SWN
Southwestern Energy®

ID # 009-00098
Reg R13-2958D
Company SWN Production Company
Facility John Harwatt Pad Initials

Conway Office
1000 SWN Drive
P.O. Box 789
Conway, Arkansas 72032
www.swn.com

March 18, 2016

RECEIVED
MAR 22 2016
WV DEP / DIV OF AIR QUALITY

Mr. Fred Durham, Director
West Virginia Department of Environmental Protection
Division of Air Quality
601 57th Street, SE
Charleston, WV 25304

Phone: (304) 926-0499
Fax: (304) 926-0479

RE: Class 1 Modification –John Harwatt Pad, Permit # R13-2958C

Mr. Durham:

SWN Production Company, LLC respectfully submits the enclosed Class 1 Modification for the John Harwatt Pad, Permit # R13-2958C located in Brooke County, West Virginia.

This modification proposes to remove one (1) G3306 NA compressor engine, 0.50 mmBtu/hr heater treater and the lower pressure tower (LPT).

If you have any questions regarding the information in this application, please contact me at (501) 548-6728 or at Travis_Lee@swn.com.

Sincerely,

Travis Lee
Sr. HS&E Coordinator

Entire Document
NON-CONFIDENTIAL

SWN PRODUCTION COMPANY, LLC

JOHN HARWATT PAD

CLASS I ADMINISTRATIVE UPDATE

SUBMITTED TO WVDEP DIVISION OF AIR QUALITY
MARCH 2016

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INTRODUCTION

SWN Production Company, LLC (SWN) submits the enclosed application for a Class I Administrative Update to Permit No. R13-2958C for the John Harwatt Pad. With this application, SWN requests authorization to eliminate the low pressure tower (LPT), flash gas compressor (EU-ENG1) and one heater treater (HT-2). Instead, the gas and liquids will be routed from the gas production units (GPU) to the heater treater and then to the storage tanks. One heater treater (EU-HT2) will also be removed. Gas vented from the storage tanks (EU-TANKS-COND and EU-TANKS-PW) and loading (EU-LOAD-COND and EU-LOAD-PW) is controlled by the combustor (APC-COMB-TKLD).

Equipment Description

Permitted equipment includes one (1) natural gas-fired 145-hp Caterpillar G3306 NA flash gas compressor engine equipped with a non-selective catalytic reduction (NSCR) catalytic converter (EU-ENG1), two (2) 1.0-mmBtu/hr natural gas-fired GPU burners (EU-GPU1 and EU-GPU2), two (2) 0.5-mmBtu/hr natural gas-fired heater treaters (EU-HT1 and EU-HT2), two (2) 1.5-mmBtu/hr natural gas-fired line heaters (EU-LH1 and EU-LH2), six (6) 400-bbl condensate storage tanks (collectively known as EU-TANKS-COND), six (6) 400-bbl produced water storage tanks (collectively known as EU-TANKS-PW), condensate truck loading (EU-LOAD-COND), produced water truck loading (EU-LOAD-PW), one (1) 8.0-mmBtu/hr vapor combustor (APC-COMB-TKLD) with one (1) 50-SCFH natural gas-fired pilot (EU-PILOT), associated fugitive emissions (EU-FUG) and fugitive haul road emissions (EU-HR). Note that other small storage tanks may be present on site (i.e., methanol, lube oil) but are considered de minimis sources per Table 45-13B and are not addressed further in this application.

The following changes are proposed to the permitted equipment:

Equipment	Unit ID	Description of Change
145-hp Caterpillar G3306 NA Engine	EU-ENG1	Remove
1.0-mmBtu/hr GPU Burner	EU-GPU1	No Change
1.0-mmBtu/hr GPU Burner	EU-GPU2	No Change
0.50-mmBtu/hr Heater Treater	EU-HT1	No Change
0.50-mmBtu/hr Heater Treater	EU-HT2	Remove
1.5-mmBtu/hr Line Heater	EU-LH1	No Change
1.5-mmBtu/hr Line Heater	EU-LH2	No Change

Equipment	Unit ID	Description of Change
Six (6) 400-bbl Condensate Tanks	EU-TANKS-COND	Revise emissions based on new process simulation, expected throughput and analysis
Six (6) 400-bbl Produced Water Tanks	EU-TANKS-PW	Revise emissions based on new process simulation, expected throughput and analysis
Condensate Truck Loading	EU-LOAD-COND	Revise emissions based on new process simulation, expected throughput and analysis
Produced Water Truck Loading	EU-LOAD-PW	Revise emissions based on new process simulation, expected throughput and analysis
8.0-mmBtu/hr Vapor Combustor	APC-COMB-TKLD	Revise emissions based on change in the composition and amount of waste gas vented to combustor from storage tanks and loading activities.
Vapor Combustor Pilot	EU-PILOT	No Change
Fugitive Emissions	EU-FUG	Revised based on change in component counts from equipment removal.
Fugitive Haul Road Emissions	EU-HR	Revised based on decrease in the expected number of trucks to be loaded annually.

Proposed Emissions

Emissions calculations for the project are presented in Attachment N. A fuel heating value of 905 Btu/scf was used to calculate emissions from natural gas-fired equipment. Actual heating value may vary (generally 905 - 1,300) but using a lower heating value in the emissions calculations provides a more conservative (higher) estimate of fuel use. Condensate tank emissions were calculated by creating a profile in the EPA TANKS 4.0.9d model using properties obtained in a representative liquids analysis as the tank contents. Although produced water storage tanks contain primarily water, a profile was created in EPA TANKS 4.0.9d assuming 1% of the total throughput as condensate and 99% as water to provide a conservative emissions estimate of the trace hydrocarbons that may be entrained in the water. Flashing emissions were calculated using ProMax process simulation software. Fugitive emissions were calculated with a component count by equipment type from a similar facility, and representative extended gas and liquids analyses. Other sources were calculated using manufacturer data when available, and AP-42, EPA or API data when no manufacturer data was available.

WVDEP APPLICATION FOR NSR PERMIT
CLASS I ADMINISTRATIVE UPDATE

WEST VIRGINIA DEPARTMENT OF ENVIRONMENTAL PROTECTION **DIVISION OF AIR QUALITY** 601 57th Street, SE Charleston, WV 25304 (304) 926-0475 www.dep.wv.gov/daq	***APPLICATION FOR NSR PERMIT*** ***AND*** ***TITLE V PERMIT REVISION*** ***(OPTIONAL)***
PLEASE CHECK ALL THAT APPLY TO **NSR (45CSR13)** (IF KNOWN): ☐ **CONSTRUCTION** ☐ **MODIFICATION** ☐ **RELOCATION** ☒ **CLASS I ADMINISTRATIVE UPDATE** ☐ **TEMPORARY** ☐ **CLASS II ADMINISTRATIVE UPDATE** ☐ **AFTER-THE-FACT**	PLEASE CHECK TYPE OF **45CSR30 (TITLE V)** REVISION (IF ANY): ☐ **ADMINISTRATIVE AMENDMENT** ☐ **MINOR MODIFICATION** ☐ **SIGNIFICANT MODIFICATION** IF ANY BOX ABOVE IS CHECKED, INCLUDE TITLE V REVISION INFORMATION AS **ATTACHMENT S** TO THIS APPLICATION

FOR TITLE V FACILITIES ONLY: Please refer to "Title V Revision Guidance" in order to determine your Title V Revision options (Appendix A, "Title V Permit Revision Flowchart") and ability to operate with the changes requested in this Permit Application.

Section I. General

1. Name of applicant *(as registered with the WV Secretary of State's Office):* SWN Production Company, LLC	2. Federal Employer ID No. ***(FEIN):*** 26-4388727
3. Name of facility *(if different from above):* John Harwatt Pad	4. The applicant is the: ☐ **OWNER** ☐**OPERATOR** ☒ **BOTH**
5A. Applicant's mailing address: 10000 Energy Drive Spring, TX 77389	5B. Facility's present physical address: Brooke County, West Virginia – near the town of West Liberty

6. **West Virginia Business Registration.** Is the applicant a resident of the State of West Virginia? ☒ **YES** ☐ **NO**
- If **YES,** provide a copy of the **Certificate of Incorporation/Organization/Limited Partnership** (one page) including any name change amendments or other Business Registration Certificate as **Attachment A.**
- If **NO,** provide a copy of the **Certificate of Authority/Authority of L.L.C./Registration** (one page) including any name change amendments or other Business Certificate as **Attachment A.**

7. If applicant is a subsidiary corporation, please provide the name of parent corporation: Southwestern Energy Corporation

8. Does the applicant own, lease, have an option to buy or otherwise have control of the *proposed site?* ☒ **YES** ☐ **NO**
- If **YES,** please explain: SWN is leasing the land on which the site is constructed
- If **NO,** you are not eligible for a permit for this source.

9. Type of plant or facility (stationary source) to be **constructed, modified, relocated, administratively updated** or **temporarily permitted** (e.g., coal preparation plant, primary crusher, etc.): Oil and natural gas production well pad	10. North American Industry Classification System **(NAICS)** code for the facility: 211111
11A. DAQ Plant ID No. (for existing facilities only): 009 - 00098	11B. List all current 45CSR13 and 45CSR30 (Title V) permit numbers associated with this process (for existing facilities only): R13-2958C

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

12A.

– For **Modifications, Administrative Updates** or **Temporary permits** at an existing facility, please provide directions to the *present location* of the facility from the nearest state road;

For **Construction** or **Relocation permits,** please provide directions to the *proposed new site location* from the nearest state road. Include a **MAP** as **Attachment B.**

Travel north on SR 2 from Wheeling, WV to the intersection of SR 2 and CR 67 just south of the community of Wellsburg, WV. Turn right on SR 67 East and travel 6.05 miles to the intersection of CR 67 and SR 88. Turn right (south) onto CR 88 and travel 3.7 miles to the town of West Liberty. After traveling 3.7 miles on CR 88, CR 88 makes a 90 degree turn to the left, continue straight onto CR 7/5 (Apple Pie Ridge Road). The U.S. Post Office will be on the left where CR 88 makes the hard left. Travel 0.84 miles on CR 7/5 and the access road to the well pad will be on the right.

12B. New site address (if applicable):	12C. Nearest city or town:	12D. County:
See above	West Liberty	Brooke
12.E. UTM Northing (KM): 4,447.84519	12F. UTM Easting (KM): 534.66711	12G. UTM Zone: 17T

13. Briefly describe the proposed change(s) at the facility:

SWN requests authorization to eliminate the low pressure tower (LPT) and flash gas compressor (EU-ENG1). Instead, the gas and liquids will be routed from the gas production units (GPU) to the heater treater and then to the storage tanks. One heater treater (EU-HT2) will also be removed.

14A. Provide the date of anticipated installation or change: N/A – If this is an **After-The-Fact** permit application, provide the date upon which the proposed change did happen: / /	14B. Date of anticipated Start-Up if a permit is granted: N/A

14C. Provide a **Schedule** of the planned **Installation** of/**Change** to and **Start-Up** of each of the units proposed in this permit application as **Attachment C** (if more than one unit is involved).

15. Provide maximum projected **Operating Schedule** of activity/activities outlined in this application:

Hours Per Day 24 Days Per Week 7 Weeks Per Year 52

16. Is demolition or physical renovation at an existing facility involved? ☐ **YES** ☒ **NO**

17. **Risk Management Plans.** If this facility is subject to 112(r) of the 1990 CAAA, or will become subject due to proposed changes (for applicability help see www.epa.gov/ceppo), submit your **Risk Management Plan (RMP)** to U. S. EPA Region III.

18. **Regulatory Discussion.** List all Federal and State air pollution control regulations that you believe are applicable to the proposed process *(if known)*. A list of possible applicable requirements is also included in Attachment S of this application (Title V Permit Revision Information). Discuss applicability and proposed demonstration(s) of compliance *(if known)*. Provide this information as **Attachment D.**

Section II. Additional attachments and supporting documents.

19. Include a check payable to WVDEP – Division of Air Quality with the appropriate **application fee** (per 45CSR22 and 45CSR13).

20. Include a **Table of Contents** as the first page of your application package.

21. Provide a **Plot Plan,** e.g. scaled map(s) and/or sketch(es) showing the location of the property on which the stationary source(s) is or is to be located as **Attachment E** (Refer to ***Plot Plan Guidance***) .

– Indicate the location of the nearest occupied structure (e.g. church, school, business, residence).

22. Provide **a Detailed Process Flow Diagram(s)** showing each proposed or modified emissions unit, emission point and control device as **Attachment F.**

23. Provide **a Process Description** as **Attachment G.**

– Also describe and quantify to the extent possible all changes made to the facility since the last permit review (if applicable).

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

24. Provide **Material Safety Data Sheets (MSDS)** for all materials processed, used or produced as **Attachment H.**

– For chemical processes, provide a MSDS for each compound emitted to the air.

25. Fill out the **Emission Units Table** and provide it as **Attachment I.**

26. Fill out the **Emission Points Data Summary Sheet (Table 1 and Table 2)** and provide it as **Attachment J.**

27. Fill out the **Fugitive Emissions Data Summary Sheet** and provide it as **Attachment K.**

28. Check all applicable **Emissions Unit Data Sheets** listed below:

☒ Bulk Liquid Transfer Operations
☒ Chemical Processes
☐ Concrete Batch Plant
☐ Grey Iron and Steel Foundry
☐ General Emission Unit, specify:
☒ Haul Road Emissions
☐ Hot Mix Asphalt Plant
☐ Incinerator
☐ Indirect Heat Exchanger
☐ Quarry
☐ Solid Materials Sizing, Handling and Storage Facilities
☒ Storage Tanks

Fill out and provide the **Emissions Unit Data Sheet(s)** as **Attachment L.**

29. Check all applicable **Air Pollution Control Device Sheets** listed below:

☐ Absorption Systems
☐ Adsorption Systems
☐ Afterburner
☐ Baghouse
☐ Condenser
☐ Electrostatic Precipitator
☒ Flare (VAPOR COMBUSTOR)
☐ Mechanical Collector
☐ Wet Collecting System
☐ Other Collectors, specify

Fill out and provide the **Air Pollution Control Device Sheet(s)** as **Attachment M.**

30. Provide all **Supporting Emissions Calculations** as **Attachment N,** or attach the calculations directly to the forms listed in Items 28 through 31.

31. **Monitoring, Recordkeeping, Reporting and Testing Plans.** Attach proposed monitoring, recordkeeping, reporting and testing plans in order to demonstrate compliance with the proposed emissions limits and operating parameters in this permit application. Provide this information as **Attachment O.**

➢ Please be aware that all permits must be practically enforceable whether or not the applicant chooses to propose such measures. Additionally, the DAQ may not be able to accept all measures proposed by the applicant. If none of these plans are proposed by the applicant, DAQ will develop such plans and include them in the permit.

32. **Public Notice.** At the time that the application is submitted, place a **Class I Legal Advertisement** in a newspaper of general circulation in the area where the source is or will be located (See 45CSR§13-8.3 through 45CSR§13-8.5 and ***Example Legal Advertisement*** for details). Please submit the **Affidavit of Publication** as **Attachment P** immediately upon receipt.

33. **Business Confidentiality Claims.** Does this application include confidential information (per 45CSR31)?

☐ **YES** ☒ **NO**

➢ If **YES,** identify each segment of information on each page that is submitted as confidential and provide justification for each segment claimed confidential, including the criteria under 45CSR§31-4.1, and in accordance with the DAQ's ***"Precautionary Notice – Claims of Confidentiality"*** guidance found in the ***General Instructions*** as **Attachment Q.**

Section III. Certification of Information

34. **Authority/Delegation of Authority.** Only required when someone other than the responsible official signs the application. Check applicable **Authority Form** below:

☐ Authority of Corporation or Other Business Entity
☐ Authority of Governmental Agency
☐ Authority of Partnership
☐ Authority of Limited Partnership

Submit completed and signed **Authority Form** as **Attachment R.**

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

35A. **Certification of Information.** To certify this permit application, a Responsible Official (per 45CSR§13-2.22 and 45CSR§30-2.28) or Authorized Representative shall check the appropriate box and sign below.

Certification of Truth, Accuracy, and Completeness

I, the undersigned ☒ **Responsible Official** / ☐ **Authorized Representative,** hereby certify that all information contained in this application and any supporting documents appended hereto, is true, accurate, and complete based on information and belief after reasonable inquiry I further agree to assume responsibility for the construction, modification and/or relocation and operation of the stationary source described herein in accordance with this application and any amendments thereto, as well as the Department of Environmental Protection, Division of Air Quality permit issued in accordance with this application, along with all applicable rules and regulations of the West Virginia Division of Air Quality and W.Va. Code § 22-5-1 et seq. (State Air Pollution Control Act). If the business or agency changes its Responsible Official or Authorized Representative, the Director of the Division of Air Quality will be notified in writing within 30 days of the official change.

Compliance Certification

Except for requirements identified in the Title V Application for which compliance is not achieved, I, the undersigned hereby certify that, based on information and belief formed after reasonable inquiry, all air contaminant sources identified in this application are in compliance with all applicable requirements.

SIGNATURE _____ *(Please use blue ink)* DATE: 3/21/16 *(Please use blue ink)*

35B. Printed name of signee: Paul Geiger		35C. Title: Sr. Vice President Ops Management
35D. E-mail: Paul_Geiger@swn.com	36E. Phone: ~~(304) 884-1633~~ 832 796 1000	36F. FAX:
36A. Printed name of contact person (if different from above): Zach Toothman		36B. Title: Engineering Facilities Supervisor
36C. E-mail: Zach_Toothman@swn.com	36D. Phone: (304) 884-1633	36E. FAX:

PLEASE CHECK ALL APPLICABLE ATTACHMENTS INCLUDED WITH THIS PERMIT APPLICATION:

- ☒ **Attachment A: Business Certificate**
- ☐ **Attachment B: Map(s)**
- ☐ **Attachment C: Installation and Start Up Schedule**
- ☐ **Attachment D: Regulatory Discussion**
- ☐ **Attachment E: Plot Plan**
- ☒ **Attachment F: Detailed Process Flow Diagram(s)**
- ☒ **Attachment G: Process Description**
- ☐ **Attachment H: Material Safety Data Sheets (MSDS)**
- ☒ **Attachment I: Emission Units Table**
- ☒ **Attachment J: Emission Points Data Summary Sheet**
- ☒ **Attachment K: Fugitive Emissions Data Summary Sheet**
- ☒ **Attachment L: Emissions Unit Data Sheet(s)**
- ☒ **Attachment M: Air Pollution Control Device Sheet(s)**
- ☒ **Attachment N: Supporting Emissions Calculations**
- ☐ **Attachment O: Monitoring/Recordkeeping/Reporting/Testing Plans**
- ☐ **Attachment P: Public Notice**
- ☐ **Attachment Q: Business Confidential Claims**
- ☐ **Attachment R: Authority Forms**
- ☐ **Attachment S: Title V Permit Revision Information**
- ☐ **Application Fee**

Please mail an original and three (3) copies of the complete permit application with the signature(s) to the DAQ, Permitting Section, at the address listed on the first page of this application. Please DO NOT fax permit applications.

FOR AGENCY USE ONLY – IF THIS IS A TITLE V SOURCE:

- ☐ ***Forward 1 copy of the application to the Title V Permitting Group and:***
- ☐ ***For Title V Administrative Amendments:***
  - ☐ ***NSR permit writer should notify Title V permit writer of draft permit,***
- ☐ ***For Title V Minor Modifications:***
  - ☐ ***Title V permit writer should send appropriate notification to EPA and affected states within 5 days of receipt,***
  - ☐ ***NSR permit writer should notify Title V permit writer of draft permit.***
- ☐ ***For Title V Significant Modifications processed in parallel with NSR Permit revision:***
  - ☐ ***NSR permit writer should notify a Title V permit writer of draft permit,***
  - ☐ ***Public notice should reference both 45CSR13 and Title V permits,***
  - ☐ ***EPA has 45 day review period of a draft permit.***

All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.

ATTACHMENT A: BUSINESS REGISTRATION CERTIFICATE

WEST VIRGINIA
STATE TAX DEPARTMENT
BUSINESS REGISTRATION CERTIFICATE

ISSUED TO:
SWN PRODUCTION COMPANY, LLC
5400D BIG TYLER RD
CHARLESTON, WV 25313-1103

BUSINESS REGISTRATION ACCOUNT NUMBER: **2307-3731**

This certificate is issued on: 12/8/2014

This certificate is issued by
the West Virginia State Tax Commissioner
in accordance with Chapter 11, Article 12, of the West Virginia Code

The person or organization identified on this certificate is registered to conduct business in the State of West Virginia at the location above.

This certificate is not transferrable and must be displayed at the location for which issued.

This certificate shall be permanent until cessation of the business for which the certificate of registration was granted, or until it is suspended, revoked or cancelled by the Tax Commissioner.

Change in name or change of location shall be considered a cessation of the business and a new certificate shall be required.

TRAVELING/STREET VENDORS: Must carry a copy of this certificate in every vehicle operated by them.
CONTRACTORS, DRILLING OPERATORS, TIMBER/LOGGING OPERATIONS: Must have a copy of this certificate displayed at every job site within West Virginia.

