



WEST VIRGINIA  
DEPARTMENT OF ENVIRONMENTAL PROTECTION  
DIVISION OF AIR QUALITY  
601 57<sup>th</sup> Street, SE  
Charleston, WV 25304  
Phone: (304) 926-0475  
www.dep.wv.gov/daq

**PERMIT DETERMINATION FORM  
(PDF)**

FOR AGENCY USE ONLY: PLANT I.D. # \_\_\_\_\_  
PDF # \_\_\_\_\_ PERMIT WRITER: \_\_\_\_\_

1. NAME OF APPLICANT (AS REGISTERED WITH THE WV SECRETARY OF STATE'S OFFICE):

Noble Energy, Inc.

2. NAME OF FACILITY (IF DIFFERENT FROM ABOVE):

Sand Hill 1 (SHL 1)

3. NORTH AMERICAN INDUSTRY  
CLASSIFICATION SYSTEM (NAICS)  
CODE:

2 1 1 1 1 1

4A. MAILING ADDRESS:  
1000 Noble Energy Drive  
Canonsburg, PA 15317

4B. PHYSICAL ADDRESS:  
1610 Luke Ln  
Wheeling, WV

5A. DIRECTIONS TO FACILITY (PLEASE PROVIDE MAP AS ATTACHMENT A):

From Interstate 70, take Dallas Pike Road Exit (Exit 11), at bottom of ramp, make a right if traveling east or left if traveling west onto CR 41 (Dallas Pike Road), and travel Dallas Pike Road approximately 4.9 miles to the town of Dallas, make a right onto CR 7 (Stone Church/Sand Hill Road), make a right onto Stone Church/Sand Hill Road and travel approximately 5.1 miles to the Sand Hill Church, turn vehicle around at church and travel back approximately 1.1 miles to CR 22 (Luke Lane), make a right onto Luke Lane and travel approximately 1.6 miles to lease road on left.

5B. NEAREST ROAD:

Stone Church / Sand Hill Rd.

5C. NEAREST CITY OR TOWN:

Dallas, WV

5D. COUNTY:

Marshall

5E. UTM NORTHING (KM):

536.3150

5F. UTM EASTING (KM):

4424.8828

5G. UTM ZONE:

17N

6A. INDIVIDUAL TO CONTACT IF MORE INFORMATION IS REQUIRED:

Phil Schlagel

6B. TITLE:

Air Quality Manager

6C. TELEPHONE:

281-872-3202

6D. FAX:

6E. E-MAIL:

phil.schlagel@nblenergy.com

7A. DAQ PLANT I.D. NO. (FOR AN EXISTING FACILITY ONLY):

\_\_\_\_\_

7B. PLEASE LIST ALL CURRENT 45CSR13, 45CSR14, 45CSR19 AND/OR TITLE V (45CSR30) PERMIT NUMBERS ASSOCIATED WITH THIS PROCESS (FOR AN EXISTING FACILITY ONLY):

7C. IS THIS PDF BEING SUBMITTED AS THE RESULT OF AN ENFORCEMENT ACTION? IF YES, PLEASE LIST:

8A. TYPE OF EMISSION SOURCE (CHECK ONE):

NEW SOURCE  ADMINISTRATIVE UPDATE

MODIFICATION  OTHER (PLEASE EXPLAIN IN 11B)

8B. IF ADMINISTRATIVE UPDATE, DOES DAQ HAVE THE APPLICANT'S CONSENT TO UPDATE THE EXISTING PERMIT WITH THE INFORMATION CONTAINED HEREIN?

YES  NO

9. IS DEMOLITION OR PHYSICAL RENOVATION AT AN EXISTING FACILITY INVOLVED?  YES  NO

10A. DATE OF ANTICIPATED INSTALLATION OR CHANGE:

\_\_\_\_/\_\_\_\_/20\_\_

10B. DATE OF ANTICIPATED START-UP:

\_\_\_\_/\_\_\_\_/20\_\_

11A. PLEASE PROVIDE A DETAILED PROCESS FLOW DIAGRAM SHOWING EACH PROPOSED OR MODIFIED PROCESS EMISSION POINT AS ATTACHMENT B.

