 %				
Gibbs Excess Model Evaluation Temperature	77	°F	Emulsion Enabled	FAI	SE				
Freeze Out Temperature Threshold Difference	1(	) °F							
				Components					
Component	Henry's Law Comp	Phase Initiator	Component	Henry's Law Con	n	Phase Initiator			
Carbon Dioxide	FALSE	FALSE	Nitrogen	FALSE	s.	FALSE			
Methane	FALSE	FALSE	Ethane	FALSE		FALSE			
Propane	FALSE	FALSE	Isobutane	FALSE		FALSE			
n-Butane	FALSE	FALSE	Isopentane	FALSE		FALSE			
n-Pentane	FALSE	FALSE	Benzene	FALSE		FALSE			
Toluene	FALSE	FALSE	Ethylbenzene	FALSE		FALSE			
p-Xvlene	FALSE	FALSE	n-Hexane	FALSE		FALSE			
2.2.4-Trimethylpentane	FALSE	FALSE	Other C6's	FALSE		FALSE			
Heptanes	FALSE	FALSE	Octanes	FALSE		FALSE			
Nonanes	FALSE	FALSE	Decanes +	FALSE		FALSE			
			Physica	I Property Method	Sets				
Liquid Molar Volume	COSTALD		Vapor Package	Peng-Robinson					
Overall Package	Peng-Robinson		Light Liquid Package	Peng-Robinson					
Stability Calculation	Peng-Robinson		Heavy Liquid Package	Peng-Robinson					
Notes:									

Single Oil Report Decanes +							
Client Name:	Tank Emission Estim	ate	Job: 1	N:\West Virginia\CNX Gas\Projects\2017\Engine Determinations\Sims Run\ProMax\Sims Run Tank Run.pmx			
Location:	0		• • •				
Flowsheet:	tanks						
			Pro	operties			
Volume Average Boiling Point	661.659 °F	Low Temperature Viscosity	6.79714	P			
Molecular Weight	284.2* lb/lbmol	Temperature of High T Viscosity	210 °	F			
Specific Gravity	0.8465*	High Temperature Viscosity	1.82072	2P			
API Gravity	35.6589	Watson K	12.2730				
Critical Temperature	951.235 °F	ASTM D86 10-90% Slope	0 °	F/%			
Critical Pressure	170.611 psig	ASTM D93 Flash Point	338.345	F			
Critical Volume	17.6652 ft^3/lbmol	Pour Point	61.4934 °	F			
Acentric Factor	0.880769	Paraffinic Fraction	71.7542	<i>K</i> 6			
Carbon to Hydrogen Ratio	6.33114?	Naphthenic Fraction	22.5066	<i>V</i> o			
Refractive Index	1.46817	Aromatic Fraction	5.73929	<i>V</i> o			
Temperature of Low T Viscosity	100 °F	Ideal Gas Heat Capacity	103.423 E	Btu/(lbmol*°F)			
Notes:							

Single Oil Report Heptanes							
Client Name:	Tank Emission Estim	ate	Job:	N:\West Virginia\CNX Gas\Projects\2017\Engine Determinations\Sims Run\ProMax\Sims Run Tank Run.pmx			
Location:	0						
Flowsheet:	tanks						
			Pro	operties			
Volume Average Boiling Point	204.170 °F	Low Temperature Viscosity	0.347616	2P			
Molecular Weight	100.21* lb/lbmol	Temperature of High T Viscosity	210 °	'F			
Specific Gravity	0.7016*	High Temperature Viscosity	0.211224	SP			
API Gravity	70.1819	Watson K	12.4336				
Critical Temperature	512.987 °F	ASTM D86 10-90% Slope	0 '	P/%			
Critical Pressure	396.167 psig	ASTM D93 Flash Point	22.6774	F			
Critical Volume	6.61841 ft^3/lbmol	Pour Point	-5.66945?	F			
Acentric Factor	0.328178	Paraffinic Fraction	72.8431	Ж			
Carbon to Hydrogen Ratio	5.34609	Naphthenic Fraction	21.4149	<i>К</i> о			
Refractive Index	1.39189	Aromatic Fraction	5.74200	<i>К</i> о			
Temperature of Low T Viscosity	100 °F	Ideal Gas Heat Capacity	37.1664 l	Btu/(lbmol*°F)			