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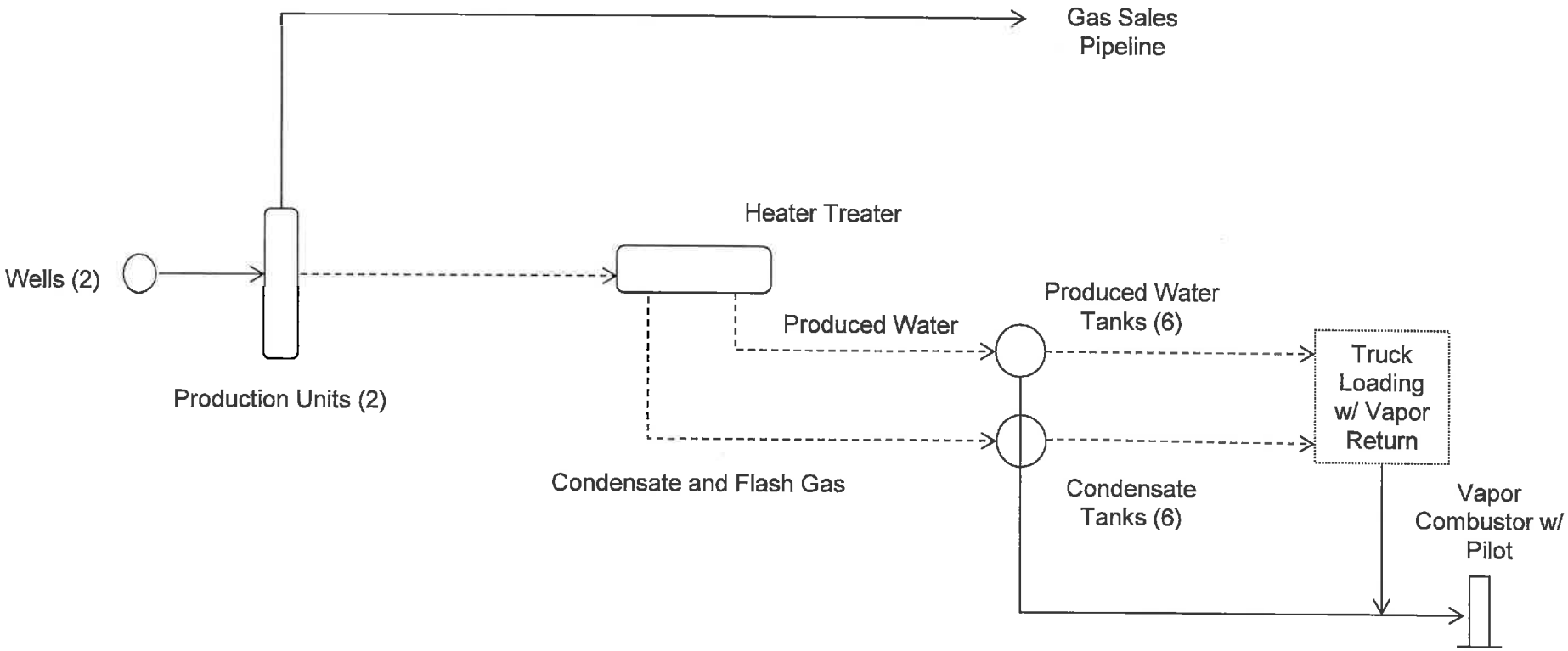

Gas/Vapor

Liquids (Condensate and Produced Water)

Note: Drawing is a depiction of general facility process and is not intended to represent facility and/or equipment layout.

SWN Production Company, LLC
John Harwatt Pad
Attachment F: Process Flow Diagram
March 2016

ATTACHMENT G: PROCESS DESCRIPTION

The facility is an oil and natural gas exploration and production facility, responsible for the production of condensate and natural gas. Storage of condensate and produced water occur on-site. A description of the facility process is as follows: Condensate, gas and water come from the wellhead(s) to the production unit(s), where the first stage of separation occurs. Fluids (condensate and produced water) will be sent to the heater treater(s). The flash from the heater treater(s) is sent to the storage tanks to be routed to the combustor for destruction. Produced water from the heater treater(s) flows into the produced water storage tank(s). Condensate flows into the storage tank(s).

The natural gas stream exits the facility for transmission via pipeline. Condensate and produced water are transported offsite via truck. Loading emissions are controlled with vapor return, which has at least 70% capture efficiency, and routed to the vapor combustor(s) for at least 98% destruction efficiency. Working, breathing and flashing vapors from the condensate and produced water storage tanks are routed to the vapor combustor(s) with a 100% capture efficiency (per WVDEP guidance) to be burned with at least 98% combustion efficiency. The vapor combustor has one (1) natural gas-fired pilot to ensure a constant flame for combustion.

A process flow diagram reflecting facility operations is shown in Attachment F.

ATTACHMENT I: EMISSION UNITS TABLE

Attachment I

Emission Units Table

(includes all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status)

Emission Unit ID[1]	Emission Point ID[2]	Emission Unit Description	Year Installed/ Modified	Design Capacity	Type[3] and Date of Change	Control Device[4]
EU-ENG1	EP-ENG1	Caterpillar G3306 NA Engine	2013	145-hp	Removal	NSCR
EU-GPU1	EP-GPU1	GPU Burner	2013	1.00-mmBtu/hr	N/A	N/A
EU-GPU2	EP-GPU2	GPU Burner	2013	1.00-mmBtu/hr	N/A	N/A
EU-HT1	EP-HT1	Heater Treater	2013	0.5-mmBtu/hr	N/A	N/A
EU-HT2	EP-HT2	Heater Treater	2013	0.5-mmBtu/hr	Removal	N/A
EU-LH1	EP-LH1	Line Heater	2013	1.5-mmBtu/hr	N/A	N/A
EU-LH2	EP-LH2	Line Heater	2013	1.5-mmBtu/hr	N/A	N/A
EU-TANKS-COND	APC-COMB-TKLD	Six (6) Condensate Tanks	2013	400-bbl each	Modification	APC-COMB-TKLD
EU-TANKS-PW	APC-COMB-TKLD	Six (6) Produced Water Tanks	2013	400-bbl each	Modification	APC-COMB-TKLD
EU-LOAD-COND	APC-COMB-TKLD	Condensate Truck Loading	2013	2,759,400 gal/yr	Modification	Vapor Return and APC-COMB-TKLD
EU-LOAD-PW	APC-COMB-TKLD	Produced Water Truck Loading	2013	1,533,000 gal/yr	Modification	Vapor Return and APC-COMB-TKLD
APC-COMB-TKLD	APC-COMB-TKLD	Vapor Combustor	2015	8.0-mmBtu/hr	Modification	N/A
EU-PILOT	APC-COMB-TKLD	Vapor Combustor Pilot	2015	50-SCFH total	N/A	N/A
EU-FUG	EP-FUG	Fugitive Emissions	2013	N/A	Modification	N/A
EU-HR	EP-HR	Fugitive Haul Road Emissions	2013	N/A	Modification	N/A

[1] For Emission Units (or Sources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.
[2] For Emission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.
[3] New, modification, removal
[4] For Control Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

ATTACHMENT J: EMISSION POINTS DATA SUMMARY SHEET

Attachment J
EMISSION POINTS DATA SUMMARY SHEET

Table 1: Emissions Data

Emission Point ID No. *(Must match Emission Units Table & Plot Plan)*	Emission Point Type[1]	Emission Unit Vented Through This Point *(Must match Emission Units Table & Plot Plan)*		Air Pollution Control Device *(Must match Emission Units Table & Plot Plan)*		Vent Time for Emission Unit (chemical processes only)		All Regulated Pollutants - Chemical Name/CAS[3] *(Speciate VOCs & HAPS)*	Maximum Potential Uncontrolled Emissions[4]		Maximum Potential Controlled Emissions[5]		Emission Form or Phase *(At exit conditions, Solid, Liquid or Gas/Vapor)*	Est. Method Used[6]	Emission Concentration[7] (ppmv or mg/m4)
		ID No.	Source	ID No.	Device Type	Short Term[2]	Max (hr/yr)		lb/hr	ton/yr	lb/hr	ton/yr			
EP-GPU1	Upward Vertical Stack	EU-GPU1	GPU Burner	N/A	None	N/A	N/A	NOx	0.11	0.48	N/A	N/A	Gas/Vapor	AP-42	N/A
								CO	0.09	0.39					
								VOC	0.01	0.03					
								SO_2	<0.01	<0.01					
								PM_{10}	0.01	0.03					
								PM_{Total}	0.01	0.04					
								n-Hexane	<0.01	0.01					
								HCHO	<0.01	<0.01					
								Benzene	<0.01	<0.01					
								Toluene	<0.01	<0.01					
								CO_2	116.98	512.36					
								CH_4	<0.01	0.01					
								N_2O	<0.01	<0.01					
EP-GPU2	Upward Vertical Stack	EU-GPU2	GPU Burner	N/A	None	N/A	N/A	NOx	0.11	0.48	N/A	N/A	Gas/Vapor	AP-42	N/A
								CO	0.09	0.39					
								VOC	0.01	0.03					
								SO_2	<0.01	<0.01					
								PM_{10}	0.01	0.03					
								PM_{Total}	0.01	0.04					
								n-Hexane	<0.01	0.01					
								HCHO	<0.01	<0.01					
								Benzene	<0.01	<0.01					
								Toluene	<0.01	<0.01					
								CO_2	116.98	512.36					
								CH_4	<0.01	0.01					
								N_2O	<0.01	<0.01					

Attachment J

EMISSION POINTS DATA SUMMARY SHEET

Table 1: Emissions Data

Emission Point ID No. *(Must match Emission Units Table & Plot Plan)*	Emission Point Type[1]	Emission Unit Vented Through This Point *(Must match Emission Units Table & Plot Plan)*		Air Pollution Control Device *(Must match Emission Units Table & Plot Plan)*		Vent Time for Emission Unit (chemical processes only)		All Regulated Pollutants - Chemical Name/CAS[3] *(Speciate VOCs & HAPS)*	Maximum Potential Uncontrolled Emissions[4]		Maximum Potential Controlled Emissions[5]		Emission Form or Phase *(At exit conditions, Solid, Liquid or Gas/Vapor)*	Est. Method Used[6]	Emission Concentration[7] (ppmv or mg/m4)
		ID No.	Source	ID No.	Device Type	Short Term[2]	Max (hr/yr)		lb/hr	ton/yr	lb/hr	ton/yr			
EP-HT1	Upward Vertical Stack	EU-HT1	Heater Treater	N/A	None	N/A	N/A	NOx	0.06	0.26	N/A	N/A	Gas/Vapor	AP-42	N/A
								CO	0.05	0.22					
								VOC	<0.01	0.01					
								SO_2	<0.01	<0.01					
								PM_{10}	<0.01	0.01					
								PM_{Total}	<0.01	0.02					
								n-Hexane	<0.01	<0.01					
								HCHO	<0.01	<0.01					
								Benzene	<0.01	<0.01					
								Toluene	<0.01	<0.01					
								CO_2	58.49	256.18					
								CH_4	<0.01	<0.01					
								N_2O	<0.01	<0.01					
EP-LH1	Upward Vertical Stack	EU-LH1	Line Heater	N/A	None	N/A	N/A	NOx	0.17	0.74	N/A	N/A	Gas/Vapor	AP-42	N/A
								CO	0.14	0.61					
								VOC	0.01	0.04					
								SO_2	<0.01	<0.01					
								PM_{10}	0.01	0.04					
								PM_{Total}	0.01	0.06					
								n-Hexane	<0.01	0.01					
								HCHO	<0.01	<0.01					
								Benzene	<0.01	<0.01					
								Toluene	<0.01	<0.01					
								CO_2	175.47	768.54					
								CH_4	<0.01	0.01					
								N_2O	<0.01	<0.01					

Attachment J
EMISSION POINTS DATA SUMMARY SHEET

Table 1: Emissions Data

Emission Point ID No. *(Must match Emission Units Table & Plot Plan)*	Emission Point Type[1]	Emission Unit Vented Through This Point *(Must match Emission Units Table & Plot Plan)*		Air Pollution Control Device *(Must match Emission Units Table & Plot Plan)*		Vent Time for Emission Unit (chemical processes only)		All Regulated Pollutants - Chemical Name/CAS[3] *(Speciate VOCs & HAPS)*	Maximum Potential Uncontrolled Emissions[4]		Maximum Potential Controlled Emissions[5]		Emission Form or Phase *(At exit conditions, Solid, Liquid or Gas/Vapor)*	Est. Method Used[6]	Emission Concentration[7] (ppmv or mg/m4)
		ID No.	Source	ID No.	Device Type	Short Term[2]	Max (hr/yr)		lb/hr	ton/yr	lb/hr	ton/yr			
EP-LH2	Upward Vertical Stack	EU-LH2	Line Heater	N/A	None	N/A	N/A	NOx	0.17	0.74	N/A	N/A	Gas/Vapor	AP-42	N/A
								CO	0.14	0.61					
								VOC	0.01	0.04					
								SO_2	<0.01	<0.01					
								PM_{10}	0.01	0.04					
								PM_{Total}	0.01	0.06					
								n-Hexane	<0.01	0.01					
								HCHO	<0.01	<0.01					
								Benzene	<0.01	<0.01					
								Toluene	<0.01	<0.01					
								CO_2	175.47	768.54					
								CH_4	<0.01	0.01					
								N_2O	<0.01	<0.01					
APC-COMB-TKLD	Upward Vertical Stack	EU-TANKS-COND, EU-TANKS-PW, EU-LOAD-COND, EU-LOAD-PW, APC-COMB-TKLD, EU-PILOT	Vapor Combustor	-	None	N/A	N/A	NOx	1.11	4.88	1.11	4.88	Gas/Vapor	O (AP-42, Mass Balance)	N/A
								CO	2.21	9.67	2.21	9.67			
								VOC	355.11	1,489.90	6.80	29.78			
								SO_2	<0.01	<0.01	<0.01	<0.01			
								PM_{10}	<0.01	<0.01	<0.01	<0.01			
								PM_{Total}	0.02	0.10	0.02	0.10			
								n-Hexane	18.51	77.66	0.35	1.55			
								HCHO	<0.01	<0.01	<0.01	<0.01			
								Benzene	0.24	1.00	<0.01	0.02			
								Toluene	1.18	4.96	0.02	0.10			
								Ethylbenzene	1.11	4.68	0.02	0.09			
								Xylenes	5.33	22.37	0.10	0.45			
								CO_2	941.11	4,122.06	941.11	4,122.06			
								CH_4	0.24	0.11	0.24	0.11			
								N_2O	<0.01	0.01	<0.01	0.01			

Attachment J
EMISSION POINTS DATA SUMMARY SHEET

Table 1: Emissions Data

Emission Point ID No. *(Must match Emission Units Table & Plot Plan)*	Emission Point Type[1]	Emission Unit Vented Through This Point *(Must match Emission Units Table & Plot Plan)*		Air Pollution Control Device *(Must match Emission Units Table & Plot Plan)*		Vent Time for Emission Unit (chemical processes only)		All Regulated Pollutants - Chemical Name/CAS[3] *(Speciate VOCs & HAPS)*	Maximum Potential Uncontrolled Emissions[4]		Maximum Potential Controlled Emissions[5]		Emission Form or Phase *(At exit conditions, Solid, Liquid or Gas/Vapor)*	Est. Method Used[6]	Emission Concentration[7] (ppmv or mg/m4)
		ID No.	Source	ID No.	Device Type	Short Term[2]	Max (hr/yr)		lb/hr	ton/yr	lb/hr	ton/yr			
EP-FUG	Fugitive	EU-FUG	Fugitive Components	-	None	N/A	N/A	VOC	N/A	2.60	N/A	N/A	Gas/Vapor	AP-42	N/A
								n-Hexane		0.11					
								Benzene		<0.01					
								Toluene		0.01					
								Ethylbenzene		0.01					
								Xylenes		0.03					
								CO_2		0.01					
								CH_4		1.56					
EP-HR	Fugitive	EU-HR	Fugitive Haul Road Emission	-	None	N/A	N/A	PM_{Total}	0.38	1.26	N/A	N/A	Gas/ Vapor	AP-42	N/A
								PM_{10}	0.10	0.30					
								$PM_{2.5}$	0.01	0.03					

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit emissions are not typically considered to be fugitive and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugitive emission activities.

1 Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.

2 Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (ie., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).

3 List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS2, VOCs, H2S, Inorganics, Lead, Organics, O3, NO, NO2, SO2, SO3, all applicable Greenhouse Gases (including CO2 and methane), etc. DO NOT LIST H2, H2O, N2, O2, and Noble Gases.

4 Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

5 Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

6 Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

7 Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmv) are used. If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of milligram per dry cubic meter (mg/m3) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO2, use units of ppmv (See 45CSR10).

Attachment J
EMISSION POINTS DATA SUMMARY SHEET

Table 2: Release Parameter Data								
Emission Point ID No. *(Must match Emission Units Table)*	Inner Diameter (ft.)	Exit Gas			Emission Point Elevation (ft)		UTM Coordinates (km)	
		Temp. (°F)	Volumetric Flow [1] (acfm) *at operating conditions*	Velocity (fps)	Ground Level *(Height above mean sea level)*	Stack Height [2] *(Release height of emissions above ground level)*	Northing	Easting
EP-GPU1	1.0 (est.)	500 (est.)	~992.4	~21.1	~1,144	10.75	4,447.84519	534.66711
EP-GPU2	1.0 (est.)	500 (est.)	~992.4	~21.1	~1,144	10.75	4,447.84519	534.66711
EP-HT1	0.7	450 (est.)	~13,067	~277.3	~1,144	10	4,447.84519	534.66711
EP-LH1	1.0 (est.)	500 (est.)	Unknown	Unknown	~1,144	10 (est.)	4,447.84519	534.66711
EP-LH2	1.0 (est.)	500 (est.)	Unknown	Unknown	~1,144	10 (est.)	4,447.84519	534.66711
EP-TANKS-COND	N/A	Ambient	N/A	N/A	~1,144	20	4,447.84519	534.66711
EP-TANKS-PW	N/A	Ambient	N/A	N/A	~1,144	20	4,447.84519	534.66711
EP-LOAD-COND	N/A	Ambient	N/A	N/A	~1,144	3 (est.)	4,447.84519	534.66711

Emission Point ID No. *(Must match Emission Units Table)*	Inner Diameter (ft.)	Exit Gas			Emission Point Elevation (ft)		UTM Coordinates (km)	
		Temp. (°F)	Volumetric Flow [1] (acfm) *at operating conditions*	Velocity (fps)	Ground Level *(Height above mean sea level)*	Stack Height [2] *(Release height of emissions above ground level)*	Northing	Easting
EP-LOAD-PW	N/A	Ambient	N/A	N/A	~1,144	3 (est.)	4,447.84519	534.66711
APC-COMB-TKLD	4.0	1,000 (est.)	Unknown	Unknown	~1,144	25	4,447.84519	534.66711
EP-PILOT	N/A	N/A	Unknown	Unknown	~1,144	N/A	4,447.84519	534.66711
EP-FUG	N/A	Ambient	N/A	N/A	~1,144	N/A	4,447.84519	534.66711
EP-HR	N/A	Ambient	N/A	N/A	~1,144	N/A	4,447.84519	534.66711
Note: In lieu of equipment UTM coordinates, site UTM coordinates provided								

[1] Give at operating conditions. Include inerts.
[2] Release height of emissions above ground level.

Notes:

****Stack parameters for heater treaters and line heaters are estimated based on typical equipment configurations but may vary.***

ATTACHMENT K: FUGITIVE EMISSIONS DATA SUMMARY SHEET

Attachment K

FUGITIVE EMISSIONS DATA SUMMARY SHEET

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not typically considered to be fugitive, and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET.

Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS
1.) Will there be haul road activities? ☒ Yes ☐ No ☒ If YES, then complete the HAUL ROAD EMISSIONS UNIT DATA SHEET.
2.) Will there be Storage Piles? ☐ Yes ☒ No ☐ If YES, complete Table 1 of the NONMETALLIC MINERALS PROCESSING EMISSIONS UNIT DATA SHEET.
3.) Will there be Liquid Loading/Unloading Operations? ☒ Yes ☐ No ☒ If YES, complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET.
4.) Will there be emissions of air pollutants from Wastewater Treatment Evaporation? ☐ Yes ☒ No ☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
5.) Will there be Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, open-ended valves, sampling connections, flanges, agitators, cooling towers, etc.)? ☒ Yes ☐ No ☒ If YES, complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS UNIT DATA SHEET.
6.) Will there be General Clean-up VOC Operations? ☐ Yes ☒ No ☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
7.) Will there be any other activities that generate fugitive emissions? ☐ Yes ☒ No ☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form.
If you answered "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions Summary."