11B. PLEASE PROVIDE A DETAILED PROCESS DESCRIPTION AS ATTACHMENT C.

12. PLEASE PROVIDE MATERIAL SAFETY DATA SHEETS (MSDS) FOR ALL MATERIALS PROCESSED, USED OR PRODUCED AS ATTACHMENT D. FOR CHEMICAL PROCESSES, PLEASE PROVIDE A MSDS FOR EACH COMPOUND EMITTED TO AIR.

**13A. REGULATED AIR POLLUTANT EMISSIONS:**

⇒ **FOR A NEW FACILITY**, PLEASE PROVIDE PLANT WIDE EMISSIONS BASED ON THE POTENTIAL TO EMIT (PTE) FOR THE FOLLOWING AIR POLLUTANTS INCLUDING ALL PROCESSES.

⇒ **FOR AN EXISTING FACILITY**, PLEASE PROVIDE THE PROPOSED CHANGE IN EMISSIONS BASED ON THE PTE OF ALL PROCESS CHANGES FOR THE FOLLOWING AIR POLLUTANTS.

*PTE FOR A GIVEN POLLUTANT IS TYPICALLY BEFORE AIR POLLUTION CONTROL DEVICES AND IS COLLECTED BASED ON THE MAXIMUM DESIGN CAPACITY OF PROCESS EQUIPMENT.*

POLLUTANT	HOURLY PTE (LB/HR)	YEARLY PTE (TON/YR) (HOURLY PTE MULTIPLIED BY 8760 HR/YR) DIVIDED BY 2000 LB/TON
PM	0.03	0.14
PM <sub>10</sub>	0.03	0.14
VOCs	2.89	12.64
CO	0.35	1.52
NO <sub>x</sub>	0.41	1.81
SO <sub>2</sub>	0.00	0.01
Pb	0.00	0.00
HAPs (AGGREGATE AMOUNT)	0.23	0.99
TAPs (INDIVIDUALLY)*	0.05	0.21
OTHER (INDIVIDUALLY)*		

\* ATTACH ADDITIONAL PAGES AS NEEDED

**13B. PLEASE PROVIDE ALL SUPPORTING CALCULATIONS AS ATTACHMENT E.**

*CALCULATE AN HOURLY AND YEARLY PTE OF EACH PROCESS EMISSION POINT (SHOWN IN YOUR DETAILED PROCESS FLOW DIAGRAM) FOR ALL AIR POLLUTANTS LISTED ABOVE INCLUDING INDIVIDUAL HAP'S (LISTED IN SECTION 112[b] OF THE 1990 CAAA), TAP'S (LISTED IN 45CSR27), AND OTHER AIR POLLUTANTS (E.G. POLLUTANTS LISTED IN TABLE 45-13A OF 45CSR13, MINERAL ACIDS PER 45CSR7, ETC.).*

**14. CERTIFICATION OF DATA**

I, RJ Moses (TYPE NAME) ATTEST THAT ALL THE REPRESENTATIONS CONTAINED IN THIS APPLICATION, OR APPENDED HERETO, ARE TRUE, ACCURATE, AND COMPLETE TO THE BEST OF MY KNOWLEDGE BASED ON INFORMATION AND BELIEF AFTER REASONABLE INQUIRY, AND THAT I AM A **RESPONSIBLE OFFICIAL**\*\* (PRESIDENT, VICE PRESIDENT, SECRETARY OR TREASURER, GENERAL PARTNER OR SOLE PROPRIETOR) OF THE APPLICANT.

SIGNATURE OF RESPONSIBLE OFFICIAL: \_\_\_\_\_

TITLE: Operations Manager

DATE: 10 / 24 / 16

\*\* THE DEFINITION OF THE PHRASE 'RESPONSIBLE OFFICIAL' CAN BE FOUND AT 45CSR13, SECTION 2.23.

**NOTE: PLEASE CHECK ENCLOSED ATTACHMENTS:**

ATTACHMENT A     ATTACHMENT B     ATTACHMENT C     ATTACHMENT D     ATTACHMENT E

RECORDS ON ALL CHANGES ARE REQUIRED TO BE KEPT AND MAINTAINED ON-SITE FOR TWO (2) YEARS.