Notes:

Single Oil Report Nonanes								
Client Name:	Tank Emission Estim	ate	Job:	N:\West Virginia\CNX Gas\Projects\2017\Engine Determinations\Sims Run\ProMax\Sims Run Tank Run.pmx				
Location:	0							
Flowsheet:	tanks							
	Properties							
Volume Average Boiling Point	296.600 °F	Low Temperature Viscosity	0.569789	cP				
Molecular Weight	128* lb/lbmol	Temperature of High T Viscosity	210	°F				
Specific Gravity	0.7424*	High Temperature Viscosity	0.313911	cP				
API Gravity	59.0981	Watson K	12.2722					
Critical Temperature	612.483 °F	ASTM D86 10-90% Slope	0	°F/%				
Critical Pressure	339.966 psig	ASTM D93 Flash Point	86.4541	°F				
Critical Volume	8.28440 ft^3/lbmol	Pour Point	-11.0241?	°F				
Acentric Factor	0.420394	Paraffinic Fraction	62.4060	%				
Carbon to Hydrogen Ratio	5.62062	Naphthenic Fraction	24.7656	%				
Refractive Index	1.41424	Aromatic Fraction	12.8284	%				
Temperature of Low T Viscosity	100 °F	Ideal Gas Heat Capacity	46.6471	Btu/(Ibmol*°F)				
Notes:								

 

 Single Oil Report Octanes

 Client Name:
 Tank Emission Estimate
 Job:
 N:\West Virginia\CNX Gas\Projects\2017\Engine Determinations\Sims Run\ProMax\Sims Run Tank Run.pmx

 Location:
 0
 Image: Comparison Comp

	Properties							
Volume Average Boiling Point	251.542 °F	Low Temperature Viscosity	0.446533 cP					
Molecular Weight	114* lb/lbmol	Temperature of High T Viscosity	210 °F					
Specific Gravity	0.724*	High Temperature Viscosity	0.258447 cP					
API Gravity	63.9420	Watson K	12.3290					
Critical Temperature	565.037 °F	ASTM D86 10-90% Slope	0 °F/%					
Critical Pressure	367.393 psig	ASTM D93 Flash Point	55.3642 °F					
Critical Volume	7.43719 ft^3/lbmol	Pour Point	-9.58266? °F					
Acentric Factor	0.374061	Paraffinic Fraction	66.6140 %					
Carbon to Hydrogen Ratio	5.49569	Naphthenic Fraction	23.6971 %					
Refractive Index	1.40406	Aromatic Fraction	9.68898 %					
Temperature of Low T Viscosity	100 °F	Ideal Gas Heat Capacity	41.8093 Btu/(lbmol*°F)					

Notes:

Single Oil Report Other C6's					
Client Name:	Tank Emission Estim	ate	Job:	N:\West Virginia\CNX Gas\Projects\2017\Engine Determinations\Sims Run\ProMax\Sims Run Tank Run.pmx	
Location:	0				
Flowsheet:	tanks				
			Pr	operties	
Volume Average Boiling Point	147.291 °F	Low Temperature Viscosity	0.256680	cP	
Molecular Weight	85* lb/lbmol	Temperature of High T Viscosity	210	°F	
Specific Gravity	0.664*	High Temperature Viscosity	0.164743	cP	
API Gravity	81.6024	Watson K	12.7512		
Critical Temperature	445.480 °F	ASTM D86 10-90% Slope	0	°F/%	
Critical Pressure	420.214 psig	ASTM D93 Flash Point	-16.5692?	°F	
Critical Volume	5.75172 ft^3/lbmol	Pour Point	5.82321?	°F	
Acentric Factor	0.277116	Paraffinic Fraction	86.4939?	%	
Carbon to Hydrogen Ratio	5.07336	Naphthenic Fraction	13.5061?	%	
Refractive Index	1.37271	Aromatic Fraction	0?	%	
Temperature of Low T Viscosity	100 °F	Ideal Gas Heat Capacity	32.5709	Btu/(Ibmol*°F)	
Notes:					