Fugitive Emissions Summary	All Regulated Pollutants - Chemical Name/CAS[1]	Maximum Potential Uncontrolled Emissions[2]		Maximum Potential Controlled Emissions[3]		Est. Method Used[4]
		lb/hr	ton/yr	lb/hr	ton/yr	
Haul Road/Road Dust Emissions Paved Haul Roads						
Unpaved Haul Roads	PM Total PM_{10} $PM_{2.5}$	0.38 0.10 0.01	1.26 0.30 0.03	N/A	N/A	O - AP-42 13.2.2
Storage Pile Emissions						
Loading/Unloading Operations - Condensate	VOC n-Hexane Benzene Toluene Ethylbenzene Xylenes Carbon Dioxide Methane	Does Not Apply	2.79 0.15 <0.01 0.01 0.01 0.04 <0.01 0.02	Does Not Apply	0.84 0.04 <0.01 <0.01 <0.01 0.01 <0.01 0.01	O – AP-42 5.2-4 / API 5-12
Loading/Unloading Operations - Produced Water	VOC n-Hexane Benzene Toluene Ethylbenzene Xylenes Carbon Dioxide Methane	Does Not Apply	0.05 <0.01 <0.01 <0.01 <0.01 <0.01 <0.01 0.01	Does Not Apply	0.02 <0.01 <0.01 <0.01 <0.01 <0.01 <0.01 <0.01	O – AP-42 5.2-4 / API 5-12
Wastewater Treatment Evaporation & Operations						

Fugitive Emissions Summary	All Regulated Pollutants - Chemical Name/CAS[1]	Maximum Potential Uncontrolled Emissions[2]		Maximum Potential Controlled Emissions[3]		Est. Method Used[4]
		lb/hr	ton/yr	lb/hr	ton/yr	
Equipment Leaks	VOC n-Hexane Benzene Toluene Ethylbenzene Xylenes Carbon Dioxide Methane	Does Not Apply	2.60 0.11 <0.01 0.01 0.01 0.03 0.01 1.56	Does Not Apply	N/A	O – EPA-453/R-95-017
General Clean-up VOC Emissions						
Other						

[1] List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS_2, VOCs, H_2S, Inorganics, Lead, Organics, O_3, NO, NO_2, SO_2, SO_3, all applicable Greenhouse Gases (including CO_2 and methane), etc. DO NOT LIST H_2, H_2O, N_2, O_2, and Noble Gases.

[2] Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

[3] Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

[4] Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

Note: Greenhouse Gas (GHG) emissions were calculated using EPA Mandatory Reporting Rule and 2009 API Compendium guidance. With the exception of fugitive emissions (which are calculated by mass balance), emissions calculation methodologies are intended to calculate metric tons (tonnes) for the purposes of emissions reporting to EPA. These values were converted to tons for consistency with other pollutants.

ATTACHMENT L: EMISSION UNIT DATA SHEETS

EUDS – Storage Tanks: Condensate

EUDS – Storage Tanks: Produced Water

EUDS – Bulk Liquid Transfer Operations: Condensate

EUDS – Bulk Liquid Transfer Operations: Produced Water

EUDS – Chemical Process Leak Sources

EUDS – Fugitive Emissions from Unpaved Haulroads

Attachment L
EMISSIONS UNIT DATA SHEET
STORAGE TANKS

Provide the following information for each new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT www.epa.gov/tnn/tanks.html), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (http://www.epa.gov/tnn/chief/).

I. GENERAL INFORMATION (required)

1. Bulk Storage Area Name Condensate Storage	2. Tank Name Six (6) 400-bbl Condensate Storage Tanks
3. Tank Equipment Identification No. (as assigned on *Equipment List Form*) EU-TANKS-COND	4. Emission Point Identification No. (as assigned on *Equipment List Form*) EP-TANKS-COND
5. Date of Commencement of Construction (for existing tanks) 2013	
6. Type of change ☐ New Construction ☐ New Stored Material ☒ Other Tank Modification	
7. Description of Tank Modification (if applicable) Change in throughput and emissions based on new process simulation and analysis.	
7A. Does the tank have more than one mode of operation? (e.g. Is there more than one product stored in the tank?) ☐ Yes ☒ No	
7B. If YES, explain and identify which mode is covered by this application (Note: A separate form must be completed for each mode).	
7C. Provide any limitations on source operation affecting emissions, any work practice standards (e.g. production variation, etc.): Not applicable	

II. TANK INFORMATION (required)

8. Design Capacity (specify barrels or gallons). Use the internal cross-sectional area multiplied by internal height. 400 barrels (per tank)	
9A. Tank Internal Diameter (ft) 12	9B. Tank Internal Height (or Length) (ft) 20
10A. Maximum Liquid Height (ft) 19	10B. Average Liquid Height (ft) 10
11A. Maximum Vapor Space Height (ft) 20	11B. Average Vapor Space Height (ft) 10
12. Nominal Capacity (specify barrels or gallons). This is also known as "working volume" and considers design liquid levels and overflow valve heights. 16,074.56 gallons (per EPA TANKS 4.0.9d)	

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13A. Maximum annual throughput (gal/yr) 2,759,400 (Total for all tanks)	13B. Maximum daily throughput (gal/day) 7,560 (Total for all tanks) *Rolling daily throughput total not to exceed maximum annual throughput.
14. Number of Turnovers per year (annual net throughput/maximum tank liquid volume) 171.66 (Total for all tanks, per EPA TANKS 4.0.9d)	
15. Maximum tank fill rate (gal/min) Unknown	
16. Tank fill method ☐ Submerged ☒ Splash ☐ Bottom Loading	
17. Complete 17A and 17B for Variable Vapor Space Tank Systems ☒ Does Not Apply	
17A. Volume Expansion Capacity of System (gal)	17B. Number of transfers into system per year
18. Type of tank (check all that apply): ☒ Fixed Roof ☒ vertical ___ horizontal ___ flat roof ☒ cone roof ___ dome roof ___ other (describe) ☐ External Floating Roof ___ pontoon roof ___ double deck roof ☐ Domed External (or Covered) Floating Roof ☐ Internal Floating Roof ___ vertical column support ___ self-supporting ☐ Variable Vapor Space ___ lifter roof ___ diaphragm ☐ Pressurized ___ spherical ___ cylindrical ☐ Underground ☐ Other (describe)	

III. TANK CONSTRUCTION & OPERATION INFORMATION (optional if providing TANKS Summary Sheets)
Refer to enclosed TANKS Summary Sheet.

19. Tank Shell Construction: ☐ Riveted ☐ Gunite lined ☐ Epoxy-coated rivets ☐ Other (describe)		
20A. Shell Color	20B. Roof Color	20C. Year Last Painted
21. Shell Condition (if metal and unlined): ☐ No Rust ☐ Light Rust ☐ Dense Rust ☐ Not applicable		
22A. Is the tank heated? ☐ YES ☐ NO		
22B. If YES, provide the operating temperature (°F)		
22C. If YES, please describe how heat is provided to tank.		
23. Operating Pressure Range (psig):		
24. Complete the following section for **Vertical Fixed Roof Tanks** ☐ Does Not Apply		
24A. For dome roof, provide roof radius (ft)		
24B. For cone roof, provide slope (ft/ft)		
25. Complete the following section for **Floating Roof Tanks** ☐ Does Not Apply		
25A. Year Internal Floaters Installed:		
25B. Primary Seal Type: (check one)	☐ Metallic (Mechanical) Shoe Seal ☐ Vapor Mounted Resilient Seal	☐ Liquid Mounted Resilient Seal ☐ Other (describe):
25C. Is the Floating Roof equipped with a Secondary Seal? ☐ YES ☐ NO		

25D. If YES, how is the secondary seal mounted? (check one) ☐ Shoe ☐ Rim ☐ Other (describe):		
25E. Is the Floating Roof equipped with a weather shield? ☐ YES ☐ NO		
25F. Describe deck fittings; indicate the number of each type of fitting:		
ACCESS HATCH		
BOLT COVER, GASKETED:	UNBOLTED COVER, GASKETED:	UNBOLTED COVER, UNGASKETED:
AUTOMATIC GAUGE FLOAT WELL		
BOLT COVER, GASKETED:	UNBOLTED COVER, GASKETED:	UNBOLTED COVER, UNGASKETED:
COLUMN WELL		
BUILT-UP COLUMN – SLIDING COVER, GASKETED:	BUILT-UP COLUMN – SLIDING COVER, UNGASKETED:	PIPE COLUMN – FLEXIBLE FABRIC SLEEVE SEAL:
LADDER WELL		
PIP COLUMN – SLIDING COVER, GASKETED:	PIPE COLUMN – SLIDING COVER, UNGASKETED:	
GAUGE-HATCH/SAMPLE PORT		
SLIDING COVER, GASKETED:	SLIDING COVER, UNGASKETED:	
ROOF LEG OR HANGER WELL		
WEIGHTED MECHANICAL ACTUATION, GASKETED:	WEIGHTED MECHANICAL ACTUATION, UNGASKETED:	SAMPLE WELL-SLIT FABRIC SEAL (10% OPEN AREA)
VACUUM BREAKER		
WEIGHTED MECHANICAL ACTUATION, GASKETED:	WEIGHTED MECHANICAL ACTUATION, UNGASKETED:	
RIM VENT		
WEIGHTED MECHANICAL ACTUATION GASKETED:	WEIGHTED MECHANICAL ACTUATION, UNGASKETED:	
DECK DRAIN (3-INCH DIAMETER)		
OPEN:	90% CLOSED:	
STUB DRAIN		
1-INCH DIAMETER:		
OTHER (DESCRIBE, ATTACH ADDITIONAL PAGES IF NECESSARY)		

26. Complete the following section for Internal Floating Roof Tanks ☐ Does Not Apply	
26A. Deck Type: ☐ Bolted ☐ Welded	
26B. For Bolted decks, provide deck construction:	
26C. Deck seam: ☐ Continuous sheet construction 5 feet wide ☐ Continuous sheet construction 6 feet wide ☐ Continuous sheet construction 7 feet wide ☐ Continuous sheet construction 5 × 7.5 feet wide ☐ Continuous sheet construction 5 × 12 feet wide ☐ Other (describe)	
26D. Deck seam length (ft)	26E. Area of deck (ft^2)
For column supported tanks: 26F. Number of columns:	26G. Diameter of each column:

IV. SITE INFORMANTION (optional if providing TANKS Summary Sheets)

27. Provide the city and state on which the data in this section are based. **Refer to enclosed TANKS Summary Sheet.**
28. Daily Average Ambient Temperature (°F)
29. Annual Average Maximum Temperature (°F)
30. Annual Average Minimum Temperature (°F)
31. Average Wind Speed (miles/hr)
32. Annual Average Solar Insulation Factor (BTU/(ft^2·day))
33. Atmospheric Pressure (psia)

V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)

34. Average daily temperature range of bulk liquid: **Refer to enclosed TANKS Summary Sheet.**	
34A. Minimum (°F)	34B. Maximum (°F)
35. Average operating pressure range of tank:	
35A. Minimum (psig)	35B. Maximum (psig)
36A. Minimum Liquid Surface Temperature (°F)	36B. Corresponding Vapor Pressure (psia)
37A. Average Liquid Surface Temperature (°F)	37B. Corresponding Vapor Pressure (psia)
38A. Maximum Liquid Surface Temperature (°F)	38B. Corresponding Vapor Pressure (psia)

39. Provide the following for <u>each</u> liquid or gas to be stored in tank. Add additional pages if necessary.

39A. Material Name or Composition			
39B. CAS Number			
39C. Liquid Density (lb/gal)			
39D. Liquid Molecular Weight (lb/lb-mole)			
39E. Vapor Molecular Weight (lb/lb-mole)			

Maximum Vapor Pressure 39F. True (psia) 39G. Reid (psia)			
Months Storage per Year 39H. From 39I. To			

VI. EMISSIONS AND CONTROL DEVICE DATA (required)

40. Emission Control Devices (check as many as apply): ☐ Does Not Apply

- ☐ Carbon Adsorption[1]
- ☐ Condenser[1]
- ☐ Conservation Vent (psig)
  - Vacuum Setting Pressure Setting
- ☐ Emergency Relief Valve (psig)
- ☐ Inert Gas Blanket of
- ☐ Insulation of Tank with
- ☐ Liquid Absorption (scrubber)[1]
- ☐ Refrigeration of Tank
- ☐ Rupture Disc (psig)
- ☐ Vent to Incinerator[1]
- ☒ Other[1] (describe): Vapor Combustor

[1] Complete appropriate Air Pollution Control Device Sheet.

41. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application).

Material Name & CAS No.	Breathing Loss (lb/hr)	Working Loss		Annual Loss (lb/yr)	Estimation Method[1]
		Amount	Units		
Refer to Attachment N Emissions Calculations and enclosed TANKS Summary Sheet.					

[1] EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)

☒ Remember to attach emissions calculations, including TANKS Summary Sheets if applicable.

Attachment L
EMISSIONS UNIT DATA SHEET
STORAGE TANKS

Provide the following information for each new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT www.epa.gov/tnn/tanks.html), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (http://www.epa.gov/tnn/chief/).

I. GENERAL INFORMATION (required)

1. Bulk Storage Area Name Produced Water Storage	2. Tank Name Six (6) 400-bbl Produced Water Storage Tanks
3. Tank Equipment Identification No. (as assigned on *Equipment List Form*) EU-TANKS-PW	4. Emission Point Identification No. (as assigned on *Equipment List Form*) EP-TANKS-PW
5. Date of Commencement of Construction (for existing tanks) 2013	
6. Type of change ☐ New Construction ☐ New Stored Material ☒ Other Tank Modification	
7. Description of Tank Modification (if applicable) Change in throughput and emissions based on new process simulation and analysis..	
7A. Does the tank have more than one mode of operation? (e.g. Is there more than one product stored in the tank?) ☐ Yes ☒ No	
7B. If YES, explain and identify which mode is covered by this application (Note: A separate form must be completed for each mode).	
7C. Provide any limitations on source operation affecting emissions, any work practice standards (e.g. production variation, etc.): Not applicable	

II. TANK INFORMATION (required)

8. Design Capacity (specify barrels or gallons). Use the internal cross-sectional area multiplied by internal height. 400 barrels (per tank)	
9A. Tank Internal Diameter (ft) 12	9B. Tank Internal Height (or Length) (ft) 20
10A. Maximum Liquid Height (ft) 19	10B. Average Liquid Height (ft) 10
11A. Maximum Vapor Space Height (ft) 20	11B. Average Vapor Space Height (ft) 10
12. Nominal Capacity (specify barrels or gallons). This is also known as "working volume" and considers design liquid levels and overflow valve heights. 16,074.56 gallons (per EPA TANKS 4.0.9d)	

13A. Maximum annual throughput (gal/yr) 1,533,000 (Total for all tanks)	13B. Maximum daily throughput (gal/day) 4,200 (Total for all tanks) *Rolling daily throughput total not to exceed maximum annual throughput.

14. Number of Turnovers per year (annual net throughput/maximum tank liquid volume) 95.37 (Total for all tanks, per EPA TANKS 4.0.9d)

15. Maximum tank fill rate (gal/min) Unknown

16. Tank fill method ☐ Submerged ☒ Splash ☐ Bottom Loading

17. Complete 17A and 17B for Variable Vapor Space Tank Systems ☒ Does Not Apply

17A. Volume Expansion Capacity of System (gal)	17B. Number of transfers into system per year

18. Type of tank (check all that apply):
☒ Fixed Roof ☒ vertical ___ horizontal ___ flat roof ☒ cone roof ___ dome roof
___ other (describe)
☐ External Floating Roof ___ pontoon roof ___ double deck roof
☐ Domed External (or Covered) Floating Roof
☐ Internal Floating Roof ___ vertical column support ___ self-supporting
☐ Variable Vapor Space ___ lifter roof ___ diaphragm
☐ Pressurized ___ spherical ___ cylindrical
☐ Underground
☐ Other (describe)

III. TANK CONSTRUCTION & OPERATION INFORMATION (optional if providing TANKS Summary Sheets)
Refer to enclosed TANKS Summary Sheet.

19. Tank Shell Construction:
☐ Riveted ☐ Gunite lined ☐ Epoxy-coated rivets ☐ Other (describe)

20A. Shell Color	20B. Roof Color	20C. Year Last Painted

21. Shell Condition (if metal and unlined):
☐ No Rust ☐ Light Rust ☐ Dense Rust ☐ Not applicable

22A. Is the tank heated? ☐ YES ☐ NO

22B. If YES, provide the operating temperature (°F)

22C. If YES, please describe how heat is provided to tank.

23. Operating Pressure Range (psig):

24. Complete the following section for **Vertical Fixed Roof Tanks** ☐ Does Not Apply

24A. For dome roof, provide roof radius (ft)

24B. For cone roof, provide slope (ft/ft)

25. Complete the following section for **Floating Roof Tanks** ☐ Does Not Apply

25A. Year Internal Floaters Installed:

25B. Primary Seal Type: (check one)
☐ Metallic (Mechanical) Shoe Seal ☐ Liquid Mounted Resilient Seal
☐ Vapor Mounted Resilient Seal ☐ Other (describe):

25C. Is the Floating Roof equipped with a Secondary Seal? ☐ YES ☐ NO

25D. If YES, how is the secondary seal mounted? (check one) ☐ Shoe ☐ Rim ☐ Other (describe):			
25E. Is the Floating Roof equipped with a weather shield? ☐ YES ☐ NO			
25F. Describe deck fittings; indicate the number of each type of fitting:			
ACCESS HATCH			
BOLT COVER, GASKETED:	UNBOLTED COVER, GASKETED:	UNBOLTED COVER, UNGASKETED:	
AUTOMATIC GAUGE FLOAT WELL			
BOLT COVER, GASKETED:	UNBOLTED COVER, GASKETED:	UNBOLTED COVER, UNGASKETED:	
COLUMN WELL			
BUILT-UP COLUMN – SLIDING COVER, GASKETED:	BUILT-UP COLUMN – SLIDING COVER, UNGASKETED:	PIPE COLUMN – FLEXIBLE FABRIC SLEEVE SEAL:	
LADDER WELL			
PIP COLUMN – SLIDING COVER, GASKETED:	PIPE COLUMN – SLIDING COVER, UNGASKETED:		
GAUGE-HATCH/SAMPLE PORT			
SLIDING COVER, GASKETED:	SLIDING COVER, UNGASKETED:		
ROOF LEG OR HANGER WELL			
WEIGHTED MECHANICAL ACTUATION, GASKETED:	WEIGHTED MECHANICAL ACTUATION, UNGASKETED:	SAMPLE WELL-SLIT FABRIC SEAL (10% OPEN AREA)	
VACUUM BREAKER			
WEIGHTED MECHANICAL ACTUATION, GASKETED:	WEIGHTED MECHANICAL ACTUATION, UNGASKETED:		
RIM VENT			
WEIGHTED MECHANICAL ACTUATION GASKETED:	WEIGHTED MECHANICAL ACTUATION, UNGASKETED:		
DECK DRAIN (3-INCH DIAMETER)			
OPEN:	90% CLOSED:		
STUB DRAIN			
1-INCH DIAMETER:			
OTHER (DESCRIBE, ATTACH ADDITIONAL PAGES IF NECESSARY)			

26. Complete the following section for Internal Floating Roof Tanks ☐ Does Not Apply	
26A. Deck Type: ☐ Bolted ☐ Welded	
26B. For Bolted decks, provide deck construction:	
26C. Deck seam: ☐ Continuous sheet construction 5 feet wide ☐ Continuous sheet construction 6 feet wide ☐ Continuous sheet construction 7 feet wide ☐ Continuous sheet construction 5 × 7.5 feet wide ☐ Continuous sheet construction 5 × 12 feet wide ☐ Other (describe)	
26D. Deck seam length (ft)	26E. Area of deck (ft^2)
For column supported tanks: 26F. Number of columns:	26G. Diameter of each column:

IV. SITE INFORMANTION (optional if providing TANKS Summary Sheets)

27. Provide the city and state on which the data in this section are based. **Refer to enclosed TANKS Summary Sheet.**
28. Daily Average Ambient Temperature (°F)
29. Annual Average Maximum Temperature (°F)
30. Annual Average Minimum Temperature (°F)
31. Average Wind Speed (miles/hr)
32. Annual Average Solar Insulation Factor (BTU/(ft^2·day))
33. Atmospheric Pressure (psia)

V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)

34. Average daily temperature range of bulk liquid: **Refer to enclosed TANKS Summary Sheet.**	
34A. Minimum (°F)	34B. Maximum (°F)
35. Average operating pressure range of tank:	
35A. Minimum (psig)	35B. Maximum (psig)
36A. Minimum Liquid Surface Temperature (°F)	36B. Corresponding Vapor Pressure (psia)
37A. Average Liquid Surface Temperature (°F)	37B. Corresponding Vapor Pressure (psia)
38A. Maximum Liquid Surface Temperature (°F)	38B. Corresponding Vapor Pressure (psia)

39. Provide the following for each liquid or gas to be stored in tank. Add additional pages if necessary.

39A. Material Name or Composition			
39B. CAS Number			
39C. Liquid Density (lb/gal)			
39D. Liquid Molecular Weight (lb/lb-mole)			
39E. Vapor Molecular Weight (lb/lb-mole)			

Maximum Vapor Pressure 39F. True (psia) 39G. Reid (psia)			
Months Storage per Year 39H. From 39I. To			

VI. EMISSIONS AND CONTROL DEVICE DATA (required)

40. Emission Control Devices (check as many as apply): ☐ Does Not Apply

- ☐ Carbon Adsorption[1]
- ☐ Condenser[1]
- ☐ Conservation Vent (psig)
  - Vacuum Setting Pressure Setting
- ☐ Emergency Relief Valve (psig)
- ☐ Inert Gas Blanket of
- ☐ Insulation of Tank with
- ☐ Liquid Absorption (scrubber)[1]
- ☐ Refrigeration of Tank
- ☐ Rupture Disc (psig)
- ☐ Vent to Incinerator[1]
- ☒ Other[1] (describe): Vapor Combustor

[1] Complete appropriate Air Pollution Control Device Sheet.

41. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application).

Material Name & CAS No.	Breathing Loss (lb/hr)	Working Loss		Annual Loss (lb/yr)	Estimation Method[1]
		Amount	Units		
Refer to Attachment N Emissions Calculations and enclosed TANKS Summary Sheet.					

[1] EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)

☒ Remember to attach emissions calculations, including TANKS Summary Sheets if applicable.

Attachment L
EMISSIONS UNIT DATA SHEET
BULK LIQUID TRANSFER OPERATIONS

Furnish the following information for each new or modified bulk liquid transfer area or loading rack, as shown on the *Equipment List Form* and other parts of this application. This form is to be used for bulk liquid transfer operations such as to and from drums, marine vessels, rail tank cars, and tank trucks.

Identification Number (as assigned on *Equipment List Form*): EU-LOAD-COND

1. Loading Area Name: Condensate Truck Loading

2. Type of cargo vessels accommodated at this rack or transfer point (check as many as apply):
☐ Drums ☐ Marine Vessels ☐ Rail Tank Cars ☒ Tank Trucks

3. Loading Rack or Transfer Point Data:

Number of pumps	One (1)
Number of liquids loaded	One (1)
Maximum number of marine vessels, tank trucks, tank cars, and/or drums loading at one time	One (1)

4. Does ballasting of marine vessels occur at this loading area?
☐ Yes ☐ No ☒ Does not apply

5. Describe cleaning location, compounds and procedure for cargo vessels using this transfer point:

Point is kept clear. Scotches are provided. Lines kept in good working order and tested periodically.

6. Are cargo vessels pressure tested for leaks at this or any other location?
☒ Yes ☐ No

If YES, describe:

Vessel pressure tested in accordance with DOT requirements, if applicable.

7. Projected Maximum Operating Schedule (for rack or transfer point as a whole):				
Maximum	Jan. - Mar.	Apr. - June	July - Sept.	Oct. - Dec.
hours/day	24	24	24	24
days/week	5	5	5	5
weeks/quarter	13	13	13	13

8. Bulk Liquid Data *(add pages as necessary):*		
Pump ID No.		N/A
Liquid Name		Condensate
Max. daily throughput (1000 gal/day)		~7.56
Max. annual throughput (1000 gal/yr)		2,759.4
Loading Method [1]		SUB
Max. Fill Rate (gal/min)		125
Average Fill Time (min/loading)		~60
Max. Bulk Liquid Temperature (°F)		50.33
True Vapor Pressure [2]		5.9008
Cargo Vessel Condition [3]		U
Control Equipment or Method [4]		O = Vapor Return w/ Combustion Controls
Minimum control efficiency (%)		70% Capture / 98% Combustion / 69% Overall
Maximum Emission Rate	Loading (lb/hr)	4.55
	Annual (lb/yr)	1,680 (based on 0.84 tons/year)
Estimation Method [5]		EPA

[1] BF = Bottom Fill SP = Splash Fill SUB = Submerged Fill
[2] At maximum bulk liquid temperature
[3] B = Ballasted Vessel, C = Cleaned, U = Uncleaned (dedicated service), O = other (describe)
[4] List as many as apply (complete and submit appropriate *Air Pollution Control Device Sheets*):CA = Carbon Adsorption LOA = Lean Oil AdsorptionCO = Condensation SC = Scrubber (Absorption)CRA = Compressor-Refrigeration-Absorption TO = Thermal Oxidation or Incineration CRC = Compression-Refrigeration-Condensation VB = Dedicated Vapor Balance (closed system) O = other (descibe)
[5] EPA = EPA Emission Factor as stated in AP-42 MB = Material Balance TM = Test Measurement based upon test data submittal O = other (describe)

9. **Proposed Monitoring, Recordkeeping, Reporting, and Testing** Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.	
MONITORING As currently permitted	RECORDKEEPING As currently permitted
REPORTING As currently permitted	TESTING As currently permitted

MONITORING. PLEASE LIST AND DESCRIBE THE PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OPERATION OF THIS PROCESS EQUIPMENT OPERATION/AIR POLLUTION CONTROL DEVICE.
RECORDKEEPING. PLEASE DESCRIBE THE PROPOSED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.
REPORTING. PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORDKEEPING.
TESTING. PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR POLLUTION CONTROL DEVICE.

10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty Not applicable

Attachment L
EMISSIONS UNIT DATA SHEET
BULK LIQUID TRANSFER OPERATIONS

Furnish the following information for each new or modified bulk liquid transfer area or loading rack, as shown on the *Equipment List Form* and other parts of this application. This form is to be used for bulk liquid transfer operations such as to and from drums, marine vessels, rail tank cars, and tank trucks.

Identification Number (as assigned on *Equipment List Form*): EU-LOAD-PW

1. Loading Area Name: Produced Water Truck Loading

2. Type of cargo vessels accommodated at this rack or transfer point (check as many as apply):
☐ Drums ☐ Marine Vessels ☐ Rail Tank Cars ☒ Tank Trucks

3. Loading Rack or Transfer Point Data:

Number of pumps	One (1)
Number of liquids loaded	One (1)
Maximum number of marine vessels, tank trucks, tank cars, and/or drums loading at one time	One (1)

4. Does ballasting of marine vessels occur at this loading area?
☐ Yes ☐ No ☒ Does not apply

5. Describe cleaning location, compounds and procedure for cargo vessels using this transfer point:

Point is kept clear. Scotches are provided. Lines kept in good working order and tested periodically.

6. Are cargo vessels pressure tested for leaks at this or any other location?
☒ Yes ☐ No

If YES, describe:

Vessel pressure tested in accordance with DOT requirements, if applicable.

7. Projected Maximum Operating Schedule (for rack or transfer point as a whole):				
Maximum	Jan. - Mar.	Apr. - June	July - Sept.	Oct. - Dec.
hours/day	24	24	24	24
days/week	5	5	5	5
weeks/quarter	13	13	13	13

8. Bulk Liquid Data *(add pages as necessary):*		
Pump ID No.		N/A
Liquid Name		Produced Water
Max. daily throughput (1000 gal/day)		~4.2
Max. annual throughput (1000 gal/yr)		1,533.0
Loading Method [1]		SUB
Max. Fill Rate (gal/min)		125
Average Fill Time (min/loading)		~60
Max. Bulk Liquid Temperature (°F)		50.33
True Vapor Pressure [2]		0.2368
Cargo Vessel Condition [3]		U
Control Equipment or Method [4]		O = Vapor Return w/ Combustion Controls
Minimum control efficiency (%)		70% Capture / 98% Combustion / 69% Overall
Maximum Emission Rate	Loading (lb/hr)	0.14
	Annual (lb/yr)	40 (based on 0.02 tons/year)
Estimation Method [5]		EPA

[1] BF = Bottom Fill SP = Splash Fill SUB = Submerged Fill
[2] At maximum bulk liquid temperature
[3] B = Ballasted Vessel, C = Cleaned, U = Uncleaned (dedicated service), O = other (describe)
[4] List as many as apply (complete and submit appropriate *Air Pollution Control Device Sheets*):CA = Carbon Adsorption LOA = Lean Oil AdsorptionCO = Condensation SC = Scrubber (Absorption)CRA = Compressor-Refrigeration-Absorption TO = Thermal Oxidation or Incineration CRC = Compression-Refrigeration-Condensation VB = Dedicated Vapor Balance (closed system) O = other (descibe)
[5] EPA = EPA Emission Factor as stated in AP-42 MB = Material Balance TM = Test Measurement based upon test data submittal O = other (describe)

9. **Proposed Monitoring, Recordkeeping, Reporting, and Testing** Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.	
MONITORING As currently permitted	RECORDKEEPING As currently permitted
REPORTING As currently permitted	TESTING As currently permitted
MONITORING. PLEASE LIST AND DESCRIBE THE PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OPERATION OF THIS PROCESS EQUIPMENT OPERATION/AIR POLLUTION CONTROL DEVICE.	
RECORDKEEPING. PLEASE DESCRIBE THE PROPOSED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.	
REPORTING. PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORDKEEPING.	
TESTING. PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR POLLUTION CONTROL DEVICE.	

10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty Not applicable

Attachment L
EMISSIONS UNIT DATA SHEET
CHEMICAL PROCESS

For chemical processes please fill out this sheet and all supplementary forms (see below) that apply. Please check all supplementary forms that have been completed.

- ☐ *Emergency Vent Summary Sheet*
- ☒ *Leak Sources Data Sheet*
- ☐ *Toxicology Data Sheet*
- ☐ *Reactor Data Sheet*
- ☐ *Distillation Column Data Sheet*

1. Chemical process area name and equipment ID number (as shown in *Equipment List Form*)
   Components in natural gas and light liquid service (EU-FUG)

2. Standard Industrial Classification Codes (SICs) for process(es)
   1311

3. List raw materials and ☒ attach MSDSs
   Natural gas and condensate

4. List Products and Maximum Production and ☐ attach MSDSs

Description and CAS Number	Maximum Hourly (lb/hr)	Maximum Annual (ton/year)
Not applicable		

5. Complete the *Emergency Vent Summary Sheet* for all emergency relief devices.

6. Complete the *Leak Source Data Sheet* and describe below or attach to application the leak detection or maintenance program to minimize fugitive emissions. Include detection instruments, calibration gases or methods, planned inspection frequency, and record-keeping, and similar pertinent information. If subject to a rule requirement (e.g. 40CFR60, Subpart VV), please list those here.

   The facility is not a natural gas processing plant (SIC 1321) and is therefore not subject to New Source Performance Standards (NSPS) Subpart KKK or Subpart OOOO requirements for a leak detection and repair (LDAR) monitoring program.

7. Clearly describe below or attach to application Accident Procedures to be followed in the event of an accidental spill or release.

   In the event of an accidental spill or release, personnel will be protected, emergency response personnel will be notified and immediate steps to stop the spill or release will be implemented.

8A. Complete the *Toxicology Data Sheet* or attach to application a toxicology report (an up-to-date material safety data sheets (MSDS) may be used) outlining the currently known acute and chronic health effects of each compound or chemical entity emitted to the air. If these compounds have already been listed in Item 3, then a duplicate MSDS sheet is not required. Include data such as the OSHA time weighted average (TWA) or mutagenicity, teratogenicity, irritation, and other known or suspected effects should be addressed. Indicate where these are unknown, and provide references.

8B. Describe any health effects testing or epidemiological studies on these compounds that are being or may be conducted by the company or required under TSCA, RCRA or other federal regulations. Discuss the persistence in the environment of any emission (e.g. pesticides, etc.).

9. **Waste Products** - Waste products status: (If source is subject to RCRA or 45CSR25, please contact the Hazardous Waste Section of WVDEP, OAQ at (304) 926-3647.)

9A. Types and amounts of wastes to be disposed:

9B. Method of disposal and location of waste disposal facilities:

Carrier: Phone:

9C. Check here if approved USEPA/State Hazardous Waste Landfill will be used ☐

10. Maximum and Projected Typical Operating Schedule for process or project as a whole (circle appropriate units).

circle units:	(hrs/day) (hr/batch)	(days), (batches/day), (batches/week)	(days/yr), (weeks/year)
10A. Maximum			
10B. Typical			

11. Complete a *Reactor Data Sheet* for each reactor in this chemical process.

12. Complete a *Distillation Column Data Sheet* for each distillation column in this chemical process.

13. **Proposed Monitoring, Recordkeeping, Reporting, and Testing**
Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

MONITORING	RECORDKEEPING
As currently permitted	As currently permitted
REPORTING	**TESTING**
As currently permitted	As currently permitted

MONITORING. Please list and describe the process parameters and ranges that are proposed to be monitored in order to demonstrate compliance with the operation of this process equipment operation or air pollution control device.

RECORDKEEPING. Please describe the proposed recordkeeping that will accompany the monitoring.

REPORTING. Please describe the proposed frequency of reporting of the recordkeeping.

TESTING. Please describe any proposed emissions testing for this process equipment or air pollution control device.

14. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty

Not applicable

Source Category	Pollutant	Number of Source Components[1]	Number of Components Monitored by Frequency[2]	Average Time to Repair (days)[3]	Estimated Annual Emission Rate (lb/yr)[4]
Pumps[5]	light liquid VOC[6,7]	0	N/A	N/A	0
	heavy liquid VOC[8]				
	Non-VOC[9]				
Valves[10]	Gas VOC	32	N/A	N/A	780
	Light Liquid VOC	61	N/A	N/A	2,840
	Heavy Liquid VOC				
	Non-VOC				
Safety Relief Valves[11]	Gas VOC	16	N/A	N/A	760
	Non VOC				
Open-ended Lines[12]	VOC	0	N/A	N/A	0
	Non-VOC				
Sampling Connections[13]	VOC				
	Non-VOC				
Compressors	VOC	0	N/A	N/A	0
	Non-VOC				
Flanges	VOC	133 (Gas), 238 (LL)	N/A	N/A	280 (Gas), 480 (LL)
	Non-VOC				
Other	VOC	0	N/A	N/A	0
	Non-VOC				

[1-13] See notes on the following page.

Note: Component counts taken by equipment type at representative facility and made site-specific according to the number of each equipment type at this site.

Notes for Leak Source Data Sheet

1. For VOC sources include components on streams and equipment that contain greater than 10% w/w VOC, including feed streams, reaction/separation facilities, and product/by-product delivery lines. Do not include certain leakless equipment as defined below by category.

2. By monitoring frequency, give the number of sources routinely monitored for leaks, using a portable detection device that measures concentration in ppm. Do not include monitoring by visual or soap-bubble leak detection methods. "M/Q(M)/Q/SA/A/O" means the time period between inspections as follows:

   Monthly/Quarterly, with Monthly follow-up of repaired leakers/Quarterly/Semi-annual/Annually/Other (specify time period)

   If source category is not monitored, a single zero in the space will suffice. For example, if 50 gas-service valves are monitored quarterly, with monthly follow-up of those repaired, 75 are monitored semi-annually, and 50 are checked bimonthly (alternate months), with non checked at any other frequency, you would put in the category "valves, gas service:" 0/50/0/75/0/50 (bimonthly).

3. Give the average number of days, after a leak is discovered, that an attempt will be made to repair the leak.

4. Note the method used: MB - material balance; EE - engineering estimate; EPA - emission factors established by EPA (cite document used); O - other method, such as in-house emission factor (specify).

5. Do not include in the equipment count sealless pumps (canned motor or diaphragm) or those with enclosed venting to a control device. (Emissions from vented equipment should be included in the estimates given in the Emission Points Data Sheet.)

6. Volatile organic compounds (VOC) means the term as defined in 40 CFR □51.100 (s).

7. A light liquid is defined as a fluid with vapor pressure equal to or greater than 0.04 psi (0.3 Kpa) at 20°C. For mixtures, if 20% w/w or more of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20 °C, then the fluid is defined as a light liquid.

8. A heavy liquid is defined as a fluid with a vapor pressure less than 0.04 psi (0.3 Kpa) at 20°C. For mixtures, if less than 20% w/w of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20 °C, then the fluid is defined as a heavy liquid.

9. LIST CO, H_2S, mineral acids, NO, NO_2, SO_3, etc. DO NOT LIST CO_2, H_2, H_2O, N_2, O_2, and Noble Gases.

10. Include all process valves whether in-line or on an open-ended line such as sample, drain and purge valves. Do not include safety-relief valves, or leakless valves such as check, diaphragm, and bellows seal valves.

11. Do not include a safety-relief valve if there is a rupture disk in place upstream of the valve, or if the valve vents to a control device.

12 Open-ended lines include purge, drain and vent lines. Do not include sampling connections, or lines sealed by plugs, caps, blinds or second valves.

13. Do not include closed-purge sampling connections.

Attachment L
FUGITIVE EMISSIONS FROM UNPAVED HAULROADS

UNPAVED HAULROADS (including all equipment traffic involved in process, haul trucks, endloaders, etc.)

k =	Particle size multiplier	4.90	1.50
s =	Silt content of road surface material (%)	3.9	3.9
p =	Number of days per year with precipitation >0.01 in.	150	150

Item Number	Description	Number of Wheels	Mean Vehicle Weight (tons)	Mean Vehicle Speed (mph)	Miles per Trip	Maximum Trips per Hour	Maximum Trips per Year	Control Device ID Number	Control Efficiency (%)
1	Light Vehicles	4	2	10	0.74	3	2,683	N/A	N/A
2	Medium Trucks	10	15	10	0.74	3	1,533	N/A	N/A
3	Heavy Trucks	18	23.5	10	0.74	2	1,533	N/A	N/A
4									
5									
6									
7									
8									

Source: *AP-42 Fifth Edition – 13.2.2 Unpaved Roads*

$E = k \times 5.9 \times (s \div 12) \times (S \div 30) \times (W \div 3)^{0.7} \times (w \div 4)^{0.5} \times ((365 - p) \div 365) =$ lb/Vehicle Mile Traveled (VMT)

Where:

k =	Particle size multiplier	4.90	1.50
s =	Silt content of road surface material (%)	3.9	3.9
S =	Mean vehicle speed (mph)	10	10
W =	Mean vehicle weight (tons)	14.9	14.9
w =	Mean number of wheels per vehicle	12	12
p =	Number of days per year with precipitation >0.01 in.	150	150

For lb/hr: [lb ÷ VMT] × [VMT ÷ trip] × [Trips ÷ Hour] = lb/hr

For TPY: [lb ÷ VMT] × [VMT ÷ trip] × [Trips ÷ Hour] × [Ton ÷ 2000 lb] = Tons/year

SUMMARY OF UNPAVED HAULROAD EMISSIONS

Item No.	PM				PM-10			
	Uncontrolled		Controlled		Uncontrolled		Controlled	
	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
1	0.11	0.36	-	-	0.03	0.09	-	-
2	0.11	0.36	-	-	0.03	0.09	-	-
3	0.16	0.54	-	-	0.04	0.12	-	-
4								
5								
6								
7								
8								
TOTALS	0.38	1.26	-	-	0.10	0.30	-	-

Note: Minimum one-per-day average pick-up trucks and service trucks even if tanker truck not required every day. Per EPA BID calculations, all emissions based on average trips. Estimated maximum hourly, daily and yearly trips provided for information only.

Revision 03/2007

FUGITIVE EMISSIONS FROM PAVED HAULROADS – *Not Applicable*

INDUSTRIAL PAVED HAULROADS (including all equipment traffic involved in process, haul trucks, endloaders, etc.)

I =	Industrial augmentation factor (dimensionless)	
n =	Number of traffic lanes	
s =	Surface material silt content (%)	
L =	Surface dust loading (lb/mile)	

Item Number	Description	Mean Vehicle Weight (tons)	Miles per Trip	Maximum Trips per Hour	Maximum Trips per Year	Control Device ID Number	Control Efficiency (%)
1							
2							
3							
4							
5							
6							
7							
8							

Source: *AP-42 Fifth Edition – 11.2.6 Industrial Paved Roads*

$E = 0.077 \times I \times (4 \div n) \times (s \div 10) \times (L \div 1000) \times (W \div 3)^{0.7} =$ lb/Vehicle Mile Traveled (VMT)

Where:

I =	Industrial augmentation factor (dimensionless)	
n =	Number of traffic lanes	
s =	Surface meterial silt content (%)	
L =	Surface dust loading (lb/mile)	
W =	Average vehicle weight (tons)	

For lb/hr: [lb ÷ VMT] × [VMT ÷ trip] × [Trips ÷ Hour] = lb/hr

For TPY: [lb ÷ VMT] × [VMT ÷ trip] × [Trips ÷ Hour] × [Ton ÷ 2000 lb] = Tons/year

SUMMARY OF PAVED HAULROAD EMISSIONS

Item No.	Uncontrolled		Controlled	
	lb/hr	TPY	lb/hr	TPY
1				
2				
3				
4				
5				
6				
7				
8				
TOTALS				

Attachment M
Air Pollution Control Device Sheet
(~~FLARE~~ VAPOR COMBUSTOR SYSTEM*)

Control Device ID No. (must match Emission Units Table): APC-COMB-TKLD

Equipment Information

1. Manufacturer: MRW Technologies, Inc. Model No. TBF-4.0-25-71200	2. Method: ☐ Elevated flare ☐ Ground flare ☒ Other Describe: One (1) Vapor Combustor
3. Provide diagram(s) of unit describing capture system with duct arrangement and size of duct, air volume, capacity, horsepower of movers. If applicable, state hood face velocity and hood collection efficiency.	
4. Method of system used: Not applicable ☐ Steam-assisted ☐ Air-assisted ☐ Pressure-assisted ☐ Non-assisted	
5. Maximum capacity of ~~flare~~-vapor combustor: ~50 scf/min ~2,970 scf/hr *Based on 71,200 scfd	6. Dimensions of stack: Diameter 4.0 ft. Height 25.0 ft.
7. Estimated combustion efficiency: (Waste gas destruction efficiency) Estimated: ≥98% Minimum guaranteed: 98%	8. Fuel used in burners: ☒ Natural Gas ☐ Fuel Oil, Number ☐ Other, Specify:
9. Number of burners: Rating: 8.0 mmBTU/hr 10. Will preheat be used? ☐ Yes ☐ No	11. Describe method of controlling flame: Pilot(s) monitored via flame rod.
12. ~~Flare~~Vapor Combustor height: 25.0 ft 13. Flare tip inside diameter: N/A ft	14. Natural gas flow rate to ~~flare~~ pilot flame per pilot light: ~0.83 scf/min ≤50 scf/hr
15. Number of pilot lights: Total 1 ≤46,000** BTU/hr	16. Will automatic re-ignition be used? ☒ Yes ☐ No
17. If automatic re-ignition will be used, describe the method: If the pilot flame is lost, the control system will automatically attempt to relight the pilot. If the re-ignition attempt fails, the pilot solenoid valve will automatically close and a local and remote alarm signal will be generated to indicate loss of pilot flame.	
18. Is pilot flame equipped with a monitor? ☒ Yes ☐ No If yes, what type? ☐ Thermocouple ☐ Infra-Red ☐ Ultra Violet ☐ Camera with monitoring control room ☒ Other, Describe: Flame rod	
19. Hours of unit operation per year: 8,760	

Revision 03/15/2007

Steam Injection

20. Will steam injection be used? ☐ Yes ☒ No	21. Steam pressure PSIG Minimum Expected: Design Maximum:
22. Total Steam flow rate: LB/hr	23. Temperature: °F
24. Velocity ft/sec	25. Number of jet streams
26. Diameter of steam jets: in	27. Design basis for steam injected: LB steam/LB hydrocarbon
28. How will steam flow be controlled if steam injection is used?	

