Division of Air Quality Permit Application Submittal

Please find attached a permit application for :

[Company Name; Facility Location]

- DAQ Facility ID (for existing facilities only):
- Current 45CSR13 and 45CSR30 (Title V) permits associated with this process (for existing facilities only):
- Type of NSR Application (check all that apply):
 - \circ Construction
 - \circ Modification
 - Class I Administrative Update
 - Class II Administrative Update
 - \circ Relocation
 - Temporary
 - Permit Determination

- Type of 45CSR30 (TITLE V) Application:
 - Title V Initial
 - o Title V Renewal
 - Administrative Amendment**
 - Minor Modification**
 - Significant Modification**
 - Off Permit Change

**If the box above is checked, include the Title V revision information as ATTACHMENT S to the combined NSR/Title V application.

- Payment Type:
 - Credit Card (Instructions to pay by credit card will be sent in the Application Status email.)
 - Check (Make checks payable to: WVDEP Division of Air Quality) Mail checks to: WVDEP – DAQ – Permitting Attn: NSR Permitting Secretary 601 57th Street, SE Charleston, WV 25304

Please wait until DAQ emails you the Facility ID Number and Permit Application Number. Please add these identifiers to your check or cover letter with your check.

- If the permit writer has any questions, please contact (all that apply):
 - Responsible Official/Authorized Representative
 - Name:
 - Email:
 - Phone Number:
 - **Company Contact**
 - Name:
 - Email:
 - Phone Number:
 - Consultant

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- Name:
- Email:
- Phone Number:





45CSR13 Modification Permit Application

Roxul USA Inc. RAN Facility

May 2023



The business of sustainability

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WVDAQ PERMIT APPLICATION FORMS

1. INTRODUCTION

1.1 Background

ROXUL USA Inc. dba Rockwool, (ROCKWOOL) submits this application for a permit modification to the West Virginia Department of Environmental Protection (WVDEP), Division of Air Quality (WVDAQ) to reflect modifications to Permit No. R14-0037. The modifications outlined in this application results in a net decrease in emissions of all regulated pollutants.

1.2 Application Overview

This permit application narrative is provided to add clarification and further detail to the permit application forms being provided to the WVDAQ for this project.

This section (Section 1) contains introductory information. Section 2 presents an overview of the proposed updates to processes and equipment. Processes with no changes have been omitted from Section 2. A summary of emissions changes is provided as Section 3. Section 4 provides a review of updates to federal regulatory requirements. A review of updates to state regulatory requirements is provided as Section 5. The WVDAQ permit application forms are provided as Appendix A.

2. PROCESS UPDATES OVERVIEW

The modifications included in this permit application reflect an aggregation of changes in equipment sizing, location, and source details. The types of permitting updates can be categorized into the following sets of changes:

- Removal of coal transfer, storage, and preparation equipment from the permit. The RAN facility will not fire coal and these sources have not been installed.
- Reallocation of eight (8) pounds per hour of carbon monoxide (CO) emissions from the Melting Furnace (IMF01) to the WESP (HE01).
- Removal, addition, and modification of raw material handling sources, including haul roads.
- Removal and modification to the capacity of various storage tanks.
- Removal of cooling towers.
- Modifications to the sizing of the combustion sources.
- Updates to release point parameters, including stack height and stack location coordinates.
- Removal of PMARK Product Marking from the permit. Inkjet (VOC) marking was not installed at RAN.
- Removal of Rockfon. The Rockfon production line currently has no plans to be constructed.
- Reduction of the annual hours of operation of the mineral wool production facility to 8,400 to reflect required annual turnarounds. The process mandates that the mineral wool production line is shut down for 2 weeks each year to conduct routine maintenance on the facility. The 8,400 hours of operation represents the maximum hours of operation of the mineral wool production line. The material handling, tanks, and paved roads will remain at 8,760 hours per year.
- Reduction of the annual hours of operation and application rate on Fleece Application Vents 1 & 2 (4,200 hours per year). This value is reflective of the maximum expected operations due to product demand.

A description of the changes to the manufacturing process and associated emission points is provided in Attachment G – Process Description.

3. SUMMARY OF EMISSION CHANGES

The updates proposed in this application will result in a net decrease in emissions. The original potential to emit, the changes due to the updates outlined in Section 2, and the resulting potential to emit are shown in the table below:

| Pollutant | Permitted Facility Emission Rate (tons/year) | Changes due to Updates (tons/year) | New Facility Emission Rate (tons/year) |
|--------------------------------|--|---------------------------------------|---|
| СО | 71.40 | -11.23 | 60.17 |
| NOx | 238.96 | -71.90 | 167.06 |
| Total PM | 250.87 | -175.37 | 75.50 |
| Filterable PM | 129.23 | -54.10 | 75.13 |
| PM ₁₀ | 153.19 | -80.13 | 73.06 |
| PM _{2.5} | 133.41 | -66.80 | 66.61 |
| SO ₂ | 147.45 | -6.11 | 141.34 |
| VOC | 471.41 | -275.23 | 196.18 |
| CO ₂ e | 152,934.82 | -30,931.87 | 122,002.95 |
| Formaldehyde | 68.63 | -51.99 | 16.64 |
| Methanol | 106.61 | -3.73 | 102.88 |
| H ₂ SO ₄ | 16.37 | -8.52 | 7.85 |
| Lead | 2.47E-04 | -5.80E-05 | 1.89E-04 |
| Total HAP | 392.59 | -128.98 | 263.61 |
| HF | 1.62 | -0.07 | 1.55 |
| HCI | 1.29 | -0.05 | 1.24 |
| COS | 1.64 | -0.07 | 1.57 |
| Arsenic | 3.93E-04 | -1.60E-05 | 3.77E-04 |
| Mercury | 2.55E-03 | -1.00E-04 | 2.45E-03 |
| Phenol | 100.22 | -24.90 | 75.32 |
| Mineral Fiber | 112.28 | -47.99 | 64.29 |
| Hexane | 0.26 | -0.15 | 0.11 |
| Benzene | 0.05 | -4.95E-02 | 5.17E-04 |

4. FEDERAL REGULATORY REQUIREMENTS

New Source Performance Standards (NSPS) are established for specific industrial categories in 40 CFR Part 60. West Virginia regulations in WV 45 CSR 16 incorporate the federal NSPS by reference. A review of the NSPS categories has been performed for applicability and is presented below.

4.1 Non-Applicable NSPS Standards

The NSPS subparts discussed in this section are not applicable but are addressed for documentation purposes.

4.1.1 40 CFR 60 Subpart Dc – Small Industrial Steam Generating Units

There are no changes to applicability of NSPS Subpart Dc due to the updates discussed in this application. Additionally, the Coal Mill Burner (IMF05) was not installed and is proposed to be removed from the permit.

4.1.2 40 CFR 60 Subpart Kb – Volatile Organic Liquid Storage Tanks

There are no changes to applicability of NSPS Subpart Kb due to the updates discussed in this application. Two of the thermal oil tanks have updated sizing, but both tanks will still have a capacity of less than 19,813 gallons (75 m³) and are therefore not subject to NSPS Subpart Kb.

4.1.3 40 CFR 60 Subpart Y – Standards Of Performance For Coal Preparation And Processing Plants

The facility will no longer prepare of process any coal and therefore is not subject to NSPS Subpart Y.

4.1.4 40 CFR 60 Subpart LL – Standards Of Performance For Metallic Mineral Processing Plants

There are no changes to applicability of NSPS Subpart LL based on updates discussed in this application.

4.1.5 40 CFR 60 Subpart VVV - Standards Of Performance For Polymeric Coating Of Supporting Substrates Facilities

There are no changes to applicability of NSPS Subpart VVV due to the updates discussed in this application.

4.1.6 40 CFR 60 Subpart CCCC – Standards Of Performance For Commercial And Industrial Solid Waste Incineration Units

There are no changes to applicability of NSPS Subpart CCCC due to the updates discussed in this application. The facility remains not subject to this subpart. Additionally, PET Coke and Coal sources were not installed and are proposed to be removed from the permit.

4.2 Applicable NSPS Standards

4.2.1 40 CFR 60 Subpart OOO – Nonmetallic Mineral Processing Plants

NSPS Subpart OOO applies to the following affected facilities in fixed or portable nonmetallic mineral processing plants that commenced construction after August 31, 1983: each crusher, grinding mill, screening operation, bucket elevator, belt conveyor, bagging operation, storage bin, enclosed truck or railcar loading station. A "nonmetallic mineral processing plant" is defined as any combination of equipment that is used to crush or grind any nonmetallic mineral. The definition of nonmetallic mineral specifically mentions limestone, dolomite, and other minerals which may be contained in stone raw materials that will be sieved, crushed (if necessary), and conveyed in the charging building operations.

Per §60.672(d), truck dumping of nonmetallic minerals into any screening operation, feed hopper, or crusher is exempt from PM standards of NSPS Subpart OOO, which would exclude the Raw Material Loading Hopper (B215). Vacuum systems are not identified as affected facilities in NSPS Subpart OOO; therefore, the Charging Building Vacuum Cleaning Filter (IMF21) is not subject to NSPS Subpart OOO. The remaining affected sources subject to PM emissions limits include the belt conveyor connected to the charging building (IMF11); indoor conveyor transfer points IMF12 and IMF16; outdoor transfer point IMF15; indoor sieve, crusher, storage bins, and belt conveyors located inside the charging building (represented by IMF17); Raw Material Reject Outdoor Collection Bin (RM_REJ); and indoor Sieve Reject Collection Bin (S_REJ). The Filter Fines Day Silo (IMF07) and Filter Fines Receiving Silo (IMF10) are conservatively considered as part of the nonmetallic mineral processing plant because the silos will store stone or mineral raw materials that have been through the charging building operations.

After the final belt conveyor transfer from charging building operations to the furnace building, raw materials are dosed to a continuous weigh bin connected to the Melting Furnace. This bin is part of the mineral wool production operations and is not considered part of the nonmetallic mineral processing plant.

A summary of the applicable emission limits to affected sources subject to NSPS Subpart OOO is shown in Table 4-1 on the following page.

| Seuree ID | Source | Control Device (if | NSPS Subpart OOO Limit | | |
|-----------|--|--------------------------------------|------------------------|---|--|
| Source ID | Description | present) | Limit | Citation | |
| RM_REJ | Raw Material Reject Collection Bin | 4-sided rubber drop guards | 7% opacity | §60.672(b) & Table | |
| S_REJ | Sieve Reject Collection Bin | Telescopic Chute & Full Enclosure | 7% opacity | 3 [fugitive emission limits] | |
| IMF14 | Raw Material Reject Stockpile | 3-sided enclosure | 7% opacity | | |
| IMF07 | One (1) Storage Silo (Filter Fines Day) | Bin Vent Filter Enclosed Indoors | 7% opacity | §60.672(a) & Table 2; §60.672(f) [opacity in lieu of | |
| IMF10 | Filter Fines Receiving Silo | Bin Vent Filter | 7% opacity | concentration limit for dry control devices on individua enclosed storage bins] | |
| IMF11 | Conveyor Transition Point (B215 to B220) | Fabric Filter Enclosed Indoors | 7% opacity | §60.672(b) & Table 3 [fugitive emission limits] | |
| IMF17 | Indoor sieve, crusher, storage bins, and belt conveyors located inside the charging building B220 | Full Enclosure | 7% opacity | §60.672(e)(1) | |
| IMF12 | Conveyor Transfer Point | Full Enclosure | 7% opacity | [fugitive emissions from building openings] | |
| IMF16 | Conveyor Transfer Point | Full Enclosure | 7% opacity | | |
| IMF15 | Transfer Points: Magnet Separator to Iron Container & Vacuum Cleaning | 4-Sided Drop Guard | 7% opacity | | |

ROCKWOOL will be required to submit applicable notifications and initial testing results for affected sources subject to NSPS Subpart OOO. Monitoring of baghouses required by §60.674(c) consists of quarterly 30-minute visible emissions inspections using EPA Method 22 or the alternative specified in §60.674(d) for operation of a bag leak detection system. Recordkeeping and reporting requirements will be applicable and will be conducted as required.

NSPS Subpart OOO does not apply to the following operations at the proposed facility as described below.

• The Recycling Plant is not part of a nonmetallic mineral processing plant because only formed mineral wool fibers are handled in this area (i.e., no stone or mineral raw materials).

- The capacity of the Melting Furnace Portable Crusher (170) will be equal to or less than the exemption threshold of 136 megagrams per hour (150 short tons per hour) per §60.670(c)(2). The portable crushing operation is separate from the charging building operations that are subject to NSPS Subpart OOO.
- Fresh and spent sorbent used in the desulfurization system at ROCKWOOL will be stored in silos and pneumatically conveyed either to or from the control system (e.g., no crushing, grinding, or other processing occurs). Sorbent handling is separate from the charging building operations that are subject to NSPS Subpart OOO. Therefore, the Sorbent Storage Silo (IMF08) and Spent Sorbent Silo (IMF09) are not part of a nonmetallic mineral processing plant and are not subject to NSPS Subpart OOO.

4.2.2 40 CFR 60 Subpart IIII - Stationary CI ICE

The Emergency Fire Pump Engine (EFP1) remains subject to this subpart. The installed unit has a maximum capacity of 316 hp (236 kW), as opposed to the original permitted value of 197 hp (147 kW). There are no changes to applicability of NSPS Subpart IIII based on the updates discussed in this application. The installed unit is an EPA certified unit. A copy of the emission guarantee with Reference to the EPA Certificate of Conformity is included in the WVDAQ Permit application forms.

4.3 NATIONAL EMISSION STANDARDS FOR HAZARDOUS AIR POLLUTANTS (NESHAP)

NESHAP standards are established for specific pollutants and source categories in 40 CFR Part 61 and Part 63 in accordance with the Clean Air Act Amendments of 1990, which required development standards for sources of HAP. West Virginia regulations in WV 45 CSR 34 incorporate the federal NESHAP by reference. Potential HAP emissions from the ROCKWOOL facility are above the major source thresholds of 10 tpy (9.07 MT/year) of an individual HAP or 25 tpy (22.7 MT/year) of total HAP emissions. Thus, ROCKWOOL is a major source of HAP and is subject to any applicable MACT standards.

There are no existing or proposed NESHAP standards under 40 CFR Part 61 that are applicable to the ROCKWOOL facility.

A review of the NESHAP regulations under 40 CFR Part 63 has been performed for applicability to the ROCKWOOL facility and is presented below.

4.3.1 40 CFR 63 Subpart DDD – Mineral Wool Production

There are no changes to applicability of NESHAP Subpart DDD based on the updates discussed in this application. The Melting Furnace (IMF01) will continue to be subject to and show compliance with the emission limits in 40 CFR 63 Subpart DDD. ROCKWOOL will operate and maintain the Melting Furnace (IMF01) in compliance with 40 CFR 63 Subpart DDD.

4.3.2 40 CFR 63 Subpart JJJJ – Paper and Other Web Coating

There are no changes to applicability of NESHAP Subpart JJJJ based on the updates discussed in this application. Only the application of fleece binder material on the mineral wool line is subject to this regulation. ROCKWOOL will continue to comply with this regulation by using 'as-applied' compliant coatings pursuant to the procedures in §63.3370(a)(2). This limits the as-applied binder to a VOC content of 0.016 lb-VOC/lb-binder. VOCs are allowed for use as a surrogate for organic HAP (OHAP) emissions per §63.3370(c)(1) and (2).

4.3.3 40 CFR 63 Subpart ZZZZ – Stationary RICE

Federal NESHAP regulations for stationary Reciprocating Internal Combustion Engines (RICE) are found at 40 CFR Part 63, Subpart ZZZZ ("RICE MACT"). For the Emergency Fire Pump Engine, as a

new emergency stationary RICE with a site rating less 500 brake hp and located at a major source of HAP, the requirements of NESHAP Subpart ZZZZ are satisfied by meeting the requirements of NSPS Subpart IIII (per §63.6590(c)(7)). No further requirements apply for such engines under this part. As discussed in Section 5.2.2, the Emergency Fire Pump Engine complies with NSPS Subpart IIII.

4.3.4 40 CFR 63 Subpart DDDDD - Industrial, Commercial, and Institutional Boilers And Process Heaters

The Natural Gas-Fired Boilers (CM03 and CM04) have an updated heat input capacity of 4.99 MMBtu/hr (1,462 kW). Since these boilers have a heat input capacity less than 5 MMBtu/hr, ROCKWOOL will now be required to perform tune-ups on these boilers every 5 years, rather than biennially, in accordance with §63.7540 and Table 3 of Boiler MACT.

5. STATE REGULATORY REQUIREMENTS

This section outlines the West Virginia state air quality regulations that could be reasonably expected to apply to ROCKWOOL and makes an applicability determination for each regulation based on activities conducted at the site and the emissions of regulated air pollutants. This review is presented to supplement and/or add clarification to the information provided in the WVDEP Rule 14 permit application forms.

The West Virginia State Regulations address federal regulations, including Prevention of Significant Deterioration permitting, Title V permitting, New Source Performance Standards, and National Emission Standards for Hazardous Air Pollutants. The regulatory requirements in reference to the facility are described in detail in the below section.

5.1 45 CSR 02 – To Prevent and Control Particulate Air Pollution From Combustion of Fuel in Indirect heat Exchangers

The Natural Gas-Fired Boilers (CM03 and CM04) have an updated heat input capacity of 4.99 MMBtu/hr (1,462 kW). There are no changes to applicability of 45 CSR 02 based on this update, and these units still qualify for the exemption noted in 45 CSR 2 Section 11, as they have a heat input rating less than 10 MMBtu/hr (2,930 kW). The Rockfon Building Heater (RFN10) will not be installed and has been removed from this application.

5.2 45 CSR 04 – To Prevent and Control the Discharge of Air Pollutants into the Air Which Causes or Contributes to an Objectionable Odor

There are no changes to applicability of 45 CSR 04 based upon the updates discussed in this application.

5.3 45 CSR 05 – To Prevent and Control Air Pollution from the Operation of Coal Preparation Plants, Coal Handling Operations, and Coal Refuse Disposal Areas

There are no changes to applicability of 45 CSR 05 based upon the updates discussed in this application. The facility is subject to the requirements of 45 CSR 7 and therefore, is not subject to this rule.

5.4 45 CSR 06 – Control of Air Pollution from the Combustion of Refuse

There are no changes to applicability of 45 CSR 06 based on the updates discussed in this application. 45 CSR 06 remains applicable to the Curing Oven Afterburner (CO-AB).

5.4.1 45 CSR 6-4.1 - Determination for Maximum Allowable Particulate Emissions

The Curing Oven Afterburner (CO-AB) has been installed with a maximum heat input capacity of 9.86 MMBtu/hr but was originally permitted at 6.83 MMBtu/hr. No updates to flow rate to the Afterburner have been made. The estimated Total PM emission rate of 3.31 lb/hr (1.50 kg/hr) remains below the maximum allowable PM emission rate mandated by 45 CSR 06, and thus there are no changes to applicability based on the updates discussed in this application.

45CSR6 Emission Standards for Incinerators – Section 4.1

Pursuant to §45-6-4.1, PM emissions from incinerators are limited to the value determined by the following formula:

Emissions (lb/hr) = F x Incinerator Capacity (tons/hr)

Where, the factor, F, is indicated in the table below:

| Incinerator Capacity | Factor F |
|-----------------------------|----------|
| A. Less than 15,000 lbs/hr | 5.43 |
| B. 15,000 lbs/hr or greater | 2.72 |

The maximum capacity of the afterburner is 24.4 tons/hour. Using this value and an F factor of 2.72, the resultant PM emission limit is 66.37 lbs/hr. The estimated worst-case PM emitted from the afterburner is 3.31 lbs/hr. This is below the allowable of 45 CSR 06.

45CSR6 Opacity Limits - Sections 4.3 and 4.4

Pursuant to §45-6-4.3, and subject to the exemptions of 4.4, the curing oven afterburner will have a 20% opacity limit during operation. Proper design and operation of the curing oven afterburner will prevent any substantive opacity from the afterburner.

5.5 45 CSR 7 – To Prevent and Control Particulate Air Pollution from Manufacturing Processes and Associated Operations

45 CSR 7 regulates the emissions of filterable particulate matter from source operations within manufacturing processes. Manufacturing processes are defined as any industrial or manufacturing actions or processes that emit smoke, particulate matter, or gaseous matter.

ROCKWOOL operates multiple manufacturer processes that will emit filterable PM into the open air, including a mineral wool manufacturing process, and material handling point source activities. These separate manufacturing processes operate with separate source operations, which are defined as the last operation in a manufacturing process preceding the emissions of air contaminants.

The facility shall not emit filterable PM into the open air from any process source operation which is greater than 20% opacity. ROCKWOOL will also have to limit fugitive emissions by equipping manufacturing processes with a system to minimize fugitive PM emissions. ROCKWOOL utilizes a combination of good housekeeping practices, partial/full enclosures, baghouses, and various filters throughout the facility to minimize PM emissions. All haul roads are paved to minimize fugitive PM emissions.

5.5.1 Mineral Wool Line

There are no changes to applicability or compliance based upon the updates discussed in this application.

There will be a reduction of the annual hours of operation of the mineral wool production facility to 8,400 to reflect required annual turnarounds. The process mandates that the mineral wool production line is shut down for 2 weeks each year to conduct routine maintenance on the facility. The 8,400 hours of operation represents the maximum hours of operation of the mineral wool production line.

5.5.2 Rockfon Line

The Rockfon Line was not installed and is being removed as part of this application and will no longer be subject to 45 CSR 7.

5.5.3 Materials Handling Sources

The expected filterable PM emission rate for the materials handling process source operation is 1.49 lb/hr (0.67 kg/hr) and will demonstrate compliance with the Rule 7 requirements. The updates to material handling sources discussed within this permit application will have no impact on compliance with the Rule 7 requirements. There is no impact to the maximum allowable total stack filterable PM emission rate.

5.5.4 Coal Milling

Coal Milling was not installed and is being removed as part of this application and will no longer be subject to 45 CSR 7.

5.6 45 CSR 10 – To Prevent and Control Air Pollution from the Emission of Sulfur Oxides

45 CSR 10 contains requirements that limit SO₂ emissions from fuel burning units, limits in-stack SO₂ concentrations of manufacturing processes, and limits hydrogen sulfide concentrations in process gas streams.

The Natural Gas-Fired Boilers (CM03 and CM04) have an updated heat input capacity of 4.99 MMBtu/hr (1,462 kW). There are no changes to applicability of 45 CSR 10 based on this update, and these units still qualify for the exemption noted in 45 CSR 2 Section 11, as they have a heat input rating less than 10 MMBtu/hr (2,930 kW).

The RAN Facility does not combust any process gas stream that potentially contain hydrogen sulfide gas.

The Melting Furnace stack (IMF01), after control by the sorbent injection system is subject to the limitation on in-stack SO₂ concentrations. Pursuant to §45-10-4.1, the Melting Furnace stack (IMF01) shall not exceed an in-stack SO₂ concentration of 2,000 parts per million by volume. The calculated in-stack SO₂ concentration based on 33.63 lb/hr of SO₂, 21,413.73 acfm, 301.73 °F is 227.48 ppm_v. This in-stack SO₂ concentration is less than the 45 CSR 10 allowable.

5.7 45 CSR 11 – Prevention of Air Pollution Emergency Episodes

There are no changes to applicability of 45 CSR 11 based on the updates discussed in this application.

5.8 45 CSR 13 – Permits For Construction, Modification, Relocation And Operation Of Stationary Sources Of Air Pollutants, Notification Requirements, Administrative Updates, Temporary Permits, General Permits, Permission To Commence Construction, And Procedures For Evaluation

45 CSR 13 outlines the requirements for the submission of deliverables as they apply to the construction or modification of stationary sources of air pollution. ROCKWOOL's initial permitting action was subject to the requirements of this rule based upon the construction of a stationary source

of air pollutants exceeding West Virginia's minor source permitting applicability thresholds (6 lb/hr AND 10 tpy of any regulated air pollutant).

When evaluating the updates contained within the permit application, the most appropriate permitting mechanism for an update to ROCKWOOL's existing air permit has been identified as a Class I Administrative Update. ROCKWOOL understands that WVDAQ will use its discretionary authority to process the permitting update as a Modification and submits this modification application based upon WVDAQ's direction.

The original permit application was submitted to the WVDAQ on November 21, 2017. At that time, the proposed facility was defined as a 'major stationary source' under 45 CSR 14 as shown in Table 3-1. Consistent with WVDAQ policy, permitting actions that are reviewed under 45 CSR 14 are also reviewed concurrently under 45 CSR 13. Permit R14-0037 was issued on April 30, 2018.

With the proposed changes outlined in this application, the RAN Facility will experience a net decrease in emissions of all pollutants. Additionally, this decrease will result in the facility no longer being defined as a 'major stationary source'. This means the facility no longer has the potential to emit two hundred fifty (250) tons per year or more of any regulated NSR pollutant.

This modification application satisfies the WVDAQ's permitting requirements and will establish the facility as a minor source for all regulated NSR pollutants. This application will be subject to public review procedures outlined in §45-13-8. ROCKWOOL will place the required Class I legal advertisement in a newspaper of general circulation in the area and pay the appropriate permit application fees required under 45 CSR 22.

5.9 45 CSR 14 – Permits for Construction and Major Modification of Major Stationary Sources of Air Pollution for the Prevention of Significant Deterioration

Federal construction permitting programs regulate new and modified sources of attainment pollutants under Prevention of Significant Deterioration. The requirements of this rule apply to the construction of any new major stationary source. In the pre-construction application (November 21, 2017), the RAN Facility was classified as a major stationary source because the facility potential to emit (PTE) exceeded two hundred fifty (250) tons per year of VOC. Further, emissions of NO_x, SO₂, PM, PM₁₀, PM_{2.5}, H₂SO₄ Mist, and CO2e were also subject to PSD review due to potential emissions greater than the PSD significant emission rate (SER) for each pollutant.

This permitting action was evaluated against the regulatory definitions of major modification and minor modification. Due to the large decrease in emissions, the facility is no longer defined as a 'major stationary source'. Therefore, the RAN facility is no longer subject to 45 CSR 14. Because the RAN Facility is not subject to 45CSR 14, air quality modeling or Best Available Control Technology (BACT) analysis is not required as part of this application.

These large emission decreases are realized because the RAN Facility was conservatively permitted to account for a wider range of potential operating conditions. Some of these potential operating conditions were never realized and this permitting action removes their potential use. Additionally, there was a reduction of the annual hours of operation of the mineral wool production facility to 8,400 to reflect required annual turnarounds to account for an annual shutdown for maintenance activities, and a reduction of the annual hours of operation and application rate on Fleece Application Vents 1 & 2 (4,200 hours per year) to reflect maximum expected operations due to product demand.

5.10 45 CSR 16 – Standards of Performance for New Stationary Sources (NSPS)

45 CSR 16 applies to registrants that are subject to 40 CFR 60 Standards of Performance for New Source Stationary Sources (NSPS).

ROCKWOOL is subject to the following NSPS subparts because of processes and equipment used at the facility:

- NSPS Subpart OOO Standards of Performance for Nonmetallic Mineral Processing Plants; and
- NSPS Subpart IIII Standards of Performance for Stationary Compression Ignition Internal Combustion Engines.

No additional NSPS are applicable for this facility. Additional descriptions of these regulations are provided in the Federal Regulations section of this regulatory discussion.

5.11 45 CSR 17 – To Prevent and Control Particulate Matter Air Pollution from Materials Handling, Preparation, Storage, and other Sources of Fugitive Particulate Matter

The facility is not subject to this rule because sources that are subject to the fugitive PM emission requirements of WV 45 CSR 7 are exempt from the provisions of WV 45 CSR 17.

5.12 45 CSR 21 – To Prevent and Control Air Pollution from the Emissions of Volatile Organic Compounds

There are no changes to applicability of 45 CSR 21 based on updates discussed in this application.

5.13 45 CSR 29 – Rules Requiring the Submission of Emission Statements for Volatile Organic Compound (VOC) Emissions and Oxides of Nitrogen (NOx) Emissions

There are no changes to applicability of 45 CSR 29 based on updates discussed in this application.

5.14 45 CSR 30 – Requirements for Operating Permits

There are no changes to applicability of 45 CSR 30 based on updates discussed in this application.

5.15 45 CSR 34 – National Emission Standards for Hazardous Air Pollutants (NESHAP)

45 CSR 34 applies to registrants that are subject to NESHAP requirements. The RAN facility is subject to the following NESHAP subparts because of processes and equipment used at the facility:

- NESHAP Subpart DDD Mineral Wool Production;
- NESHAP Subpart JJJJ Paper or Other Web Coating;
- NESHAP Subpart ZZZ Stationary Reciprocating Internal Combustion Engines (RICE); and
- NESHAP Subpart DDDDD Industrial, Commercial, and Institutional Boilers and Process Heaters.

These NESHAP requirements are described in more detail in the Federal Regulations section of this regulatory discussion.

APPENDIX A - WVDAQ PERMIT APPLICATION FORM

| WEST VIRGINIA DEPARTMENT OF ENVIRONMENTAL PROTECTION DIVISION OF AIR QUALITY 601 57 th Street, SE Charleston, WV 25304 (304) 926-0475 WWW.dep.wy.gov/dag | APPLICATION FOR NSR PERMIT AND TITLE V PERMIT REVISION (OPTIONAL) |
|---|--|
| PLEASE CHECK ALL THAT APPLY TO NSR (45CSR13) (IF KNOWN): CONSTRUCTION MODIFICATION RELOCATION CLASS I ADMINISTRATIVE UPDATE TEMPORARY CLASS II ADMINISTRATIVE UPDATE AFTER-THE-FACT | PLEASE CHECK TYPE OF 45CSR30 (TITLE V) REVISION (IF ANY): ADMINISTRATIVE AMENDMENT SIGNIFICANT MODIFICATION IF ANY BOX ABOVE IS CHECKED, INCLUDE TITLE V REVISION INFORMATION AS ATTACHMENT S TO THIS APPLICATION |
| | on Guidance" in order to determine your Title V Revision options o operate with the changes requested in this Permit Application. |
| Section | I. General |
| Name of applicant (as registered with the WV Secretary of St Roxul USA Inc. | tate's Office): 2. Federal Employer ID No. (FEIN): 99-0378111 |
| 3. Name of facility <i>(if different from above):</i> RAN Facility | 4. The applicant is the: |
| 5A. Applicant's mailing address: 665 Northport Avenue Ranson, WV 25430 | 5B. Facility's present physical address: 665 Northport Avenue Ranson, WV 25430 |
| change amendments or other Business Registration Certification | Organization/Limited Partnership (one page) including any name ate as Attachment A. rity of L.L.C./Registration (one page) including any name change |
| 7. If applicant is a subsidiary corporation, please provide the nar | ne of parent corporation: Rockwool Group |
| 8. Does the applicant own, lease, have an option to buy or other If YES, please explain: Applicant owns the site. If NO, you are not eligible for a permit for this source. | wise have control of the <i>proposed site</i> ? XYES NO |
| Type of plant or facility (stationary source) to be constructed administratively updated or temporarily permitted (e.g., or crusher, etc.): Mineral Wool Insulation Manufacturing Facility | |
| 037-00108 a | ist all current 45CSR13 and 45CSR30 (Title V) permit numbers ssociated with this process (for existing facilities only): R14-0037 |
| All of the required forms and additional information can be found u | nder the Permitting Section of DAQ's website, or requested by phone. |

| 12A. | | | | |
|--|---|-------------------------------------|--|--|
| ➡ For Modifications, Administrative Updates or Tempresent location of the facility from the nearest state | | please provide directions to the | | |
| Sor Construction or Relocation permits, please p | rovide directions to the proposed new s | ite location from the nearest state | | |
| road. Include a MAP as Attachment B. | | | | |
| From WV-9 E, take the County Route 1 exit towa Road and travel 0.4 miles. Turn left onto WV 115 | - | - | | |
| The facility is located on the left at 665 North po | | o nonipoli Avenue. | | |
| | | | | |
| | | | | |
| 12.B. New site address (if applicable): | 12C. Nearest city or town: | 12D. County: | | |
| 665 Northport Avenue Ranson, WV 25430 | Ranson | Jefferson | | |
| 12.E. UTM Northing (KM): 4362.62 | 12F. UTM Easting (KM): 252.06 | 12G. UTM Zone: 18 | | |
| 13. Briefly describe the proposed change(s) at the facility | y: | | | |
| Updating various sources to account for facility configuration detailed description of each change is provided in the permission of the pe | nit application introduction narrative | et decrease in emissions. A | | |
| 14A. Provide the date of anticipated installation or change If this is an After-The-Fact permit application, provi | | 14B. Date of anticipated Start-Up | | |
| If this is an After-The-Fact permit application, provi change did happen: | de the date upon which the proposed | if a permit is granted: | | |
| 14C. Provide a Schedule of the planned Installation of/ | Change to and Start-Up of each of the | units proposed in this permit | | |
| application as Attachment C (if more than one unit | • | | | |
| 15. Provide maximum projected Operating Schedule of Hours Per Day 24 Days Per Week | | ation: | | |
| 16. Is demolition or physical renovation at an existing fac | cility involved? 🗌 YES 🛛 🗙 NO | | | |
| 17. Risk Management Plans. If this facility is subject to | 112(r) of the 1990 CAAA, or will becom | e subject due to proposed | | |
| changes (for applicability help see www.epa.gov/cepp | o), submit your Risk Management Pla | n (RMP) to U.S. EPA Region III. | | |
| 18. Regulatory Discussion. List all Federal and State a | ir pollution control regulations that you l | believe are applicable to the | | |
| proposed process (if known). A list of possible applica | ble requirements is also included in Atta | achment S of this application | | |
| (Title V Permit Revision Information). Discuss applicability and proposed demonstration(s) of compliance (<i>if known</i>). Provide this | | | | |
| information as Attachment D. | | | | |
| Section II. Additional atta | achments and supporting de | ocuments. | | |
| 19. Include a check payable to WVDEP – Division of Air | Quality with the appropriate application | fee (per 45CSR22 and | | |
| 45CSR13). | | | | |
| 20. Include a Table of Contents as the first page of you | r application package. | | | |
| Provide a Plot Plan, e.g. scaled map(s) and/or sketo source(s) is or is to be located as Attachment E (Re | | rty on which the stationary | | |
| S Indicate the location of the nearest occupied structure | | | | |
| 22. Provide a Detailed Process Flow Diagram(s) show device as Attachment F. | ving each proposed or modified emission | ns unit, emission point and control | | |
| 23. Provide a Process Description as Attachment G . | | | | |
| Also describe and quantify to the extent possible | | | | |
| All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone. | | | | |

| 24. Provide Material Safety Data Sheets (MSDS) for all materials processed, used or produced as Attachment H. | | | | | |
|---|--|--|--|--|--|
| ⇒ For chemical processes, provide a MSDS for each compound emitted to the air. | | | | | |
| 25. Fill out the Emission Units Table and provide it as Attachment I. | | | | | |
| 26. Fill out the Emission Points Data S | ummary Sheet (Table 1 and Ta | ble 2) and provide it as Attachment J. | | | |
| 27. Fill out the Fugitive Emissions Data | a Summary Sheet and provide it | as Attachment K. | | | |
| 28. Check all applicable Emissions Unit | t Data Sheets listed below: | | | | |
| Bulk Liquid Transfer Operations | 🔀 Haul Road Emissions | Quarry | | | |
| Chemical Processes | Hot Mix Asphalt Plant | Solid Materials Sizing, Handling and Storage | | | |
| Concrete Batch Plant | Incinerator | Facilities | | | |
| Grey Iron and Steel Foundry | S Indirect Heat Exchanger | Storage Tanks | | | |
| General Emission Unit, specify | | | | | |
| Mineral Wool Line - Melting Furnad | - | | | | |
| Fill out and provide the Emissions Unit I | | | | | |
| 29. Check all applicable Air Pollution C | 1.55 | | | | |
| Absorption Systems | Baghouse | | | | |
| Adsorption Systems | | Mechanical Collector | | | |
| Afterburner | Electrostatic Precipita | tor Wet Collecting System | | | |
| Other Collectors, specify | | | | | |
| | | | | | |
| Fill out and provide the Air Pollution Co | | | | | |
| 30. Provide all Supporting Emissions (Items 28 through 31. | Calculations as Attachment N, | or attach the calculations directly to the forms listed in | | | |
| 31. Monitoring, Recordkeeping, Reporting and Testing Plans. Attach proposed monitoring, recordkeeping, reporting and testing plans in order to demonstrate compliance with the proposed emissions limits and operating parameters in this permit application. Provide this information as Attachment O. | | | | | |
| Please be aware that all permits must be practically enforceable whether or not the applicant chooses to propose such measures. Additionally, the DAQ may not be able to accept all measures proposed by the applicant. If none of these plans are proposed by the applicant, DAQ will develop such plans and include them in the permit. | | | | | |
| 32. Public Notice. At the time that the application is submitted, place a Class I Legal Advertisement in a newspaper of general | | | | | |
| circulation in the area where the sour | circulation in the area where the source is or will be located (See 45CSR§13-8.3 through 45CSR§13-8.5 and <i>Example Legal</i> | | | | |
| Advertisement for details). Please submit the Affidavit of Publication as Attachment P immediately upon receipt. | | | | | |
| 33. Business Confidentiality Claims. Does this application include confidential information (per 45CSR31)? | | | | | |
| 🗌 YES 🛛 🔯 NO | | | | | |
| If YES, identify each segment of information on each page that is submitted as confidential and provide justification for each segment claimed confidential, including the criteria under 45CSR§31-4.1, and in accordance with the DAQ's "Precautionary Notice – Claims of Confidentiality" guidance found in the General Instructions as Attachment Q. | | | | | |
| Section III. Certification of Information | | | | | |
| 34. Authority/Delegation of Authority. Only required when someone other than the responsible official signs the application. Check applicable Authority Form below: | | | | | |
| Authority of Corporation or Other Business Entity | | | | | |
| Authority of Governmental Agency | | | | | |
| Submit completed and signed Authority Form as Attachment R. | | | | | |
| All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone. | | | | | |

35A. Certification of Information. To certify this permit application, a Responsible Official (per 45CSR§13-2.22 and 45CSR§30-2.28) or Authorized Representative shall check the appropriate box and sign below.

Certification of Truth, Accuracy, and Completeness

I, the undersigned X Responsible Official / Authorized Representative, hereby certify that all information contained in this application and any supporting documents appended hereto, is true, accurate, and complete based on information and belief after reasonable inquiry I further agree to assume responsibility for the construction, modification and/or relocation and operation of the stationary source described herein in accordance with this application and any amendments thereto, as well as the Department of Environmental Protection, Division of Air Quality permit issued in accordance with this application, along with all applicable rules and regulations of the West Virginia Division of Air Quality and W.Va. Code § 22-5-1 et seq. (State Air Pollution Control Act). If the business or agency changes its Responsible Official or Authorized Representative, the Director of the Division of Air Quality will be notified in writing within 30 days of the official change.

Compliance Certification

Except for requirements identified in the Title V Application for which compliance is not achieved, I, the undersigned hereby certify that, based on information and belief formed after reasonable inquiry, all air contaminant sources identified in this application are in compliance with all applicable requirements.

| SIGNATURE (Please 35B. Printed name of signee: Mark Grave | DATE: <u>05/19/2023</u> (Please use blue lnk) 35C. Title: Director of Operations | |
|--|--|-----------|
| 35D. E-mail: Mark.Graves@rockwool.com | 36E. Phone; | 36F. FAX: |
| 36A. Printed name of contact person (if diffe Stacey Phillips | 36B. Title: Environmental Manager | |
| 36C. E-mail: Stacey.Phillips@rockwool.com | 36D. Phone: 681-247-0824 | 36E. FAX: |

| PLEASE CHECK ALL APPLICABLE ATTACHMENTS INCLUDED WITH THIS PERMIT APPLICATION: | | | |
|--|-----------|--|--|
| PLEASE CHECK ALL APPLICABLE ATTACHMENTS INCLUDED WITH THIS PERMIT APPLICATION: Attachment A: Business Certificate Attachment K: Fugitive Emissions Data Summary Sheet Attachment B: Map(s) Attachment L: Emissions Unit Data Sheet(s) Attachment C: Installation and Start Up Schedule Attachment M: Air Pollution Control Device Sheet(s) Attachment D: Regulatory Discussion Attachment N: Supporting Emissions Calculations Attachment E: Plot Plan Attachment O: Monitoring/Recordkeeping/Reporting/Test Attachment F: Detailed Process Flow Diagram(s) Attachment P: Public Notice Attachment H: Material Safety Data Sheets (MSDS) Attachment R: Authority Forms Attachment J: Emission Units Table Attachment S: Title V Permit Revision Information Attachment J: Emission Points Data Summary Sheet Application Fee | ing Plans | | |
| Please mail an original and three (3) copies of the complete permit application with the signature(s) to the DAO. Permitting Section, at the | | | |

| Please mail an original and three (3) copies of the complete permit application with the signature(s) to the DAQ, Permitting S | ection, i | at the |
|--|-----------|--------|
| address listed on the first page of this application. Please DO NOT fax permit applications. | , | |

| FOR AGENCY USE ONLY - IF THIS IS A TITLE V SOURCE: |
|---|
| Forward 1 copy of the application to the Title V Permitting Group and: |
| For Title V Administrative Amendments: |
| NSR permit writer should notify Title V permit writer of draft permit, |
| For Title V Minor Modifications: |
| Title V permit writer should send appropriate notification to EPA and affected states within 5 days of receipt, |
| NSR permit writer should notify Title V permit writer of draft permit. |
| For Title V Significant Modifications processed in parallel with NSR Permit revision: |
| NSR permit writer should notify a Title V permit writer of draft permit, |
| Public notice should reference both 45CSR13 and Title V permits, |
| EPA has 45 day review period of a draft permit. |
| All of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone. |

Appendix A - WVDAQ Forms

TABLE OF CONTENTS

Attachments:

- A Business Certificate
- C Installation and Start Up Schedule
- D Regulatory Discussion
- F Process Flow Diagram
- G Process Description
- I Emission Units Table
- J Emission Points Data Summary Sheet
- K Fugitive Emissions Data Summary Sheet
- L Emission Unit Data Sheets
- M Air Pollution Control Device Sheet
- N Supporting Emission Calculations
- O Monitoring, Recordkeeping, Reporting, and Testing Plans
- P Public Notice
- Q Business Confidential Claims
- S Title V Revision

Attachment A

WEST VIRGINIA STATE TAX DEPARTMENT BUSINESS REGISTRATION CERTIFICATE

ISSUED TO: ROXUL USA INC. DBA ROCKWOOL 71 EDMOND RD 6 KEARNEYSVILLE, WV 25430-2781

BUSINESS REGISTRATION ACCOUNT NUMBER:

2348-4027

This certificate is issued on:

10/25/2017

This certificate is issued by the West Virginia State Tax Commissioner in accordance with Chapter 11, Article 12, of the West Virginia Code

The person or organization identified on this certificate is registered to conduct business in the State of West Virginia at the location above.

This certificate is not transferrable and must be displayed at the location for which issued

This certificate shall be permanent until cessation of the business for which the certificate of registration was granted or until it is suspended, revoked or cancelled by the Tax Commissioner.

Change in name or change of location shall be considered a cessation of the business and a new certificate shall be required.

TRAVELING/STREET VENDORS: Must carry a copy of this certificate in every vehicle operated by them. CONTRACTORS, DRILLING OPERATORS, TIMBER/LOGGING OPERATIONS: Must have a copy of this certificate displayed at every job site within West Virginia.

atL006 v.4 L0875932352

Attachment C

Attachment C

Installation and Start Up Schedule

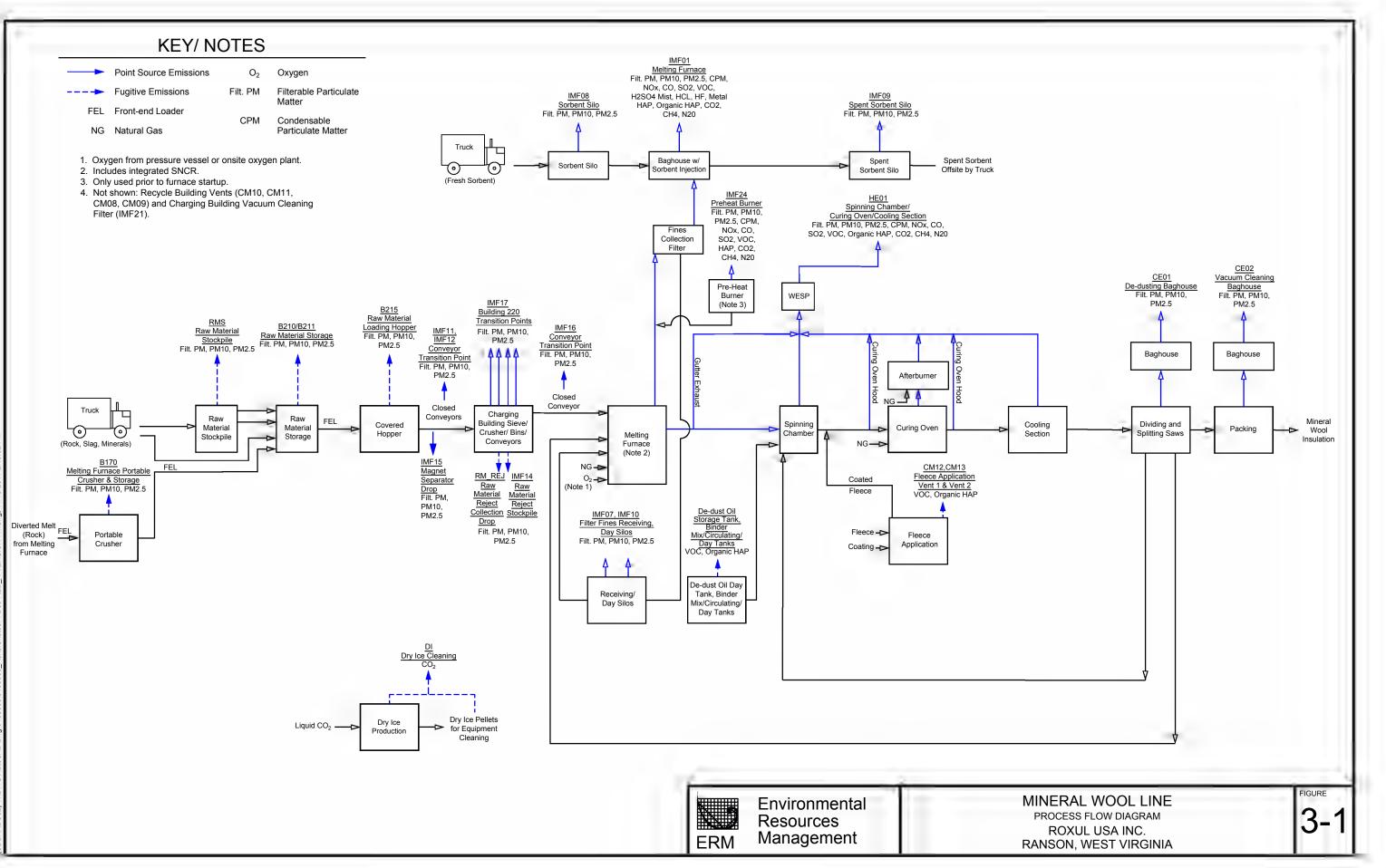
The changes outlined in this application reflect as-built construction of the facility. The facility began operation on May 22, 2021.

Attachment D

Attachment D

Regulatory Discussion

Please see the regulatory discussion in Section 4 and Section 5 of the Introduction of this permit application for the federal and state regulatory discussions, respectively. Attachment F



Attachment G

PROCESS DESCRIPTION

The mineral wool line will produce mineral wool insulation for residential, commercial, and industrial uses. Various types of insulating products can be produced with different densities, binder content, or dimensions to meet the requirements of various market sectors.

Mineral wool or "stone wool" is a natural product made partly from volcanic rocks. Rock may be supplemented with recycled mineral wool and slag from the steel industry. The following types of mineral raw materials are typically used in stone wool production:

Eruptive stones such as basalt/diabase, amphibolite, and anorthosite

- Slags such as blast furnace slag or converter slag
- Dolomite and/or limestone
- Mineral additives, such as olivine sand and high alumina content materials such as bauxite, kaoline clay, and aludross (by-product of the smelting process in the creation of aluminum from bauxite)

The mineral wool fibers are made from melted stone raw materials at very high temperatures (>2,700°F /1480°C), binder, and de-dusting oil. The various raw materials used in the melting furnace are mixed in the correct ratio to achieve the required chemistry of the fibers. The mineral wool manufacturing process consists of material handling/charging, melting, spinning, curing, cooling, cutting, and packing. Raw materials will be delivered to the site via truck, and products will leave the site via truck.

Raw Material Handling

The following changes have been made to the raw material handling from the previous permit application:

Conveyor Transition Point IMF11 is now located indoors. This source has been updated to include an indoor settling factor in addition to the fabric filter already permitted.

Seven material handling fugitive emission points are proposed to be modified in the permit, which are listed below:

- RMS, which includes a raw material stockpile with a base area of 500 m²;
- IMF17, which now includes 22 transfer points inside B220, Mixer and Crusher emissions inside B220 (previously included IMF18, which is proposed to be removed from the permit), and 2 transfer points with fabric filters inside B220;
- IMF11, which includes one transfer point inside B215;
- IMF12, which includes one transfer point inside B215;
- IMF16, which includes one transfer point inside B300;
- IMF15, which includes one transfer point outside B220; and
- IMF14, which includes a storage stockpile with a base area of 10 m².

Melting raw materials will be delivered in bulk by truck and unloaded and transferred with a front-end loader into the raw material stockpile (RMS) with three-sided enclosure. Additionally, diverted melt (rock) from the melting furnace will be delivered to a portable crusher (B170). The material from B170 and RMS will be transferred with a front end-loader to the raw material loading hopper (B215). The loading hopper feeds material onto a series of enclosed conveyors to the charging building (B220), where all subsequent melting raw material handling activities occur. A fraction of oversized material is directed to an indoor sieve and crusher, if required. Materials are then distributed to individual raw material bins. From here, they are dosed onto a belt conveyor to create a batch of charge material. The batch is conveyed into a bucket or similar vertical conveyor and then loaded into a mixer to create a homogeneous charge. The mixer is kept closed and equipped with an add-on filter that vents indoors during mixing.

The material handling sources IMF17, IMF12, IMF16, and IMF15, capture emission sources as material moves from B215 to B220, moves through B220, and exits B220 to B300 (furnace building). IMF12 includes the transfer point from the loading hopper (located inside B215) to a conveyor. From B215, material transfers to a second conveyor, and this transfer point corresponds to IMF11. The material moves outside from B215 to B220, where there is a transfer point from a magnet separator into an iron container with a 4-sided drop guard corresponding to IMF15. Material is delivered to B220 by a conveyor transfer point which is included in IMF17. IMF17 includes 22 conveyor transfer points which are indoors but otherwise uncontrolled, as well as the two conveyor transition points, which are equipped with fabric filters. Additional transfer points inside B220 included with IMF17 are one transfer point from the magnet separator to the iron container with a telescopic chute and two transfer points, one which transfers material from the magnet separator to the feeder and the second from the feeder to the crusher. Once material leaves B220, it is transferred to B300. The conveyor transfer point located inside B300 corresponds to IMF16.

The two mechanical vents on the charging building were not installed. As described above, emissions from the Mixer and Crusher are included with the other new B220 Material Handling emissions (IMF17). IMF18 is proposed to be removed from the permit.

If raw materials entering the charging building are found to be outside of specifications it is possible to collect these materials in two locations, either after the sieve or after the raw material bins. The material is directed into collection bins by conveyor, which is equipped with curtains for enclosure (RM_REJ). S-REJ is proposed to be removed from the permit.

Emissions from material handling consist of filterable PM/PM₁₀/PM_{2.5}.

Emission points from material handling include:

- Charging Building Material Handling Building Vents (IMF17)
- Five (5) Conveyor Transition Points,
 - Conveyor Transition Point (B215 to B220) (IMF11)
 - Conveyor Transition Point (B210/B211 to B220) (IMF12)
 - Conveyor Transition Point (B220 No. 1) (IMF14)
 - Conveyor Transition Point (B220 No. 2) (IMF15)
 - Conveyor Transition Point (B220 to B300) (IMF16)

Fugitive emissions from material handling consist of:

- Raw Material Storage (B210/211),
- Raw Material Outdoor Stockpile (RMS)
- Raw Material Loading Hopper (B215)
- Raw Material Reject Collection Bin (RM_REJ)
- Paved Haul Roads

Melting

During start-up a natural gas-fired preheater burner is used to warm the Melting Furnace baghouses to prevent condensation. Hot exhaust from the burner will indirectly heat the Melting Furnace baghouses before exhausting through the preheat burner stack (IMF24). The indirect heat transfer will be done by a thermal oil system including an expansion tank which is used both for preheating transfer of energy and to extract surplus heat for heat recovery. The natural gas preheat burner is rated at 5.12 MMBtu/hr (1,490 kW) heat input. The pre-heat burner will operate for approximately 2 hours (120 minutes) prior to the Melting Furnace startup. Shortly after, stone raw materials are added and heated in the first and second preheat chambers to approximately 1,022 °F (550 °C) and 1,562 °F (850 °C), respectively. From here, the preheated raw materials are introduced to the melter.

During melting furnace operation, temperatures in the melter reach approximately 3,000 °F (1,650 °C) and the resultant melt flows out of the furnace to the spinner. Gutter channels are used to direct melt from the furnace onto the spinners. An exhaust is located above the gutters to remove heat from the area to lower the temperature in the working environment, which will be directed to the Wet Electrostatic Precipitator (WESP) (HE01).

Once the system is operating at a steady state, waste wool and filter fines from the process are recycled into the melter along with stone raw materials.

Tapping is an emptying of the furnace, where melt flows directly out of the furnace and into a collection area. The tapped melt can be crushed in the portable crusher and reused in the melting process. Tapping occurs when the line shuts down, or as a result of an upset.

The melt process in the Melting Furnace is an oxidizing process, which operates with an excess of oxygen. The melting process is open to ambient building air with unrestricted air flow (i.e., there is no cover on the furnace). A "quench hood" is situated above the melter that is connected to an exhaust riser. The flue gas from the melter travels up through the riser and then through each preheating chamber, where the hot exhaust preheats stone raw materials prior to venting to add-on control devices.

In the furnace the amount of air is determined to ensure optimal operation, which includes that the air carries particles (fine material) between the pre-heater cyclones, and this requires a certain flow/air speed. The air flow is also required to cool the air before the dust filters as the filters cannot withstand the hot air from the melting process. Because the air flow is independent of the capacity, the emissions of CO and NO_x are also independent of the furnace capacity (i.e., melt rate).

Aqueous ammonia will be injected for the de- NO_x reaction to reduce NO_x emissions.

The opening at the top of the melter allows for ambient air to be pulled into the riser, which facilitates an adequate temperature for a de- NO_x reaction to occur (typically 1,400-2,000 °F or 760-1,093 °C). Therefore, it can be said that the Melting Furnace has "integrated" Selective Non-Catalytic Reduction (SNCR) technology. Binder contained in the recycled wool can also contribute in the de- NO_x reaction, but is not relied upon for the control of NO_x .

Hot flue gas is used to preheat incoming combustion air to the melter via heat exchangers situated at the outlet of the furnace. Flue gas is then directed to a baghouse to collect raw material fines. A second baghouse in series is used for control of emissions of filterable PM/PM₁₀/PM_{2.5}, and is equipped with sorbent injection to control sulfur dioxide (SO₂), sulfuric acid (H₂SO₄) mist, hydrogen chloride (HCl), and hydrogen fluoride (HF) emissions. Carryover of raw materials fines that are collected in the first baghouse will be pneumatically conveyed to a receiving silo and day silo (IMF07, IMF10) prior to reuse in the melter. The silos vent to a bin vent filter exhausting to the atmosphere.

Emissions from the Melting Furnace stack (IMF01) consist of filterable PM/PM₁₀/ PM_{2.5}, CPM, NO_x, CO, SO₂, VOC, H₂SO₄ mist, HCl, HF, metal HAP, CO₂, CH₄, N2O, and small amounts of organic HAP such as carbonyl sulfide (COS) and formaldehyde (HCHO).

As stated, de-sulfurization is applied for the control of sulfur oxides and acid gases. Sorbent material (e.g., hydrated lime as calcium hydroxide or similar) is delivered to the site by truck and loaded into an outdoor storage silo equipped with a bin vent filter. Sorbent is transported in a closed system and injected into the flue gas prior to the second baghouse as a filter media.

Spent sorbent is stored in a silo (IMF09) equipped with a bin vent filter until it is emptied into a vacuum truck for off-site disposal.

The Sorbent Silo emits filterable $PM/PM_{10}/PM_{2.5}$ (IMF08) during unloading of new sorbent. The spent sorbent silo emits $PM/PM_{10}/PM_{2.5}$ (IMF09) (with sulfur and acid gases bound in the material) during the loading of spent sorbent.

Rockwool's protocol mandates a shutdown for 2 weeks of each year to conduct routine maintenance on the facility. As a result, the hours of operation for the mineral wool production line are proposed to be modified from 8,760 to 8,400 hours per year to represent the maximum potential operating hours for the facility. This modification applies to the following emission points in the melting process:

- Pre-heat Burner (IMF24); and
- Melting Furnace (IMF01).

The emission points for material handling operations, tanks, and paved roads remains unchanged at 8,760 hours per year.

It is proposed to remove 8 pounds/hour (35.04 tons/year) of Carbon Monoxide from the Melting Furnace (IMF01) potential to emit and add it to the WESP (HE01) potential to emit. The new Melting Furnace (IMF01) CO emission rate will be 3.21 pounds/ hour (13.48 tons/year). The Secondary Energy Materials Storage Silo (IMF07B) was not installed. The source IMF07 now only contains the Filter Fines Day Silo (IMF07A) which has also been updated to include an indoor settling factor.

Spinning, Curing, and Cooling

The melt flows out of the lower part of the furnace and is led to the spinning machine via the gutter channels. The spinners are equipped with quick-rotating wheels onto which the melt is applied.

The fibers are drawn from the wheels of the spinning machine by centrifugation combined with a powerful air stream that is blown into the spinning chamber. At the same time binder and cooling water is added to the flow of fibers. Also, the material is sprayed with de-dusting oil to give water-repellent properties and reduce dust emission in the factory and the finished products. Binder and water are dosed as small droplets through nozzles on the spinning machine.

Fibers not recovered in the spinning process are directed to the Recycle Plant for re-use in the furnace.

The binder-coated fibers are collected on a perforated surface (filter net). The fibers settle on the surface as primary wool web, and air is sucked through the perforation by means of under pressure in the chamber in a vertical direction.

Emissions from the Spinning Chamber consist primarily of filterable PM/PM₁₀/PM_{2.5}, CPM, VOC, and organic HAP (formaldehyde, methanol, phenol).

Exhaust from the Spinning Chamber will be conditioned (e.g. with quenching or water spraying) prior to the WESP (HE01).

The wool web is conveyed to the pendulum (B400) which arranges multiple layers of wool onto the wool lane. For some products the edges will be cut along the wool lane by means of a mechanical saw before the curing oven. The removed edges, which is uncured wool (wet wool) is sent to the Recycle Plant via conveyors.

The density of the secondary wool lane is measured by means of isotope or x-ray device.

The wool lane is conveyed into the Curing Oven, where the remaining water in the product is evaporated and the binder is cured by means of hot air supplied from two natural gas-fired circulation burners (via direct heating). The circulation burners have a maximum heat input capacity of 5.81 MMBtu/hr (1,700 kW) each.

A natural-gas fired afterburner controls CO, VOC, and organic HAP emissions, where after the gases are directed to the WESP (HE01). The Curing Oven afterburner is rated at 9.86 MMBtu/hr (2,000 kW) heat input capacity. Emissions from the Curing Oven consist of filterable PM/PM₁₀/ PM_{2.5}, CPM, NO_x, CO, SO₂, VOC, organic HAP (formaldehyde, methanol, phenol), CO₂, CH₄, and N₂O.

The curing oven is equipped with hoods at the inlet and outlet end to control the working environment in the event that hot air escapes the curing oven due to system pressure changes. The inlet and outlet hoods vent to the WESP (HE01).

After leaving the Curing Oven, the wool web is conveyed through a Cooling Section where ambient air (from the production hall) is sucked through the cured wool web to cool it prior to cutting.

Emissions from the Cooling Section consist of filterable PM/PM₁₀/ PM_{2.5}, CPM, VOC, organic HAP (formaldehyde, methanol, phenol) and small amounts of NO_x and CO.

In summary, the following sources will be directed to the WESP as a combined emission point HE01:

- Gutter Exhaust;
- Spinning Chamber;
- Curing Oven Hoods;
- Curing Oven (following afterburner control); and
- Cooling Section.

The following emission points in the spinning, curing, and cooling process are proposed to be modified from 8,760 to 8,400 hours per year to represent the maximum potential operating hours for the facility:

- Curing Oven (CO), Curing Oven Afterburner (CO-AB), and Cooling Section (CS) (HE01);
- Dry Ice Cleaning (DI);
- De-dusting Baghouse (CE01); and
- Vacuum Cleaning Baghouse (CE02).

The spinning, curing, and cooling section are contributors of Carbon Monoxide to the WESP (HE01). As described in the Melting section above, it is proposed to remove 8 pounds/hour (35.04 tons per year) of Carbon Monoxide from the Melting Furnace (IMF01) potential to emit and add it to the WESP (HE01) potential to emit, based upon stack testing results from a similar facility.

The combined spinning, cooling, and curing will now have a CO emission rate of 9.82 pounds/hour (37.41 tons/year).

Fleece Application Vent 1 (CM12) and Fleece Application Vent 2 (CM13) will be modified so that the annual hours of operation and application rate is reduced to 4,200 hours per year. This is

reflective of the maximum expected operation for the fleece application, considering product demand.

Product Marking (P_MARK) has not been installed and is proposed to be removed from the permit.

Fleece Application

Fleece application stations will be added to the line prior to the Curing Oven for use in specialty products. This permit requests a reduction of the annual hours of operation and application rate on Fleece Application Vents 1 & 2 (4,200 hours per year). This value is reflective of the maximum expected operations due to product demand.

Rolls of fleece (fiberglass or similar facing) will be situated at two unrolling stations, above and below the mineral wool conveyor. Each upper and lower fleece will be unrolled as a continuous sheet and directed via rollers through an open dip "bath" of binder. Each dip bath will coat one side of the upper and lower fleece with binder. The coated fleece will be directed towards the top and underside of the uncured mineral wool via rollers and placed onto the surface of the uncured wool just prior to entry into the Curing Oven. The uncured mineral wool with fleece applied to the top and underside will enter the Curing Oven, where binder in the wool and on the fleece will be cured.

Binder will be fed to the dip baths via enclosed piping from the Binder Day Tank or from IBC containers (approximately 264 gal or 1 m3). The binder coating may be the same binder that is applied in the Spinning Chamber, or it can be a special binder.

Emissions from Fleece Application will consist of fugitive VOC and organic HAP emissions resulting from surface evaporation of binder in the dip tank and binder-coated fleece just prior to the Curing Oven. The majority of emissions from the binder applied to the fleece will be controlled by the Curing Oven afterburner as the fleece is cured onto the wet mineral wool in the Curing Oven. The binder's content of organic HAPs will be below requirements for additional control per the National Emission Standards for Hazardous Air Pollutants (NESHAP) for Paper or Other Web Coating (NESHAP Subpart JJJJ).

Cutting Section

After the cooling zone, the cured wool web is labeled with product features and cut to size by a water jet and/or mechanical cutting. Edges may be trimmed prior to labeling and transported to the Recycle plant via the line granulator. Labels are branded onto the product using laser marking.

Dust from the mechanical saws is removed pneumatically and directed to a baghouse filter (CE01). The collected dust/filter material is transported via closed conveyors to the Recycle Plant.

Water/fiber generated by water jet cutting is collected in the process water system and reused in the process.

Emissions from the De-dusting Baghouse (CE01) stack consist of filterable PM/ PM₁₀/ PM_{2.5}.

Stacking, Packing and Unit Load

After cutting the products are stacked, packaged in polyethylene film, palletized (as needed), and transported to one of the storage areas for finished goods.