THE PERMIT DETERMINATION FORM WITH THE INSTRUCTIONS CAN BE FOUND ON DAQ'S PERMITTING SECTION WEB SITE:

[www.dep.wv.gov/daq](http://www.dep.wv.gov/daq)

**Noble Energy, Inc.**  
**SHL 1 Production Facility**  
**Permit Determination**

**INTRODUCTION NARRATIVE**

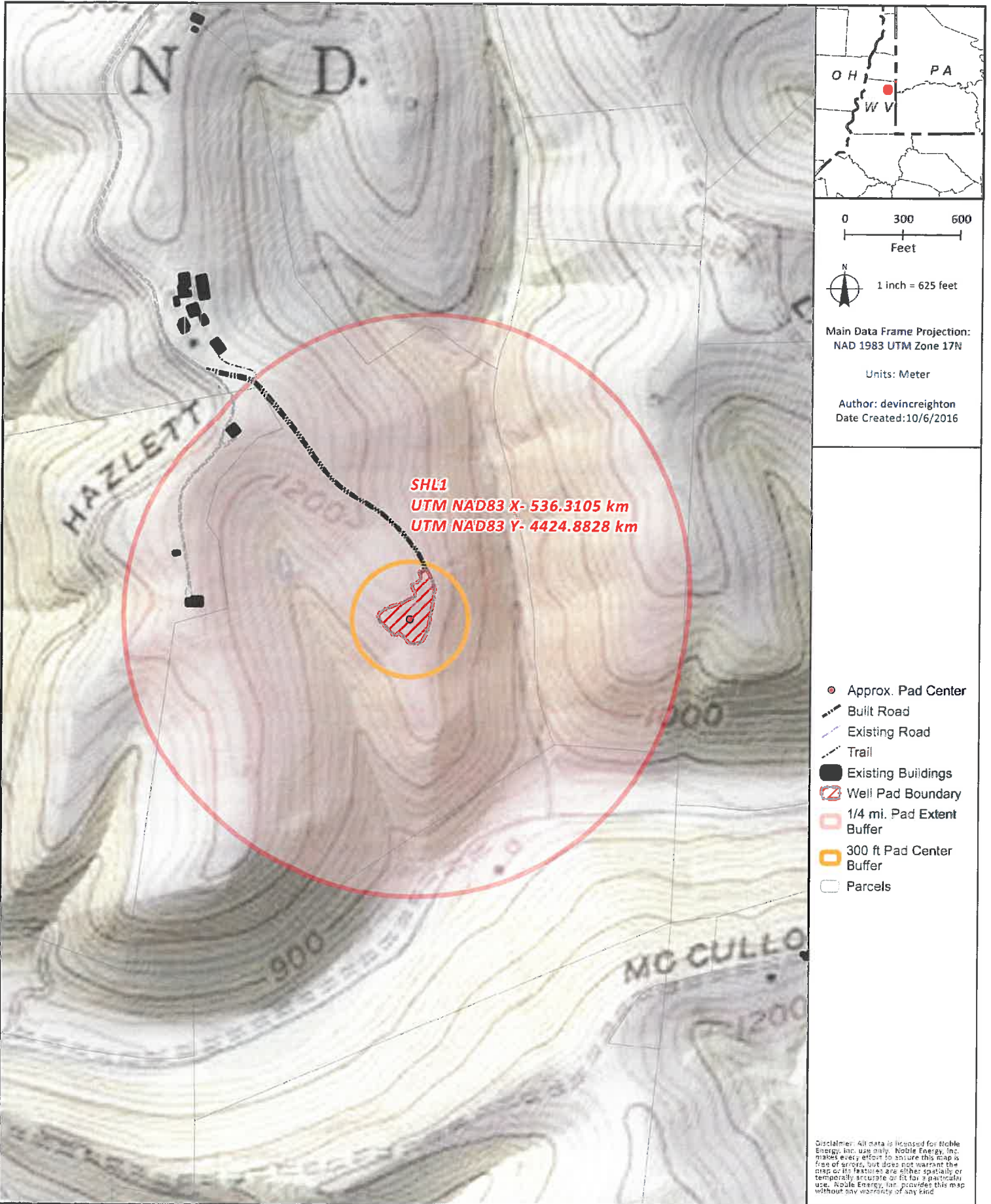
Noble Energy, Inc. (Noble) operates an oil and natural gas production facility at the SHL 1 well pad, located in Marshall County, West Virginia. The well pad consists of 5 natural gas wells, 5 gas production units and associated heaters, 2 - 400 bbl Prod Water Storage Tanks and a produced water truck loadout.