Characteristics of the Waste Gas Stream to be Burned

29.

Name	Quantity Grains of H_2S/100 ft^3	Quantity (LB/hr, ft^3/hr, etc)	Source of Material
See Vapor Combustor			
Calculations in			
Attachment N			

30. Estimate total combustible to ~~flare~~ vapor combustor: 355.11 lb/hr VOC LB/hr or ACF/hr
(Maximum mass flow rate of waste gas) ~50 scfm

31. Estimated total flow rate to ~~flare~~ vapor combustor including materials to be burned, carrier gases, auxiliary fuel, etc.:
355.11 lb/hr VOC LB/hr or ACF/hr

32. Give composition of carrier gases:

33. Temperature of emission stream: ~1,000 °F Heating value of emission stream: 2,682 BTU/ft^3 Mean molecular weight of emission stream: MW = lb/lb-mole	34. Identify and describe all auxiliary fuels to be burned. BTU/scf Not applicable BTU/scf BTU/scf BTU/scf BTU/scf
35. Temperature of ~~flare~~ vapor combustor gas: ~1,000 °F	36. ~~Flare~~ Vapor combustor gas flow rate: ~50 scf/min
37. ~~Flare~~ Vapor combustor gas heat content: 2,682 BTU/ft^3	38. ~~Flare~~ Vapor combustor gas exit velocity: scf/min

39. Maximum rate during emergency for one major piece of equipment or process unit: scf/min

40. Maximum rate during emergency for one major piece of equipment or process unit: BTU/min

41. Describe any air pollution control device inlet and outlet gas conditioning processes (e.g., gas cooling, gas reheating, gas humidification):

42. Describe the collection material disposal system: N/A
43. Have you included ***Flare Vapor Combustor Control Device*** in the Emissions Points Data Summary Sheet? Yes
44. **Proposed Monitoring, Recordkeeping, Reporting, and Testing** Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

MONITORING:	RECORDKEEPING:
As currently permitted	As currently permitted
REPORTING:	**TESTING:**
As currently permitted	As currently permitted

MONITORING:	Please list and describe the process parameters and ranges that are proposed to be monitored in order to demonstrate compliance with the operation of this process equipment or air control device.
RECORDKEEPING:	Please describe the proposed recordkeeping that will accompany the monitoring.
REPORTING:	Please describe any proposed emissions testing for this process equipment on air pollution control device.
TESTING:	Please describe any proposed emissions testing for this process equipment on air pollution control device.

45. Manufacturer's Guaranteed Capture Efficiency for each air pollutant. 100% (per WVDEP guidance)
46. Manufacturer's Guaranteed Control Efficiency for each air pollutant. $\geq$98%
47. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty.

Notes:
****Although a vapor combustor is not considered a flare by design, the function is consistent in that it combusts a waste stream for the purpose controlling emissions. Since there is not APCDS specifically for this device, the APCDS for Flare Systems most accurately reflects the characteristics of this control device.***
*****Assuming 50 SCFH fuel consumption per pilot and 905 Btu/scf fuel heating value.***

ATTACHMENT M: AIR POLLUTION CONTROL DEVICE SHEET

APCDS – COMBUSTOR

VAPOR COMBUSTOR SPECIFICATION SHEET

Tank Battery Combustor Specification Sheet
MRW Technologies, Inc.
Combustor Model Number: TBF-4.0-25-71200

Expected Destruction Removal Efficiency (DRE):	98% or Greater of Non-Methane Hydrocarbons
Unit Size:	4.0-foot Diameter 25-Foot Overall Height
Design Heat Input:	8 MMBTU/HR
Design Flow Rates:	71,200 SCFD
Design Heat Content:	2682 BTU/SCF
Waste Gas Flame Arrestor:	Enardo
Pilot Type:	MRW Electric Ignition
Pilot Operation (Continuous/Intermittent):	Continuous
Pilot Fuel Consumption:	50 SCFH or Less
Pilot Monitoring Device:	Flame Rod
Automatic Re-Ignition:	Included
Remote Alarm Indication:	Included

Description of Control Scheme:

The Combustor pilot is monitored via flame rod. If the pilot flame is lost, the control system will automatically attempt to relight the pilot. If the re-ignition attempt fails, the pilot solenoid valve will automatically close and a local & remote alarm signal will be generated to indicate loss of pilot flame.

C O M B U S T I O N S Y S T E M S
2301 West 171st Street S., Glenpool, OK 74033 • tel: 918.827.6030 • fax: 918.827.6034 • email: mrw@mrw-tech.com

ATTACHMENT N: SUPPORTING EMISSIONS CALCULATIONS

EXAMPLE CALCULATIONS

g/hp-hr Emission Factors:

Emission Factor (g/hp-hr) * Engine Rating (hp) * 1 lb/453.6 g = lb/hr

lb/mmBtu Emission Factors:

Emission Factor (lb/mmBtu) * Engine Rating (hp) * Fuel Use (Btu/hp-hr) * 1 mmBtu/1000000 Btu = lb/hr

Emission Factor (lb/mmBtu) * Combustor Rating (mmBtu/hr) = lb/hr

lb/mmscf Emission Factors:

Emission Factor (lb/mmscf) * Heater Rating (mmBtu/hr) * 1/Fuel Heating Value (Btu/scf) = lb/hr

kg/mmBtu Emission Factors:

Emission Factor (kg/mmBtu) * Engine Rating (hp) * Fuel Use (Btu/hp-hr) * 2.20462 lb/kg * 1 mmBtu/1000000 Btu = lb/hr

Emission Factor (kg/mmBtu) * Heater Rating (mmBtu/hr) * 2.20462 lb/kg = lb/hr

Emissions with Capture and Control Systems:

Uncontrolled Emissions = Potential to Emit without Capture and/or Control

Uncaptured Emissions = Uncontrolled Emissions * (1 – Capture Efficiency %)

Controlled Emissions = Captured Emissions * (1 – Control Efficiency %)

SO_2 Mass Balance:

Representative Gas Analysis (ppmv H_2S) * 32 (MW Sulfur)/34 (MW H_2S) = ppmv Fuel Sulfur Content

Fuel Sulfur Content (ppmv)/15.99 = grains/100 scf

Design Capacity (mmBtu/hr) * 1/Heating Value (Btu/scf) * 1,000,000 Btu/mmBtu * 1 pound/7,000 grains * Fuel Sulfur Content (grains/scf) * 64 (MW SO_2)/32 (MW Sulfur) = lb/hr

Fugitives:

TOC Emission Factor (lb/hr/source) * Number of Sources * VOC wt% = lb/hr VOC

Tons per Year (TPY) Conversion:

lb/hr * Hours/Year * 1 ton/2000 lb = TPY

Tonnes/Year * 1.10231131 = TPY

SWN Production Company, LLC
John Harwatt Pad
Summary of Criteria Air Pollutant Emissions

Equipment	Unit ID	NOx		CO		Total VOC[1]		SO_2[2]		PM Total[3]	
		lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
145-hp Caterpillar G3306 NA Engine w/ Catalytic Converter - Remove	EU-ENG1	-	-	-	-	-	-	-	-	-	-
1.0-mmBtu/hr GPU Burner	EU-GPU1	0.11	0.48	0.09	0.39	0.01	0.03	<0.01	<0.01	0.01	0.04
1.0-mmBtu/hr GPU Burner	EU-GPU2	0.11	0.48	0.09	0.39	0.01	0.03	<0.01	<0.01	0.01	0.04
0.50-mmBtu/hr Heater Treater	EU-HT1	0.06	0.26	0.05	0.22	<0.01	0.01	<0.01	<0.01	<0.01	0.02
0.50-mmBtu/hr Heater Treater - Remove	EU-HT2	-	-	-	-	-	-	-	-	-	-
1.5-mmBtu/hr Line Heater	EU-LH1	0.17	0.74	0.14	0.61	0.01	0.04	<0.01	<0.01	0.01	0.06
1.5-mmBtu/hr Line Heater	EU-LH2	0.17	0.74	0.14	0.61	0.01	0.04	<0.01	<0.01	0.01	0.06
Six (6) 400-bbl Condensate Tanks Routed to Vapor Combustor - Modify	EU-TANKS-COND	-	-	-	-	-	-	-	-	-	-
Six (6) 400-bbl Produced Water Tanks Routed to Vapor Combustor - Modify	EU-TANKS-PW	-	-	-	-	-	-	-	-	-	-
Condensate Truck Loading w/ Vapor Return Routed to Vapor Combustor - Modify	EU-LOAD-COND	-	-	-	-	0.19	0.84	-	-	-	-
Produced Water Truck Loading w/ Vapor Return Routed to Vapor Combustor - Modify	EU-LOAD-PW	-	-	-	-	<0.01	0.02	-	-	-	-
One (1) 8.0-mmBtu/hr Vapor Combustor - Tank/Loading Stream - Modify	APC-COMB-TKLD	1.10	4.84	2.20	9.65	6.80	29.78	-	-	0.02	0.10
Vapor Combustor Pilot	EU-PILOT	0.01	0.04	<0.01	0.02	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01
Fugitive Emissions - Modify	EU-FUG	-	-	-	-	0.59	2.60	-	-	-	-
Fugitive Haul Road Emissions - Modify	EU-HR	-	-	-	-	-	-	-	-	0.38	1.26
Post-Modification Allowable Emissions =		**1.73**	**7.58**	**2.72**	**11.89**	**7.62**	**33.39**	**<0.01**	**0.01**	**0.45**	**1.56**
Current Permit Allowable Emissions =		**2.12**	**9.28**	**3.42**	**14.95**	**8.90**	**38.96**	**<0.01**	**0.01**	**1.94**	**6.48**
Net Allowable Emissions =		**(0.39)**	**(1.71)**	**(0.70)**	**(3.06)**	**(1.28)**	**(5.57)**	**0.00**	**0.00**	**(1.49)**	**(4.92)**

Notes:

[1] Total VOC includes all constituents heavier than Propane (C3+), including hazardous air pollutants (HAP). Speciated HAP presented in following table.

[2] SO_2 emissions from fuel-burning combustion units recalculated using mass balance based on fuel sulfur content of 1.41 ppmv (0.088 grains/100 scf) assuming 1.5 ppmv H_2S. Safety factor added to representative fuel analysis of 0.6 ppmv H_2S for conservative emissions estimate.

SWN Production Company, LLC
John Harwatt Pad
Summary of Hazardous Air Pollutants

Equipment	Unit ID	Estimated Emissions (lb/hr)									
		Acetalde-hyde	Acrolein	Benzene	Ethyl-benzene	Formalde-hyde	Methanol	n-Hexane	Toluene	Xylenes	Total HAPs
145-hp Caterpillar G3306 NA Engine w/ Catalytic Converter - Remove	EU-ENG1	-	-	-	-	-	-	-	-	-	-
1.0-mmBtu/hr GPU Burner	EU-GPU1	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.0-mmBtu/hr GPU Burner	EU-GPU2	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
0.50-mmBtu/hr Heater Treater	EU-HT1	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
0.50-mmBtu/hr Heater Treater - Remove	EU-HT2	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.5-mmBtu/hr Line Heater	EU-LH1	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.5-mmBtu/hr Line Heater	EU-LH2	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
Six (6) 400-bbl Condensate Tanks Routed to Vapor Combustor - Modify	EU-TANKS-COND	-	-	-	-	-	-	-	-	-	-
Six (6) 400-bbl Produced Water Tanks Routed to Vapor Combustor - Modify	EU-TANKS-PW	-	-	-	-	-	-	-	-	-	-
Condensate Truck Loading w/ Vapor Return Routed to Vapor Combustor - Modify	EU-LOAD-COND	-	-	<0.01	<0.01	-	-	0.01	<0.01	<0.01	0.01
Produced Water Truck Loading w/ Vapor Return Routed to Vapor Combustor - Modify	EU-LOAD-PW	-	-	<0.01	<0.01	-	-	<0.01	<0.01	<0.01	<0.01
One (1) 8.0-mmBtu/hr Vapor Combustor - Tank/Loading Stream - Modify	APC-COMB-TKLD	-	-	<0.01	0.02	-	-	0.35	0.02	0.10	0.51
Vapor Combustor Pilot	EU-PILOT	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
Fugitive Emissions - Modify	EU-FUG	-	-	<0.01	<0.01	-	-	0.02	<0.01	0.01	0.03
Fugitive Haul Road Emissions - Modify	EU-HR	-	-	-	-	-	-	-	-	-	-
Post-Modification Allowable Emissions =		**-**	**-**	**0.01**	**0.02**	**-**	**-**	**0.40**	**0.02**	**0.11**	**0.57**
Current Permit Allowable Emissions =		**<0.01**	**<0.01**	**0.01**	**0.04**	**0.02**	**<0.01**	**0.50**	**0.03**	**0.12**	**0.73**
Net Allowable Emissions =		**(0.00)**	**(0.00)**	**0.00**	**(0.02)**	**-0.02**	**(0.00)**	**(0.10)**	**(0.01)**	**(0.01)**	**(0.16)**

Continued on Next Page

SWN Production Company, LLC
John Harwatt Pad
Summary of Hazardous Air Pollutants (Continued)

Equipment	Unit ID	Estimated Emissions (TPY)									
		Acetalde-hyde	Acrolein	Benzene	Ethyl-benzene	Formalde-hyde	Methanol	n-Hexane	Toluene	Xylenes	Total HAPs
145-hp Caterpillar G3306 NA Engine w/ Catalytic Converter - Remove	EU-ENG1	-	-	-	-	-	-	-	-	-	-
1.0-mmBtu/hr GPU Burner	EU-GPU1	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01
1.0-mmBtu/hr GPU Burner	EU-GPU2	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01
0.50-mmBtu/hr Heater Treater	EU-HT1	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
0.50-mmBtu/hr Heater Treater - Remove	EU-HT2	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
1.5-mmBtu/hr Line Heater	EU-LH1	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01
1.5-mmBtu/hr Line Heater	EU-LH2	-	-	<0.01	-	<0.01	-	0.01	<0.01	-	0.01
Six (6) 400-bbl Condensate Tanks Routed to Vapor Combustor - Modify	EU-TANKS-COND	-	-	-	-	-	-	-	-	-	-
Six (6) 400-bbl Produced Water Tanks Routed to Vapor Combustor - Modify	EU-TANKS-PW	-	-	-	-	-	-	-	-	-	-
Condensate Truck Loading w/ Vapor Return Routed to Vapor Combustor - Modify	EU-LOAD-COND	-	-	<0.01	<0.01	-	-	0.04	<0.01	0.01	0.06
Produced Water Truck Loading w/ Vapor Return Routed to Vapor Combustor - Modify	EU-LOAD-PW	-	-	<0.01	<0.01	-	-	<0.01	<0.01	<0.01	<0.01
One (1) 8.0-mmBtu/hr Vapor Combustor - Tank/Loading Stream - Modify	APC-COMB-TKLD	-	-	0.02	0.09	-	-	1.55	0.10	0.45	2.21
Vapor Combustor Pilot	EU-PILOT	-	-	<0.01	-	<0.01	-	<0.01	<0.01	-	<0.01
Fugitive Emissions - Modify	EU-FUG	-	-	<0.01	0.01	-	-	0.11	0.01	0.03	0.15
Fugitive Haul Road Emissions - Modify	EU-HR	-	-	-	-	-	-	-	-	-	-
Post-Modification Allowable Emissions =		**-**	**-**	**0.02**	**0.10**	**-**	**-**	**1.76**	**0.11**	**0.49**	**2.48**
Current Permit Allowable Emissions =		**0.02**	**0.01**	**0.03**	**0.16**	**0.09**	**0.02**	**2.20**	**0.15**	**0.53**	**3.20**
Net Allowable Emissions =		**(0.02)**	**(0.01)**	**(0.01)**	**(0.06)**	**(0.09)**	**(0.02)**	**(0.44)**	**(0.04)**	**(0.04)**	**(0.72)**

SWN Production Company, LLC
John Harwatt Pad
Summary of Greenhouse Gas Emissions - Metric Tons per Year (Tonnes)

Equipment	Unit ID	Carbon Dioxide (CO_2)		Methane (CH_4)		Methane (CH_4) as $CO_{2\,Eq.}$		Nitrous Oxide (N_2O)		Nitrous Oxide (N_2O) as $CO_{2\,Eq.}$		Total CO_2 + $CO_{2\,Eq.}$[1]	
		lb/hr	tonnes/yr	lb/hr	tonnes/yr	lb/hr	tonnes/yr	lb/hr	tonnes/yr	lb/hr	tonnes/yr	lb/hr	tonnes/yr
145-hp Caterpillar G3306 NA Engine w/ Catalytic Converter - Remove	EU-ENG1	-	-	-	-	-	-	-	-	-	-	-	-
1.0-mmBtu/hr GPU Burner	EU-GPU1	116.98	464.80	<0.01	0.01	0.06	0.22	<0.01	<0.01	0.07	0.26	117.10	465.28
1.0-mmBtu/hr GPU Burner	EU-GPU2	116.98	464.80	<0.01	0.01	0.06	0.22	<0.01	<0.01	0.07	0.26	117.10	465.28
0.50-mmBtu/hr Heater Treater	EU-HT1	58.49	232.40	<0.01	<0.01	0.03	0.11	<0.01	<0.01	0.03	0.13	58.55	232.64
0.50-mmBtu/hr Heater Treater - Remove	EU-HT2	58.49	232.40	<0.01	<0.01	0.03	0.11	<0.01	<0.01	0.03	0.13	58.55	232.64
1.5-mmBtu/hr Line Heater	EU-LH1	175.47	697.21	<0.01	0.01	0.08	0.33	<0.01	<0.01	0.10	0.39	175.65	697.93
1.5-mmBtu/hr Line Heater	EU-LH2	175.47	697.21	<0.01	0.01	0.08	0.33	<0.01	<0.01	0.10	0.39	175.65	697.93
Six (6) 400-bbl Condensate Tanks Routed to Vapor Combustor [2]	EU-TANKS-COND	-	-	-	-	-	-	-	-	-	-	-	-
Six (6) 400-bbl Produced Water Tanks Routed to Vapor Combustor [2]	EU-TANKS-PW	-	-	-	-	-	-	-	-	-	-	-	-
Condensate Truck Loading w/ Vapor Return Routed to Vapor Combustor - Modify	EU-LOAD-COND	<0.01	<0.01	<0.01	0.01	0.03	0.14	-	-	-	-	0.03	0.14
Produced Water Truck Loading w/ Vapor Return Routed to Vapor Combustor - Modify	EU-LOAD-PW	<0.01	<0.01	<0.01	<0.01	0.02	0.08	-	-	-	-	0.02	0.08
One (1) 8.0-mmBtu/hr Vapor Combustor - Tank/Loading Stream - Modify	APC-COMB-TKLD	935.82	3,718.44	0.02	0.07	0.44	1.75	<0.01	0.01	0.53	2.09	936.78	3,722.28
Vapor Combustor Pilot	EU-PILOT	5.29	21.03	<0.01	<0.01	<0.01	0.01	<0.01	<0.01	<0.01	0.01	5.30	21.05
Fugitive Emissions - Modify	EU-FUG	<0.01	0.01	0.36	1.42	7.56	29.72	-	-	-	-	7.56	29.73
Fugitive Haul Road Emissions - Modify	EU-HR	-	-	-	-	-	-	-	-	-	-	-	-
Post-Modification Allowable Emissions =		**1,642.97**	**6,528.30**	**0.39**	**1.55**	**8.39**	**33.01**	**<0.01**	**0.01**	**0.92**	**3.67**	**1,652.28**	**6,564.98**

Notes:

[1] CO_2 Equivalent = Pollutant times GWP multiplier. 40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier (100-Year Time Horizon): CO_2 = 1, CH_4 = 25, N_2O = 298

[2] Per API Compendium (2009) Chapter 5: Because most of the CH_4 and CO_2 emissions from storage tanks occur as a result of flashing (which is controlled by the vapor combustor in this case), working and breathing loss emissions of these gases are very small in production and virtually non-existent in the downstream segments. Vapors from the tanks are routed to the vapor combustor at this site. Therefore, GHG emissions from the condensate and produced water tanks are assumed to be negligible.