A paper surface may be applied to products either before final cutting or after they are cut to size. The paper applied is a pre-coated polyethylene (PE) paper which is warmed in electrically heated drums so that the paper adheres to the wool product.

Dispatch of finished goods in to trucks takes place from the unit load area.

Dust from the packaging area is collected by vacuum and directed to the Vacuum Cleaning Baghouse (CE02).

Emissions from the Vacuum Cleaning Baghouse consist of filterable PM/PM₁₀/PM_{2.5}.

Recycling Plant

The Recycle Plant is used to recovered materials (e.g., waste wool and de-dusting fines such as fibers and dust) from the mineral wool manufacturing line that would otherwise be sent to a landfill for disposal. The Recycling Plant can also receive mineral wool products returned from Rockwool customers, such as but not limited to products damaged in shipping, wool waste products from construction sites or directly from customers with the purpose to recover the material for new products.

The Recycle Plant process includes material handling by front end loaders (FEL) and conveyors, milling, and batching.

The Recycle Plant can operations are split in two ways of recycling:

- Direct recycling to the spinning chamber & wool collection process after sizing and milling, and
- Re-melting in the furnace after milling.

Direct recycling of wool waste consists of cured wool waste generated on the production line or damaged products from the warehouse. The cured wool waste is chopped up in pieces by knives in the line granulator, which is placed in the cold end building (B500) or in the edge-trim system with a cutting screw, which is placed in the curing oven building (B400).

The wool pieces are conveyed by covered belt conveyors to a closed recycling silo (B405). From the silo the wool pieces are sent via the dosing system and milled to the required size, and pneumatically conveyed in closed system back to the spinning and wool collection process.

The recycling silo and part of the closed conveyor in this system is placed outside the building.

In case of surplus of wool waste the direct recycling system will unload on the floor inside the building B240 and the wool is collected for re-melting in the furnace.

A FEL will be used to transfer wool waste from indoor collection areas inside the recycling building (B240) and into a loading hopper. Mineral wool products returned from Rockwool customers will be received in big bags (or similar) and fed to the loading hopper via FEL. The loading hopper feeds wool into the mill via a screw conveyor or similar. Wool waste may also be recycled directly to the mill by means of belt and screw conveyor system. Waste wool is ground in the mill and exits via multiple conveyors to storage silos for milled wool waste. The hopper loading is connected to the de-dusting filter system (CE01). The silo area has one exhaust (CM08), and the area with the mill has one exhaust (CM09).

All of the re-melting recycling plant transfer and milling operations are conducted indoors. The building is kept closed with a fast roller gate controlled by the movement of the FEL. The building is equipped with roof ventilation equipped with particulate filters to control the working environment for industrial hygiene purposes (ammonia odor and mobile FEL exhaust gases).

The recycling plant will consists of the following emission points:

- De-dusting vents to De-dusting Baghouse (CE01); and
- Four (4) Recycle Building Vents (CM08, CM09, CM10, CM11).

Binder

Binders will be mixed onsite. The binder raw materials (resin and other binder components) are delivered to the site via tank truck and unloaded into storage tanks or delivered in drums/totes.

The binder storage consists of a series of tanks in a tank farm which is covered with a sheet roof but has no facades. A secondary containment is included in the structure.

The materials may be stored in temperature-controlled tanks equipped with heating and cooling as required. From the storage tanks the components are either mixed as a batch in a mixing tank or mixed in-line. Binder mixed in the Binder Mix Tank is pumped to the Circulating Tank and from here to the Binder Day Tank in the Furnace Building.

A separate storage is made for the de-dusting oil due to fire requirements. Dedusting oil is delivered in bulk by truck or in drums or intermediate bulk container (IBC) and unloaded into the storage tanks. From the storage tank the oil is pumped into a day tank in the furnace building (B300) and from there dosed into the spinning & wool collection process.

Rockwool will use varying binder formulations as technology advances to produce formaldehyde-free resins. This application is designed to address the use of varying resin materials.

The binder consists of aqueous ammonia, silane (coupling agent), silicone oil/resin, ammonium sulfate, water, and sugar syrup that are added to the resin. Additional components of the binder that are present in alternative resins are methanol, organic acid, and inorganic acid.

Tanks storing aqueous ammonia, ammonium sulfate, water, and sugar syrup do not emit regulated pollutants, but are included in this application for completeness.

Emissions from unloading, storage, and mixing of binder consist of VOC and organic HAP (formaldehyde, phenol, methanol).

Dry Ice Cleaning

For mineral wool products where product quality requirements necessitate additional cleaning of the perforated filter net dry ice will be applied for cleaning. The filter net may also be cleaned using with water. Dry ice pellets will be used for cleaning via blasting onto the perforated filter net. A pressurized storage tank will feed liquid CO_2 to a pelletizer unit which will form dry ice pellets (solid CO_2). The system continuously produces dry ice pellets which are fed to a blasting gun that directs the pellets to the perforated filter net.

Emissions from the production of dry ice pellets and the cleaning activities consist of fugitive CO_2 .

OTHER OPERATIONS

Building Heat with Natural Gas Boilers

Building heat is supplied with natural gas boilers. Two natural gas-fired boilers were installed to provide a source of building heat when the furnace is not in operation (CM03, CM04). These two boilers were installed at a lower maximum rated heat input capacity of 4.99 MMBtu/hr (originally permitted at 5.1 MMBtu/hr).

The Rockfon building's natural gas-fired boiler for building heating (RFN10) is proposed to be removed from the permit.

Emergency Fire Pump Engines

The diesel engine fire pump was installed with a rating of 316 horsepower (hp) (236 kW). The emission factors for this source have been updated to reflect the manufacturer rating data, where available.

The engine is certified to NSPS Subpart IIII engine standards and will operate only during emergencies or other limited scenarios as allowed by federal rules (i.e., maintenance checks, readiness testing, etc.).

Process Water System

The process water system consists of a series of tanks and a filter for recirculation of process water. The collected water is filtered on a band filter and stored in buffer tanks.

The filtered process water is used for dilution of binder and for flushing of processes (e.g. to transport fibers back in the system). Process water is also used for operation of the WESP. Process water is collected storm water from outside areas to compensate for water loss due to evaporation. Additional water is supplied from the public water supply.

Storage Tanks

The following storage tanks are being added to the permit:

- One (1) Vertical Additive Buffer Tank, TK-ADB1 (396 gallons);
- One (1) Vertical Additive Buffer Tank, TK-ADB2 (132 gallons); and
- One (1) Vertical Glycol Storage Tank, TK-GLY (396 gallons).

The following storage tanks have updated sizing:

- One (1) Thermal Oil Horizontal Tank, TK-TO3 (5,283 gallons, previously 2,642 gallons);
- One (1) Thermal Oil Horizontal Expansion Tank, TK-TO4 (1,928 gallons, previously 1,321 gallons);
- Six (6) Resin Vertical Storage Tanks, TK-RS1 TK-RS6 (13,209 gallons each, previously 15,850 gallons);
- One (1) Coupling Agent Vertical Storage Tank, TK-CA (396 gallons, previously 264 gallons); and
- One (1) Additive Vertical Storage Tank, TK-AD (396 gallons, previously 53 gallons).

The following storage tanks have been updated with current AP-42 calculation methodology:

- One (1) Diesel Fuel Horizontal Storage Tank, TK-DF (1,242 gallons);
- Three (3) Binder Storage Containers, TK-BS1-TK-BS3, (ea. 264 gallons); and
- One (1) De-dust Oil Vertical Day Tank, TK-DOD (264 gallons).

The following storage tanks were not installed and are proposed to be removed from the permit:

- One (1) Used Oil Horizontal Storage Tank, TK-UO (581 gallons);
- One (1) Resin Vertical Storage Tank, TK-RS7 (15,850 gallons);
- One (1) Vertical Binder Mix Tank, TK-BM (2,642 gallons);
- One (1) De-dust Oil Vertical Storage Tank, TK-DO (15,850 gallons);
- One (1) Vertical Binder Circulating Tank, TK-BC (4,227 gallons);
- One (1) Binder Vertical Day Tank, TK-BD (793 gallons).

- One (1) Thermal Oil Horizontal Expansion Tank, TK-TO1 (212 gallons);
- One (1) Thermal Oil Horizontal Drain Tank, TK-TO2 (159 gallons);
- One (1) Paint Dilution Storage Tank, TK-PD (793 gallons); and
- One (1) Paint Dilution Day Tank, TK-PDD (397 gallons).
- •

If the storage tank is not included in one of these lists, it will remain as originally permitted.

Rockfon Line

The Rockfon Production Line has no plans to be constructed and is proposed to be removed from the permit. This removal applies to the following emission points:

- IR Zone (RFNE1);
- Hot and Press Cure (RFNE2);
- High Oven A (RFNE3);
- High Oven B (RFNE9);
- Drying Oven 1 (RFNE4);
- Drying Oven 2 & 3 (RFNE6);
- Spray Paint Cabin (RFNE5);
- Cooling Zone (RFNE7); and
- De-dusting Baghouse (RFNE8).

Energy Material Handling

The emission points from this section were not installed and are proposed to be removed from the permit. These emission points are:

- Three (3) Coal Storage Silos (IMF03A, IMF03B, IMF03C); and
- One (1) Coal Feed Tank (IMF25).

Cooling Towers

The two cooling towers were not installed, and are proposed to be removed from the permit:

- Melting Furnace Cooling Tower (IMF02); and
- Gutter Cooling Tower (HE02).

Coal Milling

The emission points from this section were not installed and are proposed to be removed from the permit. These emission points are:

- Coal Conveyor Transition Point (B231 to B235) (IMF13);
- Coal Mill Burner & Baghouse (IMF05);
- Coal Milling De-dusting Baghouse (IMF06);

- Coal Conveyor Transition Point (B231 to B235) (IMF04);
- Fugitive emissions from Coal Unloading (B230);
- Fugitive emissions from Coal Loading Hopper (B231); and
- Fugitive emissions from Coal Milling Building (B235).

Emission Units Table

(includes all emission units and air pollution control devices

that will be part of this permit application review, regardless of permitting status)

| Emission Unit ID ¹ | Emission Point ID ² | Emission Unit Description | Year Installed/ Modified | Design Capacity | Type ³ and Date of Change | Control Device ⁴ |
|----------------------------------|-----------------------------------|---|--------------------------------|---|--|--------------------------------|
| | | L1 Mi | nwool Line | | 1 | |
| B210/211 | B210/211 | Raw Material Storage | 2021 | 716 ton/day | No Change [*] | 3-sided with cover |
| RMS | RMS | Raw Material Outdoor Stockpile | 2021 | 0.12 acres 500 m ² | Modification | 3-sided enclosur |
| B215 | B215 | Raw Material Loading Hopper | NA | 562 ton/day | No Change | 3-sided w/cove |
| IMF11 | IMF11 | Conveyor Transition Point (B215 to B220) | 2021 | 1,137 scfm (1,800 Nm ³ /h) | Modification | IMF11-FF Enclosed Indoor |
| IMF17 | IMF17 | B220 Material Handling | 2021 | 716 ton/day | Modification | Enclosed Indoor |
| IMF12 | IMF12 | Conveyor Transfer Point (B215) | 2021 | 716 ton/day | Modification | Enclosed Indoo |
| IMF16 | IMF16 | Conveyor Transfer Point (B300) | 2021 | 716 ton/day | Modification | Enclosed Indoo |
| IMF15 | IMF15 | Outside B220 Transfer Point | 2021 | 716 ton/day | Modification | 4-sided drop guard |
| RM_REJ | RM_REJ | Raw Material Reject Collection Drop | NA | 6 ton/day | No Change | 4-sided rubber drop guards |
| IMF21 | IMF21 | Charging Building Vacuum Cleaning Filter | NA | 316 scfm (500 Nm3/h) | No Change | None |
| IMF24 | IMF24 | Pre-heat Burner | 2021 | 5.12 MMBtu/hr | Modification | None |
| IMF01 | IMF01 | Melting Furnace | 2021 | 21,414 scfm | Modification | IMF01-BH De-NOx De-SOx |
| IMF07 | IMF07 | Filter Fines Day Silo | 2021 | 790 scfm (1,250 Nm ³ /h) | Modification | IMF07A-FF Enclosed Indoo |
| IMF07B | IMF07 | Secondary Energy Materials Silo | NA | 790 scfm (1,250 Nm3/h) | Removal | IMF07B-FF |
| IMF10 | IMF10 | Filter Fines Receiving Silo | NA | 758 scfm (1,200 Nm3/h) | No Change | None |
| IMF08 | IMF08 | Sorbent Silo | NA | 758 scfm (1,200 Nm3/h) | No Change | None |
| IMF09 | IMF09 | Spent Sorbent Silo | NA | 758 scfm (1,200 Nm3/h) | No Change | None |
| DI | DI | Dry Ice Cleaning | 2021 | 630,000 kg/year | Modification | None |
| CM12 | CM12 | Fleece Application Vent 1 | 2021 | 388,500 kg/year | Modification | None |
| CM13 | CM13 | Fleece Application Vent 2 | 2021 | | Modification | None |
| СО | HE01 | Curing Oven | 2021 | 18,950 scfm Confidential | Modification | HE01 CO-AB |
| CO-AB | HE01 | Curing Oven Afterburner | 2021 | 9.86 MMBtu/hr | Modification | HE01 |
| CO-HD | HE01 | Curing Oven Hoods | NA | 25,267 scfm (40,000 Nm ³ /hr) | Modification | HE01 |
| GUT-EX | HE01 | Gutter Exhaust | NA | 15,792 scfm (25,000 Nm ³ /hr) | Modification | HE01 |

Emission Units Table (includes all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status)

| Emission Unit ID ¹ | Emission Point ID ² | Emission Unit Description | Year Installed/ Modified | Design Capacity | Type ³ and Date of Change | Control Device ⁴ |
|----------------------------------|-----------------------------------|--|--------------------------------|---|--|--------------------------------|
| SPN | HE01 | Spinning Chamber | NA | 258,986 scfm (410,000 Nm ³ /hr) | Modification | HE01 |
| CS | HE01 | Cooling Section | 2021 | 50,534 scfm | Modification | HE01 |
| CE01 | CE01 | De-dusting Baghouse | 2021 | 44,217 scfm (70,000 Nm3/h) | Modification | Baghouse |
| CE02 | CE02 | Vacuum Cleaning Baghouse | 2021 | 12,633 scfm (20,000 Nm3/h) | Modification | Baghouse |
| P_MARK | P_MARK | Product Marking | 2021 | NA | Removal | NA |
| CM10 | CM10 | Recycle Plant Building Vent 1 | NA | 18,950 scfm (30,000 Nm3/h) | No Change | None |
| CM11 | CM11 | Recycle Plant Building Vent 2 | NA | 18,950 scfm (30,000 Nm3/h) | No Change | None |
| CM08 | CM08 | Recycle Plant Building Vent 3 | NA | 1,579 scfm (2,500 Nm3/h) | No Change | None |
| CM09 | СМ09 | Recycle Plant Building Vent 4 | NA | 1,579 scfm (2,500 Nm3/h) | No Change | None |
| IMF14 | IMF14 | Raw Material Reject Stockpile | 2021 | 0.002 acres 10 m ² | Modification | 3-sided enclosur |
| B170 | B170 | Melting Fumace Portable Crusher & Storage | NA | 1,800 ton/day | No Change | 3-sided enclosur |
| S_REJ | S_REJ | Sieve Reject Collection Bin | 2021 | NA | Removal | 4-sided rubber drop guard |
| IMF25 | IMF25 | Coal Feed Tank | 2021 | 758 scfm (1,200 Nm3/h) | Removal | IMF25-FF |
| HE02 | HE02 | Gutter Cooling Tower | 2021 | 308 gpm (70 m3/hr) | Removal | None |
| IMF18 | IMF18 | Charging Material Handling Vent 2 | 2021 | NA | Removal | IMF17/18 – FF |
| IMF02 | IMF02 | Furnace Cooling Tower | NA | 1,321 gpm (300 m3/h) | Removal | None |
| | | Rockfon I | Production | | | |
| RFNE1 | RFNE1 | IR Zone | NA | 1,895 scfm (3,000 Nm3/h) | Removal | None |
| RFNE2 | RFNE2 | Hot Press and Cure | NA | 1,895 scfm (3,000 Nm3/h) | Removal | None |
| RFNE3 | RFNE3 | High Oven A | NA | 5,053 scfm (8,000 Nm3/h) | Removal | None |
| RFNE9 | RFNE9 | High Oven B | NA | 5,053 scfm (8,000 Nm3/h) | Removal | None |
| RFNE4 | RFNE4 | Drying Oven 1 | NA | 3,158 scfm (5,000 Nm3/h) Removal | | Particulate Filter |
| RFNE6 | RFNE6 | Drying Oven 2 & 3 | NA | 7,580 scfm (12,000 Nm3/h) | Removal | Particulate Filter |

Emission Units Table (includes all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status)

| Emission Unit ID ¹ | Emission Point ID ² | Emission Unit Description | Year Installed/ Modified | Design Capacity | Type ³ and Date of Change | Control Device ⁴ |
|----------------------------------|-----------------------------------|--|--------------------------------|---------------------------------|--|------------------------------------|
| RFNE5 | RFNE5 | Spray Paint Cabin | NA | 6,317 scfm (10,000 Nm3/h) | Removal | Particulate Filter |
| RFNE7 | RFNE7 | Cooling Zone | NA | 15,792 scfm (25,000 Nm3/h) | Removal | None |
| RFNE8 | RFNE8 | De-dusting Baghouse | NA | 74,419 scfm (117,813 Nm3/h) | Removal | Baghouse |
| RFN10 | RFN10 | RFN Building Heat | NA | NA | Removal | NA |
| | | Coa | l Milling | | | |
| IMF05 | IMF05 | Coal Milling Bumer & Baghouse | 2018 | 2,873 scfm (4,547 Nm3/h) | Removal | IMF05-BH |
| IMF06 | IMF06 | Coal Milling De-Dusting Baghouse | 2018 | 6,317 scfm (10,000 Nm3/h) | Removal | IMF06-BH |
| IMF04 | IMF04 | Coal Conveyor Transition Point (B231 to B235) | 2018 | 1,137 scfm (1,800 Nm3/h) | Removal | IMF04-FF |
| IMF13 | IMF13 | Coal Conveyor Transition Point (B231 to B235) | 2018 | 1,137 scfm (1,800 Nm3/h) | Removal | IMF13-FF |
| B235 | B235 | Coal Milling Building | 2018 | NA | Removal | Enclosed Indoors |
| B230 | B230 Coal Unloading | | 2018 | NA | Removal | 3-sided enclosure with cover |
| B231 | B231 | Coal Unloading Hopper | 2018 | NA | Removal | 3-sided enclosure with cover |
| IMF03A | IMF03A | Coal Storage Silo A | NA | 758 scfm (1,200 Nm3/h) | Removal | IMF03A-FF |
| IMF03B | IMF03B | Coal Storage Silo B | NA | 758 scfm (1,200 Nm3/h) | Removal | IMF03B-FF |
| IMF03C | IMF03C | Coal Storage Silo C | NA | 758 scfm (1,200 Nm3/h) | Removal | IMF03C-FF |
| | | Other Facilit | y-₩ide So | | | |
| CM03 | CM03 | Natural Gas Boiler 1 | 2021 | 4.99 MMBtu/h (1.462 MW) | Modification | None |
| CM04 | СМ04 | Natural Gas Boiler 2 | 2021 | 4.99 MMBtu/h (1.462 MW) | Modification | None |
| EFP1 | EFP1 | Emergency Fire Pump | 2021 | 316 hp (236 kw) | Modification | None |
| Rd_RM | RD_RM | Raw Material Paved Haul Roads | NA | NA | No Change | None |
| Rd_FP | Rd_FP | Finished Product Paved Haul Road | NA | NA | No Change | None |
| | | Facility | Storage Ta | | | |
| TK-DF | TK-DF | Diesel Fuel Tank | 2021 | 1,242 gal 4.7 m ³ | Modification | None |

Emission Units Table (includes all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status)

| Emission Unit ID ¹ | Emission Point ID ² | Emission Unit Description | Year Installed/ Modified | Design Capacity | Type ³ and Date of Change | Control Device ⁴ |
|----------------------------------|-----------------------------------|---|--------------------------------|---------------------------------|--|--------------------------------|
| TK-UO | TK-UO | Used Oil Tank | 2018 | 581 gal 2.2 m3 | Removal | None |
| TK-DO | TK-DO | De-dust Oil Storage Tank | 2021 | 15,850 gal 35.7 m3 | Removal | None |
| TK-TO1 | TK-TO1 | Thermal Oil Expansion Tank – Rockfon | 2021 | 212 gal 0.8 m ³ | Removal | None |
| TK-TO2 | TK-TO2 | Thermal Oil Drain Tank – Rockfon | 2021 | 159 gal 0.6 m ³ | Removal | None |
| ТК-ТОЗ | ТК-ТОЗ | Thermal Oil Tank – IMF | 2021 | 5,283 gal 20 m ³ | Modification | None |
| TK-TO4 | TK-TO4 | Thermal Oil Expansion Tank – IMF | 2021 | 1,928 gal 7.3 m ³ | Modification | None |
| TK-RS1 | TK-RS1 | Resin Storage Tank | 2021 | 13,209 gal 50 m ³ | Modification | None |
| TK-RS2 | TK-RS2 | Resin Storage Tank | 2021 | 13,209 gal 50 m ³ | Modification | None |
| TK-RS3 | TK-RS3 | Resin Storage Tank | 2021 | 13,209 gal 50 m ³ | Modification | None |
| TK-RS4 | TK-RS4 | Resin Storage Tank | 2021 | 13,209 gal 50 m ³ | Modification | None |
| TK-RS5 | TK-RS5 | Resin Storage Tank | 2021 | 13,209 gal 50 m ³ | Modification | None |
| TK-RS6 | TK-RS6 | Resin Storage Tank | 2021 | 13,209 gal 50 m ³ | Modification | None |
| TK-RS7 | TK-RS7 | Resin Storage Tank | 2018 | 15,850 gal 60 m3 | Removal | None |
| TK-BM | ТК-ВМ | Binder Mix Tank | 2021 | 2,642 gal 10 m3 | Removal | None |
| TK-BC | TK-BC | Binder Circulation Tank | 2021 | 4,227 gal 16 m3 | Removal | None |
| TK-BD | TK-BD | Binder Day Tank | 2021 | 793 gal 3 m3 | Removal | None |
| TK-CA | TK-CA | Coupling Agent Storage Tank | 2021 | 396 gal 1.5 m ³ | Modification | None |
| TK-AD | TK-AD | Additive Storage Tank | 2021 | 396 gal 1.5 m ³ | Modification | None |
| TK-BS1 | TK-BS1 | Binder Storage Container | 2021 | 264 gal 1 m ³ | Modification | None |
| TK-BS2 | TK-BS2 | Binder Storage Container | 2021 | 264 gal 1 m ³ | Modification | None |
| TK-BS3 | TK-BS3 | Binder Storage Container | 2021 | 264 gal 1 m ³ | Modification | None |
| TK-DOD | TK-DOD | De-dust Oil Day Tank | 2021 | 264 gal 1 m ³ | Modification | None |

Emission Units Table (includes all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status)

| Emission Unit ID ¹ | Emission Point ID ² | Emission Unit Description | Year Installed/ Modified | Design Capacity | Type ³ and Date of Change | Control Device ⁴ |
|----------------------------------|-----------------------------------|---------------------------|--------------------------------|-------------------------------|--|--------------------------------|
| TK-ADB1 | TK-ADB1 | Additive Buffer Tank | 2021 | 396 gal 1.5 m ³ | New | None |
| TK-ADB2 | TK-ADB2 | Additive Buffer Tank | 2021 | 132 gal 0.5 m ³ | New | None |
| TK-GLY | TK-GLY | Glycol Tank | 2021 | 396 gal 1.5 m ³ | New | None |
| TK-PD | TK-PD | Paint Dilution Tank | NA | 793 gal 3 m ³ | Removal | None |
| TK-PDD | TK-PDD | Paint Dilution Day Tank | NA | 397 gal 1.5 m ³ | Removal | None |

¹ For Emission Units (or <u>Sources</u>) use the following numbering system:1S, 2S, 3S,... or other appropriate designation. ² For <u>E</u>mission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation. ³ New, modification, removal

⁴ For <u>C</u>ontrol Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

At the time of this permit application submittal, B211 has not been constructed. However, there are plans to construct B211 in the future.

Attachment J EMISSION POINTS DATA SUMMARY SHEET

| | | | | | | | | : Emission | | | | | | | | | | | | | | | | | | | |
|-----------------------------|---------------------|-------------------------------|---------|--------------|---------------------------|--------------------|----------------|---|--------|-------------------|-----------------------|-------------------------------------|---|-------------------|---------------------------------|---|---|---|---|---|--|--|---|--|--|--|--|
| Emission Point ID No. | Emission Point | Emissic Vented T This I | Fhrough | Control | llution Device | Vent Ti Emissio | on Unit | All Regulated Pollutants - Chemical | Uncont | rolled | Maximum Controlled | Potential Emissions ⁵ | Emission Form or Phase | Est. Method | Emission Concen | | | | | | | | | | | | |
| (Must match Emission | Type ¹ | (Must) Emission U | match | Units Tal | ch Emission ble & Plot | (chemical) oni | | Name/CAS | Emiss | ions ⁴ | | | (At exit conditions, Solid, Liquid or | Used ⁶ | tration ⁷ (ppmv o | | | | | | | | | | | | |
| Units Table & Plot Plan) | | & Plot | | Pla | - | Short | | (Speciate VOCs & HAPS) | | | | | Gas/Vapor) | | mg/m3) | | | | | | | | | | | | |
| , | | ID No. | Source | ID No. | Device Type | Term ² | Max (hr/yr) | | lb/hr | ton/yr | lb/hr | ton/yr | | | | | | | | | | | | | | | |
| | | | | | | | Min | eral Wool I | line | | | | | | | | | | | | | | | | | | |
| IMF11 | Enclosed Indoors | IMF11 | Volume | IMF11-FF | Fabric Filter | С | 8400 | PM ₁₀ | | | <0.01 | <0.01 | Solid | EE | | | | | | | | | | | | | |
| | muoors | | | | Filter | | | PM _{2.5} | | | 0.36 | 1.52 | | | | | | | | | | | | | | | |
| | | | | | | | | NOx SO ₂ | | | 0.00 | 0.01 | | | | | | | | | | | | | | | |
| | | | | | | | | CO | | | 0.42 | 1.76 | - | | | - | | | | | | | | | | | |
| | | | | | | | | VOCs | | | 0.03 | 0.12 | | | | | | | | | | | | | | | |
| | Upward | | | | | | | PM ₁₀ | | | 0.04 | 0.16 | Gas/Vapor, | | | | | | | | | | | | | | |
| IMF24 | Vertical Stack | IMF24 | Volume | | | С | 8400 | PM _{2.5} | | | 0.04 | 0.16 | Solid | EE | | | | | | | | | | | | | |
| | | | | | | | | CO ₂ e | | | 599.87 | 2519.44 | | | | | | | | | | | | | | | |
| | | | | | | | | Lead | | | < 0.01 | < 0.01 | | | | | | | | | | | | | | | |
| | | | | | | | | Hexane | | | 0.01 | 0.04 | | | | | | | | | | | | | | | |
| | | | | | | | | Total HAPs | | | 0.01 | 0.04 | | | | | | | | | | | | | | | |
| | | | | | | | | NOx | | | 37.37 | 156.95 | | | | | | | | | | | | | | | |
| | | | | | | | | SO ₂ | | | 33.63 | 141.25 | | | | | | | | | | | | | | | |
| | | | | | | | | CO | | | 3.21 | 13.48 | 9 |) | |) | 2 | 9 | 9 | 9 | | | 9 | | | | |
| | | | | | | | | VOCs | | | 0.31 | 1.29 | | | | | | | | | | | | | | | |
| | | | | | | | | PM ₁₀ | | | 2.32 | 9.73 | | | | | | | | | | | | | | | |
| | | | | | | | | PM _{2.5} | | | 2.32 | 9.73 77076.96 | | | | | | | | | | | | | | | |
| | | | | | | | | CO ₂ e | | | 18551.00 | 7.85 | | | | | | | | | | | | | | | |
| | | | | | | | | H ₂ SO ₄ Lead | | | <0.01 | <0.01 | | | | | | | | | | | | | | | |
| IMF01 | Upward Vertical | IMF01 | Point | IMF01- | BH SCR | С | 8400 | HF | | | 0.37 | 1.55 | Gas/Vapor | EE | | | | | | | | | | | | | |
| | Stack | | | BH | SIS | _ | | HCl | | | 0.30 | 1.24 | | 22 | | | | | | | | | | | | | |
| | | | | | | | | COS | | | 0.37 | 1.57 | | | | | | | | | | | | | | | |
| | | | | | | | | Formaldehyd | | | < 0.01 | 0.02 | | | | | | | | | | | | | | | |
| | | | | | | | | e Arsenic | | | < 0.01 | <0.01 | | | | | | | | | | | | | | | |
| | | | | | | | | Mercury | | | <0.01 | <0.01 | | | | | | | | | | | | | | | |
| | | | | | | | | Phenol | | | <0.01 | <0.01 | - | - | - | - | | | | | | | | | | | |
| | | | | | | | | Mineral Fiber | | | 2.32 | 9.73 | | | | | | | | | | | | | | | |
| | | | | | | | | | | | 2.42 | 14.42 | | | | | | | | | | | | | | | |
| | Unword | | | | | | | Total HAPs | | | 3.43 | 14.42 | | | | | | | | | | | | | | | |
| IMF07 | Upward Vertical | IMF07 | Point | IMF07 -FF | FF | С | 8400 | PM ₁₀ | | | <0.01 <0.01 | 0.01 | Solid | EE | | | | | | | | | | | | | |
| | Stack | | | | | | | PM _{2.5} NOx | | | 1.57 | 6.60 | | | | | | | | | | | | | | | |
| | | | | | | | | SO ₂ | | | 0.01 | 0.05 | | | | | | | | | | | | | | | |
| | | | | | | | | CO | | | 9.82 | 41.24 | | | | | | | | | | | | | | | |
| | | | | | | | | VOC | | | 44.65 | 187.55 | | | | | | | | | | | | | | | |
| | | | | | | | | PM ₁₀ | | | 12.00 | 50.39 | | | | | | | | | | | | | | | |
| | Upward | | | | | | | PM _{2.5} | | | 12.00 | 50.39 | | | | | | | | | | | | | | | |
| HE01 | Vertical | HE01 | Point | | | С | 8400 | CO ₂ e | | | 8492.77 | 35669.62 | Gas/Vapor, Solid | EE | | | | | | | | | | | | | |
| | Stack | | | | | | | Total HAPs | | | 56.65 | 237.95 | | | | | | | | | | | | | | | |
| | | | | | | | | Formaldehyd | | | 3.27 | 13.74 | 1 | | | | | | | | | | | | | | |
| | | | | | | | | e Phenol | | + | 17.05 | 71.61 | | | | | | | | | | | | | | | |
| | | | | | | | | Mineral Fiber | | | 12.00 | 50.39 | | | | | | | | | | | | | | | |
| | | | | | | | | | | | 24.34 | 102.21 | | | | | | | | | | | | | | | |
| | Upward | | | | | | | Methanol | | | 0.77 | 3.24 | | | | | | | | | | | | | | | |
| CE01 | Vertical | CE01 | Point | Baghouse | Filter Bag | С | 8400 | PM ₁₀ PM _{2.5} | | ├ - | 0.77 | 0.94 | Solid | EE | | | | | | | | | | | | | |
| | Stack Upward | | | | | | | PM _{2.5} PM ₁₀ | | | 0.22 | 0.94 | | | | | | | | | | | | | | | |
| CE02 | Vertical | CE02 | Point | Baghouse | Filter Bag | С | 8400 | PM ₁₀ PM _{2.5} | | | 0.22 | 0.93 | Solid | EE | 1 | | | | | | | | | | | | |

| | | | | | Oth | er RAN | Facility-Wide S | ources | | | | | |
|------|--------------------|--------|-------|-------|-----|--------|-------------------|--------|--------------|--------------|---------------------|----|--|
| | | | | | | | NOx | | 0.18 | 0.77 | | | |
| | | | | | | | SO ₂ | | < 0.01 | 0.01 | | | |
| | | | | | | | СО | | 0.41 | 1.79 | | | |
| | | | | | | | VOC | | 0.03 | 0.12 | | | |
| CM03 | Upward Vertical | CM03 | Point | | с | 8760 | PM ₁₀ | | 0.04 | 0.16 | Gas/Vapor, | EE | |
| CM05 | Stack | CIVIUS | Point | | C | 8700 | PM _{2.5} | | 0.04 | 0.16 | Solid | EE | |
| | | | | | | | CO ₂ e | | 584.32 | 2559.32 | | | |
| | | | | | | | Lead | | < 0.01 | < 0.01 | | | |
| | | | | | | | Hexane | | 0.01 | 0.04 | | | |
| | | | | | | | Total HAPs | | 0.01 | 0.04 | | | |
| | | | | | | | NOx | | 0.18 | 0.77 | | | |
| | | | | | | | SO ₂ | | < 0.01 | 0.01 | | | |
| | | | | | | 8760 | СО | | 0.41 | 1.79 | | | |
| | | | | | | | VOC | | 0.03 | 0.12 | | | |
| CM04 | Upward Vertical | CM04 | Point | Point | С | | PM ₁₀ | | 0.04 | 0.16 | Gas/Vapor, Solid | EE | |
| CM04 | Stack | CIVI04 | ronn | | | | PM _{2.5} | | 0.04 | 0.16 | | EE | |
| | | | | | | | CO ₂ e | | 584.32 | 2559.32 | | | |
| | | | | | | | Lead | | < 0.01 | < 0.01 | | | |
| | | | | | | | Hexane | | 0.01 | 0.04 | | | |
| | | | | | | | Total HAPs | | 0.01 | 0.04 | | | |
| | | | | | | | NOx | | 1.80 | 0.45 | | | |
| | | | | | | | SO ₂ | | < 0.01 | < 0.01 | | | |
| | | | | | | | СО | | 0.40 | 0.10 | | | |
| | | | | | | | VOC | | 0.04 | 0.01 | | | |
| | | | | | | | PM ₁₀ | | 0.08 | 0.02 | | | |
| | | | | | | | PM _{2.5} | | 0.08 | 0.02 | | | |
| | Upward | | | | | | CO ₂ e | | 362.00 | 90.50 | | | |
| EFP1 | Vertical Stack | EFP1 | Point | | EM | 500 | Formaldehyd e | | < 0.01 | < 0.01 | Gas/Vapor | EE | |
| | Stuck | | | | | | Benzene | | < 0.01 | < 0.01 | | | |
| | | | | | | | Acetaldehyde | | < 0.01 | <0.01 | | | |
| | | | | | | | Toluene | | < 0.01 | < 0.01 | | | |
| | | | | | | | Xylene | | <0.01 | <0.01 | | | |
| | | | | | | | PAH | | <0.01 | <0.01 | | | |
| | | | | | | | Total HAPs | | <0.01 | <0.01 | | | |
| | | | | | | | Total HAPS | | ~0.01 | \0.01 | | | |

RAN Facility Storage Tanks

| | | | | | | | | | | | | • | | |
|--------|------|---------|-------|-------|------|------|-------------------|--------|--------|--------|--------|-----------|--------------------|--|
| TK-DF | Vent | TK-DF | Point | | С | 8760 | VOC | < 0.01 | < 0.01 | <0.01 | < 0.01 | Gas/Vapor | Emission Master | |
| TK-TO3 | Vent | TK- TO3 | Point | | С | 8760 | VOC | <0.01 | <0.01 | <0.01 | <0.01 | Gas/Vapor | Emission Master | |
| TK-TO4 | Vent | TK- TO4 | Point | | С | 8760 | VOC | < 0.01 | <0.01 | <0.01 | <0.01 | Gas/Vapor | Emission Master | |
| | | | | | | | Formaldehyd e | < 0.01 | 0.02 | <0.01 | 0.02 | | . | |
| TK-RS1 | Vent | TK- RS1 | Point | | С | 8760 | Methanol | < 0.01 | < 0.01 | < 0.01 | < 0.01 | Gas/Vapor | Emission Master | |
| | | | | | | | VOC | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| | | | | | | | Total HAPs | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| | | | | | | | Formaldehyd e | < 0.01 | 0.02 | <0.01 | 0.02 | | Emission | |
| TK-RS2 | Vent | TK- RS2 | Point | | С | 8760 | Methanol | < 0.01 | < 0.01 | < 0.01 | < 0.01 | Gas/Vapor | Emission Master | |
| | | | | | | | VOC | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| | | | | | | | Total HAPs | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| | | | | | | | Formaldehyd e | < 0.01 | 0.02 | < 0.01 | 0.02 | | E distante | |
| TK-RS3 | Vent | TK- RS3 | Point | | С | 8760 | Methanol | < 0.01 | < 0.01 | < 0.01 | < 0.01 | Gas/Vapor | Emission Master | |
| | | | | | | | VOC | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| | | | | | | | Total HAPs | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| | | | | | | | Formaldehyd e | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| TK-RS4 | Vent | TK- RS4 | Point | | С | 8760 | Methanol | < 0.01 | < 0.01 | < 0.01 | < 0.01 | Gas/Vapor | Emission Master | |
| | | | | | | | VOC | < 0.01 | 0.02 | < 0.01 | 0.02 | | linabier | |
| | | | | | | | Total HAPs | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| | | | | | | | Formaldehyd e | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| TK-RS5 | Vent | TK- RS5 | Point | | С | 8760 | Methanol | < 0.01 | < 0.01 | < 0.01 | < 0.01 | Gas/Vapor | Emission Master | |
| | | | | | | | VOC | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| | | -+ | | | | | Total HAPs | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| | | | | | | | Formaldehyd e | < 0.01 | 0.02 | < 0.01 | 0.02 | | | |
| TK-RS6 | Vent | TK- RS6 | Point | | С | 8760 | Methanol | < 0.01 | < 0.01 | < 0.01 | < 0.01 | Gas/Vapor | Emission Master | |
| | | | | | | | VOC | < 0.01 | 0.02 | < 0.01 | 0.02 | 1 | Waster | |
| | | | | | | | Total HAPs | < 0.01 | 0.02 | < 0.01 | 0.02 | 1 | | |
| TK-CA | Vent | TK-CA | Point | | С | 8760 | VOC | < 0.01 | <0.01 | <0.01 | <0.01 | Gas/Vapor | Emission Master | |
| TK-AD | Vent | TK-AD | Point | | С | 8760 | VOC | <0.01 | <0.01 | <0.01 | <0.01 | Gas/Vapor | Emission Master | |
| | | | | | | | Formaldehyd e | < 0.01 | <0.01 | <0.01 | <0.01 | | | |
| TK-BS1 | Vent | TK- BS1 | Point | | С | 8760 | Methanol | < 0.01 | < 0.01 | < 0.01 | < 0.01 | Gas/Vapor | Emission | |
| | | | | | | | VOC | < 0.01 | < 0.01 | < 0.01 | < 0.01 | 1 | Master | |
| | | | | | | | Total HAPs | < 0.01 | < 0.01 | < 0.01 | < 0.01 | 1 | | |
| | | | | | | | Formaldehyd e | <0.01 | <0.01 | < 0.01 | <0.01 | | | |
| TK-BS2 | Vent | TK- BS2 | Point | | С | 8760 | | < 0.01 | < 0.01 | < 0.01 | < 0.01 | Gas/Vapor | Emission | |
| | | | | | | | VOC | <0.01 | < 0.01 | <0.01 | <0.01 | 1 | Master | |
| | | | | | | | Total HAPs | < 0.01 | < 0.01 | < 0.01 | < 0.01 | 1 | | |
| | | | | | | | Formaldehyd e | <0.01 | <0.01 | <0.01 | <0.01 | | | |
| TK-BS3 | Vent | TK- BS3 | Point | | С | 8760 | Methanol | < 0.01 | < 0.01 | < 0.01 | < 0.01 | Gas/Vapor | Emission | |
| | | | | | | | VOC | <0.01 | < 0.01 | <0.01 | < 0.01 | | Master | |
| | | | | | | | Total HAPs | <0.01 | < 0.01 | <0.01 | < 0.01 | | | |
| TK-DOD | Vent | TK- DOD | Point | | С | 8760 | VOC | < 0.01 | <0.01 | <0.01 | <0.01 | Gas/Vapor | Emission Master | |
| | | | | L. L. | | | ote that uncantur | | L. | L | L | L | | |

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit memissions are not typically considered to be fugitive and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all verted emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugitive emission activities.

¹Please add descriptors such as upward vertical stack, downward vertical stack, horizontal stack, relief vent, rain cap, etc.

² Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (ie., 15 min/hr). Indicate as many rates as needed to clarify frequency of venting (e.g., 5 min/day, 2 days/wk).

³ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. DO NOT LIST H₂, H₂O, N₂, O₂, and Noble Gases.

⁴ Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
 ⁶ Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
 ⁶ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).
 ⁷ Provide for all pollutant emissions. Typically, the units of malligram per dry cubic meter (mg/m³) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO₂, use units of ppmv (see 45CSR10).

Attachment J EMISSION POINTS DATA SUMMARY SHEET

| | | | Table 2: | Release Param | eter Data | | | |
|---|-------------------------|--------------|--|-------------------|---|---|-------------|-----------|
| | | | Exit Gas | | Emission Point | Elevation (ft) | UTM Coordin | ates (km) |
| Emission Point ID No. (Must match Emission Units Table) | Inner Diameter (ft.) | Temp. (°F) | Volumetric Flow 1 (acfm) at operating conditions | Velocity (fps) | Ground Level (Height above mean sea level) | Stack Height ² (Release height of emissions above ground level) | Northing | Easting |
| | | | N | /lineral Wool Lin | e | | | |
| IMF11 | NA | Ambient Temp | NA | NA | 581.30 | 7.19 | 4362.72065 | 252.11120 |
| IMF21 | 0.49 | 104.00 | 871.87 | 29.53 | 581.30 | 9.84 | 4362.6777 | 252.07332 |
| IMF24 | 1.15 | 482.27 | 3,749.77 | 54.43 | 581.30 | 126.25 | 4362.61797 | 252.08677 |
| IMF01 | 3.28 | 271.67 | 13,636.43 | 69.27 | 581.30 | 212.70 | 4362.64453 | 252.09348 |
| IMF07 | 1.00 | 140.27 | 280.77 | 4.66 | 581.30 | 100.26 | 4362.62904 | 252.10067 |
| IMF10 | 1.08 | 145.67 | 3322.41 | 51.15 | 581.30 | 72.93 | 4362.60804 | 252.10817 |
| IMF08 | 1.08 | 68.00 | 594.30 | 9.15 | 581.30 | 72.93 | 4362.60314 | 252.10795 |
| IMF09 | 1.08 | 145.67 | 3322.41 | 51.15 | 581.30 | 72.93 | 4362.59772 | 252.10768 |
| HE01 | 12.93 | 93.02 | 39,985.01 | 51.53 | 581.30 | 212.66 | 4362.54558 | 252.12050 |
| CE01 | 3.81 | 104 | 15,831.58 | 69.33 | 581.30 | 116.14 | 4362.53451 | 252.07615 |
| CE02 | 2.30 | 104 | 7,486.47 | 54.33 | 581.30 | 98.42 | 4362.51457 | 252.06187 |
| CM10 | 2.67 | 70.27 | 7,161.88 | 44.76 | 581.30 | 51.51 | 4362.57256 | 252.09509 |
| CM11 | 2.67 | 70.27 | 7,161.88 | 44.76 | 581.30 | 64.30 | 4362.57383 | 252.06922 |
| CM08 | 1.17 | 70.27 | 1,723.22 | 24.62 | 581.30 | 51.51 | 4362.55726 | 252.0951 |
| CM09 | 1.17 | 70.27 | 1,723.22 | 24.62 | 581.30 | 51.51 | 4362.58552 | 252.09820 |
| | | | Other R | AN Facility-Wide | Sources | | | |
| CM03 | 1.00 | 232.07 | 2,508.25 | 41.80 | 581.30 | 75.62 | 4362.63842 | 252.06266 |
| CM04 | 1.00 | 232.07 | 2,508.25 | 41.80 | 581.30 | 75.62 | 4362.63877 | 252.05549 |
| EFP1 | 0.50 | 847.67 | 3,859.03 | 128.97 | 581.30 | 13.98 | 4362.5904 | 252.18352 |

¹ Give at operating conditions. Include inerts.
 ² Release height of emissions above ground level.

FUGITIVE EMISSIONS DATA SUMMARY SHEET

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not typically considered to be fugitive, and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET.

Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

| | APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS |
|-----|---|
| 1.) | Will there be haul road activities? |
| | 🛛 Yes 🔲 No |
| | If YES, then complete the HAUL ROAD EMISSIONS UNIT DATA SHEET. |
| 2.) | Will there be Storage Piles? |
| | X Yes INO |
| | If YES, complete Table 1 of the NONMETALLIC MINERALS PROCESSING EMISSIONS UNIT DATASHEET. |
| 3.) | Will there be Liquid Loading/Unloading Operations? |
| | Yes No |
| | ☐ If YES, complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET. |
| 4.) | Will there be emissions of air pollutants from Wastewater Treatment Evaporation? |
| | □ Yes |
| | If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET. |
| 5.) | Will there be Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, open-ended valves, sampling connections, flanges, agitators, cooling towers, etc.)? |
| | Yes X No |
| | ☐ If YES, complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS UNIT DATA SHEET. |
| 6.) | Will there be General Clean-up VOC Operations? |
| | Yes No |
| | If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET. |
| 7.) | Will there be any other activities that generate fugitive emissions? |
| | XYes INO |
| | If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form. |
| | ou answered "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions nmary." |

| FUGITIVE EMISSIONS SUMMARY | All Regulated Pollutants ⁻ Chemical Name/CAS ¹ | Maximum Uncontrolled | | Maximum P Controlled En | | Est. Method |
|--|---|-------------------------|--------|----------------------------|--------|-------------------|
| | Chemical MameroAc | lb/hr | ton/yr | lb/hr | ton/yr | Used ⁴ |
| Haul Road/Road Dust Emissions | PM ₁₀ | 0.83 | 2.15 | 0.25 | 0.54 | 0- |
| Paved Haul Roads | PM _{2.5} | 0.25 | 0.53 | 0.05 | 0.13 | AP42 |
| Unpaved Haul Roads | _ | — | _ | | _ | |
| | PM | 0.11 | 0.41 | 0.02 | 0.20 | |
| Storage Pile Emissions – Raw Material Outdoor Stockpile (RMS) | PM ₁₀ | 0.05 | 0.19 | <0.01 | 0.10 | EE |
| | PM _{2.5} | <0.01 | 0.03 | <0.01 | 0.015 | |
| | PM | <0.01 | <0.01 | <0.01 | <0.01 | |
| Storage Pile Emissions – Raw Material Outdoor Reject Stockpile (IMF14) | PM ₁₀ | <0.01 | <0.01 | <0.01 | <0.01 | EE |
| | PM _{2.5} | <0.01 | <0.01 | <0.01 | <0.01 | |
| | PM | 0.13 | 0.45 | 0.08 | 0.28 | |
| Storage Pile Emissions – Raw Material Storage (B210/211) | PM ₁₀ | 0.06 | 0.21 | 0.03 | 0.13 | EE |
| | PM _{2.5} | <0.01 | 0.03 | <0.01 | 0.02 | |
| | PM | 1.12 | 0.96 | 0.16 | 0.37 | |
| Storage Pile Emissions – Melting Furnace Portable Crusher & Storage (B170) | PM ₁₀ | 0.51 | 0.45 | 0.07 | 0.17 | EE |
| | PM _{2.5} | 0.14 | 0.09 | 0.011 | 0.03 | |
| Loading/Unloading Operations | _ | — | _ | | _ | - |
| Wastewater Treatment Evaporation & Operations | _ | - | _ | - | _ | _ |
| Equipment Leaks | _ | Does not apply | _ | Does not apply | _ | - |
| General Clean-up VOC Emissions | - | - | _ | | _ | - |
| | РМ | 0.05 | 0.22 | 0.013 | 0.06 | |
| Other – Raw Material Loading Hopper (B215) | PM ₁₀ | 0.02 | 0.11 | <0.01 | 0.03 | EE |
| | PM _{2.5} | <0.01 | 0.02 | <0.01 | <0.01 | |

| FUGITIVE EMISSIONS SUMMARY | All Regulated Pollutants ⁻ Chemical Name/CAS ¹ | | l Potential Emissions ² | Maximum F Controlled Er | | Est. Method Used ⁴ |
|---|---|-------|---------------------------------------|----------------------------|-------|-------------------------------------|
| | РМ | <0.01 | <0.01 | <0.01 | <0.01 | |
| Other – Raw Material Reject Collection Drop (RM_REJ) | PM10 | <0.01 | <0.01 | <0.01 | <0.01 | EE |
| (1.1 | PM _{2.5} | <0.01 | <0.01 | <0.01 | <0.01 | |
| | РМ | 1.68 | 7.39 | 0.32 | 1.39 | |
| Other – B220 Material Handling (IMF17) | PM10 | 0.62 | 2.71 | 0.12 | 0.51 | EE |
| | PM _{2.5} | 0.62 | 2.71 | 0.12 | 0.51 | |
| | РМ | 0.07 | 0.31 | 0.014 | 0.06 | |
| Other – Conveyor Transfer Point (B215) (IMF12) | PM10 | 0.03 | 0.11 | <0.01 | 0.02 | EE |
| | PM _{2.5} | 0.03 | 0.11 | <0.01 | 0.02 | |
| | РМ | 0.07 | 0.31 | 0.014 | 0.06 | |
| Other – Conveyor Transfer Point (B300) (IMF16) | PM10 | 0.03 | 0.11 | <0.01 | 0.02 | EE |
| | PM _{2.5} | 0.03 | 0.11 | <0.01 | 0.02 | |
| | РМ | 0.07 | 0.31 | 0.014 | 0.08 | |
| Other – Outside B220 Transfer Point (B300) (IMF15) | PM10 | 0.03 | 0.11 | <0.01 | | EE |
| (····· ·-) | PM _{2.5} | 0.03 | 0.11 | <0.01 | 0.03 | |

¹ List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS₂, VOCs, H₂S, Inorganics, Lead, Organics, O₃, NO, NO₂, SO₂, SO₃, all applicable Greenhouse Gases (including CO₂ and methane), etc. DO NOT LIST H₂, H₂O, N₂, O₂, and Noble Gases.

² Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

³ Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).

⁴ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other (specify).

Attachment L EMISSIONS UNIT DATA SHEET GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on *Equipment List Form*): IMF01

| 1 Name or type and model of proposed affected equires: |
|--|
| 1. Name or type and model of proposed affected source: |
| |
| |
| Melting Furnace |
| |
| |
| 2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to |
| be made to this source, clearly indicate the change(s). Provide a narrative description of |
| all features of the affected source which may affect the production of air pollutants. |
| 3. Name(s) and maximum amount of proposed process material(s) charged per hour: |
| |
| |
| |
| Mineral Inputs (55,116 lb/hr) |
| |
| |
| |
| |
| |
| Name(s) and maximum amount of proposed material(s) produced per hour: |
| |
| |
| |
| Melted Mineral – 49,600 lb/hr |
| |
| |
| |
| |
| 5. Give chemical reactions, if applicable, that will be involved in the generation of air |
| pollutants: |
| |
| |
| |
| The chemical reactions from the Melting Furnace are caused by the combustion of |
| the raw material inputs. These combustion reactions are generally considered well |
| known and for this reason are not included. |
| |
| |
| |
| * The identification number which appears here must correspond to the air pollution control |
| device identification number appearing on the List Form. |

| 6. Combust | ion Data | (if appli | cable): | | | |
|---|-------------------|-----------|-------------------|--------------------|------------------|----------------|
| (a) Type | and amo | ount in a | ppropriate units | of fuel(s) to be b | urned: | |
| | | | | | | |
| | | | | | | |
| (b) Chen | nical ana | alvsis of | proposed fuel(| s), excluding co | al. including ma | aximum percent |
| sulfu | and ash | 1: | propossa rasi(| o), onoideg oo | a, | |
| | | | | | | |
| | | | | | | |
| NA | | | | | | |
| | | | | | | |
| | | | | | | |
| (c) Theo | retical co | mbustio | n air requireme | nt (ACF/unit of fu | el): | |
| 21,414 scfr | | | • | | | noia |
| (33,900 Nm | ³ /hr) | @ | 3,000 | °F and | 14.7 | psia. |
| (d) Perce | ent exces | ss air: | | | | |
| (е) Туре | and BTL | J/hr of b | urners and all ot | her firing equipm | ent planned to b | e used: |
| | | | | | | |
| | | | | | | |
| | | | | | | |
| | | | | | | |
| | | | | | | |
| (f) If coal is proposed as a source of fuel, identify supplier and seams and give sizing of | | | | | | |
| (f) If coal is proposed as a source of fuel, identify supplier and seams and give sizing of the coal as it will be fired: | | | | | | |
| | | | | | | |
| | | | | | | |
| N/A | N/A | | | | | |
| | | | | | | |
| | | | | | | |
| | | | | | | |
| (g) Proposed maximum design heat input: 128.48 × 10 ⁶ BTU/hr. | | | | | | |
| 7. Projected operating schedule: 8400 hr/yr | | | | | | |
| Hours/Day | 2 | 4 | Days/Week | 7 | Weeks/Year | 50 |

| 8. Projected amount of pollutants that would be emitted from this affected source if no control devices were used: | | | | | |
|--|-------------------|-----------|-------|------|------------|
| @ | 271.67 | °F and | | 14.7 | psia |
| a. | NOx | 37.37 | lb/hr | | grains/ACF |
| b. | SO ₂ | 33.63 | lb/hr | | grains/ACF |
| c. | СО | 3.21 | lb/hr | | grains/ACF |
| d. | PM/PM10/PM2.5 | 2.32 | lb/hr | | grains/ACF |
| e. | Hydrocarbons | _ | lb/hr | | grains/ACF |
| f. | VOCs | 0.31 | lb/hr | | grains/ACF |
| g. | Pb | <0.01 | lb/hr | | grains/ACF |
| h. | Specify other(s) | | | | |
| | Total HAPs | 3.43 | lb/hr | | grains/ACF |
| | H2SO4 | 1.87 | lb/hr | | grains/ACF |
| | CO ₂ e | 18,351.66 | lb/hr | | grains/ACF |
| | | | lb/hr | | grains/ACF |

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

(2) Complete the Emission Points Data Sheet.

| | ing, and reporting in order to demonstrate parameters. Please propose testing in order to | | | |
|--|--|--|--|--|
| Not impacted by updates. | Not impacted by updates. | | | |
| | | | | |
| | | | | |
| | | | | |
| | | | | |
| REPORTING | TESTING | | | |
| Not impacted by updates. | Not impacted by updates. | | | |
| | | | | |
| | | | | |
| | | | | |
| | | | | |
| PROPOSED TO BE MONITORED IN ORDER TO DEM | HE PROCESS PARAMETERS AND RANGES THAT ARE IONSTRATE COMPLIANCE WITH THE OPERATION OF | | | |
| THIS PROCESS EQUIPMENT OPERATION/AIR POLLU RECORDKEEPING. PLEASE DESCRIBE THE PI | JTION CONTROL DEVICE. ROPOSED RECORDKEEPING THAT WILL ACCOMPANY | | | |
| THE MONITORING. REPORTING. PLEASE DESCRIBE THE PRO | OPOSED FREQUENCY OF REPORTING OF THE | | | |
| RECORDKEEPING. | | | | |
| EQUIPMENT/AIR POLLUTION CONTROL DEVICE. | SED EMISSIONS TESTING FOR THIS PROCESS | | | |
| 10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty | | | | |
| NA | | | | |
| | | | | |
| | | | | |
| | | | | |
| | | | | |

Attachment L Emission Unit Data Sheet (INDIRECT HEAT EXCHANGER)

Emission Unit ID No. must match List Form): CO

Control Device ID No. (must match List Form): CO-AB, HE01

Equipment Information

| 1. | Manufacture r: Bromkamp | 2. Model No. +CO=A1, +CO=A11/12/13 Serial No. |
|------------------|---|--|
| 3. | Number of units: | 4. Use: Direct-fired unit - Provide heat for the curing process. |
| 5. | Rated Boiler Horsepower. NA hp | 6. Boiler Serial No.: NA |
| 7. | Date constructed: 2021 | 8. Date of last modification and explain: NA |
| 9. | Maximum design heat input per unit: | 10. Peak heat input per unit: |
| | 9.86 ×10 ⁶ BTU/hr | 128.48 ×10 ⁶ BTU/hr |
| 11. | Steam produced at maximum design output: | 12. Projected Operating Schedule: |
| | NA LB/hr | Hours/Day 24 |
| | | Days/Week 7 |
| | psig | Weeks/Year 50 |
| 13. | Type of firing equipment to be used: | 14. Proposed type of burners and orientation: |
| | | Vertical |
| | Spreader stoker | Front Wall |
| | | |
| | Natural Gas Burner | Tangential |
| | Others, specify | Others, specify |
| 15. | Type of draft: Forced Induced | 16. Percent of ash retained in furnace: % |
| 17. | Will flyash be reinjected? Yes No | 18. Percent of carbon in flyash: % |
| | Stack or | Vent Data |
| 1 9 . | Inside diameter or dimensions: 3.28 ft. | 20. Gas exit temperature: 271 °F |
| 21. | Height: 212.70 ft. | 22. Stack serves: |
| 23. | Gas flow rate: 13,636 ft ³ /min | Other equipment also (submit type and rating of all other equipment exhausted through this |
| 24. | Estimated percent of moisture: % | stack or vent) HE01, CO-AB, CO, SPN, and CS |

| 25. | Туре | Fuel Oil No. | Natural Gas | Gas (other, specify) | Coal, Type: | Other: |
|-----|---|--|--|--------------------------------------|-------------------------------------|--------|
| | Quantity (at Design Output) | gph@60°F | 9,610 ft ³ /hr | ft ³ /hr | ТРН | |
| | Annually | ×10 ³ gal | 0.0096 ×10 ⁶ ft ³ /hr | ×10 ⁶ ft ³ /hr | tons | |
| | Sulfur | Maximum: wt. % Average: wt. % | gr/100 ft ³ | gr/100 ft ³ | Maximum: wt. % | |
| | Ash (%) | | | | Maximum | |
| | BTU Content | BTU/Gal. Lbs/Gal.@60°F | 1026 BTU/ft ³ | BTU/ft ³ | BTU/lb | |
| | Source | | | | | |
| | Supplier | | | | | |
| | Halogens (Yes/No) | | | | | |
| | List and Identify Metals | | | | | |
| 26. | Gas burner mode | | omatic hi-low | 27. Gas burner mar | nufacture: TBD | |
| | Automatic full modulation 🗍 Automatic on-off | | | 28. Oil burner manu | | |
| 29. | If fuel oil is used, | how is it atomized? | | sed Air 🗍 Rotary Cu | | |
| 30. | 30. Fuel oil preheated: Yes No | | | 31. If yes, indicate | temperature: | °F |
| | 32. Specify the calculated theoretical air requirements for combustion of the fuel or mixture of fuels described above actual cubic feet (ACF) per unit of fuel: @ °F, PSIA, % moisture | | | | | |
| 33. | 33. Emission rate at rated capacity: Ib/hr | | | | | |
| 34. | 34. Percent excess air actually required for combustion of the fuel described: % | | | | | |
| | | | Coal Chara | acteristics | | |
| | Seams: NA | | | | | |
| 36. | Proximate analysis | % of | Fixed Carbon: Moisture: Ash: | | % of Sulfur: % of Volatile Matte | |

Fuel Requirements

Emissions Stream

| Pollutant | Pounds per Hour Ib/hr | grain/ACF | @ °F | PSIA |
|--|-----------------------------|----------------------|-------------|------|
| со | I | | l | |
| Hydrocarbons | _ | | | |
| NOx | _ | | | |
| Pb | _ | | Cas Dalaw | |
| PM10 | | NO CONTROLS | - See Below | |
| SO ₂ | _ | | | |
| VOCs | | | | |
| Other (specify) | | | | |
| | | | | |
| | | | | |
| | | | | |
| 38. What quantities of poll Aggregate limit with HE0 [,] | utants will be emitted from | the boiler after cor | ntrols? | |
| Pollutant | Pounds per Hour Ib/hr | grain/ACF | @ °F | PSIA |
| со | | | | |
| Hydrocarbons | | | | |
| NOx | | | | |
| Pb | | | | |
| PM _{Fil} | | | | |
| PM 10 | | | | |
| PM _{2.5} | | | | |
| SO2 | | | | |
| VOCs | | | | |
| Other (specify) | | | | |
| | | | | |
| | | | | |
| 39. How will waste material from the process and control equipment be disposed of? Wastes are not expected from a natural gas-fired unit. | | | | |
| 40. Have you completed an Air Pollution Control Device Sheet(s) for the control(s) used on this Emission Unit. | | | | |
| | air pollution rates on the | | | |

| 42. Proposed Monitoring, Recordkeeping, Reporting, and Testing |
|---|
| Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the |
| proposed operating parameters. Please propose testing in order to demonstrate compliance with the |
| proposed emissions limits. |
| |
| MONITORING PLAN: Please list (1) describe the process parameters and how they were chosen (2) the |
| ranges and how they were established for monitoring to demonstrate compliance with the operation of this |
| process equipment operation or air pollution control device. |
| process equipment operation of an politition control device. |
| |
| |
| Not impacted by updates. |
| |
| |
| |
| |
| |
| |
| TESTING PLAN: Please describe any proposed emissions testing for this process equipment or air pollution |
| control device. |
| |
| |
| Nuclear and the second data |
| Not impacted by updates. |
| |
| |
| |
| |
| |
| |
| RECORDKEEPING: Please describe the proposed recordkeeping that will accompany the monitoring. |
| RECORDALETING. Flease describe the proposed record cepting that will accompany the monitoling. |
| |
| |
| Not impacted by updates. |
| Not impacted by apartes. |
| |
| |
| |
| |
| |
| |
| |
| REPORTING: Please describe the proposed frequency of reporting of the recordkeeping. |
| |
| |
| |
| Not impacted by updates. |
| |
| |
| |
| |
| |
| |
| |
| |
| 43. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty. |
| NA |
| |
| |
| |
| |
| |
| |
| |
| |
| |
| |
| |
| |

Attachment L EMISSIONS UNIT DATA SHEET GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form): CS

| 1. Name or type and model of proposed affected source: |
|--|
| |
| Cooling Section |
| Cooling Section |
| |
| On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants. |
| 3. Name(s) and maximum amount of proposed process material(s) charged per hour: |
| |
| |
| |
| Mineral Wool – 55,116 lb/hr |
| |
| |
| |
| 4. Name(s) and maximum amount of proposed material(s) produced per hour: |
| |
| |
| Mineral Wool – 55,116 lb/hr |
| |
| |
| |
| 5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants: |
| |
| |
| |
| NA |
| |
| |
| |

* The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

| 6. | . Combustion Data (if applicable): NA | | | | |
|----|---|----------------------|----------------|-------------------|--------------------|
| | (a) Type and amount in appropriate units of fuel(s) to be burned: | | | | |
| | | | | | |
| | | | | | |
| | | | | | |
| | (b) Chemical analysis of pr and ash: | oposed fuel(s), ex | cluding coal, | including maxim | ium percent sulfur |
| | | | | | |
| | | | | | |
| | | | | | |
| | | | | | |
| | | | | | |
| | | | | | |
| | (c) Theoretical combustion | n air requirement (A | CF/unit of fu | ıel): | |
| | @ | | °F and | | psia. |
| | (d) Percent excess air: | | | | |
| | | | f ining | | |
| | (e) Type and BTU/hr of bu | rners and all other | nring equipri | tent planned to t | be used: |
| | | | | | |
| | | | | | |
| | | | | | |
| | | | | | |
| | | | | | |
| ⊢ | (f) If coal is proposed as a | source of fuel ide | ntify supplier | and seams and | give sizing of the |
| | coal as it will be fired: | | and y ouppilo | | give sizing of the |
| | | | | | |
| | | | | | |
| | | | | | |
| | | | | | |
| | | | | | |
| | | | | | |
| Γ | (g) Proposed maximum design heat input: × 10 ⁶ BTU/hr. | | | | |
| 7. | 7. Projected operating schedule: 8400 hr/yr | | | | |
| Ho | ours/Day 24 | Days/Week | 7 | Weeks/Year | 50 |

| 8. Projected amount of pollutants that would be emitted from this affected source if no control devices were used: Aggregate limit with HE01 | | | |
|--|------------------|--------|------------------|
| @ | 2 104 | °F and | 14.7 psia |
| a. | NOx | lb/hr | grains/ACF |
| b. | SO ₂ | lb/hr | grains/ACF |
| c. | СО | lb/hr | grains/ACF |
| d. | PM/PM10/PM2.5 | lb/hr | grains/ACF |
| e. | Hydrocarbons | lb/hr | grains/ACF |
| f. | VOCs (Non-HAP) | lb/hr | grains/ACF |
| g. | Pb | lb/hr | grains/ACF |
| h. | Specify other(s) | | |
| | | lb/hr | grains/ACF |