Noble has estimated that potential and actual emissions from the production facility have not and will not exceed the WV 45CSR13 permitting thresholds. The produced water production used in this determination is the maximum actual production rate of any 12 months. Produced water production is expected to decline further through the life of the wells.

**SHL 1  
Permit Determination**

**ATTACHMENT A**

**MAP OF SHL 1 PRODUCTION FACILITY**



**SHL 1**  
**Permit Determination**

**ATTACHMENT B**

**PROCESS FLOW DIAGRAM**



**SHL 1**  
**Permit Determination**

**ATTACHMENT C**

**SHL 1 PROCESS DESCRIPTION**

The SHL 1 is an oil and gas production facility.

Condensate, gas, produced water and sand come from 5 natural gas wells through 5 sand separators.

Sand is routed from the sand separators to a sand storage box for disposal.

Condensate, gas and produced water are routed through 5 Gas Production Units (GPUs) with 5 - 1.0 MMBtu/hr Heaters where separation occurs.

The condensate and gas from the GPUs exit the facility via sales pipeline.

Produced water from the separators flows to 2 - 400 bbl Prod Water Storage Tanks.

Produced water is transported off-site by tanker truck or water pipeline.



**SHL 1**  
**Permit Determination**

**ATTACHMENT E**

**SUPPORTING CALCULATIONS**

SHL 1  
Emission Summary Sheet

Emission Unit ID Number	Source Description	Potential Emissions (tpy)														
		NOx	CO	VOC	SOx	PM	PM10	Formaldehyde	n-Hexane	Benzene	Toluene	Ethylbenzene	Xylene	2,2,4-TMP	Single HAP	Total HAPS
PW TK 1-2	400 bbl Prod Water Storage Tanks	---	---	0.58	---	---	---	---	---	---	---	---	---	---	---	---
GPU 1-5	1.0 MMBtu/hr Heaters	1.80	1.51	0.10	0.01	0.14	0.14	0.0013	0.0042	0.0005	0.0010	0.0001	0.0008	0.0000	0.0042	0.0066
TL	Produced Water Truck Loading Detail	---	---	0.05	---	---	---	---	0.0323	0.0000	0.0001	0.0000	0.0000	0.0000	0.0323	0.0339
FUG	Equipmt Component Fugitives Estimate	---	---	4.40	---	---	---	---	0.0091	0.0000	0.0003	0.0000	0.0009	0.0000	0.0091	0.0013
TE Gen	Thermo Electric Generator	0.02	0.01	0.00	0.00	0.00	0.00	---	0.16	0.01	0.04	0.01	0.07	0.1624	0.31	
Pneumatic Controllers	Pneumatic Controllers	---	---	8.09	---	---	---	---	---	---	---	---	---	---	---	---
<b>Total TPY</b>		<b>1.81</b>	<b>1.52</b>	<b>12.64</b>	<b>0.01</b>	<b>0.14</b>	<b>0.14</b>	<b>0.00</b>	<b>0.84</b>	<b>0.01</b>	<b>0.05</b>	<b>0.01</b>	<b>0.08</b>	<b>0.01</b>	<b>0.21</b>	<b>0.99</b>
<b>Total lb/hr</b>		<b>0.41</b>	<b>0.35</b>	<b>2.89</b>	<b>0.00</b>	<b>0.03</b>	<b>0.03</b>	<b>0.00</b>	<b>0.19</b>	<b>0.00</b>	<b>0.01</b>	<b>0.00</b>	<b>0.02</b>	<b>0.00</b>	<b>0.05</b>	<b>0.23</b>
<b>Total lb/day</b>		<b>9.93</b>	<b>8.32</b>	<b>69.28</b>	<b>0.06</b>	<b>0.75</b>	<b>0.75</b>	<b>0.01</b>	<b>4.60</b>	<b>0.05</b>	<b>0.26</b>	<b>0.08</b>	<b>0.45</b>	<b>0.07</b>	<b>1.14</b>	<b>5.44</b>