SWN Production Company, LLC
John Harwatt Pad
Summary of Greenhouse Gas Emissions - Short Tons per Year (Tons)

Equipment	Unit ID	Carbon Dioxide (CO_2)		Methane (CH_4)		Methane (CH_4) as $CO_{2\,Eq.}$		Nitrous Oxide (N_2O)		Nitrous Oxide (N_2O) as $CO_{2\,Eq.}$		Total CO_2 + $CO_{2\,Eq.}$[1]	
		lb/hr	tons/yr[2]	lb/hr	tons/yr[2]	lb/hr	tons/yr	lb/hr	tons/yr[2]	lb/hr	tons/yr	lb/hr	tons/yr
145-hp Caterpillar G3306 NA Engine w/ Catalytic Converter - Remove	EU-ENG1	-	-	-	-	-	-	-	-	-	-	-	-
1.0-mmBtu/hr GPU Burner	EU-GPU1	116.98	512.36	<0.01	0.01	0.06	0.24	<0.01	<0.01	0.07	0.29	117.10	512.89
1.0-mmBtu/hr GPU Burner	EU-GPU2	116.98	512.36	<0.01	0.01	0.06	0.24	<0.01	<0.01	0.07	0.29	117.10	512.89
0.50-mmBtu/hr Heater Treater	EU-HT1	58.49	256.18	<0.01	<0.01	0.03	0.12	<0.01	<0.01	0.03	0.14	58.55	256.44
0.50-mmBtu/hr Heater Treater - Remove	EU-HT2	58.49	256.18	<0.01	<0.01	0.03	0.12	<0.01	<0.01	0.03	0.14	58.55	256.44
1.5-mmBtu/hr Line Heater	EU-LH1	175.47	768.54	<0.01	0.01	0.08	0.36	<0.01	<0.01	0.10	0.43	175.65	769.33
1.5-mmBtu/hr Line Heater	EU-LH2	175.47	768.54	<0.01	0.01	0.08	0.36	<0.01	<0.01	0.10	0.43	175.65	769.33
Six (6) 400-bbl Condensate Tanks Routed to Vapor Combustor[3]	EU-TANKS-COND	-	-	-	-	-	-	-	-	-	-	-	-
Six (6) 400-bbl Produced Water Tanks Routed to Vapor Combustor[3]	EU-TANKS-PW	-	-	-	-	-	-	-	-	-	-	-	-
Condensate Truck Loading w/ Vapor Return Routed to Vapor Combustor - Modify	EU-LOAD-COND	<0.01	<0.01	<0.01	0.01	0.03	0.15	-	-	-	-	0.03	0.15
Produced Water Truck Loading w/ Vapor Return Routed to Vapor Combustor - Modify	EU-LOAD-PW	<0.01	<0.01	<0.01	<0.01	0.02	0.08	-	-	-	-	0.02	0.08
One (1) 8.0-mmBtu/hr Vapor Combustor - Tank/Loading Stream - Modify	APC-COMB-TKLD	935.82	4,098.88	0.02	0.08	0.44	1.93	<0.01	0.01	0.53	2.30	936.78	4,103.11
Vapor Combustor Pilot	EU-PILOT	5.29	23.18	<0.01	<0.01	<0.01	0.01	<0.01	<0.01	<0.01	0.01	5.30	23.21
Fugitive Emissions - Modify	EU-FUG	<0.01	0.01	0.36	1.56	7.56	32.76	-	-	-	-	7.56	32.77
Fugitive Haul Road Emissions - Modify	EU-HR	-	-	-	-	-	-	-	-	-	-	-	-
Post-Modification Allowable Emissions =		**1,642.97**	**7,196.22**	**0.39**	**1.71**	**8.39**	**36.39**	**<0.01**	**0.01**	**0.92**	**4.05**	**1,652.29**	**7,236.65**

Notes:

[1] CO_2 Equivalent = Pollutant times GWP multiplier. 40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier (100-Year Time Horizon): CO_2 = 1, CH_4 = 25, N_2O = 298

[2] EPA and API GHG calculation methodologies calculate emissions in metric tons (tonnes). These values have been converted to short tons for consistency with permitting threshold units.

[3] Per API Compendium (2009) Chapter 5: Because most of the CH_4 and CO_2 emissions from storage tanks occur as a result of flashing (which is controlled by the vapor combustor in this case), working and breathing loss emissions of these gases are very small in production and virtually non-existent in the downstream segments. Vapors from the tanks are routed to the vapor combustor at this site. Therefore, GHG emissions from the condensate and produced water tanks are assumed to be negligible.

SWN Production Company, LLC
John Harwatt Pad
Storage Tank Emissions - Criteria Air Pollutants

Tank Information

Unit ID:	EU-TANKS-COND	EU-TANKS-PW
Contents: [1]	Condensate	Produced Water
Number of Tanks: [2]	6	6
Capacity (bbl) - Per Tank:	400	400
Capacity (gal) - Per Tank:	16,800	16,800
Total Throughput (bbl/yr):	65,700	36,500
Total Throughput (gal/yr):	2,759,400	1,533,000
Total Throughput (bbl/d):	180	100
Tank Flashing Emission Factor (lb/bbl):	45.20	0.008
Total Working Losses (lb/yr): [3]	2,135.40	2.46
Breathing Losses per Tank (lb/yr): [3]	342.89	0.50
Tank Vapor Capture Efficiency:	100%	100%
Captured Vapors Routed to:	Vapor Combustor	Vapor Combustor

Uncontrolled Storage Tank Emissions

Unit ID:	EU-TANKS-COND		EU-TANKS-PW	
Emissions	**lb/hr**	**TPY**	**lb/hr**	**TPY**
Working Losses	0.24	1.07	<0.01	<0.01
Breathing Losses	0.23	1.02	<0.01	<0.01
Flashing Losses	339.00	1,484.82	0.03	0.15
Total VOC =	**339.48**	**1,486.91**	**0.03**	**0.15**

Notes:

[1] Produced water tanks assumed to contain 99% produced water and 1% condensate.

[2] SWN requests to combine working, breathing and flashing emissions from each tank type to be combined into one emissions point with a total throughput limit rather than an individual tank limit.

[3] Tank working and breathing emissions were calculated using maximum throughput in EPA TANKS 4.0.9d for working losses and multiplying results for breathing losses by the number of tanks for total potential evaporative losses from all tanks. Flashing calculated using Promax process simulation. Reports located in Attachment N. Uncontrolled tank working/breathing/flashing emissions are routed to a vapor combustor with 100% capture efficiency (per WVDEP guidance).

SWN Production Company, LLC
John Harwatt Pad
Storage Tank Emissions - Hazardous Air Pollutants

Uncontrolled Storage Tank Emissions

Unit ID:	EU-TANKS-COND		EU-TANKS-PW	
Pollutant	**lb/hr**	**TPY**	**lb/hr**	**TPY**
Total VOC = [1]	**339.48**	**1,486.91**	**0.03**	**0.15**
n-Hexane	17.69	77.50	<0.01	0.01
Benzene	0.23	1.00	<0.01	<0.01
Toluene	1.13	4.95	<0.01	<0.01
Ethylbenzene	1.07	4.67	<0.01	<0.01
Xylenes	5.10	22.32	<0.01	<0.01
Total HAPs =	**25.21**	**110.44**	**<0.01**	**0.01**

Estimated HAP Composition (% by Weight)[3]

Pollutant	Wt%
n-Hexane	5.212%
Benzene	0.067%
Toluene	0.333%
Ethylbenzene	0.314%
Xylenes	1.501%
Total HAPs =	**7.427%**

Notes:

[1] VOC emissions calculated in Criteria Air Pollutant calculations.

[2] Uncontrolled tank working/breathing/flashing emissions are routed to a vapor combustor with 100% capture efficiency.

[3] Speciated liquids analysis located in Fugitive Emissions Calculations. HAP weight % calculated as % of total hydrocarbons in the sample. All HAP assumed to volatilize from liquids for most conservative emissions estimate.

SWN Production Company, LLC
John Harwatt Pad
Condensate Truck Loading Emissions - Criteria and Hazardous Air Pollutants

Loading Information

Unit ID:	**EU-LOAD-COND**
Fill Method:	Submerged
Type of Service:	Dedicated
Mode of Operation:	Normal
Saturation Factor:	0.6
Em. Factor (lb/1000 gal): [1]	2.02
Throughput (1000 gal):	2,759.4
Control Type:	Vapor Return/Combustion
Vapor Capture Efficiency: [2]	70%
Average Fill Rate (gal/hr):	7,500
Captured Vapors Routed to:	Vapor Combustor

5.9008	= P, True vapor pressure of liquid loaded (max. psia)[3]
23.425	= M, Molecular weight of vapor (lb/lb-mol)
50.33	= T, Temperature of bulk liquid loaded (average °F)
510.33	= T, Temperature of bulk liquid loaded (°F + 460 = °R)

Uncontrolled Loading Emissions[4]

Pollutant	Max. lb/hr	Avg. lb/hr	TPY
VOC =	**15.15**	**0.64**	**2.79**
n-Hexane	0.79	0.03	0.15
Benzene	0.01	<0.01	<0.01
Toluene	0.05	<0.01	0.01
Ethylbenzene	0.05	<0.01	0.01
Xylenes	0.23	0.01	0.04
Total HAPs [5] =	**1.13**	**0.05**	**0.21**

SWN Production Company, LLC
John Harwatt Pad
Condensate Truck Loading Emissions - Criteria and Hazardous Air Pollutants (Continued)

Uncaptured Loading Emissions[4]

Pollutant	Max. lb/hr	Avg. lb/hr	TPY
VOC =	**4.55**	**0.19**	**0.84**
n-Hexane	0.24	0.01	0.04
Benzene	<0.01	<0.01	<0.01
Toluene	0.02	<0.01	<0.01
Ethylbenzene	0.01	<0.01	<0.01
Xylenes	0.07	<0.01	0.01
Total HAPs [5] =	**0.34**	**0.01**	**0.06**

Notes:

[1] AP-42 5.2-4 Eq.1: Loading Loss (lb/1000 gal) = 12.46 *S*P*M/T.

[2] Uncontrolled emissions that are captured by the collection system are routed to a vapor combustor. Per AP-42 5.2-6, 70% capture efficiency can be assumed for trucks not subject to NSPS. Uncaptured emissions shown represent those not captured by the collection system or controlled by the vapor combustor.

[3] AP-42 Section 7.1 - Properties of Selected Petroleum Liquids correlation with information obtained from TANKS 4.0.9d.

[4] Maximum lb/hr based on average hourly truck loading rate. Average lb/hr based on TPY conversion assuming continuous operation.

[5] Speciated liquids analysis located in Fugitive Emissions Calculations. HAP weight % calculated as % of total hydrocarbons in the sample. All HAP assumed to volatilize from liquids for most conservative emissions estimate.

Pollutant	Wt%
n-Hexane	5.212%
Benzene	0.067%
Toluene	0.333%
Ethylbenzene	0.314%
Xylenes	1.501%
Total HAPs =	**7.427%**

SWN Production Company, LLC
John Harwatt Pad
Condensate Truck Loading Emissions - Greenhouse Gases

Loading Information

Unit ID:	**EU-LOAD-COND**
Fill Method:	Submerged
Type of Service:	Dedicated
Mode of Operation:	Normal
TOC Em. Factor (tonne/10^6 gal): [1]	0.91
Throughput (10^6 gal):	2.7594
Control Type:	Vapor Return/Combustion
Vapor Capture Efficiency: [2]	70.00%
Average Fill Rate (gal/hr):	7,500
Captured Vapors Routed to:	Vapor Combustor

CH_4 wt% from analysis =	0.73%
CO_2 wt% from analysis =	0.01%

Uncontrolled Loading Emissions[3, 4]

Pollutant	Max. lb/hr	Avg. lb/hr	tonnes/yr	tons/yr
CH_4	0.11	<0.01	0.02	0.02
CH_4 as CO_2e	2.74	0.12	0.46	0.50
CO_2	<0.01	<0.01	<0.01	<0.01
Total CO_2 + CO_2e =	**2.74**	**0.12**	**0.46**	**0.50**

SWN Production Company, LLC
John Harwatt Pad
Condensate Truck Loading Emissions - Greenhouse Gases (Continued)

Uncaptured Loading Emissions[3, 4]

Pollutant	Max. lb/hr	Avg. lb/hr	tonnes/yr	tons/yr
CH_4	0.03	<0.01	0.01	0.01
CH_4 as CO_2e	0.82	0.03	0.14	0.15
CO_2	<0.01	<0.01	<0.01	<0.01
Total CO_2 + CO_2e =	**0.82**	**0.03**	**0.14**	**0.15**

API Compendium Table 5-12

Loading Type	Emission Factor (tonne TOC/10^6 gal)
Rail/Truck - Submerged Loading - Dedicated Normal Service	0.91
Rail/Truck - Submerged Loading - Vapor Balance Service	1.51
Rail/Truck - Splash Loading - Dedicated Normal Service	2.20
Rail/Truck - Splash Loading - Vapor Balance Service	1.51
Marine Loading - Ships/Ocean Barges	0.28
Marine Loading - Barges	0.45

Notes:

[1] API Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Gas Industry, Table 5-12.

[2] Uncontrolled emissions that are captured by the collection system are routed to a vapor combustor. Per AP-42 5.2-6, 70% capture efficiency can be assumed for trucks not subject to NSPS. Uncaptured emissions shown represent those not captured by the collection system or controlled by the vapor combustor.

[3] Maximum lb/hr based on average hourly truck loading rate. Average lb/hr based on TPY conversion assuming continuous operation.

[4] CO_2e = CO_2 equivalent (Pollutant times GWP multiplier):
40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier: CO_2 = 1, CH_4 = 25, N_2O = 298

SWN Production Company, LLC
John Harwatt Pad
Produced Water Truck Loading Emissions - Criteria and Hazardous Air Pollutants

Loading Information

Unit ID:	**EU-LOAD-PW**
Fill Method:	Submerged
Type of Service:	Dedicated
Mode of Operation:	Normal
Saturation Factor:	0.6
Em. Factor (lb/1000 gal): [1]	0.06
Throughput (1000 gal):	1,533.0
Control Type:	Vapor Return/Combustion
Vapor Capture Efficiency: [2]	70%
Average Fill Rate (gal/hr):	7,500
Captured Vapors Routed to:	Vapor Combustor

0.2368	= P, True vapor pressure of liquid loaded (max. psia)
18.237	= M, Molecular weight of vapor (lb/lb-mol)
50.33	= T, Temperature of bulk liquid loaded (average °F)
510.33	= T, Temperature of bulk liquid loaded (°F + 460 = °R)

Uncontrolled Loading Emissions[3]

Pollutant	Max. lb/hr	Avg. lb/hr	TPY
VOC =	**0.45**	**0.01**	**0.05**
n-Hexane	0.02	<0.01	<0.01
Benzene	<0.01	<0.01	<0.01
Toluene	<0.01	<0.01	<0.01
Ethylbenzene	<0.01	<0.01	<0.01
Xylenes	0.01	<0.01	<0.01
Total HAPs[4] =	**0.03**	**<0.01**	**<0.01**

SWN Production Company, LLC
John Harwatt Pad
Produced Water Truck Loading Emissions - Criteria and Hazardous Air Pollutants (Continued)

Uncaptured Loading Emissions[3]

Pollutant	Max. lb/hr	Avg. lb/hr	TPY
VOC =	**0.14**	**<0.01**	**0.02**
n-Hexane	0.01	<0.01	<0.01
Benzene	<0.01	<0.01	<0.01
Toluene	<0.01	<0.01	<0.01
Ethylbenzene	<0.01	<0.01	<0.01
Xylenes	<0.01	<0.01	<0.01
Total HAPs[4] =	**0.01**	**<0.01**	**<0.01**

Notes:

[1] AP-42 5.2-4 Eq.1: Loading Loss (lb/1000 gal) = 12.46 *S*P*M/T. Properties based on mixture of 99% water and 1% condensate.

[2] Uncontrolled emissions that are captured by the collection system are routed to a vapor combustor. Per AP-42 5.2-6, 70% capture efficiency can be assumed for trucks not subject to NSPS. Uncaptured emissions shown represent those not captured by the collection system or controlled by the vapor combustor.

[3] Maximum lb/hr based on average hourly truck loading rate. Average lb/hr based on TPY conversion assuming continuous operation.

[4] Speciated liquids analysis located in Fugitive Emissions Calculations. HAP weight % calculated as % of total hydrocarbons in the sample. All HAP assumed to volatilize from liquids for most conservative emissions estimate.

Pollutant	Wt%
n-Hexane	5.212%
Benzene	0.067%
Toluene	0.333%
Ethylbenzene	0.314%
Xylenes	1.501%
Total HAPs =	**7.427%**

SWN Production Company, LLC
John Harwatt Pad
Produced Water Truck Loading Emissions - Greenhouse Gases

Loading Information

Unit ID:	**EU-LOAD-PW**
Fill Method:	Submerged
Type of Service:	Dedicated
Mode of Operation:	Normal
TOC Em. Factor (tonne/10^6 gal): [1]	0.91
Throughput (10^6 gal):	1.533
Control Type:	Vapor Return/Combustion
Vapor Capture Efficiency: [2]	70.00%
Average Fill Rate (gal/hr):	7,500
Captured Vapors Routed to:	Vapor Combustor

CH_4 wt% from analysis =	0.73%
CO_2 wt% from analysis =	0.01%

Uncontrolled Loading Emissions[3, 4]

Pollutant	Max. lb/hr	Avg. lb/hr	tonnes/yr	tons/yr
CH_4	0.11	<0.01	0.01	0.01
CH_4 as CO_2e	2.74	0.06	0.25	0.28
CO_2	<0.01	<0.01	<0.01	<0.01
Total CO_2 + CO_2e =	**2.74**	**0.06**	**0.25**	**0.28**

SWN Production Company, LLC
John Harwatt Pad
Produced Water Truck Loading Emissions - Greenhouse Gases (Continued)

Uncaptured Loading Emissions[3, 4]

Pollutant	Max. lb/hr	Avg. lb/hr	tonnes/yr	tons/yr
CH_4	0.03	<0.01	<0.01	<0.01
CH_4 as CO_2e	0.82	0.02	0.08	0.08
CO_2	<0.01	<0.01	<0.01	<0.01
Total CO_2 + CO_2e =	**0.82**	**0.02**	**0.08**	**0.08**

API Compendium Table 5-12

Loading Type	Emission Factor (tonne TOC/10^6 gal)
Rail/Truck - Submerged Loading - Dedicated Normal Service	0.91
Rail/Truck - Submerged Loading - Vapor Balance Service	1.51
Rail/Truck - Splash Loading - Dedicated Normal Service	2.20
Rail/Truck - Splash Loading - Vapor Balance Service	1.51
Marine Loading - Ships/Ocean Barges	0.28
Marine Loading - Barges	0.45

Notes:

[1] API Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Gas Industry, Table 5-12.

[2] Uncontrolled emissions that are captured by the collection system are routed to a vapor combustor. Per AP-42 5.2-6, 70% capture efficiency can be assumed for trucks not subject to NSPS. Uncaptured emissions shown represent those not captured by the collection system or controlled by the vapor combustor.

[3] Maximum lb/hr based on average hourly truck loading rate. Average lb/hr based on TPY conversion assuming continuous operation.

[4] CO_2e = CO_2 equivalent (Pollutant times GWP multiplier):
40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier: CO_2 = 1, CH_4 = 25, N_2O = 298

SWN Production Company, LLC
John Harwatt Pad
Tanks/Loading Vapor Combustor Emissions Calculations - Criteria and Hazardous Air Pollutants

Criteria and Hazardous Air Pollutant Emissions

Unit ID	Pollutant	Emission Factors[1]	Total Captured Emissions[2]		Combustor Destruction Efficiency	Total Controlled Emissions (Post-Capture and Combustion)	
			lb/hr	TPY	%	lb/hr	TPY
APC-COMB-TKLD	NOx	0.138	-	-	-	1.10	4.84
	CO	0.2755	-		-	2.20	9.65
	PM	7.6	-		-	0.02	0.10
	VOC	Mass Balance	339.97	1,489.05	98.00%	6.80	29.78
	n-Hexane	Mass Balance	17.71	77.61	98.00%	0.35	1.55
	Benzene	Mass Balance	0.23	1.00	98.00%	<0.01	0.02
	Toluene	Mass Balance	1.13	4.96	98.00%	0.02	0.10
	Ethylbenzene	Mass Balance	1.07	4.68	98.00%	0.02	0.09
	Xylenes	Mass Balance	5.11	22.35	98.00%	0.10	0.45

Notes:

[1] Although a vapor combustor is not considered a flare by design, the function is consistent in that it combusts a waste stream for the purpose of reducing emissions; therefore, flare emission factors for NOx and CO were used to provide the most accurate emissions estimates. Although the combustor is designed to be smokeless, PM emissions have been estimated using AP-42 Table 1.4-1 factor (lb/mmscf) for a conservative estimate.

Hours per Year: 8,760
Number of Combustors: 1

NOx and CO emission factors (lb/mmBtu): *TCEQ Air Permit Technical Guidance for Chemical Sources: Flares and Vapor Oxidizers:* High Btu waste streams (>1,000 Btu/scf) based on heat input to each combustor = 8.00 mmBtu/hr Total Heat Input

[2] Total captured emissions are based on 100% capture efficiency from storage tanks and 70% capture efficiency from truck loading with 98% destruction efficiency from the vapor combustor based on 8,760 hours of operation per year. Uncaptured vapors reported at loading emission units. Captured emissions from sources controlled by VOC combustor shown in following tables.