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

(2) Complete the Emission Points Data Sheet.

| 9. Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits. | | | | |
|---|---|--|--|--|
| MONITORING | RECORDKEEPING | | | |
| Not impacted by updates. | Not impacted by updates. | | | |
| | | | | |
| | | | | |
| | | | | |
| REPORTING | TESTING | | | |
| Not impacted by updates. | Not impacted by updates. | | | |
| | | | | |
| | | | | |
| | | | | |
| | THE PROCESS PARAMETERS AND RANGES THAT ARE DNSTRATE COMPLIANCE WITH THE OPERATION OF THIS CONTROL DEVICE. | | | |
| RECORDKEEPING. PLEASE DESCRIBE THE PROMONITORING. | OPOSED RECORDKEEPING THAT WILL ACCOMPANY THE | | | |
| REPORTING. PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORD KEEPING. | | | | |
| TESTING. PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR POLLUTION CONTROL DEVICE. | | | | |
| 10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty | | | | |
| NA | | | | |
| | | | | |
| | | | | |
| | | | | |

Attachment L Emission Unit Data Sheet (INDIRECT HEAT EXCHANGER)

Emission Unit ID No. must match List Form): CM03

Control Device ID No. (must match List Form):

Equipment Information

| 1. Manufacturer: Carnus | | 2. Model No. DFNH-5004-NSI | | | | | | | |
|--|-------------------------|--|-------------------------|--|--|--|--|--|--|
| | | Serial No. | | | | | | | |
| 3. Number of units: 1 | | 4. Use | | | | | | | |
| | | Provide building heat. | | | | | | | |
| 5. Rated Boiler Horsepower. hp | | 6. Boiler Serial No.: | | | | | | | |
| 7. Date constructed: 2021 | | 8. Date of last modification and explain: NA | | | | | | | |
| 9. Maximum design heat input per unit: | | 10. Peak heat input per unit: | | | | | | | |
| 4.99 | ×10 ⁶ BTU/hr | 4.99 | ×10 ⁶ BTU/hr | | | | | | |
| 11. Steam produced at maximum design output: | | 12. Projected Operating Schedule: | | | | | | | |
| TBD | LB/hr | Hours/Day | 24 | | | | | | |
| | LD/III | Days/Week | 7 | | | | | | |
| | psig | Weeks/Year | 52 | | | | | | |
| 13. Type of firing equipment to be use | d: | 14. Proposed type of burners a | and orientation: | | | | | | |
| | | ☐ Vertical | | | | | | | |
| Spreader stoker | | Front Wall | | | | | | | |
| ☐ Oil burners ⊠ Natural Gas Burner | | Opposed Tangential | | | | | | | |
| Others, specify | | Others, specify | | | | | | | |
| | | | | | | | | | |
| 15. Type of draft: Forced | Induced | 16. Percent of ash retained in f | fumace: % | | | | | | |
| 17. Will flyash be reinjected? | 3 🗵 No | 18. Percent of carbon in flyash | .: % | | | | | | |
| Stack or Vent Data | | | | | | | | | |
| 19. Inside diameter or dimensions: | 1.00 ft. | 20. Gas exit temperature: | 232.07 °F | | | | | | |
| 21. Height: | 75.62 ft. | 22. Stack serves: | | | | | | | |
| | | This equipment only | | | | | | | |
| 23. Gas flow rate: 2508.25 | ft ³ /min | Other equipment also (submit type and rating of all other equipment exhausted through this | | | | | | | |
| 24. Estimated percent of moisture: | % | stack or vent) | | | | | | | |

| Fuel Requirements | | | | | | | | | | | |
|---|--|---|--|--|-------------------------------------|-------------------|--------|--|--|--|--|
| 25. | Туре | Fuel Oil No. | Natural Gas | G | as (other, specify) | Coal, Type: | Other: | | | | |
| | Quantity (at Desig n Output) | gph@60°F | 4864 ft ³ /hr | | ft ³ /hr | TPH | | | | | |
| | Annually | ×10 ³ gal | 42.60 ×10 ⁶ ft ³ /yr | | 10 ⁶ ft ³ /hr | tons | | | | | |
| | Sulfur | Maximum: wt. % Average: wt. % | gr/100 ft ³ | 9 | gr/100 ft ³ | Maximum: wt. % | | | | | |
| | Ash (%) | | | | | Maximum | | | | | |
| | BTU Content | BTU/Gal. Lbs/Gal.@60°F | 1026 BTU/ft ³ | | BTU/ft ³ | BTU/Ib | | | | | |
| | Source | | | | | | | | | | |
| | Supplier | | | | | | | | | | |
| | Halogens (Yes/No) | | | | | | | | | | |
| | List and Identify Metals | | | | | | | | | | |
| 26. | Gas burner mode ☐ Manual | | omatic hi-low | 27. Gas burner manufacture: TBD | | | | | | | |
| | Automatic full r | Automatic full modulation Automatic on-off 28. Oil purner manufacture: NA | | | | | | | | | |
| 29. If fuel oil is used, how is it atomized? Oil Pressure Steam Pressure Compressed Air Rotary Cup Other, specify | | | | | | | | | | | |
| | Fuel oil preheated | uel oil preheated: Yes No 31. If yes, indicate temperature: | | | | | | | | | |
| 32. | 32. Specify the calculated theoretical air requirements for combustion of the fuel or mixture of fuels described above actual cubic feet (ACF) per unit of fuel: | | | | | | | | | | |
| | @ °F, PSIA, % moisture | | | | | | | | | | |
| <u> </u> | 33. Emission rate at rated capacity: Ib/hr | | | | | | | | | | |
| 34. Percent excess air actually required for combustion of the fuel described: % Coal Characteristics | | | | | | | | | | | |
| 35. | 35. Seams: NA | | | | | | | | | | |
| | | | | | | | | | | | |
| 36. | 6. Proximate analysis (dry basis): % of Fixed Carbon: % of Sulfur: % of Moisture: % of Volatile Matter: % of Ash: % | | | | | | | | | | |

Emissions Stream

| 37. What quantities of pollu | tants will be emitted fron | n the boiler before c | ontrols? | |
|------------------------------|----------------------------|------------------------|-----------------------|-------------------|
| Pollutant | Pounds per Hour Ib/hr | grain/ACF | @ °F | PSIA |
| со | | | | |
| Hydrocarbons | | | | |
| NOx | | | | |
| Pb | | | | |
| PM10 | | | Ose Delaus | |
| SO2 | | NO CONTROIS | - See Below | |
| VOCs | | | | |
| Other (specify) | | | | |
| | | | | |
| | | | | |
| | | | | |
| 38. What quantities of pollu | tants will be emitted from | n the boiler after con | trols? | |
| Pollutant | Pounds per Hour Ib/hr | grain/ACF | @ °F | PSIA |
| со | 0.41 | | | |
| Hydrocarbons | | | | |
| NOx | 0.18 | | | |
| Pb | <0.01 | | | |
| PM/PM10/PM2.5 | 0.04 | | | |
| SO ₂ | <0.01 | | | |
| VOCs | 0.03 | | | |
| Other (specify) | | | | |
| Total HAPs | 0.01 | | | |
| CO2e | 584.32 | | | |
| | | | | |
| 39. How will waste material | from the process and co | ntrol equipment be o | lisposed of? | |
| Wastes are not expected | ed from a natural gas-fi | red boiler. | | |
| | | | | |
| 40. Have you completed an | Air Pollution Control Dev | ice Sheet(s) for the | control(s) used on th | is Emission Unit. |
| 41. Have you included the a | air pollution rates on the | Emissions Points D | ata Summary Sheet | ? Yes |
| | | | | |

| 42. Proposed Monitoring, Recordkeeping, Reporting, and Testing |
|---|
| Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the |
| proposed operating parameters. Please propose testing in order to demonstrate compliance with the |
| proposed emissions limits. |
| MONITORING PLAN: Please list (1) describe the process parameters and how they were chosen (2) the |
| |
| ranges and how they were established for monitoring to demonstrate compliance with the operation of this |
| process equipment operation or air pollution control device. |
| |
| |
| Not impacted by updates. |
| |
| |
| |
| |
| TESTING PLAN: Please describe any proposed emissions testing for this process equipment or air pollution |
| control device. |
| |
| |
| |
| Not impacted by updates. |
| |
| |
| |
| |
| |
| RECORDKEEPING: Please describe the proposed recordkeeping that will accompany the monitoring. |
| RECORDATE INC. I loude december in proposed record coping that the decempany the memory |
| |
| Not imported by undefer |
| Not impacted by updates. |
| |
| |
| |
| |
| |
| |
| REPORTING: Please describe the proposed frequency of reporting of the recordkeeping. |
| |
| |
| Not impacted by updates. |
| Not impacted by updates. |
| |
| |
| |
| |
| |
| |
| 43. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty. |
| |
| |
| |
| |
| |
| |
| |

Attachment L Emission Unit Data Sheet (INDIRECT HEAT EXCHANGER)

Emission Unit ID No. must match List Form): CM04

Control Device ID No. (must match List Form):

Equipment Information

| 1. | Manufacturer: CAMUS | | | lodel No. Serial No. | DFNH-5004 | -NSI | | |
|-----|---|-------------------------|--------|---|--|------------|-------------------------|---|
| 3. | Number of units: 1 | | | Jse i de build i | ng heat. | | | |
| 5. | Rated Boiler Horsepower. | hp | 6. B | loiler Seria | I No.: | | | |
| 7. | Date constructed: 2021 | | | ate of las IA | t modification | and explai | in: | |
| 9. | Maximum design heat input per unit | | 10. F | 'eak heat i | nput per unit: | | | |
| | 4.99 | ×10 ⁶ BTU/hr | | 4.99 | | | ×10 ⁶ BTU/hr | • |
| 11. | Steam produced at maximum desig | n output: | 12. P | rojected C | Derating Sche | dule: | | |
| | TBD | LB/hr | | | Hours/Day | 24 | | |
| | | 20/11 | | | Days/Week | 7 | | |
| | | psig | | | Weeks/Year | 52 | | |
| 13. | Type of firing equipment to be used Pulverized coal Spreader stoker Oil burners Natural Gas Burner Others, specify | 1: | 14. P | Vert Vert From Opp Tang | ype of burners iical nt Wall bosed gential ers, specify | and orien | tation: | |
| 15. | Type of draft: 🗌 Forced 🛛 | Induced | 16. P | ercent of | ash retained ir | n furnace: | | % |
| 17. | Will flyash be reinjected? | 🛛 No | 18. F | Percent of | carbon in flyas | sh: | | % |
| | | Stack or | Vent C | Data | | | | |
| 19. | Inside diameter or dimensions: | 1.00 ft. | 20. G | as exit ter | nperature: | 232.07 | , | ۴ |
| 21. | Height: 75.62 ft. | | | Stack serve | es: uipment only | | | |
| 23. | Gas flow rate: 2,508.25 | ft³/min | | Othere all oth | equipment also er equipment | | | |
| 24. | Estimated percent of moisture: | % | | stack o | or vent) | | | |

| | | | • | | | |
|-----|-----------------------------------|---|---|--------------------------------------|--------------------------------------|--------------------|
| 25. | Туре | Fuel Oil No. | Natural Gas | Gas (other, specify) | Coal, Type: | Other: |
| | Quantity (at Design Output) | gph@60°F | 4864 ft ³ /hr | ft ³ /hr | ТРН | |
| | Annually | ×10 ³ gal | 42.60 ×10 ⁶ ft ³ /yr | ×10 ⁶ ft ³ /hr | tons | |
| | Sulfur | Maximum: wt. % Average: wt. % | gr/100 ft ³ | gr/100 ft ³ | Maximum: wt. % | |
| | Ash (%) | | | | Maximum | |
| | BTU Content | BTU/Gal. Lbs/Gal.@60°F | 1026 BTU/ft ³ | BTU/ft ³ | BTU/lb | |
| | Source | | | | | |
| | Supplier | | | | | |
| | Halogens (Yes/No) | | | | | |
| | List and Identify Metals | | | | | |
| 26. | Gas burner mode Manual | | omatic hi-low | 27. Gas burner mar | nufacture: TBD | |
| | Automatic full r | | omatic on-off | 28. Oil burner manu | facture: NA | |
| 29. | lf fuel oil is used, | how is it atomized? | Oil Pressu Compress Other, specific | sed Air 🗍 Rotary Cu | | |
| 30. | Fuel oil preheated: | : 🗌 Yes 🛛 [|] No | 31. If yes, indicate | temperature: | °F |
| 32. | above actual cubic | ated theoretical ai c feet (ACF) per un °F, | | or combustion of th % m | e fuel or mixture c oisture | of fuels described |
| 33. | @ Emission rate at ra | | lb/hr | , 70 III | UISTUIE | |
| | | | or combustion o | f the fuel described: | % | |
| | | | Coal Chara | octeristics | | |
| 35. | Seams: NA | | | | | |
| 36. | Proximate analysis | % of | f Fixed Carbon: f Moisture: f Ash: | | % of Sulfur: % of Volatile Matter | r. |

Fuel Requirements

Emissions Stream

| 37. What quantities of pollu | itants will be emitted from | the boiler before co | ontrols? | |
|------------------------------|-----------------------------|-----------------------|-----------------------|-------------------|
| Pollutant | Pounds per Hour Ib/hr | grain/ACF | ۹° ۴ | PSIA |
| СО | | | | |
| Hydrocarbons | | | | |
| NOx | | | | |
| Pb | | | | |
| PM10 | | | Cas Dalaw | |
| SO2 | | No Controls | - See Below | |
| VOCs | | | | |
| Other (specify) | | | | |
| | | | | |
| | | | | |
| | | | | |
| 38. What quantities of pollu | itants will be emitted from | the boiler after con | trols? | |
| Pollutant | Pounds per Hour Ib/hr | grain/ACF | @ °F | PSIA |
| со | 0.41 | | | |
| Hydrocarbons | | | | |
| NOx | 0.18 | | | |
| Pb | <0.01 | | | |
| PM/PM10/PM2.5 | 0.04 | | | |
| SO2 | <0.01 | | | |
| VOCs | 0.03 | | | |
| Other (specify) | | | | |
| CO2e | 584.32 | | | |
| Total HAPs | 0.01 | | | |
| | | | | |
| 39. How will waste material | from the process and cor | trol equipment be d | lisposed of? | |
| Wastes are not expect | ed from a natural gas-fire | ed boiler. | | |
| | | | | |
| 40. Have you completed ar | Air Pollution Control Devi | ce Sheet(s) for the c | control(s) used on th | is Emission Unit. |
| 41. Have you included the | air pollution rates on the | Emissions Points D | ata Summary Sheet | ? Yes |
| | | | | |

| 42. Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits. |
|--|
| MONITORING PLAN: Please list (1) describe the process parameters and how they were chosen (2) the ranges and how they were established for monitoring to demonstrate compliance with the operation of this process equipment operation or air pollution control device. |
| Not impacted by updates. |
| TESTING PLAN: Please describe any proposed emissions testing for this process equipment or air pollution control device. |
| Not impacted by updates. |
| RECORDKEEPING: Please describe the proposed recordkeeping that will accompany the monitoring. |
| Not impacted by updates. |
| |
| REPORTING: Please describe the proposed frequency of reporting of the recordkeeping. |
| Not impacted by updates. |
| |
| 43. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty. |
| NA |
| |
| |

Attachment L EMISSIONS UNIT DATA SHEET GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form): EFP1

| 1. Name or type and model of proposed affected source: |
|--|
| Emergency Fire Pump Engine – 316 hp |
| |
| On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants. |
| 3. Name(s) and maximum amount of proposed process material(s) charged per hour: |
| |
| |
| |
| |
| |
| 4. Name(s) and maximum amount of proposed material(s) produced per hour: |
| |
| |
| |
| |
| |
| 5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants: |
| |
| |
| NA |
| |
| |

* The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

| 6. Combustion Data (if app | licable): | | |
|---|---------------------------------------|--------------|----------------------------------|
| (a) Type and amount in | appropriate units of fuel(| s) to be bu | Irned: |
| Diesel | | | |
| (b) Chemical analysis of and ash: | ⁻ proposed fuel(s), exclud | ing coal, ir | ncluding maximum percent sulfur |
| (c) Theoretical combust | ion air requirement (ACF | unit of fue | l): |
| @ | | °F and | psia. |
| (d) Percent excess air: | | | |
| | burners and all other firin | | |
| (f) If coal is proposed a coal as it will be fire | | / supplier a | and seams and give sizing of the |
| (g) Proposed maximum | | 2.21 | × 10º BTU/hr. |
| 7. Projected operating sch | edule: 500 hours per ye | ar | |
| Hours/Day | Days/Week | | Weeks/Year |

| 8. | Projected amount of polluta devices were used: | ants that would be e | emitted fror | n this affected source if no control |
|----|--|----------------------|--------------|--------------------------------------|
| @ | 2 | °F an | d | psia |
| a. | NOx | 1.80 | lb/hr | grains/ACF |
| b. | SO ₂ | <0.01 | lb/hr | grains/ACF |
| c. | СО | 0.40 | lb/hr | grains/ACF |
| d. | PM/PM10/PM2.5 | 0.08 | lb/hr | grains/ACF |
| e. | Hydrocarbons | | lb/hr | grains/ACF |
| f. | VOCs | 0.04 | lb/hr | grains/ACF |
| g. | Pb | | lb/hr | grains/ACF |
| h. | Specify other(s) | | | |
| | CO2e | 362 | lb/hr | grains/ACF |
| | Total HAPs | <0.01 | lb/hr | grains/ACF |
| | | | lb/hr | grains/ACF |

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

(2) Complete the Emission Points Data Sheet.

| with the proposed operating parameters. compliance with the proposed emissions lin | and reporting in order to demonstrate compliance Please propose testing in order to demonstrate |
|---|--|
| MONITORING Not impacted by updates. | RECORDKEEPING Not impacted by updates. |
| | |
| | |
| | |
| REPORTING | TESTING |
| Not impacted by updates. | Not impacted by updates. |
| | |
| | |
| | |
| | |
| | HE PROCESS PARAMETERS AND RANGES THAT ARE INSTRATE COMPLIANCE WITH THE OPERATION OF THIS I CONTROL DEVICE. |
| RECORDKEEPING. PLEASE DESCRIBE THE PROF MONITORING. | POSED RECORDKEEPING THAT WILL ACCOMPANY THE |
| REPORTING. PLEASE DESCRIBE THE PRORECORDING. | OPOSED FREQUENCY OF REPORTING OF THE |
| TESTING. PLEASE DESCRIBE ANY PROPOSED EM POLLUTION CONTROL DEVICE. | IISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR |
| 10. Describe all operating ranges and mainter maintain warranty | nance procedures required by Manufacturer to |
| Unit will comply with NSPS IIII Requirement | 'S. |
| | |
| | |
| | |
| | |

Rating Specific Emissions Data - John Deere Power Systems



Ruting Data

| Rating | 6068HI | FC48B | |
|----------------------|----------------------|----------------------|--|
| Certified Power(kW) | 2 | 16 | |
| Rated Spead | 24 | 2400 | |
| Vakicle Model Number | OEM (Clarke Emery | Fire Pump- gency) | |
| Unita | g/kW-hr | g/hp-hz | |
| NOL | 3.43 | 2.56 | |
| HC | 0.09 | 0.07 | |
| NOX + LIC | N/A | N/A | |
| Pm | 0.11 | 80.0 | |
| CO | 0.6 | 0.6 | |

Certificate Data

| Engine Model Year | 2019 | 9 |
|------------------------|------------------|---|
| EPA Faothy Name | KJDXL13.5103 | |
| EPA JD Name | 650HAA | |
| EPA Certificate Number | KJDXL13.5103-007 | |
| CARB Executive Order | | |
| Parent of Family | 6135HF485A | |
| Cinita | g/kW-hr | |
| NOT | 3.31 | |
| HC | 0.11 | |
| NOs + BC | N/A | |
| Pm | 0.10 | |
| CO | 9.6 | |

* The emission deta listed is measured from a laboratory test engine according to the test procedures of 40 CFR 89 or 40 CFR 1039, as applicable. The test engine is intended to represent naminal production bankware, and we de not gammate that every production engine will have identical test results. The family parent data represents multiple mitings and this data may have been collected at a different engine speed and load. Emission results may vary due to engine menufacturing tolerances, angine operating conditions, faels used, or other conditions beyond our control.

This information is property of Dears & Company. It is provided solely for the purpose of obtaining cartification or pennits of Dears powered equipment. Unantherized distribution of this information is prohibited.

Emissions Results by Rating run on Feb-18-2019

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <u>www.epa.gov/tnn/tanks.html</u>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<u>http://www.epa.gov/tnn/chief/</u>).

| 1. Bulk Score Area Name | Tank Name Thermal Oil Tank - IMF |
|--|--|
| Tank Equipment Identification No. (as assigned or Equipment List Form) TK-TO3 | |
| 5. Date of Commencement of Construction (for existin | g tanks) 2021 |
| 6. Type of change New Construction | New Stored Material 🛛 🥂 Other Tank Modification |
| 7. Description of Tank Modification (if applicable) | |
| Increased tank capacity from 2642 gallons to | o 5283 gallons. |
| 7A. Does the tank have more than one mode of operati (e.g. Is there more than one product stored in the tag | nk?) |
| 7B. If YES, explain and identify which mode is cover completed for each mode). N/A | ed by this application (Note: A separate form must be |
| 7C. Provide any limitations on source operation affectin variation, etc.): N/A | g emissions, any work practice standards (e.g. production |
| I. I. TANK INFORMATION (required) - See Attached Em | ission Master Report for the following information |
| Design Capacity (specify barrels or gallons). Us height. | e the internal cross-sectional area multiplied by internal |
| Sk. Tank Imme Diameter III | E Tank here Height for Longfill Im |
| 10A. Maximum Liquid Height (ft) | 10B. Average Liquid Height (ft) |
| 11A. Maximum Vapor Space Height (ft) | 11B. Average Vapor Space Height (ft) |
| 12. Nominal barrels or gallons This liquid levels and overflow valve heights. | is also known as a second considers design |

| 13A. Maximum annual throughput (gal/yr) 698 gal/yr | 13B. Maximum daily throughput (gal/day) |
|--|---|
| 14. Number of Tumovers per year (annual net throughput | t/maximum tank liquid volume) |
| 15. Maximum tank fill rate (gal/min) | |
| 16. Tank fill method Submerged | Splash Bottom Loading |
| 17. Complete 17A and 17B for Variable Vapor Space Ta | nk Systems Does Not Apply |
| 17A. Volume Expansion Capacity of System (gal) | 17B. Number of transfers into system per year |
| 18. Type of tank (check all that apply): Fixed Roofverticalhorizontalother (describe) External Floating Roofpontoon roof Domed External (or Covered) Floating Roof Internal Floating Roofvertical column su Variable Vapor Spacelifter roof Pressurizedsphericalcylindrical Underground Other (describe) | upportself-supporting diaphragm |

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <u>www.epa.gov/tnn/tanks.html</u>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (http://www.epa.gov/tnn/chief/).

| 1. | Bulk Storage Area Name | 2. | Tank Name Thermal Oil Expansion Tank - IMF |
|-----|---|-------|---|
| 3. | Tank Equipment Identification No. (as assigned on Equipment List Form) TK-TO4 | 4. | Emission Point Identification No. (as assigned on Equipment List Form) TK-TO4 |
| 5. | Date of Commencement of Construction (for existing | tanl | ıks) 2021 |
| 6. | Type of change 🗌 New Construction 🗌 N | lew | Stored Material 🛛 🗙 Other Tank Modification |
| 7. | Description of Tank Modification (if applicable) Increased tank capacity from 1321 gallons to | 19 |)28 gallons. |
| 7A. | Does the tank have more than one mode of operatio (e.g. Is there more than one product stored in the tan | | 🗌 Yes 🖾 No |
| 7B. | If YES, explain and identify which mode is covere completed for each mode). | d b | by this application (Note: A separate form must be |
| 7C. | C. Provide any limitations on source operation affecting emissions, any work practice standards (e.g. production variation, etc.): NA | | |
| П. | TANK INFORMATION (required) - See Attached Em | iss | ion Master Report for the following information |
| 8. | Design Capacity (specify barrels or gallons). Use height. | the | internal cross-sectional area multiplied by internal |
| 9A. | Tank Internal Diameter (ft) | 9B | 3. Tank Internal Height (or Length) (ft) |
| 10/ | A. Maximum Liquid Height (ft) | 10 | B. Average Liquid Height (ft) |
| 11A | A. Maximum Vapor Space Height (ft) | 11 | B. Average Vapor Space Height (ft) |
| 12. | Nominal Capacity (specify barrels or gallons). This is liquid levels and overflow valve heights. | s als | so known as "working volume" and considers design |

| 13A. Maximum annual throughput (gal/yr) 698 gal/yr | 13B. Maximum daily throughput (gal/day) |
|--|---|
| 14. Number of Tumovers per year (annual net throughput | t/maximum tank liquid volume) |
| 15. Maximum tank fill rate (gal/min) | |
| 16. Tank fill method Submerged | Splash Bottom Loading |
| 17. Complete 17A and 17B for Variable Vapor Space Ta | nk Systems Does Not Apply |
| 17A. Volume Expansion Capacity of System (gal) | 17B. Number of transfers into system per year |
| 18. Type of tank (check all that apply): Fixed Roofverticalhorizontalother (describe) External Floating Roofpontoon roof Domed External (or Covered) Floating Roof Internal Floating Roofvertical column su Variable Vapor Spacelifter roof Pressurizedsphericalcylindrical Underground Other (describe) | upportself-supporting diaphragm |

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <u>www.epa.gov/tnn/tanks.html</u>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (http://www.epa.gov/tnn/chief/).

| 1. | Bulk Storage Area Name | 2. Tank Name Additive Storage Tank | |
|-----|--|---|--|
| 3. | Tank Equipment Identification No. (as assigned on Equipment List Form) TK-AD | Emission Point Identification No. (as assigned on Equipment List Form) TK-AD | |
| 5. | Date of Commencement of Construction (for existing | tanks) 2021 | |
| 6. | Type of change 🗌 New Construction 🗌 N | lew Stored Material 🛛 🛛 Other Tank Modification | |
| 7. | Description of Tank Modification (if applicable) Updating emission calculations to AP42 met | hodology. | |
| 7A. | Does the tank have more than one mode of operatio (e.g. Is there more than one product stored in the tan | | |
| 7B. | B. If YES, explain and identify which mode is covered by this application (Note: A separate form must be completed for each mode). NA | | |
| 7C. | C. Provide any limitations on source operation affecting emissions, any work practice standards (e.g. production variation, etc.): NA | | |
| П. | TANK INFORMATION (required) - See Attached E | mission Master Report for the following information | |
| 8. | Design Capacity (specify barrels or gallons). Use height. | the internal cross-sectional area multiplied by internal | |
| 9A. | Tank Internal Diameter (ft) | 9B. Tank Internal Height (or Length) (ft) | |
| 10/ | A. Maximum Liquid Height (ft) | 10B. Average Liquid Height (ft) | |
| 11/ | A. Maximum Vapor Space Height (ft) | 11B. Average Vapor Space Height (ft) | |
| 12. | Nominal Capacity (specify barrels or gallons). This is liquid levels and overflow valve heights. | also known as "working volume" and considers design | |

| 13A. Maximum annual throughput (gal/yr) 17,171 gal/yr | 13B. Maximum daily throughput (gal/day) |
|--|---|
| 14. Number of Tumovers per year (annual net throughput | t/maximum tank liquid volume) |
| 15. Maximum tank fill rate (gal/min) | |
| 16. Tank fill method Submerged | Splash Bottom Loading |
| 17. Complete 17A and 17B for Variable Vapor Space Ta | nk Systems Does Not Apply |
| 17A. Volume Expansion Capacity of System (gal) | 17B. Number of transfers into system per year |
| 18. Type of tank (check all that apply): Fixed Roofverticalhorizontalother (describe) External Floating Roofpontoon roof Domed External (or Covered) Floating Roof Internal Floating Roofvertical column su Variable Vapor Spacelifter roof Pressurizedsphericalcylindrical Underground Other (describe) | upportself-supporting diaphragm |

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <u>www.epa.gov/tnn/tanks.html</u>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<u>http://www.epa.gov/tnn/chief/</u>).

| 1. B | Bulk Storage Area Name | 2. Tank Name Binder Storage Containers | |
|---------------|---|---|-------|
| E | Tank Equipment Identification No. (as assigned on Equipment List Form) | Emission Point Identification No. (as assigned Equipment List Form) TK-BS1, TK-BS2, and TK-BS3 | l on |
| 5. D | Date of Commencement of Construction (for existing | tanks) 2021 | |
| 6. T | ype of change 🗌 New Construction 🗌 N | New Stored Material X Other Tank Modification | |
| | Description of Tank Modification (if applicable) Jpdating emission calculations to AP42 met | thodology. | |
| | Does the tank have more than one mode of operation e.g. Is there more than one product stored in the tan | | |
| 7C. F V | NA Provide any limitations on source operation affecting variation, etc.): NA | emissions, any work practice standards (e.g. produc | ction |
| II. T/ | ANK INFORMATION (required) - See Attached E | Emission Master Report for the following info | rma |
| 8. D | | the internal cross-sectional area multiplied by inter | |
| 9A. T | ank Internal Diameter (ft) | 9B. Tank Internal Height (or Length) (ft) | |
| 10A. | Maximum Liquid Height (ft) | 10B. Average Liquid Height (ft) | |
| 11 A . | Maximum Vapor Space Height (ft) | 11B. Average Vapor Space Height (ft) | |
| | | | |

| 13A. Maximum annual throughput (gal/yr) 130,325 gal/yr | 13B. Maximum daily throughput (gal/day) |
|---|---|
| 14. Number of Tumovers per year (annual net throughput | l/ //maximum tank liquid volume) |
| | |
| 15. Maximum tank fill rate (gal/min) | |
| 16. Tank fill method Submerged | Splash Bottom Loading |
| 17. Complete 17A and 17B for Variable Vapor Space Ta | nk Systems Does Not Apply |
| 17A. Volume Expansion Capacity of System (gal) | 17B. Number of transfers into system per year |
| 18. Type of tank (check all that apply): | |
| | flat roof cone roof dome roof |
| other (describe) | |
| External Floating Roof pontoon roof | double deck roof |
| Domed External (or Covered) Floating Roof | |
| Internal Floating Roof vertical column su | pportself-supporting |
| └── Variable Vapor Space lifter roof | diaphragm |
| Pressurized spherical cylindrical | |
| | |
| Other (describe) | |
| | |

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <u>www.epa.gov/tnn/tanks.html</u>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<u>http://www.epa.gov/tnn/chief/</u>).

| 1. | Bulk Storage Area Name | 2. Tank Name Coupling Agent Storage Tank | |
|-----|---|---|--|
| 3. | Tank Equipment Identification No. (as assigned on Equipment List Form) TK-CA | Emission Point Identification No. (as assigned on Equipment List Form) TK-CA | |
| 5. | Date of Commencement of Construction (for existing | tanks) 2021 | |
| 6. | Type of change I New Construction I | lew Stored Material 🛛 🔀 Other Tank Modification | |
| 7. | Description of Tank Modification (if applicable) Updating emission calculations to AP42 methodology. | | |
| 7A. | Does the tank have more than one mode of operatio (e.g. Is there more than one product stored in the tan | | |
| 1 | completed for each mode). NA Provide any limitations on source operation affecting | d by this application (Note: A separate form must be emissions, any work practice standards (e.g. production | |
| | variation, etc.): NA I. TANK INFORMATION (required) - See Attached Emission Master Report for the following information | | |
| 8. | Design Capacity (specify barrels or gallons). Use height. | the internal cross-sectional area multiplied by internal | |
| 9A. | Tank Internal Diameter (ft) | 9B. Tank Internal Height (or Length) (ft) | |
| 10/ | A. Maximum Liquid Height (ft) | 10B. Average Liquid Height (ft) | |
| 11/ | A. Maximum Vapor Space Height (ft) | 11B. Average Vapor Space Height (ft) | |
| 12. | Nominal Capacity (specify barrels or gallons). This is liquid levels and overflow valve heights. | also known as "working volume" and considers design | |

| 13A. Maximum annual throughput (gal/yr) 4,227 gal/yr | 13B. Maximum daily throughput (gal/day) |
|--|---|
| 14. Number of Tumovers per year (annual net throughput | /maximum tank liquid volume) |
| 15. Maximum tank fill rate (gal/min) | |
| 16. Tank fill method Submerged | Splash Bottom Loading |
| 17. Complete 17A and 17B for Variable Vapor Space Ta | nk Systems Does Not Apply |
| 17A. Volume Expansion Capacity of System (gal) | 17B. Number of transfers into system per year |
| 18. Type of tank (check all that apply): Fixed Roofverticalhorizontalother (describe) External Floating Roofpontoon roof Domed External (or Covered) Floating Roof Internal Floating Roofvertical column su Variable Vapor Spacelifter roof Pressurizedsphericalcylindrical Underground Other (describe) | upportself-supporting diaphragm |

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <u>www.epa.gov/tnn/tanks.html</u>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (http://www.epa.gov/tnn/chief/).

| 1. | Bulk Storage Area Name | 2. Tank Name Diesel Fuel Tank | |
|-----|---|---|--|
| 3. | Tank Equipment Identification No. (as assigned on Equipment List Form) TK-DF | Emission Point Identification No. (as assigned on Equipment List Form) TK-DF | |
| 5. | Date of Commencement of Construction (for existing | tanks) 2021 | |
| 6. | Type of change I New Construction I | New Stored Material 🛛 🛛 Other Tank Modification | |
| 7. | Description of Tank Modification (if applicable) Updating emission calculations to AP42 methodology. | | |
| 7A. | Does the tank have more than one mode of operatio (e.g. Is there more than one product stored in the tan | | |
| 1 | B. If YES, explain and identify which mode is covered by this application (Note: A separate form must be completed for each mode). NA | | |
| 7C. | C. Provide any limitations on source operation affecting emissions, any work practice standards (e.g. production variation, etc.): NA | | |
| | Contraction of the second s | mission Master Report for the following information | |
| 8. | Design Capacity (specify barrels or gallons). Use height. | the internal cross-sectional area multiplied by internal | |
| 9A. | Tank Internal Diameter (ft) | 9B. Tank Internal Height (or Length) (ft) | |
| 10/ | A. Maximum Liquid Height (ft) | 10B. Average Liquid Height (ft) | |
| 11/ | A. Maximum Vapor Space Height (ft) | 11B. Average Vapor Space Height (ft) | |
| 12. | Nominal Capacity (specify barrels or gallons). This is liquid levels and overflow valve heights. | s also known as "working volume" and considers design | |

| 13A. Maximum annual throughput (gal/yr) 52,834 gal/yr | 13B. Maximum daily throughput (gal/day) |
|--|---|
| 14. Number of Tumovers per year (annual net throughput | t/maximum tank liquid volume) |
| 15. Maximum tank fill rate (gal/min) | |
| 16. Tank fill method Submerged | Splash Bottom Loading |
| 17. Complete 17A and 17B for Variable Vapor Space Ta | nk Systems Does Not Apply |
| 17A. Volume Expansion Capacity of System (gal) | 17B. Number of transfers into system per year |
| 18. Type of tank (check all that apply): Fixed Roof vertical horizontal other (describe) External Floating Roof pontoon roof Domed External (or Covered) Floating Roof Internal Floating Roof vertical column su Variable Vapor Space lifter roof Pressurized spherical cylindrical Underground Other (describe) | upportself-supporting diaphragm |

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <u>www.epa.gov/tnn/tanks.html</u>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<u>http://www.epa.gov/tnn/chief/</u>).

| 1. | Bulk Storage Area Name | 2. Tank Name De-dust Oil Day Tank | | | | | | | |
|-----|---|--|--|--|--|--|--|--|--|
| 3. | Tank Equipment Identification No. (as assigned on Equipment List Form) TK-DOD | | | | | | | | |
| 5. | Date of Commencement of Construction (for existing | tanks) 2021 | | | | | | | |
| 6. | Type of change New Construction | New Stored Material X Other Tank Modification | | | | | | | |
| 7. | Description of Tank Modification (if applicable) Updating emission calculations to AP42 methodology. | | | | | | | | |
| 7A. | Does the tank have more than one mode of operatio (e.g. Is there more than one product stored in the tan | | | | | | | | |
| 7B. | If YES, explain and identify which mode is covere completed for each mode). | d by this application (Note: A separate form must be | | | | | | | |
| 7C. | Provide any limitations on source operation affecting variation, etc.): NA | emissions, any work practice standards (e.g. production | | | | | | | |
| ١. | TANK INFORMATION (required) - See Attached E | mission Master Report for the following information | | | | | | | |
| 8. | Design Capacity (specify barrels or gallons). Use height. | the internal cross-sectional area multiplied by internal | | | | | | | |
| 9A. | Tank Internal Diameter (ft) | 9B. Tank Internal Height (or Length) (ft) | | | | | | | |
| 10/ | A. Maximum Liquid Height (ft) | 10B. Average Liquid Height (ft) | | | | | | | |
| 11/ | A. Maximum Vapor Space Height (ft) | 11B. Average Vapor Space Height (ft) | | | | | | | |
| 12. | Nominal Capacity (specify barrels or gallons). This is liquid levels and overflow valve heights. | s also known as "working volume" and considers design | | | | | | | |

| 3A. Maximum annual throughput (gal/yr) 13B. Maximum daily throughput (gal/day) 52,834 gal/yr 13B. Maximum daily throughput (gal/day) | | | | | | | | | |
|--|--|--|--|--|--|--|--|--|--|
| 14. Number of Tumovers per year (annual net throughput | 14. Number of Tumovers per year (annual net throughput/maximum tank liquid volume) | | | | | | | | |
| 15. Maximum tank fill rate (gal/min) | | | | | | | | | |
| 16. Tank fill method Submerged | Splash Bottom Loading | | | | | | | | |
| 17. Complete 17A and 17B for Variable Vapor Space Ta | nk Systems Does Not Apply | | | | | | | | |
| 17A. Volume Expansion Capacity of System (gal) | 17B. Number of transfers into system per year | | | | | | | | |
| 18. Type of tank (check all that apply): Fixed Roof vertical horizontal other (describe) Extemal Floating Roof pontoon roof Domed External (or Covered) Floating Roof Internal Floating Roof vertical column su Variable Vapor Space lifter roof Pressurized spherical cylind rical Underground Other (describe) | ipportself-supporting diaphragm | | | | | | | | |

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <u>www.epa.gov/tnn/tanks.html</u>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (http://www.epa.gov/tnn/chief/).

| 1. | Bulk Storage Area Name | 2. Tank Name Resin Storage Tanks | | | | | | |
|------|--|--|--|--|--|--|--|--|
| 3. | Tank Equipment Identification No. (as assigned on Equipment List Form) TK-RS1-TK-RS6 | | | | | | | |
| 5. | Date of Commencement of Construction (for existing tanks) 2021 | | | | | | | |
| 6. | Type of change I New Construction IN | New Stored Material 🛛 Other Tank Modification | | | | | | |
| 7. | Description of Tank Modification (if applicable) Updating tank sizing. | | | | | | | |
| 7A. | Does the tank have more than one mode of operation (e.g. Is there more than one product stored in the tan | | | | | | | |
| 7B. | If YES, explain and identify which mode is covere completed for each mode). | d by this application (Note: A separate form must be | | | | | | |
| 7C. | Provide any limitations on source operation affecting variation, etc.): NA | emissions, any work practice standards (e.g. production | | | | | | |
| П. (| TANK INFORMATION (required) - See Attached E | mission Master Report for the following information | | | | | | |
| 8. | Design Capacity (specify barrels or gallons). Use height. | the internal cross-sectional area multiplied by internal | | | | | | |
| 9A. | Tank Internal Diameter (ft) | 9B. Tank Internal Height (or Length) (ft) | | | | | | |
| 10A | A. Maximum Liquid Height (ft) | 10B. Average Liquid Height (ft) | | | | | | |
| 11A | A. Maximum Vapor Space Height (ft) | 11B. Average Vapor Space Height (ft) | | | | | | |
| 12. | Nominal Capacity (specify barrels or gallons). This is liquid levels and overflow valve heights. | s also known as "working volume" and considers design | | | | | | |

| I3A.Maximum annual throughput (gal/yr)13B.Maximum daily throughput (gal/day)317,007 gal/yr | | | | | | | | | |
|--|--|--|--|--|--|--|--|--|--|
| 14. Number of Tumovers per year (annual net throughput | 14. Number of Tumovers per year (annual net throughput/maximum tank liquid volume) | | | | | | | | |
| 15. Maximum tank fill rate (gal/min) | | | | | | | | | |
| 16. Tank fill method Submerged | Splash Bottom Loading | | | | | | | | |
| 17. Complete 17A and 17B for Variable Vapor Space Ta | nk Systems Does Not Apply | | | | | | | | |
| 17A. Volume Expansion Capacity of System (gal) | 17B. Number of transfers into system per year | | | | | | | | |
| 18. Type of tank (check all that apply): Fixed Roof vertical horizontal other (describe) Extemal Floating Roof pontoon roof Domed External (or Covered) Floating Roof Internal Floating Roof vertical column su Variable Vapor Space lifter roof Pressurized spherical cylind rical Underground Other (describe) | ipportself-supporting diaphragm | | | | | | | | |

Attachment L FUGITIVE EMISSIONS FROM PAVED HAULROADS

INDUSTRIAL PAVED HAULROADS (including all equipment traffic involved in process, haul trucks, endloaders, etc.)

| ltem Number | Description | Mean Vehicle Weight (tons) | Miles per Trip | Maximum Trips per Day | Maximum Trips per Year | Control Device ID Number | Control Efficiency (%) |
|----------------|---|-------------------------------------|-------------------|--------------------------|---------------------------|---|------------------------------|
| 1 | Truck - Binder Oil | 21.6 | 0.46 | 1 | 52 | | 75% |
| 2 | Truck - Oxygen | 11.3 | 0.46 | 4 | 1,144 | | |
| 3 | Truck - Raw Material to 210 | 25.0 | 0.46 | 28 | 6,656 | All roads at the | |
| 4 | Truck - DeSOx and Binder | 21.6 | 0.46 | 2 | 676 | RAN facility will be paved. | |
| 5 | Truck - Waste | 21.6 | 0.46 | 1 | 260 | ROCKWOOL will operate a streetsweeper on an as needed basis to minimize the generation of | |
| 6 | Truck – Pallet and Foil | 25.0 | 0.76 | 5 | 1,300 | | |
| 7 | Truck - Finished Goods | 13.3 | 0.76 | 73 | 20,800 | | |
| 8 | FEL – Diverted Melt from Bldg 300 to Pit Waste (170) | 17.8 | 0.27 | 67 | 12,295 | | |
| 9 | FEL – Crushed Melt from 170 to 210 | 17.8 | 0.10 | 67 | 12,295 | dusts from road traffic. | |
| 10 | FEL – Raw Material from 210 to Feed Hopper | 17.8 | 0.06 | 85 | 31,147 | | |
| 11 | FEL – Raw Material from Stockpile to 210 | 17.8 | 0.16 | 115 | 31,147 | | |
| 12 | Truck – Raw Material from Stockpile to 210 | 25.0 | 0.27 | 30 | 1,087 | | |

Source: AP-42 Fifth Edition – 11.2.6 Industrial Paved Roads

 $\mathsf{E} = [k \ge (sL)^{0.91} \ge (W)^{1.02}] \ge [1 - P/(4N)] =$

Where:

Ib/Vehicle Mile Traveled (VMT)

| k = | Particle size multiplier (lb/VMT) | PM – 0.011 PM ₁₀ – 0.0022 PM ₂₅ – 0.00054 | | | | |
|--------|---|---|--|--|--|--|
| sL = | Road surface silt loading (g/m ²) | Finished product road surface silt loading – 0.2 Raw materials road surface silt loading – 8.2 | | | | |
| P = | Number of "wet" days with at least 0.01 in of precipitation during the averaging period | 148 | | | | |
| N = | Number of days in the averaging period | 365 | | | | |
| W = | Average vehicle weight traveling the road (tons) | See table above | | | | |
| For lb | For lb/hr: [lb + VMT] × [VMT + trip] × [Trips + Hour] = lb/hr | | | | | |

For TPY: [lb + VMT] × [VMT + trip] × [Trips + Hour] × [Ton + 2000 lb] =

Tons/year

114 of 145

| Item No. | Uncontro | olled PM ₁₀ | Controll | ed PM ₁₀ | | |
|----------|------------------|-------------------------|------------------------------|---------------------|--|--|
| | lb/hr | ton/yr | lb/hr | ton/yr | | |
| 1 | <0.01 | <0.01 | <0.01 | <0.01 | | |
| 2 | 0.01 | 0.04 | <0.01 | 0.01 | | |
| 3 | 0.13 | 0.55 | 0.03 | 0.14 | | |
| 4 | 0.01 | 0.05 | <0.01 | 0.01 | | |
| 5 | <0.01 | 0.02 | <0.01 | <0.01 | | |
| 6 | <0.01 | 0.01 | <0.01 | <0.01 | | |
| 7 | 0.01 | 0.05 | <0.01 | 0.01 | | |
| 8 | 0.10 | 0.42 | 0.02 | 0.10 | | |
| 9 | 0.04 | 0.16 | 0.01 | 0.04 | | |
| 10 | 0.05 | 0.24 | 0.01 | 0.06 | | |
| 11 | 0.14 | 0.63 | 0.04 | 0.16 | | |
| 12 | <0.01 | 0.05 | <0.01 | 0.01 | | |
| TOTALS | TOTALS 0.49 2.21 | | 0.12 0.55 | | | |
| | 7 | - | | | | |
| ltem No. | Uncontro | olled PM _{2.5} | Controlled PM _{2.5} | | | |
| | lb/hr | ton/yr | lb/hr | ton/yr | | |
| 1 | <0.01 | <0.01 | <0.01 | <0.01 | | |
| 2 | <0.01 | 0.01 | <0.01 | <0.01 | | |
| 3 | 0.03 | 0.13 | 0.01 | 0.03 | | |
| 4 | <0.01 | 0.01 | <0.01 | <0.01 | | |
| 5 | <0.01 | <0.01 | <0.01 | <0.01 | | |
| 6 | <0.01 | <0.01 | <0.01 | <0.01 | | |
| 7 | <0.01 | 0.01 | <0.01 | <0.01 | | |
| 8 | 0.02 | 0.10 | 0.01 | 0.03 | | |
| 9 | 0.01 | 0.04 | <0.01 | 0.01 | | |
| 10 | 0.01 | 0.06 | <0.01 | 0.01 | | |
| 11 | 0.04 | 0.15 | 0.01 | 0.04 | | |
| 12 | <0.01 | 0.01 | <0.01 | <0.01 | | |
| TOTALS | 0.12 | 0.54 | 0.03 | 0.14 | | |

SUMMARY OF PAVED HAULROAD EMISSIONS

Attachment M

Attachment M Air Pollution Control Device Sheet (AFTERBURNER SYSTEM)

Control Device ID No. (must match Emission Units Table): **CO-AB** – **The afterburner is routed through HE01.**

| | Equipment Information | | | | |
|-----|---|--|--|--|--|
| 1. | Manufacturer: Bromkamp Model No. | 2. ☐ Thermal Energy Recovery ☑ Recuperative (Conventional) ☐ Catalytic | | | |
| 3. | Provide diagram(s) of unit describing capture system capacity, horsepower of movers. If applicable, state h | m with duct arrangement and size of duct, air volume, hood face velocity and hood collection efficiency. | | | |
| 4. | Combustion chamber dimensions:Length:ftDiameter:ftCross-sectional area:ft² | 5. Stack Dimensions: Height: 212.66 ft Diameter: 12.93 ft | | | |
| 6. | Combustion (destruction) efficiency:Estimated:95Minimum guaranteed:95% | 7. Retention or residence time of materials in combustion chamber: of materials in sec Maximum: sec Minimum: sec | | | |
| 8. | Throat diameter: ft | 9. Combustion Chamber Volume: ft ³ | | | |
| 10. | Fuel used in burners: ☑ Natural Gas ☐ Fuel Oil, Number: ☐ Other, specify: | 11. Burners per afterburner: Number of burners: 1 BTU/hr for burner: 9,860,000 | | | |
| 12. | Fuel heating value of natural gas: 1026 BTU/scf | 13. Flow rate of natural gas: ft ³ /min | | | |
| 14. | Is a catalyst material used?: ☐ Yes | 15. Expected frequency of catalyst replacement: yr(s) 16. Date catalyst was last replaced: Month/Year: | | | |
| 17. | Space Velocity of the catalyst material used: 1/hour | 18. Catalyst area:ft²19. Volume of catalyst bed:ft³ | | | |
| 20. | Minimum loading: Maximum loading: | 21. Temperature catalyst bed inlet:°FTemperature catalyst bed outlet:°F | | | |
| 22. | Explain degradation or performance indicator criteria | determining catalyst replacement: | | | |
| 23. | Heat exchanger used? Yes No | 24. Heat exchanger surface area?ft² | | | |
| | Describe heat exchanger: | 25. Average thermal efficiency: % | | | |
| | Temperature of gases: After preheat: | °F Before preheat: °F | | | |
| 27. | Dilution air flow rate: ft ³ /minut | e | | | |

28. Describe method of gas mixing used:

| | Waste Gas (Emission Stream) to be Burned | | | | | | |
|----------|--|---------------------|---|--|-----------------------|--------------------|--|
| 29. | Name | Grain | Quantity s of H ₂ S/100 ft ² | Quantity-Dens (LB/hr, ft ³ /hr, et | | of Material | |
| | | Grain | 13 01 1120/ 100 It | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| 30. | Estimate total combust | ibles to aft | erburner 18,95 | 0 scfm (capacity) | | | |
| 31. | Estimated total flow ra | ite to after | - | - | to be burned, carrie | r gases, auxiliary | |
| | fuel, etc.: | | | ACF/hr, or scfm | | | |
| | Total flow rate = Flue g | as flow rat | e | | | | |
| 32. | 32. Afterburner operating parameters: During maximum operation of feeding unit(s) During maximum operation of feeding unit(s) During maximum operation of feeding unit(s) | | | | | | |
| | Combustion chamber temperature in °F | | | | 1621.22 | | |
| | Emission stream gas temperature in °F | | | | 580 | | |
| | Combined gas stream | entering ca | atalyst bed in | | | | |
| | Flue stream leaving the | e catalyst b | bed | | | | |
| | Emission stream flow r | ate (scfm) | | | 18,950 | | |
| | Efficiency (VOC Reduc | tion) | | % | 95 % | % | |
| | Efficiency (Other; spec | ify contami | nant) | % | % | % | |
| 33. | Inlet Emission stream p | parameters | : | | | | |
| <u> </u> | | | Ma | iximum | Турі | cal | |
| | Pressure (mmHg): | | | | | | |
| | Heat Content (BTU/scf |): | | | | | |
| | Oxygen Content (%): | , | | | | | |
| | Moisture Content (%): | | | | | | |
| | Are halogenated organics present? Yes No Are particulates present? Yes No Are metals present? Yes No | | | | | | |
| 34. | For thermal afterburner ⊠Yes □ | rs, is the co No | ombustion chamb | er temperature contir | nuously monitored an | d recorded? | |
| 35. | For catalytic afterburn recorded? Yes | ers, is the | e temperature rise | e across the catalys | st bed continuously i | monitored and | |
| 36. | 36. Is the VOC concentration of exhaust monitored and recorded? Yes No | | | | | | |

| 37. Describe any air pollution control device inlet and outlet gas conditioning processes (e.g., gas cooling, gas reheating, gas humidification): | | | | | | | | | |
|---|---|--|--|--|--|--|--|--|--|
| 38 Describe the collect | ation material disposal system: | | | | | | | | |
| 36. Describe the collec | 38. Describe the collection material disposal system: | | | | | | | | |
| 39. Have you included | Afterburner Control Device in the | e Emissions Points Data Summary Sheet? | | | | | | | |
| Please propose r proposed operatir | 40. Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits. | | | | | | | | |
| MONITORING: | | RECORDKEEPING: | | | | | | | |
| Not impacted by upd | ates. | Not impacted by updates. | | | | | | | |
| REPORTING: | | TESTING: | | | | | | | |
| Not impacted by up | odates. | Not impacted by updates. | | | | | | | |
| MONITORING: RECORDKEEPING: REPORTING: TESTING: | RECORDKEEPING: REPORTING: monitored in order to demonstrate compliance with the operation of this proc equipment or air control device. Please describe the proposed recordkeeping that will accompany the monitoring. Please describe any proposed emissions testing for this process equipment on pollution control device. | | | | | | | | |
| 41. Manufacturer's Gu | aranteed Capture Efficiency for each | ch air pollutant. | | | | | | | |
| 42. Manufacturer's Guaranteed Control Efficiency for each air pollutant. 95% minimum control efficiency 43. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty. | | | | | | | | | |
| 43. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty. | | | | | | | | | |

Attachment M Air Pollution Control Device Sheet (BAGHOUSE)

Control Device ID No. (must match Emission Units Table): CE01-BH

Equipment Information and Filter Characteristics

| Model No. 3. Number of compartment online for normal operation: 8 4. Provide diagram(s) of unit describing capture system with duct arrangement and size of duct, air volume, capacity, horsepower of movers. If applicable, state hood face velocity and hood collection efficiency. 5. Baghouse Configuration: Open Pressure Closed Pressure Closed Suction (check one) Electrostatically Enhanced Fabric Other, Specify 6. Filter Fabric Bag Material: 7. Bag Dimension: Diameter 6.30 in. Polyester Polypropylene Diameter 6.30 in. Eriber Glass Ceramics ft² Other, specify 0. Operating air to cloth ratio: ft/min 11. Baghouse Operation: © Continuous Automatic Intermittent 12. Method used to clean bags: 10. Operating air to cloth ratio: ft/min 11. Baghouse Operation: © Continuous Automatic Intermittent 12. Method used to clean bags: 0. Other: Bag Collapse Pulse Jet 13. Cleaning initiated by: Frequency if timer actuated % Gas Stream Characteristics 14. Operation Hours: Max. per day: 24 15. Collection efficiency: Rating: % 14. Operation | 1. Manufacturer: TBD | 2. Total number of compartments: 8 | | | | | |
|---|--|---------------------------------------|--------|--|--|--|--|
| capacity, horsepower of movers. If applicable, state hood face velocity and hood collection efficiency. 5. Baghouse Configuration: □ Open Pressure ☑ Closed Pressure □ Closed Suction □ (check one) □ Electrostatically Enhanced Fabric □ Other, Specify 0 6. Filter Fabric Bag Material: □ Other, Specify 7. Bag Dimension: □ Diameter 6.30 in. □ Polypester ☑ Polypester □ Diameter 6.30 in. □ Length 12.55 ft. 8. Total cloth area: 7363 ft² 9. Number of bags: □ 10. Operating air to cloth ratio: ft/min 11. Baghouse Operation: ☑ Continuous □ Automatic □ Intermittent 11. 12. Method used to clean bags: □ Reverse Air Jet □ Intermittent 12. 13. Cleaning initiated by: □ Reverse Air Jet □ Other: □ Other: □ Other: 0 Other: 14. Operation Hours: Max. per day: 24 15. Collection efficiency: % Max. per y: 8400 Gas Stream Characteristics 16. Gas flow rate into the collector: 44,217 ACFM at 104 °F and PSIA ACFM: Design: PSIA 14. Operation Hours: PSIA Average Expected: PSIA Neter | Model No. | · · | | | | | |
| (check one) ☐ Electrostatically Enhanced Fabric ☐ Other, Specify 6. Filter Fabric Bag Material: 7. Bag Dimension: ☐ Nomex nylon Wool ☐ Polyester Ø Polypropylene ☐ Acrylics ☐ Ceramics ☐ Fiber Glass 0. Length 12.55 ☐ Others, specify 10. Operating air to cloth ratio: 11. Baghouse Operation: ☑ Continuous ☐ Automatic ☐ Intermittent 12. Method used to clean bags: ☐ Other: ☐ Pneumatic Shaker ☐ Sonic Cleaning ☐ Pneumatic Shaker ☐ Sonic Cleaning ☐ Manual Cleaning ☐ Reverse Air Jet ☐ Manual Cleaning ☐ Reverse Air Jet ☐ Timer ☐ Other: ☐ Bag Collapse ☐ Other: ☐ Bag Collapse ☐ Other: ☐ Manual Cleaning ☐ Reverse Jet 13. Cleaning initiated by: ☐ Frequency if timer actuated ☐ Timer ☐ Gas Stream Characteristics 14. Operation Hours: Max, per yr: 8400 Gas Stream Characteristics PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/Ib. Dry Air 18. Gas Stre | | | | | | | |
| □ Other, Specify 6. Filter Fabric Bag Material: Nomex nylon Wool Polypropylene Acrylics Ceramics Fiber Glass Cotton Weight oz./sq.yd Total cloth area: 7363 ft² Number of bags: 10. Operating air to cloth ratio: ft/min 11. Baghouse Operation: Image: Continuous Automatic Intermittent 11. Baghouse Operation: Image: Continuous Automatic Intermittent 12. Method used to clean bags: Sonic Cleaning Reverse Air Jet Intermittent 12. Method used to clean bags: Sonic Cleaning Reverse Air Jet Other: Bag Collapse Sonic Cleaning Reverse Air Jet Other: Bag Collapse Pulse Jet Other: Other: 13. Cleaning initiated by: | 5. Baghouse Configuration: Open Pressure | Closed Pressure | 'n | | | | |
| 6. Filter Fabric Bag Material: | | anced Fabric | | | | | |
| Nomex nylon Wool Diameter 6.30 in. Polyester Polypropylene Length 12.55 ft. Acrylics Ceramics 8. Total cloth area: 7363 ft² Others, specify 9. Number of bags: 10. Operating air to cloth ratio: ft/min 11. Baghouse Operation: ☑ Continuous □ Automatic Intermittent 12. Mechanical Shaker □ Sonic Cleaning □ Reverse Air Jet □ Pneumatic Shaker □ Sonic Cleaning □ Reverse Air Flow □ Other: □ Timer □ Prequency if timer actuated □ Other: □ 0 □ Stabilized by: □ □ In. of water □ Other % Gas Stream Characteristics Gas Stream Characteristics % Maximum: PSIA Average Expected: PSIA 16. Gas Stream Temperature: 104 °F 19. Fan Requirements: Np 17. Water Vapor Content of Effluent Stream: Ib. Water/Ib. Dry Air 18. Gas Stream Temperature: Np | | | | | | | |
| □ Polyester □ Polypropylene Langte 10.50 in □ Ceramics □ Langte 10.50 in □ Cotton Weight oz./sq.yd in □ 1 □ Others, specify 10. Operating air to cloth ratio: ft² 11. Baghouse Operation: ☑ Continuous □ Automatic □ 12. Method used to clean bags: □ 0 □ Intermittent 12. Method used to clean bags: □ □ Intermittent 12. Method used to clean bags: □ 0 □ Intermittent 13. Cleaning initiated by: □ Sequence Air Flow □ Other 14. Operation Hours: Max. per day: 24 15. Collection efficiency: Rating: % Max. per y: 8400 Ist collection efficiency: Rating: % Gas Stream Characteristics 16. Gas flow rate into the collector: 44,217 ACFM at 104 °F and PSIA ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/Ib. Dry Air | | - | | | | | |
| Fiber Glass 8. Total cloth area: 7363 ft² Others, specify 0. Operating air to cloth area: 7363 ft² 9. Number of bags: 10. Operating air to cloth ratio: ft/min 11. Baghouse Operation: Image: Continuous Automatic Intermittent 12. Method used to clean bags: Image: Continuous Automatic Intermittent 12. Method used to clean bags: Image: Continuous Automatic Intermittent 13. Cleaning initiated by: Image: Content of Prage Image: Content of Prage Image: Content of Prage 14. Operation Hours: Max. per day: 24 Max. per yr: 8400 15. Collection efficiency: Rating: % Gas Stream Characteristics Gas Stream Characteristics PSIA Average Expected: PSIA 16. Gas flow rate into the collector: 44,217 ACFM at 104 °F and PSIA Average Expected: PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/Ib. Dry Air Ib. Water/Ib. Dry Air N N 18. Gas Stream Temperature: 104 °F 19. Fan Requirements: hp OR ft³/mi 10. OR ft³/mi N N N N <td< td=""><td>Polyester Polypropylene</td><td></td><td></td></td<> | Polyester Polypropylene | | | | | | |
| □ Cotton Weight oz./sq.yd 9. Number of bags: □ Others, specify 11. Baghouse Operation: ☑ Continuous □ Automatic □ Intermittent 12. Method used to clean bags: □ □ Pneumatic Shaker □ Sonic Cleaning □ Pneumatic Shaker □ Sonic Cleaning □ Reverse Air Flow □ Other: □ Bag Collapse ☑ Pulse Jet □ Manual Cleaning □ Reverse Air Flow □ Timer □ Prequency if timer actuated ☑ Expected pressure drop range in. of water 14. Operation Hours: Max. per day: 24 Max. per yr: 8400 □ Other ③ Stream Characteristics Gas Stream Characteristics 16. Gas flow rate into the collector: 44,217 ACFM at 104 °F and PSIA ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/Ib. Dry Air n n 18. Gas Stream Temperature: 104 °F 19. Fan Requirements: hp 0R If ¹ /mi n n 20. Low in. H ₂ O <td></td> <td>· · · · · · · · · · · · · · · · · · ·</td> <td></td> | | · · · · · · · · · · · · · · · · · · · | | | | | |
| □ Others, specify 10. Operating air to cloth ratio: ft/min 11. Baghouse Operation: ☑ Continuous □ Automatic □ Intermittent 12. Method used to clean bags: □ Mechanical Shaker □ Sonic Cleaning □ Reverse Air Jet □ Intermittent 12. Method used to clean bags: □ Mechanical Shaker □ Sonic Cleaning □ Reverse Air Jet □ Intermittent 13. Cleaning initiated by: □ Timer □ Prequency if timer actuated □ Other 14. Operation Hours: Max. per day: 24 15. Collection efficiency: Rating: % Max. per yr: 8400 Guaranteed minimum: % Gas Stream Characteristics 16. Gas flow rate into the collector: 44,217 ACFM at 104 °F and PSIA ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/Ib. Dry Air 18. Gas Stream Temperature: 104 °F 19. Fan Requirements: hp 0R ft³/mi n 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H ₂ O 21. Particulate Loading: Inlet: grain/scf Outlet: PM ₁₀ - 0.002 <t< td=""><td></td><td></td><td></td></t<> | | | | | | | |
| 11. Baghouse Operation: Continuous Automatic Intermittent 12. Method used to clean bags: Mechanical Shaker Sonic Cleaning Reverse Air Jet Pneumatic Shaker Bag Collapse Pulse Jet Manual Cleaning Reverse Jet 13. Cleaning initiated by: Timer 14. Operation Hours: Max. per day: 24 Collection efficiency: Rating: % Gas Stream Characteristics Gas flow rate into the collector: 44,217 ACFM at 104 °F and PSIA PSIA ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA PSIA ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA Reverse are close across baghouse. Pressure Drop: High | | | | | | | |
| 12. Method used to clean bags: Mechanical Shaker Pneumatic Shaker Bag Collapse Manual Cleaning Reverse Air Flow Manual Cleaning Reverse Air Flow Manual Cleaning Reverse Jet 13. Cleaning initiated by: Timer Timer Sexpected pressure drop range 14. Operation Hours: Max. per day: 24 Max. per day: 24 Max. per yr: 8400 Gas Stream Characteristics 16. Gas flow rate into the collector: 44,217 ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/lb. Dry Air 18. Gas Stream Temperature: 104 °F 19. Fan Requirements: hp OR ft³/mi n 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. HzO Low in. HzO 21. Particulate Loading: Inlet: grain/scf Outlet: PM10 - 0.002 grain/scf | | | ft/min | | | | |
| ☐ Mechanical Shaker ☐ Sonic Cleaning ☐ Reverse Air Jet ☐ Pneumatic Shaker ☐ Reverse Air Flow ☐ Other: ☐ Manual Cleaning ☐ Reverse Jet ☐ Other: 13. Cleaning initiated by: ☐ Frequency if timer actuated ☐ Timer ☐ Other 14. Operation Hours: Max. per day: 24 15. Collection efficiency: Rating: % Max. per yr: 8400 Gas Stream Characteristics % Gas Stream Characteristics 16. Gas flow rate into the collector: 44,217 ACFM at 104 °F and PSIA ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/lb. Dry Air 18. Gas Stream Temperature: 104 °F 19. Fan Requirements: hp 0R ft³/mi n 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H₂O Low in. H₂O 21. Particulate Loading: Inlet: grain/scf Outlet: PM₁₀ - 0.002 grain/scf | 11. Baghouse Operation: 🛛 Continuous | Automatic Intermittent | | | | | |
| ☐ Timer ☐ Frequency if timer actuated ☑ Expected pressure drop range in. of water ☐ Other 14. Operation Hours: Max. per day: 24 Max. per yr: 8400 15. Collection efficiency: Rating: % Guaranteed minimum: % Gas Stream Characteristics 16. Gas flow rate into the collector: 44,217 ACFM at ACFM at ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/Ib. Dry Air 18. Gas Stream Temperature: 104 °F 19. Fan Requirements: hp OR hp ft³/mi n 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H ₂ O in. H ₂ O 21. Particulate Loading: Inlet: grain/scf Outlet: PM ₁₀ - 0.002 grain/scf | ☐ Mechanical Shaker ☐ Sonic Cleaning ☐ Pneumatic Shaker ☐ Reverse Air Flow ☐ Bag Collapse ☑ Pulse Jet | | | | | | |
| Max. per yr: 8400 Guaranteed minimum: % Gas Stream Characteristics 16. Gas flow rate into the collector: 44,217 ACFM at 104 °F and PSIA ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/Ib. Dry Air Ib. Water/Ib. Dry Air Mp 18. Gas Stream Temperature: 04 °F 19. Fan Requirements: hp 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H ₂ O 21. Particulate Loading: Inlet: grain/scf Outlet: PM ₁₀ - 0.002 grain/scf | Timer | | | | | | |
| Gas Stream Characteristics 16. Gas flow rate into the collector: 44,217 ACFM at 104 °F and PSIA ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/lb. Dry Air Ib. Water/lb. Dry Air 18. Gas Stream Temperature: 104 °F 19. Fan Requirements: hp 0R ft³/mi n n 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H2O 21. Particulate Loading: Inlet: grain/scf Outlet: PM10 - 0.002 grain/scf | | , , | | | | | |
| 16. Gas flow rate into the collector: 44,217 ACFM at 104 °F and PSIA ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/Ib. Dry Air Ib. Water/Ib. Dry Air 18. Gas Stream Temperature: 104 °F 19. Fan Requirements: hp 0R ft³/mi n 0R ft³/mi n 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H ₂ O in. H ₂ O 21. Particulate Loading: Inlet: grain/scf Outlet: PM ₁₀ - 0.002 grain/scf | | | % | | | | |
| ACFM: Design: PSIA Maximum: PSIA Average Expected: PSIA 17. Water Vapor Content of Effluent Stream: Ib. Water/Ib. Dry Air Ib. Water/Ib. Dry Air 18. Gas Stream Temperature: 104 °F 19. Fan Requirements: hp 0R ft³/mi n 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H ₂ O 21. Particulate Loading: Inlet: grain/scf Outlet: PM ₁₀ - 0.002 grain/scf | | | | | | | |
| 17. Water Vapor Content of Effluent Stream: Ib. Water/Ib. Dry Air 18. Gas Stream Temperature: 104 °F 19. Fan Requirements: hp 0R ft³/mi n 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H ₂ O 21. Particulate Loading: Inlet: grain/scf Outlet: PM ₁₀ - 0.002 grain/scf | · · · | | | | | | |
| 18. Gas Stream Temperature: 104 °F 19. Fan Requirements: hp OR ft³/mi 0 n 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H₂O 21. Particulate Loading: Inlet: grain/scf Outlet: PM₁₀ - 0.002 grain/scf | 5 | 0 1 | iA | | | | |
| OR ft³/mi 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H ₂ O Low in. H ₂ O 21. Particulate Loading: Inlet: grain/scf Outlet: PM ₁₀ - 0.002 grain/scf | | - | | | | | |
| 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H ₂ O 20. Stabilized static pressure loss across baghouse. Pressure Drop: Lighthan the state of the stat | 18. Gas Stream Temperature: 104 °F | | | | | | |
| 20. Stabilized static pressure loss across baghouse. Pressure Drop: High in. H ₂ O Low in. H ₂ O 21. Particulate Loading: Inlet: grain/scf Outlet: PM ₁₀ - 0.002 grain/scf | | OR | | | | | |
| Lowin. H2O21. Particulate Loading:Inlet:grain/scfOutlet: PM10 - 0.002 grain/scf | 20 Stabilized static process loss correspondence. Dro | | | | | | |
| 21. Particulate Loading: Inlet: grain/scf Outlet: PM ₁₀ - 0.002 grain/scf | 20. Stabilized static pressure loss across bagnouse. Pre | | | | | | |
| | 21. Particulate Loading: Inlet: | | | | | | |
| | | • • | | | | | |

| 22. Type of Pollutant(s) to be collected (if particulate give specific type): PM ₁₀ , PM _{2.5} , and HAPs | | | | | | |
|--|---------------|-----------------------------------|--------------|---------|------------------|------------------|
| 23. Is there any SO₃ in the emission s | stream? | | /es SC | D₃ cont | ent: | ppmv |
| 24. Emission rate of pollutant (specify |) into and ou | 1 | | design | | |
| Pollutant | | lb/hr | N grains/ | acf | Ol Ib/hr | UT grains/acf |
| Filterable PM ₁₀ | | | | | .77 | |
| Filterable PM _{2.5} | | | | | .21 | |
| Total HAPS | | | | | .77 | |
| 25. Complete the table: | Particle S | Size Distribution to Collector | | Fra | ction Efficiency | y of Collector |
| Particulate Size Range (microns) | Weig | ht % for Size Ra | ange | | Weight % for S | ize Range |
| 0 – 2 | | | | | | |
| 2 – 4 | | | | | | |
| 4 – 6 | | | | | | |
| 6 – 8 | | | | | | |
| 8 – 10 | | | | | | |
| 10 – 12 | | | | | | |
| 12 – 16 | | | | | | |
| 16 – 20 | | | | | | |
| 20 – 30 | | | | | | |
| 30 - 40 | | | | | | |
| 40 – 50 | | | | | | |
| 50 – 60 | | | | | | |
| 60 – 70 | | | | | | |
| 70 – 80 | | | | | | |
| 80 – 90 | | | | | | |
| 90 – 100 | | | | | | |
| >100 | | | | | | |

| 26. How is filter monitored for indications of deterioration (e.g., broken bags)? | |
|---|-----|
| Continuous Opacity | |
| Pressure Drop | |
| Alarms-Audible to Process Operator | |
| Visual opacity readings, Frequency: | |
| ☐ Other, specify: | |
| | |
| 27. Describe any recording device and frequency of log entries: | |
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| 28. Describe any filter seeding being performed: | |
| 20. Describe any filler seeding being performed. | |
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| 29. Describe any air pollution control device inlet and outlet gas conditioning processes (e.g., gas cooling, g | 100 |
| reheating, gas humidification): | jas |
| reneating, gas humidineation). | |
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| 30. Describe the collection material disposal system: | |
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| | |
| 31. Have you included Baghouse Control Device in the Emissions Points Data Summary Sheet? Yes | |

| Please propose m proposed operatin proposed emission | g parameters. Please propose | eporting in order to demonstrate compliance with the testing in order to demonstrate compliance with the |
|---|---|---|
| MONITORING: | | RECORDKEEPING: |
| | ring plan in Attachment O. | See proposed recordkeeping plan in Attachment O. |
| REPORTING: | | TESTING: |
| | ng plan in Attachment O. | See proposed reporting plan in Attachment O. |
| MONITORING: | | ocess parameters and ranges that are proposed to be strate compliance with the operation of this process |
| RECORDKEEPING: REPORTING: | Please describe the proposed rec Please describe any proposed pollution control device. | cordkeeping that will accompany the monitoring. emissions testing for this process equipment on air |
| TESTING: | Please describe any proposed pollution control device. | emissions testing for this process equipment on air |
| | aranteed Capture Efficiency for eac | |
| 34. Manufacturer's Gua | aranteed Control Efficiency for eac | h air pollutant. |
| PM ₁₀ - >99% efficiency PM _{2.5} - > 99% efficienc | | |
| 25 Describe all operati | ing ranges and maintanance proce | dures required by Manufacturer to maintain warranty. |
| 55. Describe all operati | ing ranges and maintenance proce | oures required by Manufacturer to maintain warranty. |