**SHL 1**

**Heater Detail Sheet**

Equipment ID GPU 1-5  
 Equipment Count 5  
 Equipment Usage 1.0 MMBtu/hr Heaters  
 Fuel Heating Value 1220 Btu/scf  
 Design Heat Rate\* 1.00 MMBtu/hr  
 Site Heat Rate\* 1.00 MMBtu/hr  
 Potential Operation 8760 hr/yr  
 Potential Fuel Usage 7.18 MMscf/yr

\* These are heat release rates and not the duty for the heater

*Potential Emissions*

Pollutant	Emission Factor (lb/MMscf)	Nominal Rating (MMBtu/hr)	Hrs of Operation (hrs/yr)	Estimated Emissions		Source of Emission Factor
				(lb/hr)	(tpy)	
NOx	100.00	5.000	8760	0.41	1.80	AP-42 <sup>1</sup>
CO	84.00	5.000	8760	0.34	1.51	AP-42 <sup>1</sup>
VOC	5.50	5.000	8760	0.02	0.10	AP-42 <sup>2</sup>
SO2	0.60	5.000	8760	0.00	0.01	AP-42 <sup>2</sup>
PM10	7.60	5.000	8760	0.03	0.14	AP-42 <sup>2</sup>
Benzene	0.002	5.000	8760	0.00	0.0000	AP-42 <sup>3</sup>
Toluene	0.003	5.000	8760	0.00	0.0001	AP-42 <sup>3</sup>
N-Hexane	1.80	5.000	8760	0.01	0.0323	AP-42 <sup>3</sup>
Formaldehyde	0.08	5.000	8760	0.00	0.0013	AP-42 <sup>3</sup>
Total HAPs	1.89	5.000	8760	0.01	0.03	AP-42 <sup>3</sup>
CO <sub>2</sub>	120000.00	5.000	8760	491.80	2154.10	AP-42 <sup>2</sup>
CH <sub>4</sub>	2.30	5.000	8760	0.01	0.04	AP-42 <sup>2</sup>
CO <sub>2</sub> e					2154.97	

<sup>1</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-1, Emission Factors for Nitrogen Oxides (NOx) and Carbon Monoxide (CO) from Natural Gas Combustion

<sup>2</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-2, Emission Factors for Criteria Pollutants and Greenhouse Gases from Natural Gas Combustion

<sup>3</sup> EPA AP-42, Volume I, Fifth Edition - July 1998, Table 1.4-3, Emission Factors for Speciated Organic Compounds from Natural Gas Combustion

**SHL 1  
Tank Detail Sheet**

Source ID Number	PW TK 1-2								
Equipment ID	PW TK								
Tank Description	400 bbl Prod Water Storage	Tank Potential operation							
Tank Usage	Produced Water Storage								
Tank Count	2								
Tank Capacity	400	bbl							
Tank Contents	Produced Water								
Emission Controls	NO								
Tank Orientation	Vertical, above ground								
Shell Height / Length	20 ft								
Shell Diameter	12 ft								
Roof Slope	0.06								
Roof Type (Cone, Dome, IFR, EFR, None)	Cone								

8760 hr/yr									
62,627 bbl/yr									
1.00 % Oil									
626.3 bbl/yr Oil									
0.01846 lb/bbl VOC from FESCO Flash Study									
0.00056 lb/bbl BTEX from FESCO Flash Study									

HYSYS Run, Water Out  
(Welded, Bolted, Fiberglass)  
(eg. light brown, good)  
(eg. white, fair)

Maximum water production	
Tank Construction	Welded
Roof color & condition	Gray/Medium, good
shell color & condition	Gray/Medium, good
FR Primary Seal	N/A
FR Secondary Seal	N/A

Vent pressure setting  
VOC Control Efficiency

0.03 +/- psig  
0 %

**Potential Emissions**

Pollutant	CAS	Hrs of Operation (hrs/yr)	Estimated Uncontrolled Emissions <sup>1</sup> (lb/hr)	(tpy)	(lb/yr)	Source of Emission Factor
VOC		8760	0.13	0.58	1156.09	FESCO Flash Study

