

Pleasants Energy LLC 10319 South Pleasants Highway St. Marys, WV 26170 Phone: 304-665-4200

October 13, 2017

Beverly McKeone West Virginia Department of Environmental Protection Division of Air Quality 601 57th Street, SE Charleston, WV 25304

Re: Prevention of Significant Deterioration Air Permit Application for the Turbine Uprate Project at Pleasants Energy, LLC

Dear Ms McKeone:

Pleasants Energy, LLC (Pleasants Energy) is submitting this Prevention of Significant Deterioration (PSD) air permit application for an uprate of the two simple-cycle combustion turbines at the Pleasants Energy facility, located near Waverly, West Virginia. The Pleasants Energy facility is a 300-megawatt simple-cycle electric generating station that currently operates under Title V permit number R30-07300022-2014. This project will increase the maximum output of the combustion turbines at mid to high ambient temperatures. This application does not propose to increase the fuel limit or annual emissions above the limits in PSD Permit issued in January 2017 which increased their annual operations at the facility.

The PSD permit application submitted today includes the following:

- Executive Summary
- Introduction
- Project Description
- Emissions Estimates
- Regulatory Review
- Best Available Control Technology (BACT) Analysis
- Air Dispersion Modeling
- Additional Impact Analysis
- Appendices (including the required West Virginia Department of Environmental Protection (WV DEP) application forms and other necessary information and calculations)

An application fee of \$7,000 (modification to an existing major source) will be paid upon notification that you have received our application. Attached to this letter, is a signed original hard copy of the air permit application. As requested, 3 electronic copies of the application is also being submitted on CD with the hard copy of the application.

As WV DEP proceeds with the evaluation process, please contact the following persons with questions or for additional information:

Gerald Gatti Pleasants Energy, LLC 10319 South Pleasants Highway St. Mary's, WV 26170 Phone: 304-665-4201

Phone: 304-665-4201 Gerald.Gatti@dynegy.com Mary Hauner-Davis Burns & McDonnell 9400 Ward Parkway Kansas City, MO 64114 Phone: 816-822-4252 mhauner@burnsmcd.com

If we can be of any assistance to facilitate your staff's efforts, please do not hesitate to contact me or Mary Hauner-Davis listed above. Thank you for your time and efforts on our Project.

Sincerely,

Gerald Gatti Plant Manager

To M MU.

Attachments

cc: Mary Hauner-Davis, Burns & McDonnell



Prevention of Significant Deterioration Air Construction Permit Application

Pleasants Energy, LLC

Pleasants Energy Uprate Project Project No. 100558

> Revision 0 October 2017

Prevention of Significant Deterioration Air Construction Permit Application

prepared for

Pleasants Energy, LLC
Pleasants Energy Uprate Project
Waverly, West Virginia

Project No. 100558

Revision 0 October 2017

prepared by

Burns & McDonnell Engineering Company, Inc. Kansas City, Missouri

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LIST OF ABBREVIATIONS

<u>Abbreviation</u> <u>Term/Phrase/Name</u>

°F degrees Fahrenheit

μg microgram

μg/m³ microgram per cubic meter

AERMAP AMS/EPA Regulatory Model's terrain pre-processor

AERMOD AMS/EPA Regulatory Model

AMS American Meteorological Society

AQAT Air Quality Assessment Tool

AQRV Air Quality Related Value

AQS Air Quality System

BACT Best Available Control Technology

BPIP-PRIME Building Profile Input Program – Plume Rise Model Enhancements

CAA Clean Air Act

CAIR Clean Air Interstate Rule

CCS carbon capture and sequestration

CEM continuous emission monitor

CFR Code of Federal Regulations

CH₄ methane

CO carbon monoxide

CO₂ carbon dioxide

CO₂e carbon dioxide equivalent (greenhouse gases)

CRF capital recovery factor

<u>Abbreviation</u> <u>Term/Phrase/Name</u>

CSAPR Cross State Air Pollution Rule

CSR Code of State Regulations (West Virginia)

DEM digital elevation model

EGUs electric utility generating units

EOR enhanced oil recovery

EPA U.S. Environmental Protection Agency

ESPs electrostatic precipitators

FLAG Federal Land Managers' Air Quality Related Values Work Group

FLM Federal Land Manager

g/cm³ gram per cubic centimeter

g/hp-hr grams per horsepower hour

GE General Electric

GEP Good Engineering Practice

GHG greenhouse gas

GWP global warming potentials

H₂SO₄ sulfuric acid

HAPs hazardous air pollutants

HRSG heat recovery steam generator

kJ/W-hr kilojoules per watt hour

kV kilovolt

LAER Lowest Achievable Emission Rate

lb/hr pounds per hour

<u>Abbreviation</u> <u>Term/Phrase/Name</u>

lb/MMBtu pound per million British thermal units

lb/MW-hr pound per megawatt-hour

MACT Maximum Achievable Control Technology

MMBtu/hr million British thermal units per hour

MMCF million cubic feet

MW megawatt

MW-hr megawatt-hour

N/A not applicable

N₂O nitrous oxide

NAAQS National Ambient Air Quality Standards

NAD North American Datum

NAICS North American Industry Classification System

NED National Elevation Dataset

NESHAP National Emission Standard for Hazardous Air Pollutants

ng/J nanogram per Joule

NO₂ nitrogen dioxide

NO_x nitrogen oxides

NSPS New Source Performance Standards

NSR New Source Review

 O_2 oxygen

OAQPS Office of Air Quality Planning and Standards

OEPA Ohio Environmental Protection Agency

Abbreviation <u>Term/Phrase/Name</u>

OLM Ozone Limiting Method

PANs peroxyacetyl nitrates

PBL Planetary Boundary Layer

Pleasants Energy Pleasants Energy, LLC

PM particulate matter

PM₁₀ particulate matter of 10 microns in diameter or smaller

PM_{2.5} particulate matter of 2.5 microns in diameter or smaller

ppm parts per million

ppmvd parts per million by volume, dry basis

PRIME Plume Rise Model Enhancements

PSD Prevention of Significant Deterioration

PVMRM Plume Volume Molar Ratio Method

RBLC RACT/BACT/LAER Clearinghouse

ROI radius of impact

SCR selective catalytic reduction

SIC Source Industrial Classification

SIL Significant Impact Level

SIP State Implementation Plan

SNCR selective non-catalytic reduction

SO₂ sulfur dioxide

SO₃ sulfur trioxide

SO₄ primary sulfate

Abbreviation <u>Term/Phrase/Name</u>

TDS total dissolved solids

tpy tons per year

USGS U.S. Geological Survey

UTM Universal Transverse Mercator

VOC volatile organic compounds

WVDEP West Virginia Department of Environmental Protection

1.0 EXECUTIVE SUMMARY

Pursuant to the requirements specified in the West Virginia Code of State Regulations (CSR), Title 45, Series 14 Air Quality provisions, Pleasants Energy, LLC (Pleasants Energy) is submitting this Prevention of Significant Deterioration (PSD) air construction permit application for the proposed modification of the Pleasants Energy facility. Pleasants Energy, located near Waverly, West Virginia within Pleasants County, installed two simple-cycle General Electric (GE) 7FA combustion turbines at the Pleasants Energy facility in 2001, under permit number R13-2373, with an administrative amendment in 2006 (R13-2373A). The facility received a minor source air construction permit in 2015 for the installation of TurboPhase engines to increase the output of the combustion turbines. In January 2017, Pleasants Energy also received a Prevention of Significant Deterioration (PSD) air construction permit (permit number R14-0034) to lift the original synthetic minor source limits and increase both natural gas and fuel oil (ultra-low sulfur diesel) operation for the two combustion turbines. Since the synthetic minor source limits were lifted, the facility required a PSD permit as if a permit never originally existed for the combustion turbines.

Pleasants Energy is now proposing to not install TurboPhase to increase output of the combustion turbines but would like to perform an uprate on the combustion turbines (Project). The Project will modify the combustion turbines from the 7FA.03 configuration to the 7FA.04 configuration and increase output during the summer peak season. Since the Project will physically modify the combustion turbines and due to the permitting history of the site, this Project will be subject to PSD. The operational fuel usage limits will not change from the 2017 PSD air permit limits. The facility also includes five Tier IV diesel generators that will operate in emergency situations for black start capabilities for the combustion turbines. These generators were changed to non-emergency status in the Turbophase construction permit, but will now be used for emergency purposes only.

As required pursuant to the above-referenced rules, this permit application contains the following analyses/assessments regarding emissions of regulated pollutants associated with the construction and operation of the Project:

- Evaluation of ambient air quality in the area for each regulated pollutant for which the combustion turbine Project will result in a significant net emissions increase
- Demonstration that emissions increases will not cause or contribute to an increase in ambient concentrations of pollutants exceeding the remaining available PSD Increment and the National Ambient Air Quality Standards (NAAQS)

- Assessment of any adverse impacts on soils, vegetation, visibility, and growth in the area
- A Best Available Control Technology (BACT) analysis for each regulated pollutant for which the combustion turbine Project will result in a significant net emissions increase

Potential emissions from the Project are given in Table 1-1 which includes start-up and shutdown emissions for the combustion turbines. A full description of equipment associated with the Project is provided in Part 3 of the application.

Pollutant	Preliminary Maximum Potential Emissions (tons per year) ^a	PSD Significance Levels (tons per year)
NO_x	464.6	40
CO	471.1	100
PM/PM ₁₀ ^b /PM _{2.5} ^b	83.3	25/15/10
SO_2	37.2	40
VOC	20.3	40
H ₂ SO ₄ Mist	6.0	7
Lead	0.007	0.6
CO2e	1.139.578	75 000

Table 1-1: Project Maximum Potential Emissions and PSD Significance Levels

1.1 HAP Emissions

Hazardous air pollutant (HAP) emissions from the Project were calculated to determine the total HAP emissions for National Emission Standards for Hazardous Air Pollutants (NESHAP) applicability. The Project will be an area source of HAPs and the entire Pleasants Energy facility will remain an area source of HAPs with the addition of this Project.

1.2 Air Quality Analysis

The existing air quality in the Pleasants County area is designated as attainment or unclassifiable with regard to the NAAQS for all criteria pollutants. An air dispersion modeling analysis was performed for the pollutants subject to PSD to assess potential ambient air quality impacts associated with the Project. The modeling was performed in accordance with approved West Virginia Department of Environmental Protection (WVDEP) and U.S. Environmental Protection Agency (EPA) modeling guidance. The air dispersion modeling protocol for the Project was submitted to the WVDEP in August 2017, with an update submitted in September 2017.

⁽a) Numbers in bold indicate the PSD significance level is exceeded

⁽b) Filterable plus condensable

1.3 BACT

A "top-down" BACT analysis was performed for each of the pollutants in Table 1-1 that were above the PSD significance levels: carbon monoxide (CO), nitrous oxides (NO_x), particulate matter (PM)/ particulate matter of 10 microns in diameter or smaller (PM₁₀)/ particulate matter of 2.5 microns in diameter or smaller (PM_{2.5}), and greenhouse gases (CO₂e).

BACT has been selected to minimize emissions from the Project. Emissions of NO_x from the combustion turbines will be controlled by low NO_x burners. Use of clean fuels and good combustion practices will control emissions of $PM/PM_{10}/PM_{2.5}$ and CO. Emissions of CO_2 e will be controlled by the use of natural gas as a primary fuel and with efficient turbine design.

Table 1-2 displays the BACT results for the simple-cycle combustion turbines.

Pollutant Control BACT Emissions a,b,c,d Average Low NO_x burners (natural gas) 9 ppm (natural gas) NO_x 30-day rolling Water injection (fuel oil) 42 ppm (fuel oil) 9 ppm (natural gas) CO Good combustion practices 30-day rolling 20 ppm (fuel oil) Combustion controls, inlet air filtration, and 15.9 lb/hr (natural gas) 3-run stack $PM/PM_{10}/PM_{2.5}$ low ash fuels (natural gas and 41.0 lb/hr (fuel oil) test low sulfur fuel oil) 1,300 lb CO₂/MW-hr, 12-month Use of natural gas as a primary rolling gross Greenhouse gases fuel and 1,900 lb CO₂/MW-hr, 12-month efficient turbine design rolling

Table 1-2: Summary of BACT Results – Simple-Cycle Combustion Turbines

1.4 Additional Impacts Analysis

The potential impacts of the Project on visibility, soils, vegetation, and growth are discussed in Part 8 of this application. As indicated by the analysis, the addition of the Project will not have a significant impact on visibility, soils, growth, or vegetation in the surrounding area.

⁽a) ppm = parts per million; lb/hr = pounds per hour; lb/MW-hr = pound per megawatt hour; tpy = tons per year (b) BACT emission rates only presented in this table. Maximum lb/hr and tpy are presented in Appendix C for all emission units.

⁽c) Concentration at 15 percent oxygen while operating at 60 percent load and greater under steady state conditions, unless otherwise noted

⁽d) Emission rate at loads of 60 percent and higher

2.0 INTRODUCTION

Pursuant to the requirements specified in the West Virginia Code of State Rules, Title 45 Series 14, Pleasants Energy, located near Waverly, West Virginia, within Pleasants County, is submitting this PSD construction permit application for the proposed modification of the Pleasants Energy simple-cycle combustion turbine plant. Pleasants Energy installed two simple-cycle GE 7FA combustion turbines at the Pleasants Energy facility in 2001 and operates under Title V permit number R30-07300022-2014. The facility received a minor source air construction permit in 2015 for the installation of TurboPhase engines to increase the output of the combustion turbines. In January 2017, Pleasants Energy also received a Prevention of Significant Deterioration (PSD) air construction permit to lift the original synthetic minor source limits and increase both natural gas and fuel oil (ultra-low sulfur diesel) operation for the two combustion turbines. Since the synthetic minor source limits were lifted, the facility required a PSD permit as if a permit never originally existed for the combustion turbines.

Pleasants Energy is now proposing to not install TurboPhase to increase output of the combustion turbines but would like to perform an uprate on the combustion turbines (Project). The Project will modify the combustion turbines from the 7FA.03 configuration to the 7FA.04 configuration and increase output during the summer peak season. Since the Project will physically modify the combustion turbines and due to the permitting history of the site, this Project will be subject to PSD. The facility also includes five Tier IV diesel generators that will operate in emergency situations for black start capabilities for the combustion turbines. These generators were changed to non-emergency status in the Turbophase construction permit, but will now be used for emergency purposes only.

Table 2-1 shows potential air emissions associated with the Project including start-up and shutdown emissions for the turbines. The maximum emissions from any operating load and including start-up and shutdown emissions for the combustion turbines were used to demonstrate the maximum potential emissions for each pollutant.

Pollutant	Preliminary Maximum Potential Emissions (tons per year) ^a	PSD Significance Levels (tons per year)	
NO_x	464.6	40	
СО	471.1	100	
$PM/PM_{10}^{b}/PM_{2.5}^{b}$	83.3	25/15/10	
SO_2	37.2	40	
VOC	20.3	40	
H ₂ SO ₄ Mist	6.0	7	
Lead	0.007	0.6	
CO ₂ e	1,139,578	75,000	

Table 2-1: Project Potential Emissions and PSD Significance Levels

As can be seen from Table 2-1, the Project will result in significant emission increases of CO, NO_x , $PM/PM_{10}/PM_{2.5}$, and CO_2e . These pollutants will be subject to PSD review.

The overall HAP emissions from the Project and the entire Pleasants Energy facility show that the facility will continue to be an area source of HAPs.

This construction permit application is divided into the following sections:

- Part 1 Executive Summary
- Part 2 Introduction
- Part 3 Project Description
- Part 4 Emissions Estimates (This section provides estimates of emissions associated with the combustion turbine Project.)
- Part 5 Regulatory Review (This section identifies applicable State and Federal air quality regulations.)
- Part 6 BACT Analysis
- Part 7 Air Dispersion Modeling (This section provides model descriptions and data requirements for the air quality impact assessment as well as interpretation, analysis, and comparison of the modeling results with applicable air quality regulations.)
- Part 8 Additional Impact Analysis (This section addresses other potential air quality-related impacts (i.e., growth, soil, vegetation, and visibility).

⁽a) Numbers in bold indicate the PSD significance level is exceeded

⁽b) Filterable plus condensable

Construction permit application forms and attachments required by the WVDEP are included in Appendix A of this application.

3.0 PROJECT DESCRIPTION

Pleasants Energy plans to increase the hours of operation of its two simple-cycle GE 7FA combustion turbines at the Pleasants Energy facility located near Waverly, West Virginia. They currently operate under Title V permit number R30-07300022-2014. The facility is located in Pleasants County, which is currently designated as an attainment/unclassified area for all criteria pollutants in 40 Code of Federal Regulations (CFR) Part 81. The location of the Project is shown in Figure B-1 (Appendix B). A plot plan of the Project with the emission point locations is shown in Figures B-2 and B-3 (Appendix B).

The combustion turbines operate in simple-cycle mode only to generate electricity. The combustion turbines will be permitted with restricted operation. The turbines will have a combined NO_x limit of 464.6 tpy, with compliance shown via continuous emission monitors (CEMs). Additionally, the combustion turbines will be limited to 37.2 tpy of SO₂ emissions on an annual basis. For all other pollutants, the turbines will have an overall fuel usage limit for both combustion turbines combined of 19,082,000,000 standard cubic feet per year (SCF) per year which includes both fuel oil and natural gas. Fuel oil, when combusted will be equal to 889 million cubic feet (MMCF) per gallon of fuel oil. This fuel limit methodology is consistent with their current minor source permit limitation. To accommodate the SO₂ limit of 37.2 tons per year to remain minor for PSD, Pleasants proposes a fuel oil limit of 7,688,886 gallons per year for both combustion turbines combined.

To control emissions of NO_x, each of the combustion turbines will be equipped with low NO_x burners. To minimize the emissions of sulfur dioxide (SO₂), sulfuric acid (H₂SO₄) mist, and PM/PM₁₀/PM_{2.5}, the combustion turbines will be controlled through the use of low sulfur fuels and good combustion practices.

4.0 EMISSIONS ESTIMATES

Emission of air contaminants will result from the combustion of natural gas and fuel oil (as a backup fuel) in the proposed simple-cycle combustion turbines.

A process flow diagram for the combustion turbines are shown in Figure B-4 (Appendix B). The operating conditions of the combustion turbines are discussed in detail in the sections below, along with the procedures for estimating emissions. Tables showing the emission calculations are included in Appendix C.

4.1 Combustion Turbine Emissions Calculation Method

Emissions from the F-Class combustion turbines are dependent on the ambient temperature conditions and the turbines' operating load, which can vary from 60 percent to 100 percent. To account for representative seasonal climatic variations, potential emissions from the proposed combustion turbines were analyzed at 60 and 100 percent load conditions for ambient temperatures ranging from negative (-) 10 degrees Fahrenheit (°F) to 100°F. Projected emissions were based on data provided by GE for the 7FA combustion turbine and AP-42 emission factors. Detailed calculations of the combustion turbine's emissions are provided in Appendix C.

The following conservative assumptions were used to determine potential emissions from the Project:

- A fuel limit of 19,082,000,000 standard cubic feet (SCF) of natural gas and fuel oil combined per year
- A fuel oil factor of 889 scf/gal of fuel oil combusted
- A fuel oil limit of 7,668,886 gallons per year combined per year
- A NO_x annual emissions limit from both combustion turbines combined of 464.6 tpy
- A SO₂ annual emissions limit from both combustion turbines combined of 37.2 tpy

Natural Gas Operation:

• Start-up and shutdown emissions on natural gas were based on the start-up profile (assumes 120-minutes per start-up and 60 minutes per shutdown) and 365 start-up/shutdown events¹ with up to 30 start-up/shutdown events on fuel oil

-

¹ One start-up/shutdown event is equal to one start-up plus one shutdown. All start-ups were conservatively assumed to be cold start-ups.

- NO_x emissions were based on the BACT emissions rate 9 parts per million (ppm) and 68.9 pounds per hour (lb/hr) per turbine for loads of 60 percent and higher with low NO_x burners
- CO emissions were based on the BACT emission rate of 9 ppm and 33.9 lb/hr for loads of 60 percent and greater
- PM/PM₁₀/PM_{2.5} emissions were based on an estimated maximum emission rate of 15.9 lb/hr
- SO₂ emissions were based on sulfur content of the natural gas and an estimated maximum emission rate of 2.7 lb/hr
- Volatile organic carbon (VOC) emissions were based on vendor emission rate of 3.2 lb/hr for loads of 60 percent and higher
- H₂SO₄ mist emissions were based on mass balance of 10 percent of SO₂ being converted to sulfur trioxide (SO₃) and 100 percent of SO₃ being converted to H₂SO₄ resulting in 0.41 lb/hr
- CO₂e emissions were based on AP-42 emission factors for carbon dioxide (CO₂), methane (CH₄), and nitrous oxide (N₂O), and ratioed with their appropriate global warming potentials (GWP) and summed to obtain CO₂e

Fuel Oil Operation:

- NO_x emissions were based on the BACT emissions rate 42 ppm at 15% O₂ and 470.0 lb/hr per turbine for loads of 60 percent and higher with low NO_x burners
- CO emissions were based on the BACT emission rate of 20 ppm and 76.0 lb/hr for loads of 60 percent and greater
- PM/PM₁₀/PM_{2.5} emissions were based on an estimated maximum emission rate of 41.0 lb/hr based on vendor data
- SO₂ emissions were based on sulfur content of the natural gas and an estimated maximum emission rate of 109.0 lb/hr
- VOC emissions were based on vendor emission rate of 20.0 lb/hr for loads of 60 percent and higher
- H₂SO₄ mist emissions were based on mass balance of 10 percent of SO₂ being converted to SO₃
 and 100 percent of SO₃ being converted to H₂SO₄ resulting in 17.7 lb/hr
- CO₂e emissions were based on AP-42 emission factors for CO₂, CH₄ and N₂O, and ratioed with their appropriate GWP and summed to obtain CO₂e for distillate fuel oil operation

• Start-up and shutdown emissions on fuel oil were based on the start-up profile (assumes 120-minutes per start-up and 60 minutes per shutdown) and 30 start-up/shutdown events on fuel oil² per turbine.

Based on the above assumptions, Table 4-1 displays the maximum expected hourly emission rates for each combustion turbine stack during natural gas and fuel oil operation.

GE 7FA PM/ PM₁₀/ NO_x CO VOC SO₂ H₂SO₄ CO₂e Combustion $PM_{2.5}$ **Turbine** (Uprate) pounds per hour (lb/hr) Natural gas 68.9 33.9 15.9 3.2 2.7 0.41 223,611 Fuel oil 470.0 76.0 41.0 20.0 109.0 17.7 337.813

Table 4-1: Maximum Expected Hourly Emission Rates for Each Combustion Turbine

4.2 Turbine Start-Up and Shutdown Emissions Calculation Method – Natural Gas Operation

Each combustion turbine may start up to 365 times per year which may include up to 30 starts on fuel oil. For natural gas combustion, potential start-up and shutdown emissions were based on a start-up profile and conservatively assumed that there would be up to 365 cold start-ups and 365 shutdown events per turbine per year on natural gas. One start-up and shutdown event is equivalent to one start-up (0 percent load to when the turbine is in "Mode 6," which is approximately 60 percent load or minimum load for steady state operation and emissions compliance) plus one shutdown (60 percent load or minimum load for steady state operation and emissions compliance to 0 percent load). Start-up is assumed to take 120 minutes while shutdown shall take 60 minutes for a total of 180 minutes for one start-up and shutdown event. Potential start-up and shutdown emissions for each combustion turbine are shown in Table 4-2.

Detailed calculations of the potential start-up and shutdown emissions are provided in Appendix C.

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² One start-up/shutdown event is equal to one start-up plus one shutdown. All start-ups were conservatively assumed to be cold start-ups.

Table 4-2: Potential Combustion Turbine Start-up and Shutdown Emissions – Natural Gas Operation

Pollutant	Start-up Emissions (lb/hr) ^{a,b}	Shutdown Emissions (lb/hr) ^{a,c}	Maximum Number of Starts Per Turbine ^d	Start-up /Shutdown Emissions (tpy) ^a	Total Start-up /Shutdown Emissions (Both turbines) (tpy) ^a
NO_x^a	125.5	107.2	365	65.4	130.7
COa	386.3	146.3	365	167.7	335.4
PM/PM ₁₀ / PM _{2.5}	15.9	15.9	365	8.7	17.4
VOCa	7.0	6.4	365	3.7	7.5
SO_2	2.7	2.7	365	1.5	3.0
H ₂ SO ₄	0.41	0.41	365	0.23	0.45
Lead					
CO_2	223,611	223,611	365	122,427	244,854

⁽a) lb/hr = pounds per hour; tpy = tons per year

4.3 Combustion Turbine Start-Up and Shutdown Emissions Calculation Method - Fuel Oil Operation

Potential start-up and shutdown emissions were based on a start-up profile and conservatively assumed that there would be 30 cold start-ups and 30 shutdown events per turbine per year on fuel oil. One start-up and shutdown event is equivalent to one start-up (0 percent load to when the turbine is in "Mode 6," which is approximately 60 percent load or minimum load for steady state operation and emissions compliance) plus one shutdown (60 percent load or minimum load for steady state operation and emissions compliance to 0 percent load). Start-up is assumed to take 120 minutes while shutdown shall take 60 minutes for a total of 180 minutes for one start-up and shutdown event. Potential start-up and shutdown emissions for each combustion turbine while operating on fuel oil are shown in Table 4-3.

Detailed calculations of the potential start-up and shutdown emissions are provided in Appendix C.

⁽b) Includes start-up emissions from GE Start-up Summary and actual CEMS start-up data.

⁽c) Includes shutdown emissions from GE Start-up Summary and actual CEMS shutdown data.

⁽d) One start-up and shutdown event is equivalent to one start-up plus one shutdown. All emissions based on worst-case cold start data.

Table 4-3: Potential Combustion Turbine Start-up and Shutdown Emissions – Fuel Oil Operation

Pollutant	Start-up Emissions (lb/hr) ^{a,b}	Shutdown Emissions (lb/hr) ^{a,c}	Maximum Number of Starts on Fuel Oil Per Turbine ^d	Start-up /Shutdown Emissions (tpy) ^a	Total Start-up /Shutdown Emissions (Both turbines) (tpy) ^a
NO_x	561.6	543.1	30	25.0	50.0
CO	234.4	199.7	30	10.0	20.1
PM/PM ₁₀ / PM _{2.5}	41.0	41.0	30	1.8	3.7
VOC	21.1	21.0	30	0.9	1.9
SO_2	109.0	109.0	30	4.9	9.8
H ₂ SO ₄	17.7	17.7	30	0.80	1.6
Lead	0.03	0.03	30	8.7 x 10 ⁻⁴	1.7 x 10 ⁻³
CO_2	337,813	337,813	30	15,202	30,403

⁽a) lb/hr = pounds per hour; tpy = tons per year

4.4 Maximum Start-up and Shutdown Emissions

The turbines will be limited to 365 total start-up/shutdown events per year of which up to 30 events may be on fuel oil. Table 4-4 displays the emissions from 335 start-up/shutdown events on natural gas and 30 start-up/shutdown events on fuel oil. This represents the worst-case emissions for start-up/shutdown emissions.

⁽b) Includes start-up emissions from GE Start-up Summary and actual CEMS start-up data.

⁽c) Includes shutdown emissions from GE Start-up Summary and actual CEMS shutdown data.

⁽d) One start-up and shutdown event is equivalent to one start-up plus one shutdown. All emissions based on worst-case cold start data.

Table 4-4: Potential Combustion Turbine Start-up and Shutdown Emissions – Maximum Emissions

Pollutant	Number of Natural Gas Starts Per Turbine	Start- up/Shutdown Emissions Natural Gas (tpy)	Number of Fuel Oil Starts Per Turbine	Start- up/Shutdown Emissions Fuel Oil (tpy)	Total Start- up/Shutdown Emissions (Both turbines) (tpy) ^a
NOx	335	60.0	30	25.0	170.0
CO	335	153.9	30	10.0	327.9
PM/PM ₁₀ /PM _{2.5}	335	8.0	30	1.8	19.7
VOC	335	3.4	30	0.9	8.7
SO_2	335	1.4	30	4.9	12.5
H ₂ SO ₄	335	0.21	30	0.80	2.0
Lead	335		30	8.7 x 10 ⁻⁴	0.002
CO ₂ e	335		30	15,202	255,132

⁽a) Maximum start-up/shutdown emissions based on 335 starts per year on natural gas and 30 starts per year on fuel oil.

4.5 Turbine HAP Emissions Calculation Method

The Project will emit HAPs. Detailed HAP emissions calculations from the Project are shown in Appendix C. Emissions of HAPs for this Project will be below 10 tpy of any single HAP and 25 tpy for all aggregate HAPs. HAP emissions from the Project and existing combustion equipment were evaluated for purposes of determining regulatory applicability. The facility will also remain an area source of HAPs with the addition of this Project.

4.6 Diesel Generators (Black Start Generators) Calculation Method

As discussed, the five Tier IV diesel generators were changed from emergency status to non-emergency status through the permitting action for the addition of the TurboPhase engines. Pleasants no longer wishes to operate the generators for non-emergency purposes and so would like to change their status back to emergency. As such, annual emissions for the diesel generators is now based on 100 hours, but the emission rates (lb/hr, grams per horsepower hour [g/hp-hr]) will not change. See Appendix C for annual emission calculations for the diesel generators.

5.0 REGULATORY REVIEW

Revision 0

The Project is subject to various federal and state air regulations. The combustion turbines will combust natural gas and fuel oil as backup. The facility is located approximately ¾ of a mile to the east of Waverly, West Virginia, within Pleasants County. Part 5 contains a discussion of the PSD regulations, applicable Federal regulations, and applicable WVDEP provisions. Where applicable, reference to general limitations is provided when there is no specific requirement that applies to an emission source.

In instances where there are multiple requirements, it is understood that compliance with the most restrictive requirement will demonstrate compliance with all other requirements.

Air quality permitting in West Virginia is under the jurisdiction of the WVDEP. The EPA has given the WVDEP authority to implement and enforce the federal Clean Air Act (CAA) provisions and state air regulations under its approved State Implementation Plan (SIP). The following subsections discuss the applicable federal and state air quality programs, regulations, and standards.

5.1 PSD Regulations and 45 CSR 14

The existing Pleasants Energy facility was previously permitted as a minor source facility for PSD, with a fuel usage limit that kept the facility to less than 250 tpy of any regulated PSD pollutant. In 2017, the facility received a PSD permit to increase the operational capacity of the combustion turbines. Since this PSD permit application is being submitted shortly after the 2017 permit, the facility has not yet operated to its full new operational limits under the PSD permit. Therefore, any PSD netting analysis of past actual emissions to future potential emissions will result in approximately the same pollutants being subject to PSD. Therefore, emissions estimates are based solely on the future potential emissions and netting is not part of this project. Appendix C contains the emissions estimates which do also show the past actual emissions for the combustion turbines as well as the future potential. Therefore, this Project is subject to PSD regulations.

PSD review is required for all criteria pollutants that will be emitted above significant levels in accordance with 40 CFR 52.21 (incorporated by reference in 45 CSR 14-2.74). PSD review consists of the following:

- A BACT analysis
- An air quality analysis
- An analysis of additional impacts on visibility, soils, vegetation, and growth

Three criteria were evaluated to determine PSD applicability (EPA 1990):

- 1. Whether the Project is sufficiently large (in terms of its emissions) to be a "major" stationary source or "major" modification.
- 2. Whether the source is located in a region designated as "attainment" or "unclassified."
- 3. Whether the pollutants emitted from a major stationary source exceed the significant emission levels defined by 40 CFR 51.21.

PSD pollutants include NO_x, SO₂, CO, PM, PM₁₀, PM_{2.5}, VOC, CO₂e, hydrogen sulfide, H₂SO₄ mist, fluorides, and lead. The definition of a "major stationary source" is given in 40 CFR 52.21 (b)(1)(i). The Project is not included in the 28 source categories specified in the PSD regulations as being considered a major stationary source if the potential emissions of a PSD pollutant exceed 100 tpy. Therefore, the facility would be considered a major stationary source if the potential emissions of a PSD pollutant exceed 250 tpy. Potential emissions from this Project are over 250 tpy threshold for NO_x and CO; thus meeting the first criteria for PSD applicability.

The Project is located in an attainment/unclassified area for all criteria pollutants and will be subject to PSD review rather than a non-attainment NSR.

The maximum potential emissions from the Project are listed in Table 1-1 and include start-up and shutdown emissions from the combustion turbines. The following PSD pollutants exceed the significant emission levels defined by 40 CFR 51.21: NO_x, CO, PM, PM₁₀, PM_{2.5}, and CO₂e.

Detailed calculations of potential emissions are contained in Appendix C.

PSD regulations require that the following issues be addressed:

- Determination of BACT on a case-by-case basis, taking into account costs as well as energy, environmental, and economic impacts
- Demonstration that the increase in emissions will not cause or contribute to an exceedance of the NAAQS or PSD Increment
- Analysis of the impairment, if any, to visibility, soils, vegetation, and growth

5.2 New Source Performance Standards (NSPS) (40 CFR Part 60) and 45 CSR 16

Standards of Performance for New Stationary Sources are contained in 40 CFR Part 60 and are adopted by reference in 45 CSR 16. These standards are commonly referred to as new source performance standards (NSPS). The applicable NSPS standards are listed below with a description of how Pleasants Energy plans to meet the standards.

Subpart GG

The combustion turbines are currently subject to the NSPS for combustion turbines, Subpart GG, which is applicable to combustion turbines constructed prior to 2006. However, the combustion turbines meet the definition of "modified" per Subpart A definitions and as such are considered modified after the applicable date of Subpart KKKK; therefore, Subpart GG no longer applies. See requirements under NSPS Subpart KKKK below, which is now applicable to the combustion turbines due to the uprate.

Subpart KKKK

Subpart KKKK is applicable to all stationary combustion turbines that commenced construction, modification or reconstruction after February 18, 2005, with a heat input equal to or greater than 10.7 gigajoules per hour (10 MMBtu/hr). With the modifications to the turbine for the uprate, the turbines are considered "modified" per Subpart A definitions, since there will be an emission increase on an hourly basis for NO_x (natural gas combustion only) as well as SO₂ for both fuels.

Pursuant to 40 CFR §60.4320(a) and Table 1 to Subpart KKKK, the NSPS NO_x limit applicable to the combustion turbine, for fuel oil combustion, is 42 parts per million (ppm) at 15 percent oxygen or 160 nanogram per Joule (ng/J) of useful output (1.3 pound per megawatt-hour [lb/MW-hr]) on a 30-day average. Pleasants Energy expects to have a NO_x limit of 42 ppm at 15 percent oxygen on a 30-day average when combusting fuel oil with the uprate. When combusting natural gas, Table 1 in Subpart KKKK states that new or modified combustion turbines must meet a limit of 15 ppm at 15 percent O₂ or 54 ng/J of useful output (0.43 lb/MWh). When combusting natural gas, the combustion turbines will meet a limit of 9 ppm at 15 percent O₂, and will therefore meet this limit. In accordance with Subpart KKKK, Pleasants Energy will demonstrate compliance with the NO_x emission limit by conducting performance testing pursuant to §60.4340(a), or alternatively, by installing, calibrating, maintaining, and operating a continuous monitoring system (i.e., CEM or continuous parameter monitor) in accordance with §60.4340(b).

The NSPS SO₂ limit for the turbine is 0.90 lb/MW-hr gross output, <u>or</u> limit fuel so that any fuel combusted contains total potential sulfur emissions equal to or less than 0.060 pound per million British thermal units (lb/MMBtu) SO₂ heat input. Pleasants Energy will obtain and keep on record the fuel quality characteristics of the fuel oil from the suppliers.

<u>Subpart TTTT – Not applicable</u>

Subpart TTTT sets Standards of Performance for Greenhouse Gas Emissions for Electric Utility Generating Units (EGUs). This regulation was finalized on August 3, 2015 and applies to new units that commenced construction after January 8, 2014 or reconstruction after June 18, 2015. These combustion turbines commenced construction prior to the applicable date and are not considered "new" source. Further, these combustion turbines do not meet the definition of "reconstructed" or "modified" per the NSPS, so Subpart TTTT is not applicable to the combustion turbines.

5.3 National Emission Standards for Hazardous Air Pollutants (NESHAP) and Maximum Achievable Control Technology (MACT)

NESHAPS are contained in 40 CFR Part 63 and adopted by reference in 45 CSR 34. These rules contain emissions standards set by the EPA for particular source categories to control HAPs. These categories require the maximum degree of emission reduction of certain HAPs that the EPA determines to be achievable, which is known as the Maximum Achievable Control Technology (MACT). The following MACT standards are applicable to the Project. The entire Pleasants Energy facility, including the Project will be an area source of HAPs.

Subpart YYYY- Not applicable

EPA promulgated MACT standards for new stationary combustion turbines on March 5, 2004. These standards apply to stationary combustion turbines on which construction commenced after January 14, 2003 at major sources of HAPs. On April 7, 2004, however, EPA proposed to remove gas-fired units from the combustion turbine source category regulated by Subpart YYYY. In the interim, the EPA has stayed the applicability of Subpart YYYY requirements for gas-fired combustion turbines.

This regulation is not applicable because the Pleasants Energy facility is not a major source of HAPs.

5.4 Mandatory Reporting of Greenhouse Gases – 40 CFR Part 98

40 CFR Part 98 requires facilities that emit 25,000 metric tons or more per year of greenhouse gases to submit annual reports to EPA. This facility will exceed the reporting threshold and, therefore, Pleasants Energy will report greenhouse gas emissions as required.

5.5 Clean Power Plan for Existing Units

The Clean Power Plan has been repealed. This regulation proposed a 32 percent reduction in greenhouse gas emissions from power plants. Currently, it is unknown how future regulation may affect these simple-cycle combustion turbines.

5.6 NAAQS

As stated earlier, Part 7 of this permit application will discuss the ambient air quality analysis and dispersion modeling that will performed for the Project. Modeled impacts will be compared to the NAAQS. The Project is not expected to cause or contribute to a violation of the NAAQS. A full description of the NAAQS modeling analysis will be included in Part 7 of the final permit application.

5.7 Other Ambient Air Quality Standards

Recent Federal Land Manager (FLM) proposed guidance requires, in the course of a PSD application, an assessment of air quality impacts at Class I areas if a proposed major source is located within a certain distance of the Class I area. There are four Class I Areas that are within 300 kilometers of the Project:

- Otter Creek Wilderness (130 kilometers)
- Dolly Sods Wilderness (160 kilometers)
- Shenandoah National Park (200 kilometers)
- James River Face Wilderness (253 kilometers)

A visibility and deposition analysis was performed as part of the January 2017 PSD air construction permit to lift the original synthetic minor source limits (2017 PSD Project). Given that prior visibility and deposition analysis for the 2017 PSD Project was performed and the new Project's emissions are similar (and should not increase on a maximum 24-hour or lb/hr rate for visibility pollutants) to that project's emissions, Pleasants is proposing that no visibility or deposition analysis be required. The information below summarizes the work that was performed as part of the 2017 PSD Project.

The visibility analysis demonstrated that the visibility impact was less than 5.0 percent for year for each Class I area for both natural gas and fuel oil operation. The Project was not expected to have any noticeable effect on visibility since the predicted visibility impacts were well below the level of acceptable change and no further analysis required.

The nitrogen and sulfur deposition modeling results for each Class I area were also well below the applicable Deposition Analysis Threshold (DAT) for the 2017 PSD Project. As a result, the 2017 PSD

Project was not expected to have adverse impacts resulting from deposition and no further analysis was conducted.

Concurrence was received from the FLMs for the 2017 PSD Project that there would be no significant impacts to any air quality related values (AQRVs) at Class I areas for the project.

A visibility analysis using VISCREEN was performed on 2 Class II areas and the results are presented in Part 8 of this permit application.

The PSD Class I and Class II Increment analyses are incorporated in Part 7 of this permit application.

5.8 Additional Impact Analysis

The impact of the Project on soils, vegetation, visibility, and growth was considered as part of the PSD process. The construction and operation of the Project is not expected to have a detrimental effect on plants, soils, or industrial, commercial, and residential growth. A full analysis of these impacts can be found in Part 8 of this permit application.

5.9 Acid Rain (40 CFR Part 75) and 45 CSR 33

Title IV of the CAA imposes stringent requirements on electrical utilities and is enforced through the administration of the Title IV Acid Rain Permit Program, which is designed to achieve reductions in emissions of SO₂ and NO_x. The centerpiece of the Title IV program is the establishment of an SO₂ emissions allowance and trading program. The Project will be subject to the 40 CFR Part 75 Acid Rain regulations. Pleasants Energy currently holds an Acid Rain Permit and will be required to update that permit, per the regulations.

In accordance with the Acid Rain regulations, Pleasants energy will submit the application forms to the WVDEP for the revision to their Acid Rain Permit. The contents of the Acid Rain Permit will be incorporated into the modified Title V Operating Permit discussed previously.

5.10 Clean Air Interstate Rule (CAIR) and Cross State Air Pollution Rule (CSAPR)

The facility currently holds allowances per the Cross State Air Pollution Rule (CSAPR). It is assumed that Pleasants Energy has allowances to use or may obtain more allowances for this project from the new unit set aside.

5.11 Monitoring and Compliance

Monitoring and compliance requirements for operation of the Project come from 40 CFR Part 75 (Acid Rain). The turbines qualify as non-peaking units and are required to install a NO_x CEM.

5.11.1 Continuous Emission Monitor

The Project is subject to the compliance monitoring requirements under the Acid Rain regulations in 40 CFR Part 75 and NSPS in 40 CFR Part 60. The combustion turbines will continue to employ CEMs in accordance with 40 CFR Part 75 to continuously monitor nitrogen dioxide (NO₂), and volumetric flow rate. The test plan will be contained in the Part 75 monitoring plan and certification application that will be subsequently submitted within the appropriate time periods. CEMs are not required for monitoring SO₂ emissions because natural gas has inherently low sulfur content.

5.12 Title V Operating Permit

40 CFR Part 70, otherwise known as Title V of the CAA, established an air quality operating permit program that provides a central point for tracking all applicable air quality requirements for every source required to obtain a permit. Each state was also required to establish a Title V Operating Permit Program. 45 CSR 30, Requirements for Operating Permits, establishes such a program. Pleasants Energy will follow the requirements in 45 CSR 30 in order to update their Title V permit with the changes from the Project.

5.13 West Virginia Air Quality Standards and Regulations

This section describes the WVDEP regulations which apply to the Project.

5.13.1 45 CSR 10: To Prevent and Control Air Pollution of Sulfur Oxides

Pleasants Energy will meet all applicable requirements of 45 CSR 10. The combustion turbines are classified as Type 'b' units under this rule. Pleasants Energy is located in Pleasants County, West Virginia and is therefore located in Priority Region II. They will meet the following sulfur dioxide weight emission standard as per §45-10-3.1.e:

- Type 'b' fuel burning units must not discharge sulfur dioxide from all stacks located at one plant, measured in terms of pounds per hour, in excess of the product of 3.1 and the total design heat inputs for such units in MMBtu/hr.
- Pleasants Energy will meet all testing, monitoring, recordkeeping and reporting requirements as per §45-10-8.

5.13.2 45 CSR 13: Permits for Construction, Modification, Relocation, and Operation of Stationary Sources of Air Pollutants, Notification Requirements, Administrative Updates, Temporary Permits, General Permits, Permission to Commence Construction, and Procedures for Evaluation

Pleasants Energy will meet all requirements of 45 CSR 13 in order to obtain a construction permit for this project.

5.13.3 45 CSR 20: Good Engineering Practice as Applicable to Stack Heights

Pleasant Energy will construct all stacks in accordance with good engineering practice according to 45 CSR 20.

5.13.4 45 CSR 22: Air Quality Management Fee Program

Pleasants Energy will submit all fees required by 45 CSR 22 in order to obtain a PSD construction permit.

6.0 BEST AVAILABLE CONTROL TECHNOLOGY ANALYSIS

Federal regulations specify that the owner of a facility subject to a PSD permit must perform a BACT analysis for the control of each PSD regulated pollutant emitted in significant quantities from a new stationary source located in an attainment area. As indicated in Part 5, this Project is subject to PSD review for NO_x, CO, PM/PM₁₀/PM_{2.5}, and CO₂e. Therefore, a BACT analysis has been prepared for these pollutants.

Pleasants Energy is permitting two natural gas-fired GE 7FA combustion turbines with fuel oil back-up at the Pleasants Energy facility located near Waverly, West Virginia. The combustion turbines will be operated solely in simple-cycle mode and will be permitted for 19,082,000,000 SCF of natural gas and fuel oil consumption per year combined. Fuel oil, when combusted will be equal to 889 MMCF per gallon of fuel oil. Additionally, the combustion turbines will be limited to 464.6 tpy combined NO_x emissions and 37.2 tpy combined SO₂ emissions. This Part describes the BACT analysis for the combustion turbines.

The two combustion turbines will be F-Class combustion turbines with a nominal output of 168 megawatt (MW), each³ (with a maximum heat input of 1,910 MMBtu/hr on natural gas and 2,065 MMBtu/hr on fuel oil, each).

The BACT analysis was performed using the "top-down" approach, which is described in this Part. Along with the potential annual emissions, a summary of the proposed BACT emission limits and the associated control technologies for simple-cycle combustion turbines are shown in Table 6-1. BACT is an emission limitation based on the maximum degree of reduction which the WVDEP determines is achievable, on a case-by-case basis, taking into account energy, environmental, and economic impacts and other costs.

The EPA has directed by policy that the BACT be determined using a process referred to as the "top-down" approach. The "top-down" process was outlined in a December 1, 1987 memorandum from the EPA Assistant Administrator for Air and Radiation.

³ Net output at 59 degrees Fahrenheit and 100 percent load

Pollutant	Control	BACT Emissions ^{a,b,c,d}	Average
NO	Low NO _x burners (natural gas)	9 ppm (natural gas)	20 day galling
NO_x	Water injection (fuel oil)	42 ppm (fuel oil)	30-day rolling
СО	Good combustion practices	9 ppm (natural gas) 20 ppm (fuel oil)	30-day rolling
PM/PM ₁₀ /PM _{2.5}	Combustion controls, inlet air filtration, and low ash fuels (natural gas and low sulfur fuel oil)	15.9 lb/hr (natural gas) 41.0 lb/hr (fuel oil)	3-run stack test
Greenhouse gases	Use of natural gas as a primary fuel and efficient turbine design	1,300 lb CO ₂ /MW-hr, gross 1,900 lb CO ₂ /MW-hr, gross	12-month rolling 12-month rolling

Table 6-1: Summary of BACT Results - Simple-Cycle Combustion Turbines

A BACT determination is made for each pollutant for which emissions (as a result of new emission points or a modification to existing emission points) will be greater than the PSD significant emission rate.

An emission limit proposed in a permit application does not automatically mean that the limit has been "achieved in practice" on a similar unit. Many PSD and Lowest Achievable Emission Rate (LAER) permits have been issued over the years for projects that were never constructed and, therefore, never operated. As a result, those emission limits have never been "achieved in practice." There are also instances in which incorrect limits have been posted to the RBLC, or where the ultimate and final permit limits were subsequently modified prior to permit issuance. In some cases, an applicant may have proposed very stringent limits without a meaningful commercial guarantee, perhaps to avoid a more onerous requirement or an unacceptable air quality impact, and was then unable to continuously achieve the limits in practice. It is also very important to note that an emission rate based on a BACT finding must be continuously met under all normal operating conditions, not just at one optimal design point. Therefore, there must a reasonable assurance that each BACT limit evaluated is truly "demonstrated in practice" on a similar unit and can be continuously achieved under all expected operating condition for the life of the unit.

As identified in EPA's October 1990 draft of the New Source Review (NSR) Workshop Manual, the basic steps of the "top-down" BACT analysis used in this analysis are listed below:

⁽a) ppm = parts per million; lb/MW-hr = pound per megawatt hour; tpy = tons per year

⁽b) BACT emission rates only presented in this table. Maximum lb/hr and tpy are presented in Appendix C for all emission units.

⁽c) Concentration at 15 percent oxygen while operating at 60 percent load and greater under steady state conditions, unless otherwise noted

⁽d) Emission rate at loads of 60 percent and higher

- Step 1 Identify all potential control technologies
- Step 2 Determine technical feasibility (of potential technologies)
- Step 3 Rank control technologies by control effectiveness
- Step 4 Evaluate most effective controls and document results
- Step 5 Select BACT

The EPA has interpreted the statutory and regulatory BACT definitions as containing two core requirements that must be met by any BACT determination. First, the BACT analysis must include consideration of the most effective control options that could be applied. Second, any decision to allow a less stringent emission rate must be justified by an objective analysis of "energy, environmental, and economic impacts" (EPA 1990). This is tempered, however, by the following statement from the NSR Workshop Manual:⁴

"Technologies which have not yet been applied to (or permitted for) full scale operations need not be considered available; an applicant should be able to purchase or construct a process or control device that has already been demonstrated in practice."

The first step in the "top-down" BACT process is the identification of potentially available control technologies. One of the ways to identify available control technologies is to review previous BACT determinations for similar sources. EPA's RACT/BACT/LAER Clearinghouse (RBLC) database was reviewed to identify recent BACT determinations for similar projects. This database is maintained on EPA's Technology Transfer Network website at www.epa.gov/ttn/catc. Advanced queries of the database were conducted to identify control technology determinations from January 2000 to September 2017 for sources similar to the proposed combined-cycle combustion turbines and applicable auxiliary equipment. The results of the RBLC query can be found in Appendix D in Tables D-1 to D-8.

To identify previous control technology determinations for comparable sources, a query was run using the "standard search" in which the RBLC database was searched using the following parameters:

- Combustion turbines, Simple-Cycle, 15.220 Natural gas combustion;
- Combustion turbines, Simple-Cycle, 15.290 Fuel oil combustion;
- Draft Determinations and RBLC Permits issued during or after January 2000;
- Source Industrial Classification (SIC) code of 4911 for electrical generation plants; and

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⁴ NSR Workshop Manual, EPA, October 1990, section IV.A.1. Demonstrated and Transferable Technologies. Page B-11

 North American Industry Classification System (NAICS) code for a combustion turbine electrical generation plant 221112 which includes all types of fossil fuel electrical generation plants.

The NAICS and SIC codes are the most appropriate codes to search in the advanced search option of the RBLC. The SIC and NAICS are systems of source classification developed for the purpose of differentiating industrial types. The SIC and the NAICS systems are used in many EPA documents to differentiate types of industries. It is appropriate to use these codes as the match criteria in queries of the RBLC database since other facilities that use similar turbines will likely have similar characteristics. After the NAICS and SIC codes were identified and queries run, combustion turbines that were not similar (e.g., digester gas-fired, cogeneration units, boilers, combined-cycle combustion turbines, etc.) were eliminated from the search. Information on turbine emissions was sorted from this listing. A discussion of control options identified in the RBLC database is included in each subsection.

In some cases, the RBLC listings are not clearly categorized and cover both simple- and combined-cycle installations. Also, it should be noted that all RBLC listings in California represent Lowest Achievable Emission Rate (LAER); although they are often listed as BACT, BACT and LAER are essentially the same in California. LAER is a much more stringent requirement than BACT, and involves application of control technology regardless of cost. This is not the case for the proposed combustion turbines for this Project, which are subject only to BACT.

6.1 BACT for Nitrogen Oxides (NO_x) – Combustion Turbines

6.1.1 Step 1. Identify All Potential Control Strategies

NO_x is primarily formed in combustion processes in two ways:

- 1. The combination of elemental nitrogen with oxygen in the combustion air within the high temperature environment of the combustor (thermal NO_x); and
- 2. The oxidation of nitrogen contained in the fuel (fuel NO_x).

Natural gas contains negligible amounts of fuel-bound nitrogen, although some molecular nitrogen is present. Therefore, it is assumed that essentially all NO_x emissions from the turbines originate as thermal NO_x . The rate of formation of thermal NO_x is a function of residence time and free oxygen, and is exponential with peak flame temperature.

The combustion turbines will be subject to NO_x limits per NSPS Subpart KKKK, given that they were "modified" after the applicable date for Subpart KKKK, emissions must be at least as stringent as the NSPS. Part 5 displays the applicable Subpart KKKK limits for the combustion turbines.

Control of NO_x emissions from combustion turbines is generally aimed at either the prevention of NO_x formation, or the capture or oxidation of post-combustion NO_x . Since the rate of formation of thermal NO_x is a function of residence time and free oxygen, and is exponential with peak flame temperature, "front-end" control techniques are aimed at controlling one or more of these variables. These controls include the $XONON^{TM}$ system and dry low- NO_x burners. The $XONON^{TM}$ system uses a catalyst to keep the system temperatures lower while dry low- NO_x burners offer a staged combustion process, resulting in a lower peak flame temperature.

Other control methods utilize add-on control equipment to remove NO_x from the exhaust gas stream after its formation. The most common control techniques involve the injection of ammonia into the gas stream to reduce the NO_x to molecular nitrogen and water. Ammonia can either be injected into the system without the use of a catalyst (SNCR) or with the use of a catalyst (SCR). Finally, SCONO_xTM relies upon a catalyst similar to SCR to reduce NO_x emissions, but does so without injecting ammonia into the exhaust gas stream.

The output from the RBLC search provided in Appendix D (Table D-1 and Table D-2) shows that a variety of emission limits and control technologies have been applied to combustion turbines. The most stringent limits found during a review of EPA's database were for facilities located in ozone non-attainment areas. These facilities were required to meet such low emission limits since they were subject to LAER requirements.

Typical BACT determinations for simple-cycle units that are located in attainment areas were in the 2 to 27 ppm range using dry low NO_x combustors, water injection, SCR, or a combination of these technologies. The lower emission rates listed utilize SCR (Table D-1, Appendix D). It is important to note that all reported emission limits that are less than 9 ppm are either combined cycle units are LAER or are for aeroderivitive combustion turbines. Frame simple cycle combustion turbines similar to the 7FA combustion turbines show that the lowest BACT emission limitation is 9 ppm for natural gas operation. Fuel oil operation shows varied results from 6 ppm (for aeroderivitive, smaller combustion turbines) to 65 ppm (Table D-2, Appendix D).

6.1.2 Step 2. Identify Technically Feasible Control Technologies

6.1.2.1 XONON™ System

The XONONTM system controls NO_x emissions by preventing their formation. The key to the XONONTM system is the utilization of a chemical process versus a flame to combust fuel, thus limiting temperature and NO_x formation. The XONONTM system is an integral part of the combustor. The fuel and air that are supplied to the combustor are thoroughly mixed before entering the catalyst. The catalyst is responsible for combusting the fuel to release its energy. Due to the low catalyst operating temperatures, the nitrogen molecules are not involved in the reaction chemistry; they pass through the catalyst unchanged, thereby eliminating NO_x formation. The XONONTM system does have the same high outlet temperature, and some NO_x is formed in the post-combustion process. However, use of the technology has limited NO_x emissions to less than 2.5 ppm.

Currently, the XONONTM system has not had wide-scale application. It has been demonstrated on a 1.5 MW unit in California, with the unit operating in a base load capacity (24 hours a day, 7 days a week). Tests are underway to apply this technology to other types and sizes of turbines; however, testing data is currently unavailable. As the proposed combustion turbines are expected to experience repeated start-ups and shutdowns, it is unclear how the changing load conditions would affect the XONONTM system. As this is a large combined-cycle project, and the XONONTM system has yet to demonstrate applicability for such units, the XONONTM system has been deemed technically infeasible for this Project.

6.1.2.2 SCONO_x™ System

The SCONO_xTM system is an add-on control device that reduces multiple pollutants. The SCONO_xTM system utilizes a single catalyst for the conversion of CO, VOC, and NO_x emissions into carbon dioxide (CO₂), water, and nitrogen gas. The system does not use ammonia and operates most effectively at temperatures ranging from 300°F to 700°F. The SCONO_xTM system requires natural gas, water, steam, electricity and ambient air to operate, and no special chemicals or processes are necessary. Steam is used periodically to regenerate the catalyst bed and is an integral part of the process.

The exhaust gases of the Project's simple-cycle turbine will be around 1,000°F. Therefore, the gas stream temperature will be higher than the recommended temperature range for SCONO_x (300°F to 700°F) so it would need to be cooled prior to introduction to the catalyst. Additionally, plant steam would need to be diverted to the catalyst bed in order to regenerate it. These combustion turbines are not combined-cycle so no steam is available.

Since a simple-cycle turbine exhaust is greater than $1,000^{\circ}F$, SCONO_x is considered to be technically infeasible for the Project.

6.1.2.3 Selective Non-Catalytic Reduction (SNCR)

SNCR is a post-combustion NO_x control technology in which a reagent (ammonia or urea) is injected into the exhaust gases to react chemically with NO_x, forming nitrogen and water. The success of this process in reducing NO_x emissions is highly dependent on the ability to uniformly mix the reagent into the flue gas at a zone in the exhaust stream at which the flue gas temperature is within a narrow range, typically from 1,700°F to 2,000°F. To achieve the necessary mixing and reaction, the residence time of the flue gas within this temperature window should be at least 0.5 to 1.0 seconds. The consequences of operating outside the optimum temperature range are severe. Outside the upper end of the temperature range, the reagent will be converted to NO_x. Below the lower end of the temperature range, the reagent will not react with the NO_x and the ammonia slip concentrations (ammonia discharge from the stack) will be very high. The flue gases from the combustion turbine have an exhaust temperature of more than 1,000°F. Even strategically placing the ammonia injection further upstream would probably result only in peak temperatures of around 1,300°F. Such a low temperature would require that additional fuel be combusted at some point in order to raise the temperature to the levels that SNCR will operate. Combustion of the additional fuel would not only increase the NO_x emissions, but also all other criteria pollutants, especially CO. In addition, the added fuel used to raise the exhaust gas temperature will increase the annual operating costs for the facility.

SNCR has not been applied to any combustion turbines according to the RBLC database. **Because SNCR** has never been applied to combustion turbines, it is considered to be infeasible for the turbines under consideration for this Project.

6.1.2.4 Selective Catalytic Reduction (SCR)

SCR is a post-combustion technology that employs ammonia in the presence of a catalyst to convert NO_x to nitrogen and water. The function of the catalyst is to lower the activation energy of the NO_x decomposition reaction. Technical factors related to this technology include the catalyst reactor design, optimum operating temperature, sulfur content of the fuel, de-activation due to aging, ammonia slip emissions, and the design of the ammonia injection system.

SCR represents state-of-the-art controls for combined-cycle back end gas turbine NO_x removal; it has seen only limited use on simple-cycle combustion turbines (in areas subject to LAER and small aeroderivative turbines that are probably permitted for more fuel usage than the proposed GE 7FA units

for this Project) as determined from the RBLC query. SCR technology is being permitted as LAER and BACT for *combined-cycle* turbines at 2 to 5 ppm NO_x. Conventional SCR uses a metal honeycomb or "foil" catalyst support structure and requires an HRSG to drop flue gas temperatures to less than 600°F.

Because of the high exhaust temperature of a simple-cycle turbine, a conventional SCR system is not technically feasible. Instead, a high temperature "zeolite"-based SCR system has been introduced for use on certain simple-cycle turbines. Zeolite is a sodium alumina silicate ceramic material with a design operating temperature of approximately 800 to 1,000°F. Only a few natural gas-fired installations were identified that use these high-temperature systems. Two have had major problems such as catastrophic catalyst failures; the third has not yet acquired a long enough history to sufficiently evaluate its operational effectiveness. Although vendors reported that they have catalysts that they believe will operate under the high temperature conditions, they did not identify many combustion turbines successfully operating with SCR under simple-cycle conditions.

Another option to utilizing an SCR is to dilute the exhaust air to reduce the temperature prior to the SCR catalyst. This requires a lot of extra duct work to allow time for the exhaust to be lowered to the appropriate temperature for a vanadium catalyst.

Since these combustion turbines also combust fuel oil as backup fuel, when fuel oil is used, it has been shown that the catalyst will foul very fast, making the SCR not as efficient and very costly for much more frequent catalyst replacements.

Despite this past experience, SCR is deemed feasible for natural gas-fired units because vendors say that it is available, and it will be discussed further for this combustion turbine.

SCR can be applied to the combustion turbines and is technically feasible for the proposed simplecycle combustion turbines.

6.1.2.5 Dry Low NO_x Burners

Lean premixed combustors are currently available from most turbine manufacturers for natural gas operatoin. This technology seeks to reduce combustion temperatures, thereby reducing NO_x . In a conventional combustor, the air and fuel are introduced at an approximately stoichiometric ratio and air/fuel mixing occurs at the flame front where diffusion of fuel and air reaches the combustible limit. A lean premixed combustor design premixes the fuel and air prior to combustion. Premixing results in a homogenous air/fuel mixture, which minimizes localized fuel-rich pockets that produce elevated combustion temperatures and higher NO_x emissions. A lean air-to-fuel ratio approaching the lean flammability limit is maintained, and the excess air serves as a heat sink to lower combustion

temperatures, which lowers NO_x formation. A pilot flame is used to maintain combustion stability in this fuel-lean environment.

Controlled NO_x emission guarantees using dry low NO_x burners range from 9 to 25 ppm for turbines 20 MW or greater, but vary considerably from vendor to vendor. Low NO_x burners are currently available for these combined-cycle combustion turbines and are a technically feasible control option for the units.

6.1.2.6 Water or Steam Injection

Water and/or steam injection is a common control used during fuel oil operation. Steam and water injection works to increase the thermal mass by dilution and thereby reduce peak temperatures in the flame zone. With water injection, there is an additional benefit of absorbing the latent heat of vaporization from the flame zone. Water or steam is typically injected at a water-to-fuel ratio of less than one.

Water or steam injection is usually accompanied by an efficiency penalty (typically 2 to 3 percent) but an increase in power output (typically 5 to 6 percent) due to the increased mass flow required to maintain turbine inlet temperature at manufacturer's specifications. Both CO and VOC emissions are increased by water injection depending on the amount of water that is injected. Water injection is generally used for fuel oil combustion because it is difficult to aerosolize the fuel oil for air/fuel mixing, or is used on aeroderivative combustion turbines. Because the combustion turbines will have fuel oil as backup fuel, water injection is considered a technically feasible option for this Project.

6.1.2.7 Summary of the Technically Feasible Control Options

The technical feasibility of the NO_x control options for the simple-cycle combustion turbines is summarized in Table 6-2. The expected performance has been determined considering the performance of existing systems, vendor guarantees, permitted emission limits, and the design requirements for the turbines.

Table 6-2: Summary of Technically Feasible NO_x Control Technologies for Simple-Cycle Combustion Turbines

Control System ^a		Expected Performance (ppm) ^a	Technical Feasibility	Comments ^a
Combustion controls	Dry low-NO _x burners	9	Feasible	Standard on combustion turbines for natural gas operation
	Water injection	42	Feasible	Used only during fuel oil operation
	XONON TM N/A No		Not feasible	Testing is still underway. Only used on a 1.5 MW unit not operating continuously.
Post combustion controls	SCONO _x TM	N/A	Not feasible	Effective over a limited temperature range and would require plant steam resulting in additional emissions. There is no steam produced by the plant which is required for the SCONOx.
	Selective non- catalytic reduction	N/A	Not feasible	Exhaust temperature is too low.
	Selective catalytic reduction	2 – 5 (natural gas) 9 – 24 (fuel oil)	Feasible	2 ppm is the lowest achievable emission rate with SCR on natural gas. Catalyst will be fouled on fuel oil.

(a) ppm = parts per million; MW = Megawatts; SCR = selective catalytic reduction

6.1.3 Step 3. Rank the Technically Feasible Control Technologies

Add-on controls may be used for natural gas combustion in the turbines. The GE 7FA combustion turbines with the uprate offer 9 ppm NO_x which includes low NO_x burners and 42 ppm NO_x while combusting fuel oil; therefore, low NO_x burners and water injection are used as the baseline for the proposed combustion turbines.

The technically feasible NO_x control technologies for the combustion turbines are ranked by control effectiveness in Table 6-3.