Attachment M Air Pollution Control Device Sheet (BAGHOUSE)

Control Device ID No. (must match Emission Units Table): CE02-BH

Equipment Information and Filter Characteristics

| 1. Manufacturer: TBD | 2. Total number of compartments: TBD | |
|---|--|--------|
| Model No. | Number of compartment online for no operation: TBD | ormal |
| Provide diagram(s) of unit describing capture syste capacity, horsepower of movers. If applicable, state | | ume, |
| 5. Baghouse Configuration: Open Pressure | Closed Pressure | |
| (check one) Check one Check one | anced Fabric | |
| 6. Filter Fabric Bag Material: | 7. Bag Dimension: | |
| Nomex nylon 🗌 Wool | Diameter TBD in. | - |
| Acrylics Ceramics | Length TBD ft. | |
| ☐ Fiber Glass ☐ Cotton Weight oz./sq.yd | 8. Total cloth area: TBD ft ² | |
| ☐ Cotton Weight oz./sq.yd ☐ Teflon Thickness in | 9. Number of bags: TBD | |
| Others, specify | 10. Operating air to cloth ratio: ft/m | nin |
| 11. Baghouse Operation: Continuous | Automatic X Intermittent | |
| 12. Method used to clean bags: Mechanical Shaker Sonic Cleaning Pneumatic Shaker Reverse Air Flow Bag Collapse Pulse Jet Manual Cleaning Reverse Jet | Reverse Air Jet Other: | |
| 13. Cleaning initiated by: Timer Expected pressure drop range in. of water | Frequency if timer actuated Other | |
| 14. Operation Hours: Max. per day: 24 Max. per yr: 8400 | 15. Collection efficiency: Rating: Guaranteed minimum: | % % |
| Gas Stream C | haracteristics | |
| 16. Gas flow rate into the collector: 12,633 ACFN | 1 at 104 °F and PSIA | |
| ACFM: Design: PSIA Maximum: | PSIA Average Expected: PSIA | |
| 17. Water Vapor Content of Effluent Stream: | lb. Water/lb. Dry Air | |
| 18. Gas Stream Temperature: 104 °F | 19. Fan Requirements: h | |
| | | ³/mi |
| 20. Stabilized static pressure loss across baghouse. Pre | n ssure Drop: High in | 1. H2O |
| | | n. H2O |
| 21. Particulate Loading: Inlet: | grain/scf Outlet: PM 10 - 0.002 grain/scf | |
| | Outlet: PM_{2.5} - 0.002 grain/scf | |

| 22. Type of Pollutant(s) to be collected PM₁₀ and PM_{2.5} | d (if particula | te give specific | type): | | | |
|--|-----------------|------------------|---------------|----------|---------------|-----------------|
| 23. Is there any SO₃ in the emission s | stream? | No 🗌 | Yes SC | D₃ conte | nt: | ppmv |
| 24. Emission rate of pollutant (specify | | | | design c | | litions: |
| Pollutant | | lb/hr | IN grains/ | acf | lb/hr | OUT grains/acf |
| Filterable PM ₁₀ | | | | | .22 | |
| Filterable PM _{2.5} | | | | | .22 | |
| | | | | | | |
| 25. Complete the table: | Particle S | ize Distributio | | Frac | tion Efficien | cy of Collector |
| Particulate Size Range (microns) | Weigl | nt % for Size F | | v | Veight % for | Size Range |
| 0 – 2 | | | | | | |
| 2-4 | | | | | | |
| 4 – 6 | | | | | | |
| 6 – 8 | | | | | | |
| 8 – 10 | | | | | | |
| 10 – 12 | | | | | | |
| 12 – 16 | | | | | | |
| 16 – 20 | | | | | | |
| 20 – 30 | | | | | | |
| 30 – 40 | | | | | | |
| 40 – 50 | | | | | | |
| 50 – 60 | | | | | | |
| 60 – 70 | | | | | | |
| 70 – 80 | | | | | | |
| 80 – 90 | | | | | | |
| 90 – 100 | | | | | | |
| >100 | | | | | | |

| 26. How is filter monitored for indications of deterioration (e.g., broken bags)? |
|---|
| Continuous Opacity |
| Pressure Drop Alarms-Audible to Process Operator |
| Visual opacity readings, Frequency: |
| Other, specify: |
| 27. Describe any recording device and frequency of log entries: |
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| 00. Describe any filter as discributer referenced |
| 28. Describe any filter seeding being performed: |
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| 29. Describe any air pollution control device inlet and outlet gas conditioning processes (e.g., gas cooling, gas |
| reheating, gas humidification): |
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| 30. Describe the collection material disposal system: |
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| |
| 31. Have you included Baghouse Control Device in the Emissions Points Data Summary Sheet? Yes |

| | ring, Recordkeeping, Reporting, | |
|---|--------------------------------------|---|
| | ng parameters. Please propose | eporting in order to demonstrate compliance with the testing in order to demonstrate compliance with the |
| MONITORING: | | RECORDKEEPING: |
| See proposed monito | ring plan in Attachment O. | See proposed recordkeeping plan in Attachment O. |
| | | |
| | | |
| | | |
| REPORTING: | | TESTING: |
| See proposed reporting | ng plan in Attachment O. | See proposed reporting plan in Attachment O. |
| | | |
| | | |
| | | |
| MONITORING: | | ocess parameters and ranges that are proposed to be strate compliance with the operation of this process |
| RECORDKEEPING: | equipment or air control device. | cordkeeping that will accompany the monitoring. |
| REPORTING: | Please describe any proposed | emissions testing for this process equipment on air |
| TESTING: | | emissions testing for this process equipment on air |
| 22 Manufaaturar'a Cu | pollution control device. | ah air nallutant |
| | aranteed Capture Efficiency for each | cn air pollutant. urce that is not capturing emissions from an |
| | re is not applicable to this sourc | |
| | | |
| | | |
| 34 Manufacturer's Gu | aranteed Control Efficiency for eac | h air nollutant |
| | - | |
| PM ₁₀ - >99% efficiency PM _{2.5} - > 99% efficienc | | |
| | | |
| | | |
| 35. Describe all operat | ing ranges and maintenance proce | edures required by Manufacturer to maintain warranty. |
| | | |
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Roxul USA Inc. dba ROCKWOOL Ranson, West Virginia Summary of Facility Emissions

Modified units New units Removed units

| | | | | | | | US | | _ | | _ | _ | | METRIC | | | | | | | | | | | |
|----------------|--|-----------------|-----------------|----------------|-----------------|----------------------|----------|------------------|-------------------|------------------|---------|------------------|-----------------------|-------------------|----------|------------------|-------------------|------------------------|------------------------|--------------------|---------------------|--|---------------------|--------------------|-----------|
| Source ID | Source Description | NOx (ton/vr) | SO2 (ton/yr) | CO (ton/yr) | VOC (ton/yr) | Total PM (ton/yr) | Filt. PM | PM10 (ton/yr) | PM2.5 (ton/yr) | CO2e (ton/yr) | H2SO4 | Lead (ton/yr) | Total HAP (ton/yr) | NOx (tonne/yr) | SO2 | CO (tonne/yr) | VOC (tonne/yr) | Total PM (tonne/yr) | Filt. PM (tonne/yr) | PM10 (tonne/vr) | PM2.5 (tonne/vr) | CO2e (tonne/vr) | H2SO4 (tonne/yr) | Lead (tonne/vr) | Total HAF |
| Minwool Line | | 1 | | | | 1 | | | | 1 | | | | | | | | | | | | | | | |
| B210/B211 | Raw Material Storage (B210) | | | | | 0.28 | 0.28 | 0.13 | 0.02 | | | | | 1 | | | E | 0.26 | 0.26 | 0.12 | 0.02 | 1. | | | |
| B215 | Raw Material Loading Hopper (B215) | | | | | 0.06 | 0.06 | 0.03 | 4.03E-03 | | | | | | | | | 5.10E-02 | 5.10E-02 | 2.41E-02 | 3.65E-03 | | | | - |
| IMF11 | Conveyor Transition Point (B215 to B220) | | - | - | | 1.74E-02 | 1.74E-02 | 1.74E-02 | 8.69E-03 | - | | | - | | | - | | 0.02 | 0.02 | 0.02 | 0.01 | | | | |
| IMF17 | B220 Material Handling | | | | | 1.49 | 1.49 | 0.61 | 0.56 | - | - | | | | | | - | 1.35 | 1.35 | 0.55 | 0.51 | - | | | |
| IMF12 | Conveyor Transfer Point (B215) | - | | - | - | 6.16E-02 | 6.16E-02 | 2.26E-02 | 2.26E-02 | | - | | | - | | | - | 0.06 | 0.06 | 0.02 | 0.02 | | - | | |
| IMF16 | Conveyor Transfer Point (B300) | - | | - | - | 6.16E-02 | 6.16E-02 | 2.26E-02 | 2.26E-02 | | | 1 | | - | | | - | 0.06 | 0.06 | 0.02 | 0.02 | | - | - | |
| IMF15 | Outside B220 Transfer Points | - | | | < - · · · | 7.69E-02 | 7.69E-02 | 2.82E-02 | 2.82E-02 | - | | | | | | - H - C | | 0.07 | 0.07 | 0.03 | 0.03 | | - | | |
| RM_REJ | Raw Material Reject Collection Drop | - | - | - | - | 1.12E-03 | 1.12E-03 | 5.32E-04 | 8.05E-05 | | | | | | | | - | 1.02E-03 | 1.02E-03 | 4.83E-04 | 7.31E-05 | 1000 | | - | - |
| IMF21 | Charging Building Vacuum Cleaning Filter | | | - | | 2.41E-02 | 2.41E-02 | 2.41E-02 | 1.21E-02 | - | - | | | | - | | - | 2.19E-02 | 2.19E-02 | 2.19E-02 | 1.10E-02 | | | | |
| IMF24 | Pre-heat Burner | 1.52 | 0.01 | 1.76 | 0.12 | 0.16 | 0.04 | 0.16 | 0.16 | 2,519.44 | - | 1.05E-05 | 0.04 | 1.38 | 0.01 | 1.60 | 0.10 | 0.14 | 0.04 | 0.14 | 0.14 | 2,285.59 | | 9.51E-06 | 0.04 |
| IMF01 | Melting Furnace | 156.95 | 141.25 | 13.48 | 1.29 | 9.73 | 9.73 | 9.73 | 9.73 | 77,076.96 | 7.85 | 1.57E-04 | 14.42 | 142.38 | 128.14 | 12.23 | 1.17 | 17.66 | 8.83 | 8.83 | 8.83 | 69,923.13 | 7.12 | 1.42E-04 | 13.08 |
| IMF07 | One (1) Storage Silo (Filter Fines Day) | - | - | | | 0.01 | 0.01 | 0.01 | 0.01 | - | 1000 | | | | | | | 0.01 | 0.01 | 0.01 | 0.01 | | · · · · · | | - |
| IMF10 | Filter Fines Recieving Silo | - | | - | | 0.06 | 0.06 | 0.06 | 0.03 | - | - | | | | | - | - | 0.05 | 0.05 | 0.05 | 0.03 | - | | | |
| IMF08 | Sorbent Silo | | | | | 0.06 | 0.06 | 0.06 | 0.03 | - | - | | | | | | | 0.05 | 0.05 | 0.05 | 0.03 | | | | |
| IMF09 | Spent Sorbent Silo | | | - | | 0.06 | 0.06 | 0.06 | 0.03 | | | | | | | | | 0.05 | 0.05 | 0.05 | 0.03 | | | | |
| DI | Dry Ice Cleaning | - | | - | - | - | - | | - | 1,527.80 | - | | | - | - | - | - | | - | | | 1,386.00 | - | - | |
| CM12 | Fleece Application Vent 1 | | | - | 6.85 | | | | - | - | | | 6.85 | | | | 6.22 | | | | | | | | 6.22 |
| CM13 | Fleece Application Vent 2 | | | - | | | - | | - | - | | | | | | | | | - | - | - | | - | | |
| HE01 | WESP | 6.60 | 0.05 | 41.24 | 187.55 | 50.39 | 50.39 | 50.39 | 50.39 | 35,669.62 | | | 237.95 | 5.99 | 0.05 | 37.41 | 170.15 | 91.43 | 45.72 | 45.72 | 45.72 | 32,358.97 | | | 215.86 |
| CE01 | De-dusting Baghouse | | | | | 0.94 | 0.94 | 3.24 | 0.94 | | | | 3.24 | | | - | | 0.85 | 0.85 | 2.94 | 0.85 | | - | | 2.94 |
| CE02 | Vacuum Cleaning Baghouse | | E = 1 | - | | 1.85 | 1.85 | 0.93 | 0.93 | - | | | 0.93 | | | - | | 1.68 | 1.68 | 0.84 | 0.84 | - | | | 0.84 |
| P_MARK | Product Marking | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | - | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | | 0.00 | 0.00 |
| CM10 | Recycle Plant Building Vent 1 | | <u> </u> | | | 2.90 | 2.90 | 2.90 | 1.45 | | | | - | | | | - | 2.63 | 2.63 | 2.63 | 1.31 | | | | |
| CM11 | Recycle Plant Building Vent 2 | - | | - | - | 2.90 | 2.90 | 2.90 | 1.45 | - | | | | | | | - | 2.63 | 2.63 | 2.63 | 1.31 | | | | |
| CM08 | Recycle Plant Building Vent 3 | | 0 | - | | 0.24 | 0.24 | 0.24 | 0.12 | | | | | | | | - | 0.22 | 0.22 | 0.22 | 0.11 | | | | |
| CM09 | Recycle Plant Building Vent 4 | - | | - | | 0.24 | 0.24 | 0.24 | 0.12 | - | | - | - | | - | - | - | 0.22 | 0.22 | 0.22 | 0.11 | | - | | - |
| RMS | Raw Material Outdoor Stockpile | | S = 1 | - | | 0.20 | 0.20 | 0.10 | 1.48E-02 | | - | | | | - | - | | 0.18 | 0.18 | 0.09 | 1.35E-02 | | - | | |
| IMF14 | Raw Material Reject Stockpile | - | I | - | | 1.81E-03 | 1.81E-03 | 8.51E-04 | 1.36E-04 | | - | | | | - | | - | 1.64E-03 | 1.64E-03 | 7.72E-04 | 1.23E-04 | - | - | - | |
| B170 | Melting Furnace Portable Crusher & Storage | | - | | | 1 0.59 | 0.59 | 0.27 | 0.06 | | - | | - | | | | | 0.53 | 0.53 | 0.25 | 0.05 | | | | 4 |
| Rockfon Line | | _ | | | - | | - | - | _ | | _ | - | _ | | _ | | _ | _ | | _ | - | | | - | |
| RFNE1 | IR Zone | _ | | | | - | l | | | | | | | | | | | | | | | | | | |
| RFNE2 | Hot Press and Cure | - | a | | - | 1 Dr | | | | | | | | | | | - | | | | | | | 1.0 | - |
| RFNE3 | High Oven A | _ | | | - | | | | | | | | | | | | | | | | | _ | | | |
| RFNE9 | High Oven B | | | | - | | | | | | | | | | | | - | | | | | _ | | | |
| RFNE4 RENE6 | Drying Oven 1 | | | 5 | | | | | 1.0 | | | | | | | | L | 1 | 1 | 1 | | | | | <u></u> |
| RENE5 | Drying Oven 2 & 3 Spray Paint Cabin | - | | C | | - | | | | | | | | | | · | · | | | | | | | | + |
| RENES RENE7 | Cooling Zone | - | 8 i | 0 | | | | | | | | | <u> </u> | | | | · | | | | | <u> </u> | | | <u>+</u> |
| RENE8 | De-dusting Baghouse | _ | - | _ | - | | | | | | | | | | - | | | 1 | | | | | - | - | |
| | -wide Sources | - | - | | | | | | 1 | <u> </u> | - | <u> </u> | | | | | | | | | | <u> </u> | | <u> </u> | <u></u> |
| | | | | | | 1 | | | | | _ | | | | | | | | | | | | _ | | |
| CM03 | Natural Gas Boiler 1 | 0.77 | 0.01 | 1.79 | 0.12 | 0.16 | 0.04 | 0.16 | 0.16 | 2,559.32 | and and | 1.07E-05 | 0.04 | 0.70 | 0.01 | 1.62 | 0.11 | 0.15 | 0.04 | 0.15 | 0.15 | 2,321.77 | - | 9.66E-06 | 0.04 |
| CM04 | Natural Gas Boiler 2 | 0.77 | 0.01 | 1.79 | 0.12 | 0.16 | 0.04 | 0.16 | 0.16 | 2,559.32 | | 1.07E-05 | 0.04 | 0.70 | 0.01 | 1.62 | 0.11 | 0.15 | 0.04 | 0.15 | 0.15 | 2,321.77 | | 9.66E-06 | 0.04 |
| RFN10 | RFN Building Heat | | | | | | | | | | | | | | | | | | | | | | | 1 | |
| EFP1 | Emergency Fire Pump Engine | 0.45 | 8.61E-04 | 0.10 | 0.01 | 0.02 | 0.01 | 0.02 | 0.02 | 90.50 | | | 2.14E-03 | 0.40 | 7.81E-04 | 0.09 | 0.01 | 0.02 | 0.01 | 0.02 | 0.02 | 82.10 | - | - | 1.95E-03 |
| Rd_RM | Raw Material Paved Haul Roads | | | | | 2.69 | 2.69 | 0.54 | 0.13 | | | 1 | | - | | | 1 | 2.44 | 2.44 | 0.49 | 0.12 | | - | | |
| Rd_FP | Finished Product Paved Haul Road | - | | - | | 0.07 | 0.07 | 0.01 | 0.00 | | - | 10000 | - | | - | - | | 0.06 | 0.06 | 0.01 | 0.00 | | - | | |
| Tanks | Facility Storage Tanks | | | | 0.12 | - | | | | - | - | - | 0.11 | | | - | 0.11 | | - | | | | | - | 0.10 |

Roxul USA Inc. dba ROCKWOOL Ranson, West Virginia Summary of Facility Emissions

| | | | | | | | | | U | s | | | | | | | | | | | | | | | MET | RIC | | | | | | | |
|-----------------------|--|----------|----------|----------|--------------|-----------|----------|----------|----------|------------------|----------|----------|----------|--------------|----------|----------|----------|------------|------------|------------|--------------|------------|------------|------------|------------|------------------|------------|------------|------------|--------------|------------|------------|------------|
| Source ID | Source Description | HF | HCI | COS | Formaldehyde | e Arsenic | Lead | Mercury | Phenol | Mineral Fiber | Methanol | Hexane | Benzene | Acetaldehyde | Toluene | Xylene | PAH | HF | HCI | COS | Formaldehyde | Arsenic | Lead | Mercury | Phenol | Mineral Fiber | Methanol | Hexane | Benzene | Acetaldehyde | Toluene | Xylene | PAH |
| | | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) |
| Minwool Line | 9 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| B210/B211 | Raw Material Storage (B210) | | | | | | | | | - | | | | - | | | | | | | | | | | | | | | | - | | | - |
| B215 | Raw Material Loading Hopper (B215) | - | | | | | - | | - | - | | - | | - | - | | | | - | | - | | | | - | - | 1 | | | - | | | |
| | Conveyor Transition Point (B215 to B220) | | | | | | | | - | - | | | | - | | - | | | | | | | | | | | - | | | - | | | |
| | B220 Material Handling | | | | | | | | - | - | | | | - | | - | | | | | | | | | - | - | - | | | - | | | |
| | Conveyor Transfer Point (B215) | | | | | | | | - | - | | | | - | | - | | | | | | | | | - | - | - | | | - | | | |
| IMF16 | Conveyor Transfer Point (B300) | | | | | | | | | - | | | | - | | - | | | | | | | | | | | - | | | - | | | |
| IMF15 | Outside B220 Transfer Points | | | | | | | | | - | | | | - | | | | | | | | | | | | | - | | | - | | | |
| RM REJ | Raw Material Reject Collection Drop | | | | | | | | | | | | | | | - | | | | | | | | | | | - | | | - | | | |
| IMF21 | Charging Building Vacuum Cleaning Filter | | | | | | | | - | - | | | | - | | - | | | | | | | | | | | - | | | - | | | |
| IMF24 | Pre-heat Burner | | | | | | 1.05E-05 | | - | - | | 0.04 | | - | | - | | | | | | | 9.51E-06 | | | - | - | 0.03 | | - | | | |
| IMF01 | Melting Furnace | 1.55 | 1.24 | 1.57 | 0.02 | 3.77E-04 | 1.57E-04 | 2.45E-03 | 0.31 | 9.73 | | | | - | | - | | 1.41 | 1.12 | 1.42 | 0.01 | 3.42E-04 | 1.42E-04 | 2.22E-03 | 0.28 | 8.83 | - | | | - | | | |
| IMF07 | One (1) Storage Silo (Filter Fines Day) | | | | | | - | 2.402.00 | - | - | | | | - | - | - | | | | | | | | | | - | - | | | - | | | |
| IMF10 | Filter Fines Recieving Silo | - | | | | | - | - | - | - | | | | - | - | - | | | | | - | | | | - | - | - | | | - | - | | |
| IMF08 | Sorbent Silo | | | | | | - | - | - | - | | | | - | | - | | | - | | - | | - | | - | - | - | | | - | | | |
| IMF09 | Spent Sorbent Silo | - | | | | | - | | - | - | | | | - | - | - | | | - | | - | | - | | - | - | - | | | - | | | |
| DI | Dry Ice Cleaning | | | | | | - | | - | - | | | | - | - | - | | | - | | | | - | | - | - | - | | | - | | | |
| CM12 | Fleece Application Vent 1 | | | | 0.70 | | - | | 0.10 | | 0.07 | | | | | | | | | | 0.50 | | | | 0.00 | | 0.04 | | | | | <u> </u> | + |
| CM13 | Fleece Application Vent 2 | | | | 2.78 | | - | | 3.40 | - | 0.67 | - | | - | - | - | | | | | 2.52 | | | | 3.08 | - | 0.61 | | | - | - | | |
| HE01 | WESP | | | | 13.74 | | - | | 71.61 | 50.39 | 102.21 | | | - | | - | | | | | 12.46 | | | | 64.96 | 45.72 | 92.72 | | | - | | | - |
| CE01 | De-dusting Baghouse | | | | 13.74 | | - | | - | 3.24 | | | | - | - | - | | | | | 12.40 | | | | | 2.94 | | | | - | | | |
| CE01 CE02 | | | | | | | - | - | | 0.93 | | | | - | | - | | | | | | | | | | 0.84 | - | | | - | | | |
| | Product Marking | | | | | | 0.00 | - | | 0.95 | | 0.00 | | - | - | - | | | - | | - | | 0.00 | | - | 0.84 | - | 0.00 | | | - | | |
| CM10 | Recycle Plant Building Vent 1 | | | | | | 0.00 | | | - | | 0.00 | | - | | - | | | | | | | 0.00 | | - | - | - | 0.00 | | | - | | |
| | Recycle Plant Building Vent 1 | - | | | | | - | | - | - | | | | - | - | - | | | - | | | | - | | - | - | - | | | - | - | | |
| CM08 | Recycle Plant Building Vent 2 | - | | | | | - | - | - | - | | | | - | - | - | | | - | | | | - | | - | - | - | | | - | - | | |
| CM09 | Recycle Plant Building Vent 3 | | | | | | - | - | - | - | | | | - | - | - | | | - | - | - | | - | | - | - | - | | | - | - | | - |
| RMS | Raw Material Outdoor Stockpile | | | | | | - | - | - | - | | - | | - | - | - | | | | | | | | | - | - | - | | | - | | | |
| IME14 | Raw Material Reject Stockpile | | | | | | | | | - | | | | | | | | | | | | | | | | | | | | | | | |
| B170 | Melting Euroace Portable Crusher & Storage | | | | | | - | - | - | - | | | | - | - | - | | | | | | | | | | - | - | | | - | | | |
| | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Rockfon Line RFNE1 | | | | | | | - | | | | | | | | | | - | | | | | | | | - | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | 4 | | 4 |
| | Hot Press and Cure High Oven A | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | + | +' | 4 |
| | | | | | | | - | | | | | | | | | | | | | | | | | | | | | | | | + | +' | + |
| RENES | High Oven B | | | - | | - | - | | | | | | | | | | | | | | | | - | | | | | | | | + | | + |
| | Drying Oven 1 Drying Oven 2 & 3 | _ | | - | | - | - | | | | | | | | | | | | | | | | - | | | | | | | | + | +' | + |
| | Drying Oven 2 & 3 Spray Paint Cabin | | | - | | | | | | | | | | | - | | | | | | | | | | | | | | | | + | | + |
| | | _ | | | | | _ | | | | | | | | | | | | | | | | | | | | | | | | | ' | |
| | Cooling Zone | | | | | | _ | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | De-dusting Baghouse | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| | y-wide Sources | | | | | | | | | | | | | | | | | | | | | | | | | | | | - | | | | _ |
| | Natural Gas Boiler 1 | - | | | | | 1.07E-05 | - | - | - | | 0.04 | | - | | - | | | | | - | | 9.66E-06 | | - | - | - | 0.03 | | - | | | |
| CM04 | Natural Gas Boiler 2 | - | | | | | 1.07E-05 | | | - | | 0.04 | | - | | - | | | | | - | | 9.66E-06 | | - | - | - | 0.03 | | - | | | |
| | RFN Building Heat | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| EFP1 | Emergency Fire Pump Engine | | | | 6.53E-04 | | - | - | - | - | | - | 5.17E-04 | 4.25E-04 | 2.26E-04 | 1.58E-04 | 9.30E-05 | | | | 5.93E-04 | | - | | - | - | - | | 4.69E-04 | 3.85E-04 | 2.05E-04 | 1.43E-04 | 8.44E-05 |
| | Raw Material Paved Haul Roads | | | | | | | | | - | | | | - | | - | | | | | - | | | | - | - | - | | | - | | | |
| Rd FP | Finished Product Paved Haul Road | - | | | | | - | | | | | | | - | | - | | | | | | | | | | - | - | | | | | | |
| Tanks | Facility Storage Tanks | - | | | 0.11 | | - | - | | - | 9.30E-04 | | | - | - | - | - | | | | 0.10 | | | | - | - | 8.44E-04 | | | | | | |
| | Total | 1.55 | 1.24 | 1.57 | 16.64 | | 1.89E-04 | | 75.32 | 64.29 | 102.88 | 0.11 | | 4.25E-04 | | | 9.30E-05 | 1.41 | 1.12 | 1.42 | 15.10 | | 1.71E-04 | | 68.33 | 58.32 | 93.33 | | | | 2.05E-04 | | 8.44E-05 |

| Roxul USA Inc. dba ROCKWOOL | Modified u |
|---|------------|
| Ranson, West Virginia | New units |
| Source ID: Mineral Wool Line (L1) Emissions | Removed |



| | | | | | | METR | RIC | US | 1 | | | | |
|----------------|------------------------------|-----------------------|----------|----------------------|---------|---------------------|---------------------|---------------------|---------------------|---------------------------------------|---------------------------|--------------------|--------------------------|
| Stack ID(s) | Source Description | Concer | ntration | ration Flow Rate | | Hourly Emissions | Annual Emissions | Hourly Emissions | Annual Emissions | Modele | d Emission Rate | Notes | Control Device |
| - | Pollutants | (mg/Nm ³) | (gr/scf) | (Nm ³ /h) | (scfm) | (kg/hr) | (tonne/yr) | (lb/hr) | (ton/year) | (g/s) | Averaging Period | | |
| 1 | Melting Furnace | | | | | | | | | | | | |
| | Filterable PM | 31 | 0.001 | 33,900 | 21,414 | 1.05 | 8.83 | 2.32 | 9.73 | | - | Note 2 (2) | Baghouse |
| | Total PM ₁₀ | 31 | 0.001 | 33,900 | 21,414 | 1.05 | 8.83 | 2.32 | 9.73 | 2.92E-01 | 24-hr, Annual | Note 2 (2) | Baghouse |
| | Total PM _{2.5} | 31 | 0.001 | 33,900 | 21,414 | 1.05 | 8.83 | 2.32 | 9.73 | 2.92E-01 | 24-hr, Annual | Note 2 (2) | Baghouse |
| | NOx | 500 | - | 33,900 | 21,414 | 16.95 | 142.38 | 37.37 | 156.95 | 4.71E+00 | 1-hr (base), Annual | Note 2 (6) | SNCR and Oxy-fuel burner |
| | СО | 150 | - | 33,900 | 21,414 | 1.46 | 12.23 | 3.21 | 13.48 | 4.05E-01 | 1-hr (base), 8-hr | Note 2 (6) | - |
| | SO ₂ | 450 | - | 33,900 | 21,414 | 15.26 | 128.14 | 33.63 | 141.25 | 4.24E+00 | 1-hr (base), 3-hr, 24-hr, | Note 2 (1) | Sorbent Injection System |
| | Total VOC | | | 33,900 | 21,414 | 0.14 | 1.17 | 0.31 | | | Annual - | Note 2 (1) | |
| | HF | 4.9 | | 33,900 | 21,414 | 0.14 | 1.41 | 0.37 | | _ | | Note 2 (1) | Sorbent Injection System |
| | HCI | 3.9 | | 33,900 | 21,414 | 0.17 | 1.12 | 0.37 | | _ | | Note 2 (2) | Sorbent Injection System |
| | COS | 5.5 | | 33,900 | 21,414 | 0.13 | 1.12 | 0.23 | | | | Note 2 (2) | - |
| | Formaldehyde | 0.05 | | 33,900 | 21,414 | 1.70E-03 | 0.01 | 3.74E-03 | | <u> </u> | | Note 2 (1) | |
| | H_2SO_4 Mist | 50 | | 33,900 | 21,414 | 0.85 | 7.12 | 1.87 | | _ | | Note 2 (1) | Sorbent Injection System |
| | Fluorides | 0.1 | | 33,900 | 21,414 | 3.39E-03 | 0.03 | 0.01 | | | | Note 2 (1) | Baghouse |
| | Arsenic | 0.0012 | _ | 33,900 | 21,414 | 4.07E-05 | 3.42E-04 | 8.97E-05 | | _ | _ | Note 2 (5) | Baghouse |
| | Lead | 0.0012 | | 33,900 | 21,414 | 1.70E-05 | 1.42E-04 | 3.74E-05 | | - | | Note 2 (5) | Baghouse |
| | Mercury | 0.0078 | | 33,900 | 21,414 | 2.64E-04 | 2.22E-03 | 5.83E-04 | | - | | Note 2 (5) | Baghouse |
| | Phenol | 1 | | 33,900 | 21,414 | 0.03 | 0.28 | 0.07 | - | | | Note 2 (5) | - |
| | Mineral Fiber | _ | | 33,900 | 21,414 | 1.05 | 8.83 | 2.32 | | - | _ | Note 2 (2), Note 3 | Baghouse |
| | | | | | | | | | | | | | |
| | Total HAPs | - | | 33,900 | 21,414 | 1.56 | 13.08 | 3.43 | 14.42 | - | · · · · · · · · | | Sorbent Injection System |
| | CO ₂ | 245,343 | - | 33,900 | 21,414 | 8,317.14 | 69,863.99 | 18,336.14 | 77,011.77 | | | Note 2 (6) | - |
| | CH ₄ | 4 | | 33,900 | 21,414 | 0.13 | 1.08 | 0.28 | 1.19 | · · · · · · · · · · · · · · · · · · · | - II | Note 2 (3) | - |
| | N ₂ O | 0 | - | 33,900 | 21,414 | 0.01 | 0.11 | 0.03 | 0.12 | - | - | Note 2 (3) | - |
| | CO ₂ e | - | - | 33,900 | 21,414 | 8,324.18 | 69,923.13 | 18,351.66 | 77,076.96 | - | - | - | - |
| 1 | WESP | | | | | | | | | _ | | | |
| | Filterable PM | - | _ | 585,000 | 369,529 | 5.44 | 45.72 | 12.00 | 50.39 | - | - | Note 2 (1) | WESP |
| | Total PM ₁₀ | - | - | 585,000 | 369,529 | 5.44 | 45.72 | 12.00 | | 1.51E+00 | 24-hr, Annual | Note 2 (1) | WESP |
| | Total PM _{2.5} | - | - | 585,000 | 369,529 | 5.44 | 45.72 | 12.00 | 50.39 | 1.51E+00 | 24-hr, Annual | Note 2 (1) | WESP |
| | NOx | - | - | 585,000 | 369,529 | 0.59 | 5.99 | 1.57 | 6.60 | 1.98E-01 | 1-hr, Annual | Note 2 (1) | - |
| | со | - | - | 585,000 | 369,529 | 4.45 | 37.41 | 9.82 | 41.24 | 1.24E+00 | 1-hr, 8-hr | Note 2 (1) | - |
| | SO ₂ | 1 | | E85 000 | 260 520 | 0.01 | 0.05 | 0.01 | 0.05 | 1 595 02 | 1 br 2 br 24 br Appual | 1 | |
| | 302 | - | - | 585,000 | 369,529 | 0.01 | 0.05 | 0.01 | 0.05 | 1.58E-03 | 1-hr, 3-hr, 24-hr, Annual | - | - |
| | VOC | - | - | 585,000 | 369,529 | 20.26 | 170.15 | 44.66 | 187.55 | - | - | Note 2 (1) | - |
| | Phenol | - | - | 585,000 | 369,529 | 7.73 | 64.96 | 17.05 | 71.61 | - | - | Note 2 (1) | - |
| | Formaldehyde | - | | 585,000 | 369,529 | 1.48 | 12.46 | 3.27 | 13.74 | | | Note 2 (1) | |
| | Methanol | - | | 585,000 | 369,529 | 11.04 | 92.72 | 24.34 | 102.21 | - | | Note 2 (1) | - |
| | Mineral Fiber | - | | 585,000 | 369,529 | 5.44 | 45.72 | 12.00 | | - | - | Note 2 (1), Note 3 | WESP |
| | Total HAPs | - | | 585,000 | 369,529 | 25.70 | 215.86 | 56.65 | | - | | - | - |
| | CO ₂ | - | - | 585,000 | 369,529 | 1139.28 | 9,569.97 | 2,511.68 | | - | - | | - |
| | CH₄ | | | 585,000 | 369,529 | 0.02 | 0.18 | 0.05 | | - | - | - | - |
| | N ₂ O | - | - | 585,000 | 369,529 | 9.10 | 76.46 | 20.07 | | - | - | - | - |
| | CO ₂ e | - | _ | 585,000 | 369,529 | 3,852.26 | 32,358.97 | 8,492.77 | 35,669.62 | · · · | | - | - |
| 1 | De-dusting Baghouse | | | | | | | | | | | | |
| | Filterable PM | 10 | 0.0006 | 70,000 | 44,217 | 0.10 | 0.85 | 0.21 | 0.94 | - | - | Note 1 | Baghouse |
| | Filterable PM ₁₀ | 5 | 0.0020 | 70,000 | 44,217 | 0.35 | 2.94 | 0.77 | 3.24 | 9.72E-02 | 24-hr, Annual | Note 2 (5) | Baghouse |
| | Filterable PM _{2.5} | 5 | 0.0006 | 70,000 | 44,217 | 0.10 | 0.85 | 0.21 | 0.94 | 2.69E-02 | 24-hr, Annual | Note 2 (5) | Baghouse |
| | Mineral Fiber | - | _ | 70,000 | 44,217 | 0.35 | 2.94 | 0.77 | 3.24 | - | | Note 3 | Baghouse |
| | Total HAPs | | | 70,000 | 44,217 | 0.35 | 2.94 | 0.77 | 3.24 | - | - | - | - |
| 2 | Vacuum Cleaning Baghouse | | | | | | | | | | | | |
| _ | Filterable PM | 10 | 0.0041 | 20,000 | 12,633 | 0.20 | 1.68 | 0.44 | 1.85 | - | - 1 | Note 1 | Baghouse |
| | Filterable PM ₁₀ | 5 | 0.0020 | 20,000 | 12,633 | 0.10 | 0.84 | 0.22 | | 2.78E-02 | 24-hr, Annual | Note 2 (5) | Baghouse |
| | Filterable PM _{2.5} | 5 | 0.0020 | 20,000 | 12,633 | 0.10 | 0.84 | 0.22 | | 2.78E-02 | 24-hr, Annual | Note 2 (5) | Baghouse |
| | Mineral Fiber | - | - | 20,000 | 12,633 | 0.10 | 0.84 | 0.22 | | - | | Note 3 | Baghouse |
| | | | | | | | | | | | | | |

Notes:

1. Where data was not available, speciations of PM were conservatively estimated in accordance with the below: Filterable PM was conservatively assumed to be equal to Total PM10. For CE01 and CE02, Filterable PM assumed double Filterable PM10. For clarity,

Total PM_{10} = Filterable PM_{10} + Condensable PM.

Total $PM_{2.5}$ = Filterable $PM_{2.5}$ + Condensable PM

Filterable PM = Total PM_{10} , with the exception of CE01 and CE02, where Filterable PM = 2X Filterable PM_{10}

Total PM = Filterable PM + CPM (where CPM = Total $PM_{2.5}$)

2. Calculation Method References:

1 - Stack testing from RAN Compliance Test with engineering assumptions applied.

2 - MACT Limit (40 CFR 63 Subpart DDD) emission limit. Note emission limits for formaldehyde, methanol, and phenol combined for spinning (collection) and curing.

3 - EPA Emission Factor

4 - Assumed 10% of the mass emissions of the Curing Oven for Cooling.

5 - Based upon testing from other Rockwool operations.

6 - Limits have been evaluated against data analysis of CEMS performance.

3. Mineral Fiber emissions were conservatively assumed equal to Filterable PM emissions for sources that may contain rock wool fibers.

The listed HAP, fine mineral fibers, includes mineral fiber emissions from facilities manufacturing or processing glass, rock, or slag fibers (or other mineral derived fibers) of average diameter 1 micrometer or less.

Sample Calculations:

Hourly Emissions (kg/hr) = Fan Flow Rate (Nm³/hr) * Exhaust Concentration (mg/Nm³) * 1,000,000 (mg/kg) Hourly Emission Rate Filterable PM = Concentration PM (gr/scf) * (1 lb/7,000 grains) * Flow Rate (scfm) * (60 min/hr) Annual Emissions (ton/yr) = Hourly Emission Rate (lb/hr) * 8,400 (hr/yr) / 2,000 (lb/ton) Annual Emissions (tonne/yr) = Hourly Emissions (kg/hr) * 8,400 (hr/yr) / 1,000 (kg/tonne) CO_2 Equivalent (CO_{2e}) = $CO2 + [GWP_{CH4} * CH_4)$] + [$GWP_{N2O} * N_2O$]

Roxul USA Inc. dba ROCKWOOL Ranson. West Virginia Material Handling Fugitives

Raw Material

Melting Furnace Diverted Melt

Modified units New units Removed units



| | k - Particle | E | Emission Fac | ctor ³ | | | |
|-------------------|--------------|------------------------|------------------------|-------------------|--|--|--|
| Pollutant | Size | Rock/Slag/ Minerals | Reject Raw Material | Diverted Melt | | | |
| | manaphen | (lb/ton) | (lb/ton) | (lb/ton) | | | |
| PM | 0.74 | 2.19E-03 | 2.19E-03 | 2.19E-03 | | | |
| PM ₁₀ | 0.35 | 1.04E-03 | 1.04E-03 | 1.04E-03 | | | |
| PM _{2.5} | 0.053 | 1.57E-04 | 1.57E-04 | 1.57E-04 | | | |

| Location | U - Wind | Speed ² |
|----------|----------|--------------------|
| | (mph) | m/s |
| door | 6.51 | 2.91 |

Out

Notes:

1. Moisture content chosen as worst case among various materials handled.

M-Moisture Conte

2.7

27

2.7

2. Outdoor wind speed was set at 6.51 mph based on 2011-2015 average wind speed data from station ID 13734.

3. Material drops emission factor equation per AP-42 Section 13.2.4.

Sample Calculations:

Rock/Slag/Minerals Reject Raw Material

E (lb/ton) = k (0.0032) [(U/5)^1.3] / [(M/2)^1.4], where

k = Particle Size Multiplier,

U = wind speed, (meters per second [m/s]), (miles per hour [mph]),

M = material moisture content (%)

1 Material Delivery and Front-end Loader Fugitive Emissions³

| | | | MET | RIC | U | S | | | | | MET | RIC | | | L | JS | |
|-----------|----------------------------------|--|-------------|--------------|-----------|------------|---------------------|-------------------------|-------------------|-------------|--------------|-------------|--------------|-----------|------------|-----------|------------|
| - | - | | Loading | Loading | Loading | Loading | Enclosure | Control | | UNCONTR | ROLLED | CONTI | ROLLED | UNCON | FROLLED | CONTR | ROLLED |
| Source ID | Raw Material | Source Description | Rate | Rate | Rate | Rate | Description | Efficiency ² | Pollutant | Emiss | | | ssions | | sions | | sions |
| | | | (tonne/day) | (tonne/year) | (ton/day) | (ton/year) | | (%) | | (tonne/day) | (tonne/year) | (tonne/day) | (tonne/year) | (ton/day) | (ton/year) | (ton/day) | (ton/year) |
| | | Raw Material Stockpile - | | 100.150 | 201 | 005 100 | | | PM | 7.56E-04 | 0.20 | 3.78E-04 | 0.10 | 8.34E-04 | 0.22 | 4.17E-04 | 0.11 |
| RMS | Rock/Slag/Minerals | Delivery to Stockpile [from | 690 | 186,150 | 761 | 205,193 | 3-sided | 50% | PM10 | 3.58E-04 | 0.10 | 1.79E-04 | 4.83E-02 | 3.94E-04 | 0.11 | 1.97E-04 | 5.32E-02 |
| | 14 | offsite (by truck)] | | | | | | | PM _{2.5} | 5.42E-05 | 1.46E-02 | 2.71E-05 | 7.31E-03 | 5.97E-05 | 1.61E-02 | 2.99E-05 | 8.05E-03 |
| | | Raw Material Storage - | | | | | | | PM | 7.13E-04 | 0.20 | 7.13E-04 | 0.20 | 7.85E-04 | 0.22 | 7.85E-04 | 0.22 |
| | Rock/Slag/Minerals | Delivery to 210 [from offsite (by truck) or from | 650 | 186,150 | 716 | 205,193 | none | 0% | PM ₁₀ | 3.37E-04 | 0.10 | 3.37E-04 | 0.10 | 3.71E-04 | 0.11 | 3.71E-04 | 0.11 |
| | | stockpile (by FEL)] | | | | | | | PM _{2.5} | 5.10E-05 | 0.01 | 5.10E-05 | 0.01 | 5.63E-05 | 0.02 | 5.63E-05 | 0.02 |
| | - | Raw Material Storage - | | | | | | | PM | 7.13E-04 | 0.20 | 1.78E-04 | 0.05 | 7.85E-04 | 0.22 | 1.96E-04 | 0.06 |
| B210/B211 | Rock/Slag/Minerals | Delivery into 210 | 650 | 186,150 | 716 | 205,193 | 3-sided w/ cover | 75% | PM ₁₀ | 3.37E-04 | 0.10 | 8.42E-05 | 0.02 | 3.71E-04 | 0.11 | 9.29E-05 | 0.03 |
| | | enclosure | | | | | cover | | PM _{2.5} | 5.10E-05 | 0.01 | 1.28E-05 | 3.65E-03 | 5.63E-05 | 0.02 | 1.41E-05 | 4.03E-03 |
| | 7 | | | | | | | | PM | 1.43E-03 | 0.41 | 8.91E-04 | 0.26 | 1.57E-03 | 0.45 | 9.82E-04 | 0.28 |
| | | | | Total | | | | | PM ₁₀ | 6.74E-04 | 0.19 | 4.21E-04 | 0.12 | 7.43E-04 | 0.21 | 4.64E-04 | 0.13 |
| | | | | | | | | | PM _{2.5} | 1.02E-04 | 0.03 | 6.38E-05 | 0.02 | 1.13E-04 | 0.03 | 7.03E-05 | 0.02 |
| | 1 | Raw Material Loading | | | | | 3-sided w/ | _ | PM | 5.59E-04 | 0.20 | 1.40E-04 | 0.05 | 6.16E-04 | 0.22 | 1.54E-04 | 5.62E-02 |
| B215 | Rock/Slag/Minerals | Hopper | 510 | 186,150 | 562 | 205,193 | cover | 75% | PM ₁₀ | 2.64E-04 | 0.10 | 6.61E-05 | 0.02 | 2.91E-04 | 0.11 | 7.29E-05 | 2.66E-02 |
| | | Topper | | | | | 00701 | | PM _{2.5} | 4.00E-05 | 0.01 | 1.00E-05 | 3.65E-03 | 4.41E-05 | 0.02 | 1.10E-05 | 4.03E-03 |
| | | Raw Material Reject | | | | | 4-sided rubber | | PM | 5.48E-06 | 4.08E-03 | 1.37E-06 | 1.02E-03 | 6.04E-06 | 4.50E-03 | 1.51E-06 | 1.12E-03 |
| RM_REJ | Reject Raw Material | Collection Drop | 5 | 3,723 | 6 | 4,104 | drop guards | 75% | PM ₁₀ | 2.59E-06 | 1.93E-03 | 6.48E-07 | 4.83E-04 | 2.86E-06 | 2.13E-03 | 7.14E-07 | 5.32E-04 |
| | | | | | | | diop guards | | PM _{2.5} | 3.93E-07 | 2.92E-04 | 9.81E-08 | 7.31E-05 | 4.33E-07 | 3.22E-04 | 1.08E-07 | 8.05E-05 |
| | Malting Frances | Melting Furnace Portable | | | | | | | PM | 1.79E-03 | 0.08 | 8.95E-04 | 0.04 | 1.97E-03 | 0.09 | 9.87E-04 | 0.04 |
| B170 | Melting Furnace Diverted Melt | Crusher & Storage - Drop to Pit Waste (170) (from | 1,633 | 73,467 | 1,800 | 81,000 | 3-sided | 50% | PM ₁₀ | 8.47E-04 | 0.04 | 4.23E-04 | 0.02 | 9.33E-04 | 0.04 | 4.67E-04 | 0.02 |
| | Directed Weit | portable crusher) | | | | | | | PM _{2.5} | 1.28E-04 | 5.77E-03 | 6.41E-05 | 2.88E-03 | 1.41E-04 | 6.36E-03 | 7.07E-05 | 3.18E-03 |

Notes:

FEL = Front End Loader

ton = short tons

tonne = metric tons

1. Loading rate for material storage operations is based on the maximum quantity delivered per day or per year. 2. Assumed a control efficiency of 50% due to offloading locations having 3-sided concrete enclosures and 75% efficiency for 4-sided enclosures (hopper) or 3-sided enclosures with roof. Per Application Instructions and Forms for General Permit G40-C by West Virginia Department of Environmental Protection, Telescopic Chutes have a control efficiency of 75% and Full Enclosures have an 80% control efficiency.

3. Large rocks are delivered to the pit waste area by FEL (before crushing), therefore the emissions from this drop are negligible due to size.

4. Modeled emission rates in gray are not modeled individually, but are added as a total source emission rate.

5. For Q/d screening tool, the annual steady-state-equivalent emission rate (Q) was determined based on maximum daily emissions. For example QPM10 (tpy) = PM10 (ton/day) * 365 (day/yr).

Sample Calculations:

Uncontrolled Emissions (ton/day; ton/year) = E (lb/ton) * Loading Rate (ton/day; ton/year) / 2000 (lb/ton)

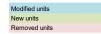
Controlled Emissions = Uncontrolled Emissions (ton/day; ton/year) * (1 - Control Efficiency (%))

Uncontrolled/Controlled Emissions (tonne/day; tonne/year) = Uncontrolled/Controlled Emissions (ton/day; ton/year) * 0.9071847 tonne/ton

Modeled 24-hr Emission Rate (g/s) = Daily Emissions (ton/day) / 24 (hr/day) [for 24-hr model averaging period] * 2,000 (lb/ton) * 453.59 (g/lb) / 3,600 (sec/hr)

Modeled Annual Emission Rate (g/s) = Annual Emissions (ton/yr) / 8,760 (hr/yr) [for annual model averaging period] * 2,000 (lb/ton) * 453.59 (g/lb) / 3,600 (sec/hr)

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2 Crusher Fugitive Emissions

| | | | Emission | ME | TRIC | | JS | Hou | urs of | METR | METRIC US | | US |
|------------|--|--------------------------------|---------------------|------------|------------|----------|-----------|-----------|----------|---------|------------|---------|----------|
| Source ID | Source ID Source Description Pollutant | | Factor ² | | Process | ing Rate | Operation | | ration | Hourly | Annual | Hourly | Annual |
| - Hereiter | | | (lb/ton) | (tonne/hr) | (tonne/yr) | (ton/hr) | (ton/yr) | (hrs/day) | (hrs/yr) | (kg/hr) | (tonne/yr) | (lb/hr) | (ton/yr) |
| | Melting Furnace | PM | 0.0054 | | | | | | | 0.37 | 0.20 | 0.81 | 0.22 |
| B170 | Diverted Melt Portable | PM ₁₀ | 0.0024 | 136.1 | 73,467 | 150.0 | 81,000 | 12 | 540 | 0.16 | 0.09 | 0.36 | 0.10 |
| | Crusher | PM _{2.5} ¹ | 0.0008 | | | | | | | 0.05 | 0.03 | 0.12 | 0.03 |

Notes:

1. PM2.5 is 15% of PM per AP-42 Appendix B, Table B.2.2 for material handling and processing of aggregate and unprocessed ore.

2. Emission factor for crushing of melting furnace diverted melt assumed to be similar to crushing of stones in AP-42 Table 11.19.2-2.

Uncontrolled PM emission factor of 0.0054 lb/ton and Uncontrolled PM in emission factor of 0.0024 lb/ton for tertiary crushing were conservatively used due to lack of emission factors for primary or secondary crushing.

Sample Calculations:

Hourly Emissions (lb/hr) = Emission Factor (lb/ton) * Processing Rate (ton/hr)

Annual Emissions (ton/yr) = Hourly Emissions (lb/hr) * Hours of Operation (hrs/yr) / 2000 (lb/ton)

Hourly Emissions (kg/hr) = Hourly Emissions (lb/hr) * 0.4535924 kg/lb

Annual Emissions (tonne/yr) = Annual Emissions (ton/yr) * 0.9071847 tonne/ton

3 Wind Erosion Emission from Outdoor Stockpiles

| p ² | p ² # of days per year with precipitation >0.01 inch | | | |
|-----------------------|---|------|--|--|
| f ³ | % of time that unobstructed wind speed >12 mph at the mean pile height | 9.06 | | |
| Stockpile Description | S - Silt content ¹ | | | |
| | | | | |

| | Emissi | on Factor ⁴ |
|--------------------------------|---------------------------|------------------------------|
| Pollutant | Raw Material Stockpile | Pit Waste (170) Stockpile |
| | lb/day/acre | lb/day/acre |
| PM | 8.03 | 8.03 |
| PM ₁₀ | 3.77 | 3.77 |
| PM _{2.5} ⁵ | 0.60 | 0.60 |

Notes:

1. Sit content chosen as worst case among various materials in stockpile. 2. Number of days per year with precipitation greater than 0.01 inch based on Table B - Precipitation Zones in West Virginia in Application Instructions and Forms for General Permit G40-C by West Virginia Department of Environmental Protection.

3. Percentage of time that the unobstructed wind speed exceeds 12 mph at the mean pile height based on AP 42 Ch. 13.2.5.2 Equation (1) and MRBIAD Aermap processed data 2012-2016.

4. Outdoor stockpile emission factor equation per WVDAQ G40-B (Nonmetallic Mineral Processing) Calculation Workbook: Stockpiles.

5. PM_{2.5} particle size multiplier of 0.075 per AP-42 Section 13.2.5-2 for Industrial Wind Erosion.

Sample Calculations:

E (lb PM/daylacre) = 1.7 * [s/1.5] * [(365-p)/235] * [f/15] E (lb PM₁₀/daylacre) = (0.47) * 1.7 * [s/1.5] * [(365-p)/235] * [f/15] E (lb PM_{2.5}/daylacre) = (0.075) * 1.7 * [s/1.5] * [(365-p)/235] * [f/15], where

s = silt content of material

p = number of days with >0.01 inch of precipitation per year,

f = percentage of time that the unobstructed wind speed exceeds 12 mph at mean pile height

| | | | | | | | METRIC US | | | | | | | |
|-------------------------------|----------|--------------------------|-------------|-------------------------|-----------|----------|--------------|----------|--------------|----------|------------|----------|------------|--|
| Stockpile Description | Stockpil | e Base Area ² | Enclosure | Control | | UNCON | TROLLED | CONT | ROLLED | UNCONTR | OLLED | CONT | ROLLED | |
| | Max | | Description | Efficiencv ¹ | Pollutant | Emi | ssions | Emi | ssions | Emissi | ons | Emi | Emissions | |
| 1 | sq. m | acre | | (%) | | (kg/hr) | (tonne/year) | (kg/hr) | (tonne/year) | (lb/hr) | (ton/year) | (lb/hr) | (ton/year) | |
| | | | | | PM | 0.02 | 0.16 | 0.01 | 0.08 | 0.04 | 0.18 | 0.02 | 0.09 | |
| Raw Material Stockpile (RMS) | 500 | 0.12 | 3-sided | 50% | PM10 | 0.01 | 0.08 | 4.40E-03 | 0.04 | 0.02 | 0.09 | 0.010 | 0.04 | |
| | | | | 1000 B | PM2.5 | 1.41E-03 | 0.01 | 7.03E-04 | 0.01 | 0.0031 | 0.014 | 0.002 | 0.01 | |
| Melting Furnace Portable | | | | | PM | 0.07 | 0.59 | 0.03 | 0.30 | 0.15 | 0.65 | 0.07 | 0.33 | |
| Crusher & Storage - Pit Waste | 1800 | 0.44 | 3-sided | 50% | PM10 | 0.03 | 0.28 | 0.02 | 0.14 | 0.07 | 0.31 | 0.03 | 0.15 | |
| (B170) Stockpile | 1 | | | | PM2.5 | 0.01 | 0.04 | 2.53E-03 | 0.02 | 0.01 | 0.05 | 0.01 | 0.02 | |
| Raw Material Reject Stockpile | | | | | PM | 3.75E-04 | 3.28E-03 | 1.87E-04 | 1.64E-03 | 8.26E-04 | 3.62E-03 | 4.13E-04 | 1.81E-03 | |
| (IMF14) | 10 | 0.002 | 3-sided | 50% | PM10 | 1.76E-04 | 1.54E-03 | 8.81E-05 | 7.72E-04 | 3.88E-04 | 1.70E-03 | 1.94E-04 | 8.51E-04 | |
| (1111 14) | | | | | PM2.5 | 2.81E-05 | 2.46E-04 | 1.41E-05 | 1.23E-04 | 6.20E-05 | 2.71E-04 | 3.10E-05 | 1.36E-04 | |

Notes:

1. Assumed a control efficiency of 50% due to offloading locations having 3-sided concrete enclosures.

One half of the pit waste stockpile area occupied by large rocks, therefore wind erosion emissions are negligible due to size.