Benzene	0.09	
Ethylbenzene	0.01	
Toluene	0.18	
Xylenes	0.14	
N-Hexane	0.72	
224-TMP	0.00	

tpy  
0.001  
0.000  
0.001  
0.001  
0.004  
0.000

# SHL 1

## Produced Water Truck Loading Detail

TL

Select Model Liquid --->

Gasoline RVP 7

or Enter These Factors Directly Below

**P=**            psia true vapor pressure  
**M=**            lb/lb-mol molecular weight of vapors  
  
**S=**  0.6 saturation factor  
**P<sub>v</sub>=**  4.3 psia true vapor pressure  
**M<sub>v</sub>=**  68 lb/lb-mol molecular weight of vapors  
**T=**  70 °F temperature  
**L<sub>1</sub>=** 4.12 lb/1000 gallons = 12.46\*S\*P\*M/(T+460)  
**L<sub>2</sub>=** 0.173 lb/bbl Loading Losses

Production: 62,627 bbl/year Produced Water  
 626 bbl/year oil based on 1% oil in the Produced Water  
 1.71580822 bbl/day

### Potential Emissions

Pollutant	Component		Component EF		Controlled	
	Wt%	lb/bbl	lb/yr	tpy	(lb/yr)	(tpy)
VOC	100%	0.173	108	108	0.0542	0.0542
TOTAL HAPS	2.3%	0.004	3	3	0.0013	0.0013
n-hexane	16.67%	0.029	18	18	0.0091	0.0091
224-TMP	0.00%	0.000	0	0	0.0000	0.0000
Benzene	0.04%	0.000	0	0	0.0000	0.0000
Toluene	0.49%	0.001	1	1	0.0003	0.0003
Ethylbenzene	0.19%	0.000	0	0	0.0000	0.0000
Xylene	1.62%	0.003	2	2	0.0009	0.0009

<sup>1</sup> EPA AP-42, Volume I, Fifth Edition - January 1995, Table 5.2-1, Saturation (S) Factors for Calculating Petroleum Liquid Loading Losses

<sup>2</sup> API Compendium of Greenhouse Gas Emissions Methodologies for the Oil and Natural Gas Industry, Table 5-12

**SHL 1**  
**Equip Component Fugitives Estimate**  
 FUG

	Counts	Emission Factor <sup>1</sup> lb/hr/component	% Control Efficiency	% VOC	VOC Emissions		Benzene lb/yr	Toluene lb/yr	E-Benzene lb/yr	Xylene lb/yr	n-Hexane lb/yr	224-TMP		%CH4	CH4 Emissions		CO <sub>2</sub> e tpy
					lb/hr	tpy						lb/yr	lb/yr		lb/hr	tpy	
Valve	Gas/Vapor	25	0.00992	0	0.04	0.17	0.05	0.11	0.01	0.17	3.63	0.00	0.00	59.83	0.15	0.65	13.65
	Light Liquid	40	0.00551	0	0.22	22.30	2.22	11.87	2.90	22.30	146.93	15.45	0.00	1.17	0.00	0.01	0.24
Pumps	Water/Oil	40	0.000216	0	0.00	0.02	0.09	0.47	0.11	0.87	0.58	0.00	0.00	1.17	0.00	0.00	0.01
	Seals																
Flanges	Light Liquid	0	0.02866	0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	1.17	0.00	0.00	0.00
	Water/Oil	0	0.0000529	0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	1.17	0.00	0.00	0.00
Open-Ended Lines	Gas/Vapor	25	0.00086	0	0.00	0.02	0.00	0.01	0.00	0.01	0.31	0.00	0.00	59.83	0.01	0.06	1.18
	Light Liquid	25	0.000243	0	0.01	0.03	0.06	0.33	0.08	0.61	4.05	0.43	0.00	100	0.01	0.03	0.56
	Water/Oil	30	0.00000617	0	0.00	0.00	0.00	0.01	0.00	0.02	0.01	0.00	0.00	100	0.00	0.00	0.02
Other	Gas/Vapor	0	0.00441	0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	59.83	0.00	0.00	0.00
	Light Liquid	0	0.00309	0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	100	0.00	0.00	0.00
	Water/Oil	0	0.00006	0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	100	0.00	0.00	0.00
Connectors	Gas/Vapor	10	0.0194	0	0.03	0.14	0.04	0.08	0.01	0.13	2.84	0.00	0.00	59.83	0.12	0.51	10.68
	Light Liquid	5	0.0165	0	0.08	0.36	0.83	4.44	1.08	8.35	55.00	5.78	0.00	100	0.08	0.36	7.59
	Water/Oil	35	0.0309	0	0.54	2.37	10.90	58.26	14.21	109.42	72.10	0.00	0.00	100	1.08	4.74	99.48
Total Emissions	Gas/Vapor	125	0.000441	0	0.01	0.04	0.01	0.02	0.00	0.04	0.81	0.00	0.00	59.83	0.03	0.14	3.03
	Light Liquid	125	0.000463	0	0.06	0.25	0.58	3.12	0.76	5.86	38.58	4.06	0.00	100	0.06	0.25	5.32
	Water/Oil	70	0.000243	0	0.01	0.04	0.17	0.92	0.22	1.72	1.13	0.00	0.00	100	0.02	0.07	1.56
					0.99	4.40	14.78	78.73	19.17	147.79	324.83	25.71		1.54	6.75	141.75	