SWN Production Company, LLC
John Harwatt Pad
Tanks/Loading Vapor Combustor Emissions Calculations - Criteria and Hazardous Air Pollutants (Continued)

Source	Captured VOC Emissions	
	lb/hr	TPY
Condensate Storage Tanks	339.48	1,486.91
Produced Water Storage Tanks	0.03	0.15
Condensate Truck Loading	0.45	1.95
Produced Water Truck Loading	0.01	0.04
Total VOC =	**339.97**	**1,489.05**

Source	Captured HAP Emissions (lb/hr)				
	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylenes
Condensate Storage Tanks	17.69	0.23	1.13	1.07	5.10
Produced Water Storage Tanks	0.00	<0.01	<0.01	<0.01	<0.01
Condensate Truck Loading	0.02	<0.01	<0.01	<0.01	0.01
Produced Water Truck Loading	<0.01	<0.01	<0.01	<0.01	<0.01
Total HAP =	**17.71**	**0.23**	**1.13**	**1.07**	**5.11**

Source	Captured HAP Emissions (TPY)				
	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylenes
Condensate Storage Tanks	77.50	1.00	4.95	4.67	22.32
Produced Water Storage Tanks	0.01	<0.01	<0.01	<0.01	0.00
Condensate Truck Loading	0.10	<0.01	0.01	0.01	0.03
Produced Water Truck Loading	<0.01	<0.01	<0.01	<0.01	<0.01
Total HAP =	**77.61**	**1.00**	**4.96**	**4.68**	**22.35**

SWN Production Company, LLC
John Harwatt Pad
Tanks/Loading Vapor Combustor Emissions Calculations - Greenhouse Gases

Equipment Information

Unit ID:	**APC-COMB-TKLD**
Description:	Vapor Combustor
Number of Combustors:	1
Burner Design Capacity (mmBtu/hr):	8.00
Stream HHV (Btu/scf):	2,682
Annual Throughput (mmscf):	26.13
Annual Operating Hours:	8,760

Greenhouse Gas (GHG) Emissions

Pollutant	lb/hr	tonnes/yr	tons/yr
CO_2	935.82	3,718.44	4,098.88
CH_4	0.02	0.07	0.08
N_2O	<0.01	0.01	0.01
CH_4 as CO_2e	0.44	1.75	1.93
N_2O as CO_2e	0.53	2.09	2.30
Total CO_2 + CO_2e =	**936.78**	**3,722.28**	**4,103.11**

40 CFR 98 Tables C-1 and C-2 Emission Factors (kg/mmBtu)[1]

Carbon Dioxide (CO_2)	53.06
Methane (CH_4)	1.00E-03
Nitrous Oxide (N_2O)	1.00E-04

Notes:
[1] CO_2e = CO_2 equivalent (Pollutant times GWP multiplier):
40 CFR 98 Table A-1, Global Warming Potential (GWP) multiplier: CO_2 = 1, CH_4 = 25, N_2O = 298

SWN Production Company, LLC
John Harwatt Pad
Uncontrolled and Controlled Emissions for Emission Points Routed to Combustor

Uncontrolled Emissions														
Pollutant	EU-TANKS-COND		EU-TANKS-PW		EU-LOAD-COND		EU-LOAD-PW		APC-COMB-TKLD		EU-PILOT		Total	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
NOx	-	-	-	-	-	-	-	-	1.10	4.84	0.01	0.04	1.11	4.88
CO	-	-	-	-	-	-	-	-	2.20	9.65	<0.01	0.02	2.21	9.67
VOC	339.48	1,486.91	0.03	0.15	15.15	2.79	0.45	0.05	-	-	<0.01	<0.01	355.11	1,489.90
SO_2	-	-	-	-	-	-	-	-	-	-	<0.01	<0.01	<0.01	<0.01
PM_{10}	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PM_{Total}	-	-	-	-	-	-	-	-	0.02	0.10	<0.01	<0.01	0.02	0.10
n-Hexane	17.69	77.50	<0.01	0.01	0.79	0.15	0.02	<0.01	-	-	<0.01	<0.01	18.51	77.66
HCHO	-	-	-	-	-	-	-	-	-	-	<0.01	<0.01	<0.01	<0.01
Benzene	0.23	1.00	<0.01	<0.01	0.01	<0.01	<0.01	<0.01	-	-	<0.01	<0.01	0.24	1.00
Toluene	1.13	4.95	<0.01	<0.01	0.05	0.01	<0.01	<0.01	-	-	<0.01	<0.01	1.18	4.96
Ethylbenzene	1.07	4.67	<0.01	<0.01	0.05	0.01	<0.01	<0.01	-	-	-	-	1.11	4.68
Xylenes	5.10	22.32	<0.01	<0.01	0.23	0.04	0.01	<0.01	-	-	-	-	5.33	22.37
CO_2	-	-	-	-	<0.01	<0.01	<0.01	<0.01	935.82	4,098.88	5.29	23.18	941.11	4,122.06
CH_4	-	-	-	-	0.11	0.02	0.11	0.01	0.02	0.08	<0.01	<0.01	0.24	0.11
N_2O	-	-	-	-	-	-	-	-	<0.01	0.01	<0.01	<0.01	<0.01	0.01

Controlled Emissions														
Pollutant	EU-TANKS-COND		EU-TANKS-PW		EU-LOAD-COND		EU-LOAD-PW		APC-COMB-TKLD		EU-PILOT		Total	
	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy	lb/hr	tpy
NOx	-	-	-	-	-	-	-	-	1.10	4.84	0.01	0.04	1.11	4.88
CO	-	-	-	-	-	-	-	-	2.20	9.65	<0.01	0.02	2.21	9.67
VOC	6.79	29.74	<0.01	<0.01	0.01	0.04	<0.01	<0.01	-	-	<0.01	<0.01	6.80	29.78
SO_2	-	-	-	-	-	-	-	-	-	-	<0.01	<0.01	<0.01	<0.01
PM_{10}	-	-	-	-	-	-	-	-	-	-	-	-	-	-
PM_{Total}	-	-	-	-	-	-	-	-	0.02	0.10	<0.01	<0.01	0.02	0.10
n-Hexane	0.35	1.55	-	<0.01	<0.01	<0.01	<0.01	<0.01	-	-	<0.01	<0.01	0.35	1.55
HCHO	-	-	-	-	-	-	-	-	-	-	<0.01	<0.01	<0.01	<0.01
Benzene	<0.01	0.02	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	-	-	<0.01	<0.01	<0.01	0.02
Toluene	0.02	0.10	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	-	-	<0.01	<0.01	0.02	0.10
Ethylbenzene	0.02	0.09	<0.01	<0.01	<0.01	<0.01	<0.01	<0.01	-	-	-	-	0.02	0.09
Xylenes	0.10	0.45	<0.01	-	<0.01	<0.01	<0.01	<0.01	-	-	-	-	0.10	0.45
CO_2	-	-	-	-	<0.01	<0.01	<0.01	<0.01	935.82	4,098.88	5.29	23.18	941.11	4,122.06
CH_4	-	-	-	-	0.11	0.02	0.11	0.01	0.02	0.08	<0.01	<0.01	0.24	0.11
N_2O	-	-	-	-	-	-	-	-	<0.01	0.01	<0.01	<0.01	<0.01	0.01

Note: Uncontrolled emissions represent the uncontrolled emissions of all emission sources that are controlled by the combustor, combustor emissions and pilot emissions. Controlled emissions are the undestroyed emissions at the combustor, combustor emissions and pilot emissions.

SWN Production Company, LLC
John Harwatt Pad
Fugitive Emissions Calculations - Criteria and Hazardous Air Pollutants and Greenhouse Gases

Equipment Information

Source Type/Service	Number of Sources[1]	Em. Factor (lb/hr/source)[2]	Control Efficiency	TOC lb/hr	TOC TPY	VOC Wt %
Valves - Gas	32	9.92E-03	0.00%	0.32	1.40	27.72%
Flanges - Gas	133	8.60E-04	0.00%	0.11	0.48	27.72%
Compressor Seals - Gas	0	1.94E-02	0.00%	0.00	0.00	27.72%
Relief Valves - Gas	16	1.94E-02	0.00%	0.31	1.36	27.72%
Open-Ended Lines - Gas	0	4.41E-03	0.00%	0.00	0.00	27.72%
			Total TOC (Gas Components) =	**0.74**	**3.24**	-
Valves - Light Oil	61	5.51E-03	0.00%	0.34	1.49	96.74%
Flanges - Light Oil	238	2.43E-04	0.00%	0.06	0.26	96.74%
Pump Seals - Light Oil	0	2.87E-02	0.00%	0.00	0.00	96.74%
Other - Light Oil	0	1.65E-02	0.00%	0.00	0.00	96.74%
			Total TOC (Liquid Components) =	**0.40**	**1.75**	-

VOC and Greenhouse Gas Emissions

Source Type/Service	VOC		CH_4		CO_2	
	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
Valves - Gas	0.09	0.39	0.15	0.67	<0.01	<0.01
Flanges - Gas	0.03	0.14	0.05	0.23	<0.01	<0.01
Compressor Seals - Gas	0.00	0.00	0.00	0.00	0.00	0.00
Relief Valves - Gas	0.09	0.38	0.15	0.65	<0.01	<0.01
Open-Ended Lines - Gas	0.00	0.00	0.00	0.00	0.00	0.00
Components in Gas Service =	**0.21**	**0.91**	**0.35**	**1.55**	**<0.01**	**0.01**
Valves - Light Oil	0.33	1.42	<0.01	0.01	<0.01	<0.01
Flanges - Light Oil	0.06	0.24	<0.01	<0.01	<0.01	<0.01
Pump Seals - Light Oil	0.00	0.00	0.00	0.00	0.00	0.00
Other - Light Oil	0.00	0.00	0.00	0.00	0.00	0.00
Components in Liquid Service =	**0.39**	**1.69**	**0.00**	**0.01**	**<0.01**	**<0.01**
Total (Gas + Liquid Components) =	**0.59**	**2.60**	**0.36**	**1.56**	**<0.01**	**0.01**

SWN Production Company, LLC
John Harwatt Pad
Fugitive Emissions Calculations (Continued)

Hazardous Air Pollutant (HAP) Emissions (lb/hr)

Source Type/Service	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylenes	2,2,4-Tri.	Total
Valves - Gas	<0.01	<0.01	<0.01	0.00	<0.01	0.00	<0.01
Flanges - Gas	<0.01	<0.01	<0.01	0.00	<0.01	0.00	<0.01
Compressor Seals - Gas	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Relief Valves - Gas	<0.01	<0.01	<0.01	0.00	<0.01	0.00	<0.01
Open-Ended Lines - Gas	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Components in Gas Service =	**<0.01**	**<0.01**	**<0.01**	**0.00**	**<0.01**	**0.00**	**<0.01**
Valves - Light Oil	0.02	<0.01	<0.01	<0.01	0.01	0.00	0.02
Flanges - Light Oil	<0.01	<0.01	<0.01	<0.01	<0.01	0.00	<0.01
Pump Seals - Light Oil	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Other - Light Oil	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Components in Liquid Service =	**0.02**	**<0.01**	**<0.01**	**<0.01**	**0.01**	**0.00**	**0.03**
Total (Gas + Liquid Components) =	**0.02**	**<0.01**	**<0.01**	**<0.01**	**0.01**	**0.00**	**0.03**

Hazardous Air Pollutant (HAP) Emissions (TPY)

Source Type/Service	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylenes	2,2,4-Tri.	Total
Valves - Gas	0.01	<0.01	<0.01	0.00	<0.01	0.00	0.01
Flanges - Gas	<0.01	<0.01	<0.01	0.00	<0.01	0.00	<0.01
Compressor Seals - Gas	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Relief Valves - Gas	0.01	<0.01	<0.01	0.00	<0.01	0.00	0.01
Open-Ended Lines - Gas	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Components in Gas Service =	**0.02**	**<0.01**	**<0.01**	**0.00**	**<0.01**	**0.00**	**0.02**
Valves - Light Oil	0.08	<0.01	<0.01	<0.01	0.02	0.00	0.11
Flanges - Light Oil	0.01	<0.01	<0.01	<0.01	<0.01	0.00	0.02
Pump Seals - Light Oil	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Other - Light Oil	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Components in Liquid Service =	**0.09**	**<0.01**	**0.01**	**0.01**	**0.03**	**0.00**	**0.13**
Total (Gas + Liquid Components) =	**0.11**	**<0.01**	**0.01**	**0.01**	**0.03**	**0.00**	**0.15**

SWN Production Company, LLC
John Harwatt Pad
Fugitive Emissions Calculations (Continued)

Typical Component Count per Equipment Type based on Representative Facility[3]

Source Type/Service	WH	GPU	HT	LPT	FGC	OT	TT-O
Valves - Gas	12	3	2	5	5	0	0
Flanges - Gas	37	15	9	24	33	3	2
Compressor Seals - Gas	0	0	0	0	3	0	0
Relief Valves - Gas	1	3	1	1	1	1	1
Open-Ended Lines - Gas	0	0	0	0	0	0	0
Valves - Light Oil	0	5	6	12	3	6	9
Connectors - Light Oil	0	20	24	48	12	24	30
Pump Seals - Light Oil	0	0	0	0	0	0	0
Other - Light Oil	0	0	0	0	0	0	0

Equipment Type	WH	GPU	HT	LPT	FGC	OT	TT-O
Number of Each Type On Pad =	2	2	1	0	0	6	1

SWN Production Company, LLC
John Harwatt Pad
Fugitive Emissions Calculations (Continued)

Speciated Gas Analysis[4]

Component	Molecular Weight	Mole %	Equiv. Wt. Basis	Weight %	HC Weight %	lb/hr	TPY
Hydrogen Sulfide	34.082	0.0000%	0.0000	0.0000%	-	0.00	0.00
Carbon Dioxide	44.010	0.1160%	0.0511	0.2207%	-	<0.01	0.01
Nitrogen	28.013	0.5180%	0.1451	0.6274%	-	<0.01	0.02
Methane	16.042	68.4810%	10.9857	47.4976%	47.9039%	0.35	1.55
Ethane	30.069	18.5940%	5.5910	24.1732%	24.3800%	0.18	0.79
Propane	44.096	7.8410%	3.4576	14.9491%	15.0769%	0.11	0.49
i-Butane	58.122	0.7440%	0.4324	1.8696%	1.8856%	0.01	0.06
n-Butane	58.122	2.2480%	1.3066	5.6491%	5.6974%	0.04	0.18
i-Pentane	72.149	0.3690%	0.2662	1.1511%	1.1609%	0.01	0.04
n-Pentane	72.149	0.6010%	0.4336	1.8748%	1.8908%	0.01	0.06
n-Hexane	86.175	0.1460%	0.1258	0.5440%	0.5486%	<0.01	0.02
Other Hexanes	86.175	0.1540%	0.1327	0.5738%	0.5787%	<0.01	0.02
Heptanes (as n-Heptane)	100.202	0.1080%	0.1082	0.4679%	0.4719%	<0.01	0.02
Benzene	78.114	0.0020%	0.0016	0.0068%	0.0068%	<0.01	<0.01
Toluene	92.141	0.0030%	0.0028	0.0120%	0.0121%	<0.01	<0.01
Ethylbenzene	106.167	0.0000%	0.0000	0.0000%	0.0000%	0.00	0.00
Xylenes	106.167	0.0020%	0.0021	0.0092%	0.0093%	<0.01	<0.01
2,2,4-Trimethylpentane	114.230	0.0000%	0.0000	0.0000%	0.0000%	0.00	0.00
Octanes (as n-Octane)	114.229	0.0550%	0.0628	0.2716%	0.2740%	<0.01	0.01
Nonanes (as n-Nonane)	128.255	0.0140%	0.0180	0.0776%	0.0783%	<0.01	<0.01
Decanes (as n-Decane)	142.282	0.0040%	0.0057	0.0246%	0.0248%	<0.01	<0.01
	TOTAL =	**100.00%**	**23.13**	**100.00%**	**100.00%**	**0.75**	**3.27**
		TOTAL HC =	**22.93**	**TOTAL VOC =**	**27.72%**	**0.20**	**0.90**
				TOTAL HAP =	**0.58%**	**<0.01**	**0.02**

SWN Production Company, LLC
John Harwatt Pad
Fugitive Emissions Calculations (Continued)

Speciated Liquids Analysis[4]

Component	Molecular Weight	Mole %	Equiv. Wt. Basis	Weight %	HC Weight %	lb/hr	TPY
Hydrogen Sulfide	34.082	0.000%	0.000	0.0000%	-	0.00	0.00
Carbon Dioxide	44.010	0.013%	0.006	0.0066%	-	<0.01	<0.01
Nitrogen	28.013	0.013%	0.004	0.0042%	-	<0.01	<0.01
Methane	16.042	3.967%	0.636	0.7292%	0.7293%	<0.01	0.01
Ethane	30.069	7.341%	2.207	2.5293%	2.5296%	0.01	0.04
Propane	44.096	10.663%	4.702	5.3878%	5.3884%	0.02	0.09
i-Butane	58.122	2.266%	1.317	1.5092%	1.5093%	0.01	0.03
n-Butane	58.122	9.909%	5.759	6.5994%	6.6001%	0.03	0.12
i-Pentane	72.149	3.583%	2.585	2.9622%	2.9625%	0.01	0.05
n-Pentane	72.149	7.447%	5.373	6.1566%	6.1573%	0.02	0.11
n-Hexane	86.175	5.278%	4.548	5.2117%	5.2123%	0.02	0.09
Other Hexanes	86.175	4.697%	4.048	4.6380%	4.6385%	0.02	0.08
Heptanes (as n-Heptane)	100.202	8.611%	8.628	9.8870%	9.8880%	0.04	0.17
Benzene	78.114	0.075%	0.059	0.0671%	0.0671%	<0.01	<0.01
Toluene	92.141	0.315%	0.290	0.3326%	0.3326%	<0.01	0.01
Ethylbenzene	106.167	0.258%	0.274	0.3139%	0.3139%	<0.01	0.01
Xylenes	106.167	1.234%	1.310	1.5012%	1.5014%	0.01	0.03
2,2,4-Trimethylpentane	114.230	0.000%	0.000	0.0000%	0.0000%	0.00	0.00
Octanes (as n-Octane)	114.229	9.377%	10.711	12.2736%	12.2749%	0.05	0.21
Nonanes (as n-Nonane)	128.255	4.833%	6.199	7.1027%	7.1035%	0.03	0.12
Decanes (as n-Decane)	142.282	20.111%	28.614	32.7878%	32.7913%	0.13	0.57
	TOTAL =	**100.00%**	**87.27**	**100.00%**	**100.00%**	**0.40**	**1.75**
		TOTAL HC =	**87.26**	**TOTAL VOC =**	**96.74%**	**0.39**	**1.69**
				TOTAL HAP =	**7.43%**	**0.03**	**0.13**

Notes:

[1] Component counts taken by equipment type at representative facility and made site-specific according to the number of each equipment type at this site.

[2] Emission Factor Source: EPA-453/R-95-017. TOC multiplied by pollutant content of streams (weight %) to obtain pollutant emissions.

[3] Equipment Type Key: WH = Well Head, GPU = Gas Production Unit, HT = Heater Treater, LPT = Low-Pressure Tower, FGC = Flash Gas Compressor, OT = Oil Tank, TT-O = Tank Truck - Oil

[4] Analyses located in Attachment N.