3. For wind erosion calculation methods, maximum g/s emissions do not vary based on model averaging period (i.e., a source permitted to operate at maximum capacity 24 hr/day, 365 day/year).

Modeled emission rates in gray are not modeled individually, but are added as a total source emission rate.

Sample Calculations:

Uncontrolled Hourly Emissions (lb/hr) = E (lb/day/acre) * day/24 hr * Base area of pile (acres)

Uncontrolled Annual Emissions (ton/year) = E (lb/day/acre) * 365 days/yr * ton/2000 lb * Base area of pile (acres)

Controlled Emissions = Uncontrolled Emissions (ton/day; ton/year) * (1 - Control Efficiency (%))

Uncontrolled/Controlled Hourly Emissions (lb/hour) = Uncontrolled/Controlled Emissions (lb/hr) * 0.4535924 kg/lb

Uncontrolled/Controlled Annual Emissions (ton/year) = Uncontrolled/Controlled Emissions (ton/yr) * 0.9071847 tonne/ton

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4 Material Handling

| | | | MET | RIC | U | S | 1 | | | | | ME | TRIC | | US | | JS |
|------------------------------|-------------------------|-------------------|-------------|--------------|-----------|------------|---|-------------------------|---------------|-----------------|-------------|--------------|-------------|--------------|-----------|------------|-----------|
| | | | Loading | Loading | Loading | Loading | Enclosure | Control | | Uncontrolled | UNCONT | ROLLED | CONTR | OLLED | UNCON | TROLLED | CONTR |
| Source ID | Source Description | Number of Sources | Rate | Rate | Rate | Rate | Description | Efficiency ² | Pollutant | Emission Factor | Emis | sions | Emiss | sions | Emis | sions | Emis |
| | | | (tonne/day) | (tonne/year) | (ton/day) | (ton/year) | | (%) | | (lb/ton) | (tonne/day) | (tonne/year) | (tonne/day) | (tonne/year) | (ton/day) | (ton/year) | (ton/day) |
| | 19 Conveyor Transfer | | 510 | 186,150 | 562 | 205,193 | | | PM | 3.00E-03 | 1.45E-02 | 5.31E+00 | 2.91E-03 | 1.06E+00 | 1.60E-02 | 5.85E+00 | 3.20E-03 |
| | Points (B220) | 19 | 510 | 186,150 | 562 | 205,193 | Full Enclosure | 80% | PM10 | 1.10E-03 | 5.33E-03 | 1.95E+00 | 1.07E-03 | 3.89E-01 | 5.87E-03 | 2.14E+00 | 1.17E-03 |
| | · · · · | | 510 | 186,150 | 562 | 205,193 | | | PM2.5 | 1.10E-03 | 5.33E-03 | 1.95E+00 | 1.07E-03 | 3.89E-01 | 5.87E-03 | 2.14E+00 | 1.17E-03 |
| | Transfer Point - | | 510 | 186,150 | 562 | 205,193 | Telescopic | | PM | 3.00E-03 | 7.65E-04 | 2.79E-01 | 3.82E-05 | 1.40E-02 | 8.43E-04 | 3.08E-01 | 4.22E-05 |
| | Magnet Separator to | 1 | 510 | 186,150 | 562 | 205,193 | Chute & Full | 95% | PM10 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 1.40E-05 | 5.12E-03 | 3.09E-04 | 1.13E-01 | 1.55E-05 |
| Iron Conta | Iron Container (B220) | | 510 | 186,150 | 562 | 205,193 | Enclosure | | PM2.5 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 1.40E-05 | 5.12E-03 | 3.09E-04 | 1.13E-01 | 1.55E-05 |
| | 2 Transfer Points - | | 510 | 186,150 | 562 | 205,193 | | | PM | 3.00E-03 | 1.53E-03 | 5.58E-01 | 3.06E-04 | 1.12E-01 | 1.69E-03 | 6.16E-01 | 3.37E-04 |
| IMF17 | Feeder (B220) | 2 | 510 | 186,150 | 562 | 205,193 | Full Enclosure | 80% | PM10 | 1.10E-03 | 5.61E-04 | 2.05E-01 | 1.12E-04 | 4.10E-02 | 6.18E-04 | 2.26E-01 | 1.24E-04 |
| | reeder (bzzo) | | 510 | 186,150 | 562 | 205,193 | | | PM2.5 | 1.10E-03 | 5.61E-04 | 2.05E-01 | 1.12E-04 | 4.10E-02 | 6.18E-04 | 2.26E-01 | 1.24E-04 |
| | Transfer Point - Mixing | | 510 | 186,150 | 562 | 205,193 | | | PM | 3.00E-03 | 7.65E-04 | 2.79E-01 | 1.53E-04 | 5.58E-02 | 8.43E-04 | 3.08E-01 | 1.69E-04 |
| | Plant to Bin (B220) | 1 | 510 | 186,150 | 562 | 205,193 | Full Enclosure | 80% | PM10 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 5.61E-05 | 2.05E-02 | 3.09E-04 | 1.13E-01 | 6.18E-05 |
| · · · · · | | | 510 | 186,150 | 562 | 205,193 | | | PM2.5 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 5.61E-05 | 2.05E-02 | 3.09E-04 | 1.13E-01 | 6.18E-05 |
| | Transfer Point - Seive | | 510 | 186,150 | 562 | 205,193 | Telescopic | | PM | 3.00E-03 | 7.65E-04 | 2.79E-01 | 3.82E-05 | 1.40E-02 | 8.43E-04 | 3.08E-01 | 4.22E-05 |
| | Separator to Bin | 1 | 510 | 186,150 | 562 | 205,193 | Chute & Full | 95% | PM10 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 1.40E-05 | 5.12E-03 | 3.09E-04 | 1.13E-01 | 1.55E-05 |
| | (B220) | | 510 | 186,150 | 562 | 205,193 | Enclosure | | PM2.5 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 1.40E-05 | 5.12E-03 | 3.09E-04 | 1.13E-01 | 1.55E-05 |
| | B220 Material | | | | | | | | PM | | 1.84E-02 | 6.70E+00 | 3.44E-03 | 1.26E+00 | 2.02E-02 | 7.39E+00 | 3.79E-03 |
| IMF17 Fugitives ⁴ | Handling Fugitives | 24 | - | - | - | - | - | - 1 | PM10 | | 6.73E-03 | 2.46E+00 | 1.26E-03 | 4.61E-01 | 7.42E-03 | 2.71E+00 | 1.39E-03 |
| | Handling Fugitives | | | | | | | | PM2.5 | | 6.73E-03 | 2.46E+00 | 1.26E-03 | 4.61E-01 | 7.42E-03 | 2.71E+00 | 1.39E-03 |
| | Conveyor Transfer | | 510 | 186,150 | 562 | 205,193 | | | PM | 3.00E-03 | 7.65E-04 | 2.79E-01 | 1.53E-04 | 5.58E-02 | 8.43E-04 | 3.08E-01 | 1.69E-04 |
| IMF12 | Point (B215) | 1 | 510 | 186,150 | 562 | 205,193 | Full Enclosure | 80% | PM10 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 5.61E-05 | 2.05E-02 | 3.09E-04 | 1.13E-01 | 6.18E-05 |
| | POINT (B215) | | 510 | 186,150 | 562 | 205,193 | | | PM2.5 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 5.61E-05 | 2.05E-02 | 3.09E-04 | 1.13E-01 | 6.18E-05 |
| | Conveyor Transfer | | 510 | 186,150 | 562 | 205,193 | | | PM | 3.00E-03 | 7.65E-04 | 2.79E-01 | 1.53E-04 | 5.58E-02 | 8.43E-04 | 3.08E-01 | 1.69E-04 |
| IMF16 | Point (B300) | 1 | 510 | 186,150 | 562 | 205,193 | Full Enclosure | 80% | PM10 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 5.61E-05 | 2.05E-02 | 3.09E-04 | 1.13E-01 | 6.18E-05 |
| | Point (B300) | | 510 | 186,150 | 562 | 205,193 | 1 | | PM2.5 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 5.61E-05 | 2.05E-02 | 3.09E-04 | 1.13E-01 | 6.18E-05 |
| | Transfer Point - | | 510 | 186,150 | 562 | 205,193 | | | PM | 3.00E-03 | 7.65E-04 | 2.79E-01 | 1.91E-04 | 6.98E-02 | 8.43E-04 | 3.08E-01 | 2.11E-04 |
| INCAS | Magnet Separator to | | 510 | 186,150 | 562 | 205,193 | 4-sided rubber | 75% | PM10 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 7.01E-05 | 2.56E-02 | 3.09E-04 | 1.13E-01 | 7.73E-05 |
| IMF15 | Iron Container | 1 | | | | , | drop guards | /5% | | | | | | | | | |
| | (Outside B220) | | 510 | 186,150 | 562 | 205,193 | , | | PM2.5 | 1.10E-03 | 2.80E-04 | 1.02E-01 | 7.01E-05 | 2.56E-02 | 3.09E-04 | 1.13E-01 | 7.73E-05 |
| | | | | 100,100 | 552 | 200,100 | | | PM | | 7.65E-04 | 2.79E-01 | 1.91E-04 | 6.98E-02 | 8.43E-04 | 3.08E-01 | 2.11E-04 |
| Total IMF15 | Outside B220 Transfer | 1 | - | - | - | - | - | | PM10 | | 2.80E-04 | 1.02E-01 | 7.01E-05 | 2.56E-02 | 3.09E-04 | 1.13E-01 | 7.73E-05 |
| TOTAL INIE 15 | Points | 1 | | | | | | · · | PM10 PM2.5 | - | 2.80E-04 | 1.02E-01 | 7.01E-05 | 2.56E-02 | 3.09E-04 | 1.13E-01 | 7.73E-05 |

Notes

 Loading rates for material transfers are based on the maximum daily or annual input to B215 Raw Material Loading Hopper.
 Per Application Instructions and Forms for General Permit G40-C by West Virginia Department of Environmental Protection, Telescopic Chutes have a 75% control efficiency. Full Enclosures have an 80% control efficiency for dump bin unloading, crushing and screening, transfer and conveying, and loading material onto piles.
 Transfer Point Immission factors were taken from AP-42 Section 11.19.2. The Tertiary Crushing Source was assumed for both Mixing and Crushing. The Conveyor Transfer Point (uncontrolled) emission factor was assumed for all transfer points. No emission factor data is available for PM_{2.5} is assumed equal to PM₁₀.
 IMF17 consists of the B220 Material Handling Fugitives shown on the Material Handling Vents summary.

Sample Calculations:

Uncontrolled Emissions (ton/day; ton/year) = E (lb/ton) * Loading Rate (ton/day; ton/year) / 2000 (lb/ton)

Controlled Emissions = Uncontrolled Emissions (ton/day; ton/year) * (1 - Control Efficiency (%))

Uncontrolled/Controlled Emissions (tonne/day; tonne/year) = Uncontrolled/Controlled Emissions (ton/day; ton/year) * 0.9071847 tonne/ton

Total Fugitive Emissions Summary

| | | PM | Λ | PN | N ₁₀ | PM | 2.5 |
|-----------|---|---------------------|--------------|--------------------|-----------------|---------------------|--------------|
| | | CONTROLLED Emiss | | CONTROLLED | | CONTROLLED Emiss | |
| Source ID | Source Description | (short tons/yr) | (tonne/year) | (short tons/vr) | (tonne/year) | (short tons/yr) | (tonne/year) |
| B210/B211 | Raw Material Storage - Delivery to 210 [from offsite (by truck) or from stockpile (by FEL)] | 0.28 | 0.26 | 0.13 | 0.12 | 0.02 | 0.02 |
| B170 | Melting Furnace Portable Crusher & Storage - Melting Furnace Slag Portable Crusher + Drop to Pit Waste (170) (from portable crusher) + Wind Erosion from Pit Waste (170) Stockpile | 0.59 | 0.53 | 0.27 | 0.25 | 0.06 | 0.05 |
| RMS | Raw Material Stockpile - Delivery to Stockpile [from offsite (by truck)] + Wind Erosion from Raw Material Stockpile | 0.20 | 0.18 | 0.10 | 0.09 | 0.015 | 0.013 |
| B215 | Raw Material Loading Hopper | 5.62E-02 | 5.10E-02 | 2.66E-02 | 2.41E-02 | 4.03E-03 | 1.46E-02 |
| RM_REJ | Raw Material Reject Collection Drop | 1.12E-03 | 1.02E-03 | 5.32E-04 | 4.83E-04 | 8.05E-05 | 7.31E-05 |
| IMF17 | B220 Material Handling Fugitives | 1.39 | 1.26 | 0.51 | 0.46 | 0.51 | 0.46 |
| IMF12 | Conveyor Transfer Point (B215) | 6.16E-02 | 5.58E-02 | 2.26E-02 | 2.05E-02 | 2.26E-02 | 2.05E-02 |
| IMF16 | Conveyor Transfer Point (B300) | 6.16E-02 | 5.58E-02 | 2.26E-02 | 2.05E-02 | 2.26E-02 | 2.05E-02 |
| IMF15 | Outside B220 Transfer Points | 7.69E-02 | 6.98E-02 | 2.82E-02 | 2.56E-02 | 2.82E-02 | 2.56E-02 |
| IMF14 | Raw Material Reject Stockpile | 1.81E-03 | 1.64E-03 | 8.51E-04 | 7.72E-04 | 1.36E-04 | 1.23E-04 |

Roxul USA Inc. dba ROCKWOOL Ranson, West Virginia Material Handling Vents

Modified units
New units

Removed units

| nanunng vent | | Removed unit | 3 | | | ME | RIC | S | METRIC | | | S | |
|-----------------------------|--|--------------|--------|-------------|-------------|---------------------|---------------------------|---------------------|---------------------|---------------------|---------------------|---------------------|---------------------|
| | | | | | | PN | , PM ₁₀ | | | | PN | 1 2.5 | |
| Source ID | Source Description ² | Fan Flo | w Rate | Exhaust Cor | ncentration | Hourly Emissions | Annual Emissions | Hourly Emissions | Annual Emissions | Hourly Emissions | Annual Emissions | Hourly Emissions | Annual Emissions |
| | | (Nm3/h) | (scfm) | (mg/Nm3) | (gr/scf) | (kg/hr) | (tonne/yr) | (lb/hr) | (ton/yr) | (kg/hr) | (tonne/yr) | (lb/hr) | (ton/yr) |
| IMF21 | Charging Building Vacuum Cleaning Filter | 500 | 316 | 5 | 0.002 | 2.50E-03 | 0.02 | 5.51E-03 | 0.02 | 1.25E-03 | 0.01 | 2.76E-03 | 0.01 |
| IMF08 | Sorbent Silo | 1,200 | 758 | 5 | 0.002 | 6.00E-03 | 0.05 | 0.01 | 0.06 | 3.00E-03 | 0.03 | 6.61E-03 | 0.03 |
| IMF07 | Filter Fines Day Silo | 1,250 | 790 | 5 | 0.002 | 6.25E-03 | 0.05 | 0.01 | 0.06 | 3.13E-03 | 0.03 | 6.89E-03 | 0.03 |
| IMF07 | Total Indoor with Settling Factor (80%) ³ | - | - | - | - | 1.25E-03 | 0.01 | 2.76E-03 | 0.01 | 6.25E-04 | 0.01 | 1.38E-03 | 0.01 |
| IMF09 | Spent Sorbent Silo | 1,200 | 758 | 5 | 0.002 | 6.00E-03 | 0.05 | 0.01 | 0.06 | 3.00E-03 | 0.03 | 6.61E-03 | 0.03 |
| IMF10 | Filter Fines Receiving Silo | 1,200 | 758 | 5 | 0.002 | 6.00E-03 | 0.05 | 0.01 | 0.06 | 3.00E-03 | 0.03 | 6.61E-03 | 0.03 |
| IMF11 | Conveyor Transition Point (B215 to B220) | 1,800 | 1,137 | 5 | 0.002 | 0.01 | 0.08 | 0.02 | 0.09 | 4.50E-03 | 0.04 | 9.92E-03 | 0.04 |
| | Total Indoor with Settling Factor (80%) ³ | - | - | - | - | 1.80E-03 | 0.02 | 3.97E-03 | 0.02 | 9.00E-04 | 0.01 | 1.98E-03 | 0.01 |
| | Conveyor Transition Point (B220 No. 1) | 1,800 | 1,137 | 5 | 0.002 | 0.01 | 0.08 | 0.02 | 0.09 | 4.50E-03 | 0.04 | 0.01 | 0.04 |
| | Conveyor Transition Point (B220 No. 2) | 1,800 | 1,137 | 5 | 0.002 | 0.01 | 0.08 | 0.02 | 0.09 | 4.50E-03 | 0.04 | 0.01 | 0.04 |
| B220 Conveyor | Mixer | 3,500 | 2,211 | 5 | 0.002 | 0.02 | 0.15 | 0.04 | 0.17 | 8.75E-03 | 0.08 | 0.02 | 0.08 |
| Transition Points, | Crusher | 3,500 | 2,211 | 5 | 0.002 | 0.02 | 0.15 | 0.04 | 0.17 | 8.75E-03 | 0.08 | 0.02 | 0.08 |
| Mixer, and | Total Indoor with Settling Factor (80%) ³ | - | - | - | - | 1.06E-02 | 0.09 | 0.02 | 0.10 | 5.30E-03 | 0.05 | 1.17E-02 | 0.05 |
| Crusher with | Total Conveyor Transition Point (B220 No. 1) | - | - | - | - | 1.80E-03 | 0.02 | 3.97E-03 | 0.02 | 9.00E-04 | 0.01 | 1.98E-03 | 0.01 |
| Fabric Filters ⁴ | Total Conveyor Transition Point (B220 No. 2) | - | - | - | - | 1.80E-03 | 0.02 | 3.97E-03 | 0.02 | 9.00E-04 | 0.01 | 1.98E-03 | 0.01 |
| | Total Mixer | | - | - | - | 3.50E-03 | 0.03 | 7.72E-03 | 0.03 | 1.75E-03 | 0.02 | 3.86E-03 | 0.02 |
| | Total Crusher | - | - | - | - | 3.50E-03 | 0.03 | 7.72E-03 | 0.03 | 1.75E-03 | 0.02 | 3.86E-03 | 0.02 |
| CM10 | Recycle Building Vent 1 | 30,000 | 18,950 | 10 | 0.004 | 0.30 | 2.63 | 0.66 | 2.90 | 0.15 | 1.31 | 0.33 | 1.45 |
| CM11 | Recycle Building Vent 2 | 30,000 | 18,950 | 10 | 0.004 | 0.30 | 2.63 | 0.66 | 2.90 | 0.15 | 1.31 | 0.33 | 1.45 |
| CM08 | Recycle Building Vent 3 | 2,500 | 1,579 | 10 | 0.004 | 0.03 | 0.22 | 0.06 | 0.24 | 0.01 | 0.11 | 0.03 | 0.12 |
| CM09 | Recycle Building Vent 4 | 2,500 | 1,579 | 10 | 0.004 | 0.03 | 0.22 | 0.06 | 0.24 | 0.01 | 0.11 | 0.03 | 0.12 |

Notes:

ton = short tons

tonne = metric tons

1. $PM_{2.5}$ is conservatively assumed to be 50% of PM for material handling.

2. Material handling vents are equipped with fabric filters or bin vent filters.

3. Per Application Instructions and Forms for General Permit G40-C by West Virginia Department of Environmental Protection, Full Enclosures have an 80% control efficiency for dump bin unloading, crushing and screening, transfer and conveying, and lo

4. Conveyor Transition Points (B220 No. 1) and (B220 No. 2) are accounted for with IMF17, as well as the Mixer and Crusher.

Sample Calculations

Hourly Emissions (kg/hr) = Fan Flow Rate (Nm³/hr) * Exhaust Concentration (mg/Nm³) * 1,000,000 (mg/kg)

Annual Emissions (tonne/yr) = Hourly Emissions (kg/hr) * 8,400 (hr/yr) / 1,000 (kg/tonne)

Hourly Emissions (lb/hr) = Fan Flow Rate (scfm) * Exhaust Concentration (gr/scf) / 7,000 (gr/lb) * 60 (min/hr)

Annual Emissions (ton/yr) = Hourly Emissions (lb/hr) * 8,400 (hr/yr) / 2,000 (lb/ton)

| Roxul USA Inc. dba ROCKWOOL | Modified units |
|-----------------------------|----------------|
| Ranson, West Virginia | New units |
| Source ID: Dry Ice Cleaning | Removed units |

Operating Parameters, per Source

| Dry Ice Production ¹ | 75 | kg/hr |
|---------------------------------------|---------|---------------|
| Annual Dry Ice Production | 630,000 | kg/yr |
| Operating Hours ² | 8,400 | hr/yr |
| CO ₂ Consumed ¹ | 2.2 | (loss factor) |

Emission Calculations⁴

| | U | S | METRIC | | | |
|-------------------------|---------|----------|---------|------------|--|--|
| Source | Hourly | Annual | Hourly | Annual | | |
| Source | (lb/hr) | (ton/yr) | (kg/hr) | (tonne/yr) | | |
| CO ₂ Emitted | 363.76 | 1,527.80 | 165.00 | 1,386.00 | | |

Notes:

ton = short tons

tonne = metric tons

1. Dry ice production per manufacturer data sheet. CO_2 consumed (loss factor) represents the total quantity of CO_2 consumed to produce 1 kg CO_2 (accounts for CO_2 system loss).

2. For conservatism, emissions from dry ice cleaning station are based on 8,760 hours per year; however, the equipment will traverse from one end of the equipment to the other when cleaning and dry ice pellets are used only when in forward movement.

Sample Calculations:

Dry Ice Production Rate (kg/yr) = Hourly Dry Ice Production Rate (kg/hr) * 8,400 (hrs/yr) CO₂ Hourly Emission Rate (lb/hr) = Hourly Dry Ice Production Rate (kg/hr) * CO₂ Loss Factor * 2.2046 (lbs/kg) CO₂ Annual Emission Rate (ton/yr) = CO2 Emission Rate (lb/hr) * 8,400 (hr/yr) / 2,000 (lb/ton) CO2 Hourly Emission Rate (kg/hr) = Hourly Emission Rate (lb/hr) * 0.45359 (kg/lb) CO₂ Annual Emission Rate (tonne/yr) = Annual Emission Rate (ton/yr) * 0.90718 (tonne/ton)

Roxul USA Inc. dba ROCKWOOL Ranson, West Virginia Source ID: Fleece Application (CM12, CM13)

| Modified units | |
|----------------|--|
| New units | |
| Removed units | |

| Operating Parameters, per Source | |
|----------------------------------|--|
|----------------------------------|--|

| Binder Applied to Fleece | 93 | kg/hr |
|---|---------|-------------------|
| Operating Hours ¹ | 4,200 | hr/yr |
| Annual Binder Usage at | | |
| Fleece Station | 388,500 | kg/yr |
| Organic HAP Emission Limit ² | 0.016 | kg OHAP/kg binder |

Emission Calculations³

| | L | JS | ME | TRIC |
|-----------|-----------|--------------|-----------|--------------|
| Pollutant | Maximum E | mission Rate | Maximum E | mission Rate |
| | (lb/hr) | (ton/yr) | (kg/hr) | (tonne/yr) |
| VOC | 3.26 | 6.85 | 1.48 | 6.22 |
| Total HAP | 3.26 | 6.85 | 1.48 | 6.22 |

Notes:

ton = short tons

tonne = metric tons

1. Emissions from the fleece application station are based on 4,200 hours per year.

2. The coating material, or in this case binder, regulated by NESHAP Subpart JJJJ is a compliant coating by formulation. The limit of 0.016 kg OHAP/kg coating material is stated in 40 CFR §63.3370(a)(2)(i) for the use of "as-applied" compliant coating materials from new affected sources (per §63.3320(b)(2) which states that HAP emissions must be limited to "no more than 1.6 percent of the mass of coating materials applied for each month at new affected sources"). Roxul may choose to comply with this limit using VOC as a surrogate for organic HAP as allowed by §63.3370(c)(1)(i) and §63.3360(c)(2). Therefore VOC emissions are shown as equal to organic HAP (Total HAP) emissions.

3. The fleece application equipment will be placed just prior to the entrance of the Curing Oven. While a majority of fleece application equipment emissions will be controlled by the Curing Oven afterburner as the fleece is cured onto the wet mineral wool in the Curing Oven, no credit is taken for VOC/organic HAP emission control in this calculation.

Sample Calculations:

Maximum Hourly Emission Rate (lb/hr) = Binder Applied to Fleece (kg/hr) * 0.016 (kg VOC/HAP / kg binder) * 2.2046 (lb/kg) Maximum Annual Emission Rate (ton/yr) = Maximum Hourly Emission Rate (lb/hr) * 4,200 (hr/yr) / 2,000 (lb/ton) Maximum Hourly Emission Rate (kg/hr) = Maximum Hourly Emission Rate (lb/hr) * 0.4535924 (kg/lb) Maximum Annual Emission Rate (tonne/yr) = Maximum Annual Emission Rate (ton/yr) * 0.9071847 (tonne/ton) Modified units

New units Removed units

Operating Parameters, PER BOILER

| Maximum Heat Input | 1,500 | kw |
|--------------------|-------------|-------------|
| Capacity | 5.12 | MMBtu/hr |
| Operating Hours | 8,400 | hr/yr |
| Fuel Type | Natural Gas | |
| Fuel HHV | 1,026 | MMbtu/MMscf |

Maximum Potential Emissions^{1,2}

| Maximum Potentia | al Emissions | 1,2 | U | S | MET | RIC |
|--|--------------|------------|---------------------|---------------------|---------------------|---------------------|
| Pollutant | Emissio | n Factor | Hourly Emissions | Annual Emissions | Hourly Emissions | Annual Emissions |
| | (lb/MMscf) | (lb/MMbtu) | (lb/hr) | (ton/yr) | (kg/hr) | (tonne/yr) |
| NO _x | 72.42 | 0.0706 | 0.36 | 1.52 | 0.16 | 1.38 |
| SO ₂ | 0.6 | 0.0006 | 3.00E-03 | 0.01 | 1.36E-03 | 0.01 |
| PM/PM _{10F} /PM _{2.5F} | 1.9 | 0.0019 | 0.01 | 0.04 | 4.30E-03 | 0.04 |
| PM _{10T} /PM _{2.5T} | 7.6 | 0.0074 | 0.04 | 0.16 | 0.02 | 0.14 |
| Condensable PM | 5.7 | 0.0056 | 0.03 | 0.12 | 0.01 | 0.11 |
| CO | 84 | 0.0819 | 0.42 | 1.76 | 0.19 | 1.60 |
| VOC | 5.5 | 0.0054 | 0.03 | 0.12 | 0.01 | 0.10 |
| Lead | 0.0005 | 4.87E-07 | 2.50E-06 | 1.05E-05 | 1.13E-06 | 9.51E-06 |
| Hexane | 1.8 | 0.0018 | 0.01 | 0.04 | 0.00 | 0.03 |
| Total HAPs | 1.89 | 0.0018 | 0.01 | 0.04 | 4.28E-03 | 0.04 |
| CO ₂ | - | 116.98 | 599.25 | 2516.84 | 271.81 | 2,283.24 |
| CH ₄ | - | 2.20E-03 | 0.01 | 0.05 | 5.12E-03 | 0.04 |
| N ₂ O | - | 2.20E-04 | 1.13E-03 | 4.74E-03 | 5.12E-04 | 4.30E-03 |
| CO ₂ e ³ | - | - | 599.87 | 2,519.44 | 272.09 | 2,285.59 |

Notes:

ton = short tons

tonne = metric tons

1. Natural Gas emission factor source AP-42 Table 1.4-1, 1.4-2, 1.4-3, and 1.4-4 for SO₂, PM_{10T}, PM_{2.5T}, CO, VOC, GHG emission factors per 40 CFR Part 98, Table C-1 and C-2. GWPs per 40 CFR 98, Table A-1.

 NO_X emission factor based on 60 ppmvd @ 3% O2 per manufacturer specification.

2. PM_{10T} and PM_{2.5T} emission factors include filterable and condensable particulate matter (e.g., Total PM₁₀, PM_{2.5}).

3. CO₂ Equivalent (CO₂e) lb/hr, ton/yr = CO₂ + [GWP_{CH4} * CH₄)] + [GWP_{N20} * N₂O].

Sample Calculations:

Hourly Emissions (lb/hr) = Emission Factor (lb/MMBtu) * Maximum Heat Input Capacity (MMBtu/hr)

Annual Emissions (ton/yr) = Hourly Emissions (lb/hr) * 8400 (hr/yr) / 2,000 (lb/ton)

Hourly Emissions (kg/hr) = Hourly Emissions (lb/hr) /2.2046 (lb/kg)

Annual Emissions (tonne/yr) = Hourly Emissions (kg/hr) * 8400 (hr/yr) / 1,000 (kg/tonne)

| | West Virginia): Facility-wide Storage Tanks | New units Removed units | | | | | | | | | | | | - | | | us | | | | | ME | TRIC | | |
|------------------------|---|----------------------------|------------------|----------|--------|----------|------------|------------------------|-----------|-------------|-------------|-----------------|--------------|-----------------------------|---------------|-------------------------|--------------------|-------------------|----------|-----------------------------|---------------|-------------------------|--------------------|-------------------|-------------|
| | | | | | | | | | | | | | | | VOC Emissions | | Spec | ated HAP Emission | ns. | | VOC Emissions | | | ed HAP Emissi | ions |
| Rockwool | | | | Capacity | Height | Diameter | Throughput | | | Temp. | Sto Temp | rage erature | Pressurized? | Breathing Loss ² | Working Loss | Total Loss ³ | Total Formaldehyde | | | Breathing Loss ² | Working Loss | Total Loss ³ | Total Formaldehyde | Total Methanol | Total Pheno |
| iource ID ⁶ | Description | Material Stored | Tank Orientation | (gal) | (ft) | (ft) | (gal/yr) | Fill Method | Roof Type | Controlled? | deg C | deg F | (Y, N) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (ton/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) | (tonne/yr) |
| TK-DF | One (1) Diesel Fuel Horizontal Storage Tank (4.7 m3, 1,242 gal) | Diesel Fuel | Horizontal | 1,242 | 16.4 | 4.4 | 52,834 | Splash Pump | Flat | No | Ambient | Ambient | No | 1.18E-04 | 4.33E-04 | 5.51E-04 | - | • | | 1.07E-04 | 3.93E-04 | 5.00E-04 | | | |
| тк-тоз | One (1) Thermal Oil Horizontal Tank (20 m3, 5,283 gal) | Thermal Oil | Horizontal | 5,283 | 21.0 | 6.6 | 698 | Splash Pump | Flat | Yes | 200 | 392 | No | | 2.18E-03 | 2.18E-03 | - | | | | 1.98E-03 | 1.98E-03 | - | | |
| тк-то4 | One (1) Thermal Oil Horizontal Expansion Tank (7.3 m3, 1,928 gal) | Thermal Oil | Horizontal | 1,928 | 13.0 | 5.2 | 698 | Splash Pump | Flat | Yes | 200 | 392 | No | | 2.18E-03 | 2.18E-03 | - | | | | 1.98E-03 | 1.98E-03 | - | | |
| TK-RS1 | No. 1 of Six (6) Resin Vertical Storage Tanks (ea. 50 m3, 13,209 gal) | Resin | Vertical | 13,209 | 21.0 | 13.8 | 317,007 | Splash Air Off or Pump | Cone | Yes | 20 | 68 | No | | 0.02 | 0.02 | 0.02 | 1.54E-04 | | | 0.02 | 0.02 | 0.02 | 1.39E-04 | |
| TK-RS2 | No. 2 of Six (6) Resin Vertical Storage Tanks (ea. 50 m3, 13,209 gal) | Resin | Vertical | 13,209 | 21.0 | 13.8 | 317,007 | Splash Air Off or Pump | Cone | Yes | 20 | 68 | No | | 0.02 | 0.02 | 0.02 | 1.54E-04 | | | 0.02 | 0.02 | 0.02 | 1.39E-04 | |
| TK-RS3 | No. 3 of Six (6) Resin Vertical Storage Tanks (ea. 50 m3, 13,209 gal) | Resin | Vertical | 13,209 | 21.0 | 13.8 | 317,007 | Splash Air Off or Pump | Cone | Yes | 20 | 68 | No | | 0.02 | 0.02 | 0.02 | 1.54E-04 | | | 0.02 | 0.02 | 0.02 | 1.39E-04 | |
| TK-RS4 | No. 4 of Six (6) Resin Vertical Storage Tanks (ea. 50 m3, 13,209 gal) | Resin | Vertical | 13,209 | 21.0 | 13.8 | 317,007 | Splash Air Off or Pump | Cone | Yes | 20 | 68 | No | | 0.02 | 0.02 | 0.02 | 1.54E-04 | | | 0.02 | 0.02 | 0.02 | 1.39E-04 | |
| TK-RS5 | No. 5 of Six (6) Resin Vertical Storage Tanks (ea. 50 m3, 13,209 gal) | Resin | Vertical | 13.209 | 21.0 | 13.8 | 317.007 | Solash Air Off or Pump | Cone | Yes | 20 | 68 | No | | 0.02 | 0.02 | 0.02 | 1.54E-04 | | | 0.02 | 0.02 | 0.02 | 1.39E-04 | |
| TK-RS6 | No. 6 of Six (6) Resin Vertical Storage Tanks (ea. 50 m3, 13,209 gal) | Resin | Vertical | 13.209 | 21.0 | 13.8 | 317.007 | Solash Air Off or Pump | Cone | Yes | 20 | 68 | No | | 0.02 | 0.02 | 0.02 | 1.54E-04 | | | 0.02 | 0.02 | 0.02 | 1.39E-04 | |
| TK-CA | One (1) Coupling Agent Vertical Storage Tank (1.5 m3, 396 gal) | Coupling Agent Solution | Vertical | 396 | 6.0 | 3.6 | 4.227 | Solash Pump | Cone | No | Ambient | Ambient | No | 2.03E-05 | 2.29E-05 | 4.31E-05 | | | | 1.84E-05 | 2.07E-05 | 3.91E-05 | | | |
| TK-AD | One (1) Additive Vertical Storage Tank (1.5 m3, 396 gal) | Binder Additive | Vertical | 396 | 6.0 | 3.6 | 17.171 | Solash Pump | Cone | No | Ambient | Ambient | No | 2.03E-06 | 7.97E-05 | 8.17E-05 | | | | 1.84E-06 | 7.23E-05 | 7.41E-05 | | | |
| TK-ADB1 | One (1) Vertical Additive Buffer Tank (1.5 m3, 396 gal) | Binder Solution | Vertical | 396 | 6.0 | 3.6 | 65,000 | Splash Pump | Cone | No | Ambient | Ambient | No | 2.03E-05 | 1.23E-04 | 1.43E-04 | 0.00 | 0.00E+00 | | 1.84E-05 | 0.00 | 0.00 | 0.00 | 0.00E+00 | |
| TK-ADB2 | One (1) Vertical Additive Buffer Tank (0.5 m3, 132 gal) | Binder Solution | Vertical | 132 | 4.0 | 2.6 | 21,667 | Splash Pump | Cone | No | Ambient | Ambient | No | 7.05E-06 | 0.00 | 0.00 | 0.00 | 0.00E+00 | | 6.40E-06 | 0.00 | 0.00 | 0.00 | 0.00E+00 | |
| TKGIY | One (1) Vertical Glycol Storage Tank (1.5 m3, 396 gal) | Givcol | Vertical | 396 | 6.0 | 3.6 | 4.752 | Solash Pump | Flat | No | Ambient | Ambient | No | 2.90E-06 | 0.00 | 0.00 | 0.00 | 0.00E+00 | | 0.00E+00 | 0.00 | 0.00 | 0.00 | 0.00E+00 | |

Ambient Ambient

Ambient Ambient

Ambient Ambient

Ambient Ambient

Ambient Ambient

Ambient

Ambient

2.50E-04

2.50E-04

2.50E-04

1.61E-04

3.72E-05

3.72E-05

3.72E-05

1.79E-05

No

No

No

No

No

No

2.87E-04

2.87E-04

2.87E-04

1.79E-04

0.03

0.03

2.84E-04

2.84E-04

2.84E-04

2.45E-06

2.45E-06

2.45E-06

9.30E-04

2.58E-04

2.58E-04

2.58E-04

0.10

2.60E-04

2.60E-04

1.62E-04

0.03

0.03

3.38E-05 2.26E-04 2.60E-04

2.26E-04

1.46E-04

3.38E-05 2.26E-04

3.38E-05

1.62E-05

2.22E-06

2.22E-06

2.22E-06

0.00

Flat

Flat

Cone

Flat

No

No

No

No

No

No

Splash Pump

Splash Pump

Splash Pump

Splash Pump

7.8 3.6 130,325 Splash Pump Flat

130,325

52,834

266,471

397 5.0 4.2 266,471 Splash Pump Flat

7.8 3.6 130,325

7.8 3.6

5.0 3.0

8.6 4.0

TK-DOD One (1) De-dust Oil Vertical Day Tank (1 m3, 264 gal). De-dust Oil Vertical TK-PD One (1) Paint Dilution Storage Tank (3 m3, 793 gal) Diluted Water-based Paint Vertical TK-PDD One (1) Paint Dilution Day Tank (1.5 m3, 397 gal) Diluted Water-based Paint Vertical

TK-BS1 No. 1 of Three (3) Binder Storage Containers (ea. 1 m3, 264 gal)

TK-BS2 No. 2 of Three (3) Binder Storage Containers (ea. 1 m3, 264 gal)

TK-BS3 No. 3 of Three (3) Binder Storage Containers (ea. 1 m3, 264 gal)

Fleece Coating

Fleece Coating

Fleece Coating

 Other
 Open Control Day Tank (1 Sm.) 207 gpt)
 Diverse
 over 1
 <th

Vertical

Vertical

Vertical

264

264

264

264.172

793

138 of 145

Roxul USA Inc. dba ROCKWOOL Ranson, West Virginia Source ID: Facility-wide Fugitive Emissions from Paved Haul Roads



Emission Estimate For Paved Haulroads¹

| k = | PM particle size multiplier ((lb/VMT)) | 0.011 |
|---|---|-----------|
| k ₁₀ = | PM10 particle size multiplier ((lb/VMT)) | 0.0022 |
| k _{2.5} = | PM2.5 particle size multiplier ((lb/VMT)) | 0.00054 |
| sL _{finishedprod} ² = | Finished product road surface silt loading, (g/m*2) | 0.2 |
| sL _{cawrat} ³ = | Raw materials road surface silt loading, (g/m^2) | 8.2 |
| W ⁶ = | Mean Vehicle Weight (tons) | see table |
| P ⁴ = | Number of days per year with precipitation >0.01 inch | 148 |
| N = | Number of days in averaging period | 365 |
| CE ⁵ | Control Efficiency. % | 75% |
| | Maximum Weeks of Operation per year: | 52 |
| | Hours of Operation per year: | 8 760 |

IIS IInite

| | | Empty | Load Carried | Loaded | W, Mean | | Maximum | | | | | PM | | | | | | PM-10 | | | | | | PM | -2.5 | | |
|-----------------|---|-------------------|---------------------|--------------------------------|-------------------|-------------------|--|------------------------------|---------------------------|------------------------------------|-------------|-------------|------------|------------|------------------------------------|-------------|-------------|------------|------------|--------------------|-----------------|------------------------------------|--------------|------------|------------|------------|--|
| Item No. | Description | Vehicle Weight | Weight ² | Vehicle Weight ³ | Vehicle Weight | Miles per Trip | Trips Per Day, Per Year ² | Maximum Trips Per Week | Maximum Trips Per Year | Uncontrolled Emission Factor | Uncontrolle | d Emissions | Controlled | Emissions | Uncontrolled Emission Factor | Uncontrolle | d Emissions | Controlled | Emissions | Total Modele Ra | | Uncontrolled Emission Factor | Uncontroller | Emissions | Controlled | | Total Modeled Emission Rate ¹ |
| | | (tons) | (tons) | (tons) | (tons) | | rear | | | (Ib/VMT) | (ton/day) | (ton/year) | (ton/day) | (ton/year) | (Ib/VMT) | (ton/day) | (ton/year) | (ton/day) | (ton/year) | 24-hr (g/s) | Annual (g/s) | (Ib/VMT) | (ton/day) | (ton/year) | (ton/day) | (ton/year) | 24-hr (g/s) |
| 1 | Truck - Oil | 10 | 23.1 | 33.1 | 21.6 | 0.46 | 1 | 1 | 52 | 1.54 | 3.54E-04 | 0.02 | 8.85E-05 | 4.60E-03 | 0.31 | 7.08E-05 | 3.68E-03 | 1.77E+05 | 9.20E-04 | 1.86E-04 | 2.65E-05 | 0.08 | 1.74E-05 | 9.03E-04 | 4.34E-06 | 2.26E-04 | 4.56E-05 |
| 2 | Truck - Oxygen | 10 | 2.5 | 12.5 | 11.3 | 0.46 | 4 | 22 | 1,144 | 0.79 | 7.29E-04 | 0.21 | 1.82E-04 | 0.05 | 0.16 | 1.46E-04 | 0.04 | 3.65E-05 | 0.01 | 3.83E-04 | 3.00E-04 | 0.04 | 3.58E-05 | 0.01 | 8.95E-06 | 2.56E-03 | 9.40E-05 |
| 3 | Truck - Raw Material (Stone) to 210 | 10 | 38.6 | 40.0 | 25.0 | 0.46 | 28 | 128 | 6,656 | 1.79 | 0.01 | 2.74 | 2.91E-03 | 0.68 | 0.36 | 2.32E-03 | 0.55 | 5.81E-04 | 0.14 | 6.10E-03 | 3.94E-03 | 0.09 | 5.71E-04 | 0.13 | 1.43E-04 | 0.03 | 1.50E-03 |
| 4 | Truck - DeSOx and Binder | 10 | 23.1 | 33.1 | 21.6 | 0.46 | 2 | 13 | 676 | 1.54 | 8.36E-04 | 0.24 | 2.09E-04 | 0.06 | 0.31 | 1.67E-04 | 0.05 | 4.18E-05 | 0.01 | 4.39E-04 | 3.44E-04 | 0.08 | 4.11E-05 | 0.01 | 1.03E-05 | 2.94E-03 | 1.08E-04 |
| 5 | Truck - Waste | 10 | 23.1 | 33.1 | 21.6 | 0.46 | 1 | 5 | 260 | 1.54 | 3.22E-04 | 0.09 | 8.04E-05 | 0.02 | 0.31 | 6.43E-05 | 0.02 | 1.61E-05 | 4.60E-03 | 1.69E-04 | 1.32E-04 | 0.08 | 1.58E-05 | 4.52E-03 | 3.95E-06 | 1.13E-03 | 4.15E-05 |
| 6 | Truck - Pallet and Foil | 10 | 33.3 | 40.0 | 25.0 | 0.76 | 5 | 25 | 1,300 | 0.06 | 1.05E-04 | 0.03 | 2.63E-05 | 0.01 | 0.01 | 2.10E-05 | 0.01 | 5.26E-06 | 1.50E-03 | 5.52E-05 | 4.33E-05 | 2.99E-03 | 5.17E-06 | 1.48E-03 | 1.29E-06 | 3.69E-04 | 1.36E-05 |
| 7 | Truck - Finished Goods | 10 | 6.6 | 16.6 | 13.3 | 0.76 | 73 | 400 | 20,800 | 0.03 | 8.85E-04 | 0.25 | 2.21E-04 | 0.06 | 0.01 | 1.77E-04 | 0.05 | 4.43E-05 | 0.01 | 4.65E-04 | 3.64E-04 | 1.57E-03 | 4.34E-05 | 0.01 | 1.09E-05 | 3.11E-03 | 1.14E-04 |
| 8* | FEL - Diverted Melt from Bldg 300 to Pit Waste (170) | 14.5 | 6.6 | 21.1 | 17.8 | 0.27 | 67 | | 12,295 | 1.26 | 0.01 | 2.10 | 2.87E-03 | 0.52 | 0.25 | 2.30E-03 | 0.42 | 5.74E-04 | 0.10 | 6.03E-03 | 3.01E-03 | 0.06 | 5.64E-04 | 0.10 | 1.41E-04 | 0.03 | 1.48E-03 |
| 94 | FEL - Crushed Melt from 170 to 210 | 14.5 | 6.6 | 21.1 | 17.8 | 0.1 | 67 | | 12.295 | 1.26 | 4.25E-03 | 0.78 | 1.06E-03 | 0.19 | 0.25 | 8.50E-04 | 0.16 | 2.13E-04 | 0.04 | 2.23E-03 | 1.12E-03 | 0.06 | 2.09E-04 | 0.04 | 5.22E-05 | 0.01 | 5.48E-04 |
| 10 ⁴ | FEL - Raw Material from 210 to Feed Hopper | 14.5 | 6.6 | 21.1 | 17.8 | 0.06 | 85 | | 31.147 | 1.26 | 3.23E-03 | 1.18 | 8.08E-04 | 0.29 | 0.25 | 6.46E-04 | 0.24 | 1.62E-04 | 0.06 | 1.70E-03 | 1.70E-03 | 0.06 | 1.59E-04 | 0.06 | 3.97E-05 | 0.01 | 4.16E-04 |
| 11.4 | FEL - Raw Material from Stockpile to 210 | 14.5 | 6.6 | 21.1 | 17.8 | 0.16 | 115 | | 31,147 | 1.26 | 0.01 | 3.15 | 2.91E-03 | 0.79 | 0.25 | 2.33E-03 | 0.63 | 5.83E-04 | 0.16 | 0.01 | 4.52E-03 | 0.06 | 5.72E-04 | 0.15 | 1.43E-04 | 0.04 | 1.50E-03 |
| | Truck - Raw Material from Stockpile to 210 (add'1 miles over Item | | | | | | | | | | | | | | | | | | | | | | | | | | |
| 12 | 3) | 10.0 | 38.6 | 40.0 | 25.0 | 0.27 | 30 | | 1,087 | 1.79 | 0.01 | 0.26 | 1.81E-03 | 0.07 | 0.36 | 1.45E-03 | 0.05 | 3.62E-04 | 0.01 | 3.80E-03 | 3.77E-04 | 0.09 | 3.56E-04 | 0.01 | 8.89E-05 | 3.22E-03 | 9.33E-04 |
| | | | | | | | | | TOTAL Raw Materi | al (Item 1-5, 8-12) | 0.05 | 10.75 | 0.01 | 2.69 | | 0.01 | 2.15 | 0.003 | 0.54 | 0.03 | 0.02 | | 0.003 | 0.53 | 6.35E-04 | 0.13 | 6.67E-03 |
| | | | | | | | | т | OTAL Finished Pro | ducts (Items 6.7) | 9.90E-04 | 0.28 | 2.48E-04 | 0.07 | | 1.98E-04 | 0.06 | 4.95E-05 | 0.01 | 5.20E-04 | 4.07E-04 | | 4.86E-05 | 0.01 | 1.22E-05 | 3.48E-03 | 1.28E-04 |

| Source | Pollutant | No. of Modeled | PER SEGME Emissio | ENT Modeled In Rates ¹ |
|----------------------------|-----------|-------------------|----------------------|--------------------------------------|
| | | Segments | 24-hr (g/s) | Annual (g/s) |
| Raw Material Paved Haul | PM-10 | 31 | 8.76E-04 | 4.99E-04 |
| Roads | PM-2.5 | | 2.15E-04 | 1.22E-04 |
| Finished Products | PM-10 | 35 | 1.49E-05 | 1.16E-05 |
| Paved Haul Roads | PM-2.5 | | 3.65E-06 | 2.86E-06 |

Metric Units

| em No. Description | Empty Vehicle Weight | Load Carried Weight | Loaded Vehicle | W, Mean | | | | | | PM | | | | | | PM-10 | | | | | | | PM-2.5 | | | |
|--|--|---|---|---|--------------------------|--------------------------------|---------------------------|------------------------------------|------------------|--------------|------------------|--------------------|------------------------------------|----------------------|--------------|-------------------|--------------|----------------|-----------------|--------------------|-------------------|--------------|----------------------|--------------|----------------|----------------|
| | | | Weight | Vehicle Weight | km per Trip | Maximum Trips Per Week | Maximum Trips Per Year | Uncontrolled Emission Factor | Uncontrolle | d Emissions | Controlled | Emissions | Uncontrolled Emission Factor | Uncontrolled | d Emissions | Controlled | Emissions | Total Modeled | | Emission Factor | Uncontrolle | d Emissions | Controlled | Emissions | Total Modele | |
| | (tonnes) | (tonnes) | (tonnes) | (tonnes) | | HUUK | | (kg/VMT) | (tonne/day) | (tonne/year) | (tonne/day) | (tonne/year) | (kg/VMT) | (tonne/day) | (tonne/year) | (tonne/day) | (tonne/year) | 24-hr (a/s) | Annual (g/s) | (kg/VMT) | (tonne/day) | (tonne/year) | (tonne/day) | (tonne/year) | 24-hr (g/s) | Annua (g/s) |
| 1 Truck - Oil | 9.07 | 21.0 | 30.1 | 19.6 | 0.74 | 1 | 52 | 0.70 | 3.21E-04 | 0.02 | 8.03E-05 | 4.17E-03 | 0.14 | 6.42E-05 | 3.34E-03 | 1.61E-05 | 8.35E-04 | | | 0.03 | 1.58E-05 | 8.20E-04 | 3.94E-06 | 2.05E-04 | | |
| 2 Truck - Oxygen | 9.07 | 2.3 | 11.4 | 10.2 | 0.74 | 22 | 1,144 | 0.36 | 6.61E-04 | 0.19 | 1.65E-04 | 0.05 | 0.07 | 1.32E-04 | 0.04 | 3.31E-05 | 0.01 | | | 0.02 | 3.25E-05 | 0.01 | 8.12E-06 | 2.32E-03 | | |
| 3 Truck - Raw Material (Stone) to 210 or Stockpile | 9.07 | 35.0 | 36.3 | 22.7 | 0.74 | 128 | 6,656 | 0.81 | 1.05E-02 | 2.48 | 2.64E-03 | 0.62 | 0.16 | 2.11E-03 | 0.50 | 5.27E-04 | 0.12 | | | 0.04 | 5.18E-04 | 0.12 | 1.29E-04 | 0.03 | | |
| 4 Truck - DeSOx and Binder | 9.07 | 21.0 | 30.1 | 19.6 | 0.74 | 13 | 676 | 0.70 | 7.59E-04 | 0.22 | 1.90E-04 | 0.05 | 0.14 | 1.52E-04 | 0.04 | 3.79E-05 | 0.01 | 1 | | 0.03 | 3.73E-05 | 0.01 | 9.31E-06 | | 1 | |
| 5 Truck - Waste | 9.07 | 21.0 | 30.1 | 19.6 | 0.74 | 5 | 260 | 0.70 | 2.92E-04 | 0.08 | 7.30E-05 | 0.02 | 0.14 | 5.84E-05 | 0.02 | 1.46E-05 | 4.17E-03 | 1 | | 0.03 | 1.43E-05 | 4.10E-03 | 3.58E-06 | 1.02E-03 | 1 | |
| 6 Truck - Pallet and Foil | 9.07 | 30.2 | 36.3 | 22.7 | 1.22 | 25 | 1.300 | 0.03 | 9.55E-05 | 0.03 | 2.39E-05 | 0.01 | 0.01 | 1.91E-05 | 0.01 | 4.77E-06 | 1.37E-03 | 1 | | 1.36E-03 | 4.69E-06 | 1.34E-03 | | 3.35E-04 | 1 | |
| 7 Truck - Finished Goods | 9.07 | 6.0 | 15.1 | 12.1 | 1.22 | 400 | 20,800 | 0.01 | 8.03E+04 | 0.23 | 2.01E-04 | 0.06 | 2.91E-03 | 1.61E-04 | 0.05 | 4.01E-05 | 0.01 | | | 7.13E-04 | 3.94E-05 | 0.01 | 9.85E-06 | 2.82E-03 | | |
| 8 FEL - Diverted Melt from Bidg 300 to Pit Waste (170) | 13.13 | 6.0 | 19.1 | 16.1 | 0.43 | | 13,553 | 0.57 | 1.04E-02 | 1.90 | 2.60E-03 | | 0.11 | 2.08E-03 | 0.38 | 5.21E-04 | 0.10 | 1 | | 0.03 | 5.11E-04 | 0.09 | 1.28E-04 | 0.02 | 1 | |
| 9 FEL - Crushed Melt from 170 to 210 | 13.13 | 6.0 | 19.1 | 16.1 | 0.16 | | 13,553 | 0.57 | 3.86E+03 | 0.70 | 9.64E-04 | 0.18 | 0.11 | 7.72E-04 | 0.14 | 1.93E-04 | 0.04 | 1 | | 0.03 | 1.89E-04 | 0.03 | 4.73E-05 | 0.01 | 1 | |
| 10 FEL - Raw Material from 210 to Feed Hopper | 13.13 | 6.0 | 19.1 | 16.1 | 0.10 | | 34.333 | 0.57 | 2.93E-03 | 1.07 | 7.33E-04 | 0.27 | 0.11 | 5.86E-04 | 0.21 | 1.47E-04 | 0.05 | 1 | | 0.03 | 1.44E-04 | 0.05 | 3.60E-05 | | 1 | |
| 11 FEL - Raw Material from Stockpile to 210 | 13.13 | 6.0 | 19.1 | 16.1 | 0.26 | | 34,333 | 0.57 | 0.01 | 2.85 | 2.64E-03 | 0.71 | 0.11 | 2.12E-03 | 0.57 | 5.29E-04 | 0.14 | | | 0.03 | 5.19E-04 | 0.14 | 1.30E-04 | 3.50E-02 | | |
| Truck - Raw Material from Stockpile to 210 (add1 miles over Iter | 9.07 | | | | | | | | | | | | | | | | | | | | | | | | | |
| 12 3) | 9.07 | 35.0 | 36.3 | 22.7 | 0.43 | | 1,087 | 0.81 | 6.57E-03 | 0.24 | 1.64E-03 | 0.06 | 0.16 | 1.31E-03 | 0.05 | 3.29E-04 | 0.01 | | | 0.04 | 3.23E-04 | 0.01 | 8.06E+05 | 2.92E-03 | | |
| | | | | | | | OTAL Raw Materi | | 0.05 8.98E-04 | 9.76 0.26 | 0.01 2.25E-04 | 2.44 | | 9.39E-03 1.80E-04 | 1.95 | 0.002 4.49E-05 | 0.49 | | | | 0.002 4.41E-05 | 0.48 | 5.76E-04 1.10E-05 | | | |
| short tons = rentic tons front end loader divided emission rates in gray are not modeled as a total, but divided out an summar. This per Day, Maximum Trings per Year, and Data Carried Webby Ton to the per Day of the tons of the source provided the source of the Lampive initial evel that based on ourschild a do at 0000 Webb to C Dd screening tool. The annual steady-state-equivalent emission rate (D) or strotled: Day Emissions (torvisity) = (E(DVMT) ⁺ Miles per tho ⁻ Max trips ⁻ Max | by truck are base ht, unless the sur ader Standard Lit as determined b er day / 2000 (Ib. per year / 2000 | d on data from a m is greater than ft. FEL load carrie ased on maximur /ton) (Ib/ton) fay, ton/year) * (1 | similar Roxul far 40 tons, which is d weight based n daily emission - Control Efficie | s the maximum I on Cat 930K W ns. For example | heel Loader QPM10 (tp | General Purp y) = PM10 (tor | ose bucket capac | ity, throughput fro | | | approximate wei | ght of basalt rock | per cubic yard b | y Pacific Mountair | n Masonry. | | | | | | | | | | | |

Note: 1. Prever blastrade emission feder equation per AP-42 Table 13.2.5.2.1.3.Equation 2. January 2011). 2. Friended product roots surfaces all loading based on AP-42 Table 13.2.5.2.2.1.3.Tigotal SIL Control Unders with Hel Spot Contributions from Arif-Skil Abraviews. ADT Category 500-5.000. 3. Rear instraints root surfaces all loading based on AP-42 Table 13.2.5.2.1.3.Tigotal SIL Content and Loading Values for Pavel Roads at Industrial Facilities, Quarry Industry. 4. Number of days per year with precipitation greater han 0.01 Inch based on Table 8. Precipitation Zones in West Vigitals in Application Instructions and Forms for General Permit G40-C by West Virginia Department of Environmental Protection. 5. Control Elicities Content with entity elicities web and Table 8. A control web/dit.

Sample Calculations: E (Ib/vehicle mile traveled (VMT)) = [k * (sL)^0.91 * (W)^1.02] * (1 - (P/4*N)

Roxul USA Inc. dba ROCKWOOL Ranson, West Virginia Source ID: Natural Gas Boilers (CM03, CM04)

Modified units New units Removed units

Operating Parameters, PER BOILER

| Maximum Llast Innut Canasity | 1,462 | kw |
|------------------------------|-------------|-------------|
| Maximum Heat Input Capacity | 4.99 | MMBtu/hr |
| Operating Hours | 8,760 | hr/yr |
| Fuel Type | Natural Gas | |
| Fuel HHV | 1,026 | MMbtu/MMscf |
| | | |

| Maximum Potential Emissions ^{1,2} | | | U | 5 | MET | RIC |
|--|------------|------------|--------------------------------|-----------------------------------|--------------------------------|--------------------------------|
| Pollutant | Emissio | n Factor | Hourly Emissions Per Source | Annual Emissions Per Source | Hourly Emissions Per Source | Annual Emissions Per Source |
| | (lb/MMscf) | (lb/MMbtu) | (lb/hr) | (ton/yr) | (kg/hr) | (tonne/yr) |
| NO _x | 36.21 | 0.0353 | 0.18 | 0.77 | 0.08 | 0.70 |
| SO ₂ | 0.6 | 0.0006 | 2.92E-03 | 0.01 | 1.32E-03 | 0.01 |
| PM/PM _{10F} /PM _{2.5F} | 1.9 | 0.0019 | 0.01 | 0.04 | 4.19E-03 | 0.04 |
| PM _{10T} /PM _{2.5T} | 7.6 | 0.0074 | 0.04 | 0.16 | 0.02 | 0.15 |
| Condensable PM | 5.7 | 0.0056 | 0.03 | 0.12 | 0.01 | 0.11 |
| CO | 84 | 0.0819 | 0.41 | 1.79 | 0.19 | 1.62 |
| VOC | 5.5 | 0.0054 | 0.03 | 0.12 | 0.01 | 0.11 |
| Lead | 0.0005 | 4.87E-07 | 2.43E-06 | 1.07E-05 | 1.10E-06 | 9.66E-06 |
| Hexane | 1.8 | 0.0018 | 0.01 | 0.04 | 0.00 | 0.03 |
| Total HAPs | 1.89 | 0.0018 | 0.01 | 0.04 | 4.17E-03 | 0.04 |
| CO ₂ | - | 116.98 | 583.72 | 2556.68 | 264.77 | 2,319.38 |
| CH ₄ | - | 2.20E-03 | 0.01 | 0.05 | 4.99E-03 | 0.04 |
| N ₂ O | - | 2.20E-04 | 1.10E-03 | 4.82E-03 | 4.99E-04 | 4.37E-03 |
| CO ₂ e ³ | - | - | 584.32 | 2,559.32 | 265.04 | 2,321.77 |

EMISSIONS SHOWN FOR AN INDIVIDUAL EMISSION POINT (PER BOILER)

Notes:

ton = short tons

tonne = metric tons

1. Natural Gas emission factor source AP-42 Table 1.4-1, 1.4-2, 1.4-3, and 1.4-4 for SO₂, PM₁₀₁, PM_{2.57}, CO, VOC, Lead, Hexane, Total HAPs, Chromium. GHG emission factors per 40 CFR Part 98, Table C-1 and C-2. GWPs per 40 CFR 98, Table A-1. NO_x emission factor based on 30 ppmvd @ 3% O2 per manufacturer specification.

2. PM_{10T} and PM_{2.5T} emission factors include filterable and condensable particulate matter. 3. CO₂ Equivalent (CO₂e) lb/hr, ton/yr = CO₂ + [GWP_{CH4} * CH₄)] + [GWP_{N20} * N₂O].

Sample Calculations:

Hourly Emissions (lb/hr) = Emission Factor (lb/MMBtu) * Maximum Heat Input Capacity (MMBtu/hr) Annual Emissions (ton/yr) = Hourly Emissions (lb/hr) * 8,760 (hr/yr) / 2,000 (lb/ton)

Hourly Emissions (kg/hr) = Hourly Emissions (lb/hr) * 0.4535924 kg/lb

Annual Emissions (tonne/yr) = Hourly Emissions (kg/hr) * 8,760 (hr/yr) / 1,000 (kg/tonne)

Roxul USA Inc. dba ROCKWOOL Ranson, West Virginia Source ID: Emergency Fire Pump Engine (EFP1)

Modified units New units Removed units

Operating Parameters, per fire pump engine Fuel type

Diesel 316 236 Maximum Firing Rate 2.21 Operating hours 500

MMBtu/hr

hp kw

hr/yr

0.0015% Sulfur

Maximum Potential Emissions

| otential Emissions | | | | U | S | MET | RIC |
|--|---------|-----------|---|---------------------|---------------------|---------------------|---------------------|
| Pollutant | | Emission | Factor | Hourly Emissions | Annual Emissions | Hourly Emissions | Annual Emissions |
| | g/kw-hr | lb/hp-hr | Source | (lb/hr) | (ton/yr) | (kg/hr) | (tonne/yr) |
| Filterable PM/PM ₁₀ /PM _{2.5} ¹ | 0.11 | 1.81E-04 | Manufacturer Rating Data | 0.06 | 0.01 | 0.03 | 0.01 |
| PM _{10T} | - | 2.35E-04 | Filterable + Condensable | 0.07 | 0.02 | 0.03 | 0.02 |
| PM _{2.5T} | - | 2.35E-04 | Filterable + Condensable | 0.07 | 0.02 | 0.03 | 0.02 |
| Condensable PM ² | - | 5.39E-05 | AP-42, Tbl. 3.4-2 | 0.02 | 4.26E-03 | 7.73E-03 | 3.87E-03 |
| NO _x ⁴ | 3.43 | 5.639E-03 | Manufacturer Rating Data | 1.78 | 0.45 | 0.81 | 0.40 |
| CO | 0.8 | 1.315E-03 | Manufacturer Rating Data | 0.42 | 0.10 | 0.19 | 0.09 |
| SO ₂ | - | 1.09E-05 | Mass Balance | 3.44E-03 | 8.61E-04 | 1.56E-03 | 7.81E-04 |
| Combustion VOC ⁵ | 0.11 | 1.808E-04 | Manufacturer Rating Data | 0.06 | 0.01 | 0.03 | 0.01 |
| Total HAPs ² | - | 2.71E-05 | AP-42, (3.87x10 ⁻³ lb/MMBtu) | 8.58E-03 | 2.14E-03 | 3.89E-03 | 1.95E-03 |
| CO ₂ | - | 1.14 | 40 CFR 98, Tbl C-1 (73.96 kg/MMBtu) | 360.75 | 90.19 | 163.64 | 81.82 |
| CH ₄ | - | 4.63E-05 | 40 CFR 98, Tbl C-2 (3.0x10-3 kg/MMBtu) | 1.46E-02 | 3.66E-03 | 6.64E-03 | 3.32E-03 |
| N ₂ O | - | 9.25E-06 | 40 CFR 98, Tbl C-2 (6.0x10-4 kg/MMBtu) | 2.93E-03 | 7.32E-04 | 1.33E-03 | 6.64E-04 |
| CO ₂ e ³ | - | - | - | 361.99 | 90.50 | 164.20 | 82.10 |

Notes:

ton = short tons

tonne = metric tons

Conservatively assuming PM= PM₁₀, PM_{2.5}.
 Per AP-42, used average brake specific fuel consumption of 7,000 Btu/hp-hr to convert lb/MMBtu emission factors to lb/hp-hr.
 CO₂ Equivalent (CO₂e) lb/hr, ton/yr = CO₂ + [GWP_{CH4} * CH₄)] + [GWP_{N20} * N₂O]. GWPs per 40 CFR 98, Table A-1 [CO₂ = 1, CH₄ = 25, N₂O = 298].
 Conservatively assumed all NSPS NOX + NMHC limit emitted as NO_X.