Control Technology ^a	Reduction (%)	Controlled Emission Level (ppm) ^a
CCD	70 44	2 – 5 (natural gas)
SCR	78 – 44	9 – 24 (fuel oil)
Low NO _x burners	N/A (baseline for natural gas)	9
Water injection	N/A (baseline for fuel oil)	42

Table 6-3: Ranking of Technically Feasible NO_x Control Technologies for Combustion Turbines

6.1.4 Step 4. Evaluate the Most Effective Controls

Recent BACT determinations have indicated a level of 2 to 25 ppm for NO_x emissions from simple-cycle units that are fired with natural gas (Table D-1, Appendix D). The combustion turbines under consideration with the uprate are able to achieve 9 ppm while combusting natural gas and 42 ppm while combusting fuel oil on a long-term basis.

The simple-cycle units will have low NO_x burners and water injection, which are standard on the combustion turbines.

6.1.4.1.1 Economic Analyses

The simple-cycle turbine BACT analysis contains economic analyses for add-on controls. This section contains information regarding the economic analyses and how they were performed.

For the controls that require an economic analysis, capital costs include the initial cost of components intrinsic to the complete control system. For both oxidation catalyst and SCR systems, these capital costs would include the catalyst modules, transition piece, support frame, piping, provisions for catalyst cleaning and removal, instrumentation, and installation costs. Additionally, the SCR system requires the installation of an ammonia injection system. Annual costs consist of the financial efficiency losses, parasitic loads, and revenue loss from operation of the control system; overhead, maintenance, labor, raw materials, and utilities are included.

Capital and operating costs have been estimated in accordance with EPA guidance. The capital cost estimating technique used in this analysis is based on a factored method of determining direct and indirect installation costs. This technique is a modified version of the "Lang Method," where installation costs are expressed as a function of known equipment costs. This method is consistent with the latest EPA

⁽a) ppm = parts per million; SCR = Selective Catalytic Reduction

guidance manual (Office of Air Quality Planning and Standards [OAQPS] Control Cost Manual) on estimating control technology costs (EPA 2002).

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Purchased equipment costs represent the delivered cost of the control equipment, auxiliary equipment, and instrumentation. Auxiliary equipment consists of all structural, mechanical, and electrical components required for continuous operation of the device. Depending on the control strategy that is used, these costs may include such items as reagent storage tanks, supply piping, the engine outlet transition piece, a catalyst removal crane, spare parts, and the catalyst and air dilution system. In this BACT evaluation, basic equipment costs were obtained from data provided by vendors and from recent projects with similar units. Instrumentation is usually not included in the basic equipment cost so the OAQPS manual allows that instrumentation may be estimated to be 10 percent of the basic equipment cost.

Direct installation costs consist of the direct expenditures for materials and labor including site preparation, foundations, structural steel, insulation, erection, piping, electrical, painting, and enclosure structures. Indirect installation costs include engineering and supervision of contractors, construction and field expenses, construction fees, contingencies, and additional permits and licensing costs.

Direct installation costs are expressed as a function of the purchased equipment cost and are based on the average installation requirements of typical systems. Indirect installation costs are designated as a percentage of the total direct cost (purchased equipment cost plus the direct installation cost) of the system. Other indirect costs include equipment start-up and performance testing, contingency funds, working capital and interest during construction.

Annualized costs are comprised of direct and indirect operation costs. Direct costs include electricity losses, labor, maintenance, replacement parts, raw materials, and utilities. Indirect operating costs include overhead, taxes, insurance, general administration, contingencies, and capital charges. Annualized cost factors used to estimate total annualized costs for the SCR and oxidation catalyst systems are presented in their respective discussions in the sections that follow. These tables are consistent with the EPA guidance on estimating control technology costs (EPA 2002).

Direct operating labor costs vary according to the system operating mode and operating time. Labor supervision is estimated as 15 percent of operating labor. Maintenance costs have been included and are itemized as appropriate. Replacement part costs, such as the cost to replace an aged or failed catalyst, have been included where appropriate. Reagent and utility costs are based upon estimated annual consumption. Based on the experience of other facilities, the catalyst is assumed to require replacement at a minimum of every three years due to failure or aging.

Most indirect operating costs are calculated as a percentage of the total capital cost. The indirect capital costs are based on the capital recovery factor (CRF), defined as:

$$CRF = \frac{i \cdot (1+i)^n}{(1+i)^n - 1}$$

Where:

i = interest rate

n = equipment economic life (years)

A control system's economic life is typically 10 to 20 years. In this analysis, a 20-year equipment economic life (typical length of financing) was used. The average interest rate is assumed to be seven percent. The CRF is calculated to be 0.094.

The cost-effectiveness for each system is calculated by dividing the annualized cost of the available control technology by the annual emissions reduction. The annual emissions reduction is the difference between the baseline emission rate and the controlled emission. All BACT capital and annual cost tables are contained in Appendix E.

6.1.4.1.2 Selective Catalytic Reduction

Energy Impacts

An SCR system results in a loss of energy due to the pressure drop across the SCR catalyst. To compensate for the energy loss in the SCR system, additional natural gas combustion is required to maintain the net energy output, which also results in additional air pollutant emissions.

Environmental Impacts

SCR systems consist of an ammonia injection system and a catalytic reactor. Urea can be decomposed in an external reactor to form ammonia for use in a SCR. Unreacted ammonia may escape through to the exhaust gas. This is commonly called "ammonia slip." It is estimated that ammonia slip from an SCR on a unit this size could be 10 ppm and may be considered to be an environmental impact. The ammonia that is released may also react with other pollutants in the exhaust stream to create fine particulates in the form of ammonium salts. In addition, the storing of the ammonia on-site is another environmental and safety concern. SCR catalysts must also be replaced on a routine basis. In some cases, these catalysts may be classified as a hazardous waste. This typically requires either returning the material to the manufacturer for recycling and reuse or disposal in designated landfills.

Burns & McDonnell

Economic Impacts

The costs associated with an SCR system for the combustion turbines operating in simple-cycle mode are shown in Table E-1, Appendix E. The costs used in this analysis is for a brand-new combustion turbine and does not take into account the fact that this would be a retrofit to existing combustion turbines. The costs would go up quite a bit if the retrofit costs were included. To be conservative, however the costs only look at the installation as a new facility. The overall total capital investment of installing an SCR system is approximately \$19,015,000. The annualized costs associated with an SCR system are shown in Table E-2, Appendix E. On an annual basis, the SCR system would cost \$2,899,000, which results in a cost per ton of NO_x removed of \$23,980 while removing only 168 tons of NO_x per year, including full permitted operation normal operation on natural gas and fuel oil. Therefore, any control of NO_x by add-on controls would result in costs that would not be economical.

An SCR is not proposed as BACT for the combustion turbine operating in simple-cycle mode because it is not economically feasible.

6.1.4.1.3 Low-NO_x Burners

Energy Impacts

Low NO_x burners are usually accompanied by an efficiency penalty (typically 2 to 3 percent) and an increase in power output (typically 5 to 6 percent). The increase in power output results from the increase in mass flow required to maintain turbine inlet temperature at manufacturer's specifications. Because there is a power increase, no energy impacts are associated with low NO_x burners.

Environmental Impacts

The low NO_x burner system may increase CO and VOC emissions on a lb/hr basis; however, the potential increase in CO and VOC emissions does not outweigh the advantages of decreased NO_x emissions to reduce health effects.

Economic Impacts

The turbine manufacturer currently installs low-NO_x burners as standard equipment on natural gas-fired combustion turbines. With the low-NO_x burners, these turbines may achieve NO_x emission rates of 9 ppm for loads of 60 percent or greater. Since the low-NO_x burners are considered standard equipment on the turbine, there is no annualized cost of the control.

Burns & McDonnell

6.1.4.1.4 Water Injection

Energy Impacts

Water injection, used during fuel oil operation only, is also usually accompanied by an efficiency penalty (typically 2 to 3 percent) and an increase in power output (typically 5 to 6 percent). No huge energy impacts are associated with water injection.

Environmental Impacts

Water injection does use water, a natural resource, to control NO_x emissions. However, at the very few operating hours that are requested in this permit (approximately 260 hours per year per turbine), the water use should be very minimal.

Economic Impacts

The turbine manufacturer currently installs water injection as standard equipment on fuel oil-firing combustion turbines. With water injection, these turbines may achieve NO_x emission rates of 42 ppm for loads of 60 percent or greater when combusting fuel oil. Since the water injection is considered standard equipment on the turbine, there is no annualized cost of the control.

6.1.4.2 Step 5. Proposed NO_x BACT Determination

The BACT recommended for control of NO_x emissions from each of the simple-cycle turbines is low NO_x burners for natural gas combustion and water injection for fuel oil operation. This control will meet a NO_x emission limit of 9 ppm at 15 percent oxygen during steady state conditions on a 30-day rolling average for natural gas operation and 42 ppm at 15 percent oxygen for fuel oil operation.

Low NO_x burners are selected as BACT for NO_x emissions from the simple-cycle combustion turbines while combusting natural gas.

Water injection is selected as BACT for NO_x emissions from the simple-cycle combustion turbines while combusting fuel oil.

6.2 BACT for Carbon Monoxide (CO) – Combustion Turbines

6.2.1 Step 1. Identify Potential Control Strategies

CO is a product resulting from incomplete combustion. Control of CO is typically accomplished by providing adequate fuel residence time and a high temperature in the combustion zone to confirm complete combustion. These control factors, however, also tend to result in increased emissions of NO_x . Conversely, a lower NO_x emission rate achieved through flame temperature control (by water injection or

dry lean pre-mix) can result in higher levels of CO emissions. A compromise is usually established where the flame temperature reduction is set to achieve the lowest NO_x emission rate possible while keeping CO emissions to an acceptable level.

CO emissions from combustion turbines are a function of oxygen availability (excess air), flame temperature, residence time at flame temperature, combustion zone design, and turbulence. Post-combustion control involves the use of catalytic oxidation; front-end control involves controlling the combustion process to suppress CO formation.

The technologies identified for reducing CO emissions from the proposed turbines are the SCONO_xTM system, an oxidation catalyst, and combustion controls. The standard technology for reducing CO emissions is to maintain "good combustion" through proper control and monitoring of the combustion process. A survey of the RBLC database (Table D-3 and Table D-4, Appendix D) indicated that most new simple-cycle combustion turbines in attainment areas do not have add-on controls for CO emissions. CO emissions from simple-cycle turbines from the permitted facilities ranged from 2 to 25 ppm for natural gas operation. It should be noted that the 2 ppm BACT rates were for combustion turbines in nonattainment areas and were likely not F-class machines, but were smaller aeroderivitives that have much lower exhaust temperatures.

6.2.2 Step 2. Identify Technically Feasible Control Technologies

6.2.2.1 SCONO_{x™} System

The SCONO_xTM system was described in the BACT analysis for NO_x in Section 6.2.2.2. Because its operating temperature is much lower than the exhaust of the simple-cycle combustion turbines, as stated in Section 6.2.2.2, SCONO_x is not feasible on the simple-cycle combustion turbines.

The SCONO_xTM system is considered to be not technically feasible for the combustion turbines.

6.2.2.2 Oxidation Catalyst

Oxidation catalysts are a post-combustion technology which does not rely on the introduction of additional chemicals, such as ammonia with SCR, for a reaction to occur. The oxidation of CO to CO₂ utilizes excess air present in the turbine exhaust; the activation energy required for the reaction to proceed is lowered in the presence of a catalyst. Products of combustion are introduced into a catalytic bed, with the optimum temperature range for these systems being between 700°F and 1,100°F. At higher temperatures, catalyst sintering may occur, potentially causing permanent damage to the catalyst. The addition of a catalyst bed onto the turbine exhaust will create a pressure drop, resulting in back pressure to

the turbine. This has the effect of reducing the efficiency of the turbine and the power generating capabilities.

The use of an oxidation catalyst is considered to be technically feasible for the combustion turbines.

6.2.2.3 Combustion Control

"Good combustion practices" include operational and combustor design elements to control the amount and distribution of excess air in the flue gas to confirm that there is enough oxygen present for complete combustion. Such control practices applied to the proposed turbines can achieve CO emission levels of 9 ppm at for natural gas operation from 60 to 100 percent load and 20 ppm from 60 to 100 percent load for fuel oil operation.

Good combustion practices are a technically feasible method of controlling CO emissions from the proposed combustion turbines.

6.2.2.4 Summary of the Technically Feasible Control Options

The technical feasibility of the CO control options for the proposed combined-cycle combustion turbines is summarized in Table 6-4. The expected performance has been determined considering the performance of existing systems, vendor guarantees, permitted emission limits, and the design requirements for the turbines.

Table 6-4: Summary of Technically Feasible CO Control Technologies for the Combustion Turbines

Control System		Expected Performance (ppm) ^{a,b}	Feasibility	Comments
Combust	tion control	9 (natural gas) 20 (fuel oil)	Feasible	Standard on turbines. Not an add-on control
Post combustion controls	$SCONO_x^{TM}$	N/A	Not feasible	Effective over a limited temperature range and would require plant steam resulting in additional emissions, produces CO ₂ emissions. There is no plant steam at this facility.
	Oxidation catalyst	2 (natural gas) 4.4 (fuel oil)	Feasible	Produces CO ₂ emissions

⁽a) ppm = parts per million

⁽b) Over all loads of 60% and greater.

6.2.3 Step 3. Rank the Technically Feasible Control Technologies

The technically feasible CO control technologies for the combustion turbines are ranked by control effectiveness in Table 6-5.

Table 6-5: Ranking of Technically Feasible CO Control Technologies for Combustion Turbines

Control Technology	Reduction (%) ^b	Controlled Emission Level (ppm) ^{a,b}
Oxidation catalyst	77	2 (natural gas) 4.4 (fuel oil)
Combustion control	N/A (baseline)	9 (natural gas) 20 (fuel oil)

⁽a) ppm = parts per million

6.2.4 Step 4. Evaluate the Most Effective Control Technologies

Operating the combustion turbines with good combustion practices will achieve 9 ppm on a long-term basis for natural gas firing and 20 ppm for fuel oil firing. The next step is to review each of the technically feasible control options for environmental, energy, and economic impacts.

6.2.4.1 Oxidation Catalyst

Energy Impacts

The addition of a catalyst bed onto the turbine exhaust for the oxidation catalyst will create a pressure drop, resulting in back pressure to the turbine. This has the effect of reducing the efficiency of the turbine and the power generating capabilities.

Environmental Impacts

The oxidation catalyst oxidizes CO to CO₂ which is released to the atmosphere. CO₂ is a greenhouse gas (GHG) that may be contributing to global warming and is now a regulated pollutant. Increasing CO₂ emissions could have a negative impact on the atmosphere. The amount of CO₂ produced is minimal, given the magnitude of GHG emissions that trigger permitting (75,000 tpy once another pollutant is subject to PSD) as compared to the amount of CO that triggers permitting (100 tpy); therefore, a slight increase in CO₂ is considered negligible compared to the decrease in CO emissions that is attained.

As with all controls that utilize catalysts for removal of pollutants, the catalyst must be disposed of after it is spent. The catalyst may be considered hazardous waste and require special treatment or disposal; even if it is not hazardous, it adds to the already full landfills. Further, the catalyst will be spent and fouled faster when fuel oil is combusted, as it is known that the fuel oil causes fouling of the catalyst.

⁽b) Over all loads of 60% and greater.

Economic Impacts

The capital costs associated with an oxidation catalyst for the combustion turbine operating in simple-cycle mode are shown in Table E-3, Appendix E. The total capital investment of installing an oxidation catalyst on the simple-cycle turbine is approximately \$8,568,400. The annualized costs associated with an oxidation catalyst are shown in Table E-4, Appendix E. On an annual basis, the oxidation catalyst would cost \$1,219,400 which results in a cost per ton of CO removed of \$18,154 while removing only 67 tons of CO per year for both natural gas operation and fuel oil operation, based on worst-case normal operation emissions. Therefore, any control of CO by add-on controls would result in costs that would not be economical.

An oxidation catalyst is not proposed as BACT for the combustion turbines because it is not economically feasible.

6.2.5 Step 5. Proposed CO BACT Determination

The BACT recommended for control of CO emissions from each of the combustion turbines is good combustion practices. These practices will meet a CO emission limit of 9 ppm at 15 percent oxygen at loads of 60 percent and greater for natural gas operation and 20 ppm at 15 percent load for loads of 60 percent and greater for fuel oil operation on 30-day rolling averages.

6.3 BACT for Particulate Matter (PM/PM₁₀/PM_{2.5}) – Combustion Turbines

6.3.1 Step 1. Identify Potential Control Strategies

Particulate (PM/PM₁₀/PM_{2.5}) emissions from natural gas combustion sources consist of inert contaminants in natural gas, of sulfates from fuel sulfur or mercaptans used as odorants, of dust drawn in from the ambient air, and of particulate of carbon and hydrocarbons resulting from incomplete combustion. Therefore, units firing fuels with low ash content and high combustion efficiency exhibit correspondingly low particulate emissions.

Post-combustion controls, such as electrostatic precipitators (ESPs) or baghouses, have never been applied to commercial gas- and oil-fired turbines. Available control strategies include the use of low ash fuel, such as natural gas and low sulfur fuel oil, and combustion controls. BACT emission rates vary in the RBLC database with rates being listed as 0.0045 to 0.017 pounds per million British thermal units (lb/MMBtu) and 2.1 to 34.9 lb/hr for natural gas-fired combustion turbines (Table D-5, Appendix D) and between 13.7 to 19.5 lb/hr for fuel oil operation (Table D-6, Appendix D). As stated previously, these emission rates vary due to many reasons.

The combustion turbines at the Pleasants Energy facility are General Electric 7FA.03 combustion turbines. These turbines were constructed around approximately 2001. Most of the combustion turbines in the RBLC database that have gone through PSD recently are much newer versions (2014-2017) of the same combustion turbine with updated equipment that can achieve lower PM/PM₁₀/PM_{2.5} emission rates and vendors can guarantee lower emission rates.

6.3.2 Step 2. Identify Technically Feasible Control Technologies

Particulate control devices are not typically installed on gas turbines. Post-combustion controls, such as ESPs or bag houses, have never been applied to commercial gas-fired turbines. For all natural gas-fired combustion units, particulate matter emissions are inherently low and add-on controls are not able to control these already low emissions much further. Therefore, the use of ESPs and bag house filters are both considered technically infeasible, and do not represent an available control technology. Further, to assist with reducing the emissions that are emitted out the stack, the inlet air, which is used during combustion of the fuel, is filtered prior to combustion and ultimately exhausted out the stack. This will further reduce the PM emissions from the outside air that is emitted out the stack.

In the absence of add-on controls, the most effective control method demonstrated for gas turbines is the use of low ash fuel, such as natural gas and low sulfur fuel oil, filtering the inlet air, and combustion controls. This was confirmed by a survey of the RBLC database (Table D-5 and Table D-6, Appendix D) which showed no add-on PM/PM₁₀/PM_{2.5} control technologies for simple-cycle combustion turbines. Proper combustion control and the firing of fuels with negligible or zero ash content (such as natural gas) is the predominant control method listed.

As mentioned earlier, the only way to potentially reduce PM/PM₁₀/PM_{2.5} emissions further from this GE 7FA.03 simple-cycle combustion turbine would be to replace the combustion turbine with a brand-new updated version of the same combustion turbine.

6.3.3 Step 3. Rank the Technically Feasible Control Technologies

The technically feasible PM/PM₁₀/PM_{2.5} control technologies for the combustion turbines are ranked by control effectiveness in Table 6-6.

Table 6-6: Ranking of Technically Feasible PM/PM₁₀/PM_{2.5} Control Technologies for Combustion Turbines

Control Technology	Reduction (%)	Controlled Emission Level ^a
Low ash and low sulfur fuel, inlet air filtration and combustion control	N/A (baseline)	15.9 lb/hr (natural gas) 41.0 lb/hr (fuel oil)
Replace combustion turbine with brand new GE 7FA.05 combustion turbine	53% (natural gas) 20% (fuel oil)	7.0 lb/hr (natural gas) 39 lb/hr (fuel oil)

⁽a) For all loads of 60% and greater.

6.3.4 Step 4. Evaluate the Most Effective Control Technologies

Energy, Environmental, and Economic Impacts

There are no energy, environmental, or economic impacts associated with combustion controls and filtering the inlet air; the use of low ash fuel is not an add-on control device.

Replacing the existing combustion turbines with a brand-new GE 7FA.05 combustion turbine would have energy, environmental and economic impacts.

Energy Impacts from Replacing the Combustion Turbine

Replacing the combustion turbine with a new combustion turbine could mean that electricity would not be produced by Pleasants Energy during the demolition and construction period, even if the combustion turbines were replaced in phases. The electricity available to the grid would be reduced significantly during the construction phase of the combustion turbine replacements. This could have a large impact on the surrounding area; it could mean brown outs and blackouts in periods of very high peak demand, especially given the fact that many of the coal plants in the area are shutting down due to environmental regulations and etc.

Environmental Impacts from Replacing the Combustion Turbine

Demolition of the existing combustion turbine will cause the production of waste, some of which may be recycled or reused in some fashion. This is an impact that would not occur if the combustion turbines were not replaced, therefore this is an environmental impact.

Economic Impacts from Replacing the Combustion Turbine

The capital costs associated with purchasing and installing a brand new 7FA.05 combustion turbine are shown in Table E-5, (Appendix E). This cost does not include the cost to demolish the existing combustion turbines, nor does it include costs lost in revenue while the demolition and construction are taking place. The total capital investment of installing a new 7FA.05 combustion turbine is approximately

⁽b) lb/hr = pounds per hour

\$73,609,000. The annualized costs associated with a brand new 7FA.05 combustion turbine are found in Table E-6, Appendix E. On an annual basis, the new combustion turbine would cost approximately \$5,932,000 which results in a cost per ton of PM/PM₁₀/PM_{2.5} removed of almost \$328,700 while reducing particulate emissions by only 18.3 tons of per year for both natural gas operation and fuel oil operation, based on worst-case normal operation emissions. Therefore, any type of reduction in PM emissions would result in costs that would not be economical.

6.3.5 Step 5. Proposed PM/PM₁₀/PM_{2.5} BACT Determination

The use of low ash and low sulfur fuels, inlet air filtration, and good combustion control represents BACT for PM/PM₁₀/PM_{2.5} control for the combustion turbines. These operational controls will limit PM/PM₁₀/PM_{2.5} emissions to approximately 15.9 lb/hr and 41.0 lb/hr for natural gas operation and fuel oil operation, respectively, on a 3-run stack test basis. This limit includes front and back half PM/PM₁₀/PM_{2.5} emissions in the combustion turbines.

6.4 BACT for Greenhouse Gases (GHG) – Combustion Turbines

6.4.1 Step 1. Identify All Potential Control Strategies

For this unit, the CO₂e emissions are due to carbon dioxide (CO₂), methane (CH₄), and nitrous oxides (N₂O) emissions. Global warming potentials (GWP) of methane and nitrous oxide emissions are normalized to the warming potential of carbon dioxide (as CO₂e) by multiplying the methane emissions by 25 and the nitrous oxide emissions by 298. Despite the higher warming potentials of methane and nitrous oxides compared to carbon dioxide, it is expected that carbon dioxide emissions will still account for over 99 percent of the CO₂e GWP for this unit, based on published emission factors for natural gasfired turbines.

There are two broad strategies for reducing CO₂ emissions from stationary combustion processes such as combustion turbines. The first is to minimize the production of CO₂ through the use of low-carbon fuels and through aggressively energy-efficient design. The use of gaseous fuels, such as natural gas, reduces the production of CO₂ during the combustion process relative to burning solid fuels (e.g., coal or coke) and liquid fuels (e.g., distillate or residual oils). Additionally, a highly efficient operation requires less fuel for process heat, which directly impacts the amount of CO₂ produced. Establishing an aggressive basis for energy recovery and facility efficiency will reduce CO₂ production and the costs to recover it.

The second strategy for CO₂ emission reduction is carbon capture and sequestration (CCS). The inherent design of the combustion turbines produces a dilute CO₂ stream for potential capture.

The CO₂ emissions from the combustion turbines can theoretically be captured through pre-combustion methods or through post-combustion methods. In the pre-combustion approach, oxygen instead of air is used to combust the fuel and a concentrated CO₂ exhaust gas is generated. This approach significantly reduces the capital and energy cost of removing CO₂ from conventional combustion processes using air as an oxygen source, but it incurs significant capital and energy costs associated with separating oxygen from the air.

Post-combustion methods are applied to conventional combustion techniques using air and carbon-containing fuels in order to isolate CO₂ from the combustion exhaust gases. Because the air used for combustion contains nearly 60 percent nitrogen, the CO₂ concentration in the exhaust gases is only 5 to 20 percent depending on the amount of excess air and the carbon content of the fuel.

6.4.2 Step 2. Identify Technically Feasible Control Technologies

6.4.2.1 Fuel Selection

6.4.2.1.1 Low-Carbon Fuels

Numerous fuels are available for use. As Table 6-7 shows, combustion of natural gas yields 40 to 50 percent less CO₂ than does combustion of coal and petroleum coke and approximately 30 percent less CO₂ than does combustion of residual oil. Accordingly, the preferential burning of a low-carbon gaseous fuel in the turbines is an extremely effective CO₂ control technique. This control technique is **technically feasible** for the combustion turbines and is an inherent part of the facility's design.

Table 6-7: CO₂ Emission Factors

Fuel	Pounds CO ₂ per MMBtu ^a
Petroleum coke	225
Coal	210
Residual oil	174
Distillate oil	161
Natural gas	117

Source: Energy Information Administration at http://www.eia.doe.gov/oiaf/1605/coefficients.html

(a) MMBtu = million British thermal units

6.4.2.1.2 Combustion of Biogenic Sources

The combustion turbines have not been designed to accommodate fibrous biomass, such as corn stover, which is the most likely biomass available in sufficient quantities for the unit from the surrounding area. For both regulatory and technical feasibility issues, therefore, **biogenic sources are not a feasible option**.

6.4.2.2 Energy Efficiency

6.4.2.2.1 Selection of Efficient Turbine Design

This option reduces carbon dioxide emissions by ensuring that the plant is as efficient as possible, thereby reducing the amount of fuel burned per megawatt-hr produced. The uprate to the combustion turbine should actually increase efficiency for certain operational scenarios.

- Combustion control optimization and energy efficient equipment The combustion turbines and their design is highly efficient. This is technically and economically feasible. Potential options that may increase efficiency include the following:
 - o Fast ramp-up/ramp-down
 - o High starting reliability
 - o 18-stage high-efficiency, axial flow compressor with variable inlet guide vanes
 - o Fuel gas heating (to a maximum of 75°F) to improve turbine efficiency
 - o Dry low-NO_x burners
 - Inlet air filtration utilizing high efficiency cartridge filters to clean combustion air and remove contaminants
 - On and off-line compressor water wash system to remove deposits and other contaminants from compressor blades to maintain efficient operation

6.4.2.3 Add-on Control Devices

6.4.2.3.1 Catalytic Oxidation

Nitrous oxide emissions are reduced by passing the combustion gases over a catalyst, converting to nitrogen plus oxygen. Similarly, VOC emissions, such as methane, may be converted from CH₄ to CO₂ plus water. For the same reasons given above in the discussion for CO BACT controls, **catalytic** oxidation is technically feasible for this unit.

6.4.2.3.2 Thermal Oxidation

There are several types of thermal oxidation technology. All of these technologies oxidize methane (CH₄) to carbon dioxide and water, by raising the temperature of the gas stream being treated to approximately 1,600°F for approximately one to two seconds. Given sufficient mixing, this residence time and temperature is capable of achieving at least a 98 percent reduction in methane emissions for these processes. Secondary pollutants are produced by thermal oxidation. These include NO_x and CO from the combustion of natural gas used to heat the process stream. Thermal oxidation technologies also may employ some form of heat recovery, either recuperative or regenerative, to reduce economic, environmental and energy costs. In the case of a turbine, it is expected that approximately 3.5 lb/hr of methane will be produced at full load (with an exhaust flow rate of approximately 2.2 million actual cubic feet per minute). The exhaust gas stream is thus both high volume and low in methane concentration, so would need to be concentrated to the point that the methane would be capable of combustion. Also, additional CO₂ would be produced due to the need for combusting natural gas to heat the methane to the oxidation point, so the overall effectiveness in reducing CO₂e emissions due to methane by oxidizing them to carbon dioxide would be much less due to the additional carbon dioxide produced in order to combust the methane in the first place. Therefore, thermal oxidation is technically infeasible for this unit.

6.4.2.4 Carbon Dioxide Capture and Sequestration (CCS)

This is a general term which is used for approaches that capture and separate CO₂ from an exhaust stream, and then store it in a place which will keep it from the atmosphere for a long time. The three general categories of carbon dioxide capture are pre-combustion CO₂ capture, oxygen-combustion, and post-combustion CO₂ capture.

6.4.2.4.1 Pre-combustion CO₂ Capture

Pre-combustion CO₂ capture is used in gasification plants, where the CO₂ is captured from the syngas prior to combustion in the turbine, where it is relatively concentrated in the gas stream. This facility is not a gasification plant; therefore, **pre-combustion capture is not technically feasible**.

6.4.2.4.2 Post-combustion CO₂ Capture

Post-combustion CO₂ capture is used for units such as pulverized coal plants. In these units, the flue gas concentration of CO₂ runs between 10-15 percent by volume, and is released at atmospheric pressure. This results in a high actual volume of gas to be treated, while trace impurities in the airflow tend to reduce the effectiveness of the CO₂ adsorbing process, and compressing the captured CO₂ from atmospheric pressure to pipeline pressure represents a large parasitic load. The currently available process

is costly and energy intensive, so research is being done on ways to increase the solvent capture efficiency and reduce the cost. These approaches include investigating the use of alternative solvents, solid sorbents, or membranes. Of these potentially more efficient approaches, most are currently at laboratory/bench scale, and are not technically feasible. Pilot scale processes are starting to be placed in service, such as a 48 MW slipstream project at Brindisi, Italy, started in March 2011, which is limited to capturing less than 10,000 tons of CO₂ per year. Another pilot program was completed at Mountaineer Power Plant near New Haven, West Virginia. Actual large-scale CCS project phases were planned for this site, however the projects were cancelled. In addition, the DOE-supported FutureGen project was also cancelled. No commercially available post-combustion CO₂ capture systems are known to have been installed at a large power plant as other than pilot-scale demonstration projects. Even though there have been no projects of this size that have successfully employed this technology, the EPA has stated in their document "PSD and Title V Permitting Guidance for Greenhouse Gases" (March 2011) that "for the purposes of a BACT analysis for GHGs, EPA classifies CCS as an add-on pollution control technology that is "available" for facilities emitting CO₂ in large amounts, including fossil fuel-fired power plants, and for industrial facilities with high-purity CO₂ streams." Because these combustion turbines will be used for peaking purposes, and will ramp up and down to follow the load, they are not considered to have a pure, constant CO₂ stream. For the purposes of this BACT analysis, post-combustion capture is considered not technically feasible for the simple-cycle combustion turbines.

6.4.2.4.3 CO₂ Sequestration

CO₂ sequestration involves transporting CO₂ to a suitable geologic location where it can be injected as a supercritical fluid into deep, underground rock formations for permanent storage. Identifying a suitable site within an economically-viable distance will require site-specific quantitative risk assessment. Four trapping methods are known: mineral trapping, physical adsorption, hydrodynamic trapping, and solubility trapping.

1. Mineral Trapping

In this method, the CO₂ is trapped by undergoing a chemical reaction with various minerals, resulting in the formation of a carbonate mineral. This process can be rapid or very slow, depending on the chemistry of the rock and water at the site. Mineral trapping is expected to result in the most stable, permanent form of geological CO₂ sequestration. Experiments have shown that basalt formations can rapidly transform injected CO₂ into carbonate minerals, beginning precipitation in a few months' time and projected complete conversion within 100 years or less, depending on depth of injection. Sandstone formations low in carbonates may also be suitable candidates, depending on the mineral contents of the formations. These methods have been demonstrated only on a laboratory scale, so are **not technically feasible**.

2. Physical Adsorption

In this case, CO₂ molecules are trapped in micropore wall surfaces of coal organic matter or organic rich shales. The hydrostatic pressure in the formation controls the adsorption process. The injection of CO₂ can also result in driving off methane for collection by other wells, helping the economics. West Virginia has multiple coal beds throughout the State. Coal beds have historically not produced much methane. Some coal beds in the U.S. are being tested for CO₂ storage/methane recovery, but this is currently at a pilot phase. Use of coal beds in West Virginia would require much further study to locate a suitable site for sequestration and are currently **not technically feasible.**

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3. Hydrodynamic Trapping

In the case of hydrodynamic trapping, the pore space of an aquifer takes the injected carbon dioxide, and the aquifer is capped by an impermeable rock layer to trap the CO₂ well below the near-surface environment. For storage purposes, the aquifer should be saline enough to be non-potable, and deep enough (over 2,700 feet) to confirm that the pressure is sufficient to keep the compressed CO₂ in a supercritical or liquid phase. As the state of West Virginia is unlikely to apply for primacy for the Class VI regulations (governing injection wells), EPA rules for a minimum of 10,000 milligrams per liter total dissolved solids (TDS) to qualify as saline enough to be suitable for injection will probably apply. Discovering locations which exceed 10,000 milligrams per liter would require more exploration and test wells to characterize the site and determine the aquifer suitability. A pilot scale injection study took place near Shadyside, Ohio but due the geologic complexities within the western Appalachian Basin, the injection rates were reported to be much lower than expected and required higher injection pressures. Due to the cost of exploration and the difficulty in finding a suitable injection site, hydrodynamic trapping is **not technically feasible** at this time.

4. Solubility Trapping

In this case, the CO₂ dissolves in the water or forms carbonic acid, becoming slightly heavier and sinking to the bottom of the aquifer. Solubility trapping also occurs during CO₂ flooding for enhanced oil recovery (EOR). In this case, the CO₂ dissolves into the oil, and is trapped by the immobile, non-recoverable oil. CO₂ flooding has been used for years for EOR, resulting in some existing injection infrastructure at oilfields, although the sequestration effects were not originally monitored. However, oil fields have stored crude oil and natural gas for millions of years, and the geologic conditions that trap oil and gas are also the conditions suitable for CO₂ storage. If the CO₂ is used for EOR, the cost of transporting it to the oilfield may be partially offset. The nearest oilfield using EOR appears to be the Appalachian Basin, located very close to the site, within 50 miles, although the existing infrastructure is

at capacity as far as ability to inject CO₂. Therefore, solubility trapping is **not technically feasible** at this time.

6.4.2.4.4 Summary of CO₂ Sequestration

To summarize, existing CO₂ capture technologies have not been applied at large power plants, as the energetic costs are prohibitive, and while more efficient approaches are being investigated, none have currently been developed past the pilot-stage. Even though post-combustion technology for CO₂ capture has not been demonstrated on a simple-cycle combustion turbine, the EPA has stated that it is considered technologically feasible. This Project will not have a pure CO₂ stream as it is a peaking plant and will ramp up and down and start-up and shutdown daily when it operates. However, a published cost estimate for a 235-MW slipstream pilot project in West Virginia is \$668 million, so scaling that linearly to a size capable of handling the approximate 300 net MW capacity of this Project would be over \$852 million. Potential carbon sequestration sites in West Virginia may exist, but the technologies to use them are mostly still in the pilot-scale phase of development, and Pleasants Energy would need to do much more investigation in order to discover where the sites are, if any, and characterize them enough to demonstrate the long-term viability of the locations. When looking at cost to construct a pipeline that may not need to be more than 50 miles, as determined from another power project (IPL Ottumwa Generating Station –in Iowa) using an average cost of approximately \$1.4 million/mile of pipeline this cost is over \$70 million. The capital costs would also need to include costs for gas compression, additional injection and monitoring wells necessary to handle the volume of CO2 produced, pipeline right-of-way, operation and maintenance costs, etc.

The facts are that the qualitative cost estimate of capture and sequestration is quite high, the technological effectiveness for the capture equipment for a unit of this size has not been demonstrated in practice yet, and there is uncertainty as to whether locations capable of storing the large amounts of CO₂ that would be produced per year exist within a closer radius of the plant, and the fact that the Pleasants Energy facility does not have a pure CO₂ stream **are sufficient to eliminate this option without requiring a more detailed site-specific technological or economic analysis.**

6.4.2.5 Summary of Technically Feasible Control Technologies

The technical feasibility of the GHG control options for the combustion turbines is summarized in Table 6-8. The expected performance has been determined considering the performance of existing systems, vendor guarantees, permitted emission limits, and the design requirements for the combustion turbines.

Table 6-8: Summary of Technically Feasible GHG Control Technologies for Combustion Turbines

Control System		Technical Feasibility	Comments
Fuel selection	Low carbon fuels	Feasible	Natural gas has been selected as the fuel for this Project
	Combustion of biogenic sources	Not feasible	
Energy efficiency	Efficient turbine design	Feasible	Standard for the turbines under consideration
Post combustion	Catalytic oxidation	Not feasible	Will reduce methane emissions but create more carbon dioxide
controls	Thermal oxidation	Not feasible	
	Pre-combustion CO ₂ capture	Not feasible	
Carbon capture	Post-combustion CO ₂ capture	Not feasible	Never demonstrated on combustion turbines and costs for a coal plant are not economically feasible
	Mineral trapping	Not feasible	
Carbon	Physical adsorption	Not feasible	
sequestration	Hydrodynamic trapping	Not feasible	
	Solubility trapping	Not feasible	

6.4.3 Step 3. Rank the Technically Feasible Control Technologies

The technically feasible control technologies are natural gas with distillate fuel oil as backup fuel, and efficient turbine design. The use of low-carbon fuels and aggressively energy-efficient design to reduce CO₂ emissions is inherent in the design of the Project combustion turbines and is considered the baseline condition.

Table 6-9 presents the ranking of the GHG technologies deemed feasible for the Project. While these two technologies are "ranked" in order of their presentation, they are more appropriately considered as a suite of measures that will be implemented to confirm that the Project generates and consumes power in the most efficient manner and thereby achieves BACT for GHGs.

Table 6-9: GHG Technology Ranking for the Project

Technology	Ranking	Applied to Project
Simple – cycle combustion turbines (employing efficient, state-of-the-art design)	1	Yes
Clean fuel – natural gas	2	Yes

6.4.4 Step 4. Evaluate the Most Effective Control Technologies

6.4.4.1 Environmental, Energy, and Economic Feasibility of Control Options

Because Pleasants Energy is proposing to utilize both of the feasible technologies for reducing GHGs from the generation of power, no detailed analysis is provided to compare the available control technologies' relative environmental, energy and economic impacts.

6.4.5 Step 5. Proposed Greenhouse Gas BACT Determination

BACT for greenhouse gas emissions from the combustion turbines is determined to be the use of natural gas as a fuel and efficient turbine design. These design options will allow the simple-cycle combustion turbines to not exceed 1,300 lb CO₂/MW-hr (gross) while combusting natural gas and 1,900 lb CO₂/MW-hr (gross) on an annual basis while combusting fuel oil.

6.5 BACT for Start-Up and Shutdown Emissions - Combustion Turbines

6.5.1 Step 1. Identify Potential Control Strategies

Criteria pollutants will be emitted during start-up and shutdown of the combustion turbines. Start-up emissions are generally higher for CO and NO_x emissions because of incomplete combustion that occurs during the transient states.

Pleasants Energy estimates not more than 365 start-up/shutdown events per turbine per year will occur on natural gas and not more than 30 start-up/shutdown events per year. One start-up/shutdown event is equivalent to one start-up (initiating the start to Mode 6 emissions compliance is achieved (approximately 60 percent load) plus one shutdown (generally 60 to 0 percent load).

6.5.2 Step 2. Identify Technically Feasible Control Technologies

There are no technically feasible control technologies for start-up and shutdown emissions from the combustion turbines, except to minimize emissions during these periods using good combustion practices.

6.5.3 Step 3. Rank the Technically Feasible Control Technologies

Since there are no technically feasible control technologies for start-up and shutdown emissions, there is nothing to rank.

6.5.4 Step 4. Evaluate the Most Effective Control Technologies

There are no technically feasible control options for start-up and shutdown emissions; therefore, there are no environmental, energy or economic impacts to discuss.

6.5.5 Step 5. Proposed Start-up and Shutdown BACT Determination

Table 6-10 displays the BACT levels for start-up and shutdown emissions for natural gas operation.

Table 6-10: Start-up and Shutdown Emissions for the Combustion Turbines on Natural Gas

Pollutant	Start-up Emissions (lb/hr) ^{a,b}	Shutdown Emissions (lb/hr) ^{a,c}	Number of Starts Per Turbine ^d	Start-up /Shutdown Emissions (tpy) ^a	Total Start-up /Shutdown Emissions (Both turbines) (tpy) ^a
NOxª	125.5	107.2	365	65.4	130.7
COa	386.3	146.3	365	167.7	335.4
$\frac{PM/PM_{10}}{PM_{2.5}}$	15.9	15.9	365	8.7	17.4
VOCa	7.0	6.4	365	3.7	7.5
SO_2	2.7	2.7	365	1.5	3.0
H ₂ SO ₄	0.41	0.41	365	0.23	0.45
Lead					

⁽a) lb/hr = pounds per hour; tpy = tons per year

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⁽b) Includes start-up emissions from GE Start-up Summary and actual CEMS start-up data.

⁽d) Includes shutdown emissions from GE Start-up Summary and actual CEMS shutdown data.

⁽a) One start-up and shutdown event is equivalent to one start-up plus one shutdown. All emissions based on worst-case cold start data.

Table 6-11: Start-up and Shutdown Emissions for the Combustion Turbines on Fuel Oil

Pollutant	Start-up Emissions (lb/hr) ^{a,b}	Shutdown Emissions (lb/hr) ^{a,c}	Number of Starts Per Turbine ^d	Start-up /Shutdown Emissions (tpy) ^a	Total Start-up /Shutdown Emissions (Both turbines) (tpy) ^a
NO_x	561.6	543.1	30	25.0	50.0
CO	234.4	199.7	30	10.0	20.1
PM/PM ₁₀ / PM _{2.5}	41.0	41.0	30	1.8	3.7
VOC	21.1	21.0	30	0.9	1.9
SO_2	109.0	109.0	30	4.9	9.8
H ₂ SO ₄	17.7	17.7	30	0.80	1.6
Lead	0.03	0.03	30	8.7 x 10 ⁻⁴	1.7 x 10 ⁻³

⁽a) lb/hr = pounds per hour; tpy = tons per year

BACT work practice standards consisting of Good Combustion Practices are applicable to the combustion turbines and will be used at all times during start-up and shutdown. Pleasants Energy will create and maintain work practice standards for start-up and shutdown prior to commercial operation and will keep the plans on-site.

⁽b) Includes start-up emissions from GE Start-up Summary and actual CEMS start-up data.

⁽c) Includes shutdown emissions from GE Start-up Summary and actual CEMS shutdown data.

⁽d) One start-up and shutdown event is equivalent to one start-up plus one shutdown. All emissions based on worst-case cold start data.

7.0 AIR DISPERSION MODELING

Since the Project is subject to PSD review, an air dispersion modeling analysis is required for each regulated NSR pollutant that exceeds its PSD significance level. According to the emission calculations for this Project, NO_x, CO, PM/PM₁₀/PM_{2.5}, and CO₂e are subject to PSD review; as a result, an air quality analysis was performed for NOx, CO, and PM₁₀/PM_{2.5} using the EPA-approved American Meteorological Society (AMS)/EPA Regulatory Model (AERMOD). Consistent with WVDEP guidance, modeling of PM and CO₂e will not be conducted, since there are no modeling thresholds for these pollutants.

A pre-project meeting was held with the WVDEP to discuss the modeling protocol that would be used for this Project. The latest version (Revision 1) of the air dispersion modeling that incorporates WVDEP's comments is presented in Appendix F of this application.

A summary of the models, the modeling techniques, and modeling results for the Project are discussed in the following sections.

7.1 Air Dispersion Model

Air dispersion modeling was performed using the latest version of the AERMOD model (Version 16216r). The AERMOD model is an EPA-approved, steady-state, Gaussian air dispersion model that is designed to estimate downwind ground-level concentrations from single or multiple sources using detailed meteorological data. AERMOD is a model currently approved for industrial sources and PSD permits; the WVDEP requested that Pleasants Energy demonstrate regulatory compliance through its use.

Major features of the AERMOD model are as follows:

- Plume rise, in stable conditions, is calculated using Briggs equations that consider wind and
 temperature gradients at stack top and half the distance to plume rise; in unstable conditions,
 plume rise is superimposed on the displacements by random convective velocities, accounting for
 updrafts and downdrafts due to momentum and buoyancy as a function of downwind distance for
 stack emissions.
- Plume dispersion receives Gaussian treatment in horizontal and vertical directions for stable conditions and non-Gaussian probability density function in vertical direction for unstable conditions.
- AERMOD creates profiles of wind, temperature, and turbulence, using all available measurement levels and accounts for meteorological data throughout the plume depth.

- Surface characteristics, such as Bowen ratio, albedo, and surface roughness length, may be specified to better simulate the modeling domain.
- Planetary Boundary Layers (PBL) such as friction velocity, Monin-Obukhov length, convective velocity scale, mechanical and convective height, and sensible heat flux may be specified.
- AERMOD uses a convective (based upon hourly accumulation of sensible heat flux) and a
 mechanical mixed layer height.
- AERMOD's terrain pre-processor (AERMAP) provides information for the advanced critical dividing streamline height algorithms and uses National Elevation Dataset (NED) to obtain elevations.
- AERMOD uses vertical and horizontal turbulence-based plume growth (from measurements and/or PBL theory) that varies with height and uses continuous growth functions.
- AERMOD uses convective updrafts and downdrafts in a probability density function to predict
 plume interaction with the mixing lid in convective conditions while using a mechanically mixed
 layer near the ground.
- Plume reflection above the lid is considered.
- AERMOD models impacts that occur within the cavity regions of building downwash via the use
 of the plume rise model enhancements (PRIME) algorithm, and then uses the standard AERMOD
 algorithms for areas without downwash.

Details of the modeling algorithms contained in the AERMOD model may be found in the User's Guide for AERMOD. The regulatory default option was selected for this analysis since it met the EPA guideline requirements and WVDEP modeling guidance requirements.

The following default model options, which were discussed in the air dispersion modeling protocol (Appendix F), were used:

- Elevated Terrain Algorithms
- Gradual Plume Rise
- Stack-tip Downwash
- Buoyancy-induced Dispersion
- Calms and Missing Data Processing Routine
- Calculate Wind Profiles
- Calculate Vertical Potential Temperature Gradient
- Rural Dispersion

7.2 Model Parameters

Modeling runs were conducted at full load and partial loads of the combustion turbines to confirm that operation of the Project will not result in impacts greater than the NAAQS and PSD Class II Increments. The expected hourly emission rates and modeling parameters for one combustion turbine operating on natural gas and fuel oil are shown in Table 7-1 and Table 7-2, respectively. These emission rates represent projected worst-case ambient conditions under various operating loads and include start-up and shutdown emissions. The annual emissions are based on worst-case annual emissions.

Table 7-1: Combustion Turbine Emissions and Modeling Parameters – Natural Gas Operation (per Turbine)

	100% Load	80% Load	60% Load	Start-up/ Shutdown
Pollutant		pounds p	er hour (lb/hr)	
NO_x	68.9 (53.0 ^b)	54.0 (53.0 ^b)	44.0 (53.0 ^b)	125.5 ^a (53.0 ^b)
CO	33.9	26.0	22.0	386.3 ^b
PM ₁₀ /PM _{2.5}	15.9 (9.5 ^b)	15.9 (9.5 ^b)	15.9 (9.5 ^b)	18.0 (9.5 ^b)
		Stack Para	meters	
Stack temperature (°F) ^c	1,131	1,097	1,143	1,097
Exit velocity (ft/s) ^c	148.2	139.6	131.0	139.6
Stack height (feet)	114.5	114.5	114.5	114.5
Stack diameter (feet)	18	18	18	18

⁽a) Maximum 1-hour start-up emissions (worst-case combustion turbine emissions during start-up)

⁽b) Maximum annual emissions, annualized based on 8,760 hours per year to obtain lb/hr rates, including start-up and shutdown emissions on gas and oil and 19,082,000,000 SCF/year fuel combusted for both turbines combined which includes fuel oil at 889 SCF/gal.

⁽c) °F = degrees Fahrenheit, ft/s = feet per second

	100% Load	80% Load	60% Load	Start-up/ Shutdown
Pollutant	pounds per hour (lb/hr)			
NO _x ^a	53.0°	53.0°	53.0°	53.0°
СО	76.0	53.0	49.0	234.4 ^b
	41.0	39.0	39.0	41.0
$PM_{10}/PM_{2.5}$	(9.5°)	(9.5°)	(9.5°)	(9.5^{c})
	Stac	k Parameters		
Stack temperature (°F) ^d	1,131	1,158	1,145	1,158
Exit velocity (ft/s) ^d	148.2	141.7	135.1	141.7
Stack height (feet)	114.5	114.5	114.5	114.5
Stack diameter (feet)	18	18	18	18

Table 7-2: Combustion Turbine Emissions and Modeling Parameters – Fuel Oil Operation (per Turbine)

7.3 Modeling Methodology

The modeling methodology used for this analysis is summarized in the sections below. Further specifications, detailed in the air dispersion modeling protocol submitted as part of this application can be found in Appendix F of this application.

7.3.1 Intermittent Emissions

Per EPA guidance (EPA, 2011), Pleasants Energy proposes to only model continuous operation for the 1-hour standards. The combustion turbine back-up fuel oil operation will not be included in the 1-hour modeling analysis as fuel oil will only be used as a back-up fuel and for testing purposes. This includes start-up emissions from fuel oil which will be, at most, 30 start-ups per turbine per year.-These operations will not contribute significantly to the annual distribution of the daily maximum 1-hour concentrations. The list of operating scenarios considered intermittent and not modeled for the 1-hour standard are listed in Table 7-3.

⁽a) The combustion turbine back-up fuel oil operation and start-up emissions are intermittent and will not be included in the NO₂ 1-hour modeling analysis

⁽b) Maximum 1-hour start-up emissions (worst-case combustion turbine emissions during start-up)

⁽c)Maximum annual emissions, annualized based on 8,760 hours per year to obtain lb/hr rates, including start-up and shutdown emissions on gas and oil and 19,082,000,000 SCF/year fuel combusted for both turbines combined which includes fuel oil at 889 SCF/gal.

⁽d) °F = degrees Fahrenheit, ft/s = feet per second

Operating Scenario	Reason Not Modeled for the 1-hour Standard ^a
Ultra-low sulfur diesel combustion in the combustion turbines	Ultra-low sulfur diesel will only be used as a back-up fuel and is limited to 7,668,886 gallons per year for both turbines combined (approximately 260 hours, each). It is not predictable as to when this will occur, and it is expected that it will happen infrequently.
Ultra-low sulfur diesel start-up for combustion	Ultra-low sulfur diesel will only be used as a back-up fuel. At most, each turbine will have 30 start-ups per year. ^a It is not predictable as to when

this will occur, and it is expected that it will happen infrequently.

Table 7-3: Operating Scenarios Not Included in 1-hour Modeling Analysis

(a) Each start-up is a maximum of 2 hours and each shutdown is a maximum of 1 hour.

7.3.2 Good Engineering Practice

turbines

Sources are subject to Good Engineering Practice (GEP) stack height requirements outlined in 40 CFR Part 51, Sections 51.100 and 51.118. As defined by the regulations, GEP height is calculated as the greater of 65 meters (measured from the ground level elevation at the base of the stack) or the height resulting from the following formula:

$$GEP = H + 1.5L$$

Where,

H =the building height; and

L = the lesser of the building height or the greatest crosswind distance of the building, also known as maximum projected width.

To meet stack height requirements, the point sources have been evaluated in terms of their proximity to nearby structures. The purpose of this evaluation is to determine if the discharge from each stack will become caught in the turbulent wake of a building or other structure, resulting in downwash of the plume. Downwash of the plume can result in elevated ground-level concentrations. EPA's 1985 *Guideline for Determination of Good Engineering Practice Stack Height* provides guidance for determining whether building downwash will occur. The downwash analysis was performed consistent with the methods prescribed in this guidance document.

Calculations for determining the direction-specific downwash parameters were performed using the most current version of the EPA's Building Profile Input Program – Plume Rise Model Enhancements, otherwise referred to as the BPIP-PRIME downwash algorithm (Version 04274). The BPIP-PRIME files are included in Appendix H as part of the modeling analysis. Modeled stack heights did not exceed the greater of 65 meters or the calculated GEP stack height, and the lesser of actual height or GEP stack height was used.

7.3.3 Receptor Grid

The overall purpose of the modeling analysis is to demonstrate that operation of the Project will not result in, or contribute to, concentrations above the NAAQS or PSD Class II Increments. The modeling runs were conducted using the AERMOD model in simple and complex terrain mode within a 20- by 20-kilometer Cartesian grid to determine the significant impact area (SIA) for each pollutant (Figure G-1, Appendix G). Based on guidance from WVDEP, the grid will incorporate the receptor spacing specified in Table 7-4. Receptors will also be placed along the fence line boundary at a spacing of 50 meters.

 Distance from Fence Line (kilometers)
 Receptor Spacing (meters)

 0-1 50

 1-3 100

 3-10 250

 10-20 500

Table 7-4: Receptor Spacing from Fence Line Boundary

Source: WVDEP

The significant impact area exceeded 20 kilometers for the 1-hour NO₂ averaging period; therefore, the grid was extended to a 50-by-50-kilometer grid for the 1-hour NO₂ modeling (Figure G-2, Appendix G). The significant impact area did not exceed 20 kilometers for all other pollutants and averaging periods and the receptor grid was not extended.

Terrain elevations were incorporated into the model. Therefore, the appropriate U.S. Geological Survey (USGS) NED were used to obtain the necessary receptor elevations. North American Datum of 1983 (NAD 83) was used to develop the Universal Transverse Mercator (UTM) coordinates for this Project.

AERMOD has a terrain preprocessor (AERMAP) which uses gridded terrain data for the modeling domain to calculate not only a XYZ coordinate, but a representative terrain-influence height associated with each receptor location selected. This terrain-influenced height is called the height scale and is separate for each individual receptor. AERMAP (Version 11103) utilized the electronic digital elevation model (DEM) terrain data to populate the model with receptor elevations.

7.3.4 Meteorological Data

Surface air meteorological data from Parkersburg Wood County Airport, West Virginia (Station ID 03804) and upper air data from Wilmington Airborne Park, Ohio (Station ID 13841) were used for years 2012 to 2016. A profile base elevation value of 263.3 meters was used. The dominant wind direction is shown in Figure G-3 in Appendix G. Based on guidance from WVDEP, a surface sensitivity analysis was

performed. AERSURFACE inputs for both the Project site and the Parkersburg Wood County Airport were used to generate meteorological data for both sets of AERSURFACE inputs. The results of the modeling analysis demonstrated that the AERSURFACE inputs for the Project site produce the worstcase results for all pollutants and averaging periods modeled for the Project. Therefore, the Project site AERSURFACE analysis was used to generate the meteorological data for the air dispersion modeling analysis. The modeling protocol in Appendix F discusses the analysis.

7.3.5 **Land Use Parameters**

Based on the Auer scheme, the existing land use for a 3-kilometer area surrounding the Project is more than 50 percent rural (Auer, 1978). Also, the population density is fewer than 750 people per square kilometer for the same area. Therefore, rural dispersion coefficients were used in the AERMOD models. The modeling protocol in Appendix F discusses the Auer scheme analysis.

7.3.6 **Modeling Thresholds**

The NAAQS, modeling/monitoring significance levels, and PSD Class II Increment thresholds for the modeled pollutants are shown in Table 7-5.

Table 7-5: NAAQS, Monitoring and Monitoring Significance Levels, and PSD Class II Increment

	Averaging Period	Monitoring Significance Level ¹	Modeling Significance Level ²	PSD Class II Increment ³	NAAQS⁴
Pollutant		microgran	ns per cubic met	er (µg/m³)	
NO	Annual	14	1	25	100
NO_2	1-hour	NA	7.4	NA	188
CO	8-hour	575	500	NA	10,000
СО	1-hour	NA	2,000	NA	40,000
DM.	Annual	NA	1	17	NA
PM_{10}	24-hour	10	5	30	150
DM	Annual	NA	0.2ª	4	12
PM _{2.5}	24-hour	4 ^b	1.2ª	9	35

Source:

- (1) Title 40 CFR 51.21(i)(5)(i)
- (2) Title 40 CFR 51.165(b)(2)
- (3) Title 40 CFR 52.21(c)
- (4) Title 40 CFR Part 50
- (a) EPA Draft Memorandum, August 18, 2016, "Guidance on Significant Impact Levels for Ozone and Fine Particles in the Prevention of Significant Deterioration Permitting Program."
- (b) The PM_{2.5} 24-hour significant monitoring concentration was vacated by the United States Court of Appeals for the District of Columbia Circuit on January 22, 2013.

The modeled values will be modeled using the appropriate form of the standard for each pollutant and averaging period. For significance modeling, all short-term and annual averaging periods will be modeled with the impact shown in Table 7-6. For PSD Class II Increment, the short-term averaging periods will be compared to the high second highest impacts, and the annual standards will be compared to the first highest impacts. The NAAQS thresholds will be modeled using the highs shown in Table 7-6 for each averaging period.

Pollutant Averaging Period Significant Impact Level High¹ NAAQS Modeled High² Annual 1st highest 1st highest NO_2 1-hour 5-year average 1st high hour day 5-year average 8th high hour day 1st highest 8-hour High 2nd highest CO 1-hour 1st highest High 2nd highest Annual 1st highest PM_{10} 24-hour 1st highest 6th highest in 5 years Annual 5-year average year 5-year average year $PM_{2.5}$ 24-hour 5-year average 1st high day 5-year average 8th high day

Table 7-6: Modeled Highs

Source:

7.3.7 Significant Impact Area Determination

The AERMOD model was run for the Project using the worst-case impact scenario for the combustion turbines. If any modeled pollutant resulted in impacts below the significance levels for each averaging period, no further modeling for that pollutant and averaging period was required to determine compliance with the NAAQS or PSD Class II Increments. However, if the modeling predicted impacts at or above the modeling significance level for any pollutant, a cumulative analysis including all point sources within the radius of impact (ROI) was required for that pollutant and averaging period.

7.3.8 Background Air Quality

As stated previously, if any pollutant exceeds its respective PSD significance level, a refined analysis (cumulative analysis) will be performed for that pollutant and averaging period. This analysis will be used to determine compliance with the PSD Class II Increments and the NAAQS. The NAAQS are set up to protect the air quality for all sensitive populations and attainment is determined by the comparison to the NAAQS thresholds. As such, there is an existing concentration of each criteria pollutant that is present in ambient air that must be included in an analysis to account for items such as mobile source emissions that

⁽¹⁾ Title 40 CFR 51.165(b)(2)

⁽²⁾ Title 40 CFR Part 50

are not accounted for in the model. Monitored ambient concentrations will be added to the modeled ground level impacts to account for these sources.

The EPA and state agencies collect ambient air quality pollutant concentrations from monitors that are placed throughout each state. The data that is collected by the monitors is available on the EPA website (http://www.epa.gov/airdata/). For the Project, background values for each pollutant were identified from the representative monitors in the area. Each pollutant has been reviewed for applicable monitors and the background values were identified based on this analysis. The monitored background levels will be added to the modeled NAAQS impacts, as previously discussed.

In accordance with EPA documentation⁵, there are three criteria that should be considered when selecting a representative existing ambient air monitor to represent ambient air concentrations for a project. These three criteria include the following:

- Monitor Location,
- Data Quality; and
- Currentness of Data.

Further discussion on these three criteria is detailed in the modeling protocol in Appendix F.

The regional background concentrations for the modeled pollutants and averaging periods for the cumulative modeling analysis are listed in Table 7-7.

Table 7-7: Background Concentration for the NO₂ 1-hour Averaging Period

Pollutant	Averaging Period	Background Concentration (µg/m³)ª	Form of the Standard	Air Quality System Monitor ID
NO_2	1-hour	68.9	98 th percentile averaged over years 2014 to 2016	Charleroi, Pennsylvania (Monitor 42-125-0005)
PM _{2.5}	24-hour	19.0	98 th percentile averaged over years 2014 to 2016	Vienna, West Virginia (Monitor 54-107-1002)

(a) $\mu g/m^3 = \text{micrograms per cubic meter}$

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⁵ U.S EPA. Ambient Air Monitoring Guidelines for Prevention of Significant Deterioration (PSD). EPA-450/4-87-007. May 1987.

Burns & McDonnell

7.3.9 Ambient Monitoring

The modeling analysis that was conducted for the Project addresses the pre-construction monitoring provision of the PSD regulations. The regulations specify significant monitoring levels for each PSD pollutant that triggers the requirement to perform one year of pre-construction ambient air monitoring. For any impacts predicted to be below the monitoring *de minimis* levels, Pleasants Energy requests pre-construction ambient air monitoring not be required. For any predicted concentrations reaching or exceeding the monitoring *de minimis* levels, Pleasants Energy plans to meet all pre-construction monitoring requirements stated in the "Ambient Monitoring Guidelines for Prevention of Significant Deterioration" (EPA).

7.3.10 NAAQS and PSD Class II Increment Analysis

Per discussions with WVDEP, all major stationary sources that emit pollutants subject to this analysis within 20 kilometers of the Project site were addressed for the NAAQS and PSD Class II Increment analysis for pollutants that exceed their respective significant impact level. Sources located 20 to 25 kilometers from the site were analyzed on a case-by-case basis. The inventories of sources were developed in accordance with applicable EPA guidance, input from the WVDEP, and the Ohio Environmental Protection Agency (OEPA). The emissions and stack parameters have been determined for the inventory sources from permits, emission inventories and other information. A list of the inventory sources provided by the WVDEP and OEPA is located in Appendix F and on DVD in Appendix H. The submitted cumulative modeling includes all stationary sources that emit pollutants subject to this analysis and that are located within 20 kilometers. Sources within 20-25 kilometers were included on a case-by-case basis.

The existing Pleasants Energy sources were included in the cumulative modeling (combustion turbines and diesel generators). The existing diesel generators were modeled to represent blackstart operation. Blackstart operation could occur in rare circumstances when all five diesel generators must be used to startup the combustion turbines at the Pleasants Energy facility. This type of operation could occur in the event of a grid failure (when no electricity is available to startup the combustion turbines) and will also occur during annual testing of blackstart capabilities. In this case, all five diesel blackstart generators would need to operate for a maximum of four hours to bring one combustion turbine online. While this operation is considered to be intermittent/emergency with regards to the 1-hour NO₂ standard, the impacts on the 24-hour PM_{2.5} standards were evaluated. Therefore, all five diesel generators were modeled to operate in a blackstart scenario for four hours out of a 24-hour period. Table 7-8 shows the modeled 24-hour averaged PM_{2.5} rate for each diesel generator during normal operation (assuming operation every hour for the 24-hour period) and during blackstart operation.

PM _{2.5} Emission Rate	PM _{2.5} Emission Rate
Normal Operation, Each Engine	Blackstart Operation, Each Engine
24-Hour Average	24-hour Average
(lb/hr)	(lb/hr)
0.72	0.12

Table 7-8: Diesel Generator 24-Hour Average PM2.5 Emission Rates

7.3.11 NO₂ Modeling – Multi-Tiered Screening Approach

The AERMOD model predicts ground-level concentrations of any generic pollutant without chemical transformations. Thus, the modeled NO_x emission rate will give ground-level modeled concentrations of NO_x NAAQS values are presented as NO₂.

The EPA has a three-tier approach to modeling NO₂ concentrations.

- Tier I total conversion, or all $NO_x = NO_2$
- Tier II use a default NO₂/NO_x ratio
- Tier III case-by-case detailed screening methods, such as OLM and Plume Volume Molar Ratio Method (PVMRM)

Initial modeling for the Project was performed using both Tier I and Tier II methodologies. It was determined from these modeling iterations that less conservative methods for determining 1-hour NO_2 compliance would be needed for this Project. Therefore, the ambient impact of the 1-hour NO_x predicted by the models was screened using the Tier III – OLM. The modeling protocol, which discussed the proposed model to be used and the OLM methodology is shown in Appendix F of this application for reference.