Calculators Report				
Client Name:	Tank Emission Estimate		Job: N:\V	
Location:	0			
Flowsheet:	tanks			
		Simple Solver 1		
		Source Code		
Residual Error (fo	r CV1) = PipelineLiquids-10			
	Calc	ulated Variable [CV1]		
SourceMoniker	ProMax:ProMax!Project!Flowsheets!tanks!F	PStreams!Pressurized Liquid!Phases!Total!Propertie	es!Std Liquid Volumetric Flow	
Value	0.292507			
Units	sgpm			
0 M "	Measure	ed Variable [PipelineLiquids]		
SourceMoniker	ProMax:ProMax!Project!Flowsheets!tanks!F	Streams!Pipeline Liquids!Phases!Total!Properties!	Liquid Volumetric Flow	
Value	10.0000			
Units	bbl/d			
		Solver Properties		
Status: Solved		Solver Properties		
Error	1.49925E-12	Iterations	2	
Calculated Value	0.292507 sapm	Max Iterations	20	
Lower Bound	sapm	Weighting	1	
Upper Bound	sapm	Priority	0	
Step Size	sapm	Solver Active	Active	
Is Minimizer	FALSE	Group		
Algorithm	Default	Skip Dependency Check	FALSE	
<b>J</b>				
Notes:				
		0		
		Simple Solver 2		
		Source Code		
Residual Error (fo	r CV1) = Pipeline_Liquids_2-25			
	Cala	ulated Veriable (C)/41		
	Caic			
SourceMoniker	ProMax:ProMax!Project!Flowsheets!tanks!F	PStreams!Pressurized Liquid 2!Phases!Total!Proper	ties!Std Liquid Volumetric Flow	
Value	25.0679			
Units	bbl/d			
	Measured	Variable [Pipeline Liquids 2]		
SourcoMonikor	ProMax: ProMax   Project  Elowshoots  tanks	Stroams Dipoling Liquids 2 Dhasos Total Droportion	all iquid Volumotric Flow	
	25 0000		sieliquid volumetric rilow	
Value	23.0000 hbl/d			
Onits	bbi/d			
		Solver Properties		
Status: Solved		Solver Fropenies		
Error	-7 59925E-12	Iterations	2	
Calculated Value	0.731147 sanm	Max Iterations	20	
Lower Bound	sanm	Weighting	1	
Upper Bound	sapm	Priority	0	
Step Size	sanm	Solver Active	Active	
ls Minimizer	FALSE	Group	, 101110	
Algorithm	Default	Skip Dependency Check	FALSE	
Notes:				

User Value Sets Report				
Client Name:	Tank Emission Estimate	Job:	N:\West Virginia	
Location:	0			
Flowsheet:	tanks			
	Ta	nk-1		
	User Value	[BlockReady]		
Parameter	1*	Upper Boun		
Lower Bound		Enforce Bou	FALSE	
	User Value	ShellLength		
Parameter	5* ft	Upper Boun	ft	
Lower Bound	0* ft	Enforce Bou	FALSE	
	Liser Value	[ShollDiam]		
Daramator	0 15€1 ¥ aius		4	
Parameter	0.40 II 0* ft	Enforce Bol		
			FALSE	
	User Value	[BreatherVP]		
Darameter	0.030000* psig		nsia	
l ower Bound	psig	Enforce Bou	FAI SE	
Lonor Boand				
	User Value [/	BreatherVacP]		
Parameter	-0.030000* psig	Upper Boun	psig	
Lower Bound	psig	Enforce Bou	FALSE	
	User Value	DomeRadius]		
Parameter	4.23* ft	Upper Boun	ft	
Lower Bound	ft	Enforce Bou	FALSE	
	User Value	e [OpPress]		
Parameter	0* psig	Upper Boun	psig	
Lower Bound	psig	Enforce Bou	FALSE	
	User Value [#	vgPercentLiq		
Parameter	50* %	Upper Boun	%	
Lower Bound	%	Enforce Bou	FALSE	
		levDereentlin1		
			<b>N</b> /	
Parameter	90" % %	Upper Boun	% ENLCE	
	70		FALSE	
	User Value	[AnnNetTP]		
Parameter	0.96470* bbl/day		bbl/day	
Parameter	9.90470 DDiruay 0* hbl/day	Enforce Bol	DDI/Udy	
	User Val	ue [OREff]		
Parameter	0* %	Upper Boun	%	
Lower Bound	%	Enforce Bou	FALSE	
	User Value	e [MaxAvgT]		
Parameter	61.15* °F	Upper Boun	°F	
Lower Bound	°F	Enforce Bou	FALSE	
	User Value	e [MinAvgT]		
Parameter	36.9667* °F	Upper Boun	°F	
Lower Bound	°F	Enforce Bou	FALSE	