5. Conservatively assumed total hydrocarbons=TOC=VOC

Sample Calculations:

Sample Calculations: Hourly Emissions (lb/hr) = Emission Factor (lb/hp-hr) * Maximum Firing Rate (hp) Annual Emissions (ton/yr) = Hourly Emissions (lb/hr) * 500 (hr/yr) / 2,000 (lb/ton) Hourly Emissions (kg/hr) = Hourly Emissions (lb/hr) * 0.4535924 kg/lb Annual Emissions (tonne/year) = Annual Emissions (ton/year) * 0.9071847 tonne/ton

Modified units New units Removed units

Operating Parameters, Curing Oven

| | Maximum Hea | t Input Capacity |
|-----------------------|-------------|------------------|
| | MW | MMBtu/hr |
| Afterburner | 2.9 | 9.86 |
| Circulation Burner #1 | | |
| | 1.7 | 5.81 |
| Circulation Burner #2 | | |
| | 1.7 | 5.81 |
| Total | 6.3 | 21.47 |
| Operating Hours | 8,400 | hr/yr |
| Fuel Type | Natural Gas | |
| Fuel HHV | 1,026 | MMbtu/MMscf |
| | | |

| Maximum Potential Emissions | | | U | 5 | M | |
|-------------------------------|--|------------|---------------------|---------------------|---------------------|---------------------|
| Pollutant | Emissio | n Factor | Hourly Emissions | Annual Emissions | Hourly Emissions | Annual Emissions |
| Ponutant | (Ib/MMscf) for SO ₂ (kg/MMBtu) for GHG | (lb/MMbtu) | (lb/hr) | (ton/yr) | (kg/hr) | (tonne/yr) |
| SO ₂ | 0.6 | 0.0006 | 0.01 | 0.05 | 5.70E-03 | 0.05 |
| Combustion - CO ₂ | 53.06 | 116.98 | 2511.69 | 10,549.09 | 1139.28 | 9,569.97 |
| Combustion - CH ₄ | 1.0E-03 | 2.20E-03 | 0.05 | 0.20 | 0.02 | 0.18 |
| Combustion - N ₂ O | 1.0E-04 | 2.20E-04 | 0.00 | 0.02 | 2.15E-03 | 0.02 |
| Process - N ₂ O | N/A | N/A | 20.06 | 84.26 | 9.1 | 76.44 |
| Total - N ₂ O | - | - | 20.07 | 84.28 | 9.10 | 76.46 |

Notes:

ton = short tons

tonne = metric tons

1. Natural Gas emission factor source AP-42 Table 1.4-2 for SO2. GHG emission factors per 40 CFR Part 98, Table C-1 and C-2. GWPs per 40 CFR 98, Table A-1.

2. Maximum g/s emissions do not vary based on model averaging period (i.e., a source permitted to operate at maximum capacity 24 hr/day, 365 day/year).

Sample Calculations:

Hourly Emissions (lb/hr) = Emission Factor (lb/MMBtu) * Maximum Heat Input Capacity (MMBtu/hr)

Annual Emissions (ton/yr) = Hourly Emissions (lb/hr) * 8,760 (hr/yr) / 2,000 (lb/ton)

Hourly Emissions (kg/hr) = Hourly Emissions (lb/hr) /2.2046 (lb/kg)

Annual Emissions (tonne/yr) = Hourly Emissions (kg/hr) * 8,760 (hr/yr) / 1,000 (kg/tonne)

Operating Parameters, Melting Furnace

| Operating Hours | 8,400 | hr/yr |
|------------------------------|-------------|-------------|
| Fuel Type | Natural Gas | |
| Maximum Heat Input Capacity | 6.8 | MW |
| Maximum ricat input Capacity | 128.48 | MMBtu/hr |
| Fuel HHV | 1,026 | MMbtu/MMscf |

100 120,000

Process CO2 Emission Factor

kg/tonne line wool tonne/yr line wool

Maximum Potential Emissions^{1,2}

| Maximum Potential Emissions ^{1,2} | | U | IS | METRIC | | | |
|--|------------|------------|---------------------|---------------------|---------------------|---------------------|--|
| Pollutant | Emissio | on Factor | Hourly Emissions | Annual Emissions | Hourly Emissions | Annual Emissions | |
| | (kg/MMBtu) | (lb/MMbtu) | (lb/hr) | (ton/yr) | (kg/hr) | (tonne/yr) | |
| NG - CO ₂ | 53.06 | 116.98 | 15,029.22 | 63,122.73 | 6.82E+03 | 57,263.99 | |
| NG - CH ₄ | 0.001 | 2.20E-03 | 0.28 | 1.19 | 0.13 | 1.08 | |
| NG - N ₂ O | 0.0001 | 2.20E-04 | 0.03 | 0.12 | 1.28E-02 | 0.11 | |
| Process - CO ₂ | N/A | N/A | 3,306.93 | 13,227.73 | 1,500.00 | 12,000.00 | |
| Total - CO ₂ | - | - | 18,336.15 | 76,350.47 | 8,317.14 | 69,263.99 | |
| Total - CH ₄ | - | - | 0.28 | 1.19 | 0.13 | 1.08 | |
| Total - N ₂ O | - | - | 0.03 | 0.12 | 0.01 | 0.11 | |

tonne = metric tons

1. GHG emission factors per 40 CFR Part 98, Table C-1 and C-2. GWPs per 40 CFR 98, Table A-1.

Sample Calculations:

Hourly Emissions (lb/hr) = Emission Factor (lb/MMBtu) * Maximum Heat Input Capacity (MMBtu/hr)

Annual Emissions (ton/yr) = Fuel HHV (MMBtu/short ton) * Fuel Usage (ton/yr) * Emission Factor (lb/MMBtu) / 2,000 (lb/ton)

Hourly Emissions (kg/hr) = Hourly Emissions (lb/hr) /2.2046 (lb/kg)

Annual Emissions (tonne/yr) = Hourly Emissions (kg/hr) * 8,760 (hr/yr) / 1,000 (kg/tonne)

Attachment O

Roxul USA Inc. dba ROCKWOOL Ranson, West Virginia Proposed Compliance Demonstration

Rockwool will maintain compliance with all monitoring, recordkeeping, and reporting (MRR) in the issued permit. Rockwool is also taking a limitation on hours and will monitor the hours of operation to ensure the facility is complying with the permit.

AIR QUALITY PERMIT NOTICE Notice of Application

Notice is given that Roxul USA, Inc. (dba ROCKWOOL) has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a Modification Permit for a mineral wool manufacturing facility located at 665 Northport Avenue, in Ranson, Jefferson County, West Virginia. The latitude and longitude coordinates are: 39.37747, -77.87844.

The applicant estimates the decreased potential to discharge the following Regulated Air Pollutants will be:

Carbon Monoxide (CO): 11.23 tons per year decrease Nitrogen Oxides (NO_x): 71.90 tons per year decrease Particulate Matter (PM): 175.37 tons per year decrease Particulate Matter 10 (PM₁₀): 80.13 tons per year decrease Particulate Matter 2.5 (PM_{2.5}): 66.80 tons per year decrease Sulfur Dioxide (SO₂): 6.11 tons per year decrease Volatile Organic Compounds (VOCs): 275.23 tons per year decrease Total Hazardous Air Pollutants (HAPs): 128.98 tons per year decrease Greenhouse Gases (as CO₂ equivalents): 30,931.87 tons per year decrease

Startup of operation under the modification permit will commence upon permit issuance. Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57th Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice. Written comments will also be received via email at DEPAirQualityPermitting@WV.gov.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 41281, during normal business hours. Dated this the 22nd day of May 2023.

By: Roxul USA, Inc. (dba ROCKWOOL) Mark Graves Director of Operations 665 Northport Avenue Ranson, WV 25430

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| TE-45 (1-3) Bindler Storing Contrained Domin Roof Biologie TE-64 Coupling Aren's Storing The Come Roof Biologie TE-65 Direct Fast Tank Horizontal Storing TE-65 Direct Fast Tank Come Roof Storing TE-647 - Greed Tank Come Roof Storing | 4.39 16.44 N/A N/A 186: 3 5 1.005 5.935 21 3.5 5 N/A N/A 453 11.41 23 0 23 1753; | 7.46 356 Normal -0.03 0.03 1.45 1204 Normal -0.03 0.03 | 2.3 Martin Modern Constraint Sectors 10, 2017 10, 20 | 11.11.22 E.510-0 0.039451047 0.027223 E.51 40.9644 E.22764 E.03956 0.946273 E.7 23.2576 E.03956 0.946275 E.7 23.2572 E.510-6 0.03945157 0.29945157 D.2 12.5556 2.450-0 0.039451567 0.299451567 0.2 1175.4697 0.1000 0.02023067 0.099915667 0.00 1175.4699 1.5000 0.02023067 0.099915667 0.00 | 5 54.65463899 130 0.00629 52834 1357.8524 0.3166 1 5 54.65463899 64.07 3.28563 4752 113.429 1 1 18.0353 20.0891506 0.3757 192024 435857343 0.3787 1 2 | Low Data Data <thd< th=""></thd<> |
| 16:03 Theme Of Instantion The Vertacula Sorge 17:022 Theme Of Instantion The 19:032 Theme Of Instantion 10:023 Theme Of Instantion The 19:042 Theme Of Instantion The 19:042 Theme Of Instantion The | 11.4.1. 23. 0 22 1.7393 5 6.5 N/A N/A 9 8 6.5 N/A N/A 9 6.56 21 N/A N/A 9397 5.149 12.35 N/A N/A 2094 | 43.7 212 kođemni 0 0 11.7 115 kođemni 0 0 15.44 2581 kođemni 0 0 45.45 1528 kođemni 0 0 | Cal Sampane Parentem Corporation International Control Co | 22,573 0.1008 22,573 0.1008 34,8844 0.0495 140,1146 0.0498 | 14.0233 26.000330 (0.2070 1.00040 0.0012) 0.2070 1.2 194 3457 306 44597 1. 0 194 3457 306 44597 1. 0 19427 4369 308 31623 1. 0 19427 4369 098 31623 1. 1 | 2112 0.00 0.01 0.00 0.00 0.00 0.00 0.00 |
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| Activity Title Climate: | TK-AD Additive Ston Pennsvivania, Harris | | om 1/1/2021 | . to 12/31/ | 2021 | | | | | | | | | |
|---|---|----------------------|--------------------|----------------------|--------------------|----------------------|--------------------|--------------------|--------------------|--------------------|----------------------|--------------------|--------------------|--|
| pa | 14.5725 psia | • | | | | | | | | | | | | |
| Equipment Tag Storage Vessel Style | TK-AD Additive Ston Cone Roof Storage | age Tank | | | | | | | | | | | | |
| Calculation Type | Normal Storage Tar | nk (11/2019 | Rev.) | | | | | | | | | | | |
| | Working and Breath | | | | | | | | | | | | | |
| Vold Space Volume Working Volume | 487.46 gai 396 gai | | | | | | | | | | | | | |
| Working Volume | 52.9375 ft^3 | | | | | | | | | | | | | |
| Shell Diameter Straight Side Height | 3.6 ft 6 ft | | | | | | | | | | | | | |
| Hro | 0.402 ft | | | | | | | | | | | | | |
| Paint Solar Absorptance | 0.25 | | | | | | | | | | | | | |
| Roof Color / Condition Shell Color / Condition | white / average white / average | | | | | | | | | | | | | |
| pbp | 0.03 | | | | | | | | | | | | | |
| pbv Equipment Comment | -0.03 | | | | | | | | | | | | | |
| Activity Comment | Imported from Exce | l on 2:55:56 | 6 PM, 5/19/20 | 022. | | | | | | | | | | |
| Pi (constant) | 3.1416 998.9 | | | | | | | | | | | | | |
| R (constant) | 330.3 | | | | | | | | | | | | | |
| Vessel Contents | | 68.000 °F | 2012.565 lb | | 109.002 lb-M | | | | | | | | | |
| Mixture Name: | Additive [Liquid] | mmHg | ь | W[I] | ІЬ-М | X[I] | A[I] | X*Pi*Al (m | nmHg) | | | | | |
| | Ethanol | 42.925 | 80.2423 | 0.039871 | 1.7417 | 0.015979 | 1 | 0.6859 | | | | | | |
| Kp (product factor) | Water 1 | 17.3515 | 1932.3231 | 0.960129 | 107.2599 | 0.984021 | 1 | 17.0742 | | | | | | |
| HI | 3.201 ft | | | | | | | | | | | | | |
| Month | | lan | Feb | Mar | Ann | May | lue | iol. | A.1.m | Sen | 0.4 | Nov | Dar | |
| Month Q | (gal) | 1458.359 | Feb 1317.2274 | Mar 1458.359 | Apr 1411.3151 | 1458.359 | 1411.315 | | Aug 1458.359 | | 1458.359 | 1411.315 | | 17171 (sum) |
| Vq | (ft^3) | 194.9542 | 176.0877 | | | 194.9542 | | 194.9542 | | 188.6654 | | 188.6654 | | 2295.429 (sum) |
| N (period) N (scaled to annual) | (number) (number) | 3.6827 43.3611 | 3.3263 43.3611 | 3.6827 43.3611 | 3.5639 43.3611 | 3.6827 43.3611 | 3.5639 43.3611 | 3.6827 43.3611 | 3.6827 43.3611 | 3.5639 43.3611 | 3.6827 43.3611 | 3.5639 43.3611 | 3.6827 43.3611 | 43.3608 (sum) |
| Kn | (number) | 0.8585 | 0.8585 | 0.8585 | 0.8585 | 0.8585 | 0.8585 | 0.8585 | 0.8585 | 0.8585 | 0.8585 | 0.8585 | 0.8585 | 0.8585 (avg) |
| Days | (number) | 31 | 28 | 31 | 30 | 31 | 30 | 31 | 31 | 30 | 31 | 30 | 31 | 365 (sum) |
| Compound Molecular Wei | | | | | | | | | | | | | | |
| Ethanol Water | (Mv) (Mv) | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 (lb/lb-male) 18.0153 (lb/lb-male) |
| | • • | 10.0133 | 10.0133 | 10.0133 | 10.0133 | 10:0133 | 10.0135 | 10.0133 | 10.0133 | 10.0133 | 16.0125 | 10.0123 | 10.0193 | TO'OTO (IN ID-IIIOIG) |
| Compound Vapor Pressure | | | | | | e | | | e | | | | | |
| Ethanol Water | (mmHg) (mmHg) | 0,1712 3,965 | 0.1934 4.5127 | 0.2871 | | 0.616 | 0.8405 21.1045 | 0.978 24.712 | 0.917 23.1091 | 0.7019 17.4902 | 0.461 11.2678 | 0.3121 7.4783 | 0.2069 | 0.509375 (avg) 12.58334 (avg) |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Working Loss Calculations | (Uncontrolled) | | | | | | | | | | | | | |
| tla tln | (*F) (*F) | 29.6088 26.2578 | 32.7413 28.8623 | 43.1801 | | 64.7897 58.8464 | 74.1836 68.1642 | 78.9011 73.0123 | 76.8843 | 68.6939 63.5422 | 56.3522 51.5831 | 45.446 41.7526 | 34.4819 31.3834 | 54.95463 (average) |
| tLx | (°F) (°F) | 32.9598 | 36.6204 | 47.8754 | | 70.733 | 80.203 | 84.7898 | 82.3809 | 53.5422 73.8456 | 61.1213 | 41.7526 | 31.3834 | 50.16028 (average) 59.74899 (average) |
| tb | ("R) | 488.6871 | | 501.7157 | | | 532.0187 | 536.7822 | 534.9704 | | 515.071 | 504.5035 | 493.6591 | 513.4392 (average) |
| pC pNc | (psia) (psia) | 0.08 14.4925 | 0.091 14.4815 | 0.138 14,4345 | | 0.3071 | 0.4245 | 0.4969 | 0.4647 14.1078 | 0.3519 14.2206 | 0.2269 14.3456 | 0.1507 | 0.0977 14.4748 | 0.253242 (average) 14.31926 (average) |
| pVa | (psia) | 0.08 | 0.091 | 0.138 | | 0.3071 | 0.4245 | 0.4969 | 0.4647 | 0.3519 | 0.2269 | 0.1507 | 0.0977 | 0.253242 (average) |
| hVo Vv | (ft) (ft^3) | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 (average) 32.582 (average) |
| wVnc | (number) | 0.0799 | 0.0794 | 0.0775 | | | 0.0715 | 0.0705 | 0.071 | 0.0726 | 0.075 | 0.0771 | 0.0791 | 0.0752 (average) |
| kE | (number) | 0.0248 | 0.0294 | 0.0367 | | 0.0502 | 0.0531 | 0.0533 | 0.0488 | 0.0436 | 0.0383 | 0.0281 | 0.0226 | 0.039492 (average) |
| tv taa | (°R) (°R) | 489.7614 488.22 | 493.0912 490.92 | 500.82 | | 525.8226 | 535.3506 | 540.0304 | 537.8465 | 529.4096 | 516./982 | 505.6156 | 494.5539 493.27 | 515.5917 (average) 512.5033 (average) |
| kb | (number) | 1 | 1 | 1 | | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| kn n | (number) (number) | 0.8585 3.6827 | 0.8585 3.3263 | 0.8585 3.6827 | | 0.8585 3.6827 | 0.8585 3.5639 | 0.8585 3.6827 | 0.8585 3.6827 | 0.8585 3.5639 | 0.8585 3.6827 | 0.8585 3.5639 | 0.8585 3.6827 | 0.8585 (average) 43.3608 (sum) |
| | | | | | | | | | | | | | | |
| Compound Vapor Density Ethanol | (vW(I)) (Ib/ft^3) | 2.90E-05 | 3.26E-05 | 4.73E-05 | 6.89E-05 | 9.72E-05 | 1.00E-04 | 2.00E-04 | 1.00E-04 | 1.00E-04 | 7.41E-05 | 5.12E-05 | 3.47E-05 | 7.79E-05 (avg) |
| Water | (lb/ft^3) | 3.00E-04 | 3.00E-04 | | | | 0.0013 | 0.0015 | 0.0014 | 0.0011 | | 5.00E-04 | | 7.83E-04 (avg) |
| Working Losses (Lw) | | | | | | | | | | | | | | |
| Air | (Ib) | 13.3804 | 11.9995 | 12.9672 | 12.2191 | 12.2873 | 11.5856 | 11.8061 | 11.8776 | 11.766 | 12.5584 | 12.4817 | 13.2323 | 148.1612 (sum) |
| Ethanol | (Ib) (Ib) | 0.0049 | 0.0049 | 0.0079 | | | 0.0211 | 0.0252 | 0.0237 | 0.0178 | 0.0124 | 0.0083 | 0.0058 | 0.1595 (sum) 1.5393 (sum) |
| Water | (Ib) | 0.044 | 0.0449 | 0.0739 | 0.1062 | 0.1577 | 0.2073 | 0.2486 | 0.2335 | 0.1737 | 0.1185 | 0.0778 | 0.0552 | T.2283 (SUM) |
| Breathing Loss Calculations | (onconcer) | | | | | | | | | | | | | |
| tan taa | (°R) (°R) | 480.87 488.22 | 482.97 490.92 | 491.67 500.82 | 500.87 511.27 | 510.77 521.47 | 520.27 530.57 | 525.27 535.37 | 523.97 533.72 | 516.17 526.07 | 504.27 514.32 | 495.77 504.02 | 486.27 493.27 | 503.2617 (avg) 512.5033 (avg) |
| tax | ("R) | 495.57 | 498.87 | 509.97 | 521.67 | 532.17 | 540.87 | 545.47 | 543.47 | 535.97 | 524.37 | 512.27 | 500.27 | 521.745 (avg) |
| tin tia | (°F) | 26.2578 29.6088 | 28.8623 32.7413 | 38.4849 43.1801 | | | 68.1642 74.1836 | 73.0123 78.9011 | 71.3878 76.8843 | 63.5422 68.6939 | 51.5831 56.3522 | 41.7526 45.446 | 31.3834 34.4819 | 50.16028 (avg) |
| tla tlx | (°F) (°F) | 29.6088 32.9598 | 32.7413 35.6204 | 43.1801 47.8754 | | 64.7897 70.733 | 74.1836 80.203 | 78,9011 84,7898 | 76.8843 82.3809 | 68.6939 73.8456 | 56.3522 61.1213 | 45.446 49.1393 | | 54.95463 (avg) 59.74899 (avg) |
| î. | (Btu/ft²day) | 622.801 | 877.2515 | 1194.204 | | | 1931.54 | 1882.997 | 1667.254 | | | | | 1247.823 (avg) |
| tb pC | (°R) (psia) | 488.6871 0.08 | 491.5779 0.091 | 501.7157 0.138 | 512.4138 0.2095 | | 532.0187 0.4245 | 536.7822 0.4969 | 534.9704 0.4647 | 527.082 0.3519 | 515.071 0.2269 | 504.5035 0.1507 | 493.6591 0.0977 | 513.4392 (avg) 0.253242 (avg) |
| pNc | (psia) | 14.4925 | 14.4815 | 14.4345 | 14.363 | 14.2654 | 14.148 | 14.0756 | 14.1078 | 14.2206 | 14.3456 | 14.4218 | 14.4748 | 14.31926 (avg) |
| pVa dPv | (psia) (psia) | 0.08 | 0.091 | 0.138 | | 0.3071 | 0.4245 | 0.4969 0.1942 | 0.4647 | 0.3519 0.1258 | 0.2269 0.0794 | 0.1507 | 0.0977 0.0246 | 0.253242 (avg) |
| dPb | (psia) (psia) | 0.0223 0.06 | 0.029 | 0.0505 | | 0.1291 | 0.1732 | 0.1942 | 0.171 0.06 | 0.06 | 0.0794 | 0.0429 | 0.0246 | 0.094033 (avg) 0.06 (avg) |
| dTv | ("R) | 13.404 | 15.5163 | 18.781 | 22.1856 | 23.7731 | 24.0777 | 23.555 | 21.9863 | 20.6067 | 19.0765 | 14.7735 | 12.3937 | 19.17745 (avg) |
| hVo ks | (ft) (number) | 3.201 0.9866 | 3.201 0.9848 | 3.201 0.9771 | | 3.201 0.9505 | 3.201 0.9328 | 3.201 0.9223 | 3.201 0.9269 | 3.201 0.9437 | 3.201 0.9629 | 3.201 0.9751 | 3.201 0.9837 | 3.201 (avg) 0.959342 (avg) |
| Vv | (ft^3) | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 (avg) |
| wVnc kE | (number) (number) | 0.0799 | 0.0794 | 0.0775 | 0.0754 | 0.0734 | 0.0715 | 0.0705 | 0.071 | 0.0726 | 0.075 | 0.0771 | 0.0791 | 0.0752 (avg) 0.039492 (avg) |
| tv | (number) (°R) | 0.0248 489.7614 | | | | 0.0502 525.8226 | | | | | | | | 0.039492 (avg) 515.5917 (avg) |
| pix pin | (psia) (psia) | 0.0918 | 0.1065 | 0.1654 | | 0.3775 | 0.5187 | 0.6022 | 0.557 | 0.4196 | 0.2696 | 0.1735 | 0.1107 | 0.304083 (avg) |
| pin | (psia) | 0.0695 | 0.0776 | 0.1148 | 0.1703 | J.2484 | 0.3455 | 0.408 | 0.386 | 0.2958 | 0.1902 | 0.1306 | 0.0861 | 0.210067 (avg) |
| Compound Vapor Density | | | | | | | | | | | | | | |
| Ethanol Water | (lb/ft^3) (lb/ft^3) | 2.90E-05 3.00E-04 | | 4.73E-05 4.00E-04 | | 9.72E-05 9.00E-04 | 1.00E-04 0.0013 | 2.00E-04 0.0015 | 1.00E-04 0.0014 | | 7.41E-05 7.00E-04 | | | 7.79E-05 (avg) 7.83E-04 (avg) |
| | , | 3.002-04 | 3.00E-04 | | 7.002-04 | 3.002-04 | 3.0013 | 3.0015 | 0.0014 | 0.0011 | 1.002-04 | 3.002-04 | 0.00E-04 | 1.00E-04 (dVg) |
| Breathing Losses (Ls) | (15) | 2.0021 | 2.1266 | 2.8717 | 3.3184 | 3.7201 | 3.7127 | 3.7954 | 3.5009 | 3.0978 | 2.9042 | 2.1138 | 1.8074 | 34 0711 /0 |
| Air Ethanoi | (lb) (lb) | 2.0021 7.00E-04 | | 2.8/1/ 0.0017 | 3.3184 0.0029 | 3.7201 | 3.7127 | 3.7954 | 3.5009 | 3.0978 0.0044 | 2.9042 | 2.1138 | | 34.9711 (sum) 4.06E-02 (sum) |
| Water | (Ib) | 0.0065 | 0.0078 | 0.016 | | 0.0454 | 0.062 | 0.0737 | 0.0638 | 0.0432 | 0.0264 | 0.0128 | 0.0072 | 0.3927 (sum) |
| Total Losses (Lt) | | | | | | | | | | | | | | |
| Alr | (Ib) | 15.3826 | 14.1261 | 15.8389 | 15.5375 | | 15.2983 | 15.6015 | 15.3785 | | 15.4626 | 14.5955 | 15.0398 | 183.1325 (sum) |
| Ethanol | (lb) (lb) | 0.0056 0.0505 | 0.0058 | 0.0096 | | 0.021 | 0.0274 0.2693 | 0.0326 | 0.0302 | 0.0223 0.2169 | 0.0152 0.1448 | 0.0097 | 0.0066 | 0.2001 (sum) 1.932 (sum) |
| Water | | | | | | | | | | | ~ | | | |

| Activity Title Climate: | TK-ADB1 Additive B Pennsylvania, Harris | | rom 1/1/202 | 1 to 12/31 | /2021 | | | | | | | | | |
|---|--|----------------------|----------------------|--------------------|---------------------|----------------------|---------------------|----------------------|--------------------|-------------------|--------------------|----------------------|---------------------|--|
| pa Equipment Tag | 14.5725 psia TK-ADB1 Additive B | | | | | | | | | | | | | |
| Storage Vessel Style | Cone Roof Storage | uneriank | | | | | | | | | | | | |
| Calculation Type | Normal Storage Tan Working and Breath | | | | | | | | | | | | | |
| Void Space Volume | 487.46 gal | ing cost ca | | | | | | | | | | | | |
| Working Volume Working Volume | 396 gal 52.9375 ft^3 | | | | | | | | | | | | | |
| Shell Diameter | 3.6 ft | | | | | | | | | | | | | |
| Straight Side Height Hro | 6 ft 0.402 ft | | | | | | | | | | | | | |
| Paint Solar Absorptance | 0.25 | | | | | | | | | | | | | |
| Roof Color / Condition Shell Color / Condition | white / average white / average | | | | | | | | | | | | | |
| pbp | 0.03 | | | | | | | | | | | | | |
| pbv Equipment Comment | -0.03 | | | | | | | | | | | | | |
| Activity Comment | Imported from Exce | | PM, 5/19/20 | 022. | | | | | | | | | | |
| Pi (constant) R (constant) | 3.1416 998.9 | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Vessel Contents Mixture Name: | 243.730 gai Additive | 68.000 °F | 2012.565 lb | | 109.002 lb-M | | | | | | | | | |
| | [Liquid] Ethanol | mmHg 42.925 | | W[I] 0.039871 | ІЬ-М | X[I] 0.015979 | A[I] 1 | X*Pi*Al (m 0.6859 | nmHg) | | | | | |
| | Water | | 1932.3231 | | | 0.984021 | | 17.0742 | | | | | | |
| Kp (product factor) HI | 1 3.201 ft | | | | | | | | | | | | | |
| n | 5.201 11 | | | | | | | | | | | | | |
| Month Q | (gal) | Jan 5520.548 | Feb 4986.3014 | Mar 5510 549 | Apr 5342.4658 | | | | Aug | Sep 5342.466 | Oct | Nov 5342.466 | Dec | 65000 (sum) |
| Vq | (ft^3) | 737.9899 | 666.5715 | 737.9899 | 714.1838 | 737.9899 | 714.1838 | 737.9899 | 737.9899 | 714.1838 | 737.9899 | 714.1838 | 737.9899 | 8689.236 (sum) |
| N (period) N (scaled to annual) | (number) (number) | 13.9408 164.1414 | 12.5917 164.1414 | 13.9408 | 13.4911 164.1414 | 13.9408 164 1414 | 13.4911 | 13.9408 164.1414 | | 13.4911 | 13.9408 | 13.4911 164.1414 | 13.9408 164.1414 | 164.1417 (sum) |
| Kn | (number) | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 (avg) |
| Days | (number) | 31 | 28 | 31 | . 30 | 31 | 30 | 31 | 31 | 30 | 31 | 30 | 31 | 365 (sum) |
| Compound Molecular We | | - | | - | | | | | | | | _ | | |
| Ethanol Water | (Mv) (Mv) | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 18.0153 | 46.07 (lb/lb-mole) 18.0153 (lb/lb-mole) |
| Compound Vapor Pressure | • • | | | | | | | | | | | | | |
| Ethanol | (mmHg) | 0.1712 | 0.1934 | 0.2871 | 0.4274 | 0.616 | 0.8405 | 0.978 | 0.917 | 0.7019 | 0.461 | 0.3121 | 0.2069 | 0.509375 (avg) |
| Water | (mmHg) | 3.965 | 4.5127 | 6.8494 | | | | | 23.1091 | | | | 4.845 | 12.58334 (avg) |
| | | | | | | | | | | | | | | |
| Working Loss Calculations | (Uncentralled) | | | | | | | | | | | | | |
| tla | (°F) | 29.6088 | 32.7413 | 43.1801 | 54.1927 | 64.7897 | 74.1836 | 78.9011 | 76.8843 | 68.5939 | 56.3522 | 45.445 | | 54.95463 (average) |
| tLn tLx | (°F) (°F) | 26.2578 32.9598 | 28.8623 36.6204 | 38.4849 47.8754 | | | 68.1642 80.203 | | 71.3878 82.3809 | | 51.5831 61.1213 | | 31.3834 37.5803 | 50.16028 (average) 59.74899 (average) |
| tb | (*R) | 488.6871 | 491.5779 | 501.7157 | 512.4138 | 522.789 | 532.0187 | 536.7822 | 534.9704 | 527.082 | 515.071 | 504.5035 | 493.6591 | 513.4392 (average) |
| pC pNc | (psla) (psia) | 0.08 14.4925 | 0.091 14,4815 | 0.138 14.4345 | | | 0.4245 14,148 | 0.4969 14.0756 | 0.4647 14.1078 | | 0.2269 14.3456 | 0.1507 14.4218 | 0.0977 14,4748 | 0.253242 (average) 14.31926 (average) |
| pVa | (psia) | 0.08 | 0.091 | 0.138 | | 0.3071 | 0.4245 | | 0,4647 | 0.3519 | 0.2269 | 0.1507 | 0.0977 | 0.253242 (average) |
| hVo Vv | (ft) (ft^3) | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 32.582 | 3.201 (average) 32.582 (average) |
| wVnc | (number) | 0.0799 | 0.0794 | 0.0775 | 0.0754 | 0.0734 | 0.0715 | 0.0705 | 0.071 | 0.0726 | 0.075 | 0.0771 | 0.0791 | 0.0752 (average) |
| kE tv | (number) (°R) | 0.0248 489.7614 | 0.0294 493.0912 | 0.0367 503.7757 | | 0.0502 525.8226 | 0.0531 535.3506 | 0.0533 | 0.0488 537.8465 | | 0.0383 | 0.0281 | 0.0226 | 0.039492 (average) 515.5917 (average) |
| taa | (°R) | 488.22 | 490.92 | 500.82 | 511.27 | 521,47 | 530.57 | 535.37 | 533.72 | 526.07 | 514.32 | 504.02 | 493.27 | 512.5033 (average) |
| kb kn | (number) (number) | 1 0.3494 | 1 0.3494 | 1 0.3494 | | 0.3494 | 1 0.3494 | 1 0.3494 | 1 0.3494 | | 1 0.3494 | 1 0.3494 | 1 0.3494 | 1 (average) 0.3494 (average) |
| n | (number) | 13.9408 | 12.5917 | 13.9408 | 13.4911 | 13.9408 | 13.4911 | 13.9408 | 13.9408 | 13.4911 | 13.9408 | 13.4911 | 13.9408 | 164.1417 (sum) |
| Compound Vapor Density | (vW(I)) | | | | | | | | | | | | | |
| Ethanol Water | (lb/ft^3) (lb/ft^3) | 2.90E-05 3.00E-04 | | 4.73E-05 | | 9.72E-05 9.00E-04 | 1.00E-04 0.0013 | 2.00E-04 0.0015 | | | | 5.12E-05 5.00E-04 | | 7.79E-05 (avg) 7.83E-04 (avg) |
| | | | | | | | 2.00.0 | 2.0013 | 0.0014 | | | | | |
| Working Losses (Lw) Air | (Ib) | 20.6158 | 18.4882 | 19.9791 | 18.8265 | 18.9315 | 17.8504 | 18.1902 | 18.3003 | 18.1284 | 19.3493 | 19.231 | 20.3875 | 228.2782 (sum) |
| Ethanol | (Ib) | 0.0075 | 0.0075 | 0.0122 | 0.0172 | 0.0251 | 0.0325 | 0.0388 | 0.0365 | 0.0275 | 0.0191 | 0.0128 | 0.009 | 0.2458 (sum) |
| Water | (Ib) | 0.0678 | 0.0692 | 0.1138 | 0.1637 | 0.2429 | 0.3194 | 0.3831 | 0.3597 | 0.2677 | 0.1825 | 0.1198 | 0.082 | 2.3716 (sum) |
| Breathing Loss Calculation | s (Uncontrolled) | | | | | | | | | | | | | |
| tan taa | (°R) (°R) | 480.87 488.22 | 482.97 490.92 | 491.67 500.82 | 500.87 511.27 | 510.77 521.47 | 520.27 530.57 | 525.27 535.37 | 523.97 533.72 | | 504.27 514.32 | 495.77 504.02 | 486.27 493.27 | 503.2617 (avg) 512.5033 (avg) |
| tax | ("R) | 495.57 | 498.87 | 509.97 | 521.67 | 532.17 | 540.87 | 545.47 | 543.47 71 3878 | 535.97 63 5422 | 524.37 51 5831 | 512.27 | 500.27 | 521.745 (avg) |
| tLn tLa | (*F) (*F) | 26.2578 29.6088 | 28.8623 32.7413 | 38.4849 43.1801 | | 58.8464 64.7897 | 68.1642 74.1836 | | , 1,20, 0 | 0010166 | 51.5831 56.3522 | 41.7526 45.446 | | 50.16028 (avg) 54.95463 (avg) |
| tLx | (°F) | 32.9598 | 35.6204 | 47.8754 | 59.7391 | 70.733 | 80.203 | 84.7898 | 82.3809 | 73.8456 | 61.1213 | 49.1393 | 37.5803 | 59.74899 (avg) |
| i tb | (Btu/ft²day) (°R) | 622.801 488.6871 | 877.2515 491.5779 | | 512.4138 | | 1931.54 532.0187 | 1882.997 535.7822 | 534.9704 | 527.082 | 515.071 | 644.6926 504.5035 | | 1247.823 (avg) 513.4392 (avg) |
| pC | (psia) | 0.08 | 0.091 14.4815 | 0.138 14,4345 | 0.2095 | 0.3071 | 0.4245 14.148 | 0.4969 14.0756 | 0.4647 14.1078 | 0.3519 | 0.2269 14.3456 | 0.1507 14.4218 | 0.0977 14.4748 | 0.253242 (avg) |
| pNc pVa | (psia) (psia) | 14.4925 0.08 | 0.091 | 0.138 | 0.2095 | 0.3071 | 14.148 0.4245 | 14.0756 0.4969 | 14.1078 0.4647 | 0.3519 | 14.3455 0.2269 | 0.1507 | 0.0977 | 14.31926 (avg) 0.253242 (avg) |
| dPv dPb | (psia) (psia) | 0.0223 0.05 | 0.029 0.05 | 0.0506 | | 0.1291 0.06 | 0.1732 0.06 | 0.1942 0.06 | 0.171 0.06 | | 0.0794 0.06 | 0.0429 | 0.0246 0.06 | 0.094033 (avg) 0.06 (avg) |
| dP0 dTv | (psia) (°R) | 13.404 | 15.5163 | 18.781 | 22.1856 | 23.7731 | 24.0777 | 23.555 | 21.9863 | 20.6067 | 19.0765 | 14.7735 | 12.3937 | 19.17745 (avg) |
| hVo ks | (ft) (number) | 3.201 0.9866 | 3.201 0.9648 | 3.201 0.9771 | | 3.201 0.9505 | 3.201 0.9328 | 3.201 0.9223 | 3.201 0.9269 | 3.201 0.9437 | 3.201 0.9629 | 3.201 0.9751 | 3.201 0.9837 | 3.201 (avg) 0.959342 (avg) |
| Vv | (ft^3) | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 (avg) |
| wVnc kE | (number) (number) | 0.0799 0.0248 | 0.0794 0.0294 | 0.0775 | 0.0754 | | 0.0715 0.0531 | 0.0705 0.0533 | 0.071 0.0488 | | 0.075 0.0383 | 0.0771 0.0281 | 0.0791 0.0226 | 0.0752 (avg) 0.039492 (avg) |
| tv | (*R) | 489.7614 | 493.0912 | 503.7757 | 515.0447 | 525.8226 | 535.3506 | 540.0304 | 537.8465 | 529.4096 | 516.7982 | 505.6156 | 494.5539 | 515.5917 (avg) |
| pix pin | (psia) (psia) | 0.0918 0.0695 | 0.1065 | 0.1654 0.1148 | | | 0.5187 0.3455 | 0.6022 | 0.557 | 0.4196 | 0.2696 0.1902 | | 0.1107 | 0.304083 (avg) 0.210067 (avg) |
| | | | 0.0770 | ~ | 0.1743 | | | J708 | 0.000 | 0.2230 | | J. 10/0 | 2.0001 | |
| Compound Vapor Density Ethanol | (wV(I)) (lb/ft^3) | 2.90E-05 | 3.26F-05 | 4.73E-05 | 6 RQF_05 | 9.72E-05 | 1.00E-04 | 2.00F-04 | 1.00E-04 | 1.00F-04 | 7.415-05 | 5.12E-05 | 3.47F-05 | 7.79E-05 (avg) |
| Water | (lb/ft^3) | 3.00E-04 | 3.00E-04 | | | 9.00E-04 | 0.0013 | 0.0015 | 0.0014 | | | 5.00E-04 | | 7.83E-04 (avg) |
| Breathing Losses (Ls) | | | | | | | | | | | | | | |
| Air | (lb) | 2.0021 | 2.1266 | 2.8717 | | 3.7201 | 3.7127 | 3.7954 | 3.5009 | | 2.9042 | | 1.8074 | 34.9711 (sum) |
| Ethanol Water | (lb) (lb) | 7.00E-04 0.0065 | 9.00E-04 0.0078 | 0.0017 | 0.0029 | 0.0047 | 0.0063 0.062 | 0.0075 | 0.0065 | 0.0044 | 0.0028 | 0.0014 0.0128 | 8.00E-04 0.0072 | 4.06E-02 (sum) 0.3927 (sum) |
| | • | | | | // | | | | | | | | | (====) |
| Total Losses (Lt) Air | (lb) | 22.6179 | 20.6148 | 22.8508 | 22.1449 | 22.6516 | 21.5631 | 21.9856 | 21.8012 | 21.2261 | 22.2534 | 21.3448 | 22.195 | 263.2492 (sum) |
| Ethanol Water | (Ib) | 0.0082 | 0.0084 | 0.0139 | 0.0201 | 0.0298 | 0.0388 | 0.0462 | 0.043 | 0.0319 | 0.0219 | 0.0142 | 0.0097 | 0.2861 (sum) |
| Water | (Ib) | 0.0743 | 0.077 | 0.1298 | 0.1916 | 0.2883 | 0.3813 | 0.4568 | 0.4235 | 0.3108 | 0.2089 | 0.192/ | 0.0892 | 2.7642 (sum) |

| Activity Title Climate: | TK-ADB2 Additive B | | rom 1/1/20 | 021 to 12/3 | 1/2021 | | | | | | | | | |
|---|--|----------------------------|----------------------------|----------------------|----------------------------|----------------------|---------------------------|---------------------|----------------------------|----------------------|--------------------------|----------------------------|----------------------------|---|
| Climate: pa | Pennsylvania, Harris 14.5725 psia | sburg | | | | | | | | | | | | |
| Equipment Tag | TK-ADB2 Additive B | uffer Tank | | | | | | | | | | | | |
| Storage Vessel Style | Cone Roof Storage | | | | | | | | | | | | | |
| Calculation Type | Normal Storage Tar Working and Breath | | | | | | | | | | | | | |
| Vold Space Volume | 166.25 gal | ing coas car | icula cion | | | | | | | | | | | |
| Working Volume | 132 gal | | | | | | | | | | | | | |
| Working Volume Shell Diameter | 17.6458 ft^3 2.6 ft | | | | | | | | | | | | | |
| Straight Side Height | 2.6 m 4 ft | | | | | | | | | | | | | |
| Нго | 0.186 ft | | | | | | | | | | | | | |
| Paint Solar Absorptance | 0.25 | | | | | | | | | | | | | |
| Roof Color / Condition Shell Color / Condition | white / average white / average | | | | | | | | | | | | | |
| pbp | white / average 0.03 | | | | | | | | | | | | | |
| pbv | -0.03 | I | | | | | | | | | | | | |
| Equipment Comment | | | | | | | | | | | | | | |
| Activity Comment Pi (constant) | Imported from Exce 3.1416 | | PM, 5/19/ | 2022. | | | | | | | | | | |
| R (constant) | 998.9 | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Vessel Contents Mixture Name: | 83.125 gai Additive | i 68.000 °F | 686.393 lb | | 37.175 lb-M | | | | | | | | | |
| Mixture Name: | [Liquid] | mmHg | lb | w[I] | Ib-M | X[I] | A[I] | X*PI*Ai (n | nmHg) | | | | | |
| | Ethanol | 42.925 | 27.3669 | 0.039671 | 0.594 | 0.015979 | 1 | 0.6859 | | | | | | |
| | Water | 17.3515 | 659.0258 | 0.960129 | 35.5814 | 0.984021 | 1 | 17.0742 | | | | | | |
| Kp (product factor) Hl | 1 2.0932 ft | | | | | | | | | | | | | |
| | 2.0002 11 | | | | | | | | | | | | | |
| Month | | | Feb | Mar | Apr | May | | Jul | Aug | | | | Dec | |
| Q. Vq | (gal) (ft^3) | 1840.211 246.0004 | TODELTER | 1840.211 246.0004 | 1780.8493 | 1840.211 246.0004 | | | 1840.211 246.0004 | 1780.849 238.0649 | 1840.211 | 1780.849 238.0649 | | 21667 (sum) 2896.456 (sum) |
| Vq N (period) | (ft^3) (number) | 246.0004 13.941 | 222.1939 12.5919 | | | 246.0004 | 238.0649 | 246.0004 13.941 | 246.0004 | | 246.0004 | 238.0649 | 246.0004 13.941 | 2896.456 (sum) 164.1441 (sum) |
| N (scaled to annual) | (number) | 164.1439 | | 164.1439 | 164.1439 | | | | 164.1439 | | | 164.1439 | | awnanta (auni) |
| Kn | (number) | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 (avg) |
| Days | (number) | 31 | 28 | 31 | 30 | 31 | 30 | 31 | 31 | 30 | 31 | 30 | 31 | 365 (sum) |
| Compound Molecular Wel | ghts (lb/lb-M) | | | | | | | | | | | | | |
| Ethanol | (Mv) | 46.07 | 46.07 | | 46.07 | 46.07 | 46.07 | 45.07 | 46.07 | | 46.07 | 46.07 | 46.07 | 46.07 (lb/lb-mole) |
| Water | (Mv) | 18.0153 | 18.0153 | | | | 18.0153 | | 18.0153 | | 18.0153 | 18.0153 | 18.0153 | 18.0153 (lb/lb-mole) |
| Compound Vapor Pressure | x (Rva) | | | | | | | | | | | | | |
| Compound vapor Pressure Ethanol | (mmHg) | 0.1712 | 0.1934 | 0.2871 | 0.4274 | 0.616 | 0.8405 | 0.978 | 0.917 | 0.7019 | 0.461 | 0.3121 | 0.2069 | 0.509375 (avg) |
| Water | (mmHg) | 3.965 | 4.5127 | 6.8494 | 10.4065 | | 21.1045 | 24.712 | 23.1091 | | 11.2678 | 7.4783 | 4.845 | 12.58334 (avg) |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Working Loss Calculations | (Uncontrolled) | | | | | | | | | | | | | |
| tla | (*F) | 29.6088 | 32.7413 | | | | 74.1836 | | | | 56.3522 | 45.446 | | 54.95463 (average) |
| tLn | (*F) | 26.2578 | 28.8623 | | | | 68.1642 | | 71.3878 | 63.5422 | 51.5831 | 41.7526 | 31.3834 | 50.16028 (average) |
| tLx tb | (°F) (°R) | 32.9598 488.6871 | 36.6204 491.5779 | 47.8754 501.7157 | 59.7391 512.4138 | 70.733 522.789 | 80.203 532.0187 | 84.7898 536.7822 | 82.3809 534.9704 | 73.8456 \$27.082 | 61.1213 515.071 | 49.1393 504.5035 | 37.5803 493.6591 | 59.74899 (average) 513.4392 (average) |
| pC | (psla) | 0.08 | 0.091 | | | 0.3071 | 0.4245 | 0.4969 | 0.4647 | 0.3519 | 0.2269 | 0.1507 | 0.0977 | 0.253242 (average) |
| pNc | (psia) | 14.4925 | 14.4815 | 14,4345 | 14.363 | 14.2654 | 14.148 | 14.0756 | 14.1078 | 14.2205 | 14.3456 | 14,4218 | 14.4748 | 14,31926 (average) |
| pVa | (psia) | 0.08 | 0.091 | 0.138 | | 0.3071 | 0.4245 | 0.4969 | 0.4647 | 0.3519 | 0.2269 | 0.1507 | 0.0977 | 0.253242 (average) |
| hVo Vv | (ft) (ft^3) | 2.0932 11.1122 | 2.0932 | | | | 2.0932 | | 2.0932 11.1122 | 2.0932 | 2.0932 | 2.0932 | 2.0932 11.1122 | 2.0932 (average) 11.1122 (average) |
| w√nc | (number) | 0.0799 | 0.0794 | | | | 0.0715 | | 0.071 | 0.0726 | 0.075 | 0.0771 | 0.0791 | 0.0752 (average) |
| kE | (number) | 0.0248 | 0.0294 | | 0.045 | | 0.0531 | | 0.0488 | 0.0436 | 0.0383 | 0.0281 | 0.0226 | 0.039492 (average) |
| tv taa | ("R) ("R) | 489.7614 488.22 | 493.0912 490.92 | 503.7757 500.82 | 515.0447 511.27 | 525.8226 521.47 | 535.3506 530.57 | 540.0304 \$35.37 | 537.8465 533.72 | 529.4096 526.07 | 516.7982 514.32 | 505.6156 504.02 | 494.5539 493.27 | 515.5917 (average) |
| kb | (number) | 400.22 | 490.92 | | | | 330.57 | | 555.72 | 528.07 | 514.52 | 304.02 | 493.27 | 512.5033 (average) 1 (average) |
| kn | (number) | 0.3494 | 0.3494 | | | | 0.3494 | | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 | 0.3494 (average) |
| n | (number) | 13.941 | 12.5919 | 13.941 | 13.4913 | 13.941 | 13.4913 | 13.941 | 13.941 | 13.4913 | 13.941 | 13.4913 | 13.941 | 164.1441 (sum) |
| Compound Vapor Density | (vw(i)) | | | | | | | | | | | | | |
| Ethanol | (lb/ft^3) | 2.90E-05 | 3.26E-05 | 4.73E-05 | 6.89E-05 | 9.72E-05 | 1.00E-04 | 2.00E-04 | 1.00E-04 | 1.00E-04 | 7.41E-05 | 5.12E-05 | 3.47E-05 | 7.79E-05 (avg) |
| Water | (lb/ft^3) | 3.00E-04 | 3.00E-04 | 4.00E-04 | 7.00E-04 | 9.00E-04 | 0.0013 | 0.0015 | 0.0014 | 0.0011 | 7.00E-04 | 5.00E-04 | 3.00E-04 | 7.83E-04 (avg) |
| | | | | | | | | | | | | | | |
| Working Losses (Lw) Air | (ІЬ) | 6.872 | 6.1628 | 6.6597 | 6.2755 | 6.3106 | 5.9502 | 6.0634 | 6.1001 | 6.0428 | 6.4498 | 6.4104 | 6,7959 | 76.0932 (sum) |
| Ethanol | (lb) | 0.0025 | 0.0025 | 0.0041 | 0.0057 | 0.0084 | 0.0108 | 0.0129 | 0.0122 | 0.0092 | 0.0064 | 0.0043 | 0.003 | 0.082 (sum) |
| Water | (њ) | 0.0226 | 0.0231 | | 0.0546 | | 0.1065 | | 0.1199 | 0.0892 | 0.0608 | 0.0399 | 0.0273 | 0.7905 (sum) |
| Breathing Loss Calculation | s (Uncontrolled) | | | | | | | | | | | | | |
| preatning Loss Calculations tan | s (Uncontrolled) (°R) | 480.87 | 482.97 | 491.67 | 500.87 | 510.77 | 520.27 | 525.27 | 523.97 | 516.17 | 504.27 | 495.77 | 486.27 | 503.2617 (avg) |
| taa | (°R) | 488.22 | 490.92 | 500.82 | 511.27 | 521.47 | 530.57 | 535.37 | 533.72 | 526.07 | 514.32 | 504.02 | 493.27 | 512.5033 (avg) |
| tax | ("R) | 495.57 | 498.87 | 509.97 | 521.67 | 532.17 | 540.87 | 545.47 | 543.47 | 535.97 | 524.37 | 512.27 | 500.27 | 521.745 (avg) |
| tLn tLa | (*F) (*F) | 26.2578 29.6088 | 28.8623 32.7413 | | 48.6463 54.1927 | 58.8464 64.7897 | 68.1642 74.1836 | | 71.3878 76.8843 | 63.5422 68.6939 | 51.5831 56.3522 | 41.7526 45.446 | 31.3834 34.4819 | 50.16028 (avg) 54.95463 (avg) |
| tla tlx | (°F) (°F) | 29.6088 32.9598 | 32.7413 | | | 64.7897 70.733 | 74.1836 80.203 | | 76.8643 62.3809 | | 56.3522 61.1213 | 45.446 49.1393 | 34.4819 37.5803 | 54.95463 (avg) 59.74899 (avg) |
| i | (Btu/ft²day) | 622.801 | 877.2515 | 1194.204 | 1525.1169 | 1758.628 | 1931.54 | 1882.997 | 1667.254 | 1349.349 | 1001.304 | 644.6926 | 518.7364 | 1247.823 (avg) |
| tb | (°R) | 488.6871 | | 501.7157 | 512.4138 | 522.789 | 532.0187 | 536.7822 | 534.9704 | 527.082 | 515.071 | 504.5035 | 493.6591 | 513.4392 (avg) |
| pC pNc | (psia) | 0.08 | 0.091 | | | 0.3071 | 0.4245 | | 0.4647 | 0.3519 | 0.2269 | 0.1507 | 0.0977 14.4748 | 0.253242 (avg) |
| pNc pVa | (psia) (psia) | 14.4925 0.08 | 14.4815 0.091 | | 14.363 0.2095 | 14.2654 0.3071 | 14.148 0.4245 | | 14.1078 0.4647 | 14.2206 0.3519 | 14.3456 0.2269 | 14.4218 0.1507 | 14.4748 0.0977 | 14.31926 (avg) 0.253242 (avg) |
| dPv | (psia) | 0.0223 | 0.029 | | 0.0863 | 0.1291 | 0.1732 | 0.1942 | 0.171 | 0.1258 | 0.0794 | 0.0429 | 0.0246 | 0.094033 (avg) |
| dPb | (psia) | 0.06 | 0.06 | 0.06 | 0.05 | 0.06 | 0.06 | | 0.06 | 0.05 | 0.06 | 0.06 | 0.05 | 0.06 (avg) |
| dTv hVo | ("R) (ft) | 13.404 2.0932 | 15.5163 2.0932 | 18.781 2.0932 | 22.1856 2.0932 | 23.7731 2.0932 | 24.0777 2.0932 | 23.555 2.0932 | 21.9863 2.0932 | 20.6067 2.0932 | 19.0765 2.0932 | 14.7735 2.0932 | 12.3937 2.0932 | 19.17745 (avg) 2.0932 (avg) |
| ks | (number) | 0.9912 | 2.0932 | | 0.9773 | 0.9671 | 0.955 | 0.9478 | 2.0552 | 0.9624 | 0.9755 | 0,9836 | 0.9893 | 0.972925 (avg) |
| Vv | (ft^3) | 11.1122 | 11.1122 | 11.1122 | 11.1122 | 11.1122 | 11.1122 | 11.1122 | 11.1122 | 11.1122 | 11.1122 | 11.1122 | 11.1122 | 11.1122 (avg) |
| wVnc | (number) | 0.0799 | 0.0794 | | 0.0754 | 0.0734 | 0.0715 | | 0.071 | 0.0726 | 0.075 | 0.0771 | 0.0791 | 0.0752 (avg) |
| kE tv | (number) (°R) | 0.0248 489.7614 | 0.0294 493.0912 | 0.0367 503.7757 | 0.045 515.0447 | 0.0502 525.8226 | 0.0531 535.3506 | 0.0533 540.0304 | 0.0488 537.8465 | 0.0436 | 0.0383 | 0.0281 505.6156 | 0.0226 494.5539 | 0.039492 (avg) 515.5917 (avg) |
| pix | (psia) | 0.0918 | 495.0912 | | | 0.3775 | 0.5187 | 0.6022 | 0.557 | 0.4196 | 0.2696 | 0.1735 | 0.1107 | 0.304083 (avg) |
| pin | (psia) | 0.0695 | 0.0776 | | | | 0.3455 | 0.408 | 0.386 | 0.2938 | 0.1902 | 0.1306 | 0.0861 | 0.210067 (avg) |
| Companyed 1/2 P ** | (| | | | | | | | | | | | | |
| Compound Vapor Density Ethanol | (wV(i)) (lb/ft^3) | 2.90E-05 | 3 765 05 | 4.73E-05 | 6 805 05 | 9.72E-05 | 1.00E-04 | 2.00E-04 | 1.00E-04 | 1.005.04 | 7.41E-05 | 5 175 05 | 3 475 05 | 7 705-05 () |
| Ethanol Water | (16/ft^3) (16/ft^3) | 2.90E-05 3.00E-04 | | 4.73E-05 4.00E-04 | | 9.72E-05 9.00E-04 | 1.00E-04 0.0013 | | 1.00E-04 0.0014 | | 7.41E-05 7.00E-04 | | | 7.79E-05 (avg) 7.83E-04 (avg) |
| | | | | | | | | | | | | | | |
| Breathing Losses (Ls) | (IL) | | | | | | | | | | | c = | | |
| Air Ethanol | (lb) (lb) | 0.6828 2.00F-04 | 0.7253 3.00E-04 | | 1.1317 | 1.2687 | 1.2662 | | 1.194 | 1.0565 | 0.9905 | 0.7209 5.00E-04 | 0.6164 3.00E-04 | 11.9268 (sum) 1.41E-02 (sum) |
| Water | (ID) (Ib) | 2.00E-04 0.0022 | 3.002-04 | 0.0055 | 0.001 | 0.0015 | 0.0022 | | 0.0023 | 0.0015 | 0.001 | 0.00E-04 | 0.0025 | 0.1354 (sum) |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Total Losses (Lt) Air Ethanol | (lb) (lb) | 7.5548 | 6.8881 | 7.6391 | 7.4073 | 7.5793 | 7.2164 | 7.3579 | 7.2941 | 7.0993 | 7.4403 | 7.1313 | 7.4123 | 88.0202 (sum) |
| | (lb) (lb) (lb) | 7.5548 0.0027 0.0248 | 6.8881 0.0028 0.0258 | 0.0047 | 7.4073 0.0067 0.0642 | 0.01 | 7.2164 0.013 0.1281 | 0.0155 | 7.2941 0.0144 0.1422 | 0.0107 | 7.4403 0.0073 0.07 | 7.1313 0.0047 0.0444 | 7.4123 0.0033 0.0298 | 88.0202 (sum) 0.0958 (sum) 0.9271 (sum) |