SWN Production Company, LLC
John Harwatt Pad
Fugitive Unpaved Haul Road Emissions Calculations

Facility Data [1]

Vehicle Type	Light Vehicles (Pick-ups and Cars)	Medium Trucks (Service Trucks)	Heavy Trucks (Tanker Trucks)[2]
Average vehicle weight ((empty + full)/2) (tons)	2	15	23.5
Number of wheels per vehicle type (w)	4	10	18
Average number of round trips/day/vehicle type	1.00	1.00	1.47
Distance per round trip (miles/trip)	0.74	0.74	0.74
Vehicle miles travelled (miles/day)	0.74	0.74	1.09
Number of days operational (days/yr)	365	365	365
Vehicle miles travelled VMT (miles/yr)	269.60	269.60	397.31
Average vehicle speed S (mph)	10	10	10
Average number of round trips/hour/vehicle type	0.06	0.06	0.08
Average number of round trips/year/vehicle type	365	365	538
Estimated maximum number of round trips/hour/vehicle type	3	3	2
Estimated maximum number of round trips/day/vehicle type	7	4	4
Estimated maximum number of round trips/year/vehicle type	2,683	1,533	1,533

190	Average Tanker Volume (bbl)
7,980	Gallons Tanker Volume
100	bwpd
180	bopd
1.47	Tanker Trucks per Day
1,500	Length Leased Access Road (ft)
450	Longest Pad Side (ft)
3,900	Total Round Trip Feet

Formula & Calculation Inputs

$E=k(s/12)^a * (W/3)^b * ((365-P) / 365)$

Reference : AP-42, Section 13.2.2 (11/06), Equation 1a and 2

where:	Rate	Units	Comment
Days per year	365		
Annual average hours per day of road operations	18		
k = PM Particle Size Multiplier	4.90	lb/VMT	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2 (PM)
k = PM10 Particle Size Multiplier	1.50	lb/VMT	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2 (PM_{10})
k = PM2.5 Particle Size Multiplier	0.15	lb/VMT	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2 ($PM_{2.5}$)
s = Surface Material Silt Content	3.9	%	State Default Data from AP-42 Data (1999 NEI Data)
P = Number of days > 0.01 inch of rain	150	days/year	AP-42 Section 13.2.2 (11/06), Figure 13.2.2-1
a = PM Constant	0.70	unitless	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2 (PM)
a = PM10 & PM2.5 Constant	0.90	unitless	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2 (PM_{10} & $PM_{2.5}$)
b = PM, PM10, & PM2.5 Constant	0.45	unitless	AP-42 Section 13.2.2 (11/06), Table 13.2.2-2
Total hourly fleet vehicle miles travelled (miles/hr)	0.14	VMT/hr	
Total annual fleet vehicle miles travelled (miles/yr)[3]	936.51	VMT/yr	
Average wheels[4]	12		
Average vehicle weight of the fleet (W)[5]	14.9	tons	
Moisture Ratio	1.00		Estimated based on 0.2% uncontrolled surface water content assuming no watering — EPA - BID Document 13.2.2 - 1998
Control Efficiency (CF)	0.00	%	Based on Moisture Ratio and Figure 13.2.2-2 Control

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SWN Production Company, LLC
John Harwatt Pad
Fugitive Unpaved Haul Road Emissions Calculations

Emission Calculations

Vehicle Type	Emission Factors			Control Efficiency	Total Vehicle Miles Travelled		Uncontrolled Emission Rates			Uncontrolled Emission Rates		
	PM	PM_{10}	$PM_{2.5}$				Total PM	Total PM_{10}	$PM_{2.5}$	Total PM	Total PM_{10}	$PM_{2.5}$
	(lbs/VMT)	(lbs/VMT)	(lbs/VMT)	(%)	(VMT/hr)	(VMT/yr)	(lb/hr)	(lb/hr)	(lb/hr)	(tons/yr)	(tons/yr)	(tons/yr)
Light Vehicles	2.70	0.66	0.07	0.00	0.04	269.60	0.11	0.03	<0.01	0.36	0.09	0.01
Medium Trucks	2.70	0.66	0.07	0.00	0.04	269.60	0.11	0.03	<0.01	0.36	0.09	0.01
Heavy Trucks	2.70	0.66	0.07	0.00	0.06	397.31	0.16	0.04	<0.01	0.54	0.12	0.01
			Total =	0.00	0.14	936.51	0.38	0.10	0.01	1.26	0.30	0.03

Notes:

1) Facility vehicle data based on estimates, GP5.1 and AP-42 13.2.2-2 defaults for industrial unpaved roads
2) Tank trucker average vehicle weight as $(W_{(empty)}+W_{(full)})/2 = (7 + 40)/2 = 23.7$ tons
3) Average vehicle miles travelled (VMT/yr) as (No. of round trip/vehicle * No. of vehicles/type * Roundtrip miles/trip)* 365 days/yr * No. of vehicle type)
4) Average wheels calculated as average of (No. of wheels per vehicle type * No. of vehicle/type)
5) Average vehicle fleet calculated as (Average weight of vehicle type * Percentage of each vehicle type on unpaved surface). Percentage of each vehicle type= $VMT_{vehicle\ type}/VMT$
6) Minimum one-per-day average pick-up trucks and service trucks even if tanker not required every day.
7) Per EPA BID calculations, all emissions based on average trips. Estimated maximum hourly, daily and yearly trips provided for information only.

Calculation of Emission Factors (AP-42, 13.2.2)

Equation 1a: $EF = k(s/12)^a (W/3)^b$ *where k, a, and b are empirical constants and*

EF = size-specific emission factor (lb/VMT)

s = surface material silt content %

W = mean vehicle weight (tons)

Equation 2: $EF_{ext} = EF*((365-P)/365)$ *where:*

EF_{ext} *= annual size-specific emission factor extrapolated for natural mitigation, lb/VMT*

EF = emission factor from Equation 1a

P = number of days in a year with at least 0.01 inches of precipitation

Calculation of Emissions

$E = EF_{ext} * VMT/yr * ((1-CF)/100) * 1\ ton/2000\ lbs$ *where:*

E = annual emissions (tons/yr)

EF_{ext} *= annual size-specific emission factor extrapolated for natural mitigation, lb/VMT*

CF = control efficiency (%)

TABLE 1-C

COMPOSITIONAL ANALYSIS OF THE SEPARATOR GAS, OIL AND MATHEMATICALLY RECOMBINED WELLSTREAM THROUGH C_{31+}

SEPARATOR GOR.....: 6920 Scf/Sep Bbl
SEPARATOR PRESSURE.....: 196 psig
SEPARATOR TEMPERATURE.....: 80 °F

	SEPARATOR GAS		SEPARATOR OIL		WELLSTREAM	
Component	Mole%	* GPM	Mole %	Liquid Volume %	Mole %	* GPM
Hydrogen Sulfide	0.000	0.000	0.000	0.000	0.000	0.000
Nitrogen	0.518	0.000	0.013	0.003	0.457	0.000
Carbon Dioxide	0.116	0.000	0.013	0.005	0.103	0.000
Methane	68.481	0.000	3.967	1.557	60.641	0.000
Ethane	18.594	5.013	7.341	4.548	17.226	4.645
Propane	7.841	2.175	10.663	6.797	8.184	2.270
Iso-butane	0.744	0.245	2.266	1.716	0.929	0.306
N-butane	2.248	0.714	9.909	7.232	3.179	1.010
2-2 Dimethylpropane	0.023	0.009	0.061	0.054	0.028	0.011
Iso-pentane	0.369	0.136	3.583	3.037	0.760	0.280
N-pentane	0.573	0.209	7.386	6.198	1.401	0.512
2-2 Dimethylbutane	0.005	0.002	0.096	0.093	0.016	0.007
Cyclopentane	0.005	0.001	0.000	0.000	0.004	0.001
2-3 Dimethylbutane	0.010	0.004	0.239	0.227	0.038	0.016
2 Methylpentane	0.079	0.033	2.207	2.121	0.338	0.141
3 Methylpentane	0.045	0.019	1.360	1.286	0.205	0.084
Other Hexanes	0.000	0.000	0.000	0.000	0.000	0.000
n-Hexane	0.146	0.061	5.278	5.027	0.770	0.319
Methylcyclopentane	0.011	0.004	0.632	0.518	0.086	0.031
Benzene	0.002	0.001	0.075	0.048	0.011	0.003
Cyclohexane	0.015	0.005	0.795	0.627	0.110	0.038
2-Methylhexane	0.019	0.009	1.704	1.835	0.224	0.105
3-Methylhexane	0.020	0.009	1.571	1.670	0.208	0.096
2,2,4 Trimethylpentane	0.000	0.000	0.000	0.000	0.000	0.000
Other Heptanes	0.017	0.007	0.734	0.740	0.104	0.046
n-Heptane	0.041	0.019	3.970	4.242	0.518	0.241
Methylcyclohexane	0.017	0.007	1.714	1.596	0.223	0.090
Toluene	0.003	0.001	0.315	0.244	0.041	0.014
Other C-8's	0.028	0.013	5.039	5.471	0.637	0.301
n-Octane	0.010	0.005	2.624	3.112	0.328	0.169
Ethylbenzene	0.000	0.000	0.258	0.231	0.031	0.012
M&P-Xylene	0.002	0.001	0.518	0.465	0.065	0.025
O-Xylene	0.000	0.000	0.716	0.631	0.087	0.033
Other C-9's	0.011	0.006	3.136	3.803	0.391	0.206
n-Nonane	0.003	0.002	1.697	2.212	0.209	0.119
Other C10's	0.003	0.002	3.432	4.573	0.420	0.243
n-Decane	0.001	0.001	1.084	1.541	0.133	0.082
Undecanes	0.000	0.000	3.626	4.957	0.441	0.262
Dodecanes	0.000	0.000	2.763	4.081	0.336	0.216
Tridecanes	0.000	0.000	2.225	3.523	0.270	0.186

TABLE 1-C

COMPOSITIONAL ANALYSIS OF THE SEPARATOR GAS, OIL AND MATHEMATICALLY RECOMBINED WELLSTREAM THROUGH C_{31+}

SEPARATOR GOR.....: 6920 Scf/Sep Bbl
SEPARATOR PRESSURE.....: 196 psig
SEPARATOR TEMPERATURE.....: 80 °F

	SEPARATOR GAS		SEPARATOR OIL		WELLSTREAM	
Component	Mole%	* GPM	Mole %	Liquid Volume %	Mole %	* GPM
Tetradecanes	0.000	0.000	1.815	3.078	0.221	0.163
Pentadecanes	0.000	0.000	1.340	2.435	0.163	0.129
Hexadecanes	0.000	0.000	0.969	1.882	0.118	0.100
Heptadecanes	0.000	0.000	0.767	1.575	0.093	0.083
Octadecanes	0.000	0.000	0.575	1.243	0.070	0.066
Nonadecanes	0.000	0.000	0.441	0.994	0.054	0.053
Eicosanes	0.000	0.000	0.323	0.757	0.039	0.040
Heneicosanes	0.000	0.000	0.233	0.574	0.028	0.030
Docosanes	0.000	0.000	0.178	0.457	0.022	0.024
Tricosanes	0.000	0.000	0.127	0.335	0.015	0.018
Tetracosanes	0.000	0.000	0.089	0.245	0.011	0.013
Pentacosanes	0.000	0.000	0.056	0.162	0.007	0.009
Hexacosanes	0.000	0.000	0.031	0.093	0.004	0.005
Heptacosanes	0.000	0.000	0.012	0.038	0.001	0.002
Octacosanes	0.000	0.000	0.008	0.025	0.001	0.001
Nonacosanes	0.000	0.000	0.007	0.022	0.001	0.001
Triacontanes	0.000	0.000	0.005	0.015	0.001	0.001
Hentriacontanes Plus	0.000	0.000	0.012	0.047	0.001	0.003
TOTALS	100.000	8.713	100.000	100.000	100.000	12.861

TOTAL SAMPLE CHARACTERISTICS						
	Specific Gravity		Molecular Weight	Vapor Volume	Gross Heating Value	
COMPONENT	°API	**	lb/lb-mole	Scf/Gal	Dry ***	Saturated ***
Gas	N/A	0.8021	23.124	114.767	1,400	1,377
Oil	73.283	0.6910	94.140	22.981	N/A	116,166
Wellstream	N/A	1.0964	31.754	42.939	N/A	N/A

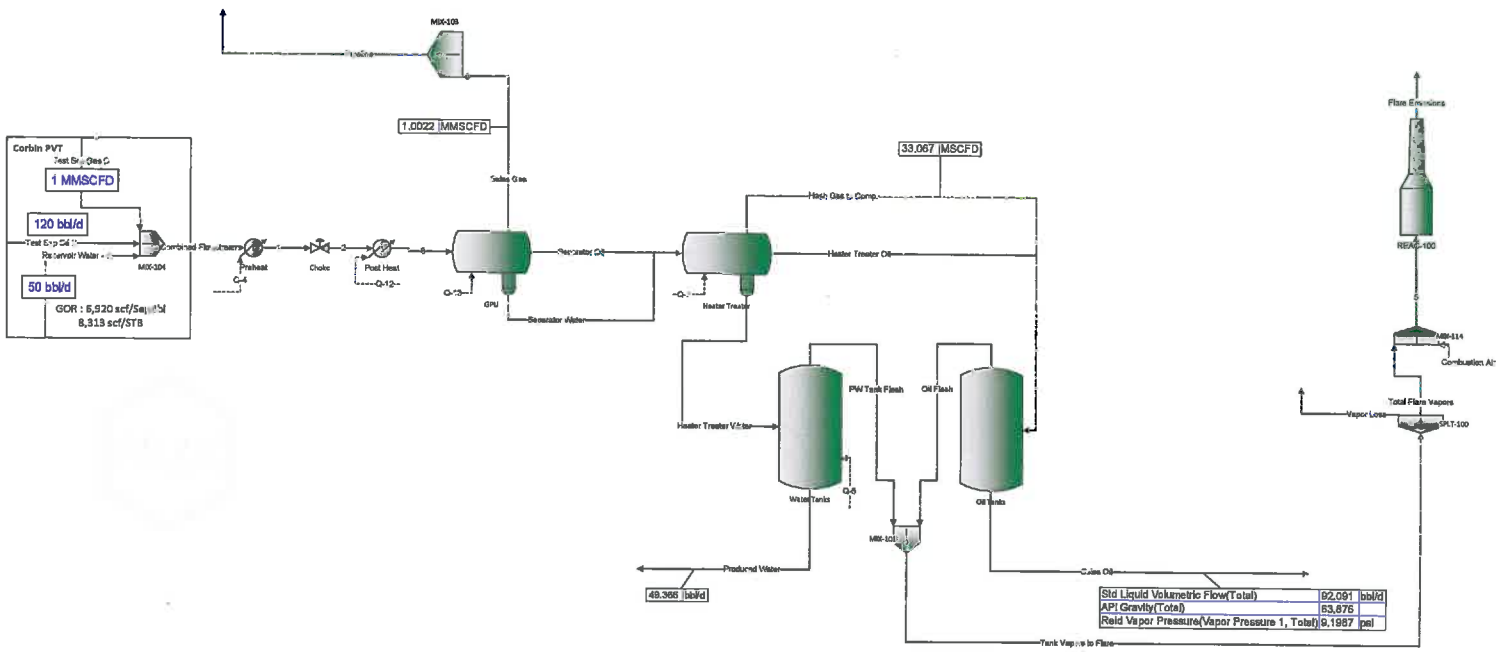
* GPM (gallons per Mscf) determined at 14.85 psia and 60 °F

** Gas specific gravity and wellstream specific gravity determined relative to air (SG=1.000).
Oil specific gravity determined relative to water (SG=1.000).

*** Gross Heating Value units for gas (real basis) and oil are BTU/Scf and BTU/Gal, respectively.

Process Simulation Results

Names	Units	Reservoir Water - C	Test Sep Gas C	Test Sep Oil C	Oil Flash	PW Tank Flash	Sales Gas	Sales Oil	Produced Water
Temperature	°F	80*	80*	80*	98.516	85	92*	98.516	85#
Pressure	psia	210.7*	210.7*	210.7*	15.196	15.196	244.7*	15.196*	15.196*
Mole Fraction Vapor	%	0	99.965	0	100	100	100	0	0
Mole Fraction Light Liquid	%	100	0.034934	100	0	0	0	100	100
Mole Fraction Heavy Liquid	%	0	0	0	0	0	0	0	0
Molecular Weight	lb/lbmol	18.015	23.124	95.66	45.946	38.306	23.144	121.79	18.016
Molar Flow	lbmol/h	40.494	109.8	12.328	4.6703	0.00063765	110.04	7.934	39.976
Mass Flow	lb/h	729.5	2539	1179.3	214.58	0.024426	2546.8	966.29	720.21
Enthalpy	Btu/h	-4.9738e+006	-3.868e+006	-1.1153e+006	-2.3056e+005	-28.989	-3.8907e+006	-8.6128e+005	-4.907e+006
Nitrogen(Mole Fraction)	%	0*	0.518*	0.013*	0.039914	0.042955	0.51662	6.6686e-005	4.9596e-007
CO2(Mole Fraction)	%	0*	0.116*	0.013*	0.073947	0.15081	0.11396	0.0011422	6.8737e-005
C1(Mole Fraction)	%	0*	68.481*	3.9671*	14.622	21.751	68.149	0.071423	0.00051421
C2(Mole Fraction)	%	0*	18.594*	7.3411*	19.316	26.293	18.518	0.52416	0.00070546
C3(Mole Fraction)	%	0*	7.841*	10.663*	23.298	23.551	7.8764	2.1207	0.0008551
Isobutane(Mole Fraction)	%	0*	0.744*	2.266*	4.2668	2.3534	0.74695	0.94565	2.3185e-005
n-Butane(Mole Fraction)	%	0*	2.248*	9.9092*	16.334	13.449	2.2963	5.0416	0.00029683
2,2-Dimethylpropane(Mole Fraction)	%	0*	0.023*	0.061001*	0.15437	0.067117	0.018499	0.065628	6.4713e-007
Isopentane(Mole Fraction)	%	0*	0.369*	3.5831*	4.0691	2.1066	0.37421	3.0886	3.0713e-005
n-Pentane(Mole Fraction)	%	0*	0.573*	7.3861*	7.0939	3.8865	0.5917	7.024	5.7646e-005


Corbin PVT
1 MMSCFD
120 bbl/d
50 bbl/d
GOR : 6,920 scf/Sep bbl
8,313 scf/STB
MIX-304
Preheat
Choke
Post Heat
GPU
1.0022 MMSCFD
33.067 MSCFD
Heater Treater
Heater Treater Oil
Heater Treater Water
PW Tank Flash
Oil Flash
Water Tanks
Oil Tanks
Produced Water
49.366 bbl/d
Sales Oil
Std Liquid Volumetric Flow(Total) 92.091 bbl/d
API Gravity(Total) 53.876
Reid Vapor Pressure(Vapor Pressure 1, Total) 9.1987 psi
Tank Vapors to Flare
Flare Emissions
REAC-100
Combustion Air
Total Flare Vapors
Vapor Loss
SPLT-100

TANKS 4.0.9d
Emissions Report - Summary Format
Tank Indentification and Physical Characteristics

Identification

User Identification:	Jon Harwatt Oil Tanks
City:	
State:	
Company:	
Type of Tank:	Vertical Fixed Roof Tank
Description:	Corbin PVT

Tank Dimensions

Shell Height (ft):	20.00
Diameter (ft):	12.00
Liquid Height (ft) :	19.00
Avg. Liquid Height (ft):	10.00
Volume (gallons):	16,074.56
Turnovers:	171.66
Net Throughput(gal/yr):	2,759,400.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft)	0.00
Slope (ft/ft) (Cone Roof)	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig)	0.03

Meterological Data used in Emissions Calculations: Pittsburgh, Pennsylvania (Avg Atmospheric Pressure = 14.11 psia)

TANKS 4.0.9d
Emissions Report - Summary Format
Liquid Contents of Storage Tank

Jon Harwatt Oil Tanks - Vertical Fixed Roof Tank

Mixture/Component	Month	Daily Liquid Surf. Temperature (deg F) Avg.	Min.	Max.	Liquid Bulk Temp (deg F)	Vapor Pressure (psia) Avg.	Min.	Max.	Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Corbin PVT	All	51.94	47.06	56.81	50.33	5.4184	4.9673	5.9008	23.4250			123.39	Option 4: RVP=8.78

TANKS 4.0.9d
Emissions Report - Summary Format
Individual Tank Emission Totals

Emissions Report for: Annual

Jon Harwatt Oil Tanks - Vertical Fixed Roof Tank

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Corbin PVT	2,135.40	342.89	2,478.29

TANKS 4.0.9d
Emissions Report - Summary Format
Tank Indentification and Physical Characteristics

Identification

User Identification:	John Harwatt Produced Water Tanks
City:	
State:	
Company:	
Type of Tank:	Vertical Fixed Roof Tank
Description:	99% Water, 1% Corbin PVT

Tank Dimensions

Shell Height (ft):	20.00
Diameter (ft):	12.00
Liquid Height (ft) :	19.00
Avg. Liquid Height (ft):	10.00
Volume (gallons):	16,074.56
Turnovers:	95.37
Net Throughput(gal/yr):	1,533,000.00
Is Tank Heated (y/n):	N

Paint Characteristics

Shell Color/Shade:	White/White
Shell Condition	Good
Roof Color/Shade:	White/White
Roof Condition:	Good

Roof Characteristics

Type:	Cone
Height (ft)	0.00
Slope (ft/ft) (Cone Roof)	0.06

Breather Vent Settings

Vacuum Settings (psig):	-0.03
Pressure Settings (psig)	0.03

Meterological Data used in Emissions Calculations: Pittsburgh, Pennsylvania (Avg Atmospheric Pressure = 14.11 psia)

TANKS 4.0.9d
Emissions Report - Summary Format
Liquid Contents of Storage Tank

John Harwatt Produced Water Tanks - Vertical Fixed Roof Tank

Mixture/Component	Month	Daily Liquid Surf. Temperature (deg F) Avg.	Min.	Max.	Liquid Bulk Temp (deg F)	Vapor Pressure (psia) Avg.	Min.	Max.	Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Produced Water	All	51.94	47.06	56.81	50.33	0.1988	0.1663	0.2368	18.2370			18.18	
Corbin PVT						5.4184	4.9673	5.9008	23.4250	0.0100	0.0516	123.39	Option 4: RVP=8.78
Water						0.1911	0.1592	0.2284	18.0200	0.9900	0.9484	18.02	Option 2: A=8.10765, B=1750.286, C=235

TANKS 4.0.9d
Emissions Report - Summary Format
Individual Tank Emission Totals

Emissions Report for: Annual

John Harwatt Produced Water Tanks - Vertical Fixed Roof Tank

	Losses(lbs)		
Components	Working Loss	Breathing Loss	Total Emissions
Produced Water	47.76	9.70	57.46
Water	45.29	9.20	54.49
Corbin PVT	2.46	0.50	2.96