Per WVDEP guidance and EPA's March 2011 memo⁶ the applicant modeled only continuous operation for the 1-hour standard. The combustion turbine back-up fuel oil operation was not included in the 1-hour modeling analysis as the combustion turbines will operate on fuel oil only in emergency situations when natural gas is curtailed and for testing purposes at periods which cannot be predicted with reasonable certainty. In addition, start-up emissions from the combustion turbines on fuel oil were not modeled for the 1-hour NO₂ standard, either, as it is expected that there will be at most 30 starts per turbine per year which will be only in emergency situations and for testing purposes at unknown time periods. These

⁶ March 1, 2011 EPA Memo from Tyler Fox. Additional Clarification Regarding Application of Appendix W Modeling Guidance for the 1-hour NO₂ National Ambient Air Quality Standard

operations will not contribute significantly to the annual distribution of the daily maximum 1-hour concentrations.

The Tier III OLM was not applied to the NO_x annual averaging period modeled impacts. All NO_x was assumed to be NO₂ for the annual averaging period; so Tier I was used for this averaging period.

7.3.11.1 In-Stack NO₂/NO_x Ratios

The amount of NO₂ present in the stack gases was determined for each piece of equipment being modeled and was determined from published data. A default in-stack NO₂/NO_x ratio of 0.5 was used for the natural gas-fired turbines per EPA's March 2011 Memo,⁷ as an appropriate equipment-specific in-stack ratio was not identified. For the cumulative modeling analysis, a default in-stack ratio NO₂/NO_x⁸ ratio of 0.5 was used for inventory sources less than 1 kilometer from the Project site (this includes the existing sources at Pleasants Energy facility). Based on guidance from WVDEP, an in-stack NO₂/NO_x ratio of 0.2 was used for inventory sources greater than 1 kilometer away from the Project site.

Additionally, an equilibrium NO₂/NO_x ratio of 0.90 was used per EPA's March 2011 Memo.

7.3.11.2 Hourly Ozone Data

The selected monitor to be used for the 1-hour hourly ozone background is the West Virginia Air Pollution Control Commission monitoring station located in Vienna, Wood County, West Virginia (Air Quality System [AQS] ID: 54-107-1002). The applicant was advised by WVDEP to use this monitor for ozone season data as it is representative of the Project site. Additionally, the Vienna monitor is located in a similar land-use area as the land-use near the Project; therefore, the monitor will provide data that is representative of the ozone concentrations in the Project area.

Because the Vienna monitor only has ozone season data available, two other monitors were selected for the non-ozone season data: the Lawrenceville monitoring station located in Pittsburg, Pennsylvania (AQS ID: 43-003-0008), and the Quaker City monitoring station located in Quaker City, Ohio (AQS ID: 39-121-9991). The Quaker City monitoring station is located closer to the Project site (approximately 70 kilometers from the Project site) than the Lawrenceville Station (approximately 170 kilometers from the Project site). The Quaker City station was deemed the most representative for the non-ozone season data due to its close proximity to the Project site. Data from the Quaker City station was used for the non-ozone season hourly data for years 2012 to 2016.

⁷ March 1, 2011 EPA Memo from Tyler Fox. Additional Clarification Regarding Application of Appendix W Modeling Guidance for the 1-hour NO₂ National Ambient Air Quality Standard

Hourly background ozone concentrations were obtained from the EPA Technology Transfer Network Air Quality System for the Vienna monitoring station located in Wood County, West Virginia (AQS ID: 54-107-1002) and the Quaker City monitoring station located in Ohio (AQS ID: 39-121-9991). Data from each monitoring station was used for the time periods previously discussed. The background data was formatted for use in the AERMOD model and processed for years 2012 to 2016 to match the meteorological data years used in the modeling. The following steps and assumptions were used to create the hourly ozone data:

- One to six missing values: The average of the previous and following value was used.
- More than six missing values: Data was substituted based the maximum of the ozone concentrations measured during that hour in the month of the missing values.

7.4 Significance Model Results

Significance modeling was performed for NO_x , CO, and $PM_{10}/PM_{2.5}$ for the operation of the combustion turbines.

7.4.1 NO₂ Results

After examining the modeling results at all load levels, it was determined that no exceedances of the annual NO₂ modeling significance level occurred, and that no further modeling was required. The annual predicted impacts were lower than the ambient air monitoring *de minimis* level and therefore no preconstruction ambient monitoring is proposed for NO₂.

The model predicted that impacts greater than the 1-hour NO₂ modeling significance level occurred, and refined modeling would be required. The maximum modeled concentrations for the NO₂ 1-hour and annual average periods are given in Table 7-9.

7.4.2 CO Results

After examining the modeling results at all load levels, it was determined that no exceedances of the 1-hour and 8-hour CO modeling significance levels occurred, and that no further modeling was required. Also the 8-hour predicted impacts were less than the ambient air monitoring *de minimis* level. The maximum modeled concentrations for CO are given in Table 7-9.

7.4.3 PM₁₀ Results

After examining the modeling results at all load levels, it was determined that no exceedances of the annual and 24-hour PM_{10} modeling thresholds occurred; therefore, no further modeling was required for this pollutant. Additionally, the 24-hour predicted impacts for PM_{10} were lower than the ambient air

monitoring *de minimis* levels and no pre-construction monitoring will be required. The maximum modeled results from the PM_{10} annual and 24-hour averaging periods are shown in Table 7-9.

7.4.4 PM_{2.5} Results

After examining the modeling results at all load levels, it was determined that no exceedances of the annual PM_{2.5} modeling thresholds occurred; therefore, no further modeling was required for this averaging period. The model predicted that impacts greater than the 24-hour PM_{2.5} modeling significance level occurred, and refined modeling would be required. The maximum modeled concentrations for the PM_{2.5} 24-hour and annual average periods is given in Table 7-9. The high first high is shown for 24-hour and annual PM₁₀ and for the 24-hour and annual PM_{2.5} the highest average first high over 5 years is shown.

Additionally, the 24-hour predicted impacts for $PM_{2.5}$ were lower than the ambient air monitoring *de minimis* levels and no pre-construction monitoring will be required.

7.4.5 Significance Modeling Summary

The maximum impacts from the Project are listed in Table 7-9. The results of the significance modeling indicate that the impacts of the CO 1-hour and 8-hour, NO₂ annual, PM₁₀ annual and 24-hour, and PM_{2.5} annual averaging periods from the Project will not result in a significant impact at any location. No further modeling is required for a PSD pollutant if the modeled impacts are below the significance levels.

Modeling Monitoring Predicted **UTM** Coordinates^a Significance De Minimis Concentration **Averaging** Level Level **Pollutant** Year Period **Easting Northing** micrograms per cubic meter (µg/m³) (meters) (meters) Annual 470,200 4,351,900 2015 0.1 14 NO_2 1-hour 4,351,900 5 years 49.2 470,200 7.5 1-hour 470,200 4,351,900 2016 179.0 2000 CO 8-hour 470,000 4,348,750 2012 66.6 500 575 Annual 2015 470,200 4,351,900 0.02 1 PM_{10} 24-hour 2016 469,000 4,342,500 2.7 5 10 Annual 470,200 4,351,900 5 years 0.02 0.2 $PM_{2.5}$ 24-hour 470,200 4,351,900 5 years 1.6 1.2 4

Table 7-9: Maximum Modeled Concentrations

(a) UTM = Universal Transverse Mercator: NAD83

The modeling analyses indicate that the Project's emissions will exceed the PSD modeling significance thresholds for the NO₂ 1-hour and the PM_{2.5} 24-hour averaging periods. Refined modeling analyses were conducted to demonstrate compliance with the NAAQS and PSD Class II Increments.

Model input and output files for each pollutant are provided in Appendix H on DVD. In addition, area plots with concentration contour plots of each pollutant are shown in Figures G-4 to G-11 in Appendix G.

7.5 PSD Class II Increment Modeling

There are no PSD Class II Increment thresholds for 1-hour NO_2 ; therefore, no PSD Class II Increment analysis was performed for NO_2 . A refined modeling analysis was conducted for the $PM_{2.5}$ 24-hour averaging period to demonstrate compliance with the PSD Class II Increment.

An inventory of sources within the expected ROI was used in the refined analysis. This inventory of sources and modeled parameters can be seen in the DVD in Appendix H of this application. An area plot with a concentration contour plot of the 24-hour PM_{2.5} Increment is shown in Figure G-12 in Appendix G

There were modeled PSD Increment exceedances for the PM_{2.5} 24-hour averaging period. Further analysis demonstrated that the proposed Project is not significant at the receptors that exceed the Increment. As such, it was determined that there is enough available PM_{2.5} PSD Class II Increment to construct and operate the proposed Project.

The results of the PSD Class II Increment analysis are shown below in Table 7-10. The second highest high was used for the 24-hour averaging periods.

UTM Coordinates^a **PSD Class II** Predicted **Averaging** Increment **Pollutant** Concentration Year Easting **Northing Period** $(\mu g/m^3)$ $(\mu g/m^3)$ (meters) (meters) 24-hour 451,500 2013 882.6b,c $PM_{2.5}$ 4,353,000

Table 7-10. PM_{2.5} Class II Increment Modeling Results

7.6 NAAQS Modeling

A refined modeling analysis was conducted for the 1-hour NO₂ and 24-hour PM_{2.5} averaging periods to demonstrate compliance with the NAAQS.

⁽a) UTM = Universal Transverse Mercator: NAD83

⁽b) Value is 2nd highest high

⁽c) The Project is not significant at any modeled exceedance

The modeling results showed that the Project is not contributing to any NAAQS exceedance. Although there were modeled NAAQS exceedances for the 1-hour NO₂ averaging period and 24-hour PM_{2.5} averaging period, further analysis (as found in Appendix H) demonstrates that the Project is not significant (does not exceed the significant impact level [SIL]) at the receptors that exceed the NAAQS. Therefore, the Project will be in compliance with the NAAQS. The NAAQS analysis modeling results are shown in Table 7-11.

		UTM Cod	rdinates ^a					
	llutant and ing Period	Easting (meters)	Northing (meters)	Year	Predicted Concentration	Background Concentration	Total Concentration	NAAQS
					micr	ograms per cubi	c meter (µg/m³)	
NO_2	1-hour	475,250	4,358,750	5 years	139.3	68.9	208.2 ^b	188
$PM_{2.5}$	24-hour	451,500	4,353,000	5 years	574.1	19.0	593.1 ^b	35

Table 7-11: NAAQS Modeling Results

The NAAQS thresholds were compared to the following highs shown in Table 7-12 for each averaging period.

Pollutant	Averaging Period	Modeled High
NO_2	1-hour	98 th Percentile
PM _{2.5}	24-hour	98 th Percentile

Table 7-12: Modeled Highs

The model input and output files (including the additional analysis) are provided on DVD in Appendix H. In addition, an area plot with a concentration contour plot is provided in Figure G-13 and G-14 in Appendix G.

7.7 PSD Class I Increment Analysis

Recent Federal Land Manager (FLM) guidance requires that a proposed major source, in the course of a PSD application, perform an assessment of air quality impacts at Class I areas if these areas are located within approximately 300 kilometers of the Project. There are four Class I Areas that are within 300 kilometers of the Project:

• Otter Creek Wilderness (130 kilometers)

⁽a) UTM = Universal Transverse Mercator: NAD83

⁽b) The Project is not significant at any modeled exceedances

- Dolly Sods Wilderness (160 kilometers)
- Shenandoah National Park (200 kilometers)
- James River Face Wilderness (253 kilometers)

The locations of the Project site and the Class I Areas are shown in Appendix F of this application (Figure A-6, Appendix A to the modeling protocol).

An analysis was performed to demonstrate that the operation of the Project will not result in, or contribute to, concentrations above the PSD Class I Increment thresholds. To determine if further analysis is required for the Class I Increment analysis, modeled impacts at receptors placed 50 kilometers in the direction of each Class I area were compared to the Class I significance thresholds. The receptor elevations were adjusted accordingly to resemble the minimum and maximum elevation at the respective Class I areas is shown in Table 7-13. The Class II modeled impacts in comparison to the Class I significance threshold is shown in Table 7-14. Based on the screening analysis, the 24-hour PM_{2.5} fuel oil screening impacts exceed the 24-hour Class I PM_{2.5} SIL for Otter Creek Wilderness and James River Face Wilderness. For all other averaging periods and pollutants, the screening modeling showed that the Project will not significantly impact the four Class I areas that are within 300 kilometers of the Project, and no further analysis is required.

Because PM_{2.5} 24-hour PSD Class I Increment screening impacts were not below the SIL 50 kilometers from the site, a PSD Class I Increment analysis using CALPUFF will need to be performed for Otter Creek Wilderness and James River Face Wilderness to assess the impacts of fuel oil operation. A Class I Increment analysis using CALPUFF was performed as part of the January 2017 PSD air construction permit to lift the original synthetic minor source limits (2017 PSD Project). The results of the 2017 PSD permit Class I Increment modeling showed the Project would only be 57 percent of the PM_{2.5} Class I Increment threshold for Otter Creek Wilderness, and 21 percent for percent of the James River Face Wilderness. Therefore, it is expected that this minor change in fuel oil emission rate (39 lb/hr to 41 lb/hr) would not contribute to any Class I Increment exceedances. (See PSD CALPUFF Class I Increment Modeling Report for Pleasants Energy project from March 2016.) Pleasants is proposing that no Class I Increment CALPUFF analysis be required, given that prior Class I Increment CALPUFF analysis for the 2017 PSD Project was performed and the new Project's emissions are similar (with a very small increase in lb/hr) to the prior 2017 PSD Project's emissions.

	UTM Coordinates ^a		Maximum	Minimum	
Class I Area	Easting (meters)	Northing (meters)	Elevation/Hill Height (meters)	Elevation/Hill Height (meters)	
Otter Creek Wilderness	518,049.4	4,342,002	1,148 / 1,148	688 / 688	
Dolly Sods Wilderness	518,049.4	4,342,002	1,219 / 1,219	824 / 824	
Shenandoah National Park	513,993.2	4,331,840	1,123 / 1,123	247 / 247	
James River Face Wilderness	501,712.5	4,316,433	792 / 792	213 / 213	

Table 7-13: Class I Receptor Coordinates and Elevations

Revision 0

Table 7-14: Class II Modeled Impacts and Class I Significant Impact Level

	Averaging	Maximum Mo	Class I Significant			
Pollutant	Time	Otter Creek Wilderness	Dolly Sods Wilderness	Shenandoah National Park	James River Face Wilderness	Impact Level (µg/m³)
PM ₁₀	24-hour	0.1019	0.0597	0.0690	0.0711	0.3
F1VI ₁₀	Annual	0.0024	0.0012	0.0012	0.0013	0.2
$PM_{2.5}$	24-hour	0.1019	0.0597	0.0690	0.0711	0.07
P1V1 _{2.5}	Annual	0.0024	0.0012	0.0012	0.0013	0.06
NO_2^b	Annual	0.0132	0.0068	0.0067	0.0073	0.1

⁽a) Numbers in bold indicate the Class I significant impact level is exceeded

7.8 Analysis of Secondary PM_{2.5} Formation

An analysis of secondary $PM_{2.5}$ formation as a result of the Project was performed and is detailed in the modeling protocol in Appendix F. Secondary $PM_{2.5}$ formation should have insignificant impacts on the overall $PM_{2.5}$ emissions from the Project.

7.9 Conclusion

The modeling results shown in Table 7-9, demonstrate that no exceedances of the annual NO₂, 8-hour and 1-hour CO, annual and 24-hour PM₁₀, and annual PM_{2.5} modeling significance levels are predicted; consequently, no further modeling is required. A refined modeling analysis was conducted to demonstrate compliance with the PSD Class II Increment for 24-hour PM_{2.5} and NAAQS for 1-hour NO₂ and 24-hour PM_{2.5}. The Project will not cause or contribute to any modeled Class II PSD Increment or NAAQS exceedances.

The operation of the Project will not cause or contribute to a significant degradation of ambient air quality. After examining the results of the model, it has been determined that the modeling requirements for CO, NO₂, and PM₁₀/PM_{2.5} have been fulfilled, and no further modeling is required.

⁽a) UTM = Universal Transverse Mercator: NAD 83

⁽b) Modeled as NO_x

8.0 ADDITIONAL IMPACT ANALYSIS

The additional impacts analysis requirement under PSD includes the ambient air quality impact analysis, soils and vegetation impacts, visibility impairment, and growth analysis for the Project.

8.1 Construction Impacts

There will be no construction associated with this Project; therefore, the potential for short-term adverse effects on air quality in the immediate area around the site will not occur.

8.2 Vegetation Impacts

The following sections briefly describe the potential effects of CO, CO₂, NO₂, PM/PM₁₀/PM_{2.5}, and synergistic effects of pollutants produced by the installation of the Project on the nearby vegetation. The potential effects of the air emissions to vegetation within the immediate vicinity of the Project will be compared to scientific research examining the effects of pollution on vegetation. Damage to vegetation often results from acute exposure to pollution, but may also occur after prolonged or chronic exposures. Acute exposures are typically manifested by internal physical damage to leaf tissues, while chronic exposures are more associated with the inhibition of physiological processes such as photosynthesis, carbon allocation, and stomatal functioning (Hallgren, 1984; Hill and Littlefield, 1969; Mansfield and Freer-Smith, 1984).

8.2.1 Carbon Monoxide

CO is not known to injure plants nor has it been shown to be taken up by plants. Consequently, no adverse impacts to vegetation at or near the Project are expected from CO stack emissions from the Project.

8.2.2 Carbon Dioxide

CO₂ is not known to injure plants. Long-term exposure to elevated CO₂ levels has shown to improve the efficiency of nutrient, water, and photosynthesis in some plants (Drake et al., 1997; Ainsworth et al., 2009). However, the improved efficiencies that result from elevated CO₂ levels may not necessarily result in greater yields for crop plants (Morgan et al., 2005). No adverse impacts to vegetation at or near the facility are expected from CO₂ stack emissions from the Project.

8.2.3 Nitrogen Oxides

During fuel combustion, atmospheric and fuel-bound nitrogen is oxidized to nitrogen oxide (NO) and small amounts of NO₂ (Chang, 1981). The NO is photochemically oxidized to NO₂, which is then subsequently consumed during the production of ozone and peroxyacetyl nitrates (PANs). NO₂ has been

shown to deleteriously impact vegetation (Taylor et al., 1975; Heath, 1980; Kozlowski and Constantinidou, 1986; Darrall, 1989). Different plant species exhibit different levels of sensitivity to nitrogen oxides; however, sensitivities to nitrogen oxides generally decrease as water becomes less available in the soil. Typical leaf injury responses include interveinal necrotic blotches for angiosperms and red-brown distal necrosis in gymnosperms (Kozlowski and Constantinidou, 1986). The blotches on the leaves and along the leaf margins are the result of cell damage and dehydration of leaf tissues. Injury threshold concentrations vary by species and dose. In general, short-term, high concentrations of NO₂ are required for deleterious impacts on plants (Prinz and Brandt, 1986). A 1-hour NO₂ concentration of 7,520 micrograms per cubic meter (µg/m³) will result in a 5 percent foliar injury for the most susceptible plant species (USEPA, 1993). For the most NO₂ sensitive plant species, the minimum concentrations at which adverse growth effects or tissue injury occurred have been reported at 1,200 μg/m³ (1 hour), 3,760 μg/m³ (4 hour averaging time), 500 μg/m³ (24 hour), 564 μg/m³ (1 month averaging time), and 94 μg/m³ (1 year averaging time) (Dvorak et al., 1978; USEPA, 1993). The injury threshold concentration for plants that are grown in West Virginia is 7,380 µg/m³ for tomato (*Lycopersicon esculentum*) and annual sunflower (Helianthus annuus). Lamb's quarters (Chenopodium album) a common, weedy plant found in disturbed areas in West Virginia was not injured for two hours at concentrations of 1.9 μg/m³ NO₂. Furthermore, short-term fumigations of approximately 1-hour, 20-hours, and 48-hours at NO₂ concentrations of 940 to 38,000 μg/m³, 470 μg/m³, and 3,000 to 5,000 μg/m³, respectively, have been shown to impair photosynthesis in a number of herbaceous [tomato, oats (Avena sativa), alfalfa and woody plants (Hill and Bennett., 1970; Capron and Mansfield, 1976; Smith, 1981). Moreover, Taylor and McLean (1970), in their review of NO₂ effects on vegetation, noted that long-term exposures of phytotoxic doses of NO₂ ranged from 280 to 560 μ g/m³.

The maximum annual modeled value for the Project is $0.1 \mu g/m^3$ and the maximum 1-hour NO₂ modeled value for the Project is $49.2 \mu g/m^3$. These levels are low, so it is highly unlikely that NO₂ emissions will impact vegetation adjacent to or surrounding the Project.

8.2.4 Particulate Matter

Particulates have been typically shown to be detrimental to vegetation within the immediate vicinity of the source. The phytotoxic response of a given plant species to particulate deposition on leaves varies depending on the concentration and composition of the airborne particulates. The effects of particle deposition are on a plant or plant community is difficult to measure. Experimental evidence indicates that the deposition of most common particulate materials on leaf surfaces result in less direct harm to plants than phytotoxic gases, which are absorbed and assimilated more rapidly and cause greater direct injury to plant tissues (Guderian, 1986). The most obvious effect of particle deposition on vegetation is a physical

smothering of the leaf surface. This will reduce light transmission to the plant and cause a decrease in photosynthesis. Other phytotoxic effects of particulate deposition on leaves that could result in plant injury include the pH and chemical make-up of the particulates (salts and trace metals) that could affect leaf chemistry.

The maximum PM_{10} 24-hour and $PM_{2.5}$ 24-hour modeled values for the Project are 2.7 μ g/m³ and 1.6 μ g/m³, respectively. These levels are low, so it is highly unlikely that PM_{10} and $PM_{2.5}$ emissions will impact vegetation adjacent to the Pleasants Energy facility.

8.2.5 Synergistic Effects of Pollutants

Air pollutants are known to act in concert to cause injury to or decrease the functioning of plants (Reinert et al., 1975; Omrod, 1982). Synergistic refers to the combined effects of pollutants when they are greater than is expected from the additive effect of the compounds. The inhibitory effects of NO_2 and NO (Capron and Mansfield, 1976), have been reported in various short-term studies for crop plants (e.g., soybean, broad bean (*Vicia faba*), annual sunflower, and tomato). The concentrations of pollutants (80 to $981 \mu g/m^3$) in this study are higher than the concentrations predicted to occur near the Project. Consequently, no synergistic effects of the air pollutants are expected to inhibit vegetation at or near the Pleasants Energy facility.

8.3 Soil Impacts

A soil inventory was completed by obtaining a soil survey within the 3-kilometer radius study area surrounding the facility. The soil survey was obtained from the Natural Resource Conservation Service. The different soil types that were found to be in excess of one percent of the total land area of the 3-kilometer study area are listed in Table 8-1. The most abundant soil type in the vicinity of the Project was Upshur-Gilpin complex, at 20.38 percent.

		•
Ashton silt loam	Lindside silt loam	Sensbaugh loam
Duncannon silt loam	Melvin silt loam	Upshur association
Gilpin-Sumritville-Upshur complex	Mentor silt loam	Upshur-Gilpin complex
Gilpin-Upshur complex	Monongahela and Tilsit silt loams	Vandalia silty clay loam
Hackers silt loam	Peabody-Gilpin complex	Water
Lakin loamy fine sand	Senecaville silt loam	

Table 8-1. Soils Within 3 kilometers of the Project

According to the U.S. Department of Agriculture Soil Conservation Service, the Upshur series consists of well drained soils formed in red clayey shale or mudstone residuum. Upshur soils are on hills and hillslopes on summits, shoulders, and backslopes. The full range of slope is from 0 to 70 percent. Surface runoff potential is medium to very rapid. Major uses of Upshur soils are for cultivation or woodland. Where Upshur soils are hayland, pasture, and cropland, they are cultivated with the principal crops being grass-legume hay, corn, soybeans, wheat, or oats. Where Upshur soils are wooded, they are dominated by oaks (*Quercus* spp.), hickory (*Carya* spp.), and yellow-poplar (*Liriodendrom tulipifera*).

Nitrates caused by NO_x deposition onto the soil can be either beneficial or detrimental to soil depending on its composition. However, the proposed NO_x emission rates and consequently the impacts generated by the Project are not expected to have an adverse impact upon soils in the immediate vicinity since they are below the NAAQS.

8.4 Industrial, Residential, and Commercial Growth Impacts

The purpose of the growth impact analysis is to quantify growth resulting from the increase in time of operation of the Project and assess air quality impacts that would result from that growth.

The facility employs six full-time employees. This Project will not significantly affect growth in the area. The increase in natural gas demand due to the operation of the Project will have no major impact on local fuel markets. No significant air quality impacts due to associated industrial/commercial growth are expected at this time.

8.5 Visibility and Deposition Analysis

8.5.1 Class I Area Analysis

Recent Federal Land Manager (FLM) guidance requires that a proposed major source, in the course of a PSD application, perform an assessment of air quality impacts at Class I areas if these areas are located within approximately 300 kilometers of the Project. There are four Class I Areas that are within 300 kilometers of the Project:

- Otter Creek Wilderness (130 kilometers)
- Dolly Sods Wilderness (160 kilometers)
- Shenandoah National Park (200 kilometers)
- James River Face Wilderness (253 kilometers)

The locations of the Project site and the Class I Areas are shown in Appendix F of this application (Figure A-6, Appendix A to the modeling protocol).

A visibility and deposition analysis was performed as part of the January 2017 PSD air construction permit to lift the original synthetic minor source limits (2017 PSD Project). Given that prior visibility and deposition analysis for the 2017 PSD Project was performed and the new Project's emissions are similar (and should not increase on a maximum 24-hour or lb/hr rate for visibility pollutants) to that project's emissions, Pleasants is proposing that no visibility or deposition analysis be required. The information below summarizes the work that was performed as part of the 2017 PSD Project.

The visibility analysis demonstrated that the visibility impact was less than 5.0 percent for year for each Class I area for both natural gas and fuel oil operation. The Project was not expected to have any noticeable effect on visibility since the predicted visibility impacts were well below the level of acceptable change and no further analysis required.

The nitrogen and sulfur deposition modeling results for each Class I area were also well below the applicable DAT for the 2017 PSD Project. As a result, the 2017 PSD Project was not expected to have adverse impacts resulting from deposition and no further analysis was conducted.

Concurrence was received from the FLMs for the 2017 PSD Project that there would be no significant impacts to any AQRVs at Class I areas for the project.

8.5.2 Class II Area Analysis

The Project will be located in a Class II area. With respect to visibility conditions around the facility, no known Class II screening visibility criteria that have been recommended at this time. A visual plume blight analysis was performed for two sites listed below:

- North Bend State Park, a state park located approximately 25 kilometers east-southeast of the Project location
- Blennerhassett Island State Historical Park, located approximately 24 kilometers west-southwest of the Project location

The visual plume blight analysis was performed in accordance with the guidelines set forth in EPA-454/R-92-023, *Workbook for Plume Visual Impact Screening and Analysis (Revised)* (1992). In the EPA document, the model VISCREEN is recommended for plume visibility analysis. Several refinement levels of VISCREEN are described. The Level-1 screening uses worst-case meteorological conditions (F-class

stability, 1 meter per second wind speed). This level of screening results in the most conservative (worst-case) visibility results. The impacts of the plume are compared to screening criteria to determine if they are perceptible. The screening criteria are a change in relative sensitivity (Delta E) value of 2.0 and a green absolute contrast value of 0.05. If the plume is determined to be imperceptible, the visibility modeling is complete; otherwise, a Level-2 screening that uses actual meteorological data and refined particle characteristics will be performed. The Level-2 screening will result in a more realistic visibility analysis. If this plume visibility still does not meet sky and terrain contrast levels, a Level-3 analysis may be required that adds more statistical analysis.

Level-1 VISCREEN

A Level-1 VISCREEN model was performed for the Project. The inputs into the model included particulate matter, NO_x , primary NO_2 , soot, and primary sulfate (SO_4). The maximum annual particulate and NO_x emission rates of 83.3 and 464.6 tpy respectively, were used in the VISCREEN analysis.

According to the workbook, primary NO₂, soot, and primary SO₄ can be assumed to be zero except for very specific sources. Since the facility is not one of the specified sources, the emissions for the last three pollutants (primary NO₂, soot, and primary SO₄) are assumed to be zero. The next set of inputs into the Level-1 VISCREEN model considers the distance between the source, observer and area, and the background visual range. Background visibility was determined from the VISCREEN manual to be 40 kilometers.

The last inputs into the model are particle sizes, background ozone, plume-source-observer angle, stability, and wind speed. All of these inputs are automatically set if the default option is chosen. For the Level-1 analysis, the workbook tells the analyst to choose the default option, which sets the following particle sizes:

- Background fine = 0.3 micrometer (μm) diameter, 1.5 gram per cubic centimeter (g/cm³) density,
- Background course = $6 \mu m \text{ diameter}$, $2.5 \text{ g/cm}^3 \text{ density}$,
- Plume particulate = $2 \mu m \text{ diameter}$, $2.5 \text{ g/cm}^3 \text{ density}$,
- Plume soot = $0.1 \mu m$ diameter, $2 g/cm^3$ density, and
- Plume primary sulfate = $0.5 \mu m$ diameter, 1.5 g/cm^3 .

The background ozone is 0.04 ppm, the plume-source-observer angle is 11.25 degrees, the worst case atmospheric stability is an F stability class, and the worst case wind speed is 1 meter per second.

The VISCREEN model output compares the calculated Delta E and contrast from the plume to present default comparison values. Delta E is the color difference parameter used to characterize the perceptibility of the plume on a color difference between the plume and a viewing background such as the sky, a cloud, or a terrain feature. Color differences are due to differences in three dimensions: brightness (L*), color hue (a*), and saturation (b*). Delta E is calculated for several lines of sight. A green contrast analysis is also performed for various lines of sight using a green wavelength and contrasting the plume with the terrain and sky backgrounds. The critical E value is 2.0 and the green contrast value is 0.05 for Class I areas; however, there are currently no Class II screening visibility criteria for the state of West Virginia.

The results of the Level-1 VISCREEN model are provided in Appendix I. The visual analyses show that the emissions from the Project exceed the Class I sky and terrain perceptibility threshold at each of the two sites; therefore, a Level-2 VISCREEN analysis was performed.

Level-2 VISCREEN

While the Level-1 screening uses the worst-case meteorological conditions, Level-2 uses observed meteorological data to provide a better, site specific analysis of the visual impacts. The site-specific average wind speed and stability class were determined for the Level-2 analysis. Under most circumstances, the one percent worst atmospheric dispersion day (i.e., the fourth worst day of any year) is typically the worst dispersion conditions for a plume.

The workbook provides guidance on how to determine the one percent worst day. A Level-2 screening analysis allows the following parameters to be adjusted to representative data if available:

- Particle size distribution
- Background visual range
- Complex terrain
- One percent worst meteorological days

Since measurements of particle size are not known, and the background visual range has not been measured in the Project area, these parameters were left at their workbook suggested values. The terrain surrounding the proposed Project is assumed to be flat; therefore, no adjustments were made for terrain. The workbook suggests ranking the plume dispersion by the product of the vertical and horizontal diffusion coefficients $(\sigma_z \sigma_y)$ and the wind speed (U). If the plume takes more than 12 hours to reach a receptor, this dispersion condition was not factored into the one percent worst day.

The analysis of the five-years of meteorological data used to determine the one percent worst day is shown in Appendix I for each of the two sites. Pre-ASOS meteorological data is required to determine the joint frequency distribution. The Parkersburg Wood County Airport, West Virginia (Station ID 03804) station does not have pre-ASOS data. Therefore, a wind rose plot for Huntington/Tri-State Airport (Station ID 03860) for years 1986 to 1990 and Parkersburg Wood County Airport for years 2009 to 2014 were generated to confirm that the data was similar. The wind rose plots are shown in Appendix I and were determined to be comparable. Integrated surface hourly meteorological data and upper air from the Huntington/Tri-State Airport (Station ID 03860) was used for years 1986 to 1990 to determine the wind speed and stability class for this analysis. Appendix I contains the joint frequency distribution results.

The visual results of the Level-2 screening analysis show that the emissions from the Project pass the Class I sky and terrain perceptibility thresholds at North Bend State Park located 25 kilometers away and Blennerhassett Island State Historical Park located 24 kilometers away, using the stability class and wind speed determined from joint frequency distribution. The results of the Level-2 VISCREEN are shown in Appendix I.

8.6 Conclusion

As shown by the results presented in this section of the application and additional supplemental information, the Project will not have a significant adverse impact on the air quality, soils, vegetation, visibility and or growth in the surrounding area.

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WEST VIRGINIA DEPARTMENT OF **ENVIRONMENTAL PROTECTION**

DIVISION OF AIR QUALITY

601 57th Street, SE Charleston, WV 25304 (304) 926-0475

APPLICATION FOR NSR PERMIT AND TITLE V PERMIT REVISION

(OPTIONAL) www.dep.wv.gov/dag PLEASE CHECK ALL THAT APPLY TO NSR (45CSR13) (IF KNOWN): PLEASE CHECK TYPE OF 45CSR30 (TITLE V) REVISION (IF ANY): □ CONSTRUCTION □ MODIFICATION □ RELOCATION ☐ ADMINISTRATIVE AMENDMENT ☐ MINOR MODIFICATION ☐ SIGNIFICANT MODIFICATION ☐ CLASS I ADMINISTRATIVE UPDATE ☐ TEMPORARY IF ANY BOX ABOVE IS CHECKED, INCLUDE TITLE V REVISION ☐ CLASS II ADMINISTRATIVE UPDATE ☐ AFTER-THE-FACT INFORMATION AS **ATTACHMENT S** TO THIS APPLICATION FOR TITLE V FACILITIES ONLY: Please refer to "Title V Revision Guidance" in order to determine your Title V Revision options (Appendix A, "Title V Permit Revision Flowchart") and ability to operate with the changes requested in this Permit Application. Section I. General 1. Name of applicant (as registered with the WV Secretary of State's Office): 2. Federal Employer ID No. (FEIN): Pleasants Energy, LLC 26-3603167 3. Name of facility (if different from above): 4. The applicant is the: ☐ OWNER ☐ OPERATOR \bowtie BOTH 5A. Applicant's mailing address: 5B. Facility's present physical address: 10319 South Pleasants Highway, St. Mary's, WV 26170 | 10319 South Pleasants Highway, St. Mary's, WV 26170 6. West Virginia Business Registration. Is the applicant a resident of the State of West Virginia? ☐ YES If YES, provide a copy of the Certificate of Incorporation/Organization/Limited Partnership (one page) including any name change amendments or other Business Registration Certificate as Attachment A. If NO, provide a copy of the Certificate of Authority/Authority of L.L.C./Registration (one page) including any name change amendments or other Business Certificate as Attachment A. 7. If applicant is a subsidiary corporation, please provide the name of parent corporation: Dynegy 8. Does the applicant own, lease, have an option to buy or otherwise have control of the *proposed site?* 🛛 YES If **YES**, please explain: Applicant owns site If **NO**, you are not eligible for a permit for this source. Type of plant or facility (stationary source) to be constructed, modified, relocated, 10. North American Industry administratively updated or temporarily permitted (e.g., coal preparation plant, primary Classification System crusher, etc.): (NAICS) code for the facility: 221112 Electric generating peaking station 11A. DAQ Plant ID No. (for existing facilities only): 11B. List all current 45CSR13 and 45CSR30 (Title V) permit numbers associated with this process (for existing facilities only): 073 - 00022R30-07300022-2014 (Title V), R13-2373, R13-2373A, R13-2373B, G60-C067, R14-0034

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

12A.							
 For Modifications, Administrative Updates or Temporary permits at an existing facility, please provide directions to the present location of the facility from the nearest state road; 							
 For Construction or Relocation permits, please provide directions to the proposed new site location from the nearest state road. Include a MAP as Attachment B. 							
From 1 st Street in Waverly, head east on Highway 2 approximately 1 mile. The Pleasants Energy facility entrance is on the south side of the highway.							
12.B. New site address (if applicable):	12C. Nearest city or town:	12D. County:					
	Waverly	Pleasants					
12.E. UTM Northing (KM): 4353.573	12F. UTM Easting (KM): 468.629	12G. UTM Zone: 17					
13. Briefly describe the proposed change(s) at the facilit The Project consists of increasing the capacity of the two	combustion turbines at the Pleasants I	Energy.					
14A. Provide the date of anticipated installation or change. If this is an After-The-Fact permit application, provided change did happen: / /	-	14B. Date of anticipated Start-Up if a permit is granted: 03/01/2018					
14C. Provide a Schedule of the planned Installation of/application as Attachment C (if more than one uni	-	units proposed in this permit					
15. Provide maximum projected Operating Schedule of activity/activities outlined in this application: Hours Per Day Days Per Week Approximately 5,000 hours per year per combustion turbine							
16. Is demolition or physical renovation at an existing facility involved? ☐ YES ☑ NO							
17. Risk Management Plans. If this facility is subject to	112(r) of the 1990 CAAA, or will becom	ne subject due to proposed					
changes (for applicability help see www.epa.gov/cepp	oo), submit your Risk Management Pla	n (RMP) to U. S. EPA Region III.					
18. Regulatory Discussion. List all Federal and State a	air pollution control regulations that you	believe are applicable to the					
proposed process (if known). A list of possible application	able requirements is also included in Att	achment S of this application					
(Title V Permit Revision Information). Discuss applica	bility and proposed demonstration(s) of	compliance (if known). Provide this					
information as Attachment D.							
Section II. Additional att	achments and supporting d	ocuments.					
19. Include a check payable to WVDEP – Division of Air Quality with the appropriate application fee (per 45CSR22 and 45CSR13).							
20. Include a Table of Contents as the first page of your application package.							
21. Provide a Plot Plan , e.g. scaled map(s) and/or sketch(es) showing the location of the property on which the stationary source(s) is or is to be located as Attachment E (Refer to Plot Plan Guidance).							
 Indicate the location of the nearest occupied structure (e.g. church, school, business, residence). 							
22. Provide a Detailed Process Flow Diagram(s) showing each proposed or modified emissions unit, emission point and control device as Attachment F.							
23. Provide a Process Description as Attachment G.							
 Also describe and quantify to the extent possible all changes made to the facility since the last permit review (if applicable). 							
All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.							
24. Provide Material Safety Data Sheets (MSDS) for a	·	d as Attachment H.					
 For chemical processes, provide a MSDS for each compound emitted to the air. 							

25.	25. Fill out the Emission Units Table and provide it as Attachment I.						
26.	6. Fill out the Emission Points Data Summary Sheet (Table 1 and Table 2) and provide it as Attachment J.						
27.	27. Fill out the Fugitive Emissions Data Summary Sheet and provide it as Attachment K.						
28.	28. Check all applicable Emissions Unit Data Sheets listed below:						
	Bulk Liquid Transfer Operations	☐ Haul Road Emissions	☐ Quarry				
	Chemical Processes	☐ Hot Mix Asphalt Plant	Solid Materials Sizing, Handling and Storage				
	Concrete Batch Plant	☐ Incinerator	Facilities				
	Grey Iron and Steel Foundry	☐ Indirect Heat Exchanger	☐ Storage Tanks				
\boxtimes	General Emission Unit, specify Combus	stion Turbines					
	out and provide the Emissions Unit Da						
	Check all applicable Air Pollution Cor		_				
	Absorption Systems	Baghouse	☐ Flare				
	Adsorption Systems	Condenser	☐ Mechanical Collector				
	Afterburner	☐ Electrostatic Precipitato	Wet Collecting System				
_	Other Collectors						
	out and provide the Air Pollution Conti						
30.	Provide all Supporting Emissions Ca Items 28 through 31.	Iculations as Attachment N, or	attach the calculations directly to the forms listed in				
31.	1. Monitoring, Recordkeeping, Reporting and Testing Plans. Attach proposed monitoring, recordkeeping, reporting and testing plans in order to demonstrate compliance with the proposed emissions limits and operating parameters in this permit application. Provide this information as Attachment O.						
>		not be able to accept all measur	er or not the applicant chooses to propose such es proposed by the applicant. If none of these plans e them in the permit.				
32.	32. Public Notice. At the time that the application is submitted, place a Class I Legal Advertisement in a newspaper of general						
	circulation in the area where the source is or will be located (See 45CSR§13-8.3 through 45CSR§13-8.5 and <i>Example Legal</i>						
	Advertisement for details). Please submit the Affidavit of Publication as Attachment P immediately upon receipt.						
33.	. Business Confidentiality Claims. Do	es this application include confid	dential information (per 45CSR31)?				
	☐ YES ☑ NO						
>		the criteria under 45CSR§31-4.	itted as confidential and provide justification for each 1, and in accordance with the DAQ's "Precautionary structions as Attachment Q.				
Section III. Certification of Information							
34.	Authority/Delegation of Authority. C Check applicable Authority Form belo		er than the responsible official signs the application.				
	Authority of Corporation or Other Busine	ess Entity 🔲 A	authority of Partnership				
	Authority of Governmental Agency		authority of Limited Partnership				
Sub	Submit completed and signed Authority Form as Attachment R.						
AII	of the required forms and additional infor	mation can be found under the Pe	rmitting Section of DAQ's website, or requested by phone.				

35A. Certification of Information. To certify this permit application, a Responsible Official (per 45CSR§13-2.22 and 45CSR§30-2.28) or Authorized Representative shall check the appropriate box and sign below.									
Certification of Truth, Accuracy, and Completeness									
I, the undersigned Responsible Official / Authorized Representative, hereby certify that all information contained in this application and any supporting documents appended hereto, is true, accurate, and complete based on information and belief after reasonable inquiry I further agree to assume responsibility for the construction, modification and/or relocation and operation of the stationary source described herein in accordance with this application and any amendments thereto, as well as the Department of Environmental Protection, Division of Air Quality permit issued in accordance with this application, along with all applicable rules and regulations of the West Virginia Division of Air Quality and W.Va. Code § 22-5-1 et seq. (State Air Pollution Control Act). If the business or agency changes its Responsible Official or Authorized Representative, the Director of the Division of Air Quality will be notified in writing within 30 days of the official change.									
	Compliance Certification Except for requirements identified in the Title V Application for which compliance is not achieved, I, the undersigned hereby certify that, based on information and belief formed after reasonable inquiry, all air contaminant sources identified in this application are in compliance with all applicable requirements.								
SIGNATURE Please	use blue ink)	ATE: 10//3//7 (Please use blue ink)							
35B. Printed name of signee: Gerald Gatti	,	35C. Title: Plant Manager							
35D. E-mail: Gerald.Gatti@dynegy.com	36E. Phone: 304-665-4201	36F. FAX: 304-665-4218							
36A. Printed name of contact person (if differe	nt from above):	36B. Title:							
36C. E-mail:	36D. Phone:	36E. FAX:							
PLEASE CHECK ALL APPLICABLE ATTACHMENTS INCLUDED WITH THIS PERMIT APPLICATION: Attachment A: Business Certificate Attachment B: Map(s) Attachment C: Installation and Start Up Schedule Attachment M: Air Pollution Control Device Sheet(s) Attachment D: Regulatory Discussion Attachment N: Supporting Emissions Calculations Attachment E: Plot Plan Attachment T: Detailed Process Flow Diagram(s) Attachment F: Detailed Process Flow Diagram(s) Attachment G: Process Description Attachment G: Business Confidential Claims Attachment H: Material Safety Data Sheets (MSDS) Attachment R: Authority Forms Attachment I: Emission Units Table Attachment J: Emission Points Data Summary Sheet Please mail an original and three (3) copies of the complete permit application with the signature(s) to the DAQ, Permitting Section, at the address listed on the first page of this application. Please DO NOT fax permit applications.									
FOR AGENCY LISE ONLY - IE THIS IS A TITLE OF	SOURCE:								
FOR AGENCY USE ONLY – IF THIS IS A TITLE V SOURCE: Forward 1 copy of the application to the Title V Permitting Group and: For Title V Administrative Amendments: NSR permit writer should notify Title V permit writer of draft permit, For Title V Minor Modifications: Itile V permit writer should send appropriate notification to EPA and affected states within 5 days of receipt, NSR permit writer should notify Title V permit writer of draft permit. For Title V Significant Modifications processed in parallel with NSR Permit revision: NSR permit writer should notify a Title V permit writer of draft permit, Public notice should reference both 45CSR13 and Title V permits, EPA has 45 day review period of a draft permit.									



I, Mac Warner, Secretary of State of the State of West Virginia, hereby certify that

PLEASANTS ENERGY, LLC

was duly authorized under the laws of this state to transact business in West Virginia as a foreign limited liability company on December 17, 1999.

The company is filed as an at-will company, for an indefinite period.

I further certify that the company has not been revoked or administratively dissolved by the State of West Virginia nor has the West Virginia Secretary of State issued a Certificate of Cancellation or Termination to the company.

Accordingly, I hereby issue this Certificate of Authorization

CERTIFICATE OF AUTHORIZATION

Validation ID:1WV2M_6A8FB

Given under my hand and the Great Seal of the State of West Virginia on this day of

September 18, 2017

Mac Warner

Secretary of State

ATTACHMENT B – MAP (SEE FIGURE B-1 IN APPENDIX B TO PSD REPORT)

ATTACHMENT C – INSTALLATION AND STARTUP SCHEDULE

Attachment C – Installation and Startup Schedule

Pleasants Energy plans to start construction on the uprate to the combustion turbines in March 2018 or as soon as the permit is granted.

ATTACHMENT D -REGULATORY DISCUSSION (SEE SECTION 5.0 IN PSD REPORT) ATTACHMENT E –
PLOT PLAN
(SEE FIGURES B-2 AND B-3 IN APPENDIX B TO PSD REPORT)

ATTACHMENT F –
PROCESS FLOW DIAGRAMS
(SEE FIGURE B-4 IN APPENDIX B TO PSD REPORT)

ATTACHMENT G - PROCESS DESCRIPTION (SEE SECTION 3.0 IN PSD REPORT)

ATTACHMENT I - EMISSION UNITS TABLE

Attachment I

Emission Units Table

(includes all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status)

Emission Unit ID ¹	Emission Point ID ²	Emission Unit Description	Year Installed/ Modified	Design Capacity	Type ³ and Date of Change	Control Device ⁴
GT01	EP1	General Electric Model 7FA Turbine	2001	1,910 MMBtu/hr (natural gas) 2,065 MMBtu/hr	Modification, date TBD	None
GT02	EP2	General Electric Model 7FA Turbine	2001	(fuel oil) 1,910 MMBtu/hr (natural gas) 2,065 MMBtu/hr (fuel oil)	Modification, date TBD	None

¹ For Emission Units (or <u>S</u>ources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.
² For <u>E</u>mission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.
³ New, modification, removal

Emission Units Table
03/2007

⁴ For <u>Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.</u>

ATTACHMENT J - EMISSION POINTS DATA SUMMARY SHEET

Attachment J EMISSION POINTS DATA SUMMARY SHEET

	Table 1: Emissions Data																
Emission Point ID No. (Must match Emission Units Table & Plot Plan)	Emission Point Type ¹	Emissic Vent Through T (Must I Emissic Table & F	ted his Point match n Units	De (Musi Emission U	ion Control vice t match Inits Table & Plan)	(chemical processes only) Chemical Name/CAS³ (Speciate VOCs		ion Unit Pollutants - cmical Chemical Name/CAS³ (Speciate VOCs		Emission Unit (chemical rocesses only) Pollutants - Chemical Name/CAS ³ (Speciate VOCs		Potential Emissions ⁴	Maximum Potential Controlled Emissions ⁵		Form or M	Est. Method Used ⁶	Emission Concentration ⁷ (ppmv or mg/m ⁴)
		ID No.	Source	ID No.	Device Type	Short Term ²	Max (hr/yr)	& HAPS)	lb/hr	ton/yr	lb/hr	ton/yr	Solid, Liquid or Gas/Vapor)				
EP1	Vertical stack	GT1						NOx, CO, PM/PM ₁₀ /PM _{2.5} , VOC, SO ₂ , H ₂ SO ₄ , CO ₂ , N ₂ O, CH ₄ , CO ₂ e, HAPs		See Append	lix C – Emi	ssions Calc	ulations				
EP2	Vertical stack	GT2						NOx, CO, PM/PM ₁₀ /PM _{2.5} , VOC, SO ₂ , H ₂ SO ₄ , CO ₂ , N ₂ O, CH ₄ , CO ₂ e, HAPs		See Append	lix C – Emi	ssions Calc	ulations				

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit emissions are not typically considered to be fugitive and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugitive emission activities.

¹ Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.

² Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (ie., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).

³ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. **LIST** Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead. Organics, O₃, NO, NO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. **DO NOT LIST** H₂, H₂O, N₂, O₂, and Noble Gases.

⁴ Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁵ Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmv) are used. If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m³) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO₂, use units of ppmv (See 45CSR10).

Attachment J EMISSION POINTS DATA SUMMARY SHEET

	Table 2: Release Parameter Data							
Emission	Inner	Exit Gas			Emission Point El	evation (ft)	UTM Coordinates (km)	
Point ID No. (Must match Emission Units Table)	Diameter (ft.)	Temp. (°F)	Volumetric Flow ¹ (acfm) at operating conditions	Velocity (fps)	Ground Level (Height above mean sea level)	Stack Height ² (Release height of emissions above ground level)	Northing	Easting
EP1	18	1,131	2,260,000	148.2	650	114.5	4,353.8100	468.6270
EP2	18	1,131	2,260,000	148.2	650	114.5	4,353.8142	468.6810

¹ Give at operating conditions. Include inerts. ² Release height of emissions above ground level.

ATTACHMENT L - EMISSION UNIT DATA SHEETS

Attachment L EMISSIONS UNIT DATA SHEET GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form):

Name or type and model of proposed affected source:
General Electric Model 7FA Turbines (GT1 and GT2) – Fuel oil combustion. Pleasants Energy is performing an uprate to GT1 and GT2.
2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.
See Process Flow Diagram (Figure B-4) in Appendix B of the PSD Air Construction Permit
3. Name(s) and maximum amount of proposed process material(s) charged per hour:
N/A
4. Name(s) and maximum amount of proposed material(s) produced per hour:
N/A
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:
Combustion of fuel oil

* The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

6. Cor	Combustion Data (if applicable):						
(a)	(a) Type and amount in appropriate units of fuel(s) to be burned:						
Ultra-	low sulfur distillate fue	l oil					
	Chemical analysis of pr and ash:	roposed fuel(s), excluding coal, in	cluding maximum percent sulf	ur			
Only	_	t of the low sulfur distillate fuel s fuel will be combusted in the cor	-	•			
(c)	Theoretical combustion	air requirement (ACF/unit of fue	l):				
	@	°F and	psia.				
(d)	Percent excess air:						
(e)	Type and BTU/hr of bu	rners and all other firing equipme	ent planned to be used:				
N/A							
	If coal is proposed as a coal as it will be fired:	source of fuel, identify supplier a	and seams and give sizing of th	ie			
N/A							
(g)	Proposed maximum de	sign heat input:	2,065 × 10 ⁶ BTU/hr.				
7. Pro	jected operating schedu	ule:	I				
Hours/Day		Days/Week	Weeks/Year				

8.	B. Projected amount of pollutants that would be emitted from this affected source if no control devices were used:					
@	1,131	°F and		psia		
a.	NO _X	470	lb/hr	grains/ACF		
b.	SO ₂	109	lb/hr	grains/ACF		
C.	СО	76	lb/hr	grains/ACF		
d.	PM ₁₀	41	lb/hr	grains/ACF		
e.	Hydrocarbons		lb/hr	grains/ACF		
f.	VOCs	20	lb/hr	grains/ACF		
g.	Pb	0.02	lb/hr	grains/ACF		
h.	Specify other(s)					
	H ₂ SO ₄	17.7	lb/hr	grains/ACF		
	CO ₂ e	337,813	lb/hr	grains/ACF		
			lb/hr	grains/ACF		
			lb/hr	grains/ACF		
			lb/hr	grains/ACF		

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

⁽²⁾ Complete the Emission Points Data Sheet.

	and reporting in order to demonstrate compliance Please propose testing in order to demonstrate
REPORTING	TESTING
	E PROCESS PARAMETERS AND RANGES THAT ARE STRATE COMPLIANCE WITH THE OPERATION OF THIS
	POSED RECORDKEEPING THAT WILL ACCOMPANY THE
REPORTING. PLEASE DESCRIBE THE PRORECORDKEEPING.	PPOSED FREQUENCY OF REPORTING OF THE
TESTING. PLEASE DESCRIBE ANY PROPOSED EMISPOLLUTION CONTROL DEVICE.	SSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR
10. Describe all operating ranges and mainter maintain warranty	nance procedures required by Manufacturer to

Attachment L **EMISSIONS UNIT DATA SHEET GENERAL**

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on *Equipment List Form*):

,
Name or type and model of proposed affected source:
General Electric Model 7FA Turbines (GT1 and GT2) - Natural gas combustion. Pleasants Energy is performing an uprate to GT1 and GT2.
2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.
See Process Flow Diagram (Figure B-4) in Appendix B of the PSD Air Construction Permit Application report.
3. Name(s) and maximum amount of proposed process material(s) charged per hour:
N/A
4. Name(s) and maximum amount of proposed material(s) produced per hour:
N/A
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:
Combustion of natural gas

The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

6.	Combustion Data (if applicable):						
	(a) Type and amount in ap	propriate units of fuel(s) to be bu	rned:				
	atural gas, maximum of 19,082,000,000 SCF per year for both turbines combined. This cludes fuel oil combustion as well.						
	(b) Chemical analysis of pour and ash:	roposed fuel(s), excluding coal, in	cluding maximum percent sulfur				
A	nnual average sulfur conter	nt of the natural gas shall not exce	ed 0.5 grains per 100 scf				
	(c) Theoretical combustion	n air requirement (ACF/unit of fue	l):				
	@	°F and	psia.				
	(d) Percent excess air:						
	(e) Type and BTU/hr of bu	rners and all other firing equipme	nt planned to be used:				
N	/A						
	(f) If coal is proposed as a coal as it will be fired:	a source of fuel, identify supplier a	and seams and give sizing of the				
N	/A						
	(g) Proposed maximum de	esign heat input: 1,9	10 × 10 ⁶ BTU/hr.				
7.	Projected operating sched	ule:					
Но	urs/Day	Days/Week	Weeks/Year				

8.	3. Projected amount of pollutants that would be emitted from this affected source if no control devices were used: *Emissions are per combustion turbine.				
@	1,131	°F and		psia	
a.	NO _X	68.9	lb/hr	grains/ACF	
b.	SO ₂	2.7	lb/hr	grains/ACF	
C.	СО	33.9	lb/hr	grains/ACF	
d.	PM ₁₀	15.9	lb/hr	grains/ACF	
e.	Hydrocarbons		lb/hr	grains/ACF	
f.	VOCs	3.2	lb/hr	grains/ACF	
g.	Pb		lb/hr	grains/ACF	
h.	Specify other(s)				
	H ₂ SO ₄	0.41	lb/hr	grains/ACF	
	CO ₂ e	223,611	lb/hr	grains/ACF	
			lb/hr	grains/ACF	
			lb/hr	grains/ACF	
			lb/hr	grains/ACF	

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

⁽²⁾ Complete the Emission Points Data Sheet.

	and reporting in order to demonstrate compliance Please propose testing in order to demonstrate
REPORTING	TESTING
	E PROCESS PARAMETERS AND RANGES THAT ARE STRATE COMPLIANCE WITH THE OPERATION OF THIS CONTROL DEVICE.
RECORDKEEPING. PLEASE DESCRIBE THE PROFMONITORING.	POSED RECORDKEEPING THAT WILL ACCOMPANY THE
REPORTING. PLEASE DESCRIBE THE PRORECORDKEEPING.	POSED FREQUENCY OF REPORTING OF THE
TESTING. PLEASE DESCRIBE ANY PROPOSED EMI POLLUTION CONTROL DEVICE.	SSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR
10. Describe all operating ranges and mainter maintain warranty	nance procedures required by Manufacturer to

ATTACHMENT O – MONITORING – RECORDKEEPING – REPORTING – TESTING (SEE SECTION 5.1 IN PSD REPORT)

ATTACHMENT P - PUBLIC NOTICE

AIR QUALITY PERMIT NOTICE Notice of Application

Notice is given that <u>Pleasants Energy</u>, <u>LLC</u> has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a <u>45CSR14 Prevention of Significant</u> <u>Deterioration Major Source Construction Permit</u> for the increase in operation of the existing simple combustion turbines. The facility is located on <u>Latitude</u>, <u>Longitude</u>: <u>39.333</u>, <u>-81.365</u>, <u>10319 South Pleasants Highway</u>, <u>St. Marys</u>, in <u>Pleasants</u> County, West Virginia.

The applicant estimates the potential to discharge the following Regulated Air Pollutants will be: <u>NO_x:</u> 464.6 tpy, CO: 471.1 tpy, VOC: 20.3 tpy, SO₂: 37.2 tpy, PM₁₀: 83.3 tpy, Total HAPs: 5.3 tpy

Startup of operation is planned to begin on or about the <u>First</u> day of <u>March</u>, <u>2018</u>. Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1250, during normal business hours.

Dated this the 16 day of October, 2017.

By: Pleasants Energy, LLC

Gerald Gatti
Plant Manager
10319 South Pleasants Highway
St. Marys, WV 26170

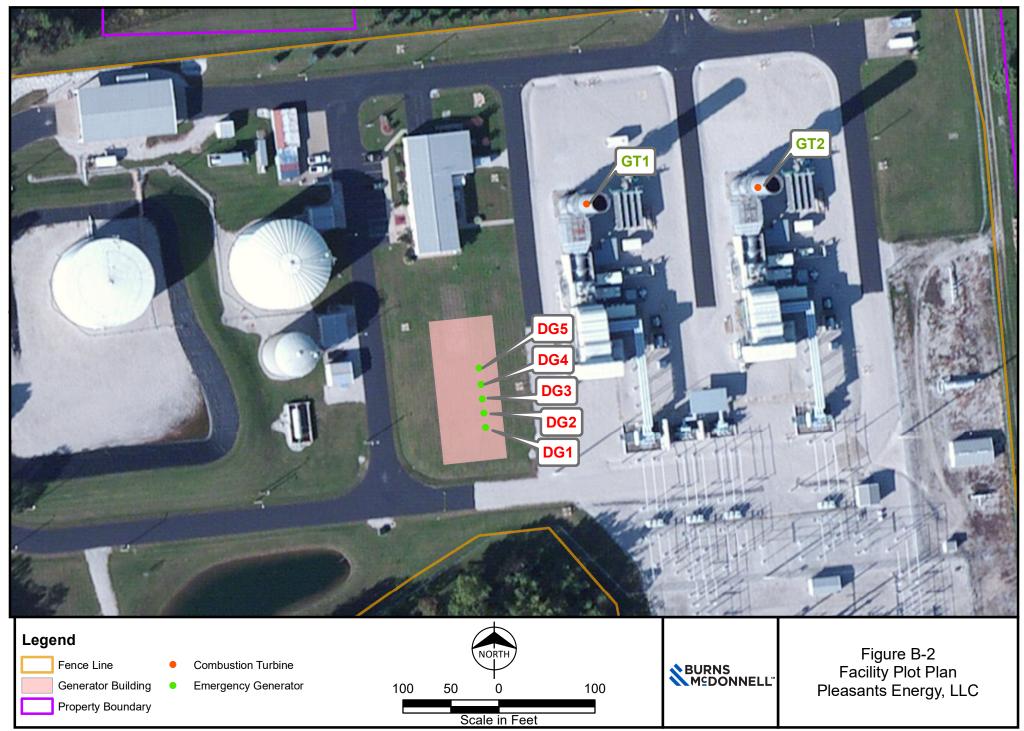
ATTACHMENT R - AUTHORITY FORM

AUTHORITY OF LIMITED LIABILITY COMPANY (LLC)

TO:

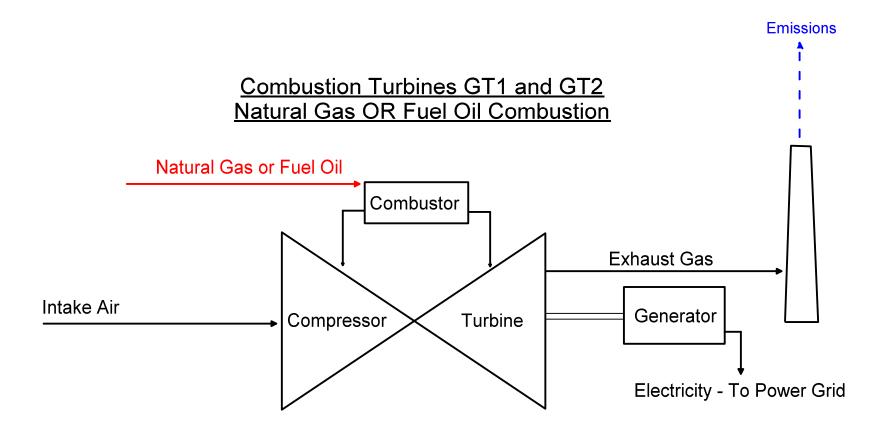
TO:	The West Virginia Departme	ent of Environmental Protection, Division of Air Quality
DATE:	<u>September 18, 2017</u>	
ATTN:	Director	
LLC's Federa	al Employer I.D. Number <u>26-36</u>	503167
Quality, a per	ndersigned hereby files with th rmit application and hereby ce n unincorporated business.	e West Virginia Department of Environmental Protection, Division of Air rtifies that the said name is a trade name which we are using in the
Furthe	er, we have agreed or certified	as follows:
(1)	The undersigned is a member obligate and legally bind all of	er and in that capacity may represent the interests of the LLC and may current or future members and the LLC.
(2)	The LLC is authorized to do	business in the State of West Virginia.
(3)	The name and business add	ress of each member:
	Member: Address:	DP Generation, LLC 601 Travis Street, Suite 1400 Houston, Texas 77002 Telephone No.: 713-767-6400
	Member: Address:	Telephone No.:
	Member:	
	Address:	
		Telephone No.:
(4)	If any other persons become r way or if the business should	members of the undersigned or our relations as such be altered in any become incorporated, the undersigned will notify you promptly.
A.D	Lu	Address: 601 Travis Street, Suite 1400
MEMBER OF	LLC (Signature)	Houston, Texas 77002 Telephone No.: 713-767-6400
Heidi D. Lewis) <u>,</u>	
Vice President	t, Group General Counsel and	Assistant Secretary on behalf of DP Generation, LLC
MEMBER OF	LLC (Typed)	
Pleasants En	ergy, LLC	
		LIABILITY COMPANY=S NAME

APPENDIX B - FIGURES



Issued: 9/13/2017

Pleasants Energy, LLC Combustion Turbine Process Flow Diagram



→ Natural Gas or Fuel Oil





Figure B-4 Combustion Turbine Process Flow Diagram



Pleasants Energy, LLC - Uprate Project Overall Project Emissions Increase and Post-Project Facility Total Emissions

Project Emissions Estimates (Maximum Potential to Emit)

Pollutant	Emissions Each Combustion Turbine (tpy)	Total Project Emissions (tpy) ^{a,b}	PSD Significant Emission Rates
NOx	232.3	464.6	40
CO	235.5	471.1	100
PM	41.7	83.3	25
PM ₁₀	41.7	83.3	15
PM _{2.5}	41.7	83.3	10
VOC	10.1	20.3	40
SO2	18.6	37.2	40
Lead	0.0	6.5E-03	0.6
H ₂ SO ₄	3.0	6.0	7
CO2e	569,789	1,139,578	75,000
Total HAPs	2.6	5.3	

⁽a) Emissions are based on worst-case emissions from any operating scenario. Based on fuel limit of 19,082,000,000 SCF of gas plus fuel oil for both turbines combined. Includes startup and shutdown emissions.

Total Facility Emissions After Project (Existing and Project Sources)

	Existing E	missions	Project Emissions	Facility Total After Project
Pollutant	Diesel Generators (Five Generators) ^a (tpy)	Diesel Storage Tank (tpy)	Total Project Emissions (Combustion Turbines) (tpy)	Total Emissions (tpy)
NOx	1.2		464.6	465.8
CO	6.3		471.1	477.4
PM/PM10	0.2		83.3	83.5
PM ₁₀	0.2		83.3	83.5
PM _{2.5}	0.2		83.3	83.5
VOC	0.7	6.9E-04	20.3	21.0
SO2	1.3E-02		37.2	37.2
Lead			6.5E-03	6.5E-03
H ₂ SO ₄	2.0E-03		6.0	6.0
CO2e	1,170		1,139,578	1,140,748
Total HAPs	3.2E-02		5.3	5.3

⁽a) Emissions based on 5 diesel generators limited to 100 hours each.