	User Value	[BulkLiqT]	
Parameter	49.0783* °F	Upper Boun	°F
Lower Bound	°F	Enforce Bou	FALSE
	User valu		
Parameter	13.7315° psia	Upper Boun	psia
Lower Bound	psia	Enloice Bot	FALSE
	User Value	e [Therml]	
Parameter	1193.89* Btu/ft^2/day	Upper Boun	Btu/ft^2/dav
Lower Bound	Btu/ft^2/day	Enforce Bou	FALSE
	User Value [Av	gWindSpeed]	
Parameter	6.16667* mi/h	Upper Boun	mi/h
Lower Bound	mi/h	Enforce Bou	FALSE
	User Value (MaxHe	urlyl opding Patol	
Paramotor			bbl/br
l ower Bound	0* bbl/hr	Enforce Bou	FALSE
	0 0000		
	User Value [Ent	rainedOilFrac]	
Parameter	1* %	Upper Boun	%
Lower Bound	%	Enforce Bou	FALSE
		<b>.</b>	
	User Value [T	urnoverRate	
Parameter	40.4561*	Upper Boun	
Lower Bound		Enforce Bol	FALSE
	User Value []	ossSatEactor	
Parameter	0.5*	Upper Boun	
Lower Bound	0.0	Enforce Bou	FALSE
	User Value [A	tmPressure]	
Parameter	13.7315* psia	Upper Boun	psia
Lower Bound	psia	Enforce Bou	FALSE
Deveryeter	User val		i -
Parameter	6.77054° psia	Enforce Bou	psia EALSE
	μοια	Enlorce Bot	TALGE
	User Value	e [MaxVP]	
Parameter	7.19440* psia	Upper Boun	psia
Lower Bound	psia	Enforce Bou	FALSE
	User Value	e [MinVP]	
Parameter	6.37364* psia	Upper Boun	psia
Lower Bound	psia	Enforce Bou	FALSE
	Liser Value [Av		
Parameter	50.6729* °F		°۲
Lower Bound	°F	Enforce Bou	FALSE
	·		
	User Value [Ma	xLiqSurfaceT]	
Parameter	56.4466* °F	Upper Boun	°F
Lower Bound	°F	Enforce Bou	FALSE
	User Value [1	otalLosses]	
Parameter	0.238990* ton/yr	Upper Boun	ton/yr
Lower Bound	ton/yr	Entorce Bol	FALSE

User Value [WorkingLosses]				
Parameter	0.0732604* ton/yr	Upper Boun	ton/yr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
	User Value [St	andingLosses]		
Parameter	0.0462348* ton/yr	Upper Boun	ton/yr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
		imSeell eccess		
Paramotor			top/ur	
Lower Bound	ton/vr	Enforce Bou	FALSE	
	User Value [W	ithdrawalLoss]		
Parameter	0* ton/yr	Upper Boun	ton/yr	
Lower Bound	ton/yr	Enforce Bol	FALSE	
	User Value [L	oadingLosses]		
Parameter	0.0827156* ton/yr	Upper Boun	ton/yr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
		ourly loading local		
Parameter			lb/br	
Lower Bound	lb/hr	Enforce Bou	FALSE	
	User Val	ue [PStar]		
Parameter		Upper Boun		
		Enlorce Bol	FALSE	
	User Value [Al	ICTotalLosses]		
Parameter	0.578286* ton/yr	Upper Boun	ton/yr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
		l opdingl oppopl		
Parameter	0 200147* top/yr		ton/yr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
	User Value [AllCN	[axHLoadingLoss]		
Parameter	0.0456957* lb/hr	Upper Boun	Ib/hr	
	ЮЛІ	Eniorce Bot	TALOL	
	User Value [AllC	FlashingLosses]		
Parameter	0.0263771* ton/yr	Upper Boun	ton/yr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
	User Value [De	ckFittingl osses]		
Parameter		Upper Boun	ton/vr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
	User Value [De	ckSeamLosses]		
Parameter	0* ton/yr	Upper Boun	ton/yr FALSE	
	tori/ yr			
	User Value [F	ashingLosses]		
Parameter	0.00877691* ton/yr	Upper Boun	ton/yr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
	User Value []	[otalResidual]		
Parameter	526.383* ton/vr	Upper Boun	ton/vr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
	User Value [G	asMoleWeight]		