1. Heavy liquids are defined as having vapor pressure 0.044 psia or less at 68°F. Light liquids are defined as having vapor pressure higher than 0.044 psia at 68°F.

2. Factors from EPA Document EPA-453/R-95-017, November 1995.

**SHL 1**

**Thermo Electric Generator**

Source ID Number TE Gen  
 Equipment ID TE Gen  
 Equipment Usage Thermo Electric Generator  
 Equipment Make Global Thermoelectric  
 Equipment Model Model 5220  
 Emission Controls None  
 Design Heat Rate\* 0.03 MMBtu/hr  
 Potential Operation 8760 hr/yr  
 Potential Fuel Usage 7.4 gal/day  
 Fuel Propane

*Potential Emissions*

Pollutant	Emission Factor (lb/10 <sup>3</sup> gal)	Nominal Rating (MMBtu/hr)	Hrs of Operation (hrs/yr)	Estimated Emissions		Source of Emission Factor
				(lb/hr)	(tpy)	
NOx	13.00	0.028	8760	0.00	0.02	AP-42 <sup>1</sup>
CO	7.50	0.028	8760	0.00	0.01	AP-42 <sup>1</sup>
TOC	1.00	0.028	8760	0.00	0.00	AP-42 <sup>1</sup>
SO2	0.10	0.028	8760	0.00	0.00	AP-42 <sup>1</sup>
PM10	0.70	0.028	8760	0.00	0.00	AP-42 <sup>1</sup>
CO <sub>2</sub>	12500.00	0.028	8760	3.85	16.88	AP-42 <sup>1</sup>
CH <sub>4</sub>	0.20	0.028	8760	0.00	0.00	AP-42 <sup>1</sup>

<sup>1</sup> EPA AP-42, Volume I, Fifth Edition - July 2008, Table 1.5-1, Emission Factors for LPG Combustion

**SHL 1**

**Pneumatic Controllers**

Equipment ID	CB PC	IB PC
Equipment Usage	Flow / Back Pressure Control	
Equipment Make	Fischer Control	
Equipment Model	DVS 6200	
Emission Controls	None	
Equipment Count	5	15
Design Flow*	19.83 SCFH	0.02 SCFH
Potential Operation Service	8760 hr/yr	8760
	NG	

*Potential Emissions*

Pollutant	% of VOC	Emission Factor (lb/SCF)	Hrs of Operation (hrs/yr)	Estimated Emissions		Source of Emission Factor
				(lb/hr)	(tpy)	
VOC		0.02	8760	1.85	8.09	Gas Analysis
n-Hexane	7.80E-02			0.14	0.63	HYSYS % of VOC
Benzene	1.70E-04			0.00	0.00	HYSYS % of VOC
Toluene	7.23E-04			0.00	0.01	HYSYS % of VOC
Ethylbenzene	9.26E-05			0.00	0.00	HYSYS % of VOC
Xylenes	6.95E-04			0.00	0.01	HYSYS % of VOC
Total HAPs			8760	0.00	0.00	HYSYS % of VOC