⁽b) Numbers in bold indicate the PSD significance level is exceeded

Pleasants Energy, LLC - Uprate Project Operating Scenarios Emissions

Number of Combustion		T
Turbines (GT1 & GT2)	2	
Fuel Limit	19,082,000,000	scf/year
Fuel Oil factor	889	scf/gal fuel oil combusted
GT1 & GT2 Combustion		
Turbine Size (NG)	1,910	MMBtu/hr
Natural gas heating value	1,020	MMBtu/MMcf
#2 Fuel Oil heating value	0.14	MMBtu/gal
Fuel Oil Consumption Rate	14,748	gal/hr
Possible hours per turbine on natural gas only	5,096	hours
Maximum hours on fuel oil per turbine	260	hours
Hour per turbine on gas with a set 200 hours on fuel oil per turbine	3,696	hours
Hour per turbine on gas with a set 260 hours on fuel oil	3275	hours
Total Number of Starts (Natural Gas + Fuel Oil)	365	
Number of Natural Gas Starts Per Turbine	335	
Number of Fuel Oil Starts		
Per Turbine	30	

Limitations for Permit					
NOx	464.60	Tons Per Year			
SO2	39	Tons Per Year			
Total Fuel Limit (Both					
Turbines Combined)	19,082,000,000	SCF/Year			
Fuel Oil Limit (Both					
Turbines Combined)	7,668,885.71	gallons/year			

Pollutant	100% Load Natural Gas Emission Rate (lb/hr)	Natural Gas Startup Emission Rate (lb/hr)	Natural Gas Shutdown Emission Rate (lb/hr)	Fuel Oil 100% Load Emission Rate (lb/hr)	Fuel Oil Startup Emission Rate (lb/hr)	Fuel Oil Shutdown Emission Rate (lb/hr)
NOx	68.90	125.46	107.22	470.00	561.64	543.09
СО	33.90	386.33	146.33	76.00	234.37	199.68
PM/PM ₁₀ /PM _{2.5}	15.90	18.00	18.00	41.00	41.00	41.00
VOC	3.20	7.03	6.39	20.00	21.14	20.95
SO ₂	2.70	2.70	2.70	109.00	109.00	109.00
H ₂ SO ₄	0.41	0.41	0.41	17.70	17.70	17.70
Lead	-			0.02	0.03	0.03
CO ₂	223,380	223,380	223,380	336,657	336,657	336,657
N ₂ O	0.42	0	0	3	3	3
CH ₄	4.21	4	4	14	14	14
CO ₂ e	223,611	223,611	223,611	337,813	337,813	337,813

Pleasants Energy, LLC - Uprate Project **Operating Scenarios Emissions**

Natural Gas Only			Fuel	Oil	
Pollutant	Fuel Limit on Natural Gas Only per Turbine ^{a,b} (tpy)	Fuel Limit on Natural Gas Only Both Turbines ^{a,b} (tpy)	0 1	nours/year	
NOx	232.30	464.60	- 0	gal/yr	
CO	235.54	471.08	- 0	SCF/yr equivalent	
PM/PM ₁₀ /PM _{2.5}	41.67	83.33	- N	MMCF/yr	
VOC	10.13	20.26	•	-	
SO ₂	6.88	13.76		9,541,000,000	SC
H ₂ SO ₄	1.05	2.11		19,082,000,000.0	SC
Lead		_			
CO ₂	569,201	1,138,402			
N ₂ O	1.07	2.15			

21.45

1,139,578

SCF/yr per turbine SCF/yr both turbines combined

Natural Gas

9,541,000,000.0 SCF/yr

Approximate

5,096 hours/year 9,731,820 MMBtu/yr 9,541 MMCF/yr

10.73

569,789

2.57E-03

446,432

1.05

9.14

446,974

(b) NOx emissions are capped at 232.3 tpy per turbine

CH₄

CO₂e

Lead CO₂

N₂O

CH₄

CO₂e

Operating Scenario	perating Scenario			l Oil	Natura	l Gas
Pollutant	Annual Emissions Per Turbine ^{a,b} (tpy)	Annual Emissions Both Turbines Combined ^{a,b} (tpy)	200	hours/year	3696	hours/year
NOx	232.30	464.60	2,949,571	gal/yr	7,057,208	MMBtu/yr
CO	213.75	427.49	2,622,169,000	SCF/yr equivalent	6,919	MMCF/yr
PM/PM ₁₀ /PM _{2.5}	34.54	69.07	2,622.17	MMCF/yr	6,918,831,000.00	SCF/yr
VOC	9.78	19.55			-	
SO ₂	15.89	31.78		9,541,000,000	SCF/yr per turbine	
H ₂ SO ₄	2.53	5.07		19,082,000,000.00	SCF/yr both turbines c	ombined

5.13E-03

892,865

2.10

18.29

893,948

⁽a) Emissions include 335 start-up/shut-down events on natural gas per turbine

⁽a) Emissions include 335 start-up/shut-down events on natural gas and 30 start-up/shut-down events on fuel oil per turbine

⁽b) NOx emissions are capped at 232.3 tpy per turbine

Pleasants Energy, LLC - Uprate Project **Operating Scenarios Emissions**

Max Fuel Oil Scenario	Max Fuel Oil Scenario - 260 Hours per Turbine		Fue	l Oil	Natura	l Gas
Pollutant	Annual Emissions Per Turbine ^{a,b,c} (tpy)	Annual Emissions Both Turbines Combined (tpy) ^{a,b,c}	260	Approximate hours/year	3275	Approximate hours/year
NOx	232.30	464.60	3,834,443	-	6,254,824	•
CO	208.90	417.81	3,408,819,700	SCF/yr equivalent	6,132,180,300	SCF/yr
PM/PM ₁₀ /PM _{2.5}	32.43	64.85	3,408.82	MMCF/yr	6,132.18	MMCF/yr
VOC	9.71	19.41				
SO ₂	18.59	37.18		9,541,000,000	SCF/yr per turbine	
H ₂ SO ₄	2.98	5.96		19,082,000,000.00	SCF/yr both turbines of	ombined
Lead	3.26E-03	6.51E-03		7,668,885.71	gallons/yr both turbines	s combined
CO ₂	409,602	819,203				
N ₂ O	1.04	2.09				
CH₄	8.67	17.34				
CO ₂ e	410,130	820,259				

⁽a) Emissions include 335 start-up/shut-down events on natural gas and 30 start-up/shut-down events on fuel oil per turbine (b) Emissions based on 2,592.1 MMCF of fuel oil and 6,948.8 MMCF of natural gas per turbine

Maximum emissions from all three scenarios

Pollutant	Maximum Emissions per Turbine ^a (tpy)	Maximum Emissions Both Turbines (tpy) ^a
NOx	232.30	464.6
co	235.54	471.1
PM/PM ₁₀ /PM _{2.5}	41.67	83.3
VOC	10.13	20.3
SO ₂	18.59	37.2
H ₂ SO ₄	2.98	6.0
Lead	0.00	0.0
CO ₂	569,201	1,138,402
N ₂ O	1.07	2.1
CH ₄	10.73	21.5
CO₂e	569,789	1,139,578

⁽a) NOx emissions are capped at 232.3 tpy per turbine

⁽c) NOx emissions are capped at 232.3 tpy per turbine

Pleasants Energy, LLC - Uprate Project Natural Gas Potential Emissions for Turbines 1 & 2

GT1 & GT2 Combustion		
Turbine Size	1,910	MMBtu/hr
Number of Combustion		
Turbines (GT1 & GT2)	2	
Natural Gas Operation	4,900	Hours per turbine
Number of Natural Gas		May include up to 30
Starts Per Turbine	365	starts on fuel oil.
Natural gas heating		
value	1,020	MMBtu/MMcf

Natural Gas Operation Emissions (lb/hr)

	100% Load Natural Gas	100% Load Natural	80% Load Natural Gas Emission	60% Load Natural Gas Emission	Natural Gas Start-up	Natural Gas Shutdown
	Emission Rate	Gas Emission Rate	Rate ^a	Rate ^a	Emissions ^b	Emissions ^c
Pollutant	(lb/MMBtu)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)	(lb/hr)
NOx		68.9	54	44	125.5	107.2
CO		33.9	26	22	386.3	146.3
PM/PM ₁₀ /PM _{2.5}		15.9	15.9	15.9	18.0	18.0
VOC		3.2	2.4	3	7.0	6.4
SO ₂		2.7			2.7	2.7
H ₂ SO ₄		0.41			0.41	0.41
Lead		-				
CO ₂	117.0	223,380			223,380	223,380
N ₂ O	2.20E-04	0.42			0.42	0.42
CH ₄	2.20E-03	4.21			4.2	4.2
CO₂e		223,611			223,611	223,611

- (a) For modeling purposes only(b) Assumes start-up is 120 minutes.(c) Assumes shut-down is 60 minutes.

Pleasants Energy, LLC - Uprate Project Natural Gas Potential Emissions for Turbines 1 & 2

Natural Gas Only Startup/Shutdown Emissions

Pollutant	Start-up Emissions (lb/hr)	Shutdown Emissions (lb/hr)	Number of Starts Per Turbine	Start- up/Shutdown Emissions (tpy)	Total Start- up/Shutdown Emissions (Both turbines) (tpy)
NOx ^a	125.5	107.2	365	65.4	130.7
CO ^a	386.3	146.3	365	167.7	335.4
PM/PM ₁₀ /PM _{2.5}	15.9	15.9	365	8.7	17.4
VOC ^a	7.0	6.4	365	3.7	7.5
SO ₂	2.7	2.7	365	1.5	3.0
H ₂ SO ₄	0.41	0.41	365	0.23	0.45
Lead					
CO ₂	223,380	223,380	365	122,300	244,601
N ₂ O	0.42	0.42	365	0.23	0.46
CH ₄	4.21	4.21	365	2.30	4.61
CO₂e	223,611	223,611	365	122,427	244,854

⁽a) Startup emissions based on CEMS data, and vendor load and startup profiles

Natural Gas Plus Fuel Oil Startup/Shutdown Emissions

Pollutant	Number of Natural Gas Starts Per Turbine	Start-up/Shutdown Emissions Natural Gas (tpy)		Start-up/Shut down Emissions Fuel Oil (tpy)	Total Start- up/Shutdown Emissions (Both turbines) (tpy) ^a
Nox	335	60.0	30	25.0	170.0
CO	335	153.9	30	10.0	327.9
PM/PM ₁₀ /PM _{2.5}	335	8.0	30	1.8	19.7
VOC	335	3.4	30	0.9	8.7
SO ₂	335	1.4	30	4.9	12.5
H ₂ SO ₄	335	0.21	30	0.80	2.0
Lead	335		20	8.7E-04	0.002
CO ₂	335	112,248	30	15,150	254,796
N ₂ O	335	0.21	30	0.12	0.67
CH₄	335	2.12	30	0.61	5.46
CO₂e	335	112,364	30	15,202	255,132

⁽a) Includes 335 start-up/shut down on natural gas and 30 start-up/shut down on fuel oil to meet total of 365 starts per year.

Stack Parameters for Combustion Turbines on Natural Gas

	Height	Temp.	Velocity	Diameter		Stack Discharge	
Scenario	(feet)	(F)	(feet/sec)	(feet)	ACFM	Type	Fuel
100% Load Natural Gas							
Operation	114.5	1131	148.2	18.00	2,260,000	Vertical	Natural Gas
80% Load Natural Gas							
Operation ^a	114.5	1097	139.58	18		Vertical	Natural Gas
60% Load Natural Gas							
Operation ^b	114.5	1143	130.96	18		Vertical	Natural Gas

⁽a) 80% Load stack parameters are also used for Start-up stack parameters. 80% load stack parameters from original permit application

⁽b) Includes shutdown emissions from "startup summary" plus an additional hour of normal emissions.

⁽b) 60% Load velocity is a 60% ratio of the 100% load velocity

Pleasants Energy, LLC - Uprate Project Fuel Oil Potential Emissions for Turbines 1 & 2

GT1 & GT2 Combustion		
Turbine Size	2,065	MMBtu/hr
Number of Combustion		
Turbines (GT1 & GT2)	2	
		Hours per turbine per
Fuel Oil Operation (Maximum)	260	year
Number of Fuel Oil Starts Per		
Turbine	30	
#2 Fuel Oil heating value	0.14	MMBtu/gal
Fuel Consumption Rate	14,748	gal/hr

Fuel Oil Operation Emissions (lb/hr)

Pollutant	100% Load Fuel Oil Emission Rate (lb/MMBtu)	100% Load Fuel Oil Emission Rate (lb/hr)	80% Load Fuel Oil Emission Rate ^a (lb/hr)	60% Load Fuel Oil Emission Rate ^a (lb/hr)	Start-up Emissions (lb/hr) ^b	Shutdown Emissions (lb/hr) ^c
NO _x		470	391	240	561.6	543.1
CO		76	53	49	234.4	199.7
PM/PM ₁₀ /PM _{2.5}		41	39	39	41.0	41.0
VOC		20	20	20	21.1	21.0
SO ₂		109	87		109.0	109.0
H ₂ SO ₄		17.7			17.7	17.7
Lead	1.4E-05	0.02			0.03	0.03
CO ₂	163.1	336,657			336,657	336,657
N ₂ O	1.32E-03	2.7			2.7	2.7
CH ₄	6.61E-03	13.7			13.7	13.7
CO ₂ e	-	337,813			337,813	337,813

⁽a) For modeling purposes only

⁽b) Assumes start-up is 120 minutes.

⁽c) Assumes shut-down is 60 minutes

Pleasants Energy, LLC - Uprate Project Fuel Oil Potential Emissions for Turbines 1 & 2

Fuel Oil Startup Emissions

Pollutant	Start-up Emissions (lb/hr) ^a	Shutdown Emissions (lb/hr) ^b	Number of Starts Per Turbine	Start- up/Shutdown Emissions (tpy)	Total Start- up/Shutdown Emissions (Both turbines) (tpy)
NOx	561.6	543.1	30	25.0	50.0
CO	234.4	199.7	30	10.0	20.1
PM/PM10/PM2.5	41.0	41.0	30	1.8	3.7
VOC	21.1	21.0	30	0.9	1.9
SO2	109.0	109.0	30	4.9	9.8
H2SO4	17.7	17.7	30	0.80	1.6
Lead	0.03	0.03	20	8.7E-04	1.7E-03
CO2	336,657	336,657	30	15,150	30,299
N2O	2.7	2.7	30	0.12	0.25
CH4	13.7	13.7	30	0.61	1.23
CO2e	337,813	337,813	30	15,202	30,403

⁽a) Startup emissions based on CEMS data, and vendor load and startup profiles

Stack Parameters

Scenario	Height (feet)	Temp. (F)	Velocity (feet/sec)	Diameter (feet)	ACFM	Stack Discharge Type	Fuel
100% Load Natural Gas						Vartical	Fuel Oil
Operation	114.5	1131	148.2	18.00	2,260,000	Vertical	ruei Oii
80% Load Natural Gas						Montheal	FI O.'I
Operation ^a	114.5	1158	141.66	18.00		Vertical	Fuel Oil
60% Load Natural Gas						Montheal	FI O'I
Operation ^b	114.5	1145	135.1	18.00		Vertical	Fuel Oil

⁽a) 80% Load stack parameters are also used for Start-up stack parameters. 80% load stack parameters from original permit application

⁽b) Includes shutdown emissions from "startup summary" for 30 minutes and one hour of full load emissions.

Pleasants Energy, LLC - Uprate Project H₂SO₄ Emissions

Combustion Turbine (one unit, fuel oil)

Sulfuric Acid Mist Emissions

Assume 10% of SO2 is converted to SO3 SO2 + 1/2 O2 = SO310 Assume 100% of SO3 is converted to H2SO4 100 SO3 + H2O = H2SO4 One unit lb/hr SO2 lb/hr H2SO4 converted to lb/hr SO2 SO3 lb/hr SO3 created created tons / year H2SO4 Tier IV Diesel Generator (one unit) 0.053 0.0081 0.00041 0.0053 0.0066 Combustion Turbine (one unit, natural gas) 2.700 0.2700 0.3374 0.4134 1.0

10.90

109.0

Conversion Percent

16.6874

Total H2SO4

13.6222

2.2

3.18

Molecular Weights									
SO2	64.0638								
SO3	80.0632								
H2SO4	98.07848								

Pleasants Energy, LLC - Uprate Project

HAPs Emissions - Existing and Project Emissions for Natural Gas Only Operation

Hours of Operation

Combustion Turbine Natural Gas Operation (2) = 5,096 hours per year per combustion turbine Combustion Turbine Fuel Oil Operation (2) = 0 hours per year per combustion turbine Tier IV Diesel Generator (5) = 100 hours per year per generator

Fuel Usage

Generators - Diesel		hp	mmBtu/hr	
	Tier IV Diesel Generator =	4,376	28.6	
	Number of diesel generators =	5		
Combustion Turbines		mmBtu/hr	mmCF/hr	1,020 MMBtu/MMcf
				Gas heat content value from AP-42
	Natural Gas Operation (Each) =	1,910	1.872	Section 1.4, updated 7/98
	Fuel Oil Operation (each) =	2,065		
	Number of Combustion Turbines =	2		

Project HAPs (Natural Gas O		
	Maximum Potential Emissions	
HAP	tpy	
Formaldehyde	1.97	Largest HAP
Toluene	1.27	2nd Largest
Xylene	0.62	3rd Largest
TOTAL Project HAPs	4.77	7
*Natural Gas Only is Worst Case Scenario		

Total Facility HAPs (Existing + Project)								
	Maximum Potential Emissions							
HAP	tpy							
Formaldehyde	1.97							
Toluene	1.27							
Xylene	0.62							
TOTAL Facility HAPs	4.80							

*Natural Gas	Only is	Worst	Case	Scena
--------------	---------	-------	------	-------

			Existing HAPS						Project Emissions								
				Fuel Oil - Diesel Generators				Natural Gas- Combustion Turbines				Fuel Oil - Combustion Turbines				Totals	
			Emission Factor ^a		Generator	Combined Generator Emissions (5 Generators)	Total Existing HAPS	Emission Factor ^b	One Combustion	Turbine Emissions	Combined Combustion Turbine Emissions(2)	Emission Factor ^b	One Combust Emiss		Combined Combustion Turbine Emissions (2)	Total Project HAPS	Total Facility HAPs (Existing - Project)
Chemical	CAS	POM?	(lb/MMBtu)	(lb/hr)	(tpy)	(tpy)	(tpy)	(lb/MMBtu)	(lb/hr)	(tpy)	(tpy)	(lb/MMBtu)	(lb/hr)	(tpy)	(tpy)	(tpy)	(tpy)
cenaphthene	83-32-9	POM	4.68E-06	1.34E-04	6.69E-06	3.35E-05	3.3E-05									0.00E+00	3.35E-05
cenaphthylene	203-96-8	POM	9.23E-06	2.64E-04	1.32E-05	6.60E-05	6.6E-05									0.00E+00	6.60E-05
cetaldehyde	75-07-0		2.52E-05	7.21E-04	3.60E-05	1.80E-04	1.8E-04	4.0E-05	7.6E-02	1.9E-01	3.9E-01					3.89E-01	0.39
crolein	107-02-8		7.88E-05	2.25E-03	1.13E-04	5.64E-04	5.6E-04	6.4E-06	1.2E-02	3.1E-02	6.2E-02					6.23E-02	6.28E-02
nthracene	120-12-7	POM	1.23E-06	3.52E-05	1.76E-06	8.80E-06	8.8E-06									0.00E+00	8.80E-06
rsenic												1.10E-05	2.3E-02	0.0E+00	0.0E+00	0.00E+00	0.00E+00
Benz(a)anthracene	56-55-3	POM	6.22E-07	1.78E-05	8.90E-07	4.45E-06	4.4E-06									0.00E+00	4.45E-06
Benzene	71-43-2		7.76E-04	2.22E-02	1.11E-03	5.55E-03	5.5E-03	1.2E-05	2.3E-02	5.8E-02	1.2E-01	5.5E-05	1.1E-01	0.0E+00	0.0E+00	1.17E-01	1.22E-01
Benzo(a)pyrene	50-32-8	POM	2.57E-07	7.35E-06	3.68E-07	1.84E-06	1.8E-06									0.00E+00	1.84E-06
enzo(b)fluoranthene	205-99-2	POM	1.10E-06	3.15E-05	1.57E-06	7.87E-06	7.9E-06									0.00E+00	7.87E-06
enzo(g,h,I)perylene	191-24-2	POM	5.56E-07	1.59E-05	7.95E-07	3.98E-06	4.0E-06									0.00E+00	3.98E-06
enzo(k)fluoranthene	205-82-3	POM	2.18E-07	6.24E-06	3.12E-07	1.56E-06	1.6E-06									0.00E+00	1.56E-06
eryllium												3.10E-07	6.4E-04	0.0E+00	0.0E+00	0.00E+00	0.00E+00
,3-Butadiene	106-99-0							4.3E-07	8.2E-04	2.1E-03	4.2E-03	1.6E-05	3.3E-02	0.0E+00	0.0E+00	4.18E-03	4.18E-03
Cadmium												4.80E-06	9.9E-03	0.0E+00	0.0E+00	0.00E+00	0.00E+00
Chromium												1.10E-05	2.3E-02	0.0E+00	0.0E+00	0.00E+00	0.00E+00
Chrysene	218-01-9	POM	1.53E-06	4.38E-05	2.19E-06	1.09E-05	1.1E-05									0.00E+00	1.09E-05
Dibenzo(a,h)anthracene	53-70-3	POM	3.46E-07	9.90E-06	4.95E-07	2.47E-06	2.5E-06									0.00E+00	2.47E-06
Ethyl benzene	100-41-4							3.2E-05	6.1E-02	1.6E-01	3.1E-01					3.11E-01	3.11E-01
Fluoranthene	206-44-0	POM	4.03E-06	1.15E-04	5.76E-06	2.88E-05	2.9E-05									0.00E+00	2.88E-05
Fluorene	86-73-7	POM	1.28E-05	3.66E-04	1.83E-05	9.15E-05	9.2E-05									0.00E+00	9.15E-05
Formaldehyde	500-00-0		7.89E-05	2.26E-03	1.13E-04	5.64E-04	5.6E-04	2.0E-04	3.9E-01	9.8E-01	2.0E+00	2.8E-04	5.8E-01	0.0E+00	0.0E+00	1.97E+00	1.97
ndeno(1,2,3-cd)pyrene	193-39-5	POM	4.14E-07	1.18E-05	5.92E-07	2.96E-06	3.0E-06		0.02				0.00	010=100	0.02	0.00E+00	2.96E-06
Manganese												7.9E-04	1.6E+00	0.0E+00	0.0E+00	0.00E+00	0.00E+00
Mercury												1.20E-06	2.5E-03	0.0E+00	0.0E+00	0.00E+00	0.00E+00
Naphthalene	91-20-3		1.30E-04	3.72E-03	1.86E-04	9.30E-04	9.3E-04	1.3E-06	2.5E-03	6.3E-03	1.3E-02	3.5E-05	7.2E-02	0.0E+00	0.0E+00	1.27E-02	1.36E-02
Vickel												4.60E-06	9.5E-03	0.0E+00	0.0E+00	0.00E+00	0.00E+00
PAH								2.2E-06	4.2E-03	1.1E-02	2.1E-02	4.0E-05	8.3E-02			2.14E-02	2.14E-02
Phenanathrene	85-01-8	POM	4.08E-05	1.17E-03	5.84E-05	2.92E-04	2.9E-04									0.00E+00	2.92E-04
Propylene	333.3	1	2.79E-03	7.98E-02	3.99E-03	2.00E-02	2.0E-02									0.00E+00	2.00E-02
Pyrene	129-00-0	POM	3.71E-06	1.06E-04	5.31E-06	2.65E-05	2.7E-05									0.00E+00	2.65E-05
Selenium	.20 00 0	. 5	5 12 00		5.572 00							2.50E-05	5.2E-02	0.0E+00	0.0E+00	0.00E+00	0.00E+00
Toluene	108-88-3		2.81E-04	8.04E-03	4.02E-04	2.01E-03	2.0E-03	1.3E-04	2.5E-01	6.3E-01	1.3E+00	2.002 00	5.22 02	5.52.50	3.32.00	1.27E+00	1.27
Xylene	1330-20-7	<u> </u>	1.93E-04	5.52E-03	2.76E-04	1.38E-03	1.4E-03	6.4E-05	1.2E-01	3.1E-01	6.2E-01					6.23E-01	6.24E-01
′	TOTAL	1		0.13	0.01	0.03	3.2E-02		0.94	2.39	4.77		2.63	0.00	0.00	4.77	4.80

(a) Emission factors from AP-42, Section 3.4, 6/1996

(b) Emission factors for combustion turbines from AP-42 Section 3.1, Updated 4/2000. Natural gas formaldehyde emission factor from Sims Roy EPA Memo "Hazardous Air Pollutant (HAP) Emission Control Technology for New Stationary Combustion Turbines" 8/21/2001.

Pleasants Energy, LLC - Uprate Project
HAPs Emissions - Existing and Project Emissions for Natural Gas and Fuel Oil Operation

Hours of Operation		
Combustion Turbine Natural Gas Operation (2) =	3,275	hours per year per combustion turbine
Combustion Turbine Fuel Oil Operation (2) =	260	hours per year per combustion turbine
Tier IV Diesel Generator (5) =	100	hours per year per generator

Fuel Usage

Generators - Diesel	hp	mmBtu/hr	
Tier IV Diesel Generator =	4,376	28.6	
Number of diesel generators =	5		
Combustion Turbines	mmBtu/hr	mmCF/hr	1,020 MMBtu/MMcf
Compastion Furbines	mmbta/m	11111017111	Gas heat content value from AP-42 Section
Natural Gas Operation (Each) =	1,910	1.872	1.4, updated 7/98
Fuel Oil Operation (each) =	2,065		•
Number of Combustion Turbines =	2		

Project HAPs (Natural Gas and Fuel Oil)							
	Maximum Potential Emissions						
HAP	tpy						
Formaldehyde	1.41						
Toluene	0.81						
Manganese	0.42						
TOTAL Project HAPs	3.75						

	Total Facility HAPs (Existing +	Project)
		Maximum
		Potential Emissions
	HAP	tpy
Largest HAP	Formaldehyde	1.41
2nd Largest	Toluene	0.82
3rd Largest	Manganese	0.42
	TOTAL Facility HAPs	3.78
_		

*Natural Gas Only is Worst Case Scenario

			Existing HAPS				Project Emissions										
				esel Generators			Natural Gas- Inte	-	Fuel Oil - Internal Combustion				Totals				
	CAS		Emission Factor ^a (lb/MMBtu)	One G	enerator (tpy)	Combined Generator Emissions (5 Generators) (tpy)	Total Existing HAPS (tpy)	Emission Factor ^b (lb/MMBtu)	One Combustion (lb/hr)	Turbine Emissions	Combined Combustion Turbine Emissions(2) (tpy)	Emission Factor ^b (lb/MMBtu)	One Combustion T	Furbine Emissions (tpy)	Combined Combustion Turbine Emissions (2) (tpy)	Total Project HAPS (tpy)	Total Facility HAPs (Existing + Project (tpy)
Chemical Acenaphthene	83-32-9	POM? POM	4.68E-06	1.34E-04	6.69E-06	3.35E-05	3.3E-05	(IS/IIIIISta)	(ID/III)	(tpy)	(гру)	(ID/IVIIVIBLU)	(15/111)	(tpy)	(tpy)	(tpy)	3.35E-05
Acenaphthylene	203-96-8	POM	9.23E-06	2.64E-04	1.32E-05	6.60E-05	6.6E-05										6.60E-05
Acetaldehyde	75-07-0	1 OW	2.52E-05	7.21E-04	3.60E-05	1.80E-04	1.8E-04	4.0E-05	7.6E-02	1.3E-01	2.5E-01					2.50E-01	0.25
Acrolein	107-02-8		7.88E-05	2.25E-03	1.13E-04	5.64E-04	5.6E-04	6.4E-06	1.2E-02	2.0E-02	4.0E-02					4.00E-02	4.06E-02
Anthracene	120-12-7	POM	1.23E-06	3.52E-05	1.76E-06	8.80E-06	8.8E-06	0.4E 00	1.22 02	2.02 02	4.02 02					4.00L 0L	8.80E-06
Arsenic	120 12 7	1 OW	1.202 00	0.022 00	1:702 00	0.002 00	0.02 00		 			1.10E-05	2.3E-02	3.0E-03	5.9E-03	5.91E-03	5.91E-03
Benz(a)anthracene	56-55-3	POM	6.22E-07	1.78E-05	8.90E-07	4.45E-06	4.4E-06					1.102 00	2.02 02	3.02 00	3.3L 30	0.012 00	4.45E-06
Benzene	71-43-2	i Oivi	7.76E-04	2.22E-02	1.11E-03	5.55E-03	5.5E-03	1.2E-05	2.3E-02	3.8E-02	7.5E-02	5.5E-05	1.1E-01	1.5E-02	3.0E-02	1.05E-01	1.10E-01
Benzo(a)pyrene	50-32-8	POM	2.57E-07	7.35E-06	3.68E-07	1.84E-06	1.8E-06	1122 00	2.02 02	0.02 02	7.02.02	0.02 00	1112 01	1102 02	0.02 02	11002 01	1.84E-06
Benzo(b)fluoranthene	205-99-2	POM	1.10E-06	3.15E-05	1.57E-06	7.87E-06	7.9E-06										7.87E-06
Benzo(g,h,l)perylene	191-24-2	POM	5.56E-07	1.59E-05	7.95E-07	3.98E-06	4.0E-06										3.98E-06
Benzo(k)fluoranthene	205-82-3	POM	2.18E-07	6.24E-06	3.12E-07	1.56E-06	1.6E-06										1.56E-06
Beryllium				U.L. 1	U. U							3.10E-07	6.4E-04	8.3E-05	1.7E-04	1.66E-04	1.66E-04
1,3-Butadiene	106-99-0							4.3E-07	8.2E-04	1.3E-03	2.7E-03	1.6E-05	3.3E-02	4.3E-03	8.6E-03	1.13E-02	1.13E-02
Cadmium	13333								VIII VIII	110_		4.80E-06	9.9E-03	1.3E-03	2.6E-03	2.58E-03	2.58E-03
Chromium												1.10E-05	2.3E-02	3.0E-03	5.9E-03	5.91E-03	5.91E-03
Chrysene	218-01-9	POM	1.53E-06	4.38E-05	2.19E-06	1.09E-05	1.1E-05										1.09E-05
Dibenzo(a,h)anthracene	53-70-3	POM	3.46E-07	9.90E-06	4.95E-07	2.47E-06	2.5E-06										2.47E-06
Ethyl benzene	100-41-4							3.2E-05	6.1E-02	1.0E-01	2.0E-01					2.00E-01	2.00E-01
Fluoranthene	206-44-0	POM	4.03E-06	1.15E-04	5.76E-06	2.88E-05	2.9E-05										2.88E-05
Fluorene	86-73-7	POM	1.28E-05	3.66E-04	1.83E-05	9.15E-05	9.2E-05										9.15E-05
Formaldehyde	500-00-0		7.89E-05	2.26E-03	1.13E-04	5.64E-04	5.6E-04	2.0E-04	3.9E-01	6.3E-01	1.3E+00	2.8E-04	5.8E-01	7.5E-02	1.5E-01	1.41E+00	1.41
Indeno(1,2,3-cd)pyrene	193-39-5	POM	4.14E-07	1.18E-05	5.92E-07	2.96E-06	3.0E-06										2.96E-06
Manganese												7.9E-04	1.6E+00	2.1E-01	4.2E-01	4.24E-01	4.24E-01
Mercury												1.20E-06	2.5E-03	3.2E-04	6.4E-04	6.44E-04	6.44E-04
Naphthalene	91-20-3		1.30E-04	3.72E-03	1.86E-04	9.30E-04	9.3E-04	1.3E-06	2.5E-03	4.1E-03	8.1E-03	3.5E-05	7.2E-02	9.4E-03	1.9E-02	2.69E-02	2.78E-02
Nickel												4.60E-06	9.5E-03	1.2E-03	2.5E-03	2.47E-03	2.47E-03
PAH								2.2E-06	4.2E-03	6.9E-03	1.4E-02	4.0E-05	8.3E-02	1.1E-02	2.1E-02	3.52E-02	3.52E-02
Phenanathrene	85-01-8	POM	4.08E-05	1.17E-03	5.84E-05	2.92E-04	2.9E-04										2.92E-04
Propylene			2.79E-03	7.98E-02	3.99E-03	2.00E-02	2.0E-02										2.00E-02
Pyrene	129-00-0	POM	3.71E-06	1.06E-04	5.31E-06	2.65E-05	2.7E-05										2.65E-05
Selenium												2.50E-05	5.2E-02	6.7E-03	1.3E-02	1.34E-02	1.34E-02
Toluene	108-88-3		2.81E-04	8.04E-03	4.02E-04	2.01E-03	2.0E-03	1.3E-04	2.5E-01	4.1E-01	8.1E-01					8.13E-01	0.82
Xylene	1330-20-7		1.93E-04	5.52E-03	2.76E-04	1.38E-03	1.4E-03	6.4E-05	1.2E-01	2.0E-01	4.0E-01					4.00E-01	4.02E-01
	TOTAL			0.13	0.01	0.03	0.03		0.94	1.53	3.07		2.63	0.34	0.68	3.75	3.78

(a) Emission factors from AP-42, Section 3.4, 6/1996

(b) Emission factors for combustion turbines from AP-42 Section 3.1, Updated 4/2000. Natural gas formaldehyde emission factor from Sims Roy EPA Memo "Hazardous Air Pollutant (HAP) Emission Control Technology for New Stationary Combustion Turbines" 8/21/2001.

Pleasants Energy, LLC - Uprate Project Total Existing and Project HAPs

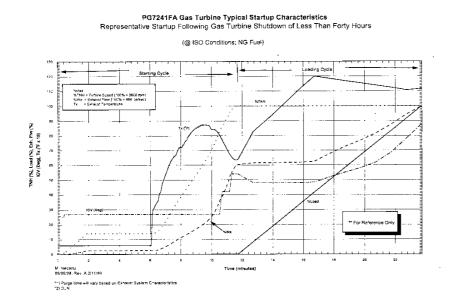
Facility HAPs						
	Maximum Potential Emissions					
HAP	tpy	1				
Formaldehyde	1.97	Li				
Acetaldehyde	0.39	2				
Ethyl benzene	0.31	3				
TOTAL Facility HAPs	5.29	1				

Largest HAP 2nd Largest 3rd Largest

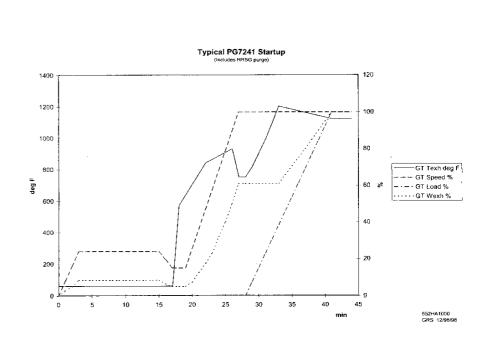
	Existing Emissions (5 diesel generators)	Turbines on Gas Only	FO & Gas Combination	Worst-Case Project Emissions	Worst-Case Facility Emissions
	HAPs	HAPs	HAPs	HAPs	HAPs
Chemical	tpy	tpy	tpy	tpy	tpy
Acenaphthene	3.35E-05	0.00	0.00	0.00	3.35E-05
Acenaphthylene	6.60E-05	0.00	0.00	0.00	6.60E-05
Acetaldehyde	1.80E-04	3.89E-01	2.50E-01	3.89E-01	3.89E-01
Acrolein	5.64E-04	6.23E-02	4.00E-02	6.23E-02	6.28E-02
Anthracene	8.80E-06	0.00	0.00	0.00	8.80E-06
Arsenic	0.00	0.00	5.91E-03	5.91E-03	5.91E-03
Benz(a)anthracene	4.45E-06	0.00	0.00	0.00	4.45E-06
Benzene	5.55E-03	1.17E-01	1.05E-01	1.17E-01	1.22E-01
Benzo(a)pyrene	1.84E-06	0.00	0.00	0.00	1.84E-06
Benzo(b)fluoranthene	7.87E-06	0.00	0.00	0.00	7.87E-06
Benzo(g,h,I)perylene	3.98E-06	0.00	0.00	0.00	3.98E-06
Benzo(k)fluoranthene	1.56E-06	0.00	0.00	0.00	1.56E-06
Beryllium	0.00	0.00	1.66E-04	1.66E-04	1.66E-04
1,3-Butadiene	0.00	4.18E-03	1.13E-02	1.13E-02	1.13E-02
	0.00	0.00	2.58E-03	2.58E-03	2.58E-03
Chromium	0.00	0.00	5.91E-03	5.91E-03	5.91E-03
Chrysene	1.09E-05	0.00	0.00	0.00	1.09E-05
Dibenzo(a,h)anthracene	2.47E-06	0.00	0.00	0.00	2.47E-06
Ethyl benzene	0.00	3.11E-01	2.00E-01	3.11E-01	3.11E-01
Fluoranthene	2.88E-05	0.00	0.00	0.00	2.88E-05
Fluorene	9.15E-05	0.00	0.00	0.00	9.15E-05
Formaldehyde	5.64E-04	1.97E+00	1.41	1.97	1.97
Indeno(1,2,3-cd)pyrene	2.96E-06	0.00	0.00	0.00	2.96E-06
Manganese	0.00	0.00	4.24E-01	4.24E-01	4.24E-01
Mercury	0.00	0.00	6.44E-04	6.44E-04	6.44E-04
Naphthalene	9.30E-04	1.27E-02	2.69E-02	2.69E-02	2.78E-02
Nickel	0.00	0.00	2.47E-03	2.47E-03	2.47E-03
PAH	0.00	2.14E-02	3.52E-02	3.52E-02	3.52E-02
Phenanathrene	2.92E-04	0.00	0.00	0.00	2.92E-04
Propylene	2.00E-02	0.00	0.00	0.00	2.00E-02
Proplylene Oxide	0.00	0.00	0.00	0.00	0.00
Pyrene	2.65E-05	0.00	0.00	0.00	2.65E-05
Selenium	0.00	0.00	1.34E-02	1.34E-02	1.34E-02
Toluene	2.01E-03	1.27	8.13E-01	1.27	1.27
Xylene	1.38E-03	6.23E-01	4.00E-01	6.23E-01	6.24E-01
TOTA	0.03	4.77	3.75	5.26	5.29

Pleasants Energy, LLC - Uprate Project Load Information

Warm start info



Cold start info



Pleasants Energy, LLC - Uprate Project Natural Gas Startup Summary

Scenario One Cold Start

Flame to Full Start No Load (FSNL)
CO 250 lbs
NOX 10 lbs

Emissions During Startup
VOC 3.83 lb
NOX 35.16 lb
CO 102.43 lb

Total Emissions

VOC 3.83 lb per start
CO 352.4 lb per start
NOX 45.16 lb per start

Scenario Two
Warm Start

Flame to Full Start No Load (FSNL) CO 250

10

Emissions During Startup VOC 3.19 lb NOX 29.32 lb CO 85.43 lb

Total Emissions

NOX

VOC 3.19 lb per start
CO 335.43 lb per start
NOX 39.32 lb per start

Shutdown

Assume Warm Start for Shutdown scenario

Full Start No Load (FSNL) to Flameout CO 27 lbs

NOX 9 lbs
Emissions During Shutdown

VOC 3.19 lb NOX 29.32 lb CO 85.43 lb

Total Emissions

VOC 3.19 lb per shutdown NOX 38.32 lb per shutdown CO 112.43 lb per shutdown

From Data Sheets:

VOC

Flame to Full Start No Load (FSNL) CO 250 lbs

CO 250 lbs NOX 10 lbs

СО

CO

NOX

Full Start No Load (FSNL) to Flameout

27 lbs

9 lbs

Percent Load Emissions (Rate of Change -1.466666667 18.5 0 9 5.3 95.5 10 100.8 -7.61 23 1.87 60.13 24 -8.375 62 28 28.5 -2.7 29 25.8

29 25.8 -1 39 15.8 0.144444444 48 17.1 0 50 17.1 50 1.84 0.0198 100 2.83

Scenario One: Cold Start Load = 0 28.055556 Load = 100 42.472222

Startup Rate = 0.1441667 minutes per load %

Scenario 2: Warm Start Load = 0 11.729412 Load = 100 23.752941

Startup Rate = 0.1202353 minutes per load %

Percent Lo Emissions Rate of Change Percent Lo Emissions Rate of Change 187.2 -0.133333 97.5 -2.5 0 0 9 186 1814 95 7.1625 1 10 -151.3462 2000 9 152.3 -49.4 23 32.5 1487.8 10 102.9 10.46923 24 1520.3 -102.45 23 239 -46.3 28 1110.5 24 192.7 -46.5 12.1 29 27 229 10.25 1064 -13.56667 32 1023.3 -9.441667 31 270 7.866667 44 910 40 340.8 11.02857 -10 47 46 890 -3.75 418 12.9 50 875 48 430.9 2.75 50 19.6 0.4 50 436.4 51 20 0.1666667 50 37 0.9 63 22 0.1428571 51 37.9 0.390323 82 70 23 0.2 50 0.444444 100 29 91 54 0.555556

100

59

NOX

Pleasants Energy, LLC - Uprate Project Fuel Oil Startup Summary

Scenario One Cold Start

Flame to Full Start No Load (FSNL)
CO 100 lbs
NOX 10 lbs

Emissions During Startup
VOC 1.14 lb
NOX 81.64 lb
CO 58.37 lb

Total Emissions

VOC 1.14 lb per start
NOX 91.64 lb per start
CO 158.4 lb per start

From Data Sheets:

Flame to Full Start No Load (FSNL)
CO 100 lbs
NOX 10 lbs

VOC

Percent Load Emissions (Rate of Change 25 0 -1.52 10 9.8 -0.62 20 3.6 -0.1 26 3 0 49 3 -1 50 2 0 60 2 0.025 100 3 0.03

Scenario One: Cold Start Load = 0 28.055556 Load = 100 42.472222

Startup Rate = 0.1441667 minutes per load %

Scenario 2: Warm Start Load = 0 11.729412 Load = 100 23.752941

Startup Rate = 0.1202353 minutes per load %

Scenario Two
Warm Start

Flame to Full Start No Load (FSNL) CO 75 NOX 5

Emissions During Startup VOC 0.95 lb NOX 68.09 lb CO 48.68 lb

Total Emissions

VOC 0.95 lb per start NOX 73.09 lb per start CO 123.68 lb per start Shutdown

Assume Warm Start for Shutdown scenario

Full Start No Load (FSNL) to Flameout

CO 75 lbs NOX 5 lbs Emissions During Shutdown

VOC 0.95 lb NOX 68.09 lb CO 48.68 lb

Total Emissions

VOC 0.95 lb per shutdown NOX 73.09 lb per shutdown CO 123.68 lb per shutdown

Full Start No Load (FSNL) to Flameout

CO 75 lbs NOX 5 lbs

CO NOX

Percent Lo Emissions Rate of Change Percent Lo Emissions Rate of Change 1040 -33.88889 0 0 108 1 18 430 -45 2 110 10 22 250 -5 10 190 18.5 26 -2.5 20 375 230 20 30 220 -3 22 415 16.25 40 190 -1 26 480 15 45 185 -1.25 30 540 17.5 49 40 715 180 -110 15.8 50 70 -0.04 46 810 13.3 100 68 49 850

Pleasants Energy, LLC - Existing Emissions Calculations Emergency Generators Emissions Estimate

Tier IV Diesel Generators (5)

Fuel Consumption, Each

Generator (100% load) 208.8 Gal/hr Heat Input, Each Generator 28.61 MMBtu/hr

Power Output, hp 4,376 hp
Power Output, kW 3000 kW
Sulfur Content of Fuel 0.0015 %

Displacement 5.29 L/cylinder

Annual Operation (per Engine) 100 hours/year (per engine)

Stack Parameters

Height (ft)	Temp. (F)	Velocity (ft/sec)	Diameter (ft)	ACFM	Stack Discharge Type	Fuel
45	882.2	124.98	2.00	23557.40	Vertical	Diesel

		Emission	Factors		Emissions (O	ne Engine)	Emissions (F	ive Engines)
Pollutant	lb/hp hr	g/hp-hr	lb/MMBtu	Source	lb/hr	tpy	lb/hr	tpy
NOx	1.10E-03	0.50		NSPS ^C	4.82	0.24	24.10	1.21
CO	5.75E-03	2.61		NSPS ^C	25.18	1.26	125.90	6.29
PM/PM ₁₀ /PM _{2.5}	1.6E-04	0.07		NSPS ^C	0.72	0.04	3.60	0.18
VOC	6.58E-04	0.30		NSPS ^C	2.88	0.14	14.39	0.72
SO ₂	1.21E-05	0.01		AP-42 ^A	0.05	2.66E-03	0.27	0.01
H ₂ SO ₄				Mass Balance	8.13E-03	4.06E-04	0.04	0.00
CO ₂			163.05	Part 98 ^B	4,664.26	233.21	23,321.28	1,166.06
N₂O			1.32E-03	Part 98 ^B	0.04	0.00	0.19	0.01
CH ₄			6.61E-03	Part 98 ^B	0.19	0.01	0.95	0.05
CO₂e					4,680.26	234.01	23,401.30	1170.07

^A AP-42 Section 3.4 (10/96) Table 3.4-1

NSPS Limits - 40 CFR Part 60, Subapart IIII, (40 CFR 60.4201(c) and 40 CFR 1039.102 - Table 7)

	NOx	СО	PM	NMHC
g/kW-hr	0.67	3.5	0.10	0.40
g/hp-hr	0.50	2.61	0.07	0.30

^B Greenhouse Gas Reporting Rule- Subpart C of Part 98

^C NSPS Subapart IIII Limits

Pleasants Energy, LLC - Existing Emissions Calculations Diesel Storage Tanks

Description:

Horizontal Fixed Roof Tanks

Assumptions for All tanks:

Weather - Columbus, Ohio data Type - Horizontal Fixed Roof Tank Color/Shade - White/White (Default)

Fuel - Distillate #2 Fuel Oil

Monthly Calculation - Throughput distributed evenly over the entire year

Generator Fuel Oil Tanks (1)

Size: 2500 gallons

VOC Emissions ¹ lb/yr tpy												
lb/yr	tpy											
1.37	6.9E-04											

¹ EPA TANKS program was run for VOC emissions from the fuel tank

Pleasants Energy, LLC - Uprate Project PSD Netting

Project Emissions Estimates (Maximum Potential to Emit)

	Past Actual	Future Potential	Net Emissions	PSD Significant
Pollutant	Emissions	Emissions	Increase	Emission Rates
NOx	126.0	464.6	338.6	40
CO	84.1	471.1	387.0	100
PM	39.6	83.3	43.8	25
PM ₁₀	13.6	83.3	69.7	15
PM _{2.5}	39.6	83.3	43.8	10
VOC	0.8	20.3	19.5	40
SO2	2.1	37.2	35.1	40
Lead	0.0	0.0	0.0	0.6
H ₂ SO ₄	0.9	6.0	5.0	7
CO2e	490,512	1,139,578	649,066	75,000

Unit 1 Past Actuals

Unit 1 Past	t Actuals																			
		Gross	Gas On-	Gas Heat	Oil Flow	Oil Heat	NG CO	FO CO	NG PM	FO PM	NG PM2.5	FO PM2.5	NG Lead	FO Lead	NG	FO	NG	FO	NG N2O	FO N2O
Year	Month	Output	Time	Input	On-Time Hours	Input MMBtu	lb/hr	lb/hr	lb/hr	lb/hr	Ib/hr	lb/hr	16 /A AA AB+	16 /0 40 4D+	H2SO4	H2SO4	Methane	Methane	16 /0 40 4D+	16 /A AA AB+
2012	lonuon:	MW-hrs	Hours	MMBtu	nours	IVIIVIBLU	,	-7	,	-,	•		lb/MMBtu	•	,	,		lb/MMBtu	,	,
	January February	1341	0.45 7.53	247.7 13272.7	0	0	33.9 33.9	76 76	15.9 15.9	41 41		41	(1.40E-05 1.40E-05	1	17.70 17.70	2.20E-03 2.20E-03			1.32E-03 1.32E-03
	March	2819	17.52	28391.2	0	0	33.9	76	15.9	41		41	`	1.40E-05 1.40E-05		17.70				1.32E-03
2012		2178	14.33	22551.4	0	0	33.9	76	15.9	41		41		1.40E-05		17.70				1.32E-03
2012		3726	25.06	38488.8	0	0	33.9	76	15.9	41		41				17.70				1.32E-03
2012		6662	46.21	69272.2	0	0	33.9	76	15.9	41		41	(1.40E-05		17.70	2.20E-03			1.32E-03
2012		14731	102.62	153320.5	0	0	33.9	76	15.9	41	15.9	41	(1.40E-05		17.70	2.20E-03			1.32E-03
	August	4633	29.87	43336.4	3.33	4770.6	33.9	76	15.9	41		41	(1.700 00		17.70	2.20E-03			1.32E-03
	September	0	0	0	0	0	33.9	76	15.9	41		41	(10⊑ 00		17.70				1.32E-03
	October	760	4.74		0	0	33.9	76	15.9	41		41		1.40E-05		17.70	2.20E-03			1.32E-03
	November	1103	7.26	11231.1	0	0	33.9	76	15.9	41		41	(1.700 00		17.70	2.20E-03			1.32E-03
	December January	1028	0	0	6.16	10667	33.9 33.9	76	15.9 15.9	41		41 41	(= 00		17.70 17.70	2.20E-03 2.20E-03			1.32E-03 1.32E-03
	February	1020	0	0	0.10	10007	33.9	76 76	15.9	41 41		41		1.40E-05 1.40E-05		17.70	2.20E-03 2.20E-03			1.32E-03
	March	0	0	0	0	0	33.9	76	15.9	41		41		_		17.70				1.32E-03
2013		4022	27.06	41656.9	0	0	33.9	76	15.9	41		41	(1.40E-05		17.70	2.20E-03			1.32E-03
2013		2208	16.73	23585.7	0.7	370.5	33.9	76	15.9	41		41	(1.40E-05		17.70	2.20E-03			1.32E-03
2013		12170	82.02	126373	0	0	33.9	76	15.9	41		41	(17.70	2.20E-03			1.32E-03
2013		27335	183.72	280953.7	0	0	33.9	76	15.9	41	15.9	41	(_		17.70				1.32E-03
2013	August	9536	62.97	95292.2	1.67	2407.3	33.9	76	15.9	41	15.9	41	(17.70	2.20E-03			1.32E-03
2013	September	5848	38.85	59764	0	0	33.9	76	15.9	41		41	(1.700 00		17.70	2.20E-03		2.20E-04	1.32E-03
	October	0	0	0	0	0	33.9	76	15.9	41		41	(10⊑ 00		17.70	2.20E-03			1.32E-03
	November	0	0	0	0	0	33.9	76	15.9	41		41	(1.40E-05		17.70	2.20E-03			1.32E-03
	December	1372	3.15		5.49	9276.5	33.9	76	15.9	41		41	(1.40E-05		17.70	2.20E-03			1.32E-03
	January	9325	0	0	55.12	97508.9	33.9	76	15.9	41		41	(17.70	2.20E-03			1.32E-03
	February	887	0	0	6.16	9647.6	33.9	76	15.9	41		41	(1. + 0L-03		17.70	2.20E-03			1.32E-03
2014	March	3755	0	0	21.32	38753.4	33.9 33.9	76 76	15.9	41		41	(1.40E-05		17.70 17.70	2.20E-03			1.32E-03 1.32E-03
2014		5776	39	59433	0	0	33.9	76 76	15.9 15.9	41 41		41 41	(7TOE 00		17.70	2.20E-03 2.20E-03			1.32E-03
2014		11901	83.9		0.14	48.1	33.9	76	15.9	41		41	,	1.40E-05		17.70	2.20E-03			1.32E-03
2014		27241	179.86		0.05	26.4	33.9	76	15.9	41		41	(1.40E-05		17.70	2.20E-03			1.32E-03
	August	32127	210.01	325016.3	2.46	3527.3	33.9	76	15.9	41		41	(17.70	2.20E-03			1.32E-03
	September	33752	218.35	338830.5	0	0	33.9	76	15.9	41		41	(_		17.70	2.20E-03			1.32E-03
	October	56894	351.1	568980.9	0.07	25.6	33.9	76	15.9	41		41	(1.40E-05		17.70	2.20E-03			1.32E-03
2014	November	12315	72.88	121600	2.03	30.1	33.9	76	15.9	41	15.9	41	(1.40E-05	0.41	17.70	2.20E-03	13.66		1.32E-03
2014	December	3684	21.75	36401.6	1.13	1625	33.9	76	15.9	41		41	(1.+0L 00		17.70	2.20E-03			1.32E-03
2015	,	4543	27.34	46524.3	0.69	224.2	33.9	76	15.9	41		41	(1.40E-05	0.41	17.70	2.20E-03			1.32E-03
	February	7628	0	0	42.48		33.9	76	15.9	41		41	(J 1 0L 00		17.70				1.32E-03
2015	March	23	0	0			33.9	76	15.9	41		41		1.40E-05		17.70			2.20E-04	
2015 2015		40667		414803.7	2 00		33.9	76	15.9	41		41				17.70				
2015		32911 48542		347502.9 509756.2			33.9 33.9	76 76	15.9 15.9	41 41		41 41		7: TOE 00		17.70 17.70				1.32E-03 1.32E-03
2015		76459		803664.3	2.44		33.9	76	15.9	41		41		_		17.70				1.32E-03
	August	67943	444.13		1.39		33.9	76	15.9	41				_		17.70				
	September	69143	448.11	712038			33.9		15.9	41						17.70				1.32E-03
	October	113388	691.04			0	33.9	76	15.9	41		41				17.70				1.32E-03
	November	20473	122.61	209789		293.6	33.9	76	15.9	41		41				17.70				1.32E-03
	December	40434	240.41	411758.1	1.84	2253.1	33.9	76	15.9	41	15.9			1.40E-05	0.41	17.70	2.20E-03	13.66	2.20E-04	1.32E-03
	January	5184	31.67	52650	0.66		33.9	76	15.9	41		41				17.70	2.20E-03	13.66		
	February	4872	28.98		0.88	492.2	33.9	76	15.9	41		41	(17.70				
	March	14563	90.54		0	0	33.9	76	15.9	41		41				17.70				1.32E-03
2016		17386	108.8		0.89		33.9	76	15.9	41						17.70				
2016		49156	305.36				33.9	76	15.9	41		41		1.102 00		17.70				1.32E-03
	June	26157	173.54	270745.2		349.5	33.9	76 76	15.9	41		41				17.70				1.32E-03
2016		1121	0	0			33.9		15.9	41						17.70				
	August	1130	115.22	Ū	0.00		33.9 33.9	76 76	15.9 15.9	41 41		41		7: TOE 00		17.70 17.70				1.32E-03 1.32E-03
	September October	18235 47523	115.33 287.3			0	33.9	76 76	15.9	41		41 41		_		17.70				1.32E-03
	November	156				798.1	33.9	76	15.9	41				_		17.70				
	December	108					33.9		15.9	41										
2010	Poocitibei	100	0.02	1070.5	0.40	004.4	55.8	70	10.0	71	10.9	+		1.TUL-UU	J. T I	17.70	uuu	10.00	004	1.026-00

Unit 1 Past Actuals

		NOv	60	DNA	DN410	DN42 F	VOC	503	Lood	H2SO4	Mathana	NZO	NOv		DNA	DN410	DN42 F	VOC	503	Lood	H3604	coa	Methane	NIZO	CO2e
Year	Month	NOx	со	PM	PM10	PM2.5	voc	SO2	Lead	H25U4	Methane	N2O	NOx	со	PM	PM10	PM2.5	voc	SO2	Lead	H2SO4	CO2	ivietnane	N2O	COZE
		lbs	lbs	lbs	lbs	lbs	lbs	lbs	lbs	lbs	lbs	lbs	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons
	January	42.1	15.26	7.16	0.7	7.16	0	0	0.00	0.05	0.55	0.05	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	14.7		0.0	14.
2012	February March	481.3 1046.7	255.27 593.93	119.73 278.57	44.9 94.3	119.73 278.57	2.7 5.6	0	0.00	2.93 6.26	29.26 62.59	2.93 6.26	0.2 0.5	0.1 0.3	0.1 0.1	0.0	0.1 0.1	0.0	0.0	0.0	0.0	788.9 1687	0.0	0.0	789. 1688.
2012		699.8	485.79	227.85	76.3	227.85	4.5	0	0.00	4.97	49.72	4.97	0.3	0.3	0.1	0.0	0.1	0.0	0.0	0.0	0.0	1340.1	0.0	0.0	1341.
2012		1088.5	849.53	398.45	130.5	398.45	7.7	0		8.49	84.85	8.49	0.5	0.4	0.2	0.1	0.2	0.0	0.0	0.0	0.0	2287.5		0.0	2289.
2012		2168	1566.52	734.74	233.9	734.74	13.8	0		15.27	152.72	15.27	1.1	8.0	0.4	0.1	0.4	0.0	0.0	0.0	0.0	4116.7	0.1	0.0	4120.
2012	- /	4386.2	3478.82	1631.66	516.1	1631.66	30.5	0	0.00	33.80	338.01	33.80	2.2	1.7	0.8	0.3	0.8	0.0	0.0	0.0	0.0	9111.2	0.2	0.0	9120.
	August September	2371.2	1265.67 0.00	611.46 0.00	161.4	611.46 0.00	10.7	107.5	0.07 0.00	15.86 0.00	65241.21 0.00	15.86 0.00	1.2 0.0	0.6 0.0	0.3	0.1 0.0	0.3	0.0	0.1	0.0	0.0	2962.3	32.6	0.0	3780. 0.
	October	280.3	160.69	75.37	24.3	75.37	1.4	0	0.00	1.64	16.36	1.64	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	441.2	0.0	0.0	441.
	November	499.5	246.11	115.43	38.1	115.43	2.2	0	0.00	2.48	24.76	2.48	0.2	0.1	0.1	0.0	0.1	0.0	0.0	0.0	0.0	667.5	0.0	0.0	668.
2012	December	0	0.00	0.00	0	0.00	0	0	0.00	0.00	0.00	0.00	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0	0.0	0.0	0.
2013	January	2297.6	468.16	252.56	39.8	252.56	5.3	240.8	0.15	14.11	145664.88	14.11	1.1	0.2	0.1	0.0	0.1	0.0	0.1	0.0	0.0	865.6		0.0	2688.
2013 2013	February	0	0.00	0.00	0	0.00	0	0	0.00	0.00	0.00	0.00	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0	0.0	0.0	0. 0.
2013		1366.3	917.33	430.25	140.5	430.25	8.2	0	0.00	0.00 9.18	0.00 91.84	0.00 9.18	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	2475.5	0.0	0.0	2478.
2013		1033	620.35	294.71	80.9	294.71	4.8	8.4	0.01	5.69	5111.42	5.69	0.5	0.3	0.1	0.0	0.1	0.0	0.0	0.0	0.0	1431.7	2.6	0.0	1496.
2013	June	4294.3	2780.48	1304.12	426.3	1304.12	24.8	0	0.00	27.86	278.60	27.86	2.1	1.4	0.7	0.2	0.7	0.0	0.0	0.0	0.0	7509.9	0.1	0.0	7517.
2013		9699.1	6228.11	2921.15	948.8	2921.15	55.8	0	0.00	61.94	619.40	61.94	4.8	3.1	1.5	0.5	1.5	0.0	0.0	0.0	0.0	16697.3	0.3	0.0	16714.
	August	3642.8	2261.60	1069.69	329	1069.69	19.9	54.2 0	0.03	24.19	33083.34	24.19	1.8	1.1 0.7	0.5	0.2	0.5	0.0	0.0	0.0	0.0	5858	16.5	0.0	6275. 3555.
	September October	1951.9	1317.02 0.00	617.72 0.00	202.7	617.72 0.00	11.9	0	0.00	13.18 0.00	131.76 0.00	13.18 0.00	1.0 0.0	0.7	0.3	0.1 0.0	0.3	0.0	0.0	0.0	0.0	3551.4	0.1	0.0	3555. 0.
	November	0	0.00	0.00	0	0.00	0	0	0.00	0.00	0.00	0.00	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0	0.0	0.0	0.
	December	1430.8	524.03	275.18	48.7	275.18	5.2	209.3	0.13	13.36		13.36	0.7	0.3	0.1	0.0	0.1	0.0	0.1	0.0	0.0	1044.8		0.0	2630.
	January	16427	4189.12	2259.92	360.6	2259.92	47.1	2200.2	1.37	128.98	1331547.93	128.98	8.2	2.1	1.1	0.2	1.1	0.0	1.1	0.0	0.1	7912.1	665.8	0.1	24575.
	February	1595.8	468.16	252.56	34.7	252.56	4.4	217.7	0.14	12.76	131744.30	12.76	8.0	0.2	0.1	0.0	0.1	0.0	0.1	0.0	0.0	782.8	65.9	0.0	2431.
2014 2014		6324	1620.32 0.00	874.12 0.00	144.2	874.12 0.00	18.3	874.3	0.54 0.00	51.26 0.00	529203.07 0.00	51.26 0.00	3.2 0.0	0.8	0.4	0.1 0.0	0.4	0.0	0.4	0.0	0.0	3144.5	264.6	0.0	9767. 0.
2014		2088.3	1322.10	620.10	198.8	620.10	11.7	0	0.00	13.10	131.03	13.10	1.0	0.0	0.0	0.0	0.3	0.0	0.0	0.0	0.0	3532		0.0	3535.
2014		4210.6	2854.85	1339.75	414.1	1339.75	24.3	1	0.00	27.22	928.42	27.22	2.1	1.4	0.7	0.2	0.7	0.0	0.0	0.0	0.0	7323.7	0.5	0.0	7339.
2014	. ,	9783.3	6101.05	2861.82	942.4	2861.82	55.2	0.6		61.71	977.27	61.71	4.9	3.1	1.4	0.5	1.4	0.0	0.0	0.0	0.0	16626	0.5	0.0	16647.
	August	12321.5	7306.30	3440.02	1111	3440.02	66.1	79		76.32	48884.13	76.32	6.2	3.7	1.7	0.6	1.7	0.0	0.0	0.0	0.0	19598.8	24.4	0.0	20221.
	September October	12154.9 18279	7402.07 11907.61	3471.77 5585.36	1141.5 1928.3	3471.77 5585.36	67.1 113.2	0.6	0.00	74.70 125.47	746.99 1603.97	74.70 125.47	6.1 9.1	3.7 6.0	1.7 2.8	0.6 1.0	1.7 2.8	0.0 0.1	0.0	0.0	0.0	20134.7 33815.5	0.4	0.0	20155. 33854.
	November	4102.2	2624.91	1242.02	409	1242.02	24	0.4	0.00	26.85	679.12	26.85	2.1	1.3	0.6	0.2	0.6	0.0	0.0	0.0	0.0	7229.2	0.3	0.0	7241.
	December	1590.9	823.21	392.16	126.8	392.16	7.9	36.4	0.02	10.17	22270.69	10.17	0.8	0.4	0.2	0.1	0.2	0.0	0.0	0.0	0.0	2295.2	11.1	0.0	2575.
2015	January	1540.1	979.27	463.00	158.5	463.00	9.3	4.9	0.00	10.55	3164.17	10.55	0.8	0.5	0.2	0.1	0.2	0.0	0.0	0.0	0.0	2783	1.6	0.0	2824.
	February	11457.2	3228.48	1741.68	294.1	1741.68	39.3	1773.7	1.11	104.85	1082407.33	104.85	5.7	1.6	0.9	0.1	0.9	0.0	0.9	0.0	0.1	6432.2	541.2	0.1	19977.
2015 2015		85.1 11358.6	62.32 8153.97	33.62 3824.43	1.4 1406.4	33.62 3824.43	0.2 82.7	1.7 0		0.59 91.45	6093.15 914.49	0.59 91.45	0.0 5.7	0.0 4.1	0.0 1.9	0.0 0.7	0.0 1.9	0.0	0.0	0.0	0.0	36.2 24651.3	3.0	0.0	112. 24676.
2015		10903.7	7466.76	3522.88		3522.88	69.7	1.2		78.15		78.15	5.7	3.7	1.8	0.7	1.8	0.0	0.0	0.0	0.0	20746.3	8.3	0.0	20966.
2015		15869.3	10807.18	5069.87	1726.4	5069.87	101.4	0	0.00	112.47	2066.06	112.47	7.9	5.4	2.5	0.9	2.5	0.1	0.0	0.0	0.1	30299.5		0.1	30342.
2015		24095.5	17161.54			8062.28	161.4	3.3		181.43	45676.07	181.43	12.0	8.6	4.0		4.0	0.1	0.0	0.0	0.1	48020.6		0.1	48618.
	August	22694.3	15161.65		2402.7	7118.66	141.9	2.2		158.71	31056.10	158.71	11.3	7.6	3.6	1.2	3.6	0.1	0.0	0.0	0.1	42186.6		0.1	42598.
	September October	21241.7 33658.8	15190.93 23426.26		2413 3911.3	7124.95 10987.54	141.7 230.9	0	0.00	156.98 253.70	1569.78 2537.03	156.98 253.70	10.6 16.8	7.6 11.7	3.6 5.5	1.2 2.0	3.6 5.5	0.1 0.1	0.0	0.0	0.1 0.1	42316.6 68388.6	0.8	0.1	42359. 68458.
	November	5998.6	4188.40		707.7	1966.72	41.8	0.3		46.64	4471.81	46.64	3.0	2.1	1.0	0.4	1.0	0.0	0.0	0.0	0.0	12491.7	2.2	0.0	12554.
	December	12308.8	8289.74			3897.96	82.9	2.1		93.76	31675.33	93.76	6.2	4.1	1.9			0.0	0.0	0.0	0.0	24653		0.0	25062.
2016	January	1614.7	1123.77	530.61	178.7	530.61	10.6	6.7	0.01	12.14	5631.59	12.14	0.8	0.6	0.3	0.1	0.3	0.0	0.0	0.0	0.0	3161.7	2.8	0.0	3233.
	February	1553.6	1049.30	496.86	166.6	496.86	9.9	6.2	0.01	11.41	6828.93	11.41	0.8	0.5	0.2	0.1	0.2	0.0	0.0	0.0	0.0	2941		0.0	3028.
2016 2016		4244.5 5397.6	3069.31 3755.96		513.1 617.8	1439.59 1766.41	30.1 36.6	17.8 21.8	0.00 0.01	33.36 40.73	333.61 7424.97	33.36 40.73	2.1 2.7	1.5 1.9	0.7 0.9	0.3 0.3	0.7 0.9	0.0	0.0	0.0	0.0	8993 10837.5		0.0	9002. 10936.
2016		15268.4	10489.26		1760.5	4929.43	103.7	61.1	0.01	109.76	10770.07	109.76	7.6	5.2	2.5	0.3		0.0	0.0	0.0	0.0	29392.4		0.0	29543.
2016		8461.7	5959.01		917.8	2800.29	54.1	118.3	0.00	60.15		60.15	4.2	3.0	1.4	0.5	1.4	0.0	0.1	0.0	0.0	16116.1	2.7	0.0	16192.
2016	July	2151.2	718.20	387.45	45.5	387.45	5.8	12.9	0.18	16.62	171599.70	16.62	1.1	0.4	0.2	0.0	0.2	0.0	0.0	0.0	0.0	1019.6	85.8	0.0	3167.
	August	1939	649.80	350.55	45.2	350.55	5.8	12.8	0.17	16.41	169412.06	16.41	1.0	0.3	0.2	0.0	0.2	0.0	0.0	0.0	0.0	1006.7	84.7	0.0	3126.
	September October	5257.2 13777.6	3909.69	1833.75 4568.07	633 1629.7	1833.75 4568.07	37.4 95.9	79.4 201.4	0.00	41.24 106.50	412.42 1065.00	41.24 106.50	2.6 6.9	2.0 4.9	0.9 2.3	0.3	0.9 2.3	0.0	0.0	0.0	0.0	11118.2 28709.7	0.2	0.0	11129. 28738.
	November	299.3	9739.47 108.94	4568.07 55.38	5.7	55.38	95.9	1.3		1.32		1.32	0.1	0.1	0.0	0.8	0.0	0.0	0.1	0.0	0.1	137.2		0.1	28738. 273.
	December	128.7	65.39	33.08	4.3	33.08	0.3	0.8		0.64			0.1	0.0	0.0	0.0		0.0	0.0	0.0	0.0	88.3		0.0	140.