Parameter	0.0318968* kg/mol	Upper Boun	kg/mol
Lower Bound	кд/тоі	EUIOICE BOI	FALSE
	User Value [Var	ReportableFrac]	
Parameter	41.3274* %	Upper Boun	%
Lower Bound	%	Enforce Bou	FALSE
		PoportableEracl	
Parameter	99 8835* %		%
Lower Bound	%	Enforce Bou	FALSE
	User Value [Flas	hReportableFrac]	~
Parameter	33.2747* %	Upper Boun	% FALSE
Lower Dound	70	Enlorce Bot	TALGE
<b>Notes:</b> This User Value Set v	was programmatically generated. GL	IID={0658807B-16DE-46C9-	972E-43AD43311EF6}
	Ta	nk-2	
	User Value	BlockReady]	
Parameter	1*	Upper Boun	
			FALOE
	User Value	ShellLength]	
Parameter	10* ft	Upper Boun	ft
Lower Bound	0* ft	Enforce Bou	FALSE
	Liser Value	[ShellDiam]	
Parameter	8.45* ft	Upper Boun	ft
Lower Bound	0* ft	Enforce Bou	FALSE
Deverenter	User Value	[BreatherVP]	nein
l ower Bound	0.0300000 psig	Enforce Bou	PSIg FALSE
	porg		
	User Value [B	BreatherVacP]	
Parameter	-0.0300000* psig	Upper Boun	psig
Lower Bound	psig	Enforce Bol	FALSE
	User Value [	DomeRadius]	
Parameter	4.23* ft	Upper Boun	ft
Lower Bound	ft	Enforce Bou	FALSE
		[OnPress]	
Parameter		Upper Boun	psig
Lower Bound	psig	Enforce Bou	FALSE
Deremeter			0/
Parameter	5U <sup>™</sup> % %	Enforce Bou	% FALSE
	User Value [N	laxPercentLiq]	
Parameter	90* %	Upper Boun	%
Lower Bound	%	Enforce Bou	FALSE
	User Value	[AnnNetTP]	
Parameter	24.9092* bbl/day	Upper Boun	bbl/day
Lower Bound	0* bbl/day	Enforce Bou	FALSE
Doromotor			0/
Parameter	U" %	Opper Boun	%

Lower Bound	%	Enforce Bou	FALSE
-	User Valu		
Parameter	61.15* °F	Upper Boun	°F
Lower Bound	۴	Enforce Bou	FALSE
Demonster			
Parameter	36.9667°°F °E	Upper Boun	
	ľ	Enlorce Bot	TAESE
	User Valu	e (BulkLigT)	
Parameter	49.0783* °F	Lipper Boun	۰F
Lower Bound	°F	Enforce Bou	FALSE
	User Va	lue [AvgP]	
Parameter	13.7315* psia	Upper Boun	psia
Lower Bound	psia	Enforce Bou	FALSE
	User Val	ue [Therml]	
Parameter	1193.89* Btu/ft^2/day	Upper Boun	Btu/ft^2/day
Lower Bound	Btu/ft^2/day	Enforce Bou	FALSE
	User Value [/	AvgWindSpeed]	
Parameter	6.16667* mi/h	Upper Boun	mi/h
Lower Bound	mi/h	Enforce Bou	FALSE
		Levelul a a dia a Data l	
		HouriyLoadingRate	
Parameter	1.03788* bbl/hr	Upper Boun	bbl/hr
Lower Bound	U <sup>*</sup> DDI/nr	Enforce Bot	FALSE
	Lisor Value [E	ntrainedOilEracl	
Doromotor			0/
Farameter	1 70	Enforce Bou	FALSE
Lonor Dound	/0		111202
	User Value I	TurnoverRate1	
Parameter	20.2260*	Upper Boun	
Lower Bound		Enforce Bou	FALSE
	User Value [L	LossSatFactor]	
Parameter	0.5*	Upper Boun	
Lower Bound		Enforce Bou	FALSE
	User Value	[AtmPressure]	
Parameter	13.7315* psia	Upper Boun	psia
Lower Bound	psia	Enforce Bou	FALSE
-	User va		
Parameter	6.82125* psia	Upper Boun	psia
Lower Bound	psia	Enforce Bot	FALSE
	Liser Val		
Doromotor			ncio
Farameter Lower Bound	nsia	Enforce Bou	FALSE
	poid		
	User Val	ue [MinVP]	
Parameter	6.41960* psia	Upper Boun	nsia
Lower Bound	psia	Enforce Bou	FALSE
	User Value [A	vgLiqSurfaceT]	
Parameter	50.6729* °F	Upper Boun	°F
Lower Bound	°F	Enforce Bou	FALSE