| Activity Title | TK-BS (1-3) Binder S | immen Contro | lear From 1 | /1/7071 to | 12/21/2021 | | | | | | | | | |
|---|---|-----------------------|----------------------|---------------------|----------------------|------------------------|---------------------|------------------------|---------------------|---------------------|---------------------|---------------------|-----------------------|--|
| Climate: pa | Pennsylvania, Harri 14.5725 psla | | iner From 14 | 1/2021 10 | 14,54,2541 | | | | | | | | | |
| Equipment Tag Storage Vessel Style | TK-BS (1-3) Binder S Dome Roof Storage | | lner | | | | | | | | | | | |
| Calculation Type | Normal Storage Ta | nk (11/2019 F | | | | | | | | | | | | |
| Void Space Volume | Working and Breat 612.72 gal | ning Loss Cak | Juation | | | | | | | | | | | |
| Working Volume Working Volume | 264 gal 35.2917 ft^3 | | | | | | | | | | | | | |
| Shell Diarneter Straight Side Height | 3.6 ft 7.8 ft | | | | | | | | | | | | | |
| Hro Paint Solar Absorptance | 0.247 ft 0.25 | 5 | | | | | | | | | | | | |
| Roof Color / Condition Shell Color / Condition | white / average white / average | | | | | | | | | | | | | |
| pbp pby | 0.03 | | | | | | | | | | | | | |
| Equipment Comment | | | | | | | | | | | | | | |
| Activity Comment Pl (constant) | Imported from Exce 3.1410 | 5 | PM, 5/19/20 | 22. | | | | | | | | | | |
| R (constant) Vessel Contents | 998. | | | | | | | | | | | | | |
| Mixture Name: | Binder Circulating | i 68.000 °F | | | 141.660 lb-M | | | | | | | | | |
| | [Liquid] Formaldehyde | 3003.344 | 2.0558 | W[I] 0.000904 | 0.0685 | 0.000483 | 1 | | imHg) | | | | | |
| | Methanol Phenol | 93.743 0 | 3.5564 | 0.000238 | 0.0378 | 0.000134 | 1 | 0.0125 0 | | | | | | |
| Kp (product factor) | Water | 17.3515 1 | 2549.7937 | 0.997567 | 141.5346 | 0.999116 | 1 | 17.3361 | | | | | | |
| н | 4.0216 ft | | | | | | | | | | | | | |
| Month Cl | (gal) | | Feb 9997.5342 | | Apr 10711.6438 | | | Jul 11058.7 | Aug 11/068.7 | | | Nov 10711.64 | Dec 11058.7 | 130325 (sum) |
| Vq N (period) | (ft^3) | 1479.67 | 1336.4759 37.8694 | 1479.67 | 1431.9385 | | 1431.939 40.5744 | 1479.67 | | 1431.939 | | 1431.939 40.5744 | 1479.67 | 17421.92 (sum) |
| N (scaled to annual) | (number) (number) | 493.6553 | 493.6553 | 493.6553 | 493.6553 | 493.6553 | 493.6553 | 493.6553 | 493.6553 | 493.6553 | 493.6553 | 493.6553 | 493.6553 | 493.6553 (sum) |
| Kn Days | (number) (number) | 0.2274 31 | 0.2274 28 | 0.2274 31 | 0.2274 30 | 0.2274 31 | 0.2274 30 | 0.2274 31 | 0.2274 31 | 0.2274 30 | 0.2274 31 | 0.2274 30 | 0.2274 31 | 0.2274 (avg) 365 (sum) |
| Compound Molecular We | | | | | | | | | | | | | | |
| Formaldehyde Methanol | (Mv) (Mv) | 30.03 32.04 | 30.03 32.04 | 30.03 32.04 | 30.03 32.04 | 30.03 32.04 | 30.03 32.04 | 30.03 32.04 | 30.03 32.04 | 30.03 32.04 | 30.03 32.04 | 30.03 32.04 | 30.03 32.04 | 30.03 (lb/lb-mole) 32.04 (lb/lb-mole) |
| Phenol Water | (Mv) (Mv) | 94.1128 18.0153 | 94.1128 18.0153 | | 94.1128 18.0153 | 94.1128 18.0153 | 94.1128 18.0153 | 94.1128 18.0153 | 94.1128 18.0153 | 94.1128 18.0153 | 94.1128 18.0153 | 94.1128 18.0153 | 94.1128 18.0153 | 94.1128 (lb/lb-mole) 18.0153 (lb/lb-mole) |
| Compound Vapor Pressu | res (Pva) | | | | | | | | | | | | | |
| Formaldehyde Methanol | (mmHg) (mmHg) | 0.7188 0.0036 | 0.7644 | 0.9329 0.0057 | 1.141 | 1.374 0.0114 | 1.6101 0.0151 | 1.7398 0.0173 | 1.6834 0.0163 | 1.4686 0.0128 | 1.1858 | 0.9731 0.0062 | 0.7907 0.0043 | 1.19855 (avg) 0.009475 (avg) |
| Methania Phenol Water | (mmHg) (mmHg) (mmHg) | 0.0056 0 4.0258 | 0.004 0 4.582 | 6.9544 | 0.0082 | 0.0114 0 15.4937 | 21.4282 | 0.01/3 0 25.0911 | 0 23.4636 | 0.0128 | 0.0088 | 0.0062 | 0.0045 0 4.9193 | 0 (avg) 0 (avg) 12.77637 (avg) |
| water | (mmrg) | 4.0258 | 4.562 | 6.9544 | 10.9661 | 15.4937 | 21.4282 | 25.0911 | 23.4636 | 17.7585 | 11.4407 | 7.595 | 4.9193 | 12.77637 (avg) |
| | | | | | | | | | | | | | | |
| Working Loss Calculations tila | (Uncontrolled) ("F) | 29.6088 | 32.7413 | 43.1801 | 54.1927 | 64.7897 | 74.1836 | 78.9011 | 76.8843 | 68.6939 | 56.3522 | 45.445 | 34.4819 | 54.95463 (average) |
| tin tix | (TF) (TF) | 26.2578 32.9598 | 28.8623 35.5204 | 38.4849 47.8754 | 48.6463 59.7391 | 58.8464 70.733 | 68.1642 80.203 | 73.0123 84.7898 | 71.3878 62.3809 | 63.5422 73.8456 | 51.5831 61.1213 | 41.7526 49.1393 | 31.3834 37.5803 | 50.16028 (average) 59.74899 (average) |
| tb pC | (*R) (psia) | 488.6871 | 491.5779 | 501.7157 | 512.4138 0.2266 | 522.789 | | | 534.9704 | 527.082 | | | 493.6591 | 513.4392 (average) 0.270483 (average) |
| pNc | (psia) | 14.4807 | 14.469 | 14.4198 | 14.3459 | 14.246 | 14.1266 | 14.0532 | 14.0858 | 14.2004 | 14.3281 | 14.4067 | 14.462 | 14.30202 (average) |
| pVa h¥o | (psia) (ft) | 0.0918 4.0216 | 0.1035 4.0216 | 0.1527 4.0216 | 0.2266 | 0.3265 4.0216 | 0.4459 4.0216 | 0.5193 4.0216 | 0.4867 4.0216 | 0.3721 4.0216 | 0.2444 4.0216 | 0.1658 4.0216 | 0.1105 4.0216 | 0.270483 (average) 4.0216 (average) |
| Vv wVnc | (ft^3) (number) | 40.9544 0.0799 | 40.9544 0.0793 | 0.0774 | 40.9544 0.0753 | 40.9544 0.0733 | 40.9544 0.0714 | 40.9544 0.0704 | 40.9544 0.0709 | 40.9544 0.0725 | 40.9544 0.0749 | 40.9544 0.077 | 40.9544 0.079 | 40.9544 (average) 0.075108 (average) |
| kE tv | (number) (*R) | 0.0249 489.7614 | 0.0295 493.0912 | 0.0368 503.7757 | 0.0452 515.0447 | 0.0504 | 0.0533 | 0.0535 540.0304 | 0.049 537.8465 | 0.0438 529.4096 | 0.0385 516.7982 | 0.0282 505.6156 | 0.0227 494.5539 | 0.03965 (average) 515.5917 (average) |
| tza kb | (*R) (number) | 486.22 1 | 490.92 1 | 500.82 1 | 511.27 1 | 521.47 1 | 530.57 1 | 535.37 1 | 533.72 1 | 526.07 1 | 514.32 1 | 504.02 1 | 493.27 1 | 512.5033 (average) 1 (average) |
| kn n | (number) (number) | 0.2274 | 0.2274 37.8694 | 0.2274 | 0.2274 | 0.2274 | 0.2274 | 0.2274 | 0.2274 | 0.2274 | 0.2274 | 0.2274 | 0.2274 | 0.2274 (average) 493.6553 (sum) |
| Compound Vapor Density | | | | | | 12.0000 | | | | | 12.2225 | | | () |
| Formaldehyde | (b/it^3) | 7.94E-05 | | 1.00E-04 | | | | | | 2.00E-04 | | | | 1.29E-04 (avg) |
| Methanol Phenol | (B/ft^3) (B/ft^3) | 4.26E-07 0 | 0 | | 0 | 0 | 1.62E-06 0 | 0 | 1.75E-06 0 | 0 | 0 | 7.05E-07 0 | 0 | 1.04E-05 (avg) 0 (avg) |
| Water | (lb/ft^3) | 3.00E-04 | 3.00E-04 | 4.00E-04 | 7.00E-04 | 0.001 | 0.0013 | 0.0015 | 0.0014 | 0.0011 | 7.00E-04 | 5.00E-04 | 3.00E-04 | 7.92E-04 (avg) |
| Warking Lasses (Lav) Air | (Ib) | 26.6816 | 24.1069 | 26.0462 | 24.5393 | 24.672 | 23.2594 | 23.7004 | 23.8446 | 23.6237 | 25.2199 | 25.0701 | 26.5821 | 297.5456 (sum) |
| Formaldehyde Methanol | (16) (16) | 0.0267 1.00E-04 | 0.0255 1.00E-04 | 0.0337 2.00E-04 | 0.039 3.00E-04 | 0.0476 4.00E-04 | 0.053 5.00E-04 | 0.0587 6.00E-04 | 0.057 6.00E-04 | 0.0489 5.00E-04 | 0.0418 3.00E-04 | 0.0339 2.00E-04 | 0.0291 2.00E-04 | 0.4949 (sum) 4.00E-09 (sum) |
| Phenol Water | (B) (B) | 0 0.0898 | 0 0.0917 | 0,1508 | 0 | 0.3219 | 0 0.4232 | 0 0.5076 | 0 0.4766 | 0.3546 | 0 0.2419 | 0.1588 | 0.1087 | 0 (sum) 3.1425 (sum) |
| Breathing Loss Calculation | | | | | | | | | | | | | | |
| tan | (77) | 480.87 | 482.97 | 491.67 | 500.87 | 510.77 | 520.27 | 525.27 | 523.97 | 516.17 | 504.27 | 495.77 | 486.27 | 503.2617 (avg) |
| taa tax | ("R) ("R) | 488.22 495.57 | 490,92 498.67 | 500.82 509.97 | 511,27 521.67 | 521.47 532.17 | 530.57 540.67 | 535.37 545.47 | 533.72 543.47 | 526.07 535.97 | 514.32 524.37 | 504.02 512.27 | 493,27 500.27 | 512,5093 (avg) 521,745 (avg) |
| tin tia | (T) (T) | 26.2578 29.6088 | 28.8623 32.7413 | | 48.6463 54.1927 | 58.8464 64.7897 | 68.1642 74.1836 | 73.0123 78.9011 | 71.3878 76.8843 | 63.5422 68.6939 | 51.5831 56.3522 | 41.7526 45.445 | 31.3834 34.4819 | 50.16028 (avg) 54.95463 (avg) |
| tLx f | ("F) (Bbu/ft ¹ day) | 32.9598 622.801 | 36.6204 877.2515 | 47.8754 1194.204 | 59.7391 1525.1169 | 70.733 1758.628 | | 64.7898 1582.997 | 82.3809 1667.254 | 73.8456 1349.349 | 61.1213 1001.304 | 49.1393 544.6925 | 37.5803 518.7364 | 59.74899 (avg) 1247.823 (avg) |
| to pC | (*R) (psia) | 488.6871 0.0918 | 491.5779 0.1035 | 501.7157 0.1527 | 512.4138 0.2266 | 522.789 0.3265 | 532.0187 0.4459 | 536.7822 0.5193 | \$34.9704 0.4867 | 527.082 0.3721 | 515.071 0.2444 | 504,5035 0.1658 | 493.6591 0.1105 | 513.4392 (avg) 0.270483 (avg) |
| pNc pVa | (psia) (psia) | 14.4807 0.0918 | 14.469 0.1035 | 14.4198 0.1527 | 14.3459 0.2266 | 14.246 | 14.1266 0.4459 | 14.0532 0.5193 | 14.0858 0.4857 | 14.2004 0.3721 | 14.3281 0.2444 | 14.4067 0.1658 | 14.462 0.1105 | 14.30202 (avg) 0.270483 (avg) |
| dPv dPb | (psia) (psia) | 0.0236 | 0.0305 | | 0.0887 | 0.1317 | 0.1757 | 0.1965 | 0.1732 | 0.128 | 0.0815 | 0.0445 | 0.0259 | 0.096033 (avg) 0.06 (avg) |
| dTv | (12) | 13.404 | 15.5163 | 18.781 | 22.1856 | 23.7731 | 24.0777 | 23.555 | 21.9863 | 20.6067 | 19.0765 | 14.7735 | 12.3937 | 19.17745 (avg) |
| h¥o ks | (ft) (number) | 4,0216 0.9808 | 4.0216 0.9784 | | 4.0216 0.9539 | 4.0216 0.9349 | 4.0216 0.9132 | 4.0216 0.9003 | 4.0216 0.906 | 4.0216 0.9265 | 4.0216 0.9505 | 4,0216 0.9659 | 4.0216 | 4.0216 (avg) 0.946325 (avg) |
| Vv wVnc | (ft^3) (number) | 40.9544 0.0799 | 40.9544 0.0793 | 0.0774 | 40.9544 0.0753 | 40.9544 0.0733 | 40.9544 0.0714 | 40.9544 0.0704 | 40.9544 0.0709 | 40.9544 0.0725 | 40.9544 0.0749 | 40.9544 0.077 | 40.9544 0.079 | 40.9544 (avg) 0.075108 (avg) |
| kE tv | (number) (*R) | 0.0249 489.7614 | 0.0295 493.0912 | 0.0368 503.7757 | 0.0452 515.0447 | 0.0504 | 0.0533 | 0.0535 | 0.049 | 0.0438 529.4096 | 0.0385 | 0.0282 | 0.0227 494.5539 | 0.03965 (avg) 515.5917 (avg) |
| pix pin | (psia) (psia) | 0.1043 | 0.1198 0.0892 | 0.181 | 0.2748 | 0.3982 | 0.5413 0.3656 | 0,6257 0.4292 | 0.5801 | 0,441 0.313 | 0.2882 0.2055 | 0.1894 | 0.1241 | 0.322325 (avg) 0.226283 (avg) |
| Compound Vapor Density | (wA(1)) | | | | | | | | | | | | | |
| Formaldehyde | (b/ft^3) | 7.94E-05 | | 1.00E-04 | | | 2.00E-04 | | 2.00E-04 | | | 1.00E-04 | | 1.29E-04 (avg) |
| Methanol Phonol | (16/ft^3) (16/ft^3) | 4.26E-07 0 | 0 | | 9.18E-07 0 | 0 | 1.62E-06 0 | 0 | 1.75E-06 0 | 1.40E-06 0 | 0 | 0 | 0 | 1.04E-06 (avg) 0 (avg) |
| Water | (b /ft^3) | 3.00E-04 | 3.00E-04 | 4.00E-04 | 7.00E-04 | 0.001 | 0.0013 | 0.0015 | 0.0014 | 0.0011 | 7,00E-04 | 5.00E-04 | 3.00E-04 | 7,92E-04 (avg) |
| Breathing Losses (Ls) Air | (Ib) | 2.5235 | 2.6804 | 3.6196 | 4.1822 | 4.6874 | 4.6763 | 4.7792 | 4.409 | 3.9028 | 3.6603 | 2.6646 | 2.2784 | 44.0637 (sum) |
| Formaldehyde Methanol | (b) (b) | 0.0025 | 0.0028 | | 0.0063 4.86E-05 | 0.0085 | 0.0097 9.71E-05 | 0.0107 | 0.0095 9.86E-05 | 0.0075 | 0.0058 4.55E-05 | 0.0035 2.36E-05 | 0.0024 | 0.0737 (sum) 6.30E-04 (sum) |
| Phenol Water | (B) (B) | 0.0083 | 0.01 | 0 | 0.0353 | 0.0572 | 0.0777 | 0 | 0.0798 | 0.0543 | 0.0334 | 0.0163 | 0.0091 | D (sum) 0.4939 (sum) |
| water Total Losses (Lt) | ,, | 0.0005 | 0.01 | 0.0203 | 0.0335 | 0.0372 | 0.0/// | 0.0922 | 0.0798 | 0.0043 | v.up94 | 0.0103 | 0.0091 | or493a (anu) |
| Air | (b) | 29.4051 | 26.7866 | | 28.7216 | | | | 28.2536 | | 28.6601 | | | 341.6093 (sum) |
| Formaldehyde Methanol | (B) (B) | 0.0292 2.00E-04 | 0.0283 2.00E-04 | | 0.0454 3.00E-04 | | 0.0627 6.00E-04 | 0.0693 7.00E-04 | 0.0665 7.00E-04 | 0.0564 5.00E-04 | 0.0475 4.00E-04 | 0.0374 3.00E-04 | 0.0316 2.00E-04 | 0.5686 (sum) 4.90E-03 (sum) |
| Phenol Water | (B) (B) | 0 0.0981 | 0 0.1017 | | 0 0.2522 | 0 0.3791 | 0 0.5009 | 0 0.5998 | 0 0.5564 | 0 0.4089 | 0 0.2752 | 0 0.1751 | 0 0.1178 | 0 (sum) 3.6363 (sum) |
| | | | | | | | | | | | | | | 4.2098 |
| | | | | | | | | | | | | | | |

| Activity Title | TK-CA Coupling A | gent Storage T | ank From 1/ | 1/2021 to : | 12/31/2021 | | | | | | | | | |
|---|-----------------------------------|----------------------|----------------------|--------------------|---------------------|----------------------|---------------------|---------------------|---------------------|--------------------|----------------------|----------------------|----------------------|--|
| Climate: pa | Pennsylvania, Hai 14.5725 psia | risburg | | | | | | | | | | | | |
| pa Equipment Tag | TK-CA Coupling A | gent Storage T | ank | | | | | | | | | | | |
| Storage Vessel Style | Cone Roof Storag | | | | | | | | | | | | | |
| Calculation Type | Normal Storage T | | | | | | | | | | | | | |
| Void Space Volume | Working and Brea 487.46 gal | athing Loss Cal | culation | | | | | | | | | | | |
| Working Volume | 396 gal | | | | | | | | | | | | | |
| Working Volume | 52.9375 ft^3 | | | | | | | | | | | | | |
| Shell Diameter Straight Side Height | 3.6 ft 6 ft | | | | | | | | | | | | | |
| Hro | 0.402 ft | | | | | | | | | | | | | |
| Paint Solar Absorptance | | 25 | | | | | | | | | | | | |
| Roof Color / Condition | white / average | | | | | | | | | | | | | |
| Shell Color / Condition pbp | white / average 0. | na | | | | | | | | | | | | |
| pbv | -0. | | | | | | | | | | | | | |
| Equipment Comment | | | | | | | | | | | | | | |
| Activity Comment Pi (constant) R (constant) | Imported from Ex 3.14 998 | 16 | PM, 5/19/20 | 022. | | | | | | | | | | |
| Vessei Contents Mixture Name: | 243.730 j Additive | gal 68.000 °F . | 2012.565 lb | | 109.002 lb-M | | | | | | | | | |
| | [Liquid] | mmHg | lb | W[I] | Ib-M | X[1] | A[I] | X*Pi*Al (m | mHg) | | | | | |
| | Ethanol | 42.925 | | 0.039871 | | 0.015979 | 1 | | | | | | | |
| Ka (amakust factor) | Water | | 1932.3231 | 0.960129 | 107.2599 | 0.984021 | 1 | 17.0742 | | | | | | |
| Kp (product factor) HI | 3.201 ft | 1 | | | | | | | | | | | | |
| | 5.202 11 | | | | | | | | | | | | | |
| Month | | | Feb | | | | | | | | | | Dec | |
| Q | (gal) (ma) | 359.0055 47.9921 | | 359.0055 | 347.4247 46.4439 | 359.0055 47.9921 | 347.4247 46.4439 | 359.0055 47.9921 | 359.0055 47.9921 | | 359.0055 47.9921 | 347.4247 46.4439 | 359.0055 47.9921 | 4227 (sum) |
| Vq N (period) | (ft^3) (number) | 47.9921 0.9066 | 43.3477 0.8188 | 47.9921 | 46.4439 | 47.9921 | 46.4439 | 47.9921 | 47.9921 | 46.4439 | 47.9921 | 45.4439 | 47.9921 | 565.068 (sum) 10.6742 (sum) |
| N (scaled to annual) | (number) | 10.6742 | 10.6742 | 10.6742 | 10.6742 | 10.6742 | 10.6742 | 10.6742 | 10.6742 | 10.6742 | 10.6742 | 10.6742 | 10.6742 | |
| Kn . | (number) | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (avg) |
| Days | (number) | 31 | 28 | 31 | 30 | 31 | 30 | 31 | 31 | 30 | 31 | 30 | 31 | 365 (sum) |
| Compound Molecular We | ights (lb/lb-M) | | | | | | | | | | | | | |
| Ethanol | (Mv) | 46.07 | 46.07 | 46.07 | 46.07 | 46.07 | 46.07 | 46.07 | 46.07 | 46.07 | 46.07 | 46.07 | 46.07 | 46.07 (lb/lb-mole) |
| Water | (Mv) | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 (lb/lb-mole) |
| Compound Vapor Pressur | es (Pva) | | | | | | | | | | | | | |
| Ethanol | (mmHg) | 0.1712 | 0.1934 | 0.2871 | 0.4274 | 0.616 | 0.8405 | 0.978 | 0.917 | 0.7019 | 0.461 | 0.3121 | 0.2069 | 0.509375 (avg) |
| Water | (mmHg) | 3.965 | 4.5127 | 6.8494 | 10.4065 | 15.2596 | 21.1045 | 24.712 | 23.1091 | 17.4902 | 11.2678 | 7.4783 | 4.845 | 12.58334 (avg) |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Working Loss Calculations | (Uncontrolled) | | | | | | | | | | | | | |
| tLa | ("F) | 29.6088 | 32.7413 | 43.1801 | 54.1927 | 64.7897 | 74.1836 | 78.9011 | 76.8843 | 68.5939 | 56.3522 | 45.446 | 34.4819 | 54.95463 (average) |
| tLn tLx | (°F) (°F) | 26.2578 32.9598 | 28.8623 36.6204 | 38.4849 47.8754 | 48.6463 59.7391 | 58.8464 70.733 | 68.1642 80.203 | 73.0123 84.7898 | 71.3878 82.3809 | 63.5422 73.8456 | 51.5831 61.1213 | 41.7526 49.1393 | 31.3834 37.5803 | 50.16028 (average) 59.74899 (average) |
| tb | ("R) | 488.6871 | 491.5779 | 501.7157 | 512,4138 | | 532.0187 | | | 527.082 | | 504.5035 | 493.6591 | 513.4392 (average) |
| pC | (psla) | 0.08 | 0.091 | 0.138 | 0.2095 | 0.3071 | 0.4245 | 0.4969 | 0.4647 | 0.3519 | 0.2269 | 0.1507 | 0.0977 | 0.253242 (average) |
| pNc | (psia) | 14.4925 | 14.4815 | | 14,363 | | 14,148 | | 14.1078 | 14.2206 | 14.3456 | 14.4218 | 14,4748 | 14.31926 (average) |
| pVa hVo | (psia) (ft) | 0.08 | 0.091 3.201 | 0.13B 3.201 | 0.2095 | 0.3071 3.201 | 0.4245 3.201 | 0.4969 | 0,4647 3,201 | 0.3519 3.201 | 0.2269 3.201 | 0.1507 3.201 | 0.0977 3.201 | 0.253242 (average) 3.201 (average) |
| Vv | (ft^3) | 32.582 | 32.582 | 32.582 | 32.582 | | 32.582 | | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 (average) |
| wVnc | (number) | 0.0799 | 0.0794 | 0.0775 | 0.0754 | 0.0734 | 0.0715 | | 0.071 | 0.0726 | 0.075 | 0.0771 | 0.0791 | 0.0752 (average) |
| kE | (number) | 0.0248 | 0.0294 | 0.0367 | 0.045 | 0.0502 | 0.0531 | 0.0533 | 0.0488 | 0.0436 | 0.0383 | 0.0281 | 0.0226 | 0.039492 (average) |
| tv taa | (°R) (°R) | 489.7614 488.22 | 493.0912 490.92 | 503.7757 500.82 | 515.0447 511.27 | 525.8226 521,47 | 535.3506 | 540.0304 535.37 | 537.8465 533.72 | 529.4096 526.07 | 516.7982 514.32 | 505.6156 504.02 | 494.5539 493.27 | 515.5917 (average) 512.5033 (average) |
| kb | (number) | | 450.52 | | | 1 | 1 | 1 | 1 | 520.07 | 1 | 1 | -55.27 | 1 (average) |
| kn | (number) | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| n | (number) | 0.9066 | 0.8188 | 0.9066 | 0.8773 | 0.9066 | 0.8773 | 0.9066 | 0.9066 | 0.8773 | 0.9066 | 0.8773 | 0.9066 | 10.6742 (sum) |
| Compound Vapor Density | (vw(I)) | | | | | | | | | | | | | |
| Ethanol | (lb/ft^3) | 2.90E-05 | 3.26E-05 | 4.73E-05 | | | | 2.00E-04 | | | | 5.12E-05 | | 7.79E-05 (avg) |
| Water | (lb/ft^3) | 3.00E-04 | 3.00E-04 | 4.00E-04 | | 9.00E-04 | 0.0013 | | 0.0014 | | | 5.00E-04 | | 7.83E-04 (avg) |
| Working Lange (1) | | | | | | | | | | | | | | |
| Working Losses (Lw) Air | (Ib) | 3.8366 | 3.4407 | 3.7181 | 3.5036 | 3.5232 | 3.322 | 3.3852 | 3,4057 | 3.3737 | 3.6009 | 3.5789 | 3.7942 | 42.4828 (sum) |
| Ethanol | (lb) | 0.0014 | 0.0014 | 0.0023 | 0.0032 | 0.0047 | 0.0061 | 0.0072 | 0.0068 | 0.0051 | 0.0035 | 0.0024 | 0.0017 | 0.0459 (sum) |
| Water | (Ib) | 0.0126 | 0.0129 | 0.0212 | 0.0305 | 0.0452 | 0.0594 | 0.0713 | 0.0669 | 0.0498 | 0.034 | 0.0223 | 0.0153 | 0.4414 (sum) |
| Breathing Loss Calculation | s (Uncontrolled) | | | | | | | | | | | | | |
| tan | ("R) | 480.87 | 482.97 | 491.67 | 500.87 | 510.77 | 520.27 | 525.27 | 523.97 | 516.17 | 504.27 | 495.77 | 486.27 | 503.2617 (avg) |
| taa | ("R) | 488.22 | 490.92 | 500.82 | 511.27 | 521.47 | 530.57 | 535.37 | 533.72 | 526.07 | 514.32 | 504.02 | 493.27 | 512.5033 (avg) |
| tax | ("R) | 495.57 | 498.87 | 509.97 | 521.67 | 532.17 | 540.87 | 545.47 | 543.47 | 535.97 | 524.37 | 512.27 | 500.27 | 521.745 (avg) |
| tLn | (*F) (*F) | 26.2578 29.6088 | 28.8623 | 38.4849 43.1801 | 48.6463 54.1927 | 58.8464 64.7897 | 68.1642 74.1836 | 73.0123 78.9011 | 71.3878 76.8843 | 63.5422 68.5939 | 51.5831 | 41.7526 | 31.3834 | 50.16028 (avg) |
| tla tix | (°F) (°F) | 29.6088 32.9598 | 32.7413 35.6204 | 43.1801 47.8754 | 54.1927 59.7391 | 64.7897 70.733 | 74.1836 80.203 | 78,9011 84,7898 | 76.8843 | 58.5939 73.8456 | 56.3522 61.1213 | 45.446 49.1393 | 34.4819 37.5803 | 54.95463 (avg) 59.74899 (avg) |
| i | (Btu/ft²day) | 622.801 | 877.2515 | | 1525.1169 | | 1931.54 | | 1667.254 | 1349.349 | 1001.304 | 644.6926 | 518.7364 | 1247.823 (avg) |
| tb | ("R) | 488.6871 | 491.5779 | 501.7157 | 512.4138 | 522.789 | 532.0187 | 536.7822 | 534.9704 | 527.082 | 515.071 | 504.5035 | 493.6591 | 513.4392 (avg) |
| pC | (psia) (esia) | 0.08 | 0.091 14.4815 | 0.138 14.4345 | 0.2095 | 0.3071 14.2654 | 0.4245 | 0.4969 14.0756 | 0.4647 14.1078 | 0.3519 | 0.2269 | 0.1507 | 0.0977 14.4748 | 0.253242 (avg) |
| pNc pVa | (psia) (psia) | 14.4925 0.08 | 14.4815 0.091 | 14.4345 0.138 | 14.363 0.2095 | 14.2654 0.3071 | 14.148 0.4245 | 14.0756 0.4969 | 14.1078 0.4647 | 14.2206 0.3519 | 14.3456 0.2269 | 14.4218 0.1507 | 14.4748 0.0977 | 14.31926 (avg) 0.253242 (avg) |
| dPv | (psia) | 0.0223 | 0.029 | 0.0506 | 0.0863 | 0.1291 | 0.1732 | 0.1942 | 0.171 | 0.1258 | 0.0794 | 0.0429 | 0.0246 | 0.094033 (avg) |
| dPb | (psia) | 0.06 | 0.05 | 0.05 | 0.06 | 0.06 | 0.05 | 0.05 | 0.06 | 0.06 | 0.06 | 0.06 | 0.06 | 0.06 (avg) |
| dTv hVo | ("R) (ft) | 13.404 3.201 | 15.5163 3.201 | 18.781 3.201 | 22.1856 3.201 | 23.7731 3.201 | 24.0777 3.201 | 23.555 3.201 | 21.9863 3.201 | 20.6067 3.201 | 19.0765 3.201 | 14.7735 3.201 | 12.3937 3.201 | 19.17745 (avg) 3.201 (avg) |
| nyo ks | (π.) (number) | 0.9866 | 0.9848 | 0.9771 | 0.9657 | 0.9505 | 0.9328 | 0.9223 | 0.9269 | 0.9437 | 0.9629 | 0.9751 | 3.201 0.9837 | 3.201 (avg) 0.959342 (avg) |
| Vv | (ft^3) | 32.582 | 32.582 | 32.582 | 32.582 | 32.5B2 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 | 32.582 (avg) |
| wVnc | (number) | 0.0799 | 0.0794 | 0.0775 | 0.0754 | 0.0734 | 0.0715 | 0.0705 | 0.071 | 0.0726 | 0.075 | 0.0771 | 0.0791 | 0.0752 (avg) |
| kE tv | (number) (°R) | 0.0248 489.7614 | 0.0294 493.0912 | 0.0367 503.7757 | 0.045 | | 0.0531 | 0.0533 540.0304 | 0.0488 | 0.0436 | 0.0383 | 0.0281 | 0.0226 | 0.039492 (avg) 515.5917 (avg) |
| pix | (psia) | 0.0918 | 493.0912 | 0.1654 | 0.2565 | 0.3775 | 0.5187 | 0.6022 | 0.557 | 0.4196 | 0.2696 | 0.1735 | 494.5539 | 0.304083 (avg) |
| pin | (psia) | 0.0695 | 0.0776 | | 0.1703 | | 0.3455 | | 0.386 | 0.2938 | 0.1902 | 0.1305 | 0.0861 | 0.210067 (avg) |
| Compound Very- De- 1 | (martin) | | | | | | | | | | | | | |
| Compound Vapor Density Ethanol | | 2 005 05 | 3 76F //F | 4.73E-05 | 6 BOC OF | 9 775 05 | 1.005.04 | 2 005 04 | 1.005.04 | 1.005.04 | 7 /15 05 | 5 125 05 | 3 475.05 | 7 705-05 (200-) |
| Ethanol Water | (lb/ft^3) (lb/ft^3) | 2.90E-05 3.00E-04 | 3.26E-05 3.00E-04 | | | 9.72E-05 9.00E-04 | 1.00E-04 0.0013 | 2.00E-04 0.0015 | 1.00E-04 0.0014 | | 7.41E-05 7.00E-04 | 5.12E-05 5.00E-04 | 3.47E-05 3.00E-04 | 7.79E-05 (avg) 7.83E-04 (avg) |
| | | | | | | | | | | | | | - / | |
| Breathing Losses (Ls) | (16) | | | | | | | | | | | | | 34 0744 / * |
| Air Ethanol | (lb) (lb) | 2.0021 7.00E-04 | 2.1266 9.00E-04 | 2.8717 0.0017 | 3.3184 0.0029 | 3.7201 0.0047 | 3.7127 0.0063 | 3.7954 0.0075 | 3.5009 0.0065 | 3.0978 0.0044 | 2.9042 0.0028 | 2.1138 0.0014 | 1.8074 8.00E-04 | 34.9711 (sum) 4.06E-02 (sum) |
| Water | (Ib) (Ib) | 0.0065 | 0.0078 | 0.0017 | 0.0279 | 0.0454 | 0.0063 | 0.00737 | 0.0638 | 0.0044 | 0.0264 | 0.0014 | 0.0072 | 4.06E-02 (sum) 0.3927 (sum) |
| | | - | | | | - | - | - | - | _ | - | - | | |
| Total Losses (Lt) | (15) | F 0307 | E 5674 | 6 1000 | £ 077 | 7 7494 | 7 /247 | 7 1000 | 6 0000 | 6 4745 | 6 5054 | 5 5000 | 5 6010 | 77 4641 () |
| Air Ethanol | (lb) (lb) | 5.8387 0.0021 | 5.5673 0.0023 | 6.5899 0.004 | 6.822 0.0061 | 7.2433 0.0094 | 7.0347 0.0124 | 7.1806 0.0147 | 6.9066 0.0133 | 6.4715 0.0095 | 6.5051 0.0063 | 5.6928 0.0038 | 5.6016 0.0024 | 77.4541 (sum) 0.0863 (sum) |
| Water | (Ib) (Ib) | 0.0191 | 0.0223 | 0.0372 | 0.0583 | | 0.1214 | 0.145 | 0.1307 | 0.093 | 0.0603 | 0.0351 | 0.0024 | 0.8338 (sum) |
| | | | | | | | | | | | | | | |

| Activity Title | TK-DF Diesel Fuel Tar | k From 1/: | 1/2021 to 12/ | 31/2021 | | | | | | | | | | |
|---|---|--------------------|---------------|--------------------|--------------------|--------------------|----------------------|----------------|-----------------|----------------------|--------------------|-------------------|------------------|--|
| Climate: | Pennsylvania, Harris | | | - | | | | | | | | | | |
| ра | 14.5725 psia | | | | | | | | | | | | | |
| Equipment Tag | TK-DF Diesel Fuel Tar | ık | | | | | | | | | | | | |
| Storage Vessel Style | Horizontal Storage | | | | | | | | | | | | | |
| Calculation Type | Normal Storage Tani Working and Breath | | | | | | | | | | | | | |
| Void Space Volume | 1861.45 gal | IIIB LOSS CA | | | | | | | | | | | | |
| Working Volume | 1204 gal | | | | | | | | | | | | | |
| Working Volume | 160.9514 ft^3 | | | | | | | | | | | | | |
| Shell Diameter | 4.39 ft | | | | | | | | | | | | | |
| Straight Side Height | 16.44 ft | | | | | | | | | | | | | |
| Paint Solar Absorptance | 0.25 | | | | | | | | | | | | | |
| Roof Color / Condition Shell Color / Condition | white / average white / average | | | | | | | | | | | | | |
| pbp | white / average 0.03 | | | | | | | | | | | | | |
| pbv | -0.03 | | | | | | | | | | | | | |
| Equipment Comment | | | | | | | | | | | | | | |
| Activity Comment | Imported from Excel | on 2:55:56 | 6 PM, 5/19/20 | 22. | | | | | | | | | | |
| Pi (constant) | 3.1416 | | | | | | | | | | | | | |
| R (constant) | 998.9 | | | | | | | | | | | | | |
| Vessel Contents | 930.725 ga | 68.000 °F | 6608.144 lb | | 50.832 lb-M | | | | | | | | | |
| Mixture Name: | Mixture | | | | | | | | | | | | | |
| | [Liquid] | mmHg | lb | W[i] | lb-M | X[i] | A[i] | X*Pi*Ai (m | nmHg) | | | | | |
| | Distillate Fuel Oil No | 0.4359 | 6608.144 | 1 | 50.8319 | 1 | 1 | 0.4359 | | | | | | |
| Kp (product factor) | 1 | | | | | | | | | | | | | |
| Month | | Jan | Feb | Mar | Apr | May | Jun | Jul | A | Sep | Oct | Nov | Dec | |
| Q | (gal) | | 4053.0192 | | • | | | | Aug 4487 271 | • | | | | 52834 (sum) |
| Vq | (ft^3) | 599.8609 | | | | | 4342.321 580.5106 | | | 4342.321 580.5106 | | | | 7062.879 (sum) |
| N (period) | (number) | 3.727 | | 3.727 | 3.6067 | 3.727 | | 3.727 | 3.727 | | 3.727 | 3.6067 | 3.727 | 43.8821 (sum) |
| N (scaled to annual) | (number) | 43.8821 | 43.8821 | 43.8821 | 43.8821 | 43.8821 | 43.8821 | | 43.8821 | 43.8821 | 43.8821 | 43.8821 | 43.8821 | |
| Kn | (number) | 0.8503 | | 0.8503 | 0.8503 | 0.8503 | | 0.8503 | 0.8503 | | | 0.8503 | | 0.8503 (avg) |
| Days | (number) | 31 | 28 | 31 | 30 | 31 | 30 | 31 | 31 | 30 | 31 | 30 | 31 | 365 (sum) |
| Compound Molecular Wei | abre (ib/ib.a.e) | | | | | | | | | | | | | |
| Distillate Fuel Oil No. 2 | gmcs(ib/ib-ivi) (Mv) | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 (lb/lb-mole) |
| Distillate Fuel Oil NO. 2 | (iviv) | 130 | 130 | 150 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 (10/10-11012) |
| Compound Vapor Pressure | :s (Pva) | | | | | | | | | | | | | |
| Distillate Fuel Oil No. 2 | (mmHg) | 0.1054 | 0.12 | 0.1812 | 0.2719 | 0.392 | 0.532 | 0.6164 | 0.5791 | 0.4459 | 0.2935 | 0.1974 | 0.1288 | 0.321967 (avg) |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Westing Lass Calculations (| () in combine () and) | | | | | | | | | | | | | |
| Working Loss Calculations (tLa | | 29.6088 | 32.7413 | 43.1801 | E4 1007 | 64.7897 | 74.1836 | 78.9011 | 76.8843 | 68.6939 | 56.3522 | 45.446 | 34.4819 | 54.95463 (average) |
| tin | (°F) (°F) | 29.6088 | | 38,4849 | | | | | 70,8643 | | 51.5831 | | | 50.16028 (average) |
| tix | (°F) | 32.9598 | | 47.8754 | 59.7391 | 70.733 | 80.203 | 84.7898 | 82.3809 | | | 49.1393 | 37.5803 | 59.74899 (average) |
| tb | ("R) | 488.6871 | | | 512.4138 | | | 536.7822 | | | | 504.5035 | | 513.4392 (average) |
| рC | (psia) | 0.002 | | 0.0035 | 0.0053 | | 0.0103 | 0.0119 | 0.0112 | | | 0.0038 | 0.0025 | 0.006225 (average) |
| pNc | (psia) | 14.5705 | 14.5702 | 14.569 | 14.5672 | 14.5649 | 14.5622 | 14.5606 | | | 14.5668 | 14.5687 | 14.57 | 14.56628 (average) |
| pVa | (psia) | 0.002 | 0.0023 | 0.0035 | 0.0053 | 0.0076 | 0.0103 | 0.0119 | 0.0112 | 0.0086 | 0.0057 | 0.0038 | 0.0025 | 0.006225 (average) |
| hVo | (ft) | 1.7239 | | 1.7239 | 1.7239 | 1.7239 | 1.7239 | 1.7239 | 1.7239 | 1.7239 | | 1.7239 | 1.7239 | 1.7239 (average) |
| Vv | (ft^3) | 124.4716 | | | | | | | | 124.4716 | | | | 124.4716 (average) |
| wVnc | (number) | 0.0804 | | 0.0782 | | 0.075 | 0.0736 | 0.073 | 0.0732 | | | 0.0778 | 0.0796 | 0.076483 (average) |
| kE | (number) | 0.0233 | | 0.0333 | 0.0392 | | 0.0413 | 0.0399 | | | 0.033 | 0.0252 | 0.021 | 0.0331 (average) |
| tv taa | (°R) (°R) | 489.7614 488.22 | | 503.7757 | | | 535.3506 | 540.0304 | | 529,4096 526.07 | | 505.6156 | | 515.5917 (average) 512.5033 (average) |
| kb | (number) | 400.22 | 450.52 | 1 | 1 | 521,47 | 1 | 1 | 1 | 520.07 | 1 | 1 | 455.27 | 1 (average) |
| kn | (number) | 0.8503 | | 0.8503 | 0.8503 | | | 0.8503 | | | | 0.8503 | 0.8503 | 0.8503 (average) |
| n | (number) | 3.727 | | 3.727 | 3.6067 | 3.727 | 3.6067 | 3.727 | 3.727 | | 3.727 | 3.6067 | 3.727 | 43.8821 (sum) |
| | | | | | | | | | | | | | | |
| Compound Vapor Density | | | | | | | | | | | | | | |
| Distillate Fuel Oil No. 2 | (lb/ft^3) | 5.04E-05 | 5.70E-05 | 8.42E-05 | 1.00E-04 | 2.00E-04 | 2.00E-04 | 3.00E-04 | 3.00E-04 | 2.00E-04 | 1.00E-04 | 9.15E-05 | 6.10E-05 | 1,45E-04 (avg) |
| Working Losses (Lw) | | | | | | | | | | | | | | |
| Air | (lb) | 40.9962 | 36.7926 | 39.8858 | 37.7674 | 38.2316 | 36.3406 | 37.2188 | 37.3606 | 36.7223 | 38.8618 | 38.4251 | 40.5907 | 459.1935 (sum) |
| Distillate Fuel Oil No. 2 | (Ib) | 0.0257 | | 0.043 | | | 0.1149 | 0.1364 | | | | 0.0451 | 0.0311 | 0.8666 (sum) |
| | - | - | - | | | _ | - | | | | - | - | - | · · |
| Breathing Loss Calculations | | | | | | | | | | | | | | |
| tan | (°R) | 480.87 | | 491.67 | 500.87 | 510.77 | 520.27 | 525.27 | | | | 495.77 | 486.27 | 503.2617 (avg) |
| taa | (°R) | 488.22 | | 500.82 | | | 530.57 | 535.37 | 533.72 | | | 504.02 | 493.27 | 512.5033 (avg) |
| tax | (*R) (*5) | 495.57 | 498.87 | 509.97 | 521.67 | | 540.87 | 545.47 | 543.47 | | | 512.27 | 500.27 | 521.745 (avg) |
| tin tia | (°F) (°F) | 26.2578 29.6088 | | 38.4849 43.1801 | 48.6463 54.1927 | 58.8464 64.7897 | 68.1642 74.1836 | | | | 51.5831 56.3522 | 41.7526 45.446 | | 50.16028 (avg) 54.95463 (avg) |
| ti.a | (°F) | 29.6088 | | 43.1801 47.8754 | 54.1927 | | 74.1836 | | | | 61.1213 | | | 54.95463 (avg) 59.74899 (avg) |
| i | (Btu/ft²day) | 622.801 | | | | | | | | 1349.349 | | | | 1247.823 (avg) |
| ъ | (°R) | 488.6871 | 491.5779 | 501.7157 | 512.4138 | 522.789 | 532.0187 | 536.7822 | 534.9704 | 527.082 | 515.071 | 504.5035 | 493.6591 | 513.4392 (avg) |
| рC | (psia) | 0.002 | | 0.0035 | 0.0053 | 0.0076 | 0.0103 | 0.0119 | 0.0112 | | | 0.0038 | 0.0025 | 0.006225 (avg) |
| pNc | (psia) | 14.5705 | | 14.569 | 14.5672 | | | | | | | | 14.57 | 14.56628 (avg) |
| pVa Jou | (psia) | 0.002 | | 0.0035 | | | | 0.0119 | 0.0112 | | | 0.0038 | | 0.006225 (avg) |
| dPv dPb | (psia) (psia) | 6.00E-04 0.06 | | 0.0013 0.06 | 0.0021 | 0.003 | 0.0039 0.06 | 0.0043 0.06 | 0.0038 0.06 | | | 0.0011 0.06 | 6.00E-04 0.06 | 2.18E-03 (avg) 0.06 (avg) |
| dPo dTv | (psia) (°R) | 13.404 | | 18.781 | | 23.7731 | | 23.555 | | | | | | 19.17745 (avg) |
| hVo | (ft) | 1.7239 | 1.7239 | 1.7239 | 1.7239 | | 1.7239 | 1.7239 | 1.7239 | | | 14.7735 | | 1.7239 (avg) |
| ks | (number) | 0.9998 | | 0.9997 | 0.9995 | | 0.9991 | 0.9989 | 0.999 | | | 0.9997 | 0.9998 | 0.999442 (avg) |
| W | (ft^3) | 124.4716 | 124.4716 | | | | | | | 124.4716 | | | | 124.4716 (avg) |
| wVnc | (number) | 0.0804 | 0.0799 | 0.0782 | 0.0765 | | | 0.073 | | | | 0.0778 | | 0.076483 (avg) |
| kE | (number) | 0.0233 | | 0.0333 | 0.0392 | | | 0.0399 | 0.0371 | | 0.033 | 0.0252 | 0.021 | 0.0331 (avg) |
| tv | (°R) | 489.7614 | | | | | | | | 529.4096 | | | | 515.5917 (avg) |
| pix pin | (psia) (psia) | 0.0023 0.0018 | | 0.0042 | 0.0064 0.0043 | | 0.0124 0.0085 | 0.0142 0.0099 | | | | 0.0044 0.0033 | | 0.0074 (avg) 0.005217 (avg) |
| P | (Inc.) | 0.0018 | 0.002 | 0.0029 | 0.0043 | 0.0002 | 0.0005 | 0.0099 | 0.0094 | 0.0075 | 0.0046 | 0.0033 | 5.0022 | 0.003211 (QAR) |
| Compound Vapor Density i | (w∀(i)) | | | | | | | | | | | | | |
| Distillate Fuel Oil No. 2 | (lb/ft^3) | 5.04E-05 | 5.70E-05 | 8.42E-05 | 1.00E-04 | 2.00E-04 | 2.00E-04 | 3.00E-04 | 3.00E-04 | 2.00E-04 | 1.00E-04 | 9.15E-05 | 6.10E-05 | 1.45E-04 (avg) |
| | | | | | | | | | | | | | | |
| Breathing Losses (Ls) | <i>a</i> | | | | | | | • | | | | - | _ | |
| Air Bhailtean Frank Off No. 2 | (Ib) | 7.2312 | | | | 11.9784 | | | | | | 7.3258 | 6.45 | 114.3862 (sum) |
| Distiliate Fuel Oil No. 2 | (lb) | 0.0045 | 0.0055 | 0.0108 | 0.0181 | 0.0279 | 0.0358 | 0.0411 | 0.0361 | 0.0258 | 0.0169 | 0.0086 | 0.0049 | 0.236 (sum) |
| Total Losses (Lt) | | | | | | | | | | | | | | |
| Air | (lb) | 48.2274 | 44,4309 | 49.9386 | 48.9665 | 50.2101 | 47.681 | 48.4565 | 47.8517 | 46.4678 | 48.5576 | 45.7509 | 47.0407 | 573.5797 (sum) |
| Distillate Fuel Oil No. 2 | (lb) | 0.0303 | | 0.0538 | 0.0791 | | 0.1507 | 0.1775 | | | | 0.0538 | 0.0361 | 1.1027 (sum) |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | 1 1027 |

| vig (m3) 3998800 5908.000 5908.000 5908.000 5908.000 500.00000 500.0000 500.0000 500.000 500.000 500.000 500.000 500.0000 500.000 500 | | | | | | | | | | | | | | | |
|---|----------------------------|---------------------|--------------|--------------|------------|------------|----------|----------|----------|----------|----------|----------|----------|----------|--|
| | Activity Title | TK-DOD De-dust oil | day tank Fr | om 1/1/2021 | to 12/31/2 | 2021 | | | | | | | | | |
| | Climate: | | sburg | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | |
| | | | day tank | | | | | | | | | | | | |
| Weaking Yoolan Signed Yoolan SigneYoolan Signed Yoolan Signed Yo | | | + (11/2010 | (Rev.) | | | | | | | | | | | |
| Vale Start Vale 232.1 af Vale Start Vale 30.5 h Vale Start Vale Vale Vale Vale Vale Vale Vale Vale | | | | | | | | | | | | | | | |
| Wathy Wathy 35.357.75 Problem Processor 33 Problem Processor 33.5 Problem Processor 33.5 < | Void Space Volume | | | | | | | | | | | | | | |
| Shel Djamen 1 30 S Har Star Market M | Working Volume | 264 gal | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | |
| Int Description Description Subject State Sta | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | |
| Description Mark / scrapt by bolicati / Control Mark / scrapt by bolicati / Control Scrapt / Scrapt by bolicati / Control Scrapt / Scrapt by bolicati / Scrapt by bolicati / Scrapt / | | ***** | | | | | | | | | | | | | |
| Shel Color Jonation and Terretories and 25.55 PM 5/19/2002. Sequence of the line and 25.55 PM 5/19/2002. A conversion of the line and 25.55 PM 5/19/2002. | | | | | | | | | | | | | | | |
| php 0.03 Construction Description | | | | | | | | | | | | | | | |
| bis de la construit de la | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | |
| Athly Convent Bus and | | | | | | | | | | | | | | | |
| NameNot by DescriptionNot by DescriptionNo | Activity Comment | Imported from Exce | l on 2:55:57 | 7 PM, 5/19/2 | 022. | | | | | | | | | | |
| Lat. During in the control i | PI (constant) | | | | | | | | | | | | | | |
| | R (constant) | 998.9 | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | |
| Liquid method is Will M.M. XIII AVIII XIIIII A VIIII A VIIIIA Sprakulet Two 1 2.657 h. 1 0.453 1 0.267 h. 500 model to the second t | | | i 68.000 *F | 1001.454 | 6 | 7.703 Ib-M | | | | | | | | | |
| Distance Processing Distance Processing <thdistance processing<="" th=""> Distance Processing</thdistance> | Mixture Name: | | | | | | win | 4.513 | | | | | | | |
| | | | | | | | | | | Imag | | | | | |
| H 2,4575 K Oct: Name Feb Mor Are May Name See Col Nave Deci O (m ²) See | Kn (product factor) | | | 1001.4545 | 1 | 7.7035 | 1 | 1 | 0.4359 | | | | | | |
| North Jah Part North No | | _ | | | | | | | | | | | | | |
| Q Image Ima | | 2.007510 | | | | | | | | | | | | | |
| Q Image Ima | Month | | Jan | Feb | Mar | Apr | Мау | Jun | Jul | Aug | Sep | Oct | Nov | Dec | |
| vq (m) 99.8600 59.8400 59.8400 59.8400 59.8400 59.8400 59.8400 59.8400 59.8400 59.8400 59.8400 59.8400 59.8400 59.8400 59.8400 59.8400 59.8400 50.8500 50.850 50.850 50.850 50.850 50.850 50.850 50.850 50.850 50.850 50.850 50.850 50.8500 50.8500 50.8500 | | (gal) | | | | | | | | 4487.271 | | | | | 52834 (sum) |
| M (sake annual) (number) 200.128 | | (ft^3) | 599.8609 | | 599.8609 | | | | | | | | | | 7062.879 (sum) |
| n pumber) 0.316 0 | | | | | | | | | | | | | | | 200.1283 (sum) |
| Days (muther) 31 28 31 30 31 30 31 30 31 30 31 30 31 30 31 30 31 30 31 30 31 30 30 30 30 30 30 30 30 30 30 30 30 30 30 130 | | | | | | | | | | | | | | | |
| Compound Modelative Weight (By/Let) Distance of New 2 (M) 130 | | | | | | | | | | | | | | | 0.3166 (avg) |
| Distlike Prior Distlik | uays | (number) | 31 | 28 | 31 | 30 | 31 | 30 | 31 | 31 | 30 | 31 | 30 | 31 | 365 (sum) |
| Distlike Prior Distlik | Compound Mala advanta | labor file file and | | | | | | | | | | | | | |
| Compand Mapor Presures (PM) 0.105 0.12 0.121 0.2719 0.392 0.532 0.616 0.5791 0.4499 0.2395 0.1374 0.1286 0.31197 (J Company Mark 100 No.2 (mmmd) 0.1054 0.127 0.127 0.127 0.128 0.127 0.128 0.127 0.128 | | | 120 | 120 | 170 | 120 | 120 | 130 | 170 | 176 | 120 | 170 | 120 | 170 | 120 (15 (15 |
| Distlike Fuel Oil Ro.2 (mmkg) 0.1054 0.12 0.1212 0.212 0.212 0.322 0.512 0.5144 0.778 0.4459 0.2295 0.1374 0.1288 0.32187 (Working Loss Cloakettoms [Uncontrolled] Lit (T) 22.5078 28.4674 64.7897 7.1186 78.9011 76.8431 68.6939 55.5521 45.444 34.4493 54.95461 57.957 55.957 55.957 55.957 55.957 55.957 55.957 55.977 | ensunate ruei VII NO. Z | (.a.a) | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 | 130 (lb/lb-mole) |
| Disklike Fuel Oil Ho.2 (mmHg) 0.1054 0.22 0.322 0.322 0.522 0.5144 0.5791 0.4459 0.2295 0.1374 0.1288 0.33167 (Working Loss Cabulations [Uncontrolled] Lit (F) 25.0581 37.413 41.1801 54.1927 64.7897 74.1816 78.0011 76.8843 68.6939 55.5521 45.444 34.4419 54.95461 35.0278 35.033 35.733 35.033 57.7350 35.033 57.7350 35.033 57.7350 35.033 57.7350 35.033 57.7350 55.037 35.037 35.033 57.7350 55.037 35.03 | Compound Vapor Pressur | res (Pva) | | | | | | | | | | | | | |
| Worke Loss Cabulations (Uncontrolled) Status (*) 25.552 35.452 35.452 35.452 35.452 35.448 35.4651 55.552 45.5461 55.552 45.5461 55.552 45.5461 55.552 45.5461 55.552 45.5461 55.552 45.5461 55.552 45.5461 55.552 45.575 55.552 45.755 55.755 55.552 45.757 55.741 55.861 15.557 15.557 55.557 | | | 0.1054 | 0.12 | 0.1812 | 0.2719 | 0.392 | 0.532 | 0.6164 | 0.5791 | 0.4459 | 0.2935 | 0.1974 | 0.1288 | 0.321967 (avg) |
| Li (P) 22.008 32.7413 43.8801 54.1327 67.7897 74.1386 75.8487 86.849 46.645 58.466 64.645 58.466 58.466 58.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 45.445 55.4551 45.4551 45.555 15.4555 55.752 45.475 55.772 45.475 15.4551 15.555 15.557 15.557 15.557 | | | | | | | | | | | | | | | |
| Li (P) 22.008 32.7413 43.8801 54.1327 67.7897 74.1386 75.8487 86.849 46.645 58.466 64.645 58.466 58.466 58.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 45.445 55.4551 45.4551 45.555 15.4555 55.752 45.475 55.772 45.475 15.4551 15.555 15.557 15.557 15.557 | | | | | | | | | | | | | | | |
| Li (P) 22.008 32.7413 43.8801 54.1327 67.7897 74.1386 75.8487 86.849 46.645 58.466 64.645 58.466 58.466 58.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 55.4521 45.445 45.445 55.4551 45.4551 45.555 15.4555 55.752 45.475 55.772 45.475 15.4551 15.555 15.557 15.557 15.557 | | | | | | | | | | | | | | | |
| tin (P) Z.5.278 Z.8673 Z.84673 R.46665 S.8466 G.1627 20123 T.13776 E.13426 L.17556 S.13381 S.016276 (e) tin (P) Z.86674 Z.5778 S.7378 G.738 G.738 G.738 G.738 G.738 G.738 G.7387 G.738 G.7387 G.7387 G.7387 G.7387 G.738 G.7387 G.738 G.7387 G.737 G | | | | | | | | | | | | | | | |
| Li. (m) 12.9398 56.2204 74.737.4 59.748916 12.131 41.139 37.3403 57.3408 57.1418 57.743 57.743 57.743 57.743 57.743 57.743 57.743 57.743 57.743 57.743 57.745 57.745 57.745 57.745 57.745 57.745 57.745 57.745 57.745 57.745 57.745 57.745 57.745 57.745 57.745 57.75 5 | | | | | | | | | | | | | | | 54.95463 (average) |
| ti (%) (#8671 491.775 51.7157 512.4138 527.78 532.0187 582.782 532.0187 502.785 72.028 515.071 505.058 493.6591 145.669 145.671 45.70 50.038 0.0023 0.0035 0.0038 0.0130 0.013 0.0112 0.0066 0.0057 0.0038 0.0120 0.0025 (phc (pink) 14.775 14.770 14.569 14.5 | | | | | | | | | | | | | | | 50.16028 (average) |
| pc (pris) 0.002 0.003 0.0035 0.0035 0.0045 0.0015 0.0018 0.0025 0.0068 0.0057 0.0038 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0025 0.0058 0.0057 0.0088 0.0025 0.0058 0.0025 0.0058 0.0057 0.0088 0.0025 0.0057 0.0088 0.0025 0.0058 0.0057 0.0088 0.0025 0.0057 0.0088 0.0025 0.0057 0.0058 0.0057 0.0078 0.0058 0.0025 0.0078 0.0025 0.0078 0.0025 0.0078 0.0025 0.0078 0.0026 0.0078 0.0028 0.0021 0.0028 0.0021 0.0028 0.0038 0.0027 0.0038 0.0025 0.0028 0.0028 0.0038 0.0028 0.0028 0.0038 < | | | | | | | | | | | | | | | 59.74899 (average) 513.4392 (average) |
| inter [mai] 14.5705 14.5705 14.5705 14.5705 14.572 14.5626 14.5521 14.5561 14.5561 14.5561 14.5561 14.5561 14.5561 14.5561 14.5561 14.5561 14.5571 14.577 14.577 14.555 14.5551 14.555 | | | | | | | | | | | | | | | 0.006225 (average) |
| pink [pink] 0.002 0.0023 0.0026 0.0033 0.0076 0.0119 0.0129 0.0756 0.0351 0.0156 0.0156 0.0156 0.0156 0.0156 0.0156 0.0156 0.0156 0.0156 0.0156 0.0156 0.0156 0.0156 <td></td> | | | | | | | | | | | | | | | |
| hvo (ri) 2.6675 | | | | | | | | | | | | | | | 0.006225 (average) |
| vv (fr.3) 18.855 | | | | | | | | | | | | | | | 2.6675 (average) |
| whre: (number) 0.0804 0.0798 0.0726 0.0736 0.0736 0.0736 0.0736 0.0736 0.0736 0.0736 0.0736 0.0738 0.0238 0.0321 0.03316 0.316 | | | | | | | | | | | | | | | 18.8556 (average) |
| kč (number) 0.0233 0.0232 0.0414 0.0413 0.0331 0.0331 0.0332 0.0232 0.0231 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 0.0316 | wVnc | | | 0.0799 | 0.0782 | 0.0765 | 0.075 | 0.0736 | 0.073 | 0.0732 | 0.0744 | 0.0762 | 0.0778 | 0.0796 | 0.076483 (average) |
| tate (%) 448.22 69.02 50.02 51.17 52.17 53.27 52.607 53.37 52.607 53.42 54.42 54.207 61.2036 60.3166 0. | kE | (number) | 0.0233 | 0.0274 | 0.0333 | 0.0392 | 0.0414 | 0.0413 | 0.0399 | 0.0371 | 0.0351 | 0.033 | 0.0252 | 0.021 | 0.0331 (average) |
| tb [number] 1 | tv | (°R) | 489.7614 | | | 515.0447 | 525.8226 | | | | | | | | 515.5917 (average) |
| in n number) 0.3166 0.3016 | | | | | | | | | | | | | | | 512.5033 (average) |
| n (number) 16.9972 15.352 16.9972 16.4489 16.9972 16.418 10.0016 10.01 | | | | | | | | | | | | | | | 1 (average) |
| Compound Vapor Density (will) Discrete Name | | | | | | | | | | | | | | | 0.3166 (average) |
| Distiliate Fuel OII No. 2 (Ib/In*3) 5.04.05 5.70E-05 8.42E-05 1.00E-04 2.00E-04 3.00E-04 2.00E-04 2.00 | n | (number) | 16.9972 | 15.3523 | 16.9972 | 16.4489 | 16.9972 | 16.4489 | 16.9972 | 16.9972 | 16.4489 | 16.99/2 | 16.4489 | 16.9972 | 200.1283 (sum) |
| Distiliate Fuel Oil No. 2 (Iby/fr3) 5.04E-05 5.70E-05 8.42E-05 1.00E-04 2.00E-04 2.00E-04 3.00E-04 3.00E-04 2.00E-04 3.00E-04 2.00E-04 9.15E-05 6.10E-05 1.145E-04 (Working Losses (Lw) Air (b) 15.2627 13.6977 14.8493 14.0607 14.2335 13.5295 13.8564 13.9092 13.6716 14.4681 14.3055 15.1118 170.9566 Distiliate Fuel Oil No. 2 (b) 0.0096 0.0098 0.016 0.0227 0.0332 0.0428 0.0508 0.0479 0.0363 0.0253 0.0168 0.0116 0.3228 (Breathing Loss Calculations (Uncontrolled) Tan (R) 480.27 493.27 14.8493 14.0607 14.2335 13.5207 525.27 523.97 516.17 504.27 495.77 486.27 503.2617 (taa (R) 486.22 490.92 500.82 511.27 521.47 530.57 535.37 533.7 524.37 514.37 504.27 495.77 512.27 512.176 (taa (R) 486.27 495.57 488.67 509.97 521.67 532.17 540.87 547 543.47 535.97 514.37 512.27 502.27 512.176 (taa (R) 495.57 488.67 509.97 521.67 532.17 540.87 547 543.47 535.97 514.37 512.27 502.27 512.176 (tau (R7) 22.6598 36.2424 47875 45.37931 70.733 60.203 64.7698 73.0176 65.552 45.464 34.4819 54.5646 (tu (R7) 32.2698 36.2741 47875 45.37931 70.733 60.203 64.7698 73.0176 65.3123 44.5139 37.5508 37.564 1247.423 (tu (R7) 22.6508 32.7413 43.1801 54.1527 64.7897 74.188 78.0203 64.7698 73.0456 61.552 13.0344 124.7423 (tu (R7) 32.598 36.6204 147875 45.37931 70.733 60.203 64.7698 12.034.914 93.491 001.304 64.46925 518.764 124.7423 (tu (R7) 45.661 4.561 41.551 151.571 154.271 45.672 14.564 14.5621 14.5621 14.5651 14.5561 14.556 13.568 14.575 14.5764 124.7423 (tu (R8) 0.002 0.0023 0.0035 0.0053 0.0076 0.013 0.0110 0.0112 0.0086 0.0057 0.0038 0.0025 0.00622 6 (phc (psis) 0.002 0.0023 0.0035 0.0053 0.0076 0.0103 0.0110 0.0112 0.0086 0.0057 0.0038 0.0025 0.00622 6 (phc (psis) 0.002 0.0023 0.0035 0.0053 0.0051 0.0013 0.0110 0.0112 0.0086 0.0057 0.0038 0.0025 0.0066 0.066 0.06 0.06 0.06 0.06 0.06 | Compound Venor Density | (MARIN) | | | | | | | | | | | | | |
| Air (b) 15.2627 13.8977 14.8493 14.0607 14.2355 13.8525 13.8504 13.9092 13.6716 14.4681 14.3055 15.1118 170.956 (Distilate Fuel OII No. 2 (b) 0.0096 0.0098 0.016 0.0227 0.0328 0.0428 0.0368 0.0479 0.0363 0.0253 0.0168 0.0116 0.3228 (Breathing Loss Calculations (Uncontrolled) Tain ('R) 480.87 482.97 491.67 500.87 510.77 520.27 523.37 531.23 544.37 531.27 524.37 512.17 521.47 501.61 501.27 502.37 532.43 512.37 503.21 514.37 532.43 512.37 532.43 513.33 533.43 550.35 551.41 501.75 521.375 512.413 513.37 533.43 550.37 532.43 513.333 533.33 533.72 534.43 533.33 533.7 533.43 533.43 550.313 543.445 501.313 143.8309 151.313 | | | 5 04E-05 | 5 70E-05 | 8 42 F-05 | 1 00F-04 | 2 00E-04 | 2 00F-04 | 3 ODE-04 | 3 00F-04 | 2 00F-04 | 1 00F-04 | 9155-05 | 6 10E-05 | 1 45F-04 (ava) |
| Air (b) 15.2627 13.697 14.4935 13.2052 13.8564 13.9052 13.8564 13.9052 13.6571 14.40355 15.1118 170.556 Breathing Loss Calculations (Uncontrolled) Example Controlled) Example Controlled) Example Controlled Example Controlled) Example Controlled Example Controlled) Example Controlled Example Controlled) Example Controlled Example Controlled <thexample controlled<="" th=""> <thexample controled<="" th=""></thexample></thexample> | Distingte i dei on ito. 2 | (10/10/07) | 3.042-03 | 5.702-05 | 0.421-05 | 1.000-04 | 1.001-04 | 2.002-04 | 3.000-04 | 3.00L 04 | 2.001-04 | 1.002 04 | J.152 05 | 0.102 05 | 1.452 04 (248) |
| Air (b) 15.2627 13.697 14.4935 13.2052 13.8564 13.9052 13.8564 13.9052 13.6571 14.40355 15.1118 170.556 Breathing Loss Calculations (Uncontrolled) Example Controlled) Example Controlled) Example Controlled Example Controlled) Example Controlled Example Controlled) Example Controlled Example Controlled) Example Controlled Example Controlled <thexample controlled<="" th=""> <thexample controled<="" th=""></thexample></thexample> | Working Losses (Lw) | | | | | | | | | | | | | | |
| Distillate Fuel OI No. 2 (b) 0.0096 0.0098 0.016 0.0277 0.0322 0.0428 0.0428 0.0429 0.0363 0.0253 0.0168 0.0116 0.03228 (not controlled) Breathing Los Calculations (Uncontrolled) Uncontrolled) Uncontrolled) Tain (°R) 480.07 482.97 491.67 500.87 510.77 520.27 521.47 535.97 534.32 504.02 493.27 512.503 (not controlled) Uncontrolled) | | (lb) | 15.2627 | 13.6977 | 14.8493 | 14.0607 | | | | 13.9092 | 13.6716 | 14.4681 | 14.3055 | 15.1118 | 170.956 (sum) |
| tan (*R) 480.87 482.97 491.67 500.87 510.77 520.27 525.27 523.97 516.17 504.27 495.77 486.27 503.2617 (i) taa (*R) 488.22 490.92 500.82 511.27 521.47 530.75 535.97 532.97 512.37 512.97 502.37 512.37 501.27 521.74 500.75 535.97 523.47 533.97 520.47 535.97 523.17 500.27 521.74 500.27 512.75 502.27 502.37 512.75 <t< td=""><td>Distillate Fuel Oil No. 2</td><td></td><td>0.0096</td><td>0.0098</td><td>0.016</td><td>0.0227</td><td>0.0332</td><td>0.0428</td><td>0.0508</td><td>0.0479</td><td>0.0363</td><td>0.0253</td><td>0.0168</td><td>0.0116</td><td>0.3228 (sum)</td></t<> | Distillate Fuel Oil No. 2 | | 0.0096 | 0.0098 | 0.016 | 0.0227 | 0.0332 | 0.0428 | 0.0508 | 0.0479 | 0.0363 | 0.0253 | 0.0168 | 0.0116 | 0.3228 (sum) |
| tan ("R) 480.87 482.97 491.67 500.87 510.77 520.27 525.27 523.97 516.17 504.27 495.77 486.27 503.2617 (intro-1000) taa ("R) 488.22 490.92 500.82 511.27 521.47 530.57 535.37 533.77 535.97 524.37 512.7 500.22 51.831 41.7526 31.384 501.602.8 (intro-1000) 511.67 535.97 521.27 500.27 521.745 (intro-1000) 500.82 513.47 533.97 512.67 512.75 512 | | | | | | | | | | | | | | | |
| taa (*R) 488.22 490.92 500.82 511.27 521.47 536.37 535.37 536.07 514.32 504.02 493.27 502.027 521.276 (1) tax (*R) 495.57 428.623 38.4449 48.6463 58.447 730.12 71.337 63.3427 535.37 521.27 501.57 501.27 501.57 | Breathing Loss Calculation | • • | | | | | | | | | | | | | |
| tax ('R) 495.57 498.87 509.97 521.67 524.75 548.47 535.97 524.37 512.27 500.27 521.45 512.47 500.27 521.45 512.47 500.27 521.45 512.47 501.23 512.47 501.23 512.48 512.47 501.23 512.48 512.43 512.48 502.08 82.369 73.245 512.34 513.472 512.475 512.475 512.57 512.48 512.57 513.572 514.572 514.572 514.572 514.572 514.572 514.572 514.572 514.572 514.572 51.572 515.572 50.575 50.575 50.575 50.575 50.575 50.575 50.575 50.575 50.575 50.575 50.575 2.6675 2.6675 2.6675 2.6675 2.6675 2.6675 2.6675 2.6675 2.6675 2.66 | tan | | | | | | | | 343.47 | | | | | | 503.2617 (avg) |
| tin (°F) 26.578 28.623 38.489 48.663 58.846 68.1642 73.0123 71.3876 63.5422 51.5831 41.7525 31.3834 50.6028 (14 175) 29.6088 32.7413 43.1801 54.1927 64.7897 74.1836 78.9011 76.8843 68.693 56.3522 45.466 34.4819 54.35463 (14 17 19 19 19 19 19 19 19 19 19 19 19 19 19 | | | | | | | | | | | | | | | 512.5033 (avg) |
| tia (°F) 29.608 32.7413 431.801 54.1927 64.7897 74.1367 78.9011 76.8043 66.939 56.3522 45.445 34.819 54.95483 (1213 49.1393 37.5803 59.74893 (1213 49.1393 37.5803 59.74893 (1213 49.1393 37.5803 59.74893 (1213 49.1393 37.5803 59.74893 (1213 49.1393 37.5803 59.74893 (1213 49.1393 37.5803 59.74893 (1213 49.1393 37.5803 59.74893 (1213 49.1393 37.5803 59.74893 (1213 49.1393 37.5803 59.74893 (1213 49.1393 37.5803 59.74893 (1213 49.1393 37.5803 59.74893 (1213 49.139 10.213 60.057 60.053 60.057 0.003 0.0057 0.003 0.0057 0.003 0.0057 0.003 0.0057 0.003 0.0057 0.003 0.0057 0.005 0.067 0.066 0.06 0.06 0.06 0.06 0.06 0.06 0.06 0.06 0.06 0.067 0.066 0.06< | | | | | | | | | | | | | | | 521.745 (avg) |
| tix (°F) 32.9598 36.8204 47.8734 59.7911 70.733 80.203 84.7898 82.3809 73.8455 61.1213 49.1939 37.5803 59.74895 (1) (Bu/ft ¹ day) 622.801 877.2515 1194.204 1525.1169 175.628 1931.54 1882.997 1667.254 1349.391 40.446.925 518.7364 1247.823 (1) | | | | | | | | | | | | | | | 50.16028 (avg) |
| 1 (Bu/ft*day) 622.801 877.2515 1194.204 1578.628 1931.54 1382.997 1567.254 1349.349 1001.304 644.6925 518.7964 1247.823 tb ('R) 488.6871 491.5779 501.7157 512.4138 522.789 532.0187 536.7822 534.9704 527.082 515.071 504.5035 493.6591 513.4392 pC (psia) 0.0023 0.0023 0.0035 0.0076 0.0130 0.0119 0.0112 0.0056 0.0057 0.0038 0.0057 0.0038 0.0057 0.0038 0.0057 0.0038 0.0057 0.0038 0.0057 0.0038 0.0057 0.006 0.066 0.06 0.067 0.006 0.073 | | | | | | | | | | | | | | | |
| th (R) 488.6971 491.5779 501.7157 512.4138 522.789 520.187 536.7822 534.9704 527082 515.071 504.5035 493.6591 513.4392 (pC (psia) 0.002 0.0023 0.0035 0.0053 0.0076 0.0103 0.0119 0.0112 0.0086 0.0057 0.0038 0.0025 0.006225 (pWe (psia) 0.002 0.0023 0.0035 0.0053 0.0076 0.0103 0.0119 0.0112 0.0086 0.0057 0.0038 0.0025 0.006225 (pVa (psia) 0.002 0.0023 0.0055 0.0053 0.0076 0.0103 0.0119 0.0112 0.0086 0.0057 0.0038 0.0025 0.006225 (dPV (psia) 0.006 4 0.0013 0.0025 0.0053 0.0076 0.0038 0.0025 0.0019 0.0011 6.00E-04 2.18E-03 (dPV (psia) 0.06 0.6 0.06 0.06 0.06 0.06 0.06 0.06 | 1 | | | | | | | | | | | | | | 59.74899 (avg) 1247.823 (avg) |
| pC (psia) 0.002 0.0023 0.0033 0.0033 0.0033 0.0103 0.0112 0.0086 0.0036 0.0038 0.0025 0.006225 (pNC pNc (psia) 14.5702 14.5702 14.5672 14.5672 14.5662 14.5613 14.5633 14.5668 14.5678 14.5672 14.5662 14.5613 14.5663 14.5667 14.571 14.56628 14.5669 14.5678 14.5672 14.5642 14.5603 14.5668 14.567 14.5672 14.5642 14.5603 14.5668 14.567 14.5672 14.5662 14.5603 14.5668 14.567 14.5672 14.5662 14.5603 14.5668 14.567 14.5672 14.5662 14.5603 14.5668 14.5678 14.5668 14.5678 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5672 14.5671 14.5676 14.571 1 | tb | | | | | | | | | | | | | | 513.4392 (avg) |
| phc (psia) 14.5705 14.5705 14.5762 14.5622 14.5623 14.5639 14.5663 14.5667 14.562 pVa (psia) 0.002 0.0023 0.0035 0.0076 0.0103 0.0112 0.0086 0.0057 0.0038 0.0024 0.0028 0.0024 0.0086 0.0057 0.0038 0.0027 0.00622 0.0023 0.0033 0.0033 0.0013 0.0013 0.0013 0.0013 0.0013 0.0014 0.0086 0.005 0.006 0.006 0.06< | | | | | | | | | | | | | | | 0.006225 (avg) |
| pVa (psia) 0.002 0.0023 0.0033 0.0035 0.0033 0.0013 0.0112 0.0086 0.0038 0.0023 0.006225 (0.0043 dPv (psia) 6.00E-04 7.00E-04 0.0013 0.0033 0.0033 0.0033 0.0038 0.0025 0.0014 0.0018 0.0019 0.0011 6.0019 0.0011 6.0019 0.0011 6.0019 0.0013 0.0019 0.0013 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0019 0.0016 0.06 | | | | | | | | | | | | | | | 14.56628 (avg) |
| iprv (psia) 6.00E-04 7.00E-04 0.0013 0.0021 0.0039 0.0038 0.0028 0.0029 0.0011 6.00E-04 2.18E-03 dPb (psia) 0.06 | | | | | | | | | | | | | | | 0.006225 (avg) |
| dTv ("R) 13.404 15.5163 18.751 22.1856 23.7731 24.0777 23.555 21.9863 20.6067 19.0765 14.0735 12.3937 19.17745 hVo (ft) 2.6675 | | (psia) | | | | | | | 0.0043 | 0.0038 | 0.0029 | 0.0019 | | | 2.18E-03 (avg) |
| hVo (ft) 2.6675 | | | | | | | | | | | | | | | 0.06 (avg) |
| ts (number) 0.9997 0.9997 0.9993 0.9993 0.9998 0.9983 0.9984 0.9988 0.9992 0.9995 0.99917 (0.99917) VV (ftr3) 18.8556 18.856 18.856 18.856 18.856 18.856 18.856 18.856 18.8 | | | | | | | | | | | | | | | 19.17745 (avg) |
| Vv (fr.*3) 18.8556 16.333 0.0023 0.002 | | (ft) | | | | | | | | | | | | | 2.6675 (avg) |
| wVnc (number) 0.0804 0.0792 0.0765 0.073 0.0732 0.0744 0.0762 0.0778 0.0796 0.07483 (k kE (number) 0.0233 0.0274 0.0333 0.0392 0.0413 0.0391 0.0351 0.0331 0.0252 0.021 0.0331 0.0392 0.0413 0.03951 0.0351 0.044 0.0028 0.00764 0.00764 0.00764 0.00764 0.00764 0.00764 0.00764 0.00764 0.00764 0.00764 0.00764 </td <td></td> <td>0.999117 (avg)</td> | | | | | | | | | | | | | | | 0.999117 (avg) |
| kE (number) 0.0233 0.0274 0.0333 0.0392 0.0413 0.0351 0.0052 0.0074 0.0074 0.0074 0.0074 0.0074 0.0074 0.0073 0.0044 0.0023 0.0022 0.0074 0.0052 0.0085 0.0099 0.0074 0.0073 0.0044 0.0023 0.0022 0.0052 0.0073 0.0044 0.0053 <td></td> <td>18.8556 (avg)</td> | | | | | | | | | | | | | | | 18.8556 (avg) |
| Tv (*R) 489.7614 493.0912 503.7757 515.0447 525.8226 535.3506 540.0304 537.8465 529.4096 516.7692 505.6156 494.5539 515.5917 (inclusion) pln (psia) 0.0023 0.0027 0.0042 0.0064 0.0022 0.0124 0.0123 0.0102 0.0044 0.0028 0.0073 (inclusion) 0.0067 0.0044 0.0023 0.0073 (inclusion) 0.0067 0.0044 0.0022 0.0073 (inclusion) 0.0073 (inclusion) 0.0073 (inclusion) 0.0023 (inclusion) 0.00517 (inclusion) Compound Vapor Density (wV(I)) Distillate Fuel OII No. 2 (ib/ft*3) 5.04E-05 5.70E-05 8.42E-05 1.00E-04 2.00E-04 3.00E-04 3.00E-04 1.00E-04 9.15E-05 6.10E-05 1.45E-04 (inclusion) Breathing Losses (Ls) //////////////////////////////////// | | | | | | | | | | | | | | | 0.076483 (avg) |
| ph (psia) 0.0023 0.0027 0.0042 0.0064 0.0032 0.0142 0.0133 0.0102 0.0067 0.0044 0.0028 0.0074 (psia) pin (psia) 0.0018 0.002 0.0042 0.0043 0.0022 0.0028 0.0074 (psia) 0.0067 0.0044 0.0028 0.0074 (psia) Compound Vapor Density (wV(I)) Distillate Fuel OII No. 2 (lb/th*3) 5.04E-05 5.70E-05 8.42E-05 1.00E-04 2.00E-04 3.00E-04 3.00E-04 3.00E-04 3.00E-04 1.00E-04 9.15E-05 6.10E-05 1.45E-04 (psia) Breathing Losses (Ls) 0.0016 0.0027 0.0042 0.0052 0.0039 0.0026 0.0017 1.7328 (psia) Air (lb) 1.0954 1.1571 1.5229 1.6965 1.8146 1.7179 1.7023 1.6893 1.4026 0.0013 7.00E-04 3.56E-02 (psia) Total Losses (Lt) 0.0016 | | | | | | | | | | | | | | | 0.0331 (avg) |
| jn (psia) 0.0018 0.002 0.0029 0.0043 0.0020 0.0085 0.0099 0.0094 0.0073 0.0048 0.0033 0.0022 0.005217 (i Compound Vapor Density (wV(I)) Distillate Fuel OII No. 2 (Ib/M*3) 5.04E-05 5.70E-05 8.42E-05 1.00E-04 2.00E-04 3.00E-04 3.00E-04 1.00E-04 9.15E-05 6.10E-05 1.45E-04 (i Breathing Losses (L) Air (Ib) 1.0954 1.1571 1.5229 1.6965 1.8146 1.7179 1.7023 1.5893 1.4763 1.4688 1.1098 0.9771 1.7328 (i Distillate Fuel OII No. 2 (Ib) 1.095-04 0.0016 0.0027 0.0042 0.0054 0.0055 0.0039 0.0026 0.0013 7.00E-04 3.56E-02 (s Total Losses (Lt) Total Losses (Lt) Compound | | | | | | | | | | | | | | | 515.5917 (avg) |
| Compound Vapor Density (wV()) Distillate Fuel OII No. 2 (Ib/ft ^{A3}) 5.04E-05 5.70E-05 8.42E-05 1.00E-04 2.00E-04 2.00E-04 3.00E-04 3.00E-04 1.00E-04 9.15E-05 6.10E-05 1.45E-04 (i Breathing Losses (Ls) Air (Ib) 1.0954 1.1571 1.5229 1.6965 1.8146 1.7179 1.7023 1.5893 1.4763 1.4688 1.1098 0.9771 17.328 (i Distillate Fuel OII No. 2 (Ib) 7.00E-04 8.00E-04 0.0016 0.0027 0.0042 0.0054 0.0062 0.0055 0.0039 0.0026 0.0013 7.00E-04 3.56E-02 (i Total Losses (Lt) | | | | | | | | | | | | | | | 0.0074 (avg) 0.005217 (avg) |
| Distillate Fuel Oll No. 2 (lb/ft ^A 3) 5.04E-05 5.70E-05 8.42E-05 1.00E-04 2.00E-04 2.00E-04 3.00E-04 3.00E-04 1.00E-04 9.15E-05 6.10E-05 1.45E-04 (r Breathing Losses (Ls) Air (lb) 1.0954 1.1571 1.5229 1.6965 1.8146 1.7179 1.7023 1.5893 1.4763 1.4688 1.1098 0.9771 17.328 (r Distillate Fuel Oll No. 2 (lb) 7.00E-04 8.00E-04 0.0016 0.0027 0.0042 0.0054 0.0062 0.0055 0.0039 0.0026 0.0013 7.00E-04 3.56E-02 (r Total Losses (Lt) | P | (Main) | 0.0018 | 0.002 | 0.0029 | 0.0043 | 0.0002 | 0.0085 | 0.0033 | 0.0054 | 0.0073 | 0.0048 | 0.0033 | 0.0022 | 0.000211 (448) |
| Distillate Fuel Oll No. 2 (lb/ft ^A 3) 5.04E-05 5.70E-05 8.42E-05 1.00E-04 2.00E-04 2.00E-04 3.00E-04 3.00E-04 1.00E-04 9.15E-05 6.10E-05 1.45E-04 (r Breathing Losses (Ls) Air (lb) 1.0954 1.1571 1.5229 1.6965 1.8146 1.7179 1.7023 1.5893 1.4763 1.4688 1.1098 0.9771 17.328 (r Distillate Fuel Oll No. 2 (lb) 7.00E-04 8.00E-04 0.0016 0.0027 0.0042 0.0054 0.0062 0.0055 0.0039 0.0026 0.0013 7.00E-04 3.56E-02 (r Total Losses (Lt) | Compound Vanor Density | (wV(i)) | | | | | | | | | | | | | |
| Breathing Losses (Ls) Air (b) 1.0954 1.1571 1.5229 1.6965 1.8146 1.7179 1.7023 1.5893 1.4763 1.4688 1.1098 0.9771 17.328 (s Distillate Fuel (Ji No. 2 (lb) 7.00E-04 8.00E-04 0.0016 0.0027 0.0042 0.0054 0.0062 0.0055 0.0039 0.0026 0.0013 7.00E-04 3.56E-02 (s Total Losses (Lt) | | | 5.04F-05 | 5.70F-05 | 8.42E-05 | 1,00F-04 | 2.00E-04 | 2.00E-04 | 3.00E-04 | 3.00E-04 | 2.00E-04 | 1.00E-04 | 9.15E-05 | 6.10E-05 | 1.45E-04 (avg) |
| Air (lb) 1.0954 1.1571 1.5229 1.6965 1.8146 1.7179 1.7023 1.5893 1.4763 1.4688 1.1098 0.9771 17328 (s Distillate Fuel Qil No. 2 (lb) 7.00E-04 8.00E-04 0.0015 0.0027 0.0042 0.0054 0.0062 0.0055 0.0039 0.0026 0.0013 7.00E-04 3.56E-02 (s Total Losses (Lt) | Province right Oil NO. 2 | (10/10-37 | J-04C-03 | 3.70E-03 | 0.725-03 | 1.005-04 | 2.002-04 | 2.000-04 | J.00E-04 | 3.000-04 | 2.000-04 | 2.002-04 | 3-136-03 | 0.105-03 | 1.40C-04 (4VB) |
| Air (lb) 1.0954 1.1571 1.5229 1.6965 1.8146 1.7179 1.7023 1.5893 1.4763 1.4688 1.1098 0.9771 17.328 (s Distillate Fuel Oli No. 2 (lb) 7.00E-04 8.00E-04 0.0016 0.0027 0.0042 0.0054 0.0062 0.0055 0.0039 0.0026 0.0013 7.00E-04 3.56E-02 (s Total Losses (Lt) | Breathing Losses (Ls) | | | | | | | | | | | | | | |
| Total Losses (Lt) | Air | | | | | | | | | | | | | | 17.328 (sum) |
| | Distillate Fuel Oil No. 2 | (Ib) | 7.00E-04 | 8.00E-04 | 0.0016 | 0.0027 | 0.0042 | 0.0054 | 0.0062 | 0.0055 | 0.0039 | 0.0026 | 0.0013 | 7.00E-04 | 3.56E-02 (sum) |
| | | | | | | | | | | | | | | | |
| AIR (ID) 15.3582 14.8548 15.3722 15.7572 16.0481 15.2474 15.5588 15.4985 15.1479 15.9369 15.4153 16.0888 188.2841 (| | (1) | | | | 4 | | 40.00 | 40.000 | | 40.47-1 | 40.000 | 40.44-4 | | |
| | | | | | | | | | | | | | | | 188.2841 (sum) |
| Distillate Fuel Oil No. 2 (lb) 0.0103 0.0106 0.0176 0.0255 0.0374 0.0482 0.057 0.0534 0.0402 0.0278 0.0181 0.0123 0.3584 (t | Disultate Fuel Oil No. 2 | (10) | 0.0103 | 0.0106 | 0.0176 | 0.0255 | 0.0374 | 0.0482 | 0.057 | 0.0534 | 0.0402 | 0.0278 | 0.0181 | 0.0123 | 0.3584 (sum) |