Unit 1 Past Actuals

		NOx	со	PM	PM10	PM2.5	voc	SO2	Lead	H2SO4	CO2	Methane	N2O	CO2e
Year	Month	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons
2012	January	-	-	-	-	-	-	-	-	-	-	-	-	-
	February		_		-	-	-	-	_	_	-	_	_	
	March		_			-			_	_		_		
2012		_	_	_	_		_	_	-	_		_	-	
2012		_	-	-	-	-	-	-	-	_	-	_	-	-
	June	-	-	-	-	-	-	-	-	-	-	-	-	-
2012		-	-	-	-	-	-	-	-	-	-	-	-	-
	August	-	-	-	-	-	-	-	-	-	-	-	-	-
	September	-	-	-	-	-	-	-	-	-	-	-	-	-
	October	-	-	-	-	-	-	-	-	-	-	-	-	-
	November	-	-	-	-	-	-	-	-	-	•	-	-	-
	December	-	-	-	-	-	-	-	-	-		-	-	-
	January	-	-	-	-	-	-	-	-	-	-	-	-	-
	February	-	-	-	-	-	-	-	-	-	-	-	-	-
	March	-	-	-	-	-	-	-	-	-	-	-	•	•
2013		-	-	-	-	-	-	-	-	-	-	-	-	-
2013		-	-	-	-	-	-	-	-	-	-	-	-	-
	June	-	-	-	-	-	-	-	-	-	-	-	-	-
2013		-	-	-	-	-	-	-	-	-	-	-	-	-
	August	-	-	-	-	-	-	-	-	-	-	-	-	-
	September	-	-	-	-	-	-	-	-	-	-	-	-	-
	October November	-	-	-	-	-	-	-	-	-	-	-	-	-
	December	9.7	6.0	2.8	0.9	2.8	5.4E-02	1.6E-01	9.6E-05	6.5E-02	31,426	94.4	- 0.1	33,806
	January	13.8	7.1	3.4	1.0	3.4	6.6E-02	7.1E-01	4.4E-04	9.8E-02	35,374		0.1	46,086
	February	14.1	7.1	3.4	1.0	3.4	6.6E-02	7.1L-01 7.6E-01	4.4L-04 4.7E-04	1.0E-01	35,374	460.2	0.1	46,907
	March	15.4	7.4	3.6	1.0	3.6	6.9E-02	9.8E-01	6.1E-04	1.1E-01	36,100		0.1	50,946
2014		15.2	7.2	3.5	1.0	3.5	6.8E-02	9.8E-01	6.1E-04	1.1E-01	35,430		0.1	50,275
2014		15.5	7.4	3.6	1.0	3.6	6.9E-02	9.8E-01	6.1E-04	1.1E-01	36,052		0.1	50,898
	June	16.0	7.7	3.7	1.0	3.7	7.2E-02	9.8E-01	6.1E-04	1.1E-01	37,656		0.1	52,508
2014		17.3	8.3	4.0	1.1	4.0	7.8E-02	9.8E-01	6.1E-04	1.2E-01	41,413		0.1	56,271
	August	19.8	9.8	4.8	1.4	4.8	9.2E-02	9.7E-01	6.0E-04	1.4E-01	49,731	588.8	0.1	64,492
	September	22.9	11.7	5.6	1.7	5.6	1.1E-01	9.7E-01	6.0E-04	1.5E-01	59,799		0.2	74,569
2014	October	27.3	14.6	7.0	2.1	7.0	1.4E-01	9.7E-01	6.0E-04	1.9E-01	76,486	589.4	0.2	91,275
2014	November	28.3	15.2	7.3	2.2	7.3	1.4E-01	9.7E-01	6.0E-04	1.9E-01	79,767	589.5	0.2	94,562
	December	28.6	15.4	7.4	2.3	7.4	1.4E-01	9.8E-01	6.1E-04	1.9E-01	80,914		0.2	95,850
	January	28.5	15.6	7.4	2.3	7.4	1.4E-01	9.2E-01	5.7E-04	1.9E-01	81,873		0.2	95,918
	February	31.3	16.4	7.9	2.4	7.9	1.5E-01	1.4E+00	8.5E-04	2.2E-01	85,089		0.2	105,906
	March	31.3		7.9	2.4	7.9	1.5E-01	1.4E+00		2.2E-01	85,107		0.2	105,963
2015	April	33.8	18.2	8.7	2.7	8.7	1.7E-01	1.4E+00		2.4E-01	96,195		0.2	117,062
2015		36.3	19.9	9.5	3.0	9.5	1.9E-01	1.4E+00		2.6E-01	105,852		0.3	126,797
	June	39.2	21.9	10.5	3.3	10.5	2.1E-01	1.4E+00		2.8E-01	117,247		0.3	138,209
2015		42.8	24.6	11.8		11.8	2.4E-01	1.4E+00		3.1E-01	132,909		0.3	154,161
	August	47.6	27.9	13.3	4.2	13.3	2.7E-01	1.4E+00		3.4E-01	151,073		0.3	172,323
	September	52.4	31.3	14.9	4.8	14.9	3.0E-01	1.4E+00		3.8E-01	170,456		0.4	191,725
	October November	60.8	37.2	17.6	5.8	17.6	3.6E-01 3.7E-01	1.4E+00 1.4E+00		4.4E-01	204,650		0.4	225,954
	December	62.3 65.0	38.2 40.2	18.1	5.9	18.1 19.0	3.7E-01 3.9E-01	1.4E+00 1.3E+00		4.5E-01 4.7E-01	210,896 222,700		0.5	232,232 243,448
	January	61.3	39.4	19.0 18.6	6.3 6.2	19.0	3.9E-01 3.8E-01	7.5E-01	8.4E-04 5.0E-04	4.7E-01 4.5E-01	222,700		0.5 0.4	232,777
	February	61.3	39.4	18.7	6.3	18.7	3.8E-01	7.0E-01	4.7E-04	4.5E-01 4.4E-01	220,325		0.4	232,777
	March	60.8	39.9	18.8	6.4	18.8	3.8E-01	4.8E-01	3.3E-04	4.4E-01	224,328		0.4	232,693
2016		62.1	40.9	19.3	6.5	19.3	3.9E-01	4.9E-01	3.4E-04	4.4E-01 4.5E-01	229,747		0.4	238,161
2016		65.4	43.2	20.3	6.9	20.3	4.1E-01	5.1E-01	3.4E-04	4.7E-01	242,677		0.5	251,165
	June	66.5	43.9	20.7	7.0		4.2E-01	5.3E-01	3.4E-04	4.8E-01	247,073		0.5	255,591
2016		64.6		20.1	6.8	20.1	4.1E-01	5.4E-01	3.8E-04	4.7E-01	239,270		0.5	248,851
	August	62.0		19.3	6.5	19.3	3.9E-01	5.2E-01	4.1E-04	4.6E-01	229,974		0.5	240,304
	September	60.3	40.0	18.9	6.4	18.9	3.9E-01	5.4E-01	4.1E-04	4.5E-01	225,466		0.4	235,791
	October	59.1	39.5	18.6	6.3	18.6		5.9E-01	4.1E-04	4.4E-01	222,913		0.4	233,233
	November	58.2	38.9	18.3	6.2	18.3	3.8E-01	5.9E-01	4.2E-04	4.4E-01	219,367		0.4	229,749
	December	57.8		18.3	6.2	18.3		5.8E-01	4.1E-04	4.3E-01	218,264		0.4	228,532

Unit 2 Past Actuals

Unit 2 Pas	t Actuals																			
Year	Month	Gross Output	Gas On- Time	Gas Heat Input	Oil Flow On-Time	Oil Heat Input	NG CO	FO CO	NG PM	FO PM	NG PM2.5	FO PM2.5	NG Lead	FO Lead	NG H2SO4	FO H2SO4	NG Methane	FO Methane	NG N2O	FO N2O
		MW-hrs	Hours	MMBtu	Hours	MMBtu	lb/hr	lb/hr	lb/hr	lb/hr	lb/hr	lb/hr	lb/MMBtu	lb/MMBtu	lb/hr	lb/hr	lb/MMBtu	,	•	lb/MMBtu
	January	0	_	0		0	33.9	76	15.9	41		41	0	1.40E-05		17.70	2.20E-03			1.32E-03
	February	1823	11.75			0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	March	3338	22.09	34632.4		0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	April	5580	38.35	58453.3		U	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	May	12505	88.27	134736.5				76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	June	5954	42.58			4672.4	33.9	76	15.9	41		41	0	1.40E-05		17.70	2.20E-03			1.32E-03
	July	0	0	0	ŭ	0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	August	0	•	0	, ,	0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	September	786	6.72			0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	October	0	0	0	O	0	33.9	76	15.9	41		41	0	1.40E-05	0.41	17.70	2.20E-03			1.32E-03
	November	608	5.73			0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	December	3437	34.7	61317.8		0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	January	0	0	0	0	0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	February	5296	44.46	70097.1	0	V	33.9	76 70	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	March	6129		63986.7	0	Ŭ	00.0	76 70	15.9	41		41	U	1.40E-05		17.70				1.32E-03
	April	2468	17.13	26112.2	0	0	33.9	76 70	15.9	41		41	0	1.40E-05		17.70	2.20E-03			1.32E-03
	May	17073	114.26	176243.7	0	0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	June	4660	31	47761.6		0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	July	3738	24.69			0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	August	0	0	0	ŭ	0	33.9	76	15.9	41		41	0	1.40E-05	0.41	17.70				1.32E-03
	September	ŭ	0.70	_	_	5504.0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	October	1689	6.76			5501.2	33.9	76 76	15.9	41		41	0	1.40E-05		17.70 17.70				1.32E-03
	November December	3721 1245	0	0		38761.4	33.9 33.9	76 76	15.9 15.9	41 41		41 41	0	1.40E-05		17.70				1.32E-03 1.32E-03
	January	3520	0	0		13198.6 36270.4	33.9	76 76	15.9	41		41	0	1.40E-05 1.40E-05		17.70				1.32E-03 1.32E-03
	February	3320	0	0		30270.4	33.9	76	15.9	41		41	0	1.40E-05		17.70	2.20E-03			1.32E-03
	March	5094	34.28	ŭ	ŭ	449.2	33.9	76	15.9	41		41	0	1.40E-05		17.70	2.20E-03			1.32E-03
	April	10822	74.3	112154.7	0.30	149.2	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	May	25249	163.58	258532.4	1.63	2311.9	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	June	21318	139.03	218982.5		2011.5	33.9	76	15.9	41		41	0	1.40E-05	0.41	17.70				1.32E-03
	July	31953	203.83	322231.7	0	0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	August	60950	370.79	612208.7	0.14	51.3	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	September	10320	61.3	102806.5		16	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	October	6778	39.55	68371.9		1543.7	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	November	1	0	0		301.3	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
2014	December	2461	0	0		25982	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
2015	January	9263	53.24	95427.3		344.6	33.9	76	15.9	41		41	0	1.40E-05	0.41	17.70	2.20E-03			1.32E-03
2015	February	30286	185.49	305809.7		0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
2015	March	30841	196.18	328152	2.29	967.1	33.9	76	15.9	41	15.9	41	0	1.40E-05	0.41	17.70	2.20E-03	13.66	2.20E-04	
	April	48305	314.36	514069.9	0.22		33.9	76	15.9	41		41		1.40E-05		17.70				1.32E-03
2015	May	87556	560.02	929385.8	2.69	3787.8	33.9	76	15.9	41	15.9	41	0	1.40E-05	0.41	17.70				1.32E-03
2015	June	88834	559.69	933037.7	0	0	33.9	76	15.9	41	15.9	41	0	1.40E-05	0.41	17.70			2.20E-04	1.32E-03
2015	July	83926	529.75	872656.4		0	33.9	76	15.9	41	15.9	41	0	1.40E-05	0.41	17.70				1.32E-03
2015	August	34095		350691.2		Ŭ	33.9	76	15.9	41			0	1.40E-05		17.70				1.32E-03
	September	32306	191.4	333653.5				76	15.9	41		41	0	1.40E-05	0.41	17.70				1.32E-03
2015	October	181	0	0	1.36	2008.7	33.9	76	15.9	41	15.9	41	0	1.40E-05	0.41	17.70				1.32E-03
2015	November	0	0	0			33.9	76	15.9	41		41	0	1.40E-05	0.41	17.70				1.32E-03
	December	8108				454.7	33.9		15.9	41		41	0	1.40E-05		17.70				1.32E-03
	January	27728		290135.4		58.6	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	February	27685		251653.3			33.9	76	15.9	41		41	0	1.40E-05		17.70				
	March	61180		650234.6		93.6	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	April	57430	371.74				33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	May	588	0	0		6395.4	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	June	1363	0	0			33.9		15.9	41			0	1.40E-05		17.70				1.32E-03
	July	50962				0	33.9		15.9	41			0	1.40E-05		17.70				
	August	66680	401.46			0	33.9	76	15.9	41		41	0	1.40E-05		17.70				1.32E-03
	September	175					33.9	76	15.9	41		41		1.40E-05		17.70				1.32E-03
	October	13		0		251.2	33.9		15.9	41			0	1.40E-05		17.70				1.32E-03
	November	0	0.0	v		00000	33.9		15.9	41			0	1.40E-05		17.70				
2016	December	66	0.6	617.5	0.35	293.9	33.9	76	15.9	41	15.9	41	0	1.40E-05	0.41	17.70	2.20E-03	13.66	2.20E-04	1.32E-03

Unit 2 Past Actuals

	Actuals																								
		NOx	со	PM	PM10	PM2.5	voc	SO2	Lead	H2SO4	Methane	N2O	NOx	со	PM	PM10	PM2.5	voc	SO2	Lead	H2SO4	CO2	Methane	N2O	CO2e
Year	Month																								
		lbs	lbs	lbs	lbs	lbs	lbs	lbs	lbs	lbs	lbs	lbs	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons
2012	January	0	0.00	0.00	0	0.00	0	0	0.00	0.00	0.00	0.00	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0	0.0	0.0	0.
	February	526.2	398.33	186.83	57.4	186.83	3.4	0	0.00	3.73	37.33	3.73	0.3		0.1	0.0	0.1		0.0	0.0	0.0	1006.3	0.0	0.0	1007.
2012	March	1052.5	748.85	351.23	116.7	351.23	6.8	0	0.00	7.64	76.35	7.64	0.5	0.4	0.2	0.1	0.2	0.0	0.0	0.0	0.0	2058	0.0	0.0	2060
2012		1843.1	1300.07	609.77	195.5	609.77	11.5		0.00	12.89	128.87	12.89	0.9		0.3	0.1	0.3	1	0.0	0.0	0.0	3473.8		0.0	3477.
2012	,	4108.4	2994.63	1404.72	452	1404.72	26.4	0.1	0.00	29.71	359.86	29.71	2.1	1.5	0.7	0.2	0.7		0.0	0.0		8007.6	0.2	0.0	8016
2012		2828.4	1686.66	808.22	229.3	808.22	14.6	105.5	0.07	20.31	63945.98	20.31	1.4		0.4	0.1	0.4		0.1	0.0		4188.4		0.0	4990.
2012		0	0.00	0.00	0	0.00	0	0	0.00	0.00	0.00	0.00	0.0		0.0	0.0	0.0		0.0	0.0	0.0	0	0.0	0.0	0.
	August September	202.0	0.00	0.00	34.8	0.00 106.85	2.1	0	0.00	0.00	0.00 24.41	0.00 2.44	0.0		0.0	0.0	0.0	1	0.0	0.0		658.1	0.0	0.0	
	October	393.9	227.81 0.00	106.85 0.00	34.0 0	0.00	2.1	0	0.00	2.44 0.00	0.00	0.00	0.2		0.1	0.0	0.1 0.0		0.0	0.0	0.0	000.1	0.0	0.0	036
	November	307.1	194.25	91.11	30.8	91.11	1.8	0	0.00	2.04	20.41	2.04	0.0		0.0	0.0	0.0		0.0	0.0		550.1	0.0	0.0	_
	December	2048.6	1176.33	551.73	208.2	551.73	12.2	_	0.00	13.52	135.18	13.52	1.0		0.3	0.1	0.3		0.0	0.0	0.0	3644.1	0.1	0.0	3647
	January	0	0.00	0.00	0	0.00	0	0	0.00	0.00	0.00	0.00	0.0		0.0	0.0	0.0	1	0.0	0.0		001111	0.0	0.0	0
	February	2177.2	1507.19	706.91	237.7	706.91	14	0	0.00	15.45	154.54	15.45	1.1	0.8	0.4	0.1	0.4	1	0.0	0.0	0.0	4165.4		0.0	4169
2013	March	2063	1372.95	643.95	216	643.95	12.8	0	0.00	14.11	141.07	14.11	1.0	0.7	0.3	0.1	0.3	0.0	0.0	0.0	0.0	3802.5	0.1	0.0	3806
2013		890.1	580.71	272.37	87.6	272.37	5.2	0	0.00	5.76	57.57	5.76	0.4		0.1	0.0	0.1		0.0	0.0	0.0	1551.8		0.0	1553
2013	,	5251.7	3873.41	1816.73	595.1	1816.73	34.9	0	0.00	38.86	388.55	38.86	2.6		0.9	0.3	0.9		0.0	0.0	0.0	10475.1	0.2	0.0	10485
2013		1563.3	1050.90	492.90	160.9	492.90	9.5		0.00	10.53	105.30	10.53	0.8		0.2	0.1	0.2		0.0	0.0		2838.2	0.1	0.0	2841
2013	_	1180.4	836.99	392.57	129.5	392.57	7.6	0	0.00	8.48		8.48	0.6		0.2	0.1	0.2		0.0	0.0	0.0	2286.2	0.0	0.0	2288
	August September	0	0.00	0.00	0	0.00	0	0	0.00	0.00	0.00	0.00	0.0		0.0	0.0	0.0		0.0	0.0	0.0	0	0.0	0.0	0
	October	1448.3	495.16	250.98	59.7	250.98	5	124.2	0.00	9.84	75148.08	9.84	0.0		0.0	0.0	0.0		0.0	0.0	0.0	1136.2		0.0	2077
	November	6252.1	1636.28	882.73	143.5	882.73	19.4	874.8	0.54	51.27	529312.32	51.27	3.1		0.1	0.0	0.4		0.1	0.0		3145		0.0	
	December	2006.8	583.68	314.88	47.7	314.88	6	297.9	0.18	17.46		17.46	1.0		0.4	0.0	0.2	1	0.1	0.0	0.0	1071.1	90.1	0.0	3326
	January	5627.8	1493.40	805.65	133.7	805.65	16.9		0.51	47.98		47.98	2.8		0.4	0.1	0.4		0.4	0.0	0.0	2942.9		0.0	9141
2014	February	0	0.00	0.00	0	0.00	0	0	0.00	0.00	0.00	0.00	0.0		0.0	0.0	0.0	0.0	0.0	0.0		0	0.0	0.0	0.
2014	March	1996	1206.17	568.83	178.2	568.83	10.6	10	0.01	12.18	6249.95	12.18	1.0	0.6	0.3	0.1	0.3	0.0	0.0	0.0	0.0	3158.8	3.1	0.0	3238.
2014		3824.3	2518.77	1181.37	375.5	1181.37	22		0.00	24.73	247.26	24.73	1.9		0.6	0.2	0.6		0.0	0.0		6664.9		0.0	
2014	,	8841.4	5669.24	2667.75	877.5	2667.75	52.2	51.8	0.03	60.05		60.05	4.4		1.3	0.4	1.3		0.0	0.0	0.0	15550.3	16.1	0.0	
2014		7114.1	4713.12	2210.58	739	2210.58	43.5	0	0.00	48.28	482.77	48.28	3.6		1.1	0.4	1.1		0.0	0.0		13012.7	0.2	0.0	13025.
2014	August	11089.1 20363.7	6909.84 12580.42	3240.90 5901.30	1088.1 2071.3	3240.90 5901.30	64 121.7		0.00	71.04 135.04	710.40 2050.22	71.04 135.04	5.5 10.2		1.6 3.0	0.5 1.0	1.6 3.0		0.0	0.0	0.0 0.1	19148.4 36387.1	0.4 1.0	0.0	19167 36432
	September	3624.2	2080.35	975.90	346.6	975.90	20.4	1.1 0.4	0.00	22.69	445.14	22.69	10.2		0.5	0.2	0.5		0.0	0.0		6110.7	0.2	0.1	6119
	October	2894.1	1425.87	674.77	233.9	674.77	14.2		0.02	17.12	21230.97	17.12	1.4	0.7	0.3	0.2	0.3	1	0.0	0.0	0.0	4188.6	10.6	0.0	4456
	November	30.4	69.92	37.72	1	37.72	0	6.8	0.00	0.40	4114.45	0.40	0.0		0.0	0.0	0.0		0.0	0.0	0.0	24.4	2.1	0.0	75
2014	December	3753.8	1092.88	589.58	96.1	589.58	12.6	581.4	0.36	34.37	354801.24	34.37	1.9		0.3	0.0	0.3	0.0	0.3	0.0	0.0	2108.2		0.0	
2015	January	3029.8	1854.24	873.17	323.9	873.17	19.1	1.8	0.00	21.49	4916.12	21.49	1.5	0.9	0.4	0.2	0.4	0.0	0.0	0.0	0.0	5698.8	2.5	0.0	5763
	February	8033.6	6288.11	2949.29	964.7	2949.29	56.7	0	0.00	67.42		67.42	4.0		1.5	0.5	1.5		0.0	0.0		18174.5	0.3	0.0	18193
	March	9880.1	6824.54		1094.9	3213.15	64.9		0.01	73.62		73.62	4.9		1.6	0.5	1.6		0.0	0.0		19579.5			
2015		14842.9		5007.34	1733.2	5007.34	102.3		0.00	113.42		113.42	7.4		2.5	0.9	2.5		0.0	0.0		30555.2		0.1	30597
2015	,	25357.6	19189.12	9014.61	3164.3	9014.61	187.2		0.05	209.90	53773.84	209.90	12.7		4.5	1.6	4.5		0.0	0.0		55540.1	26.9	0.1	56243
2015 2015		27020.3 26618.8	18973.49 17958.53	8899.07 8423.03	3154 2954.3	8899.07 8423.03	186 174.1		0.00	205.70 192.39	2057.00 1923.88	205.70 192.39	13.5 13.3		4.4	1.6 1.5	4.4		0.0	0.0		55448.7 51861.2	1.0	0.1 0.1	55505 51913
	August	11112.5	7075.27	3318.49	1189.1	3318.49	69.7	0	0.00	77.31	773.14	77.31	5.6		1.7	0.6	4.2 1.7		0.0	0.0	0.1	20841.4		0.1	
	September	9898.1	6526.46		1125	3063.76	66.4	0.4	0.00	74.01	5422.20	74.01	4.9		1.7	0.6	1.7		0.0	0.0		19857.1	2.7	0.0	19935
	October	345.9	103.36	55.76	7.3	55.76	0.9		0.03	2.66		2.66	0.2		0.0	0.0	0.0		0.0	0.0		162.9		0.0	506
	November	0	19.00	10.25	0.3	10.25	0		0.00	0.11	1181.21	0.11	0.0		0.0	0.0	0.0		0.0	0.0	0.0	7	0.6	0.0	
	December	2564.6	1651.82	778.87	283.4	778.87	16.8	9.7	0.01	18.96	6392.81	18.96	1.3		0.4	0.1	0.4	0.0	0.0	0.0	0.0	4985.6	3.2	0.0	
	January	8560.9	5783.72		982.7	2713.63	57.8	33.4	0.00	64.04	1439.86	64.04	4.3		1.4	0.5	1.4		0.0	0.0		17246.6		0.0	
	February	8468.1	5748.44		982.6	2697.51	57.8	32.9	0.00	55.58	1602.19	55.58	4.2		1.3	0.5	1.3		0.0	0.0		14961.8		0.0	
	March	18450.4	13184.23	6208.22	2205	6208.22	129.9		0.00	143.48		143.48	9.2		3.1	1.1	3.1	1	0.0	0.0		38650.3			38705
2016		18193.4	12658.23	5941.01	2046.4	5941.01	120.4	189.9	0.00	133.18		133.18	9.1		3.0	1.0	3.0		0.1	0.0		35828.4		0.1	35910
2016	,	1113.4	335.16		23.4	180.81	3	6.6	0.09	8.46		8.46	0.6		0.1	0.0	0.1		0.0	0.0		518.9		0.0	
2016 2016		2369.2 16513.9	759.24 11096.15	409.59 5204.39	55 1773.9	409.59 5204.39	7.1 104.3	15.1 224.8	0.21 0.00	19.49 115.38		19.49 115.38	1.2 8.3		0.2	0.0	0.2		0.0	0.0	0.0 0.1	1195.8 31102		0.0	
	August	21692.2	13609.49	6383.21	2305.2	6383.21	135.6		0.00	150.36		150.36	10.8		2.6 3.2	1.2	2.6 3.2		0.1	0.0		40530.7		0.1	40571
	September	217.9	124.55	62.27	7.2	62.27	0.6		0.00	1.26	9223.95	1.26	0.1		0.0	0.0	0.0	1	0.0	0.0		153.1	4.6	0.1	268
	October	61.6	30.40	16.40	0.8		0.0		0.00	0.33		0.33	0.0		0.0	0.0	0.0		0.0	0.0		20.4			
	November	0	0.00	0.00	0	0.00	0		0.00	0.00	0.00	0.00	0.0		0.0	0.0	0.0		0.0	0.0		0		0.0	
	December	149.9	46.94	23.89	3.1		0.3	0.5	0.00	0.52			0.1		0.0	0.0	0.0		0.0	0.0		60.5		0.0	

Unit 2 Past Actuals

Year	Month	NOx	со	PM	PM10	PM2.5	voc	SO2	Lead	H2SO4	CO2	Methane	N2O	CO2e
Teal	WOITE	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons
2012	January	-	-	-	-	-	-	-	-	-	-	-	-	-
	February	-	-	-	-	-	-	-	-	-	-	-	-	-
	March	-	-	-	-	-	-	-	-	-	-	-	-	-
2012		-	-	-	-	-	-	-	-	-	-	-	-	-
2012		-	-	-	-	-	-	-	-	-	-	-	-	-
2012		-	-	-	-	-	-	-	-	-	-	-	-	-
	July	-	-	-	-	-	-	-	-	-	-	-	-	-
	August	-	-	-	-	-	-	-	-	-	-	-	-	-
	September October	-	-	-	-	-	-	-	-	-	-	-	-	-
	November	-	-	-	-	-	-	-	-	-		-	-	-
	December	-	-			-	_	-	-	-		-		
	January	-			-		-	-	-	-				
	February	-	-			-	-		-	-		_		-
	March	-	_	_	_	_	_	_	_	_	_	_	_	_
2013		-	-	-	-	-	-	-	-	-		-	-	-
2013		-	-	-	-	-	-	-	-	-	-	-	-	-
2013		-	-	-	-	-	-	-	-	-	-	-	-	-
2013		-	-	-	-	-	-	-	-	-	-	-	-	•
	August	-	-	-	-	-	-	-	•	-	-	-	-	•
	September	-	-	-	-	-	-	-	-	-	-	-	-	-
	October	-	-	-	-	-	-	-	-	-	-	-	-	-
	November	-	-		-	-	-	-	-	-	-	-	-	-
	December	9.0	5.2	2.5	0.8	2.5	4.8E-02	3.5E-01	2.2E-04	6.6E-02	27,029		0.1	32,363
	January	10.4	5.5	2.7	0.8	2.7	5.3E-02	5.6E-01	3.4E-04	7.8E-02	28,500	336.4 336.4	0.1	36,934
	February March	10.3 10.5	5.4 5.6	2.6 2.7	0.8	2.6 2.7	5.2E-02 5.3E-02	5.6E-01 5.6E-01	3.4E-04 3.5E-04	7.7E-02 7.8E-02	27,997 28,548	337.9	0.1 0.1	36,430 37,020
2014		11.0	5.9	2.7	0.8	2.7	5.5E-02	5.6E-01	3.5E-04	8.1E-02	30,143		0.1	38,617
2014		12.2	6.5	3.1	0.9	3.1	6.2E-02	5.7E-01	3.5E-04	8.9E-02	33,915		0.1	42,589
2014		13.2	7.3	3.5	1.1	3.5	6.9E-02	5.4E-01	3.4E-04	9.6E-02	38,327	330.1	0.1	46,607
2014		16.0	9.0	4.3	1.3	4.3	8.5E-02	5.4E-01	3.4E-04	1.1E-01	47,901	330.2	0.1	56,191
	August	21.1	12.2	5.8	1.9	5.8	1.2E-01	5.4E-01	3.4E-04	1.5E-01	66,094	330.7	0.1	74,407
	September	21.9	12.6	6.0	1.9	6.0	1.2E-01	5.4E-01	3.4E-04	1.5E-01	68,821	330.9	0.2	77,137
2014	October	22.6	13.0	6.2	2.0	6.2	1.2E-01	5.5E-01	3.4E-04	1.6E-01	70,915	336.2	0.2	79,366
	November	22.6	12.9	6.1	2.0	6.1	1.2E-01	5.5E-01	3.4E-04	1.6E-01	70,652	337.2	0.2	79,128
	December	23.0	12.9	6.2	2.0	6.2	1.2E-01	7.0E-01	4.4E-04	1.6E-01	69,884	425.8	0.2	80,579
	January	23.8	13.4	6.4	2.0	6.4	1.3E-01	7.0E-01	4.4E-04	1.7E-01	72,734	427.1	0.2	83,460
	February	25.2	14.6	6.9	2.2	6.9	1.4E-01	7.0E-01	4.4E-04	1.8E-01	79,738		0.2	90,472
	March	27.2	15.9	7.6	2.4	7.6	1.5E-01	7.0E-01	4.4E-04	1.9E-01	87,627		0.2	98,451
2015 2015	Mov	30.7 35.7	18.5 22.3	8.8 10.6	2.8 3.5	8.8 10.6	1.8E-01 2.1E-01	7.0E-01 7.0E-01	4.4E-04 4.5E-04	2.2E-01 2.6E-01	102,128 124,661	431.1 444.5	0.2	112,973 135,852
2015		42.1	26.8	12.7	4.2	12.7	2.1E-01 2.6E-01	7.0E-01 7.0E-01	4.5E-04 4.5E-04	3.1E-01	150,966		0.3	162,184
2015		48.4	31.1	14.7	4.2	14.7	3.0E-01	7.0E-01	4.5E-04	3.6E-01	175,754		0.3	186,997
	August	51.2	32.8	15.5	5.2	15.5	3.2E-01	7.0E-01	4.5E-04	3.8E-01	186,174		0.4	197,428
	September	53.7	34.5	16.3	5.5	16.3	3.3E-01	7.0E-01	4.5E-04	4.0E-01	196,103		0.4	207,396
	October	53.4	34.4	16.2	5.5	16.2	3.3E-01	6.7E-01	4.4E-04	4.0E-01	195,616		0.4	206,611
2015	November	51.8	34.0	16.0	5.5	16.0	3.3E-01	4.5E-01	3.1E-04	3.8E-01	194,047		0.4	201,737
	December	52.0	34.2	16.1	5.5	16.1	3.3E-01	3.8E-01	2.6E-04	3.8E-01	196,005		0.4	202,608
	January	52.7	35.3	16.6	5.7	16.6	3.4E-01	1.8E-01	1.4E-04	3.9E-01	203,156		0.4	206,674
	February	54.8	36.7	17.3	6.0	17.3	3.6E-01	1.9E-01	1.4E-04	4.0E-01	210,637		0.4	214,169
	March	58.9	39.7	18.7	6.5	18.7	3.9E-01	2.0E-01	1.3E-04	4.3E-01	228,383		0.4	231,903
2016		62.5	42.3	19.9	6.9	19.9	4.1E-01	2.5E-01	1.4E-04	4.6E-01	242,965		0.5	246,522
2016		60.6	40.9	19.2	6.7	19.2	4.0E-01	2.4E-01	1.5E-04	4.5E-01	235,449			239,347
2016 2016		59.4 60.8	39.9 41.0	18.8 19.3	6.5 6.7	18.8 19.3	3.9E-01 4.0E-01	2.4E-01 3.0E-01	2.0E-04 2.0E-04	4.4E-01 4.5E-01	229,541 235,517	200.8 200.9	0.4	234,69° 240,674
	August	61.1	41.0	19.3	6.8	19.3	4.0E-01 4.0E-01	3.7E-01	2.0E-04 2.0E-04	4.5E-01 4.6E-01	235,517		0.5	240,674
	September	60.2	40.8	19.4	6.7	19.4	4.0E-01	3.7E-01	2.0E-04 2.0E-04	4.5E-01	234,610		0.5	
	October	59.5	40.8	19.2	6.6	19.2	3.9E-01	3.6E-01	2.0E-04 2.0E-04	4.5E-01	232,526		0.3	237,622
	November	59.5	40.4	19.0	6.6	19.0	3.9E-01	3.6E-01	2.0E-04	4.5E-01	232,520		0.4	237,584
	December	58.6	40.1	18.9	6.6	18.9	3.9E-01	2.2E-01	1.1E-04	4.4E-01	231,490			234,36

Pleasants Energy, LLC - Uprate Project

								Combined Units						
Beginning	Ending	NOx	CO	PM	PM10	PM2.5	VOC	SO2	Lead	H2SO4	CO2	Methane	N2O	CO2e
Month	Month	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons	tons
Jan-12	Dec-13	18.7	11.2	5.3	1.6	5.3	0.1	0.5	0.0	0.1	58454.6	307.0	0.1	66168.9
Feb-12	Jan-14	24.2	12.6	6.1	1.8	6.1	0.1	1.3	0.0	0.2	63874.8	763.7	0.2	83020.0
Mar-12	Mar-14	24.3	12.5	6.1	1.7	6.1	0.1	1.3	0.0	0.2	63368.6	796.6	0.2	83337.2
Apr-12	Apr-14	25.9	12.9	6.3	1.8	6.3	0.1	1.5	0.0	0.2	64647.7	930.5	0.2	87965.8
May-12	May-14	26.2	13.1	6.4	1.8	6.4	0.1	1.5	0.0	0.2	65573.2	930.5	0.2	88892.2
Jun-12	Jun-14	27.6	13.9	6.7	1.9	6.7	0.1	1.5	0.0	0.2	69966.8	938.4	0.2	93487.3
Jul-12	Jul-14	29.2	15.0	7.2	2.1	7.2	0.1	1.5	0.0	0.2	75982.5	922.8	0.2	99114.2
Aug-12	Aug-14	33.3	17.3	8.3	2.5	8.3	0.2	1.5	0.0	0.2	89314.1	923.1	0.2	112461.6
Sep-12	Sep-14	40.9	22.0	10.5	3.2	10.5	0.2	1.5	0.0	0.3	115825.9	919.5	0.3	138898.5
Oct-12	Oct-14	44.8	24.3	11.6	3.6	11.6	0.2	1.5	0.0	0.3	128619.5	919.8	0.3	151706.5
Nov-12	Nov-14	50.0	27.6	13.2	4.1	13.2	0.3	1.5	0.0	0.3	147401.0	925.5	0.3	170641.1
Dec-12	Dec-14	50.8	28.2	13.4	4.2	13.4	0.3	1.5	0.0	0.3	150419.0	926.7	0.3	173690.5
Jan-13	Jan-15	51.6	28.4	13.5	4.2	13.5	0.3	1.7	0.0	0.4	150798.6	1020.9	0.4	176428.3
Feb-13	Feb-15	52.2	28.9	13.8	4.3	13.8	0.3	1.6	0.0	0.4	154606.7	986.5	0.4	179377.8
Mar-13	Mar-15	56.5	31.0	14.8	4.6	14.8	0.3	2.1	0.0	0.4	164827.4	1257.3	0.4	196378.5
Apr-13	Apr-15	58.5	32.3	15.5	4.8	15.5	0.3	2.1	0.0	0.4	172734.0	1262.3	0.4	204413.8
May-13	May-15	64.5	36.7	17.5	5.5	17.5	0.3	2.1	0.0	0.5	198323.6	1262.9	0.5	230035.0
Jun-13	Jun-15	72.0	42.2	20.1	6.4	20.1	0.4	2.1	0.0	0.5	230513.4	1279.2	0.5	262648.8
Jul-13	Jul-15	81.3	48.7	23.1	7.5	23.1	0.5	2.1	0.0	0.6	268213.4	1280.1	0.6	300393.1
Aug-13	Aug-15	91.2	55.7	26.4	8.7	26.4	0.5	2.1	0.0	0.7	308662.6	1291.8	0.7	341157.9
Sep-13	Sep-15	98.8	60.7	28.8	9.5	28.8	0.6	2.1	0.0	0.7	337247.6	1291.5	0.7	369750.9
Oct-13	Oct-15	106.1	65.8	31.2	10.3	31.2	0.6	2.1	0.0	0.8	366558.7	1293.2	0.8	399121.1
Nov-13	Nov-15	114.2	71.6	33.9	11.3	33.9	0.7	2.0	0.0	0.8	400266.4	1281.9	0.8	432564.8
Dec-13	Dec-15	114.1	72.2	34.1	11.4	34.1	0.7	1.8	0.0	0.8	404943.2	1151.0	0.8	433968.4
Jan-14	Jan-16	117.0	74.4	35.2	11.8	35.2	0.7		0.0	0.9	418704.6	1083.8	0.9	446055.5
Feb-14	Feb-16	114.0	74.7	35.2	12.0	35.2	0.7	0.9	0.0	0.8	423481.2	628.9	0.8	439451.1
Mar-14	Feb-16	116.1	76.3	35.9	12.3	35.9	0.7	0.9	0.0	0.8	432041.2	598.0	0.8	447244.4
Apr-14	Mar-16	119.7	79.7	37.5	12.9	37.5	0.8	0.7	0.0	0.9	452711.2	464.9	0.9	464595.3
May-14	Apr-16	124.7	83.1	39.1	13.4	39.1	0.8	0.7	0.0	0.9	472711.7	468.0	0.9	484682.7
Jun-14	May-16	126.0	84.1	39.6	13.6	39.6	0.8	0.7	0.0	0.9	478126.2	484.4	0.9	490512.0
Jul-14	Jun-16	125.9	83.9	39.5	13.6	39.5	0.8	0.8	0.0	0.9	476614.0	535.7	0.9	490282.4
Aug-14	Jul-16	125.3	83.6	39.4	13.5	39.4	0.8	0.8	0.0	0.9	474787.6	578.5	0.9	489525.1
Sep-14	Aug-16	123.1	82.2	38.7	13.3	38.7	0.8	0.9	0.0	0.9	467563.3	608.5	0.9	483047.4
Oct-14	Sep-16	120.5	80.8	38.1	13.1	38.1	0.8	0.9	0.0	0.9	460076.3	610.6	0.9	475609.1
Nov-14	Oct-16	118.7	79.9	37.7	13.0	37.7	0.8	1.0	0.0	0.9	455439.3	606.0	0.9	470854.8
Dec-14	Nov-16	117.7	79.3	37.3	12.9	37.3	0.8	1.0	0.0	0.9	451881.1	607.5	0.9	467332.8
Jan-15	Dec-16	116.5	78.8	37.1	12.8	37.1	0.8	0.8	0.0	0.9	449753.8	515.3	0.9	462896.7

		Max Periods													
	NOx	СО	PM	PM10	PM2.5	VOC	SO2	Lead	H2SO4	CO2	Methane	N2O	CO2e		
Combined emissions	126.0	84.1	39.6	13.6	39.6	0.8	2.1	1.3E-03	0.9	478,126	1293.2	0.9	490,512		
Beginning of 24 months	May-14	May-14	May-14	May-14	May-14	May-14	Mar-13	Sep-13	Jun-14	May-14	Sep-13	Jun-14	May-14		
End of 24 months	May-16	May-16	May-16	May-16	May-16	May-16	Mar-15	Sep-15	Jun-16	May-16	Sep-15	Jun-16	May-16		



								Emission			
RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Limit 1	Units	Туре	Notes
*PA-0306	2/12/2016	PARTNERS/WESTMORELAND GEN FAC	TENASKA PA PARTNERS LLC	PA	0		SCR, DLN, and good combustion practice	2	PPMVD@15% O2	LAER	Combined cycle
MD-0040	11/12/2008	CPV ST CHARLES	COMPETITIVE POWER VENTURES, INC./CPV MARYLAND, LLC	MD			DRY LOW NOX BURNER AND SCR	2	PPMVD @ 15% O2	LAER	Combined cycle
MD-0040	11/12/2008	CPV ST CHARLES	COMPETITIVE POWER VENTURES, INC./CPV MARYLAND, LLC	MD			DRY LOW NOX BURNER AND SCR	2	PPMVD @ 15% O2	LAER	Combined cycle
*OR-0050	3/5/2014	TROUTDALE ENERGY CENTER, LLC	TROUTDALE ENERGY CENTER, LLC	OR	2988		Utilize dry low-NOx burners when combusting natural gas; Utilize water injection when combusting ULSD; Utilize selective catalytic reduction (SCR) with aqueous ammonia injection at all times except during startup and shutdown; Limit the time in startup or shutdown.	2	PPMDV AT 15% O2	BACT-PSD	Combined cycle
NJ-0075	9/24/2009	BAYONNE ENERGY CENTER	BAYONNE ENERGY CENTER, LLC	NJ	603		SELECTIVE CATALYTIC REDUCTION SYSTEM (SCR) AND WET LOW-EMISSION (WLE) COMBUSTORS SUBJECT TO LAER	2.5	PPMVD@15%O2	LAER	LAER, Aeroderivatives
		PSEG FOSSIL LLC KEARNY									
NJ-0076	9/16/2010	GENERATING STATION HOWARD DOWN STATION	PSEG FOSSIL LLC VINELAND MUNICIPAL ELECTRIC UTILITY (VMEU)	NJ			SCR and Use of Clean Burning Fuel: Natural gas THE TURBINE WILL UTILIZE WATER INJECTION AND SELECTIVE CATALYTIC REDUCTION (SCR) TO CONTROL NOX EMISSION AND USE CLEAN FUELS NATURAL GAS AND ULTRA LOW SULFUR DISTILLATE OIL TO MINIMIZE NOX EMISSIONS		PPMVD@15%O2	OTHER CASE-BY-CASE OTHER CASE-BY-CASE	Aeroderivatives Aeroderivatives
*CA-1238	10/13/2016	PUENTE POWER		CA		MW			PPMVD	OTHER CASE-BY-CASE	Aeroderivatives
CA-1175	7/2/2008	ESCONDIDO ENERGY CENTER LLC		CA	46.5		SCR water injection		PPMV@15% OXYGE	BACT-PSD	Aeroderivatives
CA-1173	12/11/2009	EL CAJON ENERGY LLC	EL CAJON ENERGY LLC	CA	49.95		Water injection and SCR		PPMV	BACT-PSD BACT-PSD	Aeroderivatives
*OR-0050	3/5/2014	TROUTDALE ENERGY CENTER, LLC	TROUTDALE ENERGY CENTER, LLC	OR	1690	MMBtu/hr	Utilize water injection when combusting natural gas or ULSD; Utilize selective catalytic reduction (SCR) with aqueous ammonia injection at all times except during startup and shutdown; Limit the time in startup or shutdown.	2.5	PPMDV AT 15% O2	BACT-PSD	Aeroderivatives
*NJ-0086	8/26/2016		BAYONNNE ENERGY CENTER LLC	NJ		MMBTU/YR	Selective Catalytic Reduction, water injection, use of natural gas a low NOx emitting fuel		PPMVD@15%O2	LAER	LAER and Aeroderivatives
CA-1176	12/4/2008	ORANGE GROVE PROJECT	BATOMINE ENERGY SENTER EES	CA	49.8		SCR water injection		PPM	BACT-PSD	Aeroderivatives
*ND-0029		PIONEER GENERATING STATION	BASIN ELECTRIC POWER COOPERATIVE	ND		MMBtu/hr	Water injection plus SCR		PPPMVD	BACT-PSD	Aeroderivatives
LA-0307	3/21/2016	MAGNOLIA LNG FACILITY	MAGNOLIA LNG, LLC	LA	333	mm btu/hr	Dry Low NOX burners and good combustion practices	5	PPMVD@15% O2	LAER	LAER
*ND-0030	9/16/2013	LONESOME CREEK GENERATING STATION	BASIN ELECTRIC POWER COOP.	ND	412	MMBtu/hr	SCR	5	PPMVD	BACT-PSD	Aeroderivatives
*WY-0070	8/28/2012	CHEYENNE PRAIRIE GENERATING STATION	BLACK HILLS POWER, INC.	WY	40	MW	SCR	5	PPMV AT 15% O2	BACT-PSD	Aeroderivatives
TX-0540		BOSQUE COUNTY POWER PLANT	BOSQUE POWER COMPANY LLC	TX	170	MW	BACT IS 9 PPMVD AT 15% O2 THROUGH THE USE OF DRY LOW-NOX (DLN) COMBUSTERS WHEN THE COMBUSTION TURBINE IS OPERATING IN THE SIMPLE CYCLE MODE.	9	PPMVD	BACT-PSD	
FL-0354	8/25/2015	LAUDERDALE PLANT	FLORIDA POWER & LIGHT	FL		MMBtu/hr (approx)	Dry-low-NOx combustion system. Wet injection when firing ULSD.		PPMVD@15%O2	BACT-PSD	
*TX-0733	5/12/2015	ANTELOPE ELK ENERGY CENTER	GOLDEN SPREAD ELECTRIC COOPERATIVE, INC.	TX		MW	Dry Low NOx burners		PPMVD AT 15% O2	BACT-PSD	
*ND-0028	2/22/2013	R.M. HESKETT STATION	MONTANA-DAKOTA UTILITIES CO.	ND		MMBTU/H	Dry low-NOx combustion (DLN)		PPMVD @15% OYYO	BACT-PSD	
FL-0319	3/10/2009	GREENLAND ENERGY CENTER	JACKSONVILLE ELECTRIC AUTHORITY (JEA)	FL		GAL/YR	DLN Combustion System when firing natural gas and water injection system when firing fuel oil.		PPMVD @15% O2 (G	BACT-PSD	
FL-0310	1/12/2009	SHADY HILLS GENERATING STATION	SHADY HILLS POWER COMPANY	FL		MW	FIRING NATURAL GAS AND USING DLN 2.6 COMBUSTORS TO MINIMIZE NOX EMISSSIONS.		PPMVD @ 15% O2	BACT-PSD	
*TX-0734	5/8/2015	CLEAR SPRINGS ENERGY CENTER (CSEC)	NAVASOTA SOUTH PEAKERS OPERATING COMPANY II, LLC.	TX	193	MW	dry low-NOx (DLN) burners	0	PPMVD @ 15% O2	BACT-PSD	
LA-0316	2/17/2017	CAMERON LNG FACILITY	CAMERON LNG LLC	LA		mm btu/hr	good combustion practices and dry low nox burners		PPMVD @ 15% O2	BACT-PSD	
TX-0764		NACOGDOCHES POWER ELECTRIC GENERATING PLANT	NACOGDOCHES POWER, LLC	TX		MW	Dry Low NOx burners, good combustion practices, limited operations		PPMVD @ 15% O2	BACT-PSD	
TX-0768	10/9/2015	SHAWNEE ENERGY CENTER	SHAWNEE ENERGY CENTER, LLC	TX	230	MW	Dry Low NOx burners	9	PPMVD @ 15% O2	BACT-PSD	

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Emission Limit 1	Units	Туре	Notes
TX-0769	10/27/2015	VAN ALSTYNE ENERGY CENTER (VAEC)	NAVASOTA NORTH COUNTRY PEAKERS OPERATING COMPANY I	TX		MW	DLN burners	9	PPMVD @ 15% O2	BACT-PSD	
TX-0777	12/9/2015	UNION VALLEY ENERGY CENTER	NAVASOTA SOUTH PEAKERS OPERATING COMPANY I, LLC.	TX		MW	dry low NOX burners		PPMVD @ 15% O2	BACT-PSD	
12-0111	1292013	CENTER	SI ELIVINICO COM TAVI I, EEC.	1/	100	NVV	Emission controls consist of dry low-NOx combustors (DLN). DLN combustors use two stages of combustion, transitioning from initial startup with fuel and flame in the primary nozzles only, through a lean lean stage with fuel and flame in the primary and secondary nozzles, to fuel in the secondary stage only, extinguishing the primary flame, and in full operation, premix mode, with fuel to both nozzles, but flame only in the second stage. When		1 MVD @ 13% 02	BAC11 08	
		HILL COUNTY GENERATING					natural gas and air are well-mixed before combustion, the flame temperature and resulting NOx emissions are greatly reduced compared to conventional diffusion				
TX-0794	4/7/2016	FACILITY	BRAZOS ELECTRIC COOPERATIVE	TX	171	MW	flame combustion.	9	PPMVD @ 15% O2	BACT-PSD	
							Required to employ dry low-NOx technology and wet injection. Water injection must be used when firing				
*FL-0346	4/22/2014	LAUDERDALE PLANT PSO RIVERSIDE JENKS	FLORIDA POWER & LIGHT PUBLIC SERVICE CO OF	FL	2000	MMBtu/hr (approx)	ULSD.	9	PPMVD @ 15% 02	BACT-PSD	
OK-0120	3/22/2007	POWER STA	OKLAHOMA	OK			DRY-LOW NOX BURNERS	9	PPMVD	BACT-PSD	
*TX-0694	2/2/2015	INDECK WHARTON ENERGY CENTER	INDECK WHARTON, L.L.C.	TX	220	MW	DLN combustors	9	PPMVD	BACT-PSD	
*TX-0695	8/1/2014	ECTOR COUNTY ENERGY CENTER	INVENERGY THERMAL DEVELOPMENT LLC	TX	180	MW	DLN combustors	q	PPMVD	BACT-PSD	
*TX-0696	9/22/2014	ROAN'S PRAIRIE GENERATING STATION	TENASKA ROAN'S PRAIRIE PARTNERS (TRPP), LLC	TX		MW	DLN combustors		PPMVD	BACT-PSD	
*TX-0701	5/13/2013	ECTOR COUNTY ENERGY CENTER	INVENERGY THERMAL DEVELOPMENT LLC	TX		MW	Dry low NOx combustor	9	PPMVD	BACT-PSD	
TX-0819	4/28/2017	GAINES COUNTY POWER PLANT	SOUTHWESTERN PUBLIC SERVICE COMPANY	TX	227.5	MW	Dry Low NOx burners (control), natural gas, good combustion practices, limited operating hours (prevention)	9) PPMV	BACT-PSD	
GA-0139	5/14/2010	DAHLBERG COMBUSDTION TURBINE ELECTRIC GENERATING FACILITY (P	SOUTHERN POWER COMPANY	GA	1530	MW	DRY LOW NOX BURNERS (FIRING NATURAL GAS). WATER INJECTION (FIRING FUEL OIL).	9	PPM@15%02	BACT-PSD	
*MN-0075	7/1/2008	GREAT RIVER ENERGY - ELK RIVER STATION	GREAT RIVER ENERGY	MN	2169	MMBTU/H	DRY LOW-NOX COMBUSTION WHEN COMBUSTING NATURAL GAS	9	PPM	BACT-PSD	
MN-0075	7/1/2008	GREAT RIVER ENERGY - ELK RIVER STATION	GREAT RIVER ENERGY	MN		MMBTU/H	DRY LOW-NOX COMBUSTION WHEN COMBUSTING NATURAL GAS		PPM	BACT-PSD	
*TX-0686	4/22/2014	ANTELOPE ELK ENERGY CENTER	GOLDEN SPREAD ELECTRIC COOPERATIVE, INC.	TX	202	MW	DLN	9	PPM	BACT-PSD	
*TX-0688	12/19/2014	SR BERTRON ELECTRIC GENERATION STATION	NRG TEXAS POWER	TX	225	MW	DLN	9	PPM	BACT-PSD	
TX-0788	3/24/2016	NECHES STATION	APEX TEXAS POWER LLC	TX	232	MW	Dry low-NOx burners (DLN), good combustion practices	9	PPM	BACT-PSD	
FL-0355	9/10/2015	FORT MYERS PLANT	FLORIDA POWER & LIGHT (FPL) PROGRESS ENERGY FLORIDA	FL	2262.4	MMBtu/hr gas	DLN and wet injection (for ULSD operation)	9	PPMVD@15% O2	BACT-PSD	
FL-0285	1/26/2007	PLANT	(PEF)	FL	1972	MMBTU/H	WATER INJECTION DRY LOW NOX	15	PPMVD	BACT-PSD	
*TX-0691	5/20/2014	PH ROBINSON ELECTRIC GENERATING STATION	NRG TEXAS POWER LLC	TX	65	MW	DLN combustors	15	PPMVD	BACT-PSD	
*IN-0173	6/4/2014	MIDWEST FERTILIZER CORPORATION	MIDWEST FERTILIZER CORPORATION	IN	283	MMBTU/H, EACH	DRY LOW NOX COMBUSTORS	22.65	PPMVD AT 15% OXY	BACT-PSD	
*IN-0180	6/4/2014	MIDWEST FERTILIZER CORPORATION	MIDWEST FERTILIZER CORPORATION	IN	283	MMBTU/H, EACH	DRY LOW NOX COMBUSTORS	22.65	PPMVD AT 15% OXY	BACT-PSD	
*IN-0264	1/6/2017	MONTPELIER GENERATING STATION	AES OHIO GENERATION, LLC	IN	270.9	MMBTU/H	WATER INJECTION	25	PPMV	BACT-PSD	
OK-0127	6/13/2008	WESTERN FARMERS ELECTRIC ANADARKO	WESTERN FARMERS ELECTRIC COOPERATIVE	ОК	462.7	MMBTU/H	WATER INJECTION	25	PPM	BACT-PSD	
*MN-0075	7/1/2008	GREAT RIVER ENERGY - ELK RIVER STATION	GREAT RIVER ENERGY	MN	2169	MMBTU/H	WATER INJECTION WHEN COMBUSTING FUEL OIL	42	PPM	BACT-PSD	
MN-0075	7/1/2008	GREAT RIVER ENERGY - ELK RIVER STATION	GREAT RIVER ENERGY	MN	2169	MMBTU/H	WATER INJECTION WHEN COMBUSTING FUEL OIL	42	PPM	BACT-PSD	
IL-0121	9/27/2016	INVENERGY NELSON EXPANSION LLC	INVENERGY	IL	190	MW	low-NOx combustion technology and water injection for ULSD.	5	LB/H	BACT-PSD	
*CO-0076	12/11/2014	PUEBLO AIRPORT GENERATING STATION	BLACK HILLS ELECTRIC GENERATION, LLC	СО	799.7	mmbtu/hr each	SCR and dry low NOx burners	23	LB/H	BACT-PSD	Aeroderivatives

Table D-1 - RBLC Results for NOx Emissions for Simple Cycle Combustion Turbine (Natural Gas)

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Emission Limit 1	Units	Туре	Notes
OH-0333		DAYTON POWER & LIGHT ENERGY LLC	DAYTON POWER & LIGHT COMPANY	ОН	15020	H/YR	dry low NOx burners	161	LB/H	BACT-PSD	
LA-0258	12/21/2011	CALCASIEU PLANT	ENTERGY GULF STATES LA LLC	LA	1900	MM BTU/H EACH	DRY LOW NOX COMBUSTORS	240	LB/H	BACT-PSD	
IN-0261	2/28/2017	VERMILLION GENERATING STATION	DUKE ENERGY INDIANA, LLC VERMILLION GENERATING STA	IN	80	MW	GOOD COMBUSTION PRACTICES	250	LB/H	BACT-PSD	
OH-0333		DAYTON POWER & LIGHT ENERGY LLC	DAYTON POWER & LIGHT COMPANY	ОН	4216	H/YR	Water injection	269	LB/H	BACT-PSD	
LA-0224		ARSENAL HILL POWER PLANT	SOUTHWEST ELECTRIC POWER COMPANY (SWEPCO)	LA	2110		ACCORDING TO MANUFACTURE'S RECOMMENDED PROCEDURES.	400	LB/H	BACT-PSD	
LA-0224		ARSENAL HILL POWER PLANT	SOUTHWEST ELECTRIC POWER COMPANY (SWEPCO)	LA	2110		COMPLETE EVENTS AS QUICKLY AS POSSIBLE ACCORDING TO MANUFACTURE'S RECOMMENDED PROCEDURES.	400	LB/H	BACT-PSD	
FL-0310	1/12/2009	SHADY HILLS GENERATING STATION	SHADY HILLS POWER COMPANY	FL	2.5	MW	PURCHASE MODEL IS AT LEAST AS STRINGENT AS THE BACT VALUES, UNDER EPA CERTIFICATION.	6.9	G/HP-H	BACT-PSD	
GA-0139		DAHLBERG COMBUSDTION TURBINE ELECTRIC GENERATING FACILITY	SOUTHERN POWER COMPANY	GA	1530		DRY LOW NOX BURNERS (FIRING NATURAL GAS), WATER INJECTION (FIRING FUEL OIL).	297	T/YR	BACT-PSD	

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Emission Limit 1	Units	Туре	Notes
*NJ-0086	8/26/2016	BAYONNNE ENERGY CENTER	BAYONNNE ENERGY CENTER LLC	NJ	720	H/YR	SCR and water injection		PPMVD@1 5% O2	LAER	LAER, Aeroderivatives
TX-0794		HILL COUNTY GENERATING FACILITY	BRAZOS ELECTRIC COOPERATIVE	TX	171	MW	DLN, WATER INJECTION		PPMVD @ 15% O2	BACT- PSD	
WI-0240	1/26/2006	WE ENERGIES CONCORD	WISCONSIN ELECTRIC POWER	WI	100	mw	WATER INJECTION		PPMDV @ 15% O2	BACT- PSD	
OH-0253		DAYTON POWER AND LIGHT COMPANY	DAYTON POWER AND LIGHT COMPANY	ОН	1115	MMBTU/ H	WATER INJECTION	195	LB/H	BACT- PSD	
OH-0253		DAYTON POWER AND LIGHT COMPANY	DAYTON POWER AND LIGHT COMPANY	ОН	1115	MMBTU/ H	WATER INJECTION	195	LB/H	BACT- PSD	
OH-0333		DAYTON POWER & LIGHT ENERGY LLC	DAYTON POWER & LIGHT COMPANY	ОН	4216	H/YR	Water injection	269	LB/H	BACT- PSD	