User Value [MaxLiqSurfaceT]				
Parameter	56.4466* °F	Upper Boun	°F	
Lower Bound	۴	Enforce Bou	FALSE	
	User Value [	TotalLosses]		
Parameter	0.669613* ton/yr	Upper Boun	ton/yr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
		lerkingl eccel		
Parameter			ton/vr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
	User Value [St	andingLosses]		
Parameter	0.0529473* ton/yr	Upper Boun	ton/yr	
	tonyy		TALGE	
	User Value [R	imSealLosses]		
Parameter	0* ton/yr	Upper Boun	ton/yr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
	User Value (W	ithdrawall.oss1		
Parameter	0* ton/vr	Upper Boun	ton/vr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
	User Value [Lo	oadingLosses]		
Parameter	0.207586* ton/yr ton/yr	Upper Boun Enforce Bou	ton/yr FALSE	
	tonyy	Enloree Bot	TALOL	
	User Value [MaxH	ourlyLoadingLoss]		
Parameter	0.0473940* lb/hr	Upper Boun	lb/hr	
Lower Bound	lb/hr	Enforce Bou	FALSE	
	User Val	ue [PStar]		
Parameter		Upper Boun		
Lower Bound		Enforce Bou	FALSE	
Parameter			ton/vr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
_	User Value [AllC	LoadingLosses]		
Parameter	0.499490* ton/yr	Upper Boun	ton/yr	
	l01//yi			
	User Value [AllCN	[axHLoadingLoss]		
Parameter	0.114039* lb/hr	Upper Boun	lb/hr	
Lower Bound	lb/hr	Enforce Bou	FALSE	
	Liser Value [AllC	Flashing osses		
Parameter	0.146857* ton/vr	Upper Boun	ton/vr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
	User Value [Dec	CKFittingLosses]		
Parameter	0* ton/yr	Upper Boun	ton/yr	
	l01//yi			
	User Value [De	ckSeamLosses]		
Parameter	0* ton/yr	Upper Boun	ton/yr	
Lower Bound	ton/yr	Enforce Bou	FALSE	
	liser Value [Fi	ashingl osses]		
		aoning_cooocoj		

Parameter	0.0489183* ton/yr	Upper Boun	ton/yr
Lower Bound	ton/yr	Enforce Bou	FALSE
	User Value [	FotalResidual]	
Parameter	1315.64* ton/yr	Upper Boun	ton/yr
Lower Bound	ton/yr	Enforce Bou	FALSE
		acMoloWoight]	
	User value [G	asmoleweightj	
Parameter	0.0319284* kg/mol	Upper Boun	kg/mol
Lower Bound	kg/mol	Enforce Bou	FALSE
	User Value [Vap	ReportableFrac]	
Parameter	41.5595* %	Upper Boun	%
Lower Bound	%	Enforce Bou	FALSE
		PapartableEreel	
-		ReportableFlac	
Parameter	99.8819* %	Upper Boun	%
Lower Bound	%	Enforce Bou	FALSE
	User value [Flas	nReportableFrac	
Parameter	33.3102* %	Upper Boun	%
Lower Bound	%	Enforce Bou	FALSE
Notes:			
This User Value Set v	was programmatically generated. GL	JID={F5CF85E9-4310-4AEB-	-9008-EEC20CB8B39F}