| Activity Title Climate: | TK-GLY - Giycol Tani Pennsylvania, Harris | | /2021 to 12/ | 31/2021 | | | | | | | | | | |
|---|--|----------------------|--------------------|----------------------|--------------------|--------------------|---|--------------------|---------------------|---------------------|--------------------|----------------------|--------------------|--|
| ра | 14.5725 psia | | | | | | | | | | | | | |
| Equipment Tag Storage Vessel Style | TK-GLY - Glycol Tank Horizontal Storage | | | | | | | | | | | | | |
| Calculation Type | Normal Storage Tan | k (11/2019 | Rev.) | | | | | | | | | | | |
| Malal Caraca Malana | Working and Breath | ning Loss Ca | alculation | | | | | | | | | | | |
| Void Space Volume Working Volume | 4S6.85 gal 396 gal | | | | | | | | | | | | | |
| Working Volume | 52.9375 ft^3 | | | | | | | | | | | | | |
| Shell Diameter | 3.6 ft | | | | | | | | | | | | | |
| Straight Side Height Paint Solar Absorptance | 6 ft 0.25 | | | | | | | | | | | | | |
| Roof Color / Condition | white / average | | | | | | | | | | | | | |
| Shell Color / Condition | white / average 0.03 | | | | | | | | | | | | | |
| pop pbv | -0.03 | | | | | | | | | | | | | |
| Equipment Comment | | | | | | | | | | | | | | |
| Activity Comment Pi (constant) | Imported from Excel 3.1416 | | 6 PM, 5/19/20 | 022. | | | | | | | | | | |
| R (constant) | 998.9 | | | | | | | | | | | | | |
| Vessel Contents | 338 435 ml | 68 000 °C | 2122.663 lb | | 34.198 lb-M | | | | | | | | | |
| Mixture Name: | ZZ8.423 gal Mixture | 00.000 F | 2122.005 10 | | 34.190 IQ-IVI | | | | | | | | | |
| | [Liquid] | mmHg | | W[i] | lb-M | | | X*Pi*Ai (m | mHg) | | | | | |
| Kp (product factor) | Ethylene Glycol | | 2122.6628 | 1 | 34.1979 | 1 | 1 | 0.0925 | | | | | | |
| kp (productiactor) | - | | | | | | | | | | | | | |
| Month | | Jan | Feb | | Apr | | | | | | | | Dec | |
| Q. Va | (gal) (ft^3) | 403.5945 53.9527 | | 403.5945 53.9527 | 390.5753 | 403.5945 | | 403.5945 53.9527 | 403.5945 53.9527 | 390.5753 52.2123 | | 390.5753 52.2123 | 403.5945 | 4752 (sum) 635.2496 (sum) |
| N (period) | (number) | 1.0192 | | 1.0192 | 0.9863 | | 0.9863 | 1.0192 | 1.0192 | 0.9863 | 1.0192 | 0.9863 | 1.0192 | 12.0001 (sum) |
| N (scaled to annual) | (number) | 12 | | 12 | 12 | | 12 | 12 | 12 | 12 | | 12 | 12 | |
| Kn Days | (number) (number) | 1 | | 1 31 | 1 30 | | 1 30 | 1 31 | 1 31 | 1 30 | 1 31 | 1 30 | 1 | 1 (avg) 365 (sum) |
| | | | | | | | | | | | | | | |
| Compound Molecular Weig Ethylene Glycol | ghts (lb/lb-M) (Mv) | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 (lb/lb mala) |
| Eurylene Glycol | (NN) | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 62.07 | 02.07 | 62.07 | 62.07 | 02.07 | 62.07 (lb/lb-mole) |
| Compound Vapor Pressure | | | | | | | | | | | | | | |
| Ethylene Glycol | (mmHg) | 0.0149 | 0.0174 | 0.0292 | 0.0494 | 0.0801 | 0.1213 | 0.1485 | 0.1362 | 0.0953 | 0.0546 | 0.0326 | 0.019 | 0.066542 (avg) |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Working Loss Calculations (tLa | (°F) | 29.6088 | 32.7413 | 43.1801 | 54.1927 | 64.7897 | 74.1836 | 78.9011 | 76.8843 | 68.6939 | 56.3522 | 45.446 | 34.4819 | 54.95463 (average) |
| tLn | (°F) | 26.2578 | 28.8623 | | 48.6463 | 58.8464 | 68.1642 | 73.0123 | 71.3878 | 63.5422 | 51.5831 | | | 50.16028 (average) |
| tLx | (°F) | 32.9598 | | 47.8754 | 59.7391 | 70.733 | 80.203 | 84.7898 | 82.3809 | 73.8456 | | 49.1393 | 37.5803 | 59.74899 (average) |
| tb pC | (°R) (psia) | 488.6871 3.00E-04 | | 501.7157 6.00E-04 | 512.4138 0.001 | | 0.0023 | 536.7822 0.0029 | 534.9704 0.0026 | 527.082 0.0018 | | 504.5035 6.00E-04 | | 513.4392 (average) 1.28E-03 (average) |
| pNc | (psia) | 14.5722 | 14.5722 | 14.5719 | 14.5715 | 14.571 | 14.5702 | 14.5696 | 14.5699 | 14.5707 | 14.5714 | 14.5719 | 14.5721 | 14.57122 (average) |
| pVa | (psia) | 3.00E-04 | | 6.00E-04 | 0.001 | | 0.0023 | 0.0029 | 0.0026 | 0.0018 | | 6.00E-04 | | 1.28E-03 (average) |
| hVo Vv | (ft) (ft^3) | 1.4137 30.5569 | | 1.4137 30.5569 | 1.4137 30.5569 | | 1.4137 30.5569 | 1.4137 30.5569 | 1.4137 30.5569 | 1.4137 30.5569 | 1.4137 30.5569 | 1.4137 30.5569 | 1.4137 30.5569 | 1.4137 (average) 30.5569 (average) |
| wVnc | (number) | 0.0804 | 0.0799 | 0.0782 | 0.0765 | | 0.0737 | 0.073 | 0.0733 | 0.0744 | 0.0762 | 0.0779 | 0.0796 | 0.076508 (average) |
| kE tv | (number) | 0.0233 489.7614 | | | 0.0391 | | 0.0411 | 0.0397 | 0.0369 | 0.0349 | 0.0329 | 0.0251 | 0.021 | 0.032992 (average) |
| taa | (°R) (°R) | 489.7014 | | 503.7757 500.82 | 515.0447 | | 535.3506 530.57 | 535.37 | 533.72 | 526.07 | 514.32 | 505.6156 504.02 | 494.5559 | 515.5917 (average) 512.5033 (average) |
| kb | (number) | 1 | | | 1 | | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| kn n | (number) (number) | 1 1.0192 | | | 1 0.9863 | | 1 0.9863 | 1 1.0192 | 1 1.0192 | 1 0.9863 | 1 1.0192 | 1 0.9863 | 1 1.0192 | 1 (average) 12.0001 (sum) |
| | | | | | | | | | | | | | | |
| Compound Vapor Density (| | 3 405 06 | 3.005.00 | C 405 0C | 1 075 05 | 1 705 05 | 2 5 25 05 | 1 085 05 | 2 825 05 | 2.015.05 | 1 105 05 | 7 225 05 | 4 305 05 | |
| Ethylene Glycol | (lb/ft^3) | 3.40E-06 | 3.96E-06 | 6.49E-06 | 1.07E-05 | 1.70E-05 | 2.551-05 | 3.08E-05 | 2.83E-05 | 2.011-05 | 1.185-05 | 7.222-06 | 4.30E-06 | 1.41E-05 (avg) |
| Working Losses (Lw) | | | | | | | | | | | | | | |
| Air Ethylene Glycol | (lb) (lb) | 4.3369 2.00E-04 | 3.8923 2.00F-04 | 4.2198 4.00E-04 | 3.996 6.00F-04 | 4.0456 9.00E-04 | 3.846 0.0013 | 3.9393 0.0017 | 3.9541 0.0015 | 3.8861 | 4.1119 6.00E-04 | 4.0653 4.00E-04 | 4.2941 2.00F-04 | 48.5874 (sum) 9.10E-03 (sum) |
| Englishe offen | (10) | 1.002 04 | 2.002 04 | 4.002 04 | 0.002 04 | 5.002 04 | 0.0015 | 0.0017 | 0.0015 | 0.0011 | 0.002 04 | 4.002.04 | 2.002 04 | 5.102 05 (Juli) |
| Breathing Loss Calculations | | | | | | | | | | | | | | |
| tan taa | (°R) (°R) | 480.87 488.22 | | 491.67 500.82 | 500.87 511.27 | 510.77 521.47 | 520.27 530.57 | 525.27 535.37 | 523.97 533.72 | 516.17 526.07 | 504.27 514.32 | 495.77 504.02 | 486.27 493.27 | 503.2617 (avg) 512.5033 (avg) |
| tax | (*R) | 495.57 | 498.87 | 509.97 | 521.67 | 532.17 | 540.87 | 545.47 | 543.47 | 535.97 | 524.37 | 512.27 | 500.27 | 521.745 (avg) |
| tLn Ha | (°F) | 26.2578 29.6088 | | | 48.6463 | | 68.1642 | 73.0123 | 71.3878 | 63.5422 | | | 31.3834 | 50.16028 (avg) |
| tLa tLx | (°F) (°F) | 32.9598 | | 43.1801 47.8754 | 54.1927 59.7391 | | 74.1836 80.203 | 78.9011 84.7898 | 76.8843 82.3809 | 68.6939 73.8456 | 56.3522 61.1213 | 45.446 49.1393 | | 54.95463 (avg) 59.74899 (avg) |
| 1 | (Btu/ft²day) | 622.801 | 877.2515 | 1194.204 | 1525.1169 | 1758.628 | 1931.54 | 1882.997 | 1667.254 | 1349.349 | 1001.304 | 644.6926 | 518.7364 | 1247.823 (avg) |
| њ -С | (°R) | 488.6871 | | 501.7157 6.00E-04 | 512.4138 0.001 | | 532.0187 0.0023 | 536.7822 0.0029 | 534.9704 0.0026 | 527.082 0.0018 | | 504.5035 6.00E-04 | | 513.4392 (avg) |
| pC pNc | (psia) (psia) | 3.00E-04 14.5722 | | 14.5719 | 14.5715 | | | 14.5696 | 14.5699 | 14.5707 | | 14.5719 | | 1.28E-03 (avg) 14.57122 (avg) |
| pVa | (psia) | 3.00E-04 | 3.00E-04 | 6.00E-04 | 0.001 | 0.0015 | 0.0023 | 0.0029 | 0.0026 | 0.0018 | 0.0011 | 6.00E-04 | 4.00E-04 | 1.28E-03 (avg) |
| dPv dPb | (psia) (psia) | 9.89E-05 0.06 | | 3.00E-04 0.06 | 5.00E-04 0.06 | | 0.0012 0.06 | 0.0015 0.06 | 0.0013 0.06 | 8.00E-04 0.06 | 5.00E-04 0.06 | 2.00E-04 0.06 | 1.00E-04 0.06 | 6.17E-04 (avg) 0.06 (avg) |
| dīv | (°R) | 13.404 | | | 22.1856 | | 24.0777 | 23.555 | 21.9863 | 20.6067 | 19.0765 | | | 19.17745 (avg) |
| hVo | (ft) | 1.4137 | 1.4137 | 1.4137 | 1.4137 | 1.4137 | 1.4137 | 1.4137 | 1.4137 | 1.4137 | 1.4137 | 1.4137 | 1.4137 | 1.4137 (avg) |
| ks Vv | (number) (ft^3) | 1 30.5569 | | 1 30.5569 | 0.9999 30.5569 | | 0.9998 30.5569 | 0.9998 30.5569 | 0.9998 30.5569 | 0.9999 30.5569 | 0.9999 30.5569 | 1 30.5569 | 1 30.5569 | 0.999917 (avg) 30.5569 (avg) |
| wVnc | (number) | 0.0804 | | | 0.0765 | | 0.0737 | 0.073 | 0.0733 | 0.0744 | 0.0762 | 0.0779 | 0.0796 | 0.076508 (avg) |
| kE | (number) | 0.0233 | 0.0274 | 0.0332 | 0.0391 | 0.0413 | 0.0411 | 0.0397 | 0.0369 | 0.0349 | 0.0329 | 0.0251 | 0.021 | 0.032992 (avg) |
| tv pix | (°R) (psia) | 489.7614 3.00E-04 | | 503.7757 7.00E-04 | 515.0447 0.0012 | 525.8226 0.002 | 535.3506 0.003 | 540.0304 0.0037 | 537.8465 0.0033 | 529.4096 0.0023 | | 505.6156 8.00E-04 | | 515.5917 (avg) 1.62E-03 (avg) |
| pix pin | (psia) (psia) | 3.00E-04 2.00E-04 | | 4.00E-04 | 7.00E-04 | | 0.003 | 0.0037 | 0.0033 | | | 8.00E-04 5.00E-04 | | 1.00E-03 (avg) |
| | | | | | | | | | | | | | | |
| Compound Vapor Density i Ethylene Glycol | (WV(I)) (Ib/ft^3) | 3.40E-06 | 3.96F-06 | 6.49E-06 | 1.07F-05 | 1.70E-05 | 2.53E-05 | 3.08F-05 | 2,835-05 | 2.01E-05 | 1.18E-05 | 7.22F-06 | 4.30F-06 | 1.41E-05 (avg) |
| | | 2.402-00 | 3.30L-00 | VO | 140, 0-03 | 2.702-03 | | 0.002-00 | 2.302-03 | | 2.202-03 | | | (a.B. |
| Breathing Losses (Ls) | (15) | | 4 | | | 3 0044 | , , ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,, | | | | | | 1 | 28.0017 () |
| Air Ethylene Glycol | (lb) (lb) | 1.773 7.49E-05 | | 2.4634 2.00E-04 | 2.7426 4.00E-04 | 2.9313 7.00E-04 | 2.7732 0.001 | 2.747 0.0012 | 2.5648 0.001 | 2.384 6.00E-04 | 2.3739 4.00E-04 | 1.7948 2.00E-04 | 1.5811 8.55E-05 | 28.0017 (sum) 5.95E-03 (sum) |
| | | | | | | | | | | - • | | | | |
| Total Losses (Lt) Air | (lb) | 6.1099 | 5.7649 | 6.6831 | 6.7386 | 6.9769 | 6.6192 | 6.6862 | 6.519 | 6.2701 | 6.4858 | 5.8601 | 5.8752 | 76.589 (sum) |
| Ethylene Glycol | (Ib) | 3.00E-04 | | 6.00E-04 | 9.00E-04 | | 0.0023 | 0.0028 | 0.0025 | 0.0017 | | 5.00E-04 | | 1.48E-02 (sum) |
| | | | | | | | | | | | | | | 1.48E-02 |
| | | | | | | | | | | | | | | 1.405-02 |

1.48E-02

| Activity Title | TK-RS (1-6) Resin T | [ank From 1/ | 1/2021 to 12/3 | 31/2021 | | | | | | | | | | |
|---|---|------------------|------------------|----------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|------------------|-------------------------------|
| Climate: | Pennsylvania, Han | risburg | | | | | | | | | | | | |
| pa | 14.5725 psia | | | | | | | | | | | | | |
| Equipment Tag | TK-RS (1-6) Resin T | | | | | | | | | | | | | |
| 5torage Vessel 5tyle Calculation Type | Cone Roof Storage Isothermal Storage | | 010 Boy) | | | | | | | | | | | |
| calculation type | Working Loss Calc | | 019 Nev.) | | | | | | | | | | | |
| Void Space Volume | 17592.22 gal | | | | | | | | | | | | | |
| Working Volume | 13314 gal | | | | | | | | | | | | | |
| Working Volume | 1779.8229 ft^3 | | | | | | | | | | | | | |
| Shell Diameter | 11.41 ft | | | | | | | | | | | | | |
| Straight Side Height | 23 ft | | | | | | | | | | | | | |
| Hro | 0 ft | | | | | | | | | | | | | |
| Paint Solar Absorptance | 0.2 | 5 | | | | | | | | | | | | |
| Roof Color / Condition Shell Color / Condition | white / average | | | | | | | | | | | | | |
| pbp | white / average | 0 | | | | | | | | | | | | |
| pby | | õ | | | | | | | | | | | | |
| Equipment Comment | | • | | | | | | | | | | | | |
| Activity Comment | Imported from Ex | cel on 2:55:50 | 6 PM, 5/19/20 | 22. | | | | | | | | | | |
| Pi (constant) | 3.141 | .6 | | | | | | | | | | | | |
| R (constant) | 998. | 9 | | | | | | | | | | | | |
| Veren Contractor | 0000 440 | | 77750 000 " | | ADEC 247 1 | | | | | | | | | |
| Vessel Contents Mixture Name: | - | ai 08.000 °F | 73359.990 lb | | 4056.247 lb-M | | | | | | | | | |
| witkture indme: | Rockwool Resin [Liquid] | mmHg | lb | W[i] | lb-M | X[i] | A[i] | X*Pi*Ai (m | mHa) | | | | | |
| | Formaldehyde | 3003.344 | | 0.001975 | | 0.001189 | A(I) 1 | 3.5719 | 6/ | | | | | |
| | Methanol | 93.743 | | 0.000554 | | 0.000313 | 1 | 0.0293 | | | | | | |
| | Phenol | 0 | | 0.003533 | | 0.000679 | 1 | 0 | | | | | | |
| | Water | 17.3515 | 72915.279 | 0.993938 | 4047.3995 | 0.997819 | 1 | 17.3136 | | | | | | |
| Kp (product factor) | | 1 | | | | | | | | | | | | |
| HI | 11.5 ft | | | | | | | | | | | | | |
| Month | | Jan | Feb | Mar | Apr | Мау | Jun | Jul | Aug | Sep | Oct | Nov | Dec | |
| Q | (gal) | 161543.3 | | | | - | | | - | • | | | | 1902042 (sum) |
| Vq | (ft^3) | 21595.2 | | | 20898.5778 | 21595.2 | | 21595.2 | 21595.2 | 20898.58 | 21595.2 | | 21595.2 | 254266 (sum) |
| N (period) | (number) | 12.1333 | 10.9591 | 12.1333 | 11.7419 | 12.1333 | 11.7419 | 12.1333 | 12.1333 | 11.7419 | 12.1333 | 11.7419 | 12.1333 | 142.8598 (sum) |
| N (scaled to annual) | (number) | 142.8603 | | 142.8603 | 142.8603 | | | 142.8603 | | 142,8603 | | | | |
| Kn | (number) | 0.3767 | 0.3767 | 0.3767 | 0.3767 | 0,3767 | 0.3767 | 0.3767 | 0.3767 | 0.3767 | 0.3767 | 0.3767 | 0.3767 | 0.3767 (avg) |
| Days | (number) | 31 | 28 | 31 | 30 | 31 | 30 | 31 | 31 | 30 | 31 | 30 | 31 | 365 (sum) |
| Compound Molecular W | eights (lb/lb-M) | | | | | | | | | | | | | |
| Formaldehyde | (Mv) | 30.03 | 30.03 | 30.03 | 30.03 | 30.03 | 30.03 | 30.03 | 30.03 | 30.03 | 30.03 | 30.03 | 30.03 | 30.03 (lb/lb-mol |
| Methanol | (Mv) | 32.04 | 32.04 | | 32.04 | 32.04 | 32.04 | 32.04 | 32.04 | 32.04 | 32.04 | 32.04 | 32.04 | 32.04 (lb/lb-mol |
| Phenol | (Mv) | 94.1128 | 94.1128 | 94.1128 | 94.1128 | 94.1128 | 94.1128 | 94.1128 | 94.1128 | 94.1128 | 94.1128 | 94.1128 | 94.1128 | 94.1128 (lb/lb-mol |
| Water | (Mv) | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 | 18.0153 (lb/lb-mol |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Working Loss Calculation | s (Uncontrolled) | | | | | | | | | | | | | |
| kb | (number) | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| kn | (number) | 0.3767 | 0.3767 | | 0.3767 | 0.3767 | 0.3767 | 0.3767 | 0.3767 | 0.3767 | 0.3767 | 0.3767 | 0.3767 | 0.3767 (average) |
| n | (number) | 12.1333 | 10.9591 | 12.1333 | 11.7419 | 12.1333 | 11.7419 | 12.1333 | 12.1333 | 11.7419 | 12.1333 | 11.7419 | 12.1333 | 142.8598 (sum) |
| Compound Vanor Dansit | | | | | | | | | | | | | | |
| Compound Vapor Densit Formaldehyde | (lb/ft^3) | 4.00E-04 | 4.00E-04 | 4.00E-04 | 4 005-04 | 4.00E-04 | 4 00F-04 | 4 005-04 | 4.00E-04 | 4.00E-04 | 4.005-04 | 4.00E-04 | 4.00F-04 | 4.00E-04 (avg) |
| Methanol | (lb/ft^3) | 3.21E-06 | 3.21E-06 | | | 3.21E-06 | | | | 3.21E-06 | | | | 3.21E-06 (avg) |
| Phenol | (lb/ft^3) | 0 | 0 | | 0 | 0 | 0 | 0 | 0 | 0 | 0 | | 0 | 0 (avg) |
| Water | (lb/ft^3) | 0.0011 | 0.0011 | 0.0011 | 0.0011 | 0.0011 | 0.0011 | 0.0011 | 0.0011 | 0.0011 | 0.0011 | 0.0011 | 0.0011 | 0.0011 (avg) |
| | | | | | | | | | | | | | | |
| Working Losses (Lw) | <i></i> . | | | | | | | | | | | | | |
| Air | (Ib) | 589.4531 | | 589.4531 | | | 570.4385 | | | | | 570.4385 | | 6940.335 (sum) |
| Formaldehyde Methanol | (lb) (lb) | 2.9796 0.0261 | 2.6912 0.0236 | | 2.8835 0.0253 | 2.9796 0.0261 | 2.8835 0.0253 | 2.9796 0.0261 | 2.9796 0.0261 | 2.8835 0.0253 | 2.9796 0.0261 | 2.8835 0.0253 | 2.9796 0.0261 | 35.0824 (sum) 0.3075 (sum) |
| Phenol | (Ib) (Ib) | 0.0201 | 0.0230 | | 0.0233 | 0.0201 | | 0.0201 | 0.0201 | 0.023 | 0.0201 | | 0.0261 | 0.5075 (sum) 0 (sum) |
| Water | (Ib) | 8.6642 | 7.8257 | | 8.3847 | 8.6642 | 8.3847 | 8.6642 | 8.6642 | 8.3847 | 8.6642 | | 8.6642 | 102.0139 (sum) |
| | | | | | | | | | | | | | | • • |
| Total Losses (Lt) | | | | | | | | | | | | | | |
| Air Formoldobudo | (lb) | 589.4531 | | 589.4531 | 570.4385 | | | | | 570.4385 | | 570.4385 | | 6940.335 (sum) |
| Formaldehyde Methanol | (lb) (lb) | 2.9796 0.0261 | 2.6912 0.0236 | | 2.8835 0.0253 | 2.9796 0.0261 | 2.8835 0.0253 | 2.9796 0.0261 | 2.9796 0.0261 | 2.8835 0.0253 | 2.9796 0.0261 | 2.8835 0.0253 | 2.9796 0.0261 | 35.0824 (sum) |
| Phenol | (lb) (lb) | 0.0261 | 0.0236 | | 0.0253 | 0.0261 | | 0.0261 | 0.0261 | 0.0253 | 0.0261 | | 0.0261 | 0.3075 (sum) 0 (sum) |
| Water | (lb) | 8.6642 | 7.8257 | | 8.3847 | 8.6642 | 8.3847 | 8.6642 | 8.6642 | 8.3847 | 8.6642 | 8.3847 | 8.6642 | 102.0139 (sum) |
| | •·-• | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | 137.4038 |
| | | | | | | | | | | | | | | |

| A | | | | | 124 12024 | | | | | | | | | |
|---|---------------------------|---------------|---------------|------------|------------------|---------|---------|------------|---------|------------------|---------|---------|---------|-----------------|
| Activity Title Climate: | TK-TO1 Thermal Oil N/A | Expansion 1 | ank From 1/1, | 2021 to 12 | /31/2021 | | | | | | | | | |
| | N/A N/A | | | | | | | | | | | | | |
| pa Faula and Taa | N/A TK-TO1 Thermal Oil | | | | | | | | | | | | | |
| Equipment Tag Storage Vessel Style | Horizontal Storage | Expansion 1 | ank | | | | | | | | | | | |
| Calculation Type | Isothermal Storage | Tank /11/20 | | | | | | | | | | | | |
| calculation type | | | L9 Rev.) | | | | | | | | | | | |
| Void Cross Volume | Working Loss Calcu | lation | | | | | | | | | | | | |
| Void Space Volume | 343.7 gal | | | | | | | | | | | | | |
| Working Volume | 212 gal 28.3403 ft^3 | | | | | | | | | | | | | |
| Working Volume | | | | | | | | | | | | | | |
| Shell Diameter | 3ft | | | | | | | | | | | | | |
| Straight Side Height | 6.5 ft 0.2 | - | | | | | | | | | | | | |
| Paint Solar Absorptance Roof Color / Condition | white / average | 5 | | | | | | | | | | | | |
| • | • | | | | | | | | | | | | | |
| Shell Color / Condition | white / average | | | | | | | | | | | | | |
| pbp | | D D | | | | | | | | | | | | |
| pbv | , i | 0 | | | | | | | | | | | | |
| Equipment Comment | | | | | | | | | | | | | | |
| Activity Comment | Imported from Exc | | PM, 5/19/202 | 2. | | | | | | | | | | |
| Pi (constant) | 3.1410 | | | | | | | | | | | | | |
| R (constant) | 998.9 | 9 | | | | | | | | | | | | |
| Vessel Contents | 171.050 | | 1000 001 11 | | 6.528 lb-M | | | | | | | | | |
| | - | il 572.000 °F | 1200.301 ID | | 6.528 ID-IVI | | | | | | | | | |
| Mixture Name: | Mixture | | | | | | | | | | | | | |
| | [Liquid] | mmHg | | W[i] | | | | X*Pi*Ai (m | ımHgj | | | | | |
| | Paratherm | 474.4084 1 | 1266.3606 | 1 | 6.5276 | 1 | 1 | 474.4084 | | | | | | |
| Kp (product factor) | | L | | | | | | | | | | | | |
| Month | | Jan | Feb | Mar | Apr | May | Jun | Jul | Aug | Sep | Oct | Nov | Dec | |
| Q | (gal) | 15.2877 | 13.8082 | 15.2877 | 14. 794 5 | 15.2877 | 14.7945 | 15.2877 | 15.2877 | 14. 794 5 | 15.2877 | 14.7945 | 15.2877 | 180.0001 (sum) |
| Va | (gai) (ft^3) | 2.0437 | 13.8082 | 2.0437 | 14.7545 | 2.0437 | 14.7543 | 2.0437 | 2.0437 | 14.7545 | 2.0437 | 14.7343 | 2.0437 | 24.0626 (sum) |
| Vy N (period) | (number) | 0.0721 | 0.0651 | 0.0721 | 0.0698 | 0.0721 | 0.0698 | 0.0721 | 0.0721 | 0.0698 | 0.0721 | 0.0698 | 0.0721 | 0.849 (sum) |
| | | 0.0721 | | 0.8491 | 0.0658 | 0.8491 | 0.8491 | 0.8491 | 0.8491 | 0.0058 | 0.8491 | 0.8491 | 0.8491 | 0.849 (sum) |
| N (scaled to annual) Kn | (number) | | | 0.8491 | | | 0.8491 | 0.8491 | 0.8491 | 0.8491 | 0.8491 | | 0.8491 | 1 (aug |
| | (number) | 1 31 | | 31 | - | 31 | 30 | 31 | 31 | 30 | 31 | 1 30 | 31 | 1 (avg) |
| Days | (number) | 31 | 28 | 31 | 30 | 31 | 30 | 31 | 31 | 30 | 31 | 30 | 31 | 365 (sum) |
| Compound Molecular We | ights (lh/lh_M) | | | | | | | | | | | | | |
| Paratherm | (Mv) | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 (lb/lb-mol |
| Fulderin | (1414) | 1.54 | | 1.54 | 1.54 | 134 | | 134 | 1.54 | 1,4 | 1.74 | 1.54 | 1.74 | 194 (10/10-110) |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Working Loss Calculations | s (Uncontrolled) | | | | | | | | | | | | | |
| kb | (number) | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| kn | (number) | 1 | | 1 | | | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| n | (number) | 0.0721 | | 0.0721 | 0.0698 | 0.0721 | 0.0698 | 0.0721 | 0.0721 | 0.0698 | 0.0721 | 0.0698 | 0.0721 | 0.849 (sum) |
| | ,, | | | | | | | | | | | | | |
| Compound Vapor Density | (vW(i)) | | | | | | | | | | | | | |
| Paratherm | (lb/ft^3) | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 (avg) |
| | (.=, , | | | | | | | | | | | | | (|
| Working Losses (Lw) | | | | | | | | | | | | | | |
| Air | (lb) | 0.0295 | 0.0267 | 0.0295 | 0.0286 | 0.0295 | 0.0286 | 0.0295 | 0.0295 | 0.0286 | 0.0295 | 0.0286 | 0.0295 | 0.3476 (sum) |
| Paratherm | (lb) | 0.3285 | | 0.3285 | 0.3179 | 0.3285 | 0.3179 | 0.3285 | 0.3285 | 0.3179 | 0.3285 | 0.3179 | 0.3285 | 3.8678 (sum) |
| | ·/ | | | | | | | 0.0100 | | | 0.0200 | | | () |
| Total Losses (Lt) | | | | | | | | | | | | | | |
| Air | (lb) | 0.0295 | 0.0267 | 0.0295 | 0.0286 | 0.0295 | 0.0286 | 0.0295 | 0.0295 | 0.0286 | 0.0295 | 0.0286 | 0.0295 | 0.3476 (sum) |
| Paratherm | (Ib) | 0.3285 | | 0.3285 | 0.3179 | 0.3285 | 0.3179 | 0.3285 | 0.3285 | 0.3179 | 0.3285 | 0.3179 | 0.3285 | 3.8678 (sum) |
| | | 0.0000 | 0.2.007 | | 5.5275 | | 2.02.0 | 2.02.00 | | | | | | 2.2070 (3411) |
| | | | | | | | | | | | | | | 3.8678 |
| | | | | | | | | | | | | | | |

| A | | | . /. /2020 | | | | | | | | | | | |
|-------------------------------|------------------------------|-----------------|--------------|--------------|------------------|---------|---------|------------|------------|------------------|---------|------------------|---------|----------------|
| Activity Title Climate: | TK-TO2 Thermal Oil N/A | i Drain Tank Fi | rom 1/1/2021 | to 12/31/ | 2021 | | | | | | | | | |
| pa | N/A | | | | | | | | | | | | | |
| Pa Equipment Tag | TK-TO2 Thermal Oil | Drain Tank | | | | | | | | | | | | |
| Storage Vessel Style | Horizontal Storage | | | | | | | | | | | | | |
| Calculation Type | Isothermal Storage | Tank (11/201 | 9 Rev.) | | | | | | | | | | | |
| | Working Loss Calcul | | • | | | | | | | | | | | |
| Void Space Volume | 343.7 gal | | | | | | | | | | | | | |
| Working Volume | 159 gal | | | | | | | | | | | | | |
| Working Volume | 21.2552 ft^3 | | | | | | | | | | | | | |
| Shell Diameter | 3 ft | | | | | | | | | | | | | |
| Straight Side Height | 6.5 ft | | | | | | | | | | | | | |
| Paint Solar Absorptance | 0.25 | 5 | | | | | | | | | | | | |
| Roof Color / Condition | white / average | | | | | | | | | | | | | |
| Shell Color / Condition | white / average | _ | | | | | | | | | | | | |
| pbp | | 0 | | | | | | | | | | | | |
| pbv | L L | D | | | | | | | | | | | | |
| Equipment Comment | International Association | | DNA 5/10/202 | | | | | | | | | | | |
| Activity Comment | Imported from Exce 3.1416 | | PM, 5/19/202 | . z . | | | | | | | | | | |
| Pi (constant) R (constant) | 5.1410 998.9 | | | | | | | | | | | | | |
| (Constant) | 556.5 | 5 | | | | | | | | | | | | |
| Vessel Contents | 171.850 ga | il 572.000 °F | 1266.361 lb | | 6.528 lb-M | | | | | | | | | |
| Mixture Name: | Mixture | | | | | | | | | | | | | |
| | [Liquid] | mmHg | Ь | w [i] | lb-M | X[i] | A[i] | X*Pi*Ai (m | mHg) | | | | | |
| | Paratherm | 474.4084 | | | | 1 | | 474.4084 | u , | | | | | |
| Kp (product factor) | 1 | 1 | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Month | | Jan | Feb | Mar | Apr | May . | Jun | Jul | Aug | Sep | Oct | Nov I | Dec | |
| Q | (gal) | 15.2877 | 13.8082 | 15.2877 | 14. 794 5 | 15.2877 | 14.7945 | 15.2877 | 15.2877 | 14. 794 5 | 15.2877 | 14. 794 5 | 15.2877 | 180.0001 (sum) |
| Vq | (ft^3) | 2.0437 | 1.8459 | 2.0437 | 1.9777 | 2.0437 | 1.9777 | 2.0437 | 2.0437 | 1.9777 | 2.0437 | 1.9777 | 2.0437 | 24.0626 (sum) |
| N (period) | (number) | 0.0961 | 0.0868 | 0.0961 | 0.093 | 0.0961 | 0.093 | 0.0961 | 0.0961 | 0.093 | 0.0961 | 0.093 | 0.0961 | 1.1315 (sum) |
| N (scaled to annual) | (number) | 1.1321 | | 1.1321 | 1.1321 | 1.1321 | 1.1321 | 1.1321 | 1.1321 | 1.1321 | 1.1321 | 1.1321 | 1.1321 | |
| Kn | (number) | 1 | | 1 | | | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (avg) |
| Days | (number) | 31 | 28 | 31 | 30 | 31 | 30 | 31 | 31 | 30 | 31 | 30 | 31 | 365 (sum) |
| Compound Molecular We | ights (lb/lb-M) | | | | | | | | | | | | | |
| Paratherm | (Mv) | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 | 194 (lb/lb-mol |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Working Loss Calculations | • • | | | | | | | | | | | | | |
| kb | (number) | 1 | | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| kn | (number) | 1 | | 1 | | | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| n | (number) | 0.0961 | 0.0868 | 0.0961 | 0.093 | 0.0961 | 0.093 | 0.0961 | 0.0961 | 0.093 | 0.0961 | 0.093 | 0.0961 | 1.1315 (sum) |
| Compound Vapor Density | (www.fill) | | | | | | | | | | | | | |
| Paratherm | (lb/ft^3) | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 | 0.1608 (avg) |
| | (10/10 0/ | 012000 | 012000 | 012000 | 012000 | 012000 | 012000 | 012000 | 012000 | 0.2000 | 012000 | 0.1000 | 012000 | 012000 (UIB) |
| Working Losses (Lw) | | | | | | | | | | | | | | |
| Air | (lb) | 0.0295 | 0.0267 | 0.0295 | 0.0286 | 0.0295 | 0.0286 | 0.0295 | 0.0295 | 0.0286 | 0.0295 | 0.0286 | 0.0295 | 0.3476 (sum) |
| Paratherm | (lb) | 0.3285 | 0.2967 | 0.3285 | 0.3179 | 0.3285 | 0.3179 | 0.3285 | 0.3285 | 0.3179 | 0.3285 | 0.3179 | 0.3285 | 3.8678 (sum) |
| | | | | | | | | | | | | | | |
| Total Losses (Lt) | | | | | | | | | | | | | | |
| Air | (lb) | 0.0295 | 0.0267 | 0.0295 | 0.0286 | 0.0295 | 0.0286 | 0.0295 | 0.0295 | 0.0286 | 0.0295 | 0.0286 | 0.0295 | 0.3476 (sum) |
| Paratherm | (lb) | 0.3285 | 0.2967 | 0.3285 | 0.3179 | 0.3285 | 0.3179 | 0.3285 | 0.3285 | 0.3179 | 0.3285 | 0.3179 | 0.3285 | 3.8678 (sum) |
| | | | | | | | | | | | | | | 3,8678 |
| | | | | | | | | | | | | | | 3.6070 |

| Activity Title | TK-TO3 Thermal O | il Tank From | 1/1/2021 to 12 | /31/2021 | | | | | | | | | | |
|----------------------------|-----------------------------|---------------|----------------|----------|--------------|---------|---------|------------|---------|---------|---------|---------|---------|-------------------|
| Climate: | N/A | | | | | | | | | | | | | |
| pa | N/A | | | | | | | | | | | | | |
| Equipment Tag | TK-TO3 Thermal O | | | | | | | | | | | | | |
| Storage Vessel Style | Horizontal Storage | | | | | | | | | | | | | |
| Calculation Type | Isothermal Storage | | 019 Rev.) | | | | | | | | | | | |
| | Working Loss Calcu | lation | | | | | | | | | | | | |
| Void Space Volume | 5309.44 gal | | | | | | | | | | | | | |
| Working Volume | 5283 gal | | | | | | | | | | | | | |
| Working Volume | 706.2344 ft^3 | | | | | | | | | | | | | |
| Shell Diameter | 6.56 ft | | | | | | | | | | | | | |
| Straight Side Height | 21 ft | _ | | | | | | | | | | | | |
| Paint Solar Absorptance | 0.2 | 5 | | | | | | | | | | | | |
| Roof Color / Condition | white / average | | | | | | | | | | | | | |
| Shell Color / Condition | white / average | • | | | | | | | | | | | | |
| pbp | | 0 | | | | | | | | | | | | |
| pbv | | 0 | | | | | | | | | | | | |
| Equipment Comment | Income and the second frame | | | | | | | | | | | | | |
| Activity Comment | Imported from Exc 3.141 | | 5 PM, 5/19/202 | . | | | | | | | | | | |
| Pi (constant) | 5.141 998. | | | | | | | | | | | | | |
| R (constant) | 998. | 9 | | | | | | | | | | | | |
| Vessel Contents | 2654 720 at | al 302 000 °E | 19562.601 lb | 10 | 0.698 lb-M | | | | | | | | | |
| Mixture Name: | Mixture | ar 332.000 T | 19902.001 10 | 10 | 0.030 10-141 | | | | | | | | | |
| WIALUTE NAME. | [Liquid] | mmHg | Ь | W[i] lb- | м | X[i] | A[i] | X*Pi*Ai (m | mHa) | | | | | |
| | Power Steering Flu | - | 19562.6005 | | 100.698 | 1 | | 113.8539 | ····· | | | | | |
| Kp (product factor) | | 1 | 10002.0000 | - | 100.000 | - | - | 100.0000 | | | | | | |
| | | - | | | | | | | | | | | | |
| Month | | Jan | Feb | Mar Ap | r | May | Jun | Jul . | Aug | Sep | Oct I | vov | Dec | |
| Q | (gal) | 59.2822 | 53.5452 | 59.2822 | 57.3699 | 59.2822 | 57.3699 | 59.2822 | 59.2822 | 57.3699 | 59.2822 | 57.3699 | 59.2822 | 698.0002 (sum) |
| Vq | (ft^3) | 7.9249 | 7.158 | 7.9249 | 7.6692 | 7.9249 | 7.6692 | 7.9249 | 7.9249 | 7.6692 | 7.9249 | 7.6692 | 7.9249 | 93.3091 (sum) |
| N (period) | (number) | 0.0112 | 0.0101 | 0.0112 | 0.0109 | 0.0112 | 0.0109 | 0.0112 | 0.0112 | 0.0109 | 0.0112 | 0.0109 | 0.0112 | 0.1321 (sum) |
| N (scaled to annual) | (number) | 0.1321 | 0.1321 | 0.1321 | 0.1321 | 0.1321 | 0.1321 | 0.1321 | 0.1321 | 0.1321 | 0.1321 | 0.1321 | 0.1321 | |
| Kn | (number) | 1 | . 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (avg) |
| Days | (number) | 31 | 28 | 31 | 30 | 31 | 30 | 31 | 31 | 30 | 31 | 30 | 31 | 365 (sum) |
| | | | | | | | | | | | | | | |
| Compound Molecular Wo | | | | | | | | | | | | | | |
| Power Steering Fluid | (Mv) | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 (lb/lb-mol |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Working Loss Calculation | s (Uncontrolled) | | | | | | | | | | | | | |
| kb | (number) | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| kn | (number) | 1 | | | 1 | 1 | 1 | | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| n | (number) | 0.0112 | 0.0101 | 0.0112 | 0.0109 | 0.0112 | 0.0109 | 0.0112 | 0.0112 | 0.0109 | 0.0112 | 0.0109 | 0.0112 | 0.1321 (sum) |
| | | | | | | | | | | | | | | |
| Compound Vapor Density | / (vW(i)) | | | | | | | | | | | | | |
| Power Steering Fluid | (lb/ft^3) | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 (avg) |
| | | | | | | | | | | | | | | |
| Working Losses (Lw) | | | | | | | | | | | | | | |
| Air | (lb) | 0.3139 | | | 0.3037 | 0.3139 | 0.3037 | | 0.3139 | 0.3037 | 0.3139 | 0.3037 | 0.3139 | 3.6956 (sum) |
| Power Steering Fluid | (lb) | 0.3709 | 0.335 | 0.3709 | 0.3589 | 0.3709 | 0.3589 | 0.3709 | 0.3709 | 0.3589 | 0.3709 | 0.3589 | 0.3709 | 4.3669 (sum) |
| | | | | | | | | | | | | | | |
| Total Losses (Lt) | <i>(</i> 1 ,) | | | | | | | | | o oor- | | | 0.040- | 0.0000 (|
| Air Barra Chandra Fluid | (lb) | 0.3139 | | | 0.3037 | 0.3139 | 0.3037 | | 0.3139 | 0.3037 | 0.3139 | 0.3037 | 0.3139 | 3.6956 (sum) |
| Power Steering Fluid | (lb) | 0.3709 | 0.335 | 0.3709 | 0.3589 | 0.3709 | 0.3589 | 0.3709 | 0.3709 | 0.3589 | 0.3709 | 0.3589 | 0.3709 | 4.3669 (sum) |
| | | | | | | | | | | | | | | 4.3669 |
| | | | | | | | | | | | | | | 4.3007 |

| a sali da a Tial a | TK TO 4 The second O | | | a /2024 += 4 | 2 (24 /2024 | | | | | | | | | |
|-----------------------------|---------------------------|----------------|--------------------|--------------|---------------|--------|---------|------------|---------|---------|---------|---------|---------|-------------------|
| Activity Title Climate: | TK-TO4 Thermal Oi N/A | i Expansion | Iank From 1/ | 1/ 2021 to 1 | 2/31/2021 | | | | | | | | | |
| | N/A | | | | | | | | | | | | | |
| pa Equipment Tag | TK-TO4 Thermal Oi | il Evenneine 1 | Tank | | | | | | | | | | | |
| Storage Vessel Style | Horizontal Storage | | | | | | | | | | | | | |
| Calculation Type | Isothermal Storage | | 10 Pov) | | | | | | | | | | | |
| Calculation Type | Working Loss Calcu | | Ta Ken' | | | | | | | | | | | |
| Void Space Volume | 2096.26 gal | liation | | | | | | | | | | | | |
| Working Volume | - | | | | | | | | | | | | | |
| Working Volume | 1928 gal 257.7361 ft^3 | | | | | | | | | | | | | |
| Shell Diameter | 5.249 ft | | | | | | | | | | | | | |
| Straight Side Height | 12.95 ft | | | | | | | | | | | | | |
| Paint Solar Absorptance | 0.2 | F | | | | | | | | | | | | |
| Roof Color / Condition | white / average | 5 | | | | | | | | | | | | |
| Shell Color / Condition | white / average | | | | | | | | | | | | | |
| pbp | | 0 | | | | | | | | | | | | |
| pbp pbv | | 0 | | | | | | | | | | | | |
| Equipment Comment | | • | | | | | | | | | | | | |
| Activity Comment | Imported from Exc | al on 2:EE:Ef | DM E/10/7 | ררו | | | | | | | | | | |
| Pi (constant) | 3.141 | |) F IVI, 3/ 13/ 20 | <i>i</i> . | | | | | | | | | | |
| R (constant) | 998. | | | | | | | | | | | | | |
| R (Constant) | 556. | 3 | | | | | | | | | | | | |
| Vessel Contents | 1048 130 m | al 392.000 °F | 7773 658 lb | | 39.757 lb-M | | | | | | | | | |
| Mixture Name: | Mixture | 1 332.000 1 | //23.000 10 | | 33.737 10-141 | | | | | | | | | |
| WIALLIE Maine. | [Liquid] | mmHg | lb | W[i] | lb-M | X[i] | A[i] | X*Pi*Ai (m | mHa) | | | | | |
| | Power Steering Flu | - | 7723.6577 | 1 | | | | 113.8539 | ыБ/ | | | | | |
| Kp (product factor) | | 1 110.0000 | //20.00/// | - | 33.7575 | - | - | 115.0005 | | | | | | |
| Kp (product factor) | | 1 | | | | | | | | | | | | |
| Month | | Jan | Feb | Mar | Apr | May | Jun | Jul | Aug | Sep | Oct | Nov | Dec | |
| Q | (gal) | 59,2822 | | | | - | 57.3699 | | 59.2822 | 57.3699 | 59.2822 | 57.3699 | 59,2822 | 698.0002 (sum) |
| Va | (ft^3) | 7.9249 | | | | | 7.6692 | | 7.9249 | 7.6692 | 7.9249 | 7.6692 | 7.9249 | 93.3091 (sum) |
| N (period) | (number) | 0.0307 | 0.0278 | 0.0307 | 0.0298 | 0.0307 | 0.0298 | 0.0307 | 0.0307 | 0.0298 | 0.0307 | 0.0298 | 0.0307 | 0.3619 (sum) |
| N (scaled to annual) | (number) | 0.362 | | | | | 0.362 | | 0.362 | 0.362 | 0.362 | 0.362 | 0.362 | |
| Kn | (number) | 1 | | | | | 1 | | 1 | 1 | 1 | 1 | 1 | 1 (avg) |
| Days | (number) | 31 | | | | | 30 | | 31 | 30 | 31 | 30 | 31 | 365 (sum) |
| 1* | (| | | | | | | | | | | | | |
| Compound Molecular Wo | eights (Ib/Ib-M) | | | | | | | | | | | | | |
| Power Steering Fluid | (Mv) | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194.27 | 194,27 | 194.27 | 194.27 (lb/lb-mol |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | |
| Working Loss Calculation | | | | | | | | | | | | | | |
| kb | (number) | 1 | | | | | 1 | | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| kn | (number) | 1 | | | | | 1 | | 1 | 1 | 1 | 1 | 1 | 1 (average) |
| n | (number) | 0.0307 | 0.0278 | 0.0307 | 0.0298 | 0.0307 | 0.0298 | 0.0307 | 0.0307 | 0.0298 | 0.0307 | 0.0298 | 0.0307 | 0.3619 (sum) |
| | | | | | | | | | | | | | | |
| Compound Vapor Density | | | | | | | | | | | | | | |
| Power Steering Fluid | (lb/ft^3) | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 | 0.0468 (avg) |
| Westine Leases (Lud | | | | | | | | | | | | | | |
| Working Losses (Lw) | (11-) | | 0.00 | | | | | | | 0.000- | 0.0455 | o 007- | 0.04.05 | 0.0050 (|
| Air | (lb) | 0.3139 | | | | 0.3139 | 0.3037 | 0.3139 | 0.3139 | 0.3037 | 0.3139 | 0.3037 | 0.3139 | 3.6956 (sum) |
| Power Steering Fluid | (lb) | 0.3709 | 0.335 | 0.3709 | 0.3589 | 0.3709 | 0.3589 | 0.3709 | 0.3709 | 0.3589 | 0.3709 | 0.3589 | 0.3709 | 4.3669 (sum) |
| T-1-11 /14) | | | | | | | | | | | | | | |
| Total Losses (Lt) | /IL-1 | 0 26 20 | 0 202- | 0.0470 | 0 200- | 0 2420 | 0 200- | 0 2400 | 0.0400 | 0 200- | 0.2400 | 0 202- | 0 24 20 | 2 5055 (|
| Air Dewer Steering Fluid | (lb) | 0.3139 | | | | 0.3139 | 0.3037 | 0.3139 | 0.3139 | 0.3037 | 0.3139 | 0.3037 | 0.3139 | 3.6956 (sum) |
| Power Steering Fluid | (lb) | 0.3709 | 0.335 | 0.3709 | 0.3589 | 0.3709 | 0.3589 | 0.3709 | 0.3709 | 0.3589 | 0.3709 | 0.3589 | 0.3709 | 4.3669 (sum) |
| | | | | | | | | | | | | | | 4.3669 |
| | | | | | | | | | | | | | | 4.3002 |