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Emission Limit 1	Units	Туре	Notes
MD-0040	11/12/2008	CPV ST CHARLES	COMPETITIVE POWER VENTURES, INC./CPV MARYLAND, LLC	MD			OXIDATION CATALYST	2	PPMVD @ 15% O2	BACT-PSD	Combined cycle
			COMPETITIVE POWER VENTURES,								,
MD-0040	11/12/2008	CPV ST CHARLES	INC./CPV MARYLAND, LLC	MD			OXIDATION CATALYST Oxidation catalyst:	2	PPMVD @ 15% O2	BACT-PSD	Combined cycle
*OR-0050	3/5/2014	TROUTDALE ENERGY CENTER, LLC	TROUTDALE ENERGY CENTER, LLC	OR	2988	MMBtu/hr	Limit the time in startup or shutdown.	3.3	PPMDV AT 15% O2	BACT-PSD	Combined cycle
*MN-0075	7/1/2008	GREAT RIVER ENERGY - ELK RIVER STATION	GREAT RIVER ENERGY	MN	2169	MMBTU/H MMBtu/hr	GOOD COMBUSTION PRACTICES	4	PPM	BACT-PSD	Refuse-derived fuel
FL-0354	8/25/2015	LAUDERDALE PLANT	FLORIDA POWER & LIGHT	FL	2100	(approx)	Good combustion minimizes CO formation	4	PPMVD@15%O2	BACT-PSD	
*FL-0346	4/22/2014	LAUDERDALE PLANT	FLORIDA POWER & LIGHT	FL	2000	MMBtu/hr (approx)	Good combustion practices	4	PPMVD @ 15% O2	BACT-PSD	Combined cycle
*TX-0694	2/2/2015	INDECK WHARTON ENERGY CENTER	INDECK WHARTON, L.L.C.	TX	220	MW	DLN combustors	4	PPMVD	BACT-PSD	Combined cycle
FL-0319	3/10/2009	GREENLAND ENERGY CENTER	JACKSONVILLE ELECTRIC AUTHORITY (JEA)	FL	30213	GAL/YR	Good Combustion	4.1	PPMVD @ 15% O2 (GAS)	BACT-PSD	
		BAYONNNE ENERGY CENTER	BAYONNNE ENERGY CENTER LLC	NJ	0440000	MADTHAD	Add-on control is CO Oxidation Catalyst, and use of natural gas as				
*NJ-0086	8/26/2016	BAYONNNE ENERGY CENTER	BAYONNNE ENERGY CENTER LLC	NJ	2143980	MMBTU/YR	fuel for pollution prevention	5	PPMVD@15%O2	BACT-PSD	
NJ-0075	9/24/2009	BAYONNE ENERGY CENTER	BAYONNE ENERGY CENTER, LLC	NJ	603	MMBTU/H	CO OXIDATION CATALYST AND CLEAN BURNING FUELS	5	PPMVD@15%O2	OTHER CASE-BY-CASE	Aeroderivatives
NJ-0076	10/27/2010	PSEG FOSSIL LLC KEARNY GENERATING STATION	PSEG FOSSIL LLC	NJ	8940000	MMBtu/year (HHV)	Oxidation Catalyst, Good combustion practices CONTROL CO EMISSION, IN ADDITION TO USING CLEAN	5	PPMVD@15% O2	OTHER CASE-BY-CASE	Aeroderivatives
NJ-0077	9/16/2010	HOWARD DOWN STATION	VINELAND MUNICIPAL ELECTRIC UTILITY (VMEU)	NJ	5000	MMFT3/YR	BURNING FUELS, NATURAL GAS AND ULTRA LOW SULFUR DISTILLATE OIL WITH 15 PPM SULFUR BY WEIGHT	5	PPMVD@15%O2	OTHER CASE-BY-CASE	Aeroderivatives
		CHEYENNE PRAIRIE GENERATING		1407							
*WY-0070	8/28/2012	STATION CHEYENNE PRAIRIE GENERATING	BLACK HILLS POWER, INC.	WY	40	MW	Oxidiation Catalyst	b	PPMV AT 15% O2	BACT-PSD	Aeroderivatives
*WY-0070	8/28/2012	STATION	BLACK HILLS POWER, INC.	WY	40	MW	Oxidation Catalyst	6	PPMV AT 15% O2	BACT-PSD	Aeroderivatives
*WY-0070	8/28/2012	CHEYENNE PRAIRIE GENERATING STATION	BLACK HILLS POWER, INC.	WY	40	MW	Oxidation Catalyst	6	PPMV AT 15% O2	BACT-PSD	Aeroderivatives
*ND-0029	5/14/2013	PIONEER GENERATING STATION	BASIN ELECTRIC POWER COOPERATIVE	ND	451	MMBtu/hr	Catalytic oxidation system	6	PPMVD	BACT-PSD	Aeroderivatives
*ND-0030	9/16/2013	LONESOME CREEK GENERATING STATION	BASIN ELECTRIC POWER COOP.	ND	412	MMBtu/hr	Oxidation Catalyst	6	PPMVD	BACT-PSD	Aeroderivatives
*OR-0050	3/5/2014	TROUTDALE ENERGY CENTER, LLC	TROUTDALE ENERGY CENTER, LLC	OR	1690	MMBtu/hr	Oxidation catalyst; Limit the time in startup or shutdown.	6	PPMDV AT 15% O2	BACT-PSD	Aeroderivatives
									PPMVD @ 15% O2		
FL-0310	1/12/2009	SHADY HILLS GENERATING STATION	SHADY HILLS POWER COMPANY	FL	1/0	MW		6.5	NG	BACT-PSD	Aeroderivatives
FL-0285	1/26/2007	PROGRESS BARTOW POWER PLANT	PROGRESS ENERGY FLORIDA (PEF)	FL	1972	MMBTU/H	GOOD COMBUSTION	8	PPMVD	BACT-PSD	Combined cycle
GA-0139	5/14/2010	DAHLBERG COMBUSDTION TURBINE ELECTRIC GENERATING FACILITY (P	SOUTHERN POWER COMPANY	GA	1530	MW	GOOD COMBUSTION PRACTICES	9	PPM@15%02	BACT-PSD	
TX-0540	2/27/2009	BOSQUE COUNTY POWER PLANT	BOSQUE POWER COMPANY LLC	TX	170	MW	MINIMIZE THE PRODUCTS OF INCOMPLETE COMBUSTION AND ACHIEVE 9 PPMVD AT 15% O2 IN THE TURBINE EXHAUST OVER A ROLLING 3-HOUR PERIOD.	9	PPMVD	BACT-PSD	
TX-0777	12/9/2015	UNION VALLEY ENERGY CENTER	NAVASOTA SOUTH PEAKERS OPERATING COMPANY I, LLC.	TX	193	8 MW	dry low NOx burners and good combustion practices	a	PPMVD @ 15% O2		
		ANTELOPE ELK ENERGY CENTER	GOLDEN SPREAD ELECTRIC COOPERATIVE, INC.	TX		MW	Good combustion practices; limited hours		PPMVD	BACT-PSD	
*TX-0686	4/22/2014	SR BERTRON ELECTRIC GENERATION						-			
*TX-0688	12/19/2014	STATION	NRG TEXAS POWER INVENERGY THERMAL DEVELOPMENT	TX	225	MW	Good Combustion Practices	9	PPM	BACT-PSD	
*TX-0695	8/1/2014	ECTOR COUNTY ENERGY CENTER	LLC	TX	180	MW	DLN combustors	9	PPMVD	BACT-PSD	
*TX-0696	9/22/2014	ROAN'S PRAIRIE GENERATING STATION	TENASKA ROAN'S PRAIRIE PARTNERS (TRPP), LLC	TX	600	MW	DLN combustors	g	PPMVD	BACT-PSD	
*TX-0701	5/13/2013	ECTOR COUNTY ENERGY CENTER	INVENERGY THERMAL DEVELOPMENT LLC	TX	180	MW	Good combustion practices	g	PPMVD	BACT-PSD	
*TX-0733	5/12/2015	ANTELOPE ELK ENERGY CENTER	GOLDEN SPREAD ELECTRIC COOPERATIVE, INC.	TX	202	MW	Good combustion practices; limited operating hours	9	PPMVD @ 15% O2	BACT-PSD	
*TX-0734	5/8/2015	CLEAR SPRINGS ENERGY CENTER (CSEC)	NAVASOTA SOUTH PEAKERS OPERATING COMPANY II, LLC.	TX	183	8 MW	DLN burners and good combustion practices	9	PPMVD @ 15% O2	BACT-PSD	
TX-0764	10/14/2015	NACOGDOCHES POWER ELECTRIC GENERATING PLANT	NACOGDOCHES POWER, LLC	TX		MW	dry low NOx burners, good combustion practices, limited operation		PPMVD @ 15% O2		
		NACOGDOCHES POWER ELECTRIC								DAGT BOD	
TX-0764	10/14/2015	GENERATING PLANT	NACOGDOCHES POWER, LLC	TX	232	MW	dry low NOx burners, good combustion practices, limited operation	9	PPMVD @ 15% O2	BACT-PSD	

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput Units	Control Device	Emission Limit 1	Units	Туре	Notes
KDEGID	1 dillin bato	1 acmty Name	Corporation	Otate	Tilloughput Ollits	33/10/ 20/100		Onics	Туре	Hotes
TX-0768	10/9/2015	SHAWNEE ENERGY CENTER	SHAWNEE ENERGY CENTER, LLC	TX	230 MW	dry low NOx burners and Imitted operation, clean fuel	9	PPMVD @ 15% O2		
TX-0768	10/9/2015	SHAWNEE ENERGY CENTER	SHAWNEE ENERGY CENTER, LLC	TX	230 MW	dry low NOx burners and Imilted operation, clean fuel	,	PPMVD @ 15% O2	BACT-PSD	
174-07-00	10/3/2013	SIN WILL ENERGY SERVER	STATE CHEROLOGIA CENTER, EES	17.	200	Premixing of fuel and air enhances combustion efficiency and		7.1 mvD @ 10% 02	5,101,105	
TX-0794	4/7/2016	HILL COUNTY GENERATING FACILITY	BRAZOS ELECTRIC COOPERATIVE	TX	171 MW	minimizes emissions.	9	PPMVD @ 15% O2		
TX-0769	10/27/2015	VAN ALSTYNE ENERGY CENTER (VAEC)	NAVASOTA NORTH COUNTRY PEAKERS OPERATING COMPANY I	TX	183 MW	DLN burners and good combustion practices	9	PPMVD @ 15% O2		
			NAVASOTA NORTH COUNTRY PEAKERS							
TX-0769	10/27/2015	VAN ALSTYNE ENERGY CENTER (VAEC)		TX	183 MW	DLN burners and good combustion practices	9	PPMVD @ 15% O2	BACT-PSD	
TX-0777	12/9/2015	UNION VALLEY ENERGY CENTER	NAVASOTA SOUTH PEAKERS OPERATING COMPANY I, LLC.	TX	183 MW	dry low NOx burners and good combustion practices	Ş	PPMVD @ 15% O2	BACT-PSD	
TV 0700	0/04/0040	NECHES STATION	APEX TEXAS POWER LLC	TX	232 MW	good combustion practices		PPM	BACT-PSD	
TX-0788	3/24/2016	NECHESSIATION	AFEX TEXAS FOWER LLC	1/	232 WW	good combustion practices		FFW	BACT-P3D	
TX-0788	3/24/2016	NECHES STATION	APEX TEXAS POWER LLC	TX	232 MW	good combustion practices	9	PPM		
TX-0819	4/28/2017	GAINES COUNTY POWER PLANT	SOUTHWESTERN PUBLIC SERVICE COMPANY	TX	227.5 MW	Good combustion practices; limited operating hours	9	PPMVD		
						Premixing of fuel and air enhances combustion efficiency and				
TX-0794	4/7/2016	HILL COUNTY GENERATING FACILITY	BRAZOS ELECTRIC COOPERATIVE	TX	171 MW	minimizes emissions.	9	PPMVD @ 15% O2	BACT-PSD	
LA-0316	2/17/2017	CAMERON LNG FACILITY	CAMERON LNG LLC	LA	1069 mm btu/hr	good combustion practices and fueled by natural gas	15	PPMVD	BACT-PSD	
		B.M. UEGVETT OTATION	MONTHUA DAMOTA LITE ITEO CO					PPMVD @ 15%	2107.000	
*ND-0028	2/22/2013	R.M. HESKETT STATION	MONTANA-DAKOTA UTILITIES CO.	ND	986 MMBTU/H	Good Combustion	28	OXYGEN	BACT-PSD	
OK-0127	6/13/2008	WESTERN FARMERS ELECTRIC ANADARKO	WESTERN FARMERS ELECTRIC COOPERATIVE	OK	462.7 MMBTU/H	NO CONTROLS FEASIBLE.	63	PPM	BACT-PSD	
*MN-0075	7/1/2008	GREAT RIVER ENERGY - ELK RIVER STATION	GREAT RIVER ENERGY	MN	2169 MMBTU/H	GOOD COMBUSTION CONTROL	150	PPM	BACT-PSD	
WIN-0073	77 17 2000	GREAT RIVER ENERGY - ELK RIVER	GREAT RIVER ENERGY	IVIIV	2109 WWW.DTO/TT	GOOD COMISSION CONTROL	150		BACT-1 GD	
MN-0075	7/1/2008	STATION	GREAT RIVER ENERGY	MN	2169 MMBTU/H	GOOD COMBUSTION CONTROL	150	PPM	BACT-PSD	
*MN-0075	7/1/2008	GREAT RIVER ENERGY - ELK RIVER STATION	GREAT RIVER ENERGY	MN	2169 MMBTU/H	GOOD COMBUSTION CONTROL	250	PPM	BACT-PSD	
		GREAT RIVER ENERGY - ELK RIVER								
MN-0075	7/1/2008	STATION	GREAT RIVER ENERGY	MN	2169 MMBTU/H	GOOD COMBUSTION CONTROL	250	PPM	BACT-PSD	
*IN-0264	1/6/2017	MONTPELIER GENERATING STATION	AES OHIO GENERATION, LLC	IN	270.9 MMBTU/H	NATURAL GAS AS PRIMARY FUEL; GOOD COMBUSTION PRACTICES	0.2	LB/MMBTU	LAER	
*IN 0470	0/4/0044	MIDWEST FERTILIZER CORPORATION	MIDWEST FERTILIZER CORPORATION	IN	MMBTU/H,	GOOD COMBUSTION PRACTICES AND PROPER DESIGN	0.00	LB/MMBTU	BACT-PSD	
*IN-0173	6/4/2014	MIDWEST FERTILIZER CORFORATION	WIDWEST FERTILIZER CORFORATION	IIN	MMBTU/H.	GOOD COMBUSTION FRACTICES AND FROPER DESIGN	0.00	LB/MINIB I U	BACT-P3D	
*IN-0180	6/4/2014	MIDWEST FERTILIZER CORPORATION	MIDWEST FERTILIZER CORPORATION	IN	283 EACH	GOOD COMBUSTION PRACTICES AND PROPER DESIGN	0.03	LB/MMBTU	BACT-PSD	
LA-0307	3/21/2016	MAGNOLIA LNG FACILITY	MAGNOLIA LNG, LLC	LA	333 mm btu/hr	good combustion practices and fueled by natural gas	0.062	LB/MM BTU	OTHER CASE-BY-CASE	
		TENASKA PA								
*PA-0306	2/12/2016	PARTNERS/WESTMORELAND GEN FAC	TENASKA PA PARTNERS LLC	PA	0	Oxidation Catalyst and good combustion practice	15.9	LB/HR		
*PA-0306	2/12/2016	TENASKA PA PARTNERS/WESTMORELAND GEN FAC	TENASKA PA PARTNERS LLC	PA	0	Oxidation Catalyst and good combustion practice	15.9	LB/HR	BACT-PSD	
14.005	40/0/224	CADINE DACC INC TERMINA	SABINE PASS LNG, LP & SABINE PASS		200 14407117	Cond combustion practices and full-district to the	47.11	I DA	DAOT SOS	
LA-0257	12/6/2011	SABINE PASS LNG TERMINAL	LIQUEFACTION, LL	LA	286 MMBTU/H	Good combustion practices and fueled by natural gas DRY LOW EMISSIONS (DLE) COMBUSTION TECHNOLOGY	17.48	LB/H	BACT-PSD	
LA-0219	8/15/2007	CREOLE TRAIL LNG IMPORT TERMINAL	CREOLE TRAIL LNG, LP	LA	30 MW EA.	WITH LEAN PREMIX OF AIR AND FUEL	17.8	LB/H	BACT-PSD	
*CO-0076	12/11/2014	PUEBLO AIRPORT GENERATING STATION	BLACK HILLS ELECTRIC GENERATION, LLC	со	mmbtu/hr 799.7 each	Catalytic Oxidation.	55	LB/H	BACT-PSD	
22 00/0		-								
OK-0120	3/22/2007	PSO RIVERSIDE JENKS POWER STA	PUBLIC SERVICE CO OF OKLAHOMA	OK		GOOD COMBUSTION PRACTICES & DESIGN		LB/H	BACT-PSD	
OH-0333	12/3/2009	DAYTON POWER & LIGHT ENERGY LLC	DAYTON POWER & LIGHT COMPANY	OH	15020 H/YR	efficient combution technology	301	LB/H	BACT-PSD	
IN-0261	2/28/2017	VERMILLION GENERATING STATION	DUKE ENERGY INDIANA, LLC VERMILLION GENERATING STA	IN	80 MW	GOOD COMBUSTION PRACTICES	525	LB/H	BACT-PSD	
LA-0258	12/21/2011	CALCASIEU PLANT	ENTERGY GULF STATES LA LLC	LA	MM BTU/H 1900 EACH	DRY LOW NOX COMBUSTORS	781	LB/H	BACT-PSD	
OH-0333	12/3/2009	DAYTON POWER & LIGHT ENERGY LLC	DAYTON POWER & LIGHT COMPANY SOUTHWEST ELECTRIC POWER	ОН	4216 H/YR	efficient combustion technology COMPLETE EVENTS AS QUICKLY AS POSSIBLE ACCORDING	800	LB/H	BACT-PSD	
LA-0224	3/20/2008	ARSENAL HILL POWER PLANT	COMPANY (SWEPCO) SOUTHWEST ELECTRIC POWER	LA	2110 MMBTU/H	TO MANUFACTURE'S RECOMMENDED PROCEDURES. COMPLETE EVENTS AS QUICKLY AS POSSIBLE ACCORDING	964.57	LB/H	BACT-PSD	
LA-0224	3/20/2008	ARSENAL HILL POWER PLANT	COMPANY (SWEPCO)	LA	2110 MMBTU/H	TO MANUFACTURE'S RECOMMENDED PROCEDURES.	1508.15	LB/H	BACT-PSD	

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput U	Inits	Control Device	Emission Limit 1	Units	Туре	Notes
FL-0310	1/12/2009	SHADY HILLS GENERATING STATION	SHADY HILLS POWER COMPANY	FL	2.5 MW		PURCHASED MODEL IS AT LEAST AS STRINGENT AS THE BACT VALUES UNDER EPA'S CERTIFICATION.	8.5	G/HP-H	BACT-PSD	

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Emission Limit 1	Units	Туре	Notes
*NJ-0086	8/26/2016	BAYONNNE ENERGY CENTER	BAYONNNE ENERGY CENTER LLC	NJ	720	H/YR	Oxidation Catalyst	5	PPMVD@ 15%O2	OTHER CASE-BY- CASE	LAER, Aeroderivatives
NV-0036	5/5/2005		NEWMONT NEVADA ENERGY INVESTMENT, LLC	NV	373.3	MMBTU/H	OXIDATION CATALYST	6	PPMVD	BACT-PSD	Aeroderivatives
FL-0319	3/10/2009		JACKSONVILLE ELECTRIC AUTHORITY (JEA)	FL	30213	GAL/YR	Good Combustion	8	PPMVD @ 15% O2 (GAS)	BACT-PSD	Aeroderivatives
TX-0794	4/7/2016		BRAZOS ELECTRIC COOPERATIVE	TX	171	MW	complete combustion and therefore minimizes emissions		PPMVD @ 15% O2	BACT-PSD	
TX-0525	9/13/2005	TEXAS GENCO UNITS 1 AND2	TEXAS GENCO	TX	550	MMBTU/H		71	LB/H	BACT-PSD	
TX-0525	9/13/2005	TEXAS GENCO UNITS 1 AND2	TEXAS GENCO	TX	550	MMBTU/H		112.5	LB/H	BACT-PSD	
OH-0253	3/7/2006	DAYTON POWER AND LIGHT COMPANY	DAYTON POWER AND LIGHT COMPANY	ОН	1115	MMBTU/H		350	LB/H	OTHER CASE-BY- CASE	
TX-0506		NRG TEXAS ELECTRIC POWER GENERATION	NRG TEXAS	TX	80	MW		401	LB/H	BACT-PSD	
TX-0506		NRG TEXAS ELECTRIC POWER GENERATION	NRG TEXAS	TX	80	mw		563	LB/H	BACT-PSD	
OH-0253	3/7/2006	DAYTON POWER AND LIGHT COMPANY	DAYTON POWER AND LIGHT COMPANY	ОН	1115	MMBTU/H		800	LB/H	OTHER CASE-BY- CASE	
OH-0333			DAYTON POWER & LIGHT COMPANY	ОН	4216	H/YR	efficient combustion technology	800	LB/H	BACT-PSD	

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Emission Limit 1	Units	Туре	Notes
KBEGIB	T CHINE Date	WESTERN FARMERS	WESTERN FARMERS ELECTRIC	Otato	rmougnput	Onito	Control Bevice	Emission Emile 1	Cinto	1,400	Hotes
OK-0127	6/13/2008	ELECTRIC ANADARKO	COOPERATIVE	OK	462.7	MMBTU/H	NO CONTROLS FEASIBLE.	4	LB/H	BACT-PSD	Aeroderivative
LA-0307	3/21/2016	MAGNOLIA LNG FACILITY	MAGNOLIA LNG, LLC	LA	333	mm btu/hr	good combustion practices and fueled by natural gas	5	LB/H	OTHER CASE-BY- CASE	Aorodorivativo
LA-0307	3/21/2010	INVENERGY NELSON	MAGNOLIA LING, LLC	LA	333	min blu/m	inaturai gas	3	LB/III	CAGE	Aeroderivative
IL-0121	9/27/2016	EXPANSION LLC	INVENERGY	IL	190	MW	turbine design and good combustion practices	5	LB/H	BACT-PSD	Smaller turbines
		D. 1. (0.1 1) E. 1. E. 1. E. 1. C. 1. (1. C. 1.					BURNING CLEAN FUELS, NATURAL GAS			OT 155 0405 514	
NJ-0075	9/24/2009	BAYONNE ENERGY CENTER	BAYONNE ENERGY CENTER, LLC	NJ	603	MMBTU/H	AND ULTRA LOW SULFUR DISTILLATE OIL WITH SULFUR CONTENT OF 15 PPM.	5	LB/H	OTHER CASE-BY- CASE	Not PSD
140-0073	3/24/2009	CENTER	BATONINE ENERGY GENTER, EEG	140	003	WIND TO/TT	USE OF CLEAN BURNING FUELS;	, , ,	LB/III	OAGE	NOTIOD
							NATURAL GAS AS PRIMARY FUEL AND				
		HOWARD DOWN	VINELAND MUNICIPAL ELECTRIC				ULTRA LOW SULFUR DISTILLATE OIL WITH 15 PPMSULFUR BY WEIGHT AS BACKUP				
NJ-0077	9/16/2010	STATION	UTILITY (VMEU)	NJ	5000	MMFT3/YR	FUEL THE TWEIGHT AS BACKUP	5	LB/H	BACT-PSD	Smaller turbines
		LONESOME CREEK	·								
*ND-0030	9/16/2013	GENERATING STATION PIONEER GENERATING	BASIN ELECTRIC POWER COOP. BASIN ELECTRIC POWER	ND	412	MMBtu/hr		5	LB/H	BACT-PSD	Aeroderivative
*ND-0029	5/14/2013	STATION	COOPERATIVE	ND	451	MMBtu/hr		5.4	LB	BACT-PSD	Aeroderivative
		PSEG FOSSIL LLC									
NII 0070	40/07/0040	KEARNY GENERATING	P050 5000# 11.0		004000	MMBtu/year	Good combustion practice, Use of Clean		I D#1	DAOT DOD	0
NJ-0076	10/27/2010	STATION	PSEG FOSSIL LLC	NJ	8940000	(HHV)	Burning Fuel: Natural gas	6	LB/H	BACT-PSD	Smaller turbines
*ND-0028	2/22/2013	R.M. HESKETT STATION	MONTANA-DAKOTA UTILITIES CO.	ND	986	MMBTU/H	Good Combustion Practices	7.3	LB/H	BACT-PSD	Smaller Turbine
TV 0040	4/00/0047	GAINES COUNTY	SOUTHWESTERN PUBLIC SERVICE COMPANY	TV	207.5	A 43.47	Pipeline quality natural gas; limited hours;	0.5	TAVD	DACT DCD	
TX-0819	4/28/2017	POWER PLANT UNION VALLEY ENERGY	NAVASOTA SOUTH PEAKERS	TX	227.5	IVIVV	good combustion practices pipeline quality natural gas, good combustion	8.5	T/YR	BACT-PSD	
TX-0777	12/9/2015	CENTER	OPERATING COMPANY I, LLC.	TX	183	MW	practices	8.6	LB/H	BACT-PSD	
		DAHLBERG									
		COMBUSTION TURBINE					GOOD COMBUSTION PRACTICES PIPELINE				
GA-0139	5/14/2010	ELECTRIC GENERATING FACILITY (P	SOUTHERN POWER COMPANY	GA	1530	MW	QUALITY NATURAL GAS, ULTRA LOW SULFUR DISTILLATE FUEL	9.1	LB/H	BACT-PSD	
0/10100	0/14/2010	TROUTDALE ENERGY	COOTHERITO WEIL COMM 7411	O/ t	1000	10100	Utilize only natural gas or ULSD fuel; Limit the	0.1	LB/H TOTAL	BACTION	
*OR-0050	3/5/2014	CENTER, LLC	TROUTDALE ENERGY CENTER, LLC	OR	1690	MMBtu/hr	time in startup or shutdown.	9.1	PM	BACT-PSD	Aeroderivative
		·	·				GOOD COMBUSTION PRACTICES IN				
01/ 04/00	0/00/0007	PSO RIVERSIDE JENKS	DUDU O OFDVIOL OO OF OK ALIOMA	014			COMBINATION WITH THE USE OF LOW-	40	I D#1	DAOT DOD	
OK-0120	3/22/2007	POWER STA ELECTRIC GENERATING	PUBLIC SERVICE CO OF OKLAHOMA	OK			ASH FUEL Pipeline quality natural gas; limited hours;	10	LB/H	BACT-PSD	
TX-0764	10/14/2015	PLANT	NACOGDOCHES POWER, LLC	TX	232	MW	good combustion practices.	12.09	LB/HR		
T)/ 0700	0/04/0040	NEOLIEO OTATIONI	ABEV TEVAO BOMEDILIO	T)/	000			40.4	I D#1	DAOT DOD	
TX-0788	3/24/2016	NECHES STATION	APEX TEXAS POWER LLC	TX	232	MW	good combustion practices, low sulfur fuel	13.4	LB/H	BACT-PSD	
		HILL COUNTY					Premixing of fuel and air enhances combustion				
TX-0794	4/7/2016	GENERATING FACILITY	BRAZOS ELECTRIC COOPERATIVE	TX	171	MW	efficiency and minimizes emissions.	14	LB/H	BACT-PSD	
LA-0258	12/21/2011	CALCASIEU PLANT	ENTERGY GULF STATES LA LLC	LA	1900	MM BTU/H EACH	USE OF PIPELINE NATURAL GAS	17	LB/H	BACT-PSD	
		TROUTDALE ENERGY					Utilize only natural gas or ULSD fuel; Limit the		LB/H TOTAL		
*OR-0050	3/5/2014	CENTER, LLC SHAWNEE ENERGY	TROUTDALE ENERGY CENTER, LLC	OR	2988	MMBtu/hr	time in startup or shutdown.	23.6	PM	BACT-PSD	
TX-0768	10/9/2015	CENTER	SHAWNEE ENERGY CENTER, LLC	TX	230	MW	Pipeline quality natural gas; limited hours; good combustion practices.	84.1	LB/HR	BACT-PSD	
							g				
FL-0355	9/10/2015	FORT MYERS PLANT	FLORIDA POWER & LIGHT (FPL)	FL	2262.4	MMBtu/hr gas	Use of clean fuels, and annual VE test	0.005	LB/MMBTU	BACT-PSD	
IL-0121	9/27/2016	INVENERGY NELSON EXPANSION LLC	INVENERGY	IL	190	MW	turbine design and good combustion practices	0.0066	LB/MMBTU	BACT-PSD	
3121	3,2,,2010	MONTPELIER		-	130		USE NATURAL GAS AS PRIMARY FUEL;	5.5500		2,10.100	
*IN-0264	1/6/2017	GENERATING STATION	AES OHIO GENERATION, LLC	IN	270.9	MMBTU/H	GOOD COMBUSTION PRACTICES	0.0066	LB/MMBTU	BACT-PSD	
IN-0261	2/28/2017	VERMILLION GENERATING STATION	DUKE ENERGY INDIANA, LLC VERMILLION GENERATING STA	IN	90	MW	GOOD COMBUSTION PRACTICES	0.0076	LB/MM BTU	BACT-PSD	
IIN-UZU I	2/20/2017	GLINERATING STATION	VERWILLION GENERATING STA	IIN	80	IVIVV	good combustion practices and fueled by	0.0076	LD/IVIIVI D I U	DACI-FOD	
LA-0316	2/17/2017	CAMERON LNG FACILITY	CAMERON LNG LLC	LA	1069	mm btu/hr	natural gas	0.0076	LB/MM BTU	BACT-PSD	
		MIDWEST FERTILIZER	MIDWEST FERTILIZER				GOOD COMBUSTION PRACTICES AND				
*IN-0180	6/4/2014	CORPORATION	CORPORATION	IN	283	MMBTU/H, EACH	PROPER DESIGN	0.0076	LB/MMBTU	BACT-PSD	
			COMPETITIVE POWER VENTURES,						LB/MMBTU @		
MD-0040	11/12/2008	CPV ST CHARLES	INC./CPV MARYLAND, LLC	MD				0.012	15% O2	BACT-PSD	Combined cycle

Table D-5 - RBLC Results for PM10/PM2.5 Emissions for Simple Cycle Combustion Turbine (Natural Gas)

										_	
RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Emission Limit 1	Units	Туре	Notes
			COMPETITIVE POWER VENTURES,						LB/MMBTU @		
MD-0040	11/12/2008	CPV ST CHARLES	INC./CPV MARYLAND, LLC	MD				0.012	15% O2	BACT-PSD	
		DAYTON POWER &									
OH-0333	12/3/2009		DAYTON POWER & LIGHT COMPANY	OH	15020	H/YR		0.013	LB/MMBTU	BACT-PSD	
		DAYTON POWER &									
OH-0333	12/3/2009	LIGHT ENERGY LLC	DAYTON POWER & LIGHT COMPANY	OH	4216	H/YR		0.026	LB/MMBTU	BACT-PSD	
		SHADY HILLS									
FL-0310	1/12/2009	GENERATING STATION	SHADY HILLS POWER COMPANY	FL	170	MW		10	% OPACITY	BACT-PSD	
		GREENLAND ENERGY	JACKSONVILLE ELECTRIC								
FL-0319	3/10/2009	CENTER	AUTHORITY (JEA)	FL	30213	GAL/YR	Use of low ash, low sulfur fuels,	10	OPACITY	BACT-PSD	
		GREAT RIVER ENERGY -					FUEL LIMITED TO NATURAL GAS AND				
MN-0075	7/1/2008	ELK RIVER STATION	GREAT RIVER ENERGY	MN	2169	MMBTU/H	ULTRA-LOW SULFUR FUEL OIL	0		BACT-PSD	
		GREAT RIVER ENERGY -					FUEL LIMITED TO NATURAL GAS AND				
MN-0075	7/1/2008	ELK RIVER STATION	GREAT RIVER ENERGY	MN	2169	MMBTU/H	ULTRA-LOW SULFUR FUEL OIL	0		BACT-PSD	
*TV 0004	E/00/0044	PH ROBINSON ELECTRIC		TX	0.5					BACT-PSD	
*TX-0691	5/20/2014	GENERATING STATION	NRG TEXAS POWER LLC	IX	65	MW		0		BACT-PSD	
*TX-0694	2/2/2015	INDECK WHARTON ENERGY CENTER	INDECK WHARTON, L.L.C.	TX	220	MW				BACT-PSD	
17-0094	2/2/2013	ECTOR COUNTY	INVENERGY THERMAL	1.	220	IVIVV		0		DACT-POD	
*TX-0695	8/1/2014	ENERGY CENTER	DEVELOPMENT LLC	TX	190	MW		0		BACT-PSD	
17-0093	0/1/2014	ROAN'S PRAIRIE	TENASKA ROAN'S PRAIRIE	1/	100	IVIVV		0		BACT-F3D	
*TX-0696	9/22/2014		PARTNERS (TRPP), LLC	TX	600	MW		0		BACT-PSD	
174-0030	3/22/2014	ECTOR COUNTY	INVENERGY THERMAL	17	000	IVIVV	Firing pipeline quality natural gas and good	0		DA01-1 0D	
*TX-0701	5/13/2013	ENERGY CENTER	DEVELOPMENT LLC	TX	180	MW	combustion practices	0		BACT-PSD	
17(07 0 1	0/10/2010	ENERGY GENTER	DEVELOT MEITT EEG	17.	100	10.00	compaction practices	-		BACTIOD	
		ANTELOPE ELK ENERGY	GOLDEN SPREAD ELECTRIC				Pipeline quality natural gas; limited hours;				
*TX-0733	5/12/2015	CENTER	COOPERATIVE, INC.	TX	202	MW	good combustion practices.	0		BACT-PSD	
			GOLDEN SPREAD ELECTRIC				Pipeline quality natural gas; limited hours;	1			
*TX-0733	5/12/2015	CENTER	COOPERATIVE, INC.	TX	202	MW	good combustion practices.	0		BACT-PSD	
						MMBtu/hr					
*FL-0346	4/22/2014	LAUDERDALE PLANT	FLORIDA POWER & LIGHT	FL	2000	(approx)	Good combustion practice and low-sulfur fuel	0		BACT-PSD	
		GREAT RIVER ENERGY -					FUEL LIMITED TO NATURAL GAS AND				
*MN-0075	7/1/2008	ELK RIVER STATION	GREAT RIVER ENERGY	MN	2169	MMBTU/H	ULTRA-LOW SULFUR FUEL OIL			CASE-BY-CASE BASIS	3
		GREAT RIVER ENERGY -					FUEL LIMITED TO NATURAL GAS AND				
*MN-0075	7/1/2008	ELK RIVER STATION	GREAT RIVER ENERGY	MN	2169	MMBTU/H	ULTRA-LOW SULFUR FUEL OIL			BACT-PSD	
						MMBtu/hr			GR. S / 100		
FL-0354	8/25/2015	LAUDERDALE PLANT	FLORIDA POWER & LIGHT	FL	2100	(approx)	Clean fuel prevents PM formation	2	SCF GAS	BACT-PSD	

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Emission Limit 1	Units	Туре	Notes
TX-0794	4/7/2016	HILL COUNTY GENERATING FACILITY	BRAZOS ELECTRIC COOPERATIVE	TX	171	MW	complete combustion and therefore minimizes emissions	9.8	LB/H	BACT-PSD	PM10
NV-0036	5/5/2005	TS POWER PLANT	NEWMONT NEVADA ENERGY INVESTMENT, LLC	NV	373.3	MMBTU/H	LOW ASH FUEL	13.7	LB/H	BACT-PSD	
*NJ-0086	8/26/2016	BAYONNNE ENERGY CENTER	BAYONNNE ENERGY CENTER LLC	NJ	720	H/YR	Use of ULSD, a clean burning fuel	14	LB/H	OTHER CASE-BY- CASE	Aeroderivative
OH-0253	3/7/2006	DAYTON POWER AND LIGHT COMPANY	DAYTON POWER AND LIGHT COMPANY	ОН	1115	MMBTU/H		15	LB/H	OTHER CASE-BY- CASE	
OH-0253	3/7/2006	DAYTON POWER AND LIGHT COMPANY	DAYTON POWER AND LIGHT COMPANY	ОН	1115	MMBTU/H		15	LB/H	OTHER CASE-BY- CASE	
TX-0506	4/19/2006	NRG TEXAS ELECTRIC POWER GENERATION	NRG TEXAS	TX	80	MW		15	LB/H	BACT-PSD	Smaller turbine
TX-0525	9/13/2005	TEXAS GENCO UNITS 1 AND2	TEXAS GENCO	TX	550	MMBTU/H		15	LB/H	BACT-PSD	Smaller turbine
TX-0506	4/19/2006	NRG TEXAS ELECTRIC POWER GENERATION	NRG TEXAS	TX	80	mw		19.5	LB/H	BACT-PSD	Smaller turbine
TX-0525	9/13/2005	TEXAS GENCO UNITS 1 AND2	TEXAS GENCO	TX	550	MMBTU/H		19.5	LB/H	BACT-PSD	
OH-0333	12/3/2009	DAYTON POWER & LIGHT ENERGY LLC	DAYTON POWER & LIGHT COMPANY	ОН	4216	H/YR		0.026	LB/MMBT U	BACT-PSD	

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Emission Limit 1	Units	Туре
*ND-0028	2/22/2013	R.M. HESKETT STATION	MONTANA-DAKOTA UTILITIES CO.	ND	986	MMBTU/H		413198	TONS/12 MONTH	BACT-PSD
*ND-0029	5/14/2013	GENERATING STATION	POWER COOPERATIVE	ND	451	MMBtu/hr		243147	TONS	BACT-PSD
*ND-0030	9/16/2013	CREEK GENERATING	BASIN ELECTRIC POWER COOP.	ND	412	MMBtu/hr	High efficiency turbines	220122	TONS	BACT-PSD
*IN-0173	6/4/2014	FERTILIZER CORPORATION	MIDWEST FERTILIZER CORPORATION	IN	283	MMBTU/H, EACH	PRACTICES AND PROPER DESIGN	12666	BTU/KW-H, MINIMUM	BACT-PSD
*IN-0180	6/4/2014	FERTILIZER CORPORATION	MIDWEST FERTILIZER CORPORATION	IN	283	MMBTU/H, EACH	PRACTICES AND PROPER DESIGN	12666	BTU/KW-H, MINIMUM	BACT-PSD
FL-0355	9/10/2015	FORT MYERS PLANT	FLORIDA POWER & LIGHT (FPL)	FL	2262.4	MMBtu/hr gas	Use of low-emitting fuel and efficient turbine	0.005	LB/MMBTU	BACT-PSD
IL-0121	9/27/2016	NELSON EXPANSION LLC	INVENERGY	IL	190	MW	Turbine-generator design and proper operation	0.0066	LB/MMBTU	BACT-PSD
*IN-0264	1/6/2017	GENERATING STATION	AES OHIO GENERATION, LLC	IN	270.9	MMBTU/H	FUEL; GOOD COMBUSTION PRACTICES	5	PPMVD@15%O2	OTHER CASE-BY-CASE
LA-0307	3/21/2016	MAGNOLIA LNG FACILITY	MAGNOLIA LNG, LLC	LA	333	mm btu/hr	combustion/operating/maintenanc e practices and fueled by natural	0		OTHER CASE-BY-CASE
LA-0316	2/17/2017	CAMERON LNG FACILITY	CAMERON LNG LLC	LA	1069	mm btu/hr	fueled by natural gas; Use high thermal efficiency turbines	8.6	LB/H	BACT-PSD
*PA-0306	2/12/2016	PARTNERS/WEST MORELAND GEN	TENASKA PA PARTNERS LLC	PA	0		Good combustion practices	1881905	TPY	
*OR-0050	3/5/2014	ENERGY CENTER, LLC	TROUTDALE ENERGY CENTER, LLC	OR	2988	MMBtu/hr	Thermal efficiency Clean fuels	1000	PER GROSS MWH	BACT-PSD
*OR-0050	3/5/2014	LLC	TROUTDALE ENERGY CENTER, LLC	OR	1690	MMBtu/hr	Thermal efficiency Clean fuels	1707	LB OF CO2 /GROSS MWH	BACT-PSD
TX-0761	9/15/2015	ELECTRIC GENERATING	NRG TEXAS POWER	TX	359	MW		1232	LB /MW H	
TX-0762	9/15/2015	ELECTRIC GENERATING	NRG TEXAS POWER	TX	359	MW		1232	LB CO2/MWH	
TX-0819	4/28/2017	GAINES COUNTY POWER PLANT	PUBLIC SERVICE COMPANY	TX	227.5	MW	Pipeline quality natural gas; limited hours; good combustion practices	1300	LB/MW H	
*TX-0735	05/19/2015 EST	ANTELOPE ELK ENERGY CENTER	ELECTRIC COOPERATIVE, INC.	TX	202	MW	Energy efficiency, good design & combustion practices	1304	LB CO2/MWHR	BACT-PSD
*TX-0824	6/30/2017	COUNTY GENERATING	SOUTHERN POWER	TX	920	MW	practices, and procedures, CT inlet air cooling, periodic CT burner		LB/MW HR	
TX-0788	3/24/2016	NECHES STATION	APEX TEXAS POWER LLC	TX	232	MW	good combustion practiceS	1341	LB/MW H	
FL-0354	8/25/2015	LAUDERDALE PLANT	FLORIDA POWER & LIGHT	FL	2100	MMBtu/hr (appro	Use of natural gas with restricted use of ULSD as backup fuel	1372	LB/MWH	BACT-PSD
TX-0771	11/10/2015	SHAWNEE ENERGY CENTER	SHAWNEE ENERGY CENTER, LLC	TX	230	MW		1398	LB/MWH	
TX-0794	4/7/2016	GENERATING FACILITY	BRAZOS ELECTRIC COOPERATIVE	TX	171	MW		1434	LB/MWH	
TX-0775	11/13/2015	ENERGY CENTER (CSEC)	PEAKERS OPERATING COMPANY II, LLC.	TX	183	MW	Low carbon fuel, good combustion, efficient combined cycle design	1461	LB/MW H	
TX-0778	12/16/2015	UNION VALLEY ENERGY CENTER	PEAKERS OPERATING COMPANY II, LLC.	TX	183	MW		1461	LB/MW H	

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Emission Limit 1	Units	Туре
TX-0780		VAN ALSTYNE ENERGY CENTER	PEAKERS OPERATING COMPANY I, LLC.	TX	183	mw		1461	LB/MWH	

RBLCID	Permit Date	Facility Name	Corporation	State	Throughput	Units	Control Device	Emission Limit 1	Units	Туре
TX-0794	4/7/2016	HILL COUNTY GENERATING FACILITY	BRAZOS ELECTRIC COOPERATIVE	TX	171	MW		1434	LB/MWH	BACT-PSD



Table E-1
Simple-Cycle Operation NOx BACT - SCR Capital Costs

ltem	Value	Basis
Direct Costs		
Purchased Equipment Cost		
Equipment cost + auxiliaries [A]	\$9,500,000	A
Instrumentation	\$950,000	0.10 x A
Freight	\$475,000	0.05 x A
Total Purchased Equipment Cost (PEC) [B]	\$10,925,000	B = 1.15 x A
Direct Installation Costs	4074 000	0.00
Foundations and supports	\$874,000	0.08 x B
Handling and erection	\$1,529,500	0.14 x B
Electrical	\$437,000	0.04 x B
Piping	\$218,500	0.02 x B
Insulation for ductwork	\$109,250	0.01 x B
Painting	\$109,250	0.01 x B
Total Direct Installation Cost	\$3,277,500	0.30 x B
Site Preparation (SP)	\$0	As required
Buildings (Bldg.)	\$546,250	As required (5-18% PEC)
Total Direct Cost (DC)	\$14,748,750	1.30B + SP + Bldg.
Indirect Costs (Installation)		
Engineering	\$1,092,500	0.10 x B
Construction and field expenses	\$546,250	0.05 x B
Contractor fees	\$1,092,500	0.10 x B
Start-up	\$218,500	0.02 x B
Performance test	\$109,250	0.01 x B
Contingencies	\$546,250	0.05 x B
CEMs	\$70,000	Vendor estimate
PSD Permit	\$75,000	Application + Draft Permit
Other	\$0	As required
Construction Period	0.5	Years
Interest Rate	7	Percent
Interest during construction (Int.)	\$516,206	DC * i * n
Total Indirect Cost (IC)	\$4,266,456	0.33B + Int. + CEMs + PSD
Total Capital Investment (TCI) = DC + IC	\$19,015,206	1.63B + Bldg. + Int. + CEMs + PSD

Appendix E SCR - Capital Costs Combustion Turbine

Table E-2
Simple-Cycle Operation NOx BACT - SCR Annual Costs

Simple-Cycle Operation	n NOx BACT	- SCR Annual Costs
ltem	Value	Basis
Direct Annual Costs (DC)		
bliect Allitual Gosts (DG)		
Electricity		
Press. Drop (in W.C.)	5.0	Pressure drop - catalyst bed
Power output of Turbine (kW)	167,800	ISO Rating
Power Loss Due to Pressure Drop (%)	0.50%	0.1% for every 1" pressure drop
Power Loss Due to Pressure Drop (kW)	839	
Unit cost (\$/kWh)	\$0.045	Estimated market value
Cost of Power Loss (\$/yr)	\$180,167	Based on operation of 4772 hours/yr
Operating Labor		
Catalyst labor req.	\$26,843	1/2 hr/shift @ \$30/hr
Ammonia delivery requirement (SCR)	\$720	24 hr/yr (3 deliveries per year) @ \$30/hr
Ammonia recordkeeping and reporting (SCR)	\$1,200	40 hours per year @ \$30/hr
Catalyst cleaning	\$1,200	40 hours per year @ \$30/hr
Supervisor	\$4,026	15% Operating labor
Total Cost (\$/yr)	\$33,989	1
Ammonia	255	400/
Requirement (tons/yr)	658	19% aqueous ammonia
Unit Cost (\$/ton)	\$275	Estimate
Total Cost (\$/yr)	\$181,055	
Process Air		
Requirement (scf/lb NH ₃)	350	
Requirement (mscf/yr)	1,099,629	
Unit Cost (\$/mscf)	\$0.20	\$0.20 per 1000 scf
Total Cost (\$/yr)	\$219,926	
Ostalisat Maintanana		
Catalyst Maintenance	\$8,948	1/2 hr/shift @ \$20/hr
Catalyst system maintenance labor		1/2 hr/shift @ \$30/hr 1 hr/day @ \$30/hr
Ammonia system maintenance labor Material	\$10,950 \$19,898	100% of maintenance labor
		100 % Of Ithalfiterialice labor
Total Cost (\$/yr)	\$39,795	
Catalyst Replacement		
Catalyst Cost (\$)	\$1,113,624	Catalyst modules
Catalyst Disposal Cost (\$)	\$55,681	Assume 5% of Catalyst Cost
Catalyst replacement labor	\$9,600	8 workers, 40 hr, every 3 years
Catalyst Life (yrs)	3	n
Interest Rate (%)	7%	i
CRF	0.381	Amoritization of catalyst over 3 years
Total Cost (\$/yr)	\$449,224	(Material + Labor Costs) * CRF
Indirect Annual Costs (IC)		
Overhead Overhead	\$0	OAQPS SCR Assumption
Administrative charges	\$0 \$0	OAQPS SCR Assumption
Annual Contingency	\$0 \$0	OAQPS SCR Assumption
- ,	\$0 \$0	OAQPS SCR Assumption
Property taxes Insurance	\$0 \$0	OAQPS SCR Assumption OAQPS SCR Assumption
III SULAI ICE	·	•
	¢1 704 004	
Capital Recovery	\$1,794,901 \$1,794,901	CRF * TCI (20 year life, 7% interest)
	\$1,794,901 \$1,794,901	CRF * TCI (20 year life, 7% Interest)
Capital Recovery Total Indirect Costs (\$/yr)		CRF * TCI (20 year life, 7% Interest)
Capital Recovery Total Indirect Costs (\$/yr) Total Annualized Costs (TAC) (\$)	\$1,794,901	78% Reduction (2 ppm on Natural Gas)
Capital Recovery	\$1,794,901 \$2,899,056 120.9	

Table E-3
Simple-Cycle Operation CO BACT - CO Catalyst Capital Costs

ltem	Value	Basis
Direct Costs		
Purchased Equipment Cost		
Equipment cost + auxiliaries [A]	\$4,075,000	Α
Instrumentation	\$407,500	0.10 x A
Freight	\$225,000	Vendor quote
Total Purchased Equipment Cost (PEC) [B]	\$4,707,500	B = 1.10 x A
Direct Installation Costs		
Foundations and supports	\$376,600	0.08 x B
Handling and erection	\$659,050	0.14 x B
Electrical	\$188,300	0.04 x B
Piping	\$94,150	0.02 x B
Insulation for ductwork	\$47,075	0.01 x B
Painting	\$47,075	0.01 x B
Total Direct Installation Cost	\$1,412,250	0.30 x B
Site Preparation (SP)	\$0	As required
Buildings (Bldg.)	\$517,825	As required (5-18% PEC)
Total Direct Cost (DC)	\$6,637,575	1.30B + SP + Bldg.
Indirect Costs (Installation)		
Engineering	\$470,750	0.10 x B
Construction and field expenses	\$235,375	0.05 x B
Contractor fees	\$470,750	0.10 x B
Start-up	\$94,150	0.02 x B
Performance test	\$47,075	0.01 x B
Contingencies	\$235,375	0.05 x B
CEMs	\$70,000	Vendor estimate
PSD Permit	\$75,000	Application + Draft Permit
Other	\$0	As required
Construction Period	0.5	Years
Interest Rate	7	Percent
Interest during construction (Int.)	\$232,315	DC * i * n
Total Indirect Cost (IC)	\$1,930,790	0.33B + Int.+ CEM + PSD
Total Capital Investment (TCI) = DC + IC	\$8,568,365	1.63B + Bldg. + Int.+ PSD + CEM

Table E-4
Simple-Cycle Operation CO BACT - CO Catalyst Annual Costs

Item	Value	Basis
Direct Annual Costs (DC)		
· ·		
Electricity	5 0	
Press. Drop (in W.C.)	5.0	Pressure drop - catalyst bed
Power output of Turbine (kW)	167.8	ISO Rating
Power Loss Due to Pressure Drop (%)	0.50%	0.1% for every 1" pressure drop
Power Loss Due to Pressure Drop (kW)	0.839	Estimated market value
Unit cost (\$/kWh)	\$0.045	
Cost of Power Loss (\$/yr)	\$180	Based on operation of 4772 hours/yr
Operating Labor		All costs based on \$30 per hour
Catalyst labor req.	\$8,948	1/2 hour per shift
Supervisor	\$1,342	15% Operating labor
Total Cost (\$/yr)	\$10,290	
Catalyst		
Catalyst replacement labor	\$3,210	8 workers, 40 hr, every 3 years
Material	\$3,210	100% of maintenance labor
Catalyst Cost (\$)	\$1,000,000	Catalyst modules
Catalyst Disposal Cost (\$)	\$50,000	Assume 5% of Catalyst Cost
Catalyst Life (yrs)	3	n
Interest Rate (%)	7	İ
CRF	0.38	Amoritization of catalyst over 3 years
Total Cost (\$/yr)	\$400,104	(Material + Labor Costs) * CRF
Indirect Annual Costs (IC)		
Overhead	\$0	OAQPS SCR Assumption
Administrative charges	\$0	OAQPS SCR Assumption
Annual Contingency	\$0	OAQPS SCR Assumption
Property taxes	\$0	OAQPS SCR Assumption
Insurance	\$0	OAQPS SCR Assumption
Capital Recovery	\$808,793	CRF * TCI (20 year life, 7% interest)
Total Indirect Costs (\$/yr)	\$808,793	
Total Annualized Costs (TAC) (\$)	\$1,219,367	
Total Pollutant Controlled (ton/yr)		
Carbon Monoxide (CO) (Gas)	59.5	2 ppmvd @ 15% O2 (77% Reduction)*
Carbon Monoxide (CO) (Fuel Oil)	7.7	4.4 ppmvd @ 15%O2 (77% Reduction)
COST EFFECTIVENESS (\$/ton)	\$18,154	

Table E-5
Simple-Cycle Operation PM10/PM2.5 BACT - New 7FA Capital Costs

ltem	Value	Basis
Direct Costs		
Durchased Faulianeaut Coat		
Purchased Equipment Cost	¢20,000,000	Δ
Equipment cost + auxiliaries [A] Instrumentation	\$36,000,000 \$3,600,000	A 0.10 x A
	\$3,600,000	0.10 x A 0.05 x A
Freight	\$1,800,000	
Total Purchased Equipment Cost (PEC) [B]	\$41,400,000	B = 1.15 x A
Direct Installation Costs		
Foundations and supports	\$3,312,000	0.08 x B
Handling and erection	\$5,796,000	0.14 x B
Electrical	\$1,656,000	0.04 x B
Piping	\$828,000	0.02 x B
Insulation for ductwork	\$414,000	0.01 x B
Painting	\$414,000	0.01 x B
Total Direct Installation Cost	\$12,420,000	0.30 x B
Site Preparation (SP)	\$0	As required
Buildings (Bldg.)	\$2,070,000	As required (5-18% PEC)
Total Direct Cost (DC)	\$55,890,000	1.30B + SP + Bldg.
Indirect Costs (Installation)		
Engineering	\$4,140,000	0.10 x B
Construction and field expenses	\$2,070,000	0.05 x B
Contractor fees	\$4,140,000	0.10 x B
Start-up	\$828,000	0.02 x B
Performance test	\$414,000	0.01 x B
Contingencies	\$2,070,000	0.05 x B
CEMs	\$70,000	Vendor estimate
PSD Permit	\$75,000	Application + Draft Permit
Other	\$0	As required
Construction Period	1	Years
Interest Rate	7	Percent
Interest during construction (Int.)	\$3,912,300	DC * i * n
Total Indirect Cost (IC)	\$17,719,300	0.33B + Int. + CEMs + PSD
Total Capital Investment (TCI) = DC + IC	\$73,609,300	1.63B + Bldg. + Int. + CEMs + PSD

Table E-6
Simple-Cycle Operation PM10/PM2.5 BACT - New 7FA Annual Cost

Item	Value	Basis
Direct Annual Costs (DC)		Assumed none for this analysis
Indirect Annual Costs (IC)		
Overhead	\$0	OAQPS SCR Assumption
Administrative charges	\$0	OAQPS SCR Assumption
Annual Contingency	\$0	OAQPS SCR Assumption
Property taxes	\$0	OAQPS SCR Assumption
Insurance	\$0	OAQPS SCR Assumption
Capital Recovery	\$5,931,909	CRF * TCI (30 year life, 7% interest)
Total Indirect Costs (\$/yr)	\$5,931,909	
Total Annualized Costs (TAC) (\$)	\$5,931,909	
Total Pollutant Controlled (ton/yr) (Natural Gas)	18.0	Reduction on Natural Gas Based on Vendor Data
Total Pollutant Controlled (ton/yr) (Fuel Oil)	0.3	Reduction on Fuel Oil
COST EFFECTIVENESS (\$/ton)	\$328,674	





Prevention of Significant Deterioration Class II Air Dispersion Modeling Protocol

Pleasants Energy, LLC

Pleasants Energy Uprate Project Project No. 100558

> Revision 1 October 2017

Prevention of Significant Deterioration Class II Air Dispersion Modeling Protocol

prepared for

Pleasants Energy, LLC
Pleasants Energy Uprate Project
St. Marys, West Virginia

Project No. 100558

Revision 1 October 2017

prepared by

Burns & McDonnell Engineering Company, Inc. Kansas City, Missouri

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LIST OF ABBREVIATIONS

Abbreviation

μg/m³ micrograms per cubic meter

AERMOD AMS/EPA Regulatory Model

AQAT Air Quality Assessment Tool

AQRV Air Quality Related Value

AQS Air Quality System

BPIP-PRIME Building Profile Input Program – Plume Rise Model Enhancements

CFR Code of Federal Regulations

CO carbon monoxide

CO₂e carbon dioxide equivalent (greenhouse gases)

CSAPR Cross State Air Pollution Rule

DAT Deposition Analysis Threshold

EMISFACT emission factor

EPA U.S. Environmental Protection Agency

FLM Federal Land Manager

GEP Good Engineering Practice

H₂SO₄ mist sulfuric acid mist

MW megawatt

NAAQS National Ambient Air Quality Standards

NAD 83 North American Datum of 1983

NED National Elevation Dataset

NO₂ nitrogen dioxide

Abbreviation

NOx nitrogen oxides

OEPA Ohio Environmental Protection Agency

OLM Ozone Limiting Method

Pleasants Energy Pleasants Energy, LLC

PM₁₀ particulate matter less than 10 microns in diameter

PM_{2.5} particulate matter less than 2.5 microns in diameter

PSD Prevention of Significant Deterioration

PVMRM Plume Volume Molar Ratio Method

scf standard cubic feet

scf/year standard cubic feet per year

SIA significant impact area

SO₂ sulfur dioxide

USGS U.S. Geological Survey

UTM Universal Transverse Mercator

VOC volatile organic compounds

WVDEP West Virginia Department of Environmental Protection

WWTP Wastewater Treatment Plant

 ΔE relative sensitivity

1.0 INTRODUCTION

Pleasants Energy, LLC (Pleasants Energy) installed two simple-cycle General Electric 7FA combustion turbines at the Pleasants Energy facility in 2002 and is currently operating under permit number R30-07300022-2014. The facility received a minor source air construction permit in 2015 for the installation of TurboPhase engines to increase the output of the combustion turbines. In January 2017, Pleasants Energy also received a Prevention of Significant Deterioration (PSD) air construction permit to lift the original synthetic minor source limits and increase both natural gas and fuel oil (ultra-low sulfur diesel) operation for the two combustion turbines. Since the synthetic minor source limits were lifted, the facility required a PSD permit as if a permit was never originally existed for the combustion turbines.

Pleasants Energy is now proposing to not install TurboPhase to increase output of the combustion turbines but would like to perform an uprate on the combustion turbines (Project). The Project will modify the combustion turbines from the 7FA.03 configuration to the 7FA.04 configuration and increase output during the summer peak season. Since the Project will physically modify the combustion turbines and due to the permitting history of the site, this Project will be subject to PSD. The facility also includes five Tier IV diesel generators that will operate in emergency situations for black start capabilities for the combustion turbines.

Since a PSD permit requires an assessment of ambient impacts for those pollutants subject to PSD review, this document presents a Class II air dispersion modeling protocol to be used in developing the PSD application. Submittal of this protocol will allow the West Virginia Department of Environmental Protection (WVDEP) to review and comment on the methodology to be used in the modeling analysis.

Included in this document is a brief description of the Project, proposed model, and input parameters for the proposed model. This modeling protocol has been drafted in accordance with the U.S. Environmental Protection Agency (EPA) and WVDEP modeling guidelines (EPA, 2017).

2.0 PROJECT DESCRIPTION

The existing combustion turbines will be modified from the 7FA.03 configuration to the 7FA.04 configuration to increase the output of the combustion turbines. The location of the Pleasants Energy site is shown in Figure A-1 in Appendix A.

Pleasants County is currently designated as an attainment/unclassified area for all criteria pollutants; therefore, the Project is not subject to non-attainment new source review.

The Project emission units, emission unit sizes, number of units, and fuels combusted are displayed in Table 2-1. Note that the hours of operation are approximate at this time and Pleasants Energy will likely be requesting fuel usage limits instead of hours of operation limits for the combustion turbines.

Table 2-1: Project Emission Units and Approximate Hours of Operation Estimates

Emissions Unit	Size ^a	Number of Units	Fuel	Estimated Operation ^b
			Natural gas	19,082,000,000
Combustion	191.2 MW (gas) 196.9 MW (fuel oil)	2	Ultra-low sulfur diesel	scf/year, both turbines combined
turbine			Natural gas	365 start-ups (each)
			Ultra-low sulfur diesel	30 start-ups (each)

⁽a) MW = megawatts; scf/year = standard cubic feet

The preliminary estimated maximum potential air emissions for the combustion turbines are presented in Table 2-2. The emissions include total annual emissions while operating on natural gas and fuel oil as well as start-up and shutdown emissions.

⁽b) The air permit application will request fuel usage limits and tons per year limits for both combustion turbines combined. This will include start-up and shutdown emissions as well as fuel oil and natural gas normal operation. The standard cubic feet (scf) limit includes both fuel oil and gas where fuel oil usage equals 889 scf for every gallon combusted.

Table 2-2: Preliminary Estimated Potential Emissions from the Project and PSD Significance Levels

Pollutant ^a	Preliminary Estimated Potential Emissions (tons per year) ^a	PSD Significance Levels (tons per year) ¹
NO_x	>40	40
CO	>100	100
PM_{10}^{b}	>15	15
$PM_{2.5}^{b}$	>10	10
VOC	<40	40
SO_2	<40	40
CO ₂ e	>75,000	75,000
H ₂ SO ₄ mist	<7	7
Lead	<0.6	0.6

Source:

- (1) 40 CFR 52.21(b)(23)(i)
- (a) Numbers in **bold** indicate the PSD significance level is exceeded
- (b) Filterable plus condensable

Based on the preliminary estimated potential emissions shown in the table above, it is expected that nitrogen oxides (NO_x) , carbon monoxide (CO), particulate matter less than 10 microns in diameter (PM_{10}) , particulate matter less than 2.5 microns in diameter $(PM_{2.5})$, and greenhouse gases as carbon dioxide equivalents (CO_2e) will be subject to PSD review.

3.0 PROPOSED MODEL AND MODELING METHODOLOGY

The owner is proposing to use the most current version of the AMS/EPA Regulatory Model (AERMOD) for the air quality analysis (Version 16216r). The AERMOD model is an EPA-approved, steady-state Gaussian plume model capable of modeling multiple sources in simple and complex terrain.

The following model options will be used:

- Elevated Terrain Algorithms
- Stack-tip Downwash
- Gradual Plume Rise
- Buoyancy-induced Dispersion
- Calms and Missing Data Processing Routine
- Calculate Wind Profiles
- Default Vertical Potential Temperature Gradient
- Rural Dispersion

Details of the modeling algorithms contained in AERMOD may be found in the User's Guide for AERMOD (EPA, 2016). The regulatory default option will be selected for this analysis.

3.1 Modeling Parameters

It is expected that NO_x , CO, PM_{10} , $PM_{2.5}$, and CO_2 e will be subject to PSD review, and an air quality analysis will be performed for NO_x , CO, PM_{10} and $PM_{2.5}$. Modeling of CO_2 e will not be carried out because there are no modeling thresholds for these pollutants.

3.2 Emission Source Parameters

To confirm that the Project will not exceed the National Ambient Air Quality Standards (NAAQS) and PSD Class II Increment, modeling runs will be conducted at full and partial loads (100 percent load, 80 percent load, 60 percent) and will also include a start-up scenario for the combustion turbines on natural gas. Fuel oil operation will also be modeled at the same loads including start-up as well. The emission rates modeled will represent the projected worst-case ambient conditions under various operating loads. Combustion turbine annual emissions will be based on worst-case emissions taking into account the fuel usage limit and will include start-up and shutdown emissions as well.

3.3 Intermittent Emissions

Per EPA guidance (EPA, 2011), Pleasants Energy proposes to only model continuous operation for the 1-hour standards. The combustion turbine back-up fuel oil operation will not be included in the 1-hour modeling analysis as fuel oil will only be used as a back-up fuel and for testing purposes. This includes start-up emissions from fuel oil which will be, at most, 30 start-ups per turbine per year.-These operations will not contribute significantly to the annual distribution of the daily maximum 1-hour concentrations. The list of operating scenarios considered intermittent and not modeled for the 1-hour standard are listed in Table 3-1.

Ultra-low sulfur diesel combustion in the combustion turbines

Ultra-low sulfur diesel start-up for combustion turbines

Reason Not Modeled for the 1-hour Standard

Ultra-low sulfur diesel will only be used as a back-up fuel and is limited to 7,668,886 gallons per year for both turbines combined (approximately 260 hours, each). It is not predictable as to when this will occur, and it is expected that it will happen infrequently.

Ultra-low sulfur diesel will only be used as a back-up fuel. At most, each turbine will have 30 start-ups per year. It is not predictable as to when this will occur, and it is expected that it will happen infrequently.

Table 3-1: Operating Scenarios Not Included in 1-hour Modeling Analysis

3.4 Emission Factors

Emission factor (EMISFACT) modeling options in AERMOD allow a user to model emissions only when certain criteria are met. EMISFACT will be used to model the appropriate hourly restrictions on any equipment activities that only occur over a certain number of hours per day or seasons per year. If this option is utilized, a more detailed breakdown of operation times will be presented with the final modeling analysis. Pleasants Energy understands that hourly restrictions in the modeling will likely result in corresponding permit limitations. Pleasants Energy will work with the WVDEP and discuss the use of EMISFACT in the modeling prior to submitting the air permit application and modeling analysis.

3.5 Good Engineering Practice Stack Height

Sources are subject to Good Engineering Practice (GEP) stack height requirements outlined in 40 Code of Federal Regulations (CFR) Part 51, Sections 51.100 and 51.118. As defined by the regulations, GEP height is calculated as the greater of 65 meters (measured from the ground level elevation at the base of the stack) or the height resulting from the following formula:

GEP = H + 1.5L

⁽a) Each start-up is a maximum of 2-hours and each shutdown is a maximum of 1-hour.

Where,

H = the building height; and

L = the lesser of the building height or the greatest crosswind distance of the building, also known as maximum projected width.

To meet stack height requirements, the proposed point sources will be evaluated in terms of their proximity to nearby structures. The purpose of this evaluation is to determine if the discharge from each stack will become caught in the turbulent wake of a building or other structure, resulting in downwash of the plume. Downwash of the plume can result in elevated ground-level concentrations. In EPA's 1985 *Guideline for Determination of Good Engineering Practice Stack Height*, EPA provides guidance for determining whether building downwash will occur. The downwash analysis will be performed consistent with the methods prescribed in this guidance document.

Calculations for determining the direction-specific downwash parameters will be performed using the most current version of the EPA's Building Profile Input Program – Plume Rise Model Enhancements, otherwise referred to as the BPIP-PRIME downwash algorithm (Version 04274). The BPIP-PRIME files will be submitted to WVDEP as part of the modeling analysis. Modeled stack heights will not exceed the greater of 65 meters or the calculated GEP stack height, and the lesser of actual height or GEP stack height will be used.

3.6 Receptor Grid

The overall purpose of the modeling analysis is to demonstrate that operation of the Project will not result in, or contribute to, concentrations above the NAAQS or PSD Class II Increments. The modeling runs will be conducted using the AERMOD model in simple and complex terrain mode within a 40- by 40-kilometer Cartesian grid to determine the significant impact area (SIA) for each pollutant. Based on guidance from WVDEP, the grid will incorporate the receptor spacing specified in Table 3-2. Receptors will also be placed along the fence line boundary at a spacing of 50 meters.

Table 3-2: Receptor Spacing from Fence Line Boundary

Distance from Fence Line (kilometers)	Receptor Spacing (meters)
0 – 1	50
1 – 3	100
3 – 10	250
10 – 20	500

Source: WVDEP

If the SIA exceeds 20 kilometers, the grid will be extended to encompass the entire SIA and 500-meter spacing will be used. If the modeling impacts show "hot spots" outside 1,000 meters, 100-meter grid spacing will be used to encompass the maximum concentrations to check that the maximum impact has been identified.

Terrain elevations will be incorporated into the model. Therefore, the appropriate U.S. Geological Survey (USGS) National Elevation Dataset (NED) will be used to obtain the necessary receptor elevations. North American Datum of 1983 (NAD 83) will be used to develop the Universal Transverse Mercator (UTM) coordinates for this Project.

AERMOD has a terrain preprocessor (AERMAP) which uses gridded terrain data for the modeling domain to calculate not only a XYZ coordinate, but also a representative terrain-influenced height associated with each receptor location selected. This terrain-influenced height is called the height scale and is separate for each individual receptor. AERMAP (Version 11103) will utilize the electronic NED data to populate the model with receptor elevations.

3.7 Meteorological Data

AERMOD requires a preprocessor called AERMET (Version 16216) to process meteorological data for 5 years from offsite locations to estimate the boundary layer parameters for the dispersion calculations. AERMET requires the input of surface roughness length, albedo, and Bowen ratio to define land surface characteristics for its calculations; therefore, an AERSURFACE analysis will be performed as discussed in Section 3.7.2.

Raw meteorological data obtained from National Climatic Data Center website was used to process the meteorological data, the methodology used to process the data is explained in the following sections.

3.7.1 Meteorological Station Selection

Meteorological surface stations near the Project were reviewed to determine which surface station would provide the most representative data for the air dispersion modeling. Parkersburg Wood County Airport is located fewer than 20 kilometers from the Project site, and the difference in elevation between the station and the Project site is approximately 15 meters. Additionally, Parkersburg Wood County Airport is a regional airport in a fairly rural setting which is similar to the characteristics of the Project site.

Analysis of the site and airport albedo, Bowen ratio, and surface roughness was also prepared for comparison. This is discussed in further detail in Section 3.6.1.

3.7.2 Sensitivity Analysis

Surface characteristics such as albedo, Bowen ratio, and surface roughness, influence the dispersive capacity of the atmosphere. The surface characteristics for the Parkersburg Wood County Airport location used in processing meteorological data were evaluated for representativeness to the Project site.

AERSURFACE was run for both the Parkersburg Wood County Airport and Project site locations and the surface roughness, Bowen ratio, and albedo corresponding with the appropriate monthly surface moisture classifications are shown in Table A-2 and Table A-3, Appendix A, respectively. Based on guidance from WVDEP, a sensitivity analysis was performed. AERSURFACE inputs for both the Project site and the Parkersburg Wood County Airport were used to generate meteorological data for both sets of AERSURFACE inputs. The significance model was run with both sets of meteorological data (all loads and fuel scenarios for the Project). The results of this analysis show that the AERSURFACE inputs for the Project site produce the worst-case results for all pollutants and averaging periods modeled for the Project (as described in Section 3.1). Therefore, the Project site AERSURFACE analysis was used to generate the meteorological data for the air dispersion modeling analysis.

3.7.3 AERMET

Surface air meteorological data from Parkersburg Wood County Airport, West Virginia (Station ID 03804) and upper air data from Wilmington Airborne Park, Ohio (Station ID 13841) will be used in the analysis. A profile base elevation value of 263.3 meters will be used. The most recent 5-year data set available covers the period of 2012 to 2016. One-minute meteorological data will be included in the meteorological files.

3.7.4 AERSURFACE

The land surface characteristics were generated using the most current version of AERSURFACE (Version 13016). AERSURFACE incorporates the most current recommended procedures for determining land surface characteristics (EPA, 2015). Because characterizing land use can often be a subjective process, the AERSURFACE program was developed by the EPA to standardize the methodology of determining the surface roughness length, albedo, and Bowen ratio.

The inputs used in the AERSURFACE analysis are listed in Table 3-3, below. The AERSURFACE site center was based on the location of the Project site. The analysis was run three times to account for the various moisture options (dry, average, and wet). The 1-kilometer study radius is a default setting that is recommended by the AERSURFACE user guide. The circle of study was divided into 12 equal sectors to provide the best land surface characteristics for surface roughness calculations around the Project site.

USGS National Land Cover Data for West Virginia was used as land cover input for AERSURFACE. Land surface characteristics were calculated monthly to produce the highest temporal resolution possible. Surface roughness and albedo were calculated using default settings and standard seasonal definitions.

Table 3-3: AERSURFACE Inputs

Input Parameter	AERSURFACE Input
Study radius	1 kilometer
Vary by sector	Yes
Number of sectors	12
Temporal resolution	Monthly
Continuous snow cover	No
Reassign months to different seasons?	No
Airport	Yes
Arid region	No
Surface moisture	Average, wet, dry ^a

⁽a) AERSURFACE was run 3 times to account for the various surface moisture conditions.

A historical precipitation analysis was performed to determine the moisture conditions for AERSURFACE. Thirty years of monthly precipitation data was obtained from the Northeast Regional Climate Center website for the Marietta Wastewater Treatment Plant (WWTP) in Marietta, Ohio. The Marietta WWTP (Station ID 334927) is part of the Cooperative Observer Network and is the closest station to the Pleasants Energy facility that collects historical precipitation data.

The precipitation data was analyzed to determine whether the moisture condition for the 5-year period (2012-2016) is wet, dry, or average based on historical conditions. Data from this 5-year period was averaged for each month and compared to the monthly 30th and 70th percentile values of the 30-year historical data set. If the average monthly value was less than the 30th percentile value it was designated "dry," if the average monthly value was greater than the 70th percentile value it was designated "wet," and if the average monthly value was between the 30th and 70th percentile value, it was designated "average." The precipitation analysis is included in Table A-1, Appendix A.

As shown in Table 3-3 AERSURFACE was run for each surface moisture condition. The resulting surface albedo, Bowen ratio, and surface roughness output were used to run AERMET for each surface condition. The resulting AERMET file was compiled to correspond with the monthly surface moisture condition for the 5-year period.

3.8 Land Use Parameters

Based on the Auer scheme, the existing land use for a 3-kilometer area surrounding the Project site is more than 50 percent rural (Auer, 1978). Also, the population density is fewer than 750 people per square kilometer for the same area. Because this area is considered rural, the rural dispersion coefficients option in the AERMOD model will be selected. The land use surrounding the Project is shown in Figure A-2, Appendix A.

3.9 Modeling Thresholds

The NAAQS, modeling/monitoring significance levels, and PSD Class II Increment thresholds for the modeled pollutants are shown in Table 3-4.

Table 3-4: NAAQS, Monitoring and Monitoring Significance Levels, and PSD Class II Increment

Monitoring Modeling

According Significance Constitution of Const

	Averaging Period	Monitoring Significance Level ¹	Modeling Significance Level ²	PSD Class II Increment ³	NAAQS⁴
Pollutant		micrograi	ns per cubic met	er (µg/m³)	
NO	Annual	14	1	25	100
NO_2	1-hour	NA	7.4	NA	188
CO	8-hour	575	500	NA	10,000
СО	1-hour	NA	2,000	NA	40,000
DM	Annual	NA	1	17	NA
PM_{10}	24-hour	10	5	30	150
PM _{2.5}	Annual	NA	0.2ª	4	12
	24-hour	4 ^b	1.2ª	9	35

Source:

- (1) Title 40 CFR 51.21(i)(5)(i)
- (2) Title 40 CFR 51.165(b)(2)
- (3) Title 40 CFR 52.21(c)
- (4) Title 40 CFR Part 50
- (a) EPA Draft Memorandum, August 18, 2016, "Guidance on Significant Impact Levels for Ozone and Fine Particles in the Prevention of Significant Deterioration Permitting Program."
- (b) The PM_{2.5} 24-hour significant monitoring concentration was vacated by the United States Court of Appeals for the District of Columbia Circuit on January 22, 2013.

The modeled values will be modeled using the appropriate form of the standard for each pollutant and averaging period. For significance modeling, all short-term and annual averaging periods will be modeled with the impact shown in Table 3-5. For PSD Class II Increment, the short-term averaging periods will be compared to the high second highest impacts, and the annual standards will be compared to the first highest impacts. The NAAQS thresholds will be modeled using the highs shown in Table 3-5 for each averaging period.

Table 3-5: Modeled Highs

Pollutant	Averaging Period	Significant Impact Level High ¹	NAAQS Modeled High ²
Annual		1st highest	1st highest
NO_2	1-hour	5-year average 1st high hour day	5-year average 8th high hour day
СО	8-hour	1st highest	High 2nd highest
	1-hour	1st highest	High 2nd highest
DM	Annual	1st highest	
PM_{10}	24-hour	1st highest	6th highest in 5 years
DM	Annual	5-year average year	5-year average year
PM _{2.5}	24-hour	5-year average 1st high day	5-year average 8th high day

Source:

- (1) Title 40 CFR 51.165(b)(2)
- (2) Title 40 CFR Part 50

3.10 PM_{2.5} Significant Impact Level Justification

The United States Court of Appeals for the District of Columbia Circuit on January 22, 2013, vacated and remanded portions of the EPA rule establishing significant impact levels for PM_{2.5}. An analysis was performed to determine whether the vacated PM_{2.5} significant impact levels are justified for this area.

The data that is collected by the monitors is available on the EPA website (http://www.epa.gov/airdata/). The most representative monitor for the 24-hour and annual PM_{2.5} background concentrations is the Vienna West Virginia monitor (Air Quality System [AQS] ID: 54-107-1002) located in Vienna, West Virginia. This is the closest operating PM_{2.5} monitor and is most representative of the site. This monitor is located approximately 10 miles west from the Project. The difference between the representative monitor value and the NAAQS standard (for both the 24-hour and annual standards) is sufficiently greater than the PM_{2.5} significant impact level

Therefore, the use of PM_{2.5} significant impact level is justified for this area, as demonstrated in Table 3-6.

Doromotor	PM _{2.5} 24 Hour Average	PM _{2.5} Annual Average			
Parameter	micrograms per cubic meter				
2013-2015 design value ¹	19.0	8.9			
NAAQS ²	35.0	12.0			
Difference NAAQS minus design value	16.0	3.1			
PSD Class II significant impact level ³	1.2	0.2			

Table 3-6: Vienna PM_{2.5} Monitor (AQS ID: 54-107-1002)

Source:

- (1) EPA, http://www.epa.gov/airdata/, accessed 2017
- (2) Title 40 CFR Part 50
- (3) EPA Draft Memorandum, August 18, 2016, "Guidance on Significant Impact Levels for Ozone and Fine Particles in the Prevention of Significant Deterioration Permitting Program."

3.11 Ambient Monitoring

The modeling analysis for emission sources for the Project will also address the pre-construction monitoring provision of the PSD regulations (EPA, 1987). The regulations specify monitoring *de minimis* levels for each PSD pollutant that, if exceeded, trigger the requirement to perform 1 year of pre-construction ambient air monitoring. If any predicted concentrations reach or exceed the monitoring *de minimis* levels, the owner will consult with the WVDEP to determine if pre-construction ambient air monitoring will be required. If modeled values exceed their respective monitoring *de minimis* values, the owner will request a waiver to use local ambient monitoring data to fulfill the pre-construction monitoring provisions of the PSD regulations or develop an acceptable monitoring plan at that time. For any impacts predicted to be below the monitoring *de minimis* levels, the owner will request an exemption from pre-construction ambient air monitoring, given that representative monitors in the area may be used for appropriate background concentrations.

3.12 Background Air Quality

As stated previously, if any pollutant exceeds its respective PSD significance level, a refined analysis (cumulative analysis) will be performed for that pollutant and averaging period. This analysis will be used to determine compliance with the PSD Class II Increments and the NAAQS. The NAAQS are set up to protect the air quality for all sensitive populations, and attainment is determined by the comparison to the NAAQS thresholds. As such, there are existing concentrations of each criteria pollutant that are present in ambient air that must be included in an analysis to account for items such as mobile source emissions that are not accounted for in the model. Monitored ambient emission levels will be added to the modeled ground level impacts to account for these sources.

The EPA and the WVDEP collect ambient air quality pollutant concentrations from monitors that are placed throughout the State (as do other state agencies, in their respective states). The data that is collected by the monitors is available on the EPA website (http://www.epa.gov/airdata/). Background values for 1-hour nitrogen dioxide (NO₂) and 24-hour PM_{2.5} were identified from the monitors in the area. Each pollutant has been reviewed for applicable monitors, and the background values were identified based on this analysis. The monitored background levels will be added to the modeled impacts, as previously discussed.

In accordance with EPA documentation (EPA, 1987), there are three criteria that should be considered when selecting a representative existing ambient air monitor to represent ambient air concentrations for a Project. These three criteria are:

- Monitor location
- Data quality
- Currentness of data

Further discussion on these three criteria is presented below.

3.12.1 Monitor Location and Currentness of Data

The selected monitors for the Project are located in West Virginia and Pennsylvania, as noted in Figure A-3, Appendix A. For each pollutant, the closest and most current monitor was selected. Land use was considered in the selection of representative monitors for the proposed Project. Monitored concentrations should represent the land use within the immediate vicinity of the site, as much as is practicable. The land use surrounding the Project and each of the selected monitors are shown in Figures A-2, A-4, and A-5 in Appendix A. As demonstrated in the figures, the monitors appear to be located in more urban areas, which commonly have higher (more conservative) air emissions concentrations. Therefore, the chosen sites would likely have conservative values compared to the emissions at the Project site.

3.12.2 Data Quality

Data quality was a factor in the selection of the proposed monitor. The selected monitors were reviewed for completeness, and it was determined that all data years for each pollutant are more than 80 percent complete. Therefore, the monitors meet the requirement for 80 percent completeness per EPA documentation (EPA, 1987).

3.12.3 NO₂ Background Concentration

The most representative monitor for the 1-hour NO₂ background concentration is the Charleroi, Pennsylvania monitor (AQS ID 42-125-0005) located in Washington County, Pennsylvania, shown in Figure A-3. This is the closest operating NO₂ monitor that is also representative of the Project site. This monitor is located approximately 95 miles northeast from the Project. Figure A-4 displays the land-use near the monitor. The land use is more urban than the area surrounding the Project site so monitored values are expected to be conservative when used for the Project. The regional background concentration that will be used for the 1-hour NO₂ emissions from this monitor is listed in Table 3-7.

3.12.4 PM_{2.5} Background Concentration

The most representative monitor for the $PM_{2.5}$ background concentration is the Vienna, West Virginia monitor (AQS ID: 54-107-1002) located in Wood County, West Virginia, shown in Figure A-3. This is the closest operating $PM_{2.5}$ monitor and is most representative of the Project site. This monitor is located approximately 10 miles west from the Project. This monitor is located in a similar land-use area (Figure A-5) as the land use near the proposed Project (Figure A-2). The regional background concentration that will be used for $PM_{2.5}$ emissions from this monitor is listed Table 3-7.

3.12.5 Background Concentration Values

The values listed in Table 3-7 will be used as background levels and will be added to the modeled impacts for each pollutant if NAAQS modeling is required.

Averaging Background Value Air Quality System Pollutant Period $(\mu g/m^3)^a$ Form of the Standard ID 98th percentile averaged over 1-hour 68.9 Charleroi, years 2014 to 2016 NO_2 Pennsylvania Maximum arithmetic mean for 42-125-0005 16.0 Annual years 2014 to 2016 98th percentile averaged over 24-hour 19.0 Vienna, West years 2014 to 2016 Virginia $PM_{2.5}$ Arithmetic mean averaged over 54-107-1002 8.9 Annual years 2014 to 2016

Table 3-7: Background Concentrations for Air Modeling

Source: EPA, http://www.epa.gov/airdata/ (a) µg/m³ = micrograms per cubic meter

3.13 NAAQS and PSD Class II Increment Analysis

Per discussions with WVDEP, all major stationary sources that emit pollutants subject to this analysis within 20 kilometers of the Project site will be addressed for the cumulative modeling analysis for pollutants that exceed their respective significant impact level. WVDEP also recommended including sources located 20 to 25 kilometers from the site on a case-by-case basis. The inventories of sources will be developed in accordance with applicable EPA guidance, input from the WVDEP, and the Ohio Environmental Protection Agency (OEPA). The list of all facilities considered for the January 2017 PSD permit cumulative modeling is shown Table A-3 in Appendix A, as provided by the WVDEP and OEPA. The facilities that were excluded from the inventory are indicated Table A-3, as well as the methodology for removing them. All inventory sources that were modeled for NO₂ and PM_{2.5} for the January 2017 PSD permit are shown in Tables A-4 and A-5, respectively. These sources will also be used for the current Project application. Maps that display the locations of the inventory sources that will be included in the refined modeling are shown in Figures A-7 and A-8 in Appendix A, for NO₂ and PM_{2.5}, respectively. Once the emissions and stack parameters have been determined for the inventory sources from permits, emission inventories and other information, the final modeling inventory will be determined in conjunction with the WVDEP prior to final models being submitted.

Background air quality concentrations (as described in Section 3.12) will be added to model-predicted concentrations for comparison to the NAAQS. If the refined analysis does not result in any concentrations above the NAAQS or PSD Class II Increments, no further modeling will be conducted.

3.14 NO₂ Modeling – Multi-Tiered Screening Approach

The AERMOD model gives the emission results for all pollutants, including NO_x. However, impacts of NO₂ must be examined for comparison to the NAAQS, PSD Class II Increments, and significance values. The EPA has a three-tier approach to modeling NO₂ concentrations:

- Tier I total conversion, or all $NO_x = NO_2$
- Tier II use a default NO₂/NO_x ratio
- Tier III case-by-case detailed screening methods, such as the Ozone Limiting Method (OLM) or Plume Volume Molar Ratio Method (PVMRM)

Initial screening modeling was performed using both Tier I and Tier II methodologies. It was determined from these modeling iterations that less conservative methods for determining 1-hour NO₂ compliance would be needed for the Project. To account for the conversion of NO_x to NO₂ in the modeling, the Tier III approach using the OLM method will be used for the 1-hour NO₂ PSD significance and refined

(cumulative) air dispersion modeling. The PSD significance threshold will be compared to the modeled first high, while the NAAQS threshold will be compared to the 5-year average modeled 98th percentile of the annual distribution of maximum daily 1-hour values.

The amount of NO₂ present in the stack gases was determined from published data for each piece of equipment being modeled. The in-stack NO₂/NO_x ratios shown in Table 3-8 will be used for the Project emission sources.

 Emission Source
 NO₂/NO₂ Ratio
 Reference

 Natural gas-fired/fuel oil-fired combustion turbine
 0.5
 Default in-stack NO₂/NO₂ ratio²

Table 3-8: NO₂/NO_x Ratios

Upon review of the EPA In-Stack Ratio database, there were no exact matches for the sources at the Pleasants Energy facility. Therefore, to be conservative, a default in-stack NO_2/NO_x ratio of 0.5 was used for all onsite emission units based on EPA's March 2011 memo. Based on guidance from WVDEP, an instack NO_2/NO_x ratio of 0.2 will be used for inventory sources farther than 1-3 kilometers away from the project site. Otherwise, the default in-stack NO_2/NO_x of 0.5 will be used unless source-specific data is available.

Additionally, an equilibrium NO₂/NO_x ratio of 0.90 will be used per EPA's March 2011 memo.

3.14.1 Annual NO₂ Averaging Period

At this time, it is expected that the Tier I approach will be used for the analysis. Based on preliminary modeling, it is not expected that Tier II or Tier III methodologies will be necessary for this air quality analysis. However, if a Tier II or Tier III analysis is used, the WVDEP will be consulted for concurrence on the methodologies.

3.14.2 Specifying Combined Plumes

When using the OLM option, the model includes an option for specifying which sources are to be modeled as combined plumes (NO_x within the plumes competes for the available ambient ozone). A group ID of ALL will be selected for this modeling analysis, which means that the OLM will be applied on a combined plume basis to all sources within a specified source group. The use of this option is in accordance with the methodology presented in EPA's June 2010 memo which states, "Applications of the

⁽a) Default in-stack NO₂/NO_x ratio per EPA's March 2011 memo.

OLM option in AERMOD, subject to approval under Section 3.2.2e of Appendix W, should routinely utilize the 'OLMGROUP ALL' option for combining plumes (EPA, 2011)."

3.14.3 Background Ozone

The selected monitor to be used for the 1-hour hourly ozone background is the West Virginia Air Pollution Control Commission monitoring station located in Vienna, Wood County, West Virginia (AQS ID: 54-107-1002). The applicant was advised by WVDEP to use this monitor for ozone season data as it is representative of the Project site. Additionally, the Vienna monitor is in a similar land-use area (Figure A-5 in Appendix A) as the land-use near the proposed Project (Figure A-2); therefore, the monitor will provide data that is representative of the ozone concentrations in the Project area.

Because the Vienna monitor only has ozone season data available, two other monitors were reviewed for representative non-ozone season data: the Lawrenceville monitoring station located in Pittsburg, Pennsylvania (AQS ID: 43-003-0008), and the Quaker City monitoring station located in Quaker City, Ohio (AQS ID: 39-121-9991). The Quaker City monitoring station is located closer to the Project site (approximately 70 kilometers from the Project site) than the Lawrenceville Station (approximately 170 kilometers from the Project site). The Quaker City station was deemed the most representative for the non-ozone season data due to its close proximity to the Project site. Data from the Quaker City station was used for the non-ozone season hourly data for years 2012-2016.

Hourly background ozone concentrations were obtained from the EPA Technology Transfer Network AQS for the Vienna monitoring station located in Wood County, West Virginia (AQS ID: 54-107-1002) and the Quaker City monitoring station located in Ohio (AQS ID: 39-121-9991). Data from each monitoring station was used for the time periods previously discussed. The background data was formatted for use in the AERMOD model and processed for years 2012 to 2016 to match the meteorological data years used in the modeling. The following steps and assumptions were used to create the hourly ozone data:

- One to six missing values: The average of the previous and following value was used.
- More than six missing values: Data was substituted based the maximum of the ozone concentrations measured during that hour in the month of the missing values.

4.0 CLASS I AREA IMPACTS

Recent Federal Land Manager (FLM) guidance requires that a proposed major source, in the course of a PSD application, perform an assessment of air quality impacts at Class I areas if these areas are located within approximately 300 kilometers of the Project. There are four Class I Areas that are within 300 kilometers of the Project:

- Otter Creek Wilderness (130 kilometers)
- Dolly Sods Wilderness (160 kilometers)
- Shenandoah National Park (200 kilometers)
- James River Face Wilderness (253 kilometers)

The locations of the Project site and the Class I Areas are shown in Figure A-6, Appendix A.

4.1 Visibility and Deposition

A visibility and deposition analysis was performed as part of the January 2017 PSD air construction permit to lift the original synthetic minor source limits (2017 PSD Project). Given that prior visibility and deposition analysis for the 2017 PSD Project was performed and the new Project's emissions are similar (and should not increase on a maximum 24-hour or lb/hr rate for visibility pollutants) to that project's emissions, Pleasants is proposing that no visibility or deposition analysis be required. The information below summarizes the work that was performed as part of the 2017 PSD Project.

The visibility analysis demonstrated that the visibility impact was less than 5.0 percent for year for each Class I area for both natural gas and fuel oil operation. The TurboPhase Project was not expected to have any noticeable effect on visibility since the predicted visibility impacts were well below the level of acceptable change and no further analysis required.

The Nitrogen and Sulfur deposition modeling results for each Class I area were also well below the applicable Deposition Analysis Threshold (DAT) for the 2017 PSD Project. As a result, the 2017 PSD Project was not expected to have adverse impacts resulting from deposition and no further analysis was conducted.

Concurrence was received from the FLMs for the 2017 PSD Project that there would be no significant impacts to any air quality values (AQRVs) at Class I areas for the project.

4.2 PSD Class I Increment

An analysis will be performed to demonstrate that the operation of the Project will not result in, or contribute to, concentrations above the PSD Class I Increment threshold.

Since all of the Class I areas are located greater than 50 kilometers from the Project, a screening analysis to determine if further analysis is required will be performed for each of the four Class I areas. Modeled impacts at receptors placed 50 kilometers in the direction of each Class I area will be compared to the Class I significant impact level using AERMOD. Both the minimum and maximum receptor elevations at each of the respective Class I areas will be modeled.

5.0 ANALYSIS OF SECONDARY PM_{2.5} FORMATION

In addition to direct emissions of PM_{2.5}, other pollutants, chiefly NO_x and sulfur dioxide (SO₂), can lead to formation of PM_{2.5} further downwind. The photochemical reactions that transform these pollutants into nitrates and sulfates, which become the major species of PM_{2.5}, take place over hours or days. The Project is estimated to be significant for NO_x precursors (greater than 40 tons per year) for the formation of secondary PM_{2.5}, so this analysis is focusing only on the NO_x emission and secondary PM_{2.5} from the NO_x emissions from this project.

As is the case with almost all $PM_{2.5}$ modeling, the highest impacts are closest to the fence line and the sources, while the high impacts from the NO_x emissions are usually much farther out from the source and fence line. Further, the NO_x emissions that form particulate, namely particulate nitrates would be formed farther out from the site as well. This secondary $PM_{2.5}$ analysis will focus on the likelihood of the formation of particulate nitrates and how regional emissions of NO_x have historically been predicted to be insignificant on monitored and modeled values of $PM_{2.5}$ in the region.

A review of regional monitors that show speciation of PM_{2.5} show that nitrate is a very small percentage of the overall PM_{2.5} in the area. Three monitors were examined. On an annual average for years 2012-2014, the PM_{2.5} speciation showed that sulfates made up approximately 20.5 to 29.5 percent of the PM_{2.5} organic carbon made up 19.7 to 29.1 percent of the PM_{2.5} and 4.3 to 20.6 percent is nitrates. Nitrates made up a small portion of the overall PM_{2.5} in these three closest speciated PM_{2.5} monitors. This shows that nitrates does not play a significant role in the PM_{2.5} formation in the area.

Further, a more refined analysis of $PM_{2.5}$ and nitrates was performed on a seasonal basis. Table 5-1 displays the contribution of nitrate seasonally on the $PM_{2.5}$ monitored values and Table 5-2 displays the overall annual distribution of $PM_{2.5}$ over the seasons. The tables show that $PM_{2.5}$ is higher in the warmer months and lower in the winter months, however more nitrate contributes to the overall $PM_{2.5}$ values in the colder months (due to the volatility of ammonium nitrates). Overall these tables show that nitrate has a small contribution to the overall $PM_{2.5}$ values in the region, especially when reviewed on a seasonal basis.

Table 5-1: Average Percent Nitrate Contributions to Total PM_{2.5}

2012							
Monitor	Winter	Spring	Summer	Fall	Annual		
Guthrie	7.0%	2.5%	1.9%	7.4%	4.3%		
South Charleston	9.8%	5.0%	3.3%	8.1%	6.5%		
Moundsville	9.1%	3.7%	2.4%	8.8%	6.1%		
2013							
Monitor	Winter	Spring	Summer	Fall	Annual		
Guthrie	12.3%	2.1%	1.6%	6.4%	5.1%		
South Charleston	10.7%	5.0%	2.4%	13.5%	7.0%		
Moundsville	15.7%	4.0%	2.3%	12.2%	8.5%		
2014							
Monitor	Winter	Spring	Summer	Fall	Annual		
Guthrie	14.9%	3.4%	1.8%	10.2%	6.8%		
Moundsville	28.3%	5.2%	2.3%	14.7%	10.3%		

Source: EPA, http://www.epa.gov/airdata/.

Table 5-2: Seasonal Total PM_{2.5} Contribution

2012								
Monitor	Winter	Spring	Summer	Fall	Annual			
Guthrie	24.2%	26.8%	31.4%	17.5%	100.0%			
South Charleston	23.9%	26.1%	29.4%	20.6%	100.0%			
Moundsville	25.2%	23.8%	26.1%	24.9%	100.0%			
2013								
Monitor	Winter	Spring	Summer	Fall	Annual			
Guthrie	19.8%	22.3%	35.5%	22.4%	100.0%			
South Charleston	24.3%	25.0%	28.5%	22.1%	100.0%			
Moundsville	24.2%	26.6%	26.8%	22.4%	100.0%			
2014								
Monitor	Winter	Spring	Summer	Fall	Annual			
Guthrie	23.6%	25.0%	33.2%	18.2%	100.0%			
South Charleston	23.9%	25.7%	28.9%	21.5%	100.0%			
Moundsville	28.6%	23.9%	30.0%	17.5%	100.0%			

Source: EPA, http://www.epa.gov/airdata/.

Another way to review the potential impact of NO_x on $PM_{2.5}$ concentrations is to perform an analysis using regional modeling. Because of the well-established relationship between NO_x , regional transport, and the formation of $PM_{2.5}$, to assist states to meet the $PM_{2.5}$ NAAQS, EPA finalized the Cross State Air

Pollution Rule (CSAPR). Although CSAPR was vacated in August 2012 and has since been reinstated, the rule included extensive modeling to support the emissions reductions necessary in each state to achieve the $PM_{2.5}$ NAAQS in the eastern United States that is relevant to this analysis.

EPA used a regional model, CAMx, and the Air Quality Assessment Tool (AQAT) to determine levels of reduction from electric generating units necessary to achieve the NAAQS at every site. The documentation includes extensive tables showing impacts at all PM_{2.5} monitoring sites in the eastern United States and emission reduction levels necessary to achieve those results.

To examine the possible secondary PM_{2.5} impacts of the Project, the modeling EPA used to establish the final 2014 budgets in CSAPR is used for this analysis. The CSAPR website is located at http://www.epa.gov/airtransport/. Using these models, one can take the difference in ground-level modeled PM_{2.5} annual values to see the reduction in PM_{2.5} as a result of the SO₂ and NO_x reductions. This modeling will be used to determine PM_{2.5} secondary concentrations due to the NOx emissions from this Project.

6.0 ADDITIONAL IMPACT ANALYSIS

The additional impacts analysis requirement under PSD will include the ambient air quality impact analysis, soils and vegetation impacts, visibility impairment, and growth analysis on Class II areas. This analysis will follow EPA's guidance provided in the *New Source Review Workshop Manual* (October 1990 draft).

The growth analysis will quantify the number of employees, the availability of housing in the area, associated commercial and industrial growth, and construction related activities and mobile sources. The number of employees is not envisioned to be large enough to result in a quantifiable increase in emissions from residential, commercial, or industrial growth.

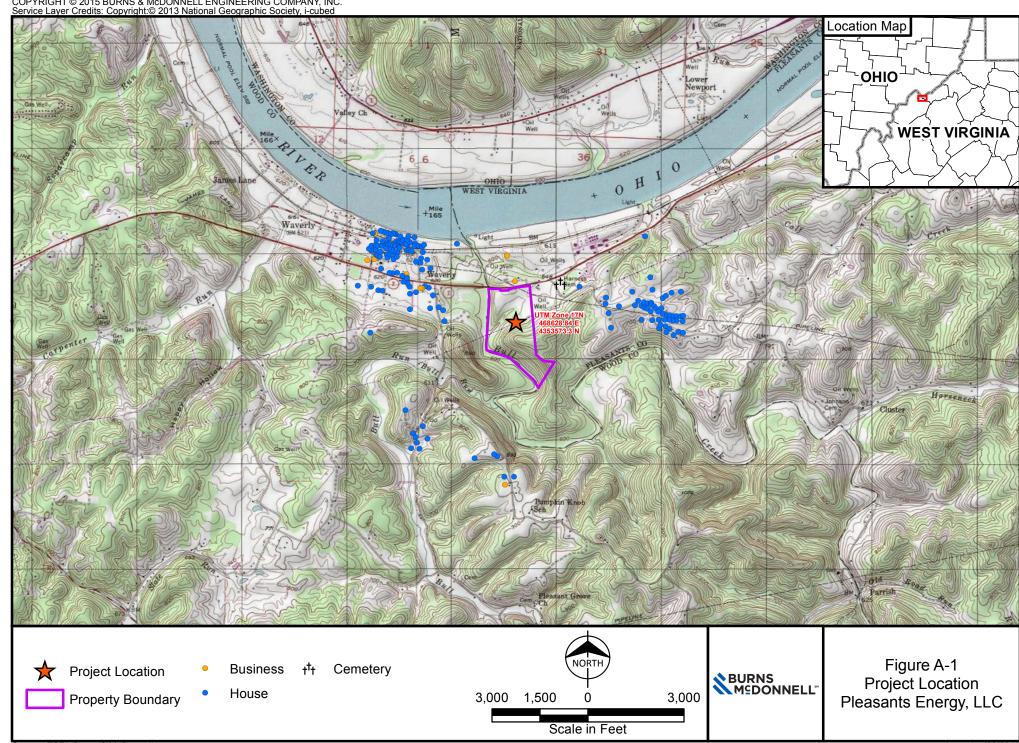
The visual plume blight analysis will be performed in accordance with the guidelines set forth in EPA-454/R-92-023, *Workbook for Plume Visual Impact Screening and Analysis (Revised)* (1992). Pleasants Energy proposes to perform a visual plume blight analysis on two nearby areas of visual interest, North Bend State Park and Blennerhassett Island State Historical Park located approximately 25 kilometers east-southeast and 24 kilometers west-southwest, respectively of the Project site. In the EPA document, the model VISCREEN is recommended for plume visibility analysis. Several refinement levels of VISCREEN are described. The Level-1 screening uses worst-case meteorological conditions (F-class stability, 1 meter per second wind speed). This level of screening results in the most conservative (worst-case) visibility results. The impacts of the plume are compared to screening criteria to determine if they are perceptible. The screening criteria are a change in relative sensitivity (Δ E) value of 2.0 and a green absolute contrast value of 0.05. If the plume is determined to be imperceptible, the visibility modeling is complete; otherwise, a Level-2 screening that uses actual meteorological data and refined particle characteristics will be performed. The Level-2 screening will result in a more realistic visibility analysis. If this plume visibility still does not meet sky and terrain contrast levels, a Level-3 analysis may be required that adds more statistical analysis.

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Source: ESRI, Burns & McDonnell Issued: 4/28/2015

Table A-1: Precipitation (inches) Amount for 30 Years at Marietta Wastewater Treatment Plant, Marietta, OH*

Year	January	February	March	April	May	June	July	August	September	October	November	December
1987	1.59	1.4	2.23	3.52	2.3	6.57	1.55	3.27	2.21	1.49	1.98	3.61
1988	1.99	2.87	3.63	2.67	1.54	0.92	5.21	2.81	4.73	2.19	4.46	2.6
1989	3.57	5.65	6.28	5.61	4.58	5.5	2.37	10.68	6.63	4.15	1.84	2.29
1990	3.17	3.69	2.37	2.1	8.28	5.23	5.09	6.75	3.7	4.26	2.28	7.94
1991	3.37	M	4.96	4.37	1.64	4	4.07	6.52	5.01	1.1	3.35	5.74
1992	1.9	1.47	4.89	2.05	2.37	2.07	6.81	3.56	M	0.7	3.68	2.6
1993	2.68	2.31	5.37	2.47	1.73	4.15	2.76	3.79	3.32	3.64	3.39	2.08
1994	6.57	4.47	5.13	5.64	3.26	3.61	6.7	4.47	1.77	0.92	2.47	2.86
1995	4.61	2.29	М	2.1	M	5.18	M	3.97	M	М	2.88	2.76
1996	4.83	3.57	4.53	2.99	8.4	5.31	6.6	2.43	6.29	M	3.02	3.78
1997	2.27	1.58	8.93	1.8	3.57	6.57	6.61	5.12	2.26	1.35	2.2	2.56
1998	4.37	3.92	3.23	4.62	3.7	11.76	2.23	0.88	3.85	2.26	1.76	2.11
1999	6.25	3.23	3.36	2.84	2.28	1.69	2.54	3.14	1.26	3.44	3.18	3.52
2000	2.44	6.58	3.37	4.35	5.37	2.9	6.76	3.6	5.21	1.21	1.27	2.97
2001	2.09	0.95	3	3.85	6.09	4.39	4.38	3.76	1.92	2.01	3.47	2.51
2002	3.02	1.17	6.43	5.32	4.77	4.73	3.49	0.52	3.09	4.95	3.45	2.37
2003	2.06	3.99	0.52	3.25	6.4	8.93	8.81	4.99	7.08	3.24	5.81	2.95
2004	4.27	2.03	3.7	4.77	4.88	2.62	3.48	3.78	8.51	3.08	3.27	2.29
2005	5.79	1.88	4.16	5.28	2.94	1.4	4.01	3.72	1.29	3.88	2.69	2.18
2006	3.76	0.6	2.1	3.99	3.57	3.66	5.6	3.06	5.44	6.63	2.38	1.84
2007	3.69	2.51	3.14	3.38	0.92	2.19	4.73	3.44	0.91	2.67	3.29	5.11
2008	2.29	4.2	5.92	2.55	4.2	6.18	4.11	2.6	1.17	2.25	2.24	5.73
2009	4.39	1.66	1.67	4.22	4.15	6.93	3.67	2.12	2.07	3.74	1.2	3.88
2010	2.37	2.34	2.8	1.03	7.03	6.09	7.19	1.52	1.43	1.84	2.97	3.41
2011	2	4.09	6.09	7.04	3.43	5.98	3.63	5.06	7.03	6.2	4.98	2.97
2012	4.63	1.69	4.48	1.79	6.07	2.74	2.99	3.33	6.37	4.34	0.47	6.8
2013	2.49	1.58	2.74	1.52	2.05	6.16	9.39	6.69	1.75	2	3.88	5.09
2014	2.19	3.89	2.5	3.02	4.83	5.31	4.15	3.4	0.94	4.43	1.92	3.72
2015	2.28	1.81	5.64	3.67	2.27	6.21	2.25	2.3	4.11	2.32	2.33	4.49
2016	2.18	3.4	2.87	3.84	4.42	3.27	3.49	2.87	1.23	3.12	0.83	4.83
2012-2016 Avg.	2.75	2.47	3.65	2.77	3.93	4.74	4.45	3.72	2.88	3.24	1.89	4.99
30th percentile	2.28	1.74	2.92	2.63	2.60	3.51	3.49	3.00	1.79	2.03	2.23	2.59
70th percentile	3.91	3.64	4.93	4.26	4.81	6.01	5.44	3.84	4.98	3.73	3.31	3.81
Average / Dry / Wet ?	Average	Average	Average	Average	Average	Average	Average	Average	Average	Average	Dry	Wet

Data obtained from http://www.nrcc.cornell.edu/ Accessed 9/3/2015

Wet Months 1
Dry Months 1
Average Months 10

^{*}M stands for missing data

Table A-2: Airport AERSURFACE Inputs Corresponding with Monthly Surface Moisture Classifications

Time Frequency	Wind Sector	Surface Albedo	Bowen Ratio	Surface Roughness	Surface Moisture
January	1 of 12	0.17	0.83	0.105	Average
January	2 of 12	0.17	0.83	0.265	Average
January	3 of 12	0.17	0.83	0.369	Average
January	4 of 12	0.17	0.83	0.272	Average
January	5 of 12	0.17	0.83	0.166	Average
January	6 of 12	0.17	0.83	0.172	Average
January	7 of 12	0.17	0.83	0.151	Average
January	8 of 12	0.17	0.83	0.24	Average
January	9 of 12	0.17	0.83	0.183	Average
January	10 of 12	0.17	0.83	0.444	Average
January	11 of 12	0.17	0.83	0.309	Average
January	12 of 12	0.17	0.83	0.175	Average
February	1 of 12	0.17	0.83	0.105	Average
February	2 of 12	0.17	0.83	0.265	Average
February	3 of 12	0.17	0.83	0.369	Average
February	4 of 12	0.17	0.83	0.272	Average
February	5 of 12	0.17	0.83	0.166	Average
February	6 of 12	0.17	0.83	0.172	Average
February	7 of 12	0.17	0.83	0.151	Average
February	8 of 12	0.17	0.83	0.24	Average
February	9 of 12	0.17	0.83	0.183	Average
February	10 of 12	0.17	0.83	0.444	Average
February	11 of 12	0.17	0.83	0.309	Average
February	12 of 12	0.17	0.83	0.175	Average
March	1 of 12	0.15	0.54	0.134	Average
March	2 of 12	0.15	0.54	0.368	Average
March	3 of 12	0.15	0.54	0.494	Average
March	4 of 12	0.15	0.54	0.343	Average
March	5 of 12	0.15	0.54	0.2	Average
March	6 of 12	0.15	0.54	0.249	Average
March	7 of 12	0.15	0.54	0.199	Average
March	8 of 12	0.15	0.54	0.288	Average
March	9 of 12	0.15	0.54	0.232	Average
March	10 of 12	0.15	0.54	0.651	Average
March	11 of 12	0.15	0.54	0.457	Average
March	12 of 12	0.15	0.54	0.232	Average
April	1 of 12	0.15	0.54	0.134	Average
April	2 of 12	0.15	0.54	0.368	Average
April	3 of 12	0.15	0.54	0.494	Average
April	4 of 12	0.15	0.54	0.343	Average
April	5 of 12	0.15	0.54	0.2	Average
April	6 of 12	0.15	0.54	0.249	Average
April	7 of 12	0.15	0.54	0.199	Average
April	8 of 12	0.15	0.54	0.199	Average
April	9 of 12	0.15	0.54	0.232	Average
April	10 of 12	0.15	0.54	0.651	Average
April	11 of 12	0.15	0.54	0.457	Average
	12 of 12	0.15	0.54	0.437	
April May	1 of 12	0.15	0.54	0.232	Average
May	2 of 12	0.15	0.54	0.368	Average
May					Average
May	3 of 12	0.15	0.54	0.494	Average

Table A-2: Airport AERSURFACE Inputs Corresponding with Monthly Surface Moisture Classifications

Time Frequency		Surface Albedo	Bowen Ratio	Surface Roughness	Surface Moisture
May	4 of 12	0.15	0.54	0.343	Average
May	5 of 12	0.15	0.54	0.2	Average
May	6 of 12	0.15	0.54	0.249	Average
May	7 of 12	0.15	0.54	0.199	Average
May	8 of 12	0.15	0.54	0.288	Average
May	9 of 12	0.15	0.54	0.232	Average
May	10 of 12	0.15	0.54	0.651	Average
May	11 of 12	0.15	0.54	0.457	Average
May	12 of 12	0.15	0.54	0.232	Average
June	1 of 12	0.16	0.35	0.272	Average
June	2 of 12	0.16	0.35	0.563	Average
June	3 of 12	0.16	0.35	0.698	Average
June	4 of 12	0.16	0.35	0.484	Average
June	5 of 12	0.16	0.35	0.253	Average
June	6 of 12	0.16	0.35	0.383	Average
June	7 of 12	0.16	0.35	0.367	Average
June	8 of 12	0.16	0.35	0.423	Average
June	9 of 12	0.16	0.35	0.391	Average
June	10 of 12	0.16	0.35	0.913	Average
June	11 of 12	0.16	0.35	0.629	Average
June	12 of 12	0.16	0.35	0.38	Average
July	1 of 12	0.16	0.35	0.272	Average
July	2 of 12	0.16	0.35	0.563	Average
July	3 of 12	0.16	0.35	0.698	Average
July	4 of 12	0.16	0.35	0.484	Average
July	5 of 12	0.16	0.35	0.253	Average
July	6 of 12	0.16	0.35	0.383	Average
July	7 of 12	0.16	0.35	0.367	Average
July	8 of 12	0.16	0.35	0.423	Average
July	9 of 12	0.16	0.35	0.391	Average
July	10 of 12	0.16	0.35	0.913	Average
July	11 of 12	0.16	0.35	0.629	Average
July	12 of 12	0.16	0.35	0.38	Average
August	1 of 12	0.16	0.35	0.272	Average
August	2 of 12	0.16	0.35	0.563	Average
August	3 of 12	0.16	0.35	0.698	Average
August	4 of 12	0.16	0.35	0.484	Average
August	5 of 12	0.16	0.35	0.253	Average
August	6 of 12	0.16	0.35	0.383	Average
August	7 of 12	0.16	0.35	0.367	Average
August	8 of 12	0.16	0.35	0.423	Average
August	9 of 12	0.16	0.35	0.391	Average
August	10 of 12	0.16	0.35	0.913	Average
August	11 of 12	0.16	0.35	0.629	Average
August	12 of 12	0.16	0.35	0.38	Average
September	1 of 12	0.16	0.83	0.265	Average
September	2 of 12	0.16	0.83	0.559	Average
September	3 of 12	0.16	0.83	0.693	Average
September	4 of 12	0.16	0.83	0.472	Average
September	5 of 12	0.16	0.83	0.234	Average
September	6 of 12	0.16	0.83	0.363	Average

Table A-2: Airport AERSURFACE Inputs Corresponding with Monthly Surface Moisture Classifications

Time Frequency	Wind Sector	Surface Albedo	Bowen Ratio	Surface Roughness	Surface Moisture
September	7 of 12	0.16	0.83	0.358	Average
September	8 of 12	0.16	0.83	0.414	Average
September	9 of 12	0.16	0.83	0.381	Average
September	10 of 12	0.16	0.83	0.909	Average
September	11 of 12	0.16	0.83	0.608	Average
September	12 of 12	0.16	0.83	0.367	Average
October	1 of 12	0.16	0.83	0.265	Average
October	2 of 12	0.16	0.83	0.559	Average
October	3 of 12	0.16	0.83	0.693	Average
October	4 of 12	0.16	0.83	0.472	Average
October	5 of 12	0.16	0.83	0.234	Average
October	6 of 12	0.16	0.83	0.363	Average
October	7 of 12	0.16	0.83	0.358	Average
October	8 of 12	0.16	0.83	0.414	Average
October	9 of 12	0.16	0.83	0.381	Average
October	10 of 12	0.16	0.83	0.909	Average
October	11 of 12	0.16	0.83	0.608	Average
October	12 of 12	0.16	0.83	0.367	Average
November	1 of 12	0.16	1.77	0.265	Dry
November	2 of 12	0.16	1.77	0.559	Dry
November	3 of 12	0.16	1.77	0.693	Dry
November	4 of 12	0.16	1.77	0.472	Dry
November	5 of 12	0.16	1.77	0.234	Dry
November	6 of 12	0.16	1.77	0.363	Dry
November	7 of 12	0.16	1.77	0.358	Dry
November	8 of 12	0.16	1.77	0.414	Dry
November	9 of 12	0.16	1.77	0.381	Dry
November	10 of 12	0.16	1.77	0.909	Dry
November	11 of 12	0.16	1.77	0.608	Dry
November	12 of 12	0.16	1.77	0.367	Dry
December	1 of 12	0.17	0.38	0.105	Wet
December	2 of 12	0.17	0.38	0.265	Wet
December	3 of 12	0.17	0.38	0.369	Wet
December	4 of 12	0.17	0.38	0.272	Wet
December	5 of 12	0.17	0.38	0.166	Wet
December	6 of 12	0.17	0.38	0.172	Wet
December	7 of 12	0.17	0.38	0.151	Wet
December	8 of 12	0.17	0.38	0.24	Wet
December	9 of 12	0.17	0.38	0.183	Wet
December	10 of 12	0.17	0.38	0.444	Wet
December	11 of 12	0.17	0.38	0.309	Wet
December	12 of 12	0.17	0.38	0.175	Wet

Table A-3: Site AERSURFACE Inputs Corresponding with Monthly Surface Moisture Classifications

Time Frequency	Wind Sector	Surface Albedo		Surface Roughness	Surface Moisture
January	1 of 12	0.16	0.78	0.034	Average
January	2 of 12	0.16	0.78	0.098	Average
January	3 of 12	0.16	0.78	0.117	Average
January	4 of 12	0.16	0.78	0.16	Average
January	5 of 12	0.16	0.78	0.484	Average
January	6 of 12	0.16	0.78	0.339	Average
January	7 of 12	0.16	0.78	0.325	Average
January	8 of 12	0.16	0.78	0.224	Average
January	9 of 12	0.16	0.78	0.156	Average
January	10 of 12	0.16	0.78	0.104	Average
January	11 of 12	0.16	0.78	0.044	Average
January	12 of 12	0.16	0.78	0.02	Average
February	1 of 12	0.16	0.78	0.034	Average
February	2 of 12	0.16	0.78	0.098	Average
February	3 of 12	0.16	0.78	0.117	Average
February	4 of 12	0.16	0.78	0.16	Average
February	5 of 12	0.16	0.78	0.484	Average
February	6 of 12	0.16	0.78	0.339	Average
February	7 of 12	0.16	0.78	0.325	Average
February	8 of 12	0.16	0.78	0.224	Average
February	9 of 12	0.16	0.78	0.156	Average
February	10 of 12	0.16	0.78	0.104	Average
February	11 of 12	0.16	0.78	0.044	Average
February	12 of 12	0.16	0.78	0.02	Average
March	1 of 12	0.15	0.52	0.046	Average
March	2 of 12	0.15	0.52	0.14	Average
March	3 of 12	0.15	0.52	0.175	Average
March	4 of 12	0.15	0.52	0.247	Average
March	5 of 12	0.15	0.52	0.739	Average
March	6 of 12	0.15	0.52	0.509	Average
March	7 of 12	0.15	0.52	0.495	Average
March	8 of 12	0.15	0.52	0.341	Average
March	9 of 12	0.15	0.52	0.216	Average
March	10 of 12	0.15	0.52	0.147	Average
March	10 of 12	0.15	0.52	0.061	<u> </u>
March	12 of 12	0.15	0.52	0.007	Average
	1 of 12	0.15	0.52	0.027	Average
April			0.52	0.046	Average
April	2 of 12	0.15	0.52		Average
April	3 of 12	0.15 0.15	0.52	0.175 0.247	Average
April	4 of 12				Average
April	5 of 12	0.15	0.52	0.739	Average
April	6 of 12	0.15	0.52	0.509	Average
April	7 of 12	0.15	0.52	0.495	Average
April	8 of 12	0.15	0.52	0.341	Average
April	9 of 12	0.15	0.52	0.216	Average
April	10 of 12	0.15	0.52	0.147	Average
April	11 of 12	0.15	0.52	0.061	Average
April	12 of 12	0.15	0.52	0.027	Average
May	1 of 12	0.15	0.52	0.046	Average
May	2 of 12	0.15	0.52	0.14	Average
May	3 of 12	0.15	0.52	0.175	Average

Table A-3: Site AERSURFACE Inputs Corresponding with Monthly Surface Moisture Classifications

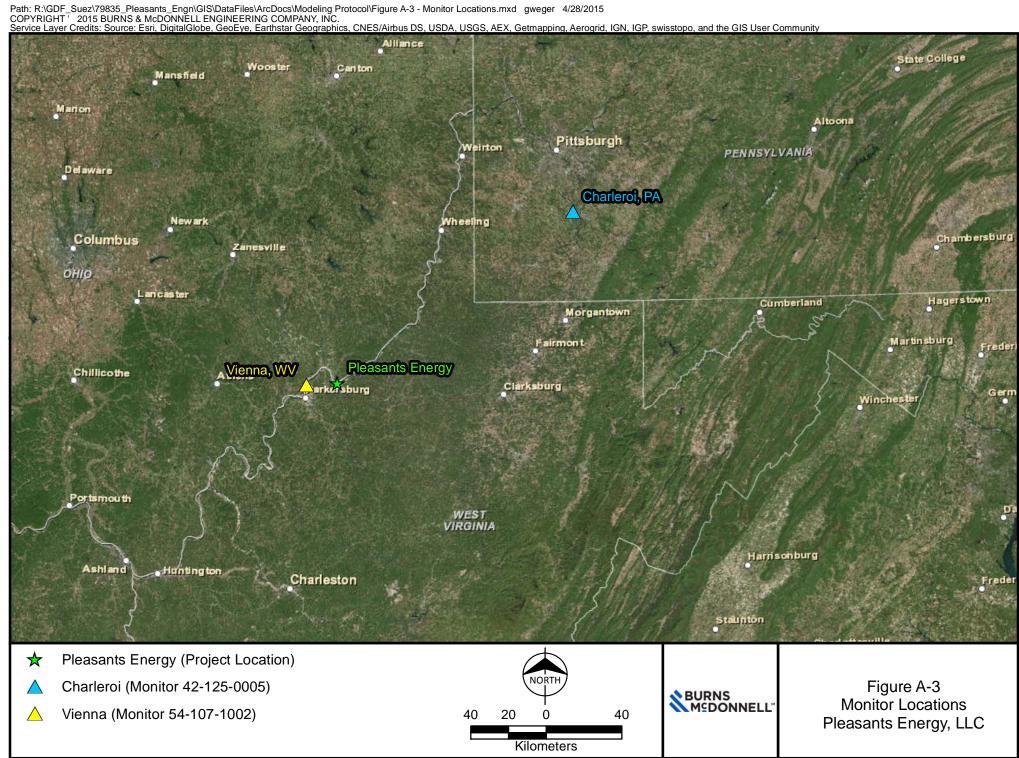
Time Frequency	Wind Sector	Surface Albedo	Bowen Ratio	Surface Roughness	Surface Moisture
May	4 of 12	0.15	0.52	0.247	Average
May	5 of 12	0.15	0.52	0.739	Average
May	6 of 12	0.15	0.52	0.509	Average
May	7 of 12	0.15	0.52	0.495	Average
May	8 of 12	0.15	0.52	0.341	Average
May	9 of 12	0.15	0.52	0.216	Average
May	10 of 12	0.15	0.52	0.147	Average
May	11 of 12	0.15	0.52	0.061	Average
May	12 of 12	0.15	0.52	0.027	Average
June	1 of 12	0.16	0.33	0.106	Average
June	2 of 12	0.16	0.33	0.362	Average
June	3 of 12	0.16	0.33	0.439	Average
June	4 of 12	0.16	0.33	0.564	Average
June	5 of 12	0.16	0.33	1.075	Average
June	6 of 12	0.16	0.33	0.736	Average
June	7 of 12	0.16	0.33	0.676	Average
June	8 of 12	0.16	0.33	0.584	Average
June	9 of 12	0.16	0.33	0.452	Average
June	10 of 12	0.16	0.33	0.313	Average
June	11 of 12	0.16	0.33	0.138	Average
June	12 of 12	0.16	0.33	0.06	Average
July	1 of 12	0.16	0.33	0.106	Average
July	2 of 12	0.16	0.33	0.362	Average
July	3 of 12	0.16	0.33	0.439	Average
July	4 of 12	0.16	0.33	0.564	Average
July	5 of 12	0.16	0.33	1.075	Average
July	6 of 12	0.16	0.33	0.736	Average
July	7 of 12	0.16	0.33	0.676	Average
July	8 of 12	0.16	0.33	0.584	Average
July	9 of 12	0.16	0.33	0.452	Average
July	10 of 12	0.16	0.33	0.313	Average
July	11 of 12	0.16	0.33	0.138	Average
July	12 of 12	0.16	0.33	0.06	Average
August	1 of 12	0.16	0.33	0.106	Average
August	2 of 12	0.16	0.33	0.362	Average
August	3 of 12	0.16	0.33	0.439	Average
August	4 of 12	0.16	0.33	0.564	Average
August	5 of 12	0.16	0.33	1.075	Average
August	6 of 12	0.16	0.33	0.736	Average
August	7 of 12	0.16	0.33	0.676	Average
August	8 of 12	0.16	0.33	0.584	Average
August	9 of 12	0.16	0.33	0.452	Average
August	10 of 12	0.16	0.33	0.313	Average
August	11 of 12	0.16	0.33	0.138	Average
August	12 of 12	0.16	0.33	0.06	Average
September	1 of 12	0.16	0.78	0.106	Average
September	2 of 12	0.16	0.78	0.362	Average
September	3 of 12	0.16	0.78	0.439	Average
September	4 of 12	0.16	0.78	0.564	Average
September	5 of 12	0.16	0.78	1.075	Average
September	6 of 12	0.16	0.78	0.736	Average

Table A-3: Site AERSURFACE Inputs Corresponding with Monthly Surface Moisture Classifications

Time Frequency	Wind Sector	Surface Albedo	Bowen Ratio	Surface Roughness	Surface Moisture
September	7 of 12	0.16	0.78	0.676	Average
September	8 of 12	0.16	0.78	0.584	Average
September	9 of 12	0.16	0.78	0.452	Average
September	10 of 12	0.16	0.78	0.313	Average
September	11 of 12	0.16	0.78	0.138	Average
September	12 of 12	0.16	0.78	0.06	Average
October	1 of 12	0.16	0.78	0.106	Average
October	2 of 12	0.16	0.78	0.362	Average
October	3 of 12	0.16	0.78	0.439	Average
October	4 of 12	0.16	0.78	0.564	Average
October	5 of 12	0.16	0.78	1.075	Average
October	6 of 12	0.16	0.78	0.736	Average
October	7 of 12	0.16	0.78	0.676	Average
October	8 of 12	0.16	0.78	0.584	Average
October	9 of 12	0.16	0.78	0.452	Average
October	10 of 12	0.16	0.78	0.313	Average
October	11 of 12	0.16	0.78	0.138	Average
October	12 of 12	0.16	0.78	0.06	Average
November	1 of 12	0.16	1.59	0.106	Dry
November	2 of 12	0.16	1.59	0.362	Dry
November	3 of 12	0.16	1.59	0.439	Dry
November	4 of 12	0.16	1.59	0.564	Dry
November	5 of 12	0.16	1.59	1.075	Dry
November	6 of 12	0.16	1.59	0.736	Dry
November	7 of 12	0.16	1.59	0.676	Dry
November	8 of 12	0.16	1.59	0.584	Dry
November	9 of 12	0.16	1.59	0.452	Dry
November	10 of 12	0.16	1.59	0.313	Dry
November	11 of 12	0.16	1.59	0.138	Dry
November	12 of 12	0.16	1.59	0.06	Dry
December	1 of 12	0.16	0.36	0.034	Wet
December	2 of 12	0.16	0.36	0.098	Wet
December	3 of 12	0.16	0.36	0.117	Wet
December	4 of 12	0.16	0.36	0.16	Wet
December	5 of 12	0.16	0.36	0.484	Wet
December	6 of 12	0.16	0.36	0.339	Wet
December	7 of 12	0.16	0.36	0.325	Wet
December	8 of 12	0.16	0.36	0.224	Wet
December	9 of 12	0.16	0.36	0.156	Wet
December	10 of 12	0.16	0.36	0.104	Wet
December	11 of 12	0.16	0.36	0.044	Wet
December	12 of 12	0.16	0.36	0.02	Wet

Developed, High Intensity

State Highway



Issued: 4/28/2015 Source: ESRI, Burns & McDonnell

Emergent Herbaceous Wetlands

Developed, Medium Intensity

Developed, High Intensity

Shrub/Scrub

State Boundary

Highway

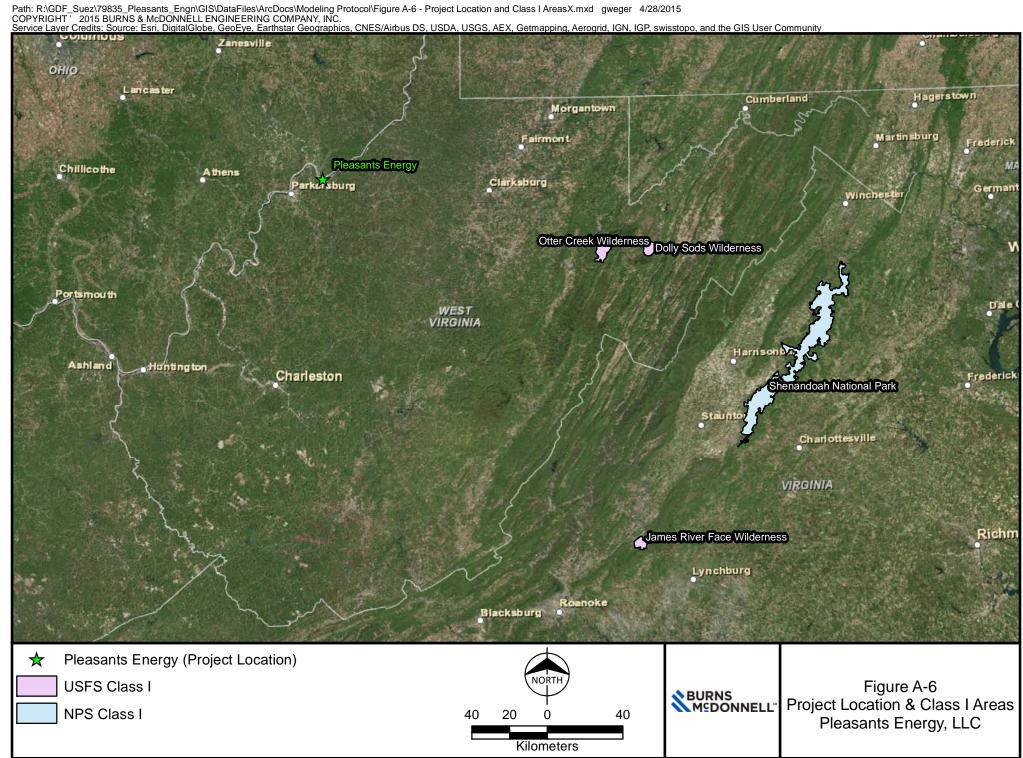


Table A-3 All Inventory Sources Considered

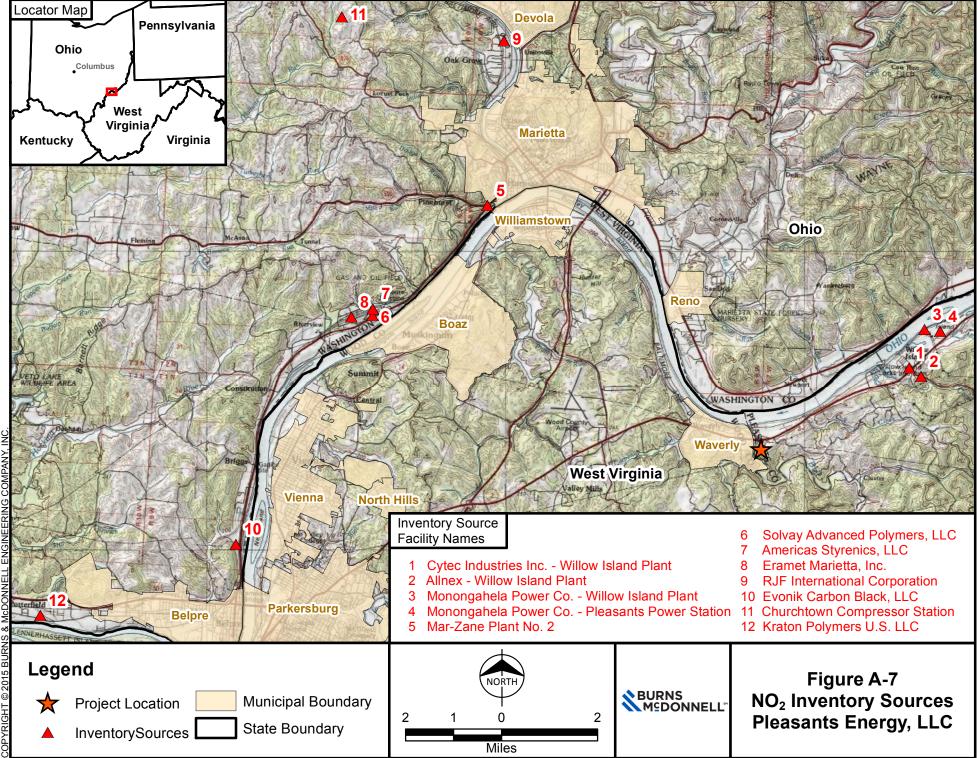
State	Site ID	Facility Site Name	Latitude	Longitude	Easting (X) (meters)	Northing (Y) (meters)	Distance (kilometers)	Included in Modeling?	Reason Not Included
WV	54-073-00003	Cytec Industries Inc Willow Island Plant	39.35556	-81.30639	473602.8	4356278.1	5.7	Yes	
WV	54-073-00004	Monongahela Power Co Willow Island Plant	39.36722	-81.30056	474109.7	4357571.2	6.8	Yes	
WV	54-073-00005	Monongahela Power Co Pleasants Power Station	39.36667	-81.29444	474636.0	4357507.8	7.2	Yes	
WV	54-085-00004	Dominion - Craig Compressor Station	39.07306	-81.09833	491494.2	4324887.5	37	Yes	
WV	54-107-00001	DuPont Washington Works	39.26945	-81.67000	442204.3	4346890.9	27.3	No	> 25 km from Project
WV	54-107-00010	Sabic Innovative Plastics LLC	39.25583	-81.67695	441593.9	4345384.8	28.2	No	> 25 km from Project
WV	54-107-00100	Columbia Gas - Rockport 4C4570	39.06889	-81.55194	452252.7	4324565.4	33.3	No	> 25 km from Project
WV	54-107-00121	Waste Management - Northwestern Landfill	39.24917	-81.49250	457503.7	4344542.1	14.3	Yes	
WV	54-073-00005	Allegheny Energy Supply Co. LLC - Pleasants Power Station	39.36680	-81.29440	474639.8	4357522.5	7.2	Yes	
WV	54-073-00030	Allnex Willow Island Plant	39.35305	-81.30177	474000.3	4355999.1	5.9	Yes	
ОН	0684020001	Americas Styrenics, LLC (0684020001)	39.37278	-81.51527	455616	4358272	14	Yes	
ОН	0684000213	Columbus Southern Power Company - Waterford Plant (0684000213)	39.53333	-81.71694	438387	4376208	38	No	> 25 km from Project
ОН	0684020006	Eramet Marietta, inc. (0684020006)	39.37028	-81.52361	454896	4357998	14	Yes	
ОН	0684010049	Evonik Carbon Black, LLC (0684010049)	39.30139	-81.56805	451020	4350376	18	Yes	
ОН	0684000105	Globe Metallurgical Inc. (0684000105)	39.58445	-81.67805	441772	4381856	39	No	> 25 km from Project
ОН	0684010011	Kraton Polymers U.S. LLC	39.27945	-81.64389	444464	4347985	25	Yes	
ОН	0684000148	Marietta Industrial Enterprises	39.34806	-81.55139	452488	4355547	16	Yes	
ОН	0684020005	Mar-Zane Plant No. 2	39.40417	-81.47083	459462	4361735	12	Yes	
ОН	0684000000	Muskingum River Power Plant	39.59056	-81.67944	441658	4382535	38	No	> 25 km from Project
ОН	0684000149	Ohio Oil Gathering Corporation - Bells Run Terminal	39.37908	-81.28876	475129	4358884	8	No	One fugitive source
ОН	0684020037	R. H. Gorsuch Station (0684020037)	39.36722	-81.52084	455133	4357658	14	No	PER Ohio EPA - Gorsuch is shutdown, since 2010.
ОН	0684020020	RJF International Corporation	39.45389	-81.46472	460017	4367250	16	Yes	
ОН	0684010138	Skyline Steel, LLC (0684010138)	39.32389	-81.56333	451443	4352871	17	Yes	
ОН	0684020008	Solvay Advanced Polymers LLC (0684020008)	39.37072	-81.51544	455600	4358043	14	Yes	
ОН	0684000212	Washington Energy Facility (0684000212)	39.58222	-81.64889	444274	4381590	37	No	> 25 km from Project
ОН	684020025	Churchtown Compressor Station (Cobra Pipeline Co. LTD) (0684020025)	39.460831	-81.528061	454572.06	4368020.5	20	Yes	

Table A-4: NO₂ Inventory Sources Modeled

State	Site ID	Facility Site Name	Easting (X) (meters)	Northing (Y) (meters)	Distance (kilometers)
WV	54-073-00003	Cytec Industries Inc Willow Island Plant	473602.8	4356278.1	6
WV	54-073-00030	Allnex - Willow Island Plant	474000.3	4355999.1	6
WV	54-073-00004	Monongahela Power Co Willow Island Plant	474109.7	4357571.2	7
WV	54-073-00005	Monongahela Power Co Pleasants Power Station	474636.0	4357507.8	7
ОН	0684020005	Mar-Zane Plant No. 2	459462.0	4361735.0	12
ОН	0684020008	Solvay Advanced Polymers, LLC	455600.0	4358043.0	14
ОН	0684020001	Americas Styrenics, LLC	455616.0	4358272.0	14
OH	0684020006	Eramet Marietta, Inc.	454896.0	4357998.0	14
ОН	0684020020	RJF International Corporation	460017.0	4367250.0	16
ОН	0684010049	Evonik Carbon Black, LLC	451020.0	4350376.0	18
OH	0684020025	Churchtown Compressor Station	454572.1	4368020.5	20
OH	0684010011	Kraton Polymers U.S. LLC	444464.0	4347985.0	25
ОН	0684010138	Skyline Steel, LLC (0684010138)	451443	4352871	17

Table A-5: PM_{2.5} Inventory Sources Modeled

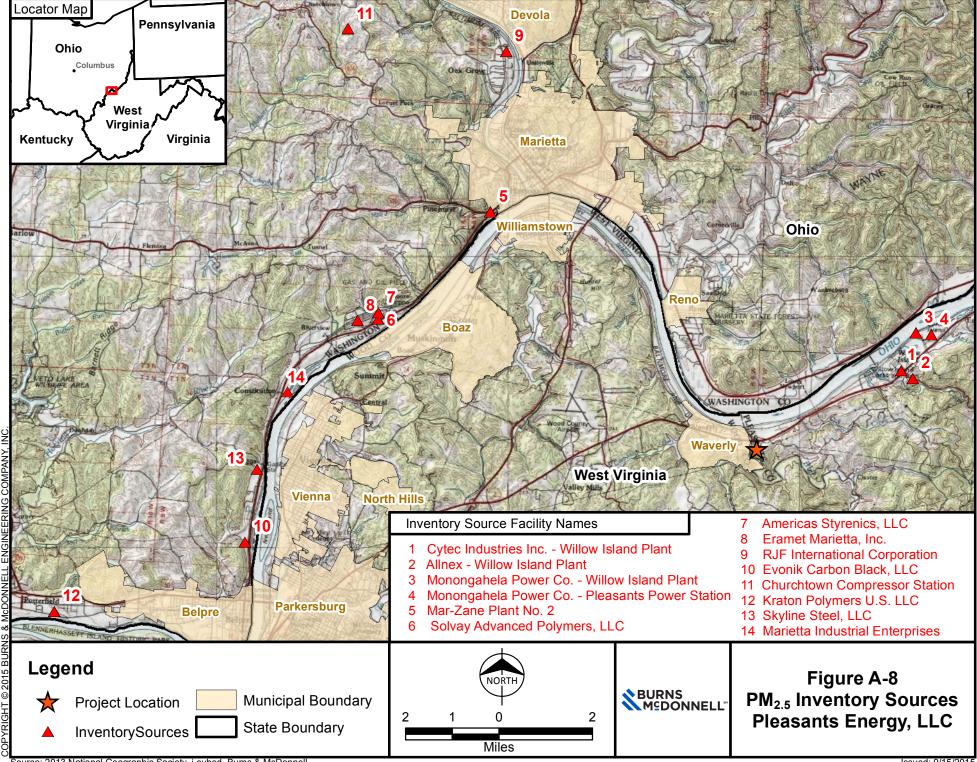
State	Site ID	Facility Site Name	Easting (X) (meters)	Northing (Y) (meters)	Distance (kilometers)
WV	54-073-00003	Cytec Industries Inc Willow Island Plant	473602.8	4356278.1	6
WV	54-073-00030	Allnex - Willow Island Plant	474000.3	4355999.1	6
WV	54-073-00004	Monongahela Power Co Willow Island Plant	474109.7	4357571.2	7
WV	54-073-00005	Monongahela Power Co Pleasants Power Station	474636.0	4357507.8	7
ОН	0684020001	Americas Styrenics, LLC	455616.0	4358272.0	14
ОН	0684020006	Eramet Marietta, Inc.	454896.0	4357998.0	14
OH	0684010049	Evonik Carbon Black, LLC	451020.0	4350376.0	18
ОН	0684010011	Kraton Polymers U.S. LLC	444464.0	4347985.0	25
ОН	0684000148	Marietta Industrial Enterprises	452488	4355547	16
ОН	0684020005	Mar-Zane Plant No. 2	459462.0	4361735.0	12
ОН	0684020020	RJF International Corporation	460017.0	4367250.0	16
ОН	0684020008	Solvay Advanced Polymers, LLC	455600.0	4358043.0	14
ОН	0684010138	Skyline Steel, LLC (0684010138)	451443	4352871	17
ОН	0684020025	Churchtown Compressor Station	454572.1	4368020.5	20



7/22/2015

kasamuelson

iles\ArcDocs\Modeling Protocol\Figure A-7- Inventory Sources.mxd



9/15/2015

cronchetti

iles\ArcDocs\Modeling Protocol\Figure A-8- Inventory Sources.mxd



CREATE AMAZING.



Figure G-1: 20 kilometer by 20 kilometer Cartesian Grid

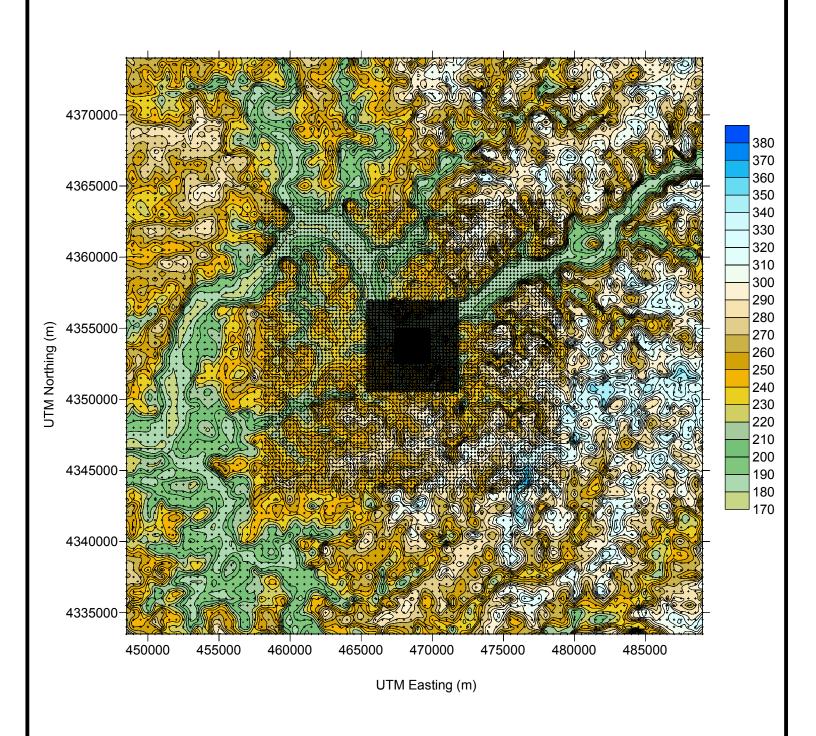






Figure G-2: 50 kilometer by 50 kilometer Cartesian Grid

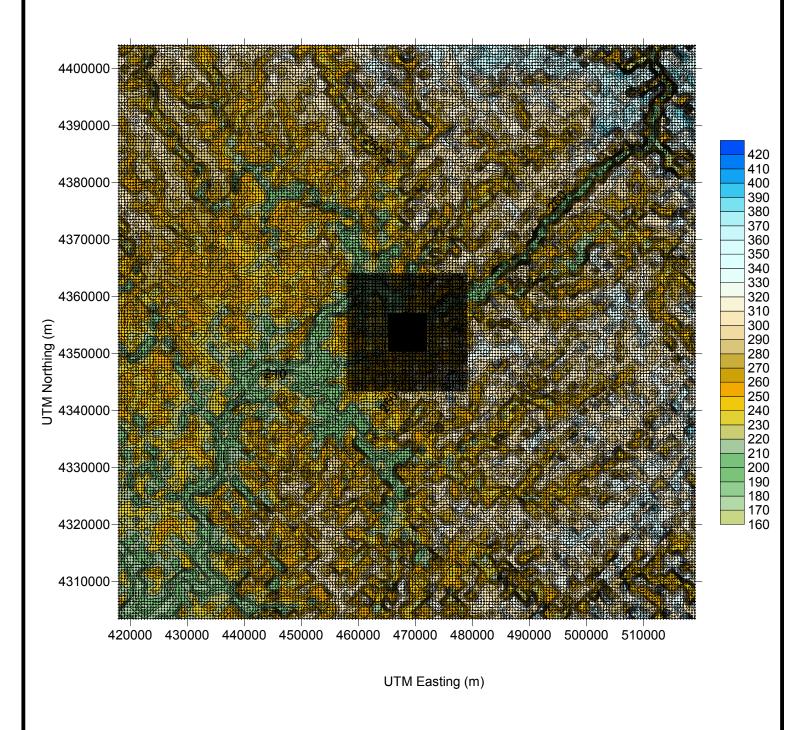
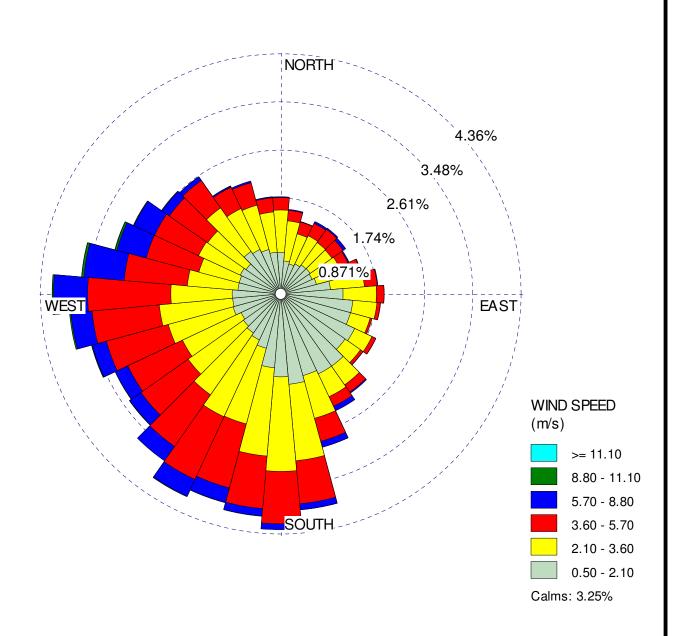


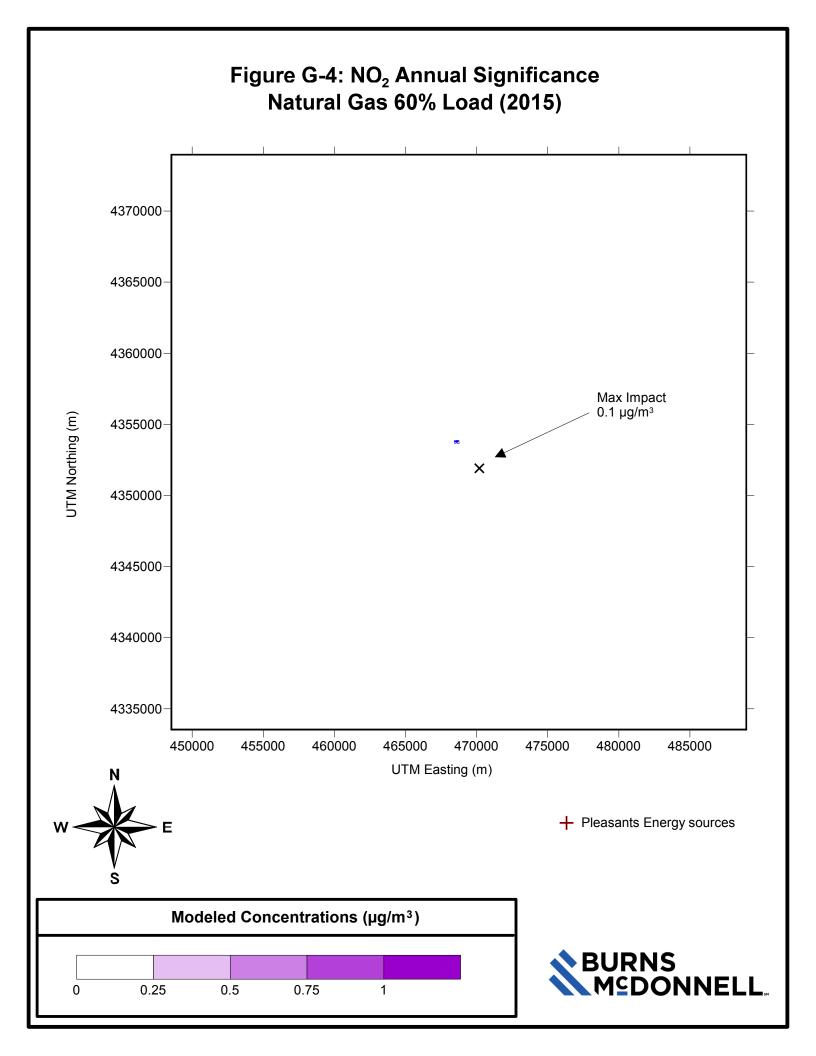




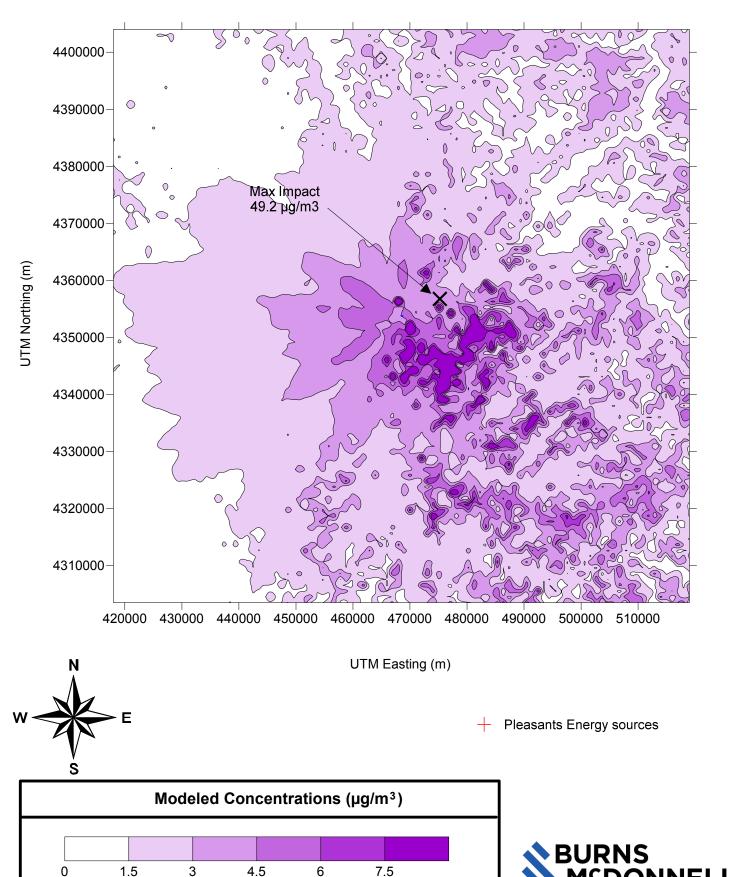
Figure G-3: Parkersburg Wood County Airport (Station ID 03804) Wind Speed and Wind Direction (Blowing From) for Years 2012 to 2016

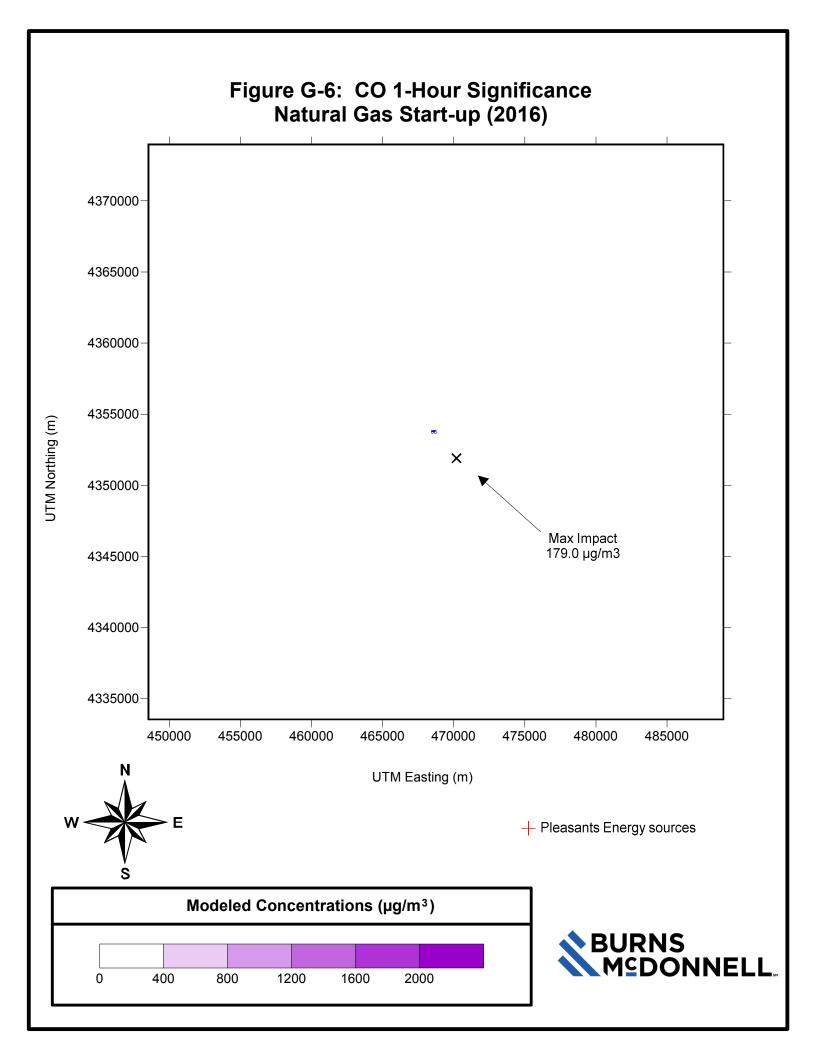


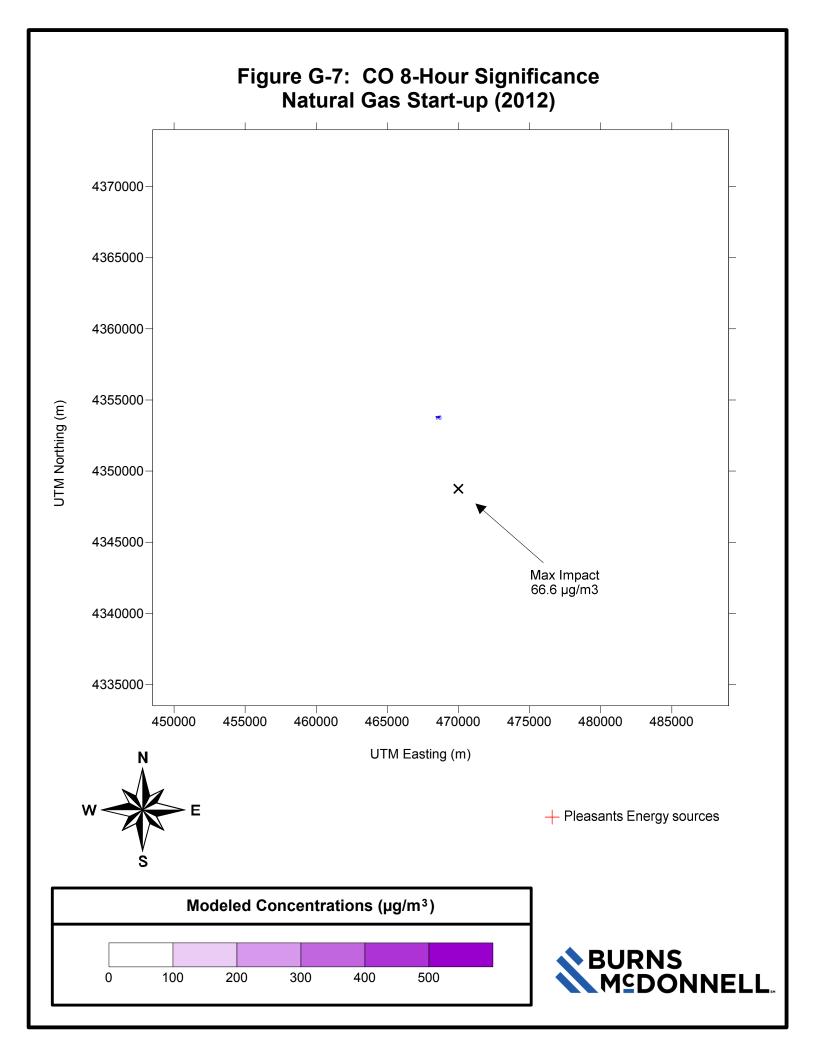


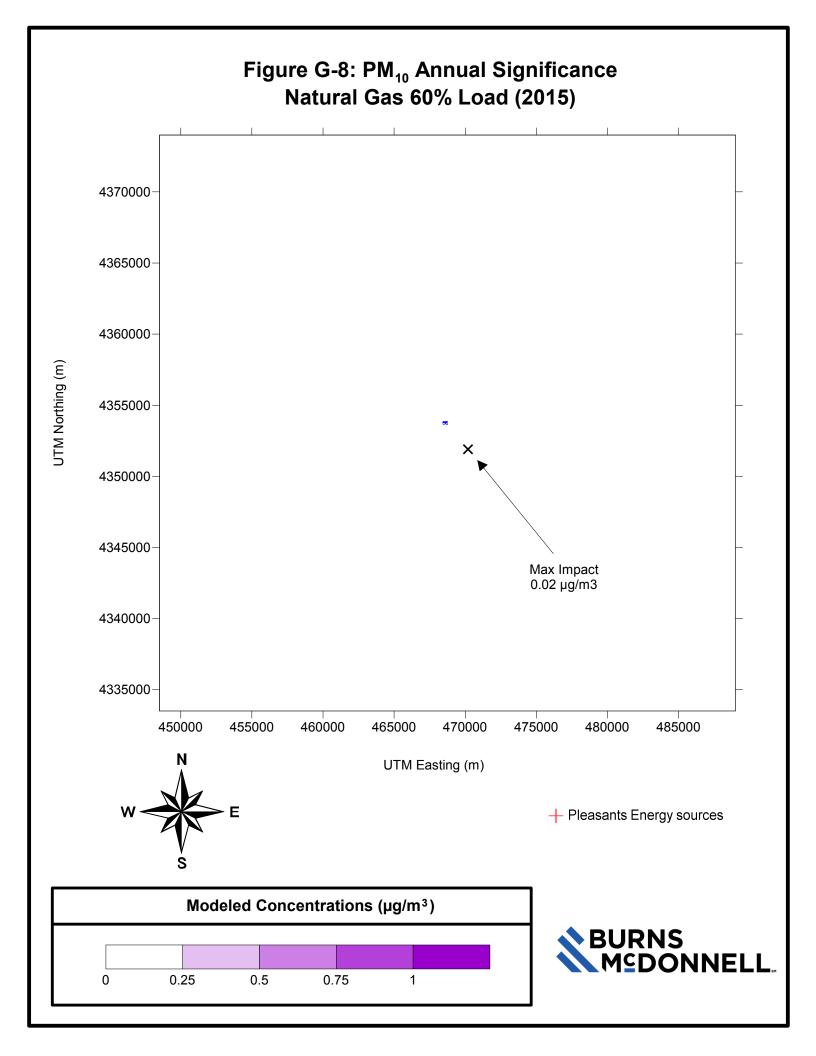


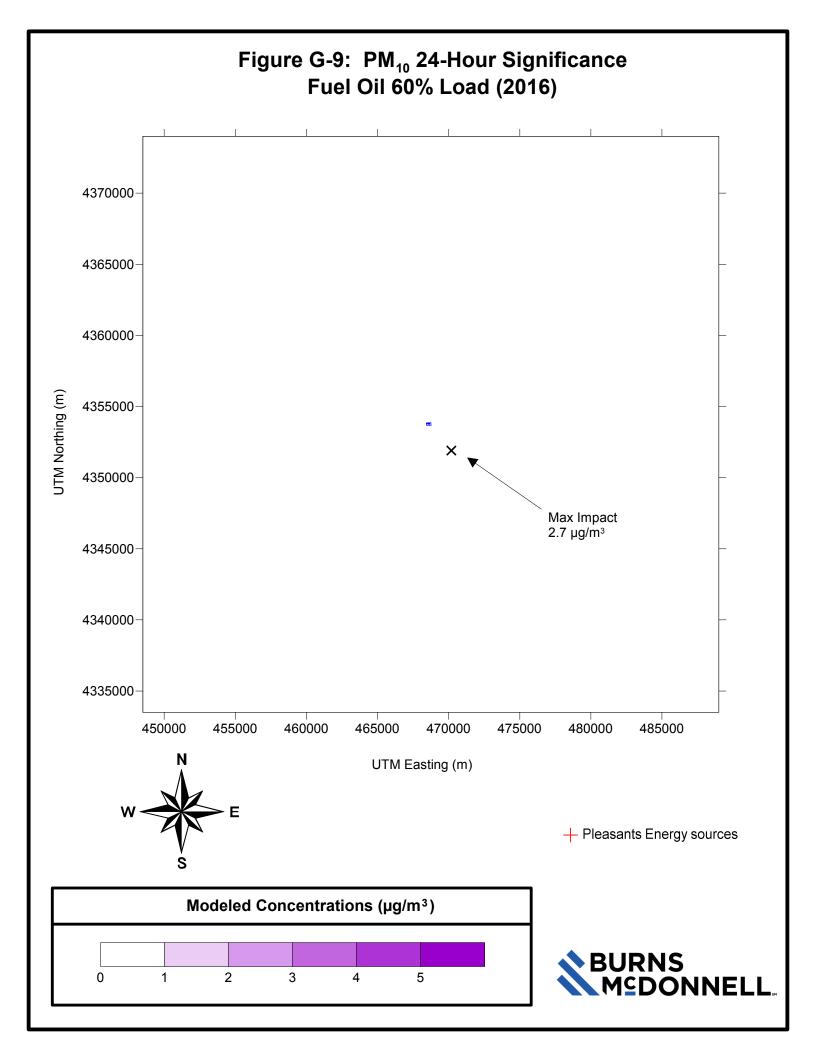


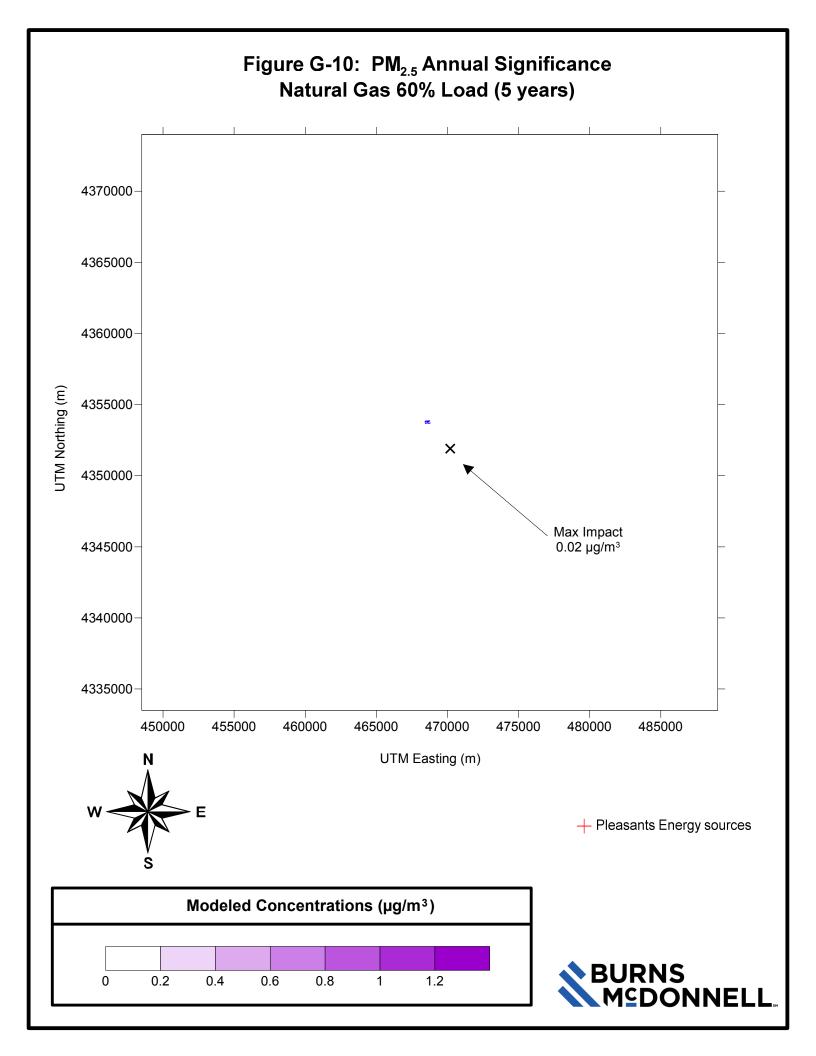


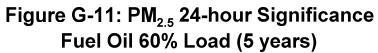


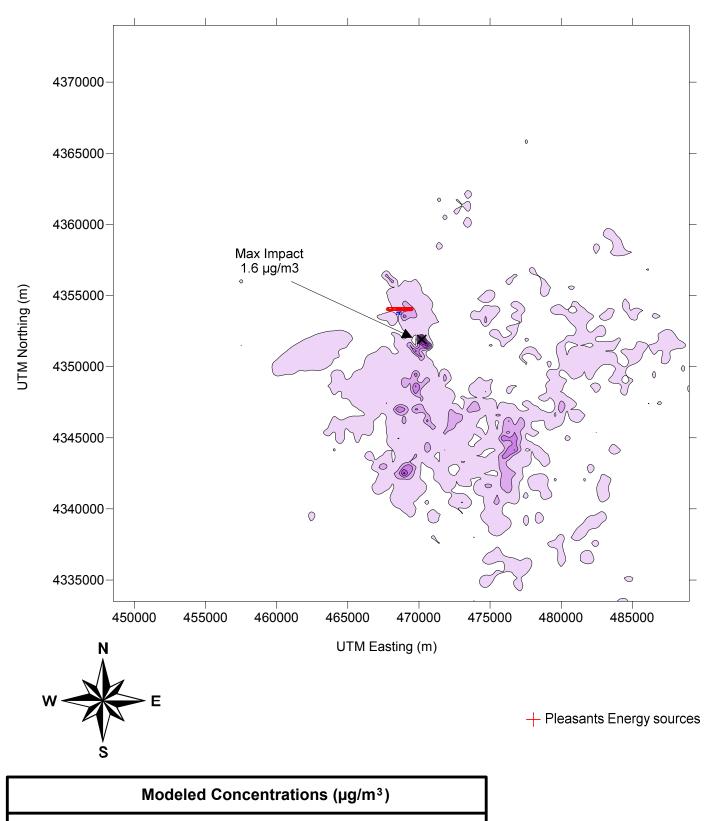












1.2

1

0.2

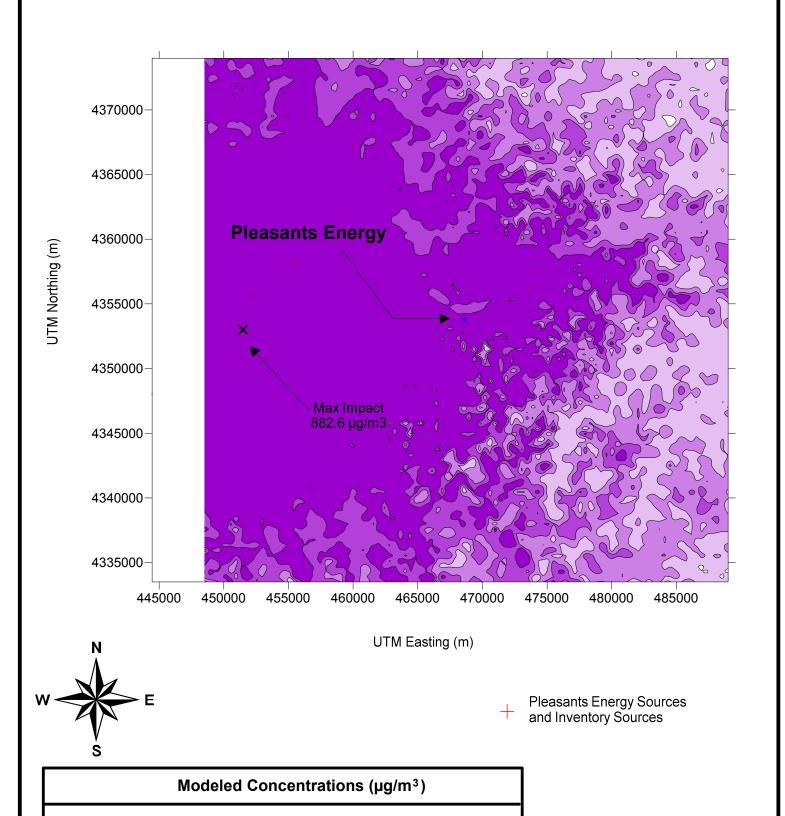
0.4

0.6

8.0



Figure G-12: Class II Increment PM_{2.5} 24-hour (2013)



2

6

8

BURNS MCDONNELL.



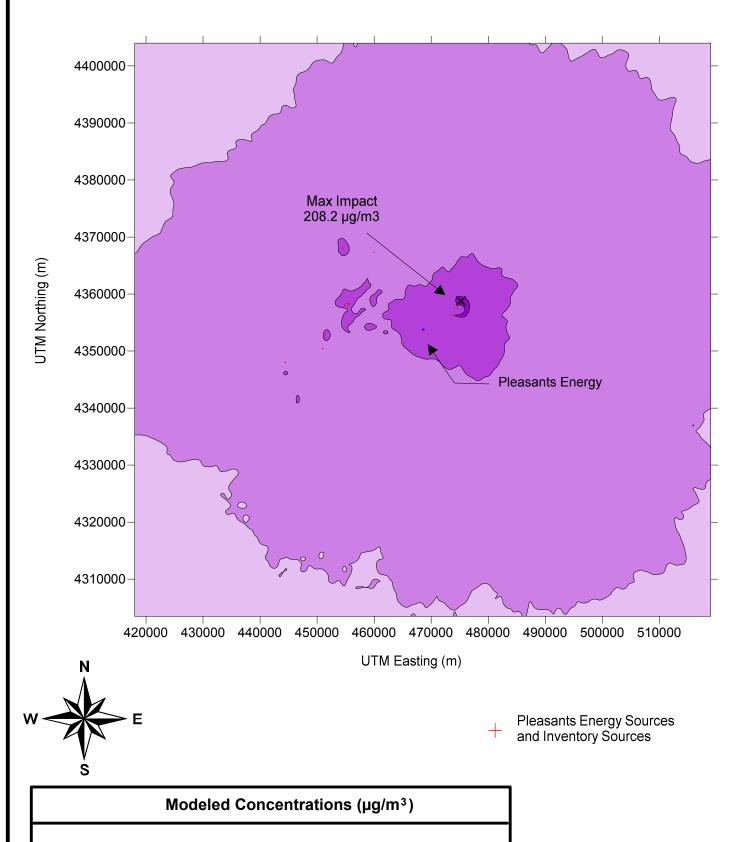
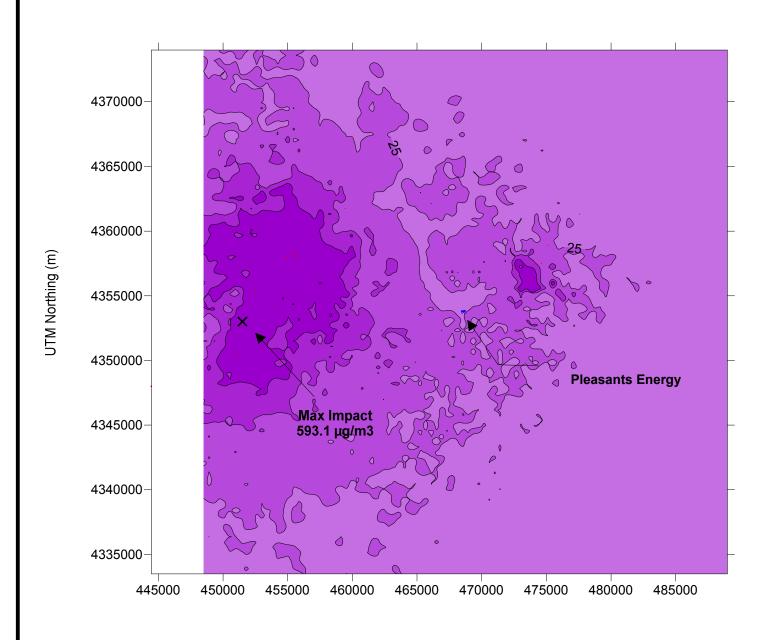
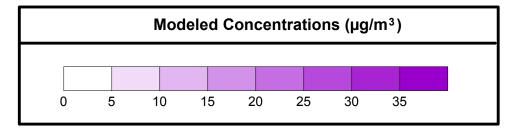




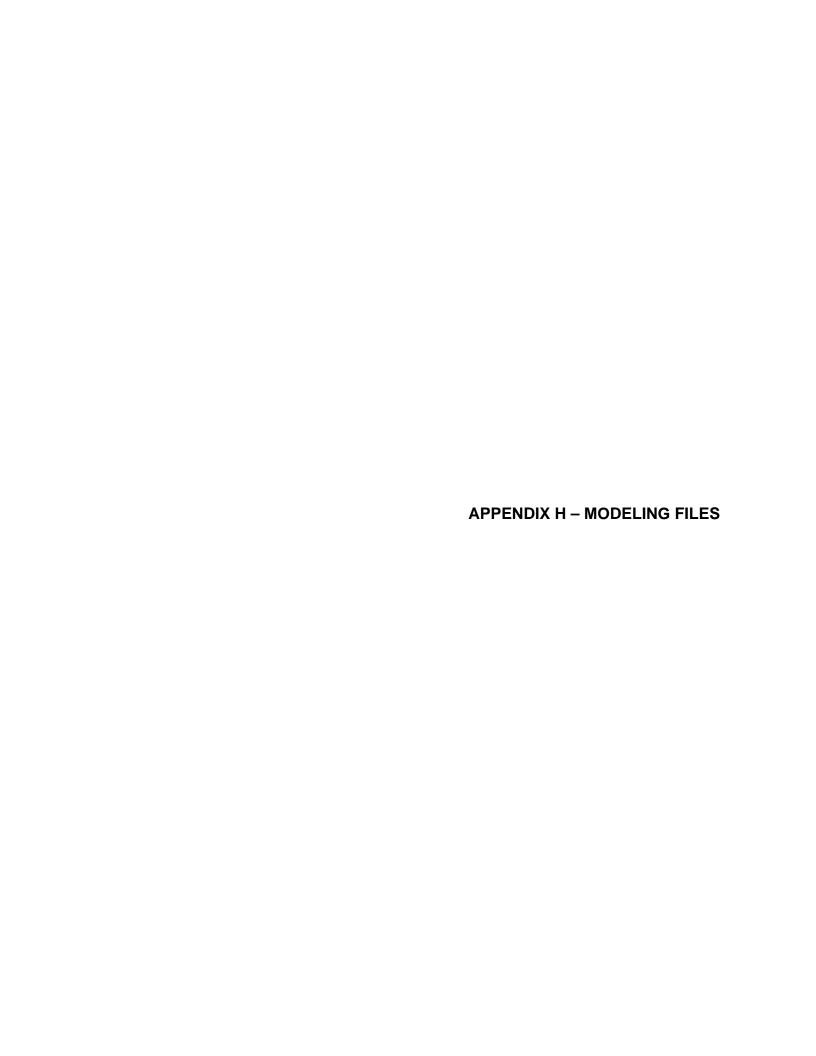
Figure G-14: NAAQS PM_{2.5} 24-hour With Background (5 years)













VISCREEN Level I

Visual Effects Screening Analysis for Source: Pleasants Energy, LLC Class I Area: North Bend State Park

*** Level-1 Screening ***

Input Emissions for

Particulates 83.30 TON/YR
NOx (as NO2) 464.60 TON/YR
Primary NO2 0.00 TON/YR
Soot 0.00 TON/YR
Primary SO4 0.00 TON/YR

**** Default Particle Characteristics Assumed

Transport Scenario Specifications:

Background Ozone: 0.04 ppm
Background Visual Range: 40.00 km
Source-Observer Distance: 25.00 km
Min. Source-Class I Distance: 25.00 km
Max. Source-Class I Distance: 25.00 km
Plume-Source-Observer Angle: 11.25 degrees

Stability: 6

Wind Speed: 1.00 m/s

RESULTS

Asterisks (*) indicate plume impacts that exceed screening criteria

Maximum Visual Impacts INSIDE Class I Area Screening Criteria ARE Exceeded

					Del	ta E	Con	trast
					=====	=====	=====	======
Backgrnd	Theta	Azi	Distance	Alpha	Crit	Plume	Crit	Plume
=======	=====	===	=======	=====	====	=====	====	=====
SKY	10.	84.	25.0	84.	2.00	2.073*	0.05	0.001
SKY	140.	84.	25.0	84.	2.00	0.798	0.05	-0.011
TERRAIN	10.	84.	25.0	84.	2.00	0.916	0.05	0.011
TERRAIN	140.	84.	25.0	84.	2.00	0.228	0.05	0.006

Maximum Visual Impacts OUTSIDE Class I Area Screening Criteria ARE Exceeded

					Del	ta E	Con	trast
					=====	=====	=====	======
Backgrnd	Theta	Azi	Distance	Alpha	Crit	Plume	Crit	Plume
=======	=====	===	=======	=====	====	=====	====	=====
SKY	10.	25.	17.9	144.	2.00	2.451*	0.05	0.002
SKY	140.	25.	17.9	144.	2.00	0.888	0.05	-0.015
TERRAIN	10.	0.	1.0	168.	2.00	2.698*	0.05	0.032
TERRAIN	140.	0.	1.0	168.	2.00	0.737	0.05	0.029

Blennerhassett 9/13/2017

Visual Effects Screening Analysis for Source: Pleasants Energy, LLC Class I Area: Blennerhassett Island

*** Level-1 Screening ***

Input Emissions for

Particulates 83.30 TON/YR
NOx (as NO2) 464.60 TON/YR
Primary NO2 0.00 TON/YR
Soot 0.00 TON/YR
Primary SO4 0.00 TON/YR

**** Default Particle Characteristics Assumed

Transport Scenario Specifications:

Background Ozone: 0.04 ppm
Background Visual Range: 40.00 km
Source-Observer Distance: 24.00 km
Min. Source-Class I Distance: 24.00 km
Max. Source-Class I Distance: 24.00 km
Plume-Source-Observer Angle: 11.25 degrees

Stability: 6

Wind Speed: 1.00 m/s

RESULTS

Asterisks (*) indicate plume impacts that exceed screening criteria

Maximum Visual Impacts INSIDE Class I Area Screening Criteria ARE Exceeded

					Del	ta E	Con	trast
					=====	=====	=====	======
Backgrnd	Theta	Azi	Distance	Alpha	Crit	Plume	Crit	Plume
=======	=====	===	=======	=====	====	=====	====	=====
SKY	10.	84.	24.0	84.	2.00	2.155*	0.05	0.001
SKY	140.	84.	24.0	84.	2.00	0.832	0.05	-0.012
TERRAIN	10.	84.	24.0	84.	2.00	0.981	0.05	0.011
TERRAIN	140.	84.	24.0	84.	2.00	0.241	0.05	0.006

Maximum Visual Impacts OUTSIDE Class I Area Screening Criteria ARE Exceeded

					Del	ta E	Con	trast
					=====	=====	=====	======
${\tt Backgrnd}$	Theta	Azi	Distance	Alpha	Crit	Plume	Crit	Plume
=======	=====	===	=======	=====	====	=====	====	=====
SKY	10.	20.	15.8	149.	2.00	2.607*	0.05	0.002
SKY	140.	20.	15.8	149.	2.00	0.929	0.05	-0.017
TERRAIN	10.	0.	1.0	168.	2.00	2.958*	0.05	0.035
TERRAIN	140.	0.	1.0	168.	2.00	0.801	0.05	0.032

VISCREEN Level II

Visual Effects Screening Analysis for Source: Pleasants Energy, LLC Class I Area: North Bend State Park

 $\,$ *** User-selected Screening Scenario Results *** Input Emissions for

Particula	tes	83.30	TON/YR
NOx (as No	02) 4	64.60	TON/YR
Primary N	02	0.00	TON/YR
Soot		0.00	TON/YR
Primary S	04	0.00	TON/YR

PARTICLE CHARACTERISTICS

	Density	Diameter
	======	=======
Primary Part.	2.5	6
Soot	2.0	1
Sulfate	1.5	4

Transport Scenario Specifications:

Background Ozone:	0.04 ppm
Background Visual Range:	40.00 km
Source-Observer Distance:	25.00 km
Min. Source-Class I Distance:	25.00 km
Max. Source-Class I Distance:	25.00 km
Plume-Source-Observer Angle:	11.25 degrees

Stability: 5

Wind Speed: 4.00 m/s

RESULTS

Asterisks (*) indicate plume impacts that exceed screening criteria

Maximum Visual Impacts INSIDE Class I Area Screening Criteria ARE NOT Exceeded

					Del	ta E	Con	trast
					=====	=====	=====	======
Backgrnd	Theta	Azi	Distance	Alpha	Crit	Plume	Crit	Plume
=======	=====	===	=======	=====	====	=====	====	=====
SKY	10.	84.	25.0	84.	2.29	0.291	0.05	0.000
SKY	140.	84.	25.0	84.	2.00	0.112	0.05	-0.002
TERRAIN	10.	84.	25.0	84.	2.00	0.128	0.05	0.001
TERRAIN	140.	84.	25.0	84.	2.00	0.031	0.05	0.001

Maximum Visual Impacts OUTSIDE Class I Area Screening Criteria ARE NOT Exceeded

	DOLO		g CIICCIIC		.01	ccaca		
					Del	ta E	Con	trast
					=====	=====	=====	======
Backgrnd	Theta	Azi	Distance	Alpha	Crit	Plume	Crit	Plume
=======	=====	===	=======	=====	====	=====	====	=====
SKY	10.	0.	1.0	168.	2.00	0.501	0.05	0.003
SKY	140.	0.	1.0	168.	2.00	0.107	0.05	-0.005
TERRAIN	10.	0.	1.0	168.	2.00	0.533	0.05	0.007
TERRAIN	140.	0.	1.0	168.	2.00	0.148	0.05	0.007

Visual Effects Screening Analysis for Source: Pleasants Energy, LLC Class I Area: Blennerhassett Island

*** User-selected Screening Scenario Results *** Input Emissions for

Particulates	83.30	TON/YR
NOx (as NO2)	464.60	TON/YR
Primary NO2	0.00	TON/YR
Soot	0.00	TON/YR
Primary SO4	0.00	TON/YR

PARTICLE CHARACTERISTICS

	Density	Diameter
	======	======
Primary Part.	2.5	6
Soot	2.0	1
Sulfate	1.5	4

Transport Scenario Specifications:

Background Ozone:	0.04 ppm
Background Visual Range:	40.00 km
Source-Observer Distance:	24.00 km
Min. Source-Class I Distance:	24.00 km
Max. Source-Class I Distance:	24.00 km
Plume-Source-Observer Angle:	11.25 degrees

Stability: 6
Wind Speed: 3.00 m/s

RESULTS

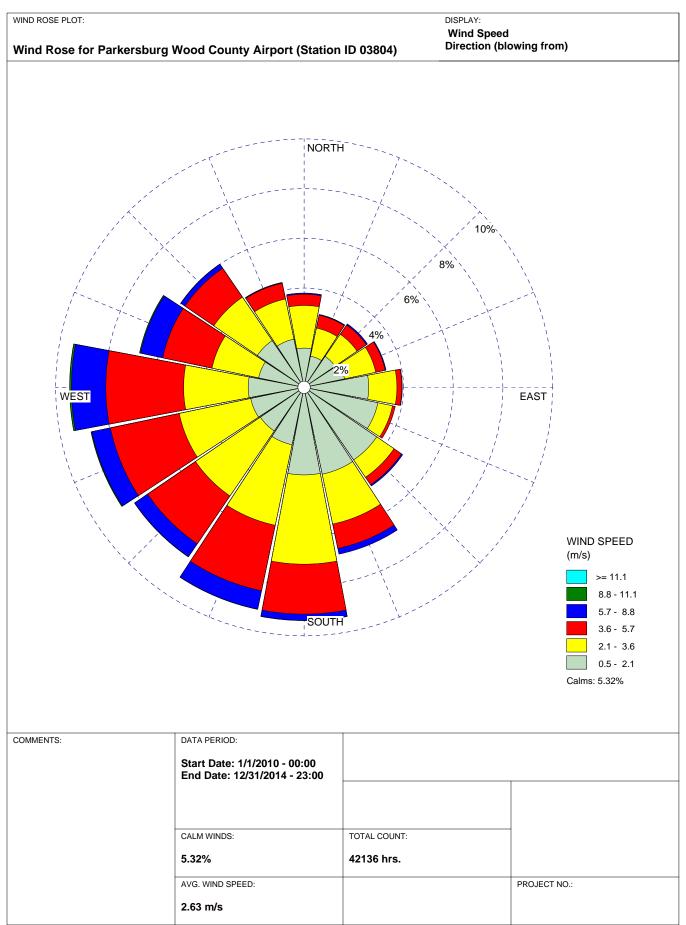
Asterisks (*) indicate plume impacts that exceed screening criteria

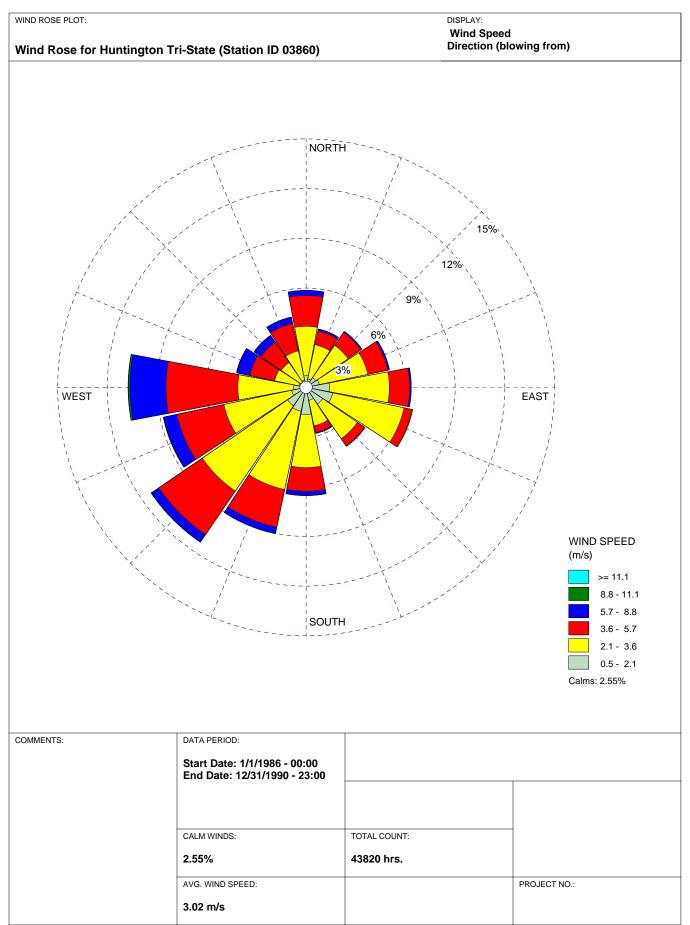
Maximum Visual Impacts INSIDE Class I Area Screening Criteria ARE NOT Exceeded

					Del	ta E	Con	trast
					=====	=====	=====	======
Backgrnd	Theta	Azi	Distance	Alpha	Crit	Plume	Crit	Plume
=======	=====	===	=======	=====	====	=====	====	=====
SKY	10.	84.	24.0	84.	2.00	0.732	0.05	0.000
SKY	140.	84.	24.0	84.	2.00	0.283	0.05	-0.004
TERRAIN	10.	84.	24.0	84.	2.00	0.332	0.05	0.004
TERRAIN	140.	84.	24.0	84.	2.00	0.081	0.05	0.002

Maximum Visual Impacts OUTSIDE Class I Area Screening Criteria ARE NOT Exceeded

	DCIC		g CIICCIIC	<i> </i>	10 I LI2	cccaca			
					Del	ta E	Con	ntrast	
					=====	=====	=====	======	
Backgrnd	Theta	Azi	Distance	Alpha	Crit	Plume	Crit	Plume	
=======	=====	===	=======	=====	====	=====	====	=====	
SKY	10.	0.	1.0	168.	2.00	0.971	0.05	0.008	
SKY	140.	0.	1.0	168.	2.00	0.168	0.05	-0.008	
TERRAIN	10.	0.	1.0	168.	2.00	1.131	0.05	0.015	
TERRAIN	140.	0.	1.0	168.	2.00	0.301	0.05	0.013	





North Bend State Park Joint Frequency Distribution*

						Probability							
					[0 -6 hr		7-12 hr		13-18 hr		19-24 hr	
					Transport		Cumulative						
Class	σ_{y}	σ_{z}	u	$\sigma_y \sigma_z u$	Time (hr)	%	%	%	Cumulative %	%	Cumulative %	%	Cumulative %
F,1	609.75	85.68	1.00	52240.50	13.9	0.00	0.00	0.01	0.01	0.00	0.00	0.02	0.02
F,2	609.75	85.68	2.00	104481.01	4.6	0.10	0.10	0.01	0.02	0.00	0.00	0.13	0.15
E,1	915.66	141.85	1.00	129882.76	13.9	0.00	0.10	0.00	0.02	0.00	0.00	0.01	0.16
F,3	609.75	85.68	3.00	156721.51	2.8	0.26	0.36	0.00	0.02	0.00	0.00	0.27	0.43
E,2	915.66	141.85	2.00	259765.52	4.6	0.04	0.39	0.05	0.07	0.01	0.01	0.09	0.52
D,1	1222.78	255.11	1.00	311942.35	13.9	0.02	0.41	0.00	0.07	0.00	0.01	0.00	0.52
E,3	915.66	141.85	3.00	389648.28	2.8	0.27	0.68	0.05	0.13	0.04	0.05	0.34	0.86
E,4	915.66	141.85	4.00	519531.04	2.0	0.17	0.86	0.00	0.13	0.06	0.11	0.39	1.25
D,2	1222.78	255.11	2.00	623884.71	4.6	0.13	0.99	0.20	0.33	0.10	0.21	0.12	1.37
E,5	915.66	141.85	5.00	649413.80	1.5	0.12	1.11	0.01	0.34	0.01	0.22	0.13	1.50
D,3	1222.78	255.11	3.00	935827.06	2.8	0.31	1.42	0.46	0.79	0.61	0.83	0.51	2.01
D,4	1222.78	255.11	4.00	1247769.41	2.0	0.39	1.81	0.55	1.34	0.85	1.68	0.44	2.45
D,5	1222.78	255.11	5.00	1559711.77	1.5	0.38	2.19	0.48	1.83	0.69	2.37	0.42	2.87
D,6	1222.78	255.11	6.00	1871654.12	1.3	0.28	2.47	0.54	2.37	0.88	3.25	0.38	3.25
D,7	1222.78	255.11	7.00	2183596.47	1.1	0.17	2.65	0.36	2.72	0.72	3.97	0.31	3.56
D,8	1222.78	255.11	8.00	2495538.83	0.9	0.12	2.77	0.11	2.83	0.28	4.26	0.08	3.64

^{*}Huntington/Tri-State Airport (Station ID 03860) was used for years 1986 to 1990

Blennerhassett Island State Historical Park Joint Frequency Distribution*

						Probability							
					[0 -6 hr		7-12 hr		13-18 hr		19-24 hr	
					Transport		Cumulative						
Class	σ_{y}	σ_{z}	u	$\sigma_y \sigma_z u$	Time (hr)	%	%	%	Cumulative %	%	Cumulative %	%	Cumulative %
F,1	588.25	83.79	1.00	49289.23	13.3	0.10	0.10	0.01	0.01	0.00	0.00	0.05	0.05
F,2	588.25	83.79	2.00	98578.47	4.4	0.33	0.43	0.05	0.05	0.00	0.00	0.31	0.37
E,1	883.38	138.57	1.00	122414.03	13.3	0.02	0.45	0.03	0.08	0.00	0.00	0.05	0.41
F,3	588.25	83.79	3.00	147867.70	2.7	1.17	1.62	0.05	0.14	0.00	0.00	1.13	1.54
E,2	883.38	138.57	2.00	244828.05	4.4	0.15	1.76	0.16	0.30	0.00	0.00	0.11	1.65
D,1	1179.69	248.49	1.00	293140.53	13.3	0.01	1.77	0.06	0.37	0.00	0.00	0.04	1.69
E,3	883.38	138.57	3.00	367242.08	2.7	0.63	2.40	0.21	0.58	0.06	0.06	0.87	2.56
E,4	883.38	138.57	4.00	489656.11	1.9	0.35	2.75	0.05	0.62	0.06	0.13	0.43	2.99
D,2	1179.69	248.49	2.00	586281.06	4.4	0.17	2.92	0.35	0.97	0.16	0.28	0.25	3.23
E,5	883.38	138.57	5.00	612070.14	1.5	0.13	3.05	0.00	0.97	0.01	0.29	0.20	3.43
D,3	1179.69	248.49	3.00	879421.59	2.7	0.78	3.83	1.12	2.09	1.01	1.31	0.72	4.16
D,4	1179.69	248.49	4.00	1172562.12	1.9	0.54	4.37	0.84	2.93	0.98	2.28	0.57	4.72
D,5	1179.69	248.49	5.00	1465702.65	1.5	0.21	4.58	0.27	3.21	0.48	2.77	0.38	5.11
D,6	1179.69	248.49	6.00	1758843.18	1.2	0.16	4.73	0.17	3.38	0.16	2.92	0.15	5.25
D,7	1179.69	248.49	7.00	2051983.72	1.0	0.06	4.79	0.04	3.42	0.05	2.98	0.06	5.32
D,8	1179.69	248.49	8.00	2345124.25	0.9	0.03	4.82	0.02	3.43	0.02	3.00	0.00	5.32

^{*}Huntington/Tri-State Airport (Station ID 03860) was used for years 1986 to 